

# 1 Anaerobic biotransformation of nitroanilines enhanced by the 2 presence of low amounts of carbon materials

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9

## 10 Abstract

11 Three microporous activated carbons -original (AC<sub>0</sub>), chemical oxidized with HNO<sub>3</sub>  
12 (AC<sub>HNO3</sub>) and thermal treated (AC<sub>H2</sub>)-, and three mesoporous carbons - xerogels (CXA  
13 and CXB) and nanotubes (CNT)-, were tested on the biological reduction of *o*-, *m*- and  
14 *p*-nitroaniline (NoA) at a concentration above the half maximal inhibitory concentration  
15 (IC<sub>50</sub>) for a methanogenic consortium degrading a mixture of volatile fatty acids (VFA)  
16 containing acetate, propionate and butyrate. NoAs were only partially reduced in the  
17 absence of carbon materials (CM). Rates were dependent on the nitro group position,  
18 increasing in the order *meta*>*para*>*ortho*. CM lead to NoAs almost total reduction and  
19 at higher rates. With AC<sub>0</sub> and AC<sub>H2</sub>, rates increased 3-fold, 4-fold and 8 fold for *o*-, *m*-  
20 and *p*-NoA, respectively.

21

22 *Keywords*: anaerobic bioreduction; activated carbon; carbon nanotubes, carbon xerogel,

23 nitroanilines.

## 24 **Introduction**

25 NoAs are commonly used in the industrial production of pharmaceuticals and synthetic  
26 dyes originating contaminated wastewaters (Harter, 1985). They have also been  
27 reported as products of anaerobic reduction of azo dyes (Donlon et al., 1997; Garrigós et  
28 al., 2002) and explosives (Spain, 1995). In soils, herbicide microbial degradation also  
29 originates nitroanilines. They are categorized as toxic and mutagenic substances and  
30 concern on their removal is logic (Malca-Mor and Stark, 1982; Chung et al., 1997).  
31 Some published results on biological degradation of NoAs under anaerobic conditions  
32 have shown their transformation via reduction of the nitro group, forming nitroso and  
33 hydroxylamino intermediates to the corresponding amines, through a six-electron  
34 transfer mechanism donated by co-substrates (Spain, 1995; Razo-Flores et al., 1997a).  
35 However, NoAs biological reduction has been described as proceeding at very low rates  
36 and/or need acclimatized biomass (Saupe, 1999; Khalid et al., 2009). Redox mediators,  
37 compounds that can be reversibly oxidized and reduced, shuttling the electrons from a  
38 co-substrate to the organic compound to be degraded, can help as electron carriers,  
39 increasing the rates of biotransformation of contaminants (Van der Zee and Cervantes,  
40 2009). This is very important for the efficient operation of advanced biological reactors  
41 with granular anaerobic sludge, such as the upflow anaerobic sludge bed (UASB), on  
42 organic compounds removal, as the electron transfer limitations can lead to poor  
43 performance (need of long hydraulic retention times to reach a satisfactory extent) or  
44 even collapse of anaerobic reactors (Cervantes et al., 2001). Insoluble CM have been  
45 shown as a feasible redox mediators for the microbial reduction of azo dyes presenting  
46 advantages in comparison with soluble quinones, such as their easier removal from the  
47 medium and the no need of continuous addition (Van der Zee et al., 2003; Pereira et al.,  
48 2010; Pereira et al., 2014). Besides, CM can be modified in order to gain advantage of  
49 their unique specific proprieties (Figueiredo et al., 1999; Pereira et al., 2010;  
50 Amezquita-Garcia et al., 2013).

51 In the present study, different CM, including microporous ( $AC_0$ ,  $AC_{HNO_3}$  and  $AC_{H_2}$ )  
52 and mesoporous CM (CX, CNT) were explored for the first time as redox mediators on  
53 the anaerobic biological reduction of nitroanilines. Three NoAs differing only in the  
54 position of nitro group, *ortho*, *meta* and *para* (*o*-, *m*- and *p*-NoA) were tested. The  
55 potential toxic effect of NoA and final degradation products was evaluated for a  
56 methanogenic consortium degrading VFA.

57

## 58 **Experimental**

59

### 60 **Chemicals**

61 *o*-NoA (98%), *m*-NoA (98%), *p*-NoA (>99%), *m*-phenylenediamine (*m*-Phe, 98%), *p*-  
62 phenylenediamine (*p*-Phe, 98%) were purchase from Sigma. Acetonitrile (ACN) was  
63 purchased from Panreac at HPLC analytic grade.

64

### 65 **Preparation and Characterization of Carbon Materials**

66 Microporous CM comprise the commercial NoritROX0.8  $AC_0$  and two samples with  
67 different chemical composition on the surface, maintaining the original textural  
68 properties, prepared from chemical ( $AC_{HNO_3}$ ) and thermal ( $AC_{H_2}$ ) treatment of  $AC_0$ . As  
69 mesoporous CM, two CX synthesized by the sol-gel process at pH 6.25 (CXA) and  
70 5.45 (CXB) to obtain materials with different textural properties and a commercial CNT  
71 (Nanocyl 3100, 95%, diameter of 9.5 nm, an average length of 1.5  $\mu$ m) were used.  
72 Preparation and characterisation of tested CM are already described in Pereira et al.  
73 (2010, 2014).

74

## 75 **Biological assays**

76 Biological reduction of nitroanilines was conducted in 70 mL serum bottles, sealed with  
77 a butyl rubber stopper, containing 25 mL of medium. The primary electron donating  
78 substrate of the medium was composed of 2 g L<sup>-1</sup> chemical oxygen demand (COD) of a  
79 NaOH-neutralised volatile fatty acids (VFA) mixture, containing acetate, propionate  
80 and butyrate in a COD based ratio of 1:10:10. Basal nutrients were also added: NH<sub>4</sub>Cl  
81 (2.8 g L<sup>-1</sup>), CaCl<sub>2</sub> (0.06 g L<sup>-1</sup>), KH<sub>2</sub>PO<sub>4</sub> (2.5 g L<sup>-1</sup>), MgSO<sub>4</sub>·7H<sub>2</sub>O (1 g L<sup>-1</sup>). Medium was  
82 buffered at a pH of 7.3 ± 0.2 with NaHCO<sub>3</sub> (2.5 g L<sup>-1</sup>). Anaerobic granular sludge  
83 collected from an anaerobic Internal Circulation reactor of a brewery wastewater  
84 treatment plant was the inoculum at a concentration of 2.5 ± 0.5 g L<sup>-1</sup> volatile suspended  
85 solids (VSS). Nitroanilines were added at the final concentration of 1 mM. The effect of  
86 the different CM on biological reduction was tested at a concentration of 0.1 g L<sup>-1</sup>. This  
87 concentration is in accordance with a previous published work (Pereira et al., 2010) in  
88 which AC concentrations from 0.1 g L<sup>-1</sup> to 0.6 g L<sup>-1</sup> were tested and lead to an increase  
89 of the dye adsorption (from less than 10 % to 65 %), without accelerating the dye  
90 reduction rates, beyond the concentration of 0.1 g L<sup>-1</sup>. These results are important once  
91 activated carbon is costly and therefore the use of low amounts is an advantage for  
92 biological processes application. Furthermore, as a redox mediator, AC is recycled from  
93 its oxidized and reduced states and thus should be effective at low concentrations.  
94 Sludge was incubated overnight at 37 °C in a rotary shaker at 120 rpm. After the pre-  
95 incubation period, NoAs and VFA's (2 gCOD L<sup>-1</sup>) were added with a syringe from the  
96 stock solution to the desired concentration. Controls without CM and without biomass  
97 were also conducted. All experiments were prepared in triplicate.

98

## 99 **Effect of nitroamines and final products on a methanogenic consortium**

100 Serum bottles of 25 mL, containing 12.5 mL of buffer solution with 3.05 g L<sup>-1</sup> sodium  
101 bicarbonate and 1 g L<sup>-1</sup> of Resazurin, were supplemented with 0.4 g anaerobic granular  
102 sludge which corresponds to 2.1 ± 0.2 g of volatile suspended solids (VSS) per litre, and  
103 the headspace was flushed with a mixture of N<sub>2</sub>/CO<sub>2</sub> (80/20 vol/vol). The final pH was  
104 7.2 ± 0.2. Following the addition of 0.125 mol L<sup>-1</sup> Na<sub>2</sub>S, under strict anaerobic  
105 conditions, the flasks were incubated overnight at 37 °C and 120 rpm. After that period,  
106 the mixture of VFA 1:10:10 (acetate, propionate and butyrate as mass of COD) at the  
107 final concentration of 2 gCOD L<sup>-1</sup>, and the solutions to be tested, were added and the  
108 Flasks were maintained at 37 °C and 120 rpm during the entire assay. The pressure was  
109 measured every 60 min by using a hand-held pressure transducer able of measuring a  
110 pressure variation of ± 202.6 kPa (0 to 202.6 kPa) with a minimum detectable variation  
111 of 0.5 kPa, corresponding to 0.05 mL of biogas in a 10 mL headspace. The assay was  
112 finished when the pressure remained stable. 500 µL of sample volume were collected  
113 every day using a gas-tight syringe and methane content of the biogas was measured by  
114 gas chromatography using a Chrompack Haysep Q (80–100 mesh) column (Chrompack,  
115 Les Ulis, France), with N<sub>2</sub> as carrier gas at 30 mL min<sup>-1</sup> and a flame-ionization detector.  
116 Temperatures of the injection port, column, and flame-ionization detector were 110, 35  
117 and 220 °C, respectively. The values of methane production were corrected for the  
118 standard temperature and pressure conditions (STP). In the biodegradability  
119 experiments the methane production was expressed as mg COD-CH<sub>4</sub> g<sub>VSS</sub><sup>-1</sup> day<sup>-1</sup>. In  
120 order to determine the activities, the values of pressure (calibrated as an analogical  
121 signal in mV) were plotted as a function of time and the initial slopes of the methane  
122 were calculated. SMA values were determined dividing the initial slope by the VSS  
123 content of each vial at the end of the experiment and were expressed in mL CH<sub>4</sub> g<sub>VSS</sub><sup>-1</sup>

124 day<sup>-1</sup>. Background methane production due to the residual substrate was subtracted. Test  
125 included series containing increasing NoAs in the range of 0.25 to 1 mM, to evaluate  
126 their effect on the methanogenic consortium activity. The final products of biological  
127 reduction were also tested. Two controls were made in the same conditions, one  
128 containing only VFAs and the other without any substrate (blank assay). All batch  
129 experiments were performed in triplicate. The effect of tested compounds was evaluated  
130 by comparing with the control containing only VFAs.

### 131 132 **Analytical techniques**

133 Reactions were monitored spectrophotometrically in a 96-well plate reader (ELISA BIO-  
134 TEK, Izasa) and by HPLC. NoAs show a yellow colour with maximum wavelengths at  
135 410 for *o*-NoA, 350 for *m*-NoA and 380 nm for *p*-NoA. At select intervals, samples  
136 were withdrawn (300 µL), centrifuged at 5000 rpm for 10 min to remove the biomass  
137 and/or CM and diluted to obtain less than one absorbance unit. The UV-vis spectra  
138 (200–800 nm) were recorded and nitroaniline concentration calculated at  $\lambda_{\max}$ . Molar  
139 extinction coefficients were calculated at  $\lambda_{\max}$ :  $\epsilon_{410\text{ nm}} = 1.345\text{ mM}^{-1}\text{ cm}^{-1}$  for *o*-NoA;  $\epsilon_{350}$   
140  $\text{nm} = 0.582\text{ mM}^{-1}\text{ cm}^{-1}$  for *m*-NoA and  $\epsilon_{380\text{ nm}} = 3.104\text{ mM}^{-1}\text{ cm}^{-1}$  for *p*-NoA. Reduction  
141 extent (RE) was calculated according to equation  $\text{RE} (\%) = [(A_0 - A_t)/A_0] * 100$ , where  
142  $A_0$ , is the absorbance at  $\lambda_{\max}$  at the beginning of incubation and  $A_t$ , the absorbance at  
143  $\lambda_{\max}$  at a selected time (t). First-order reduction rate constants were calculated in  
144 OriginPro 6.1 software, applying the equation  $C_t = C_0 + C_i e^{-kt}$ , where  $C_t$  is the  
145 concentration at time t;  $C_0$ , the offset;  $C_i$ , the concentration at time initial time; k, the  
146 first-order rate constant ( $\text{h}^{-1}$ ) and t, is the accumulated time of the experiment.

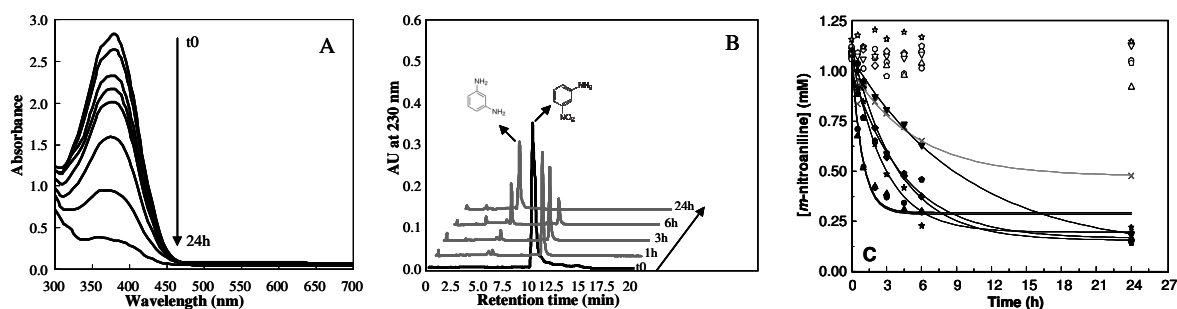
147 HPLC analyses were performed in a HPLC (JASCOAS-2057 Plus) equipped with a  
148 Diode Array Detector detector. A C18 reverse phase Nucleodur MNC18 column  
149 (250x9x4.0 mm, 5 µM particle size and pore of 100 Å from Macherey-Nagel,  
150 Switzerland) was used. Mobile phase was composed of the solvents: A (ultrapure water)  
151 and B (Acetonitrile). Compounds were eluted at a flow rate of 0.5 mL min<sup>-1</sup> and at room  
152 temperature, with isocratic condition containing 50 % of A and 50% of B, during 20  
153 min. Compounds elution was monitored at  $\lambda_{\max}$  of compounds (410, 350 and 380 nm)  
154 and at 230 nm for reduction products (5-ASA and phenylenediamines).

## 155 156 **Results and Discussion**

### 157 158 **Carbon materials as redox mediators on NoA biological reduction**

159 Biological reduction of structurally related NoAs by granular anaerobic biomass and the  
160 effect of different CM as redox mediators was studied and compared. During the  
161 reaction, the yellow colour decreased and, in the presence of CM, the solution turned  
162 colourless. As monitored by spectrophotometry, a decrease of the visible spectra was  
163 observed (fig. 1A). In addition, the reactions were followed by HPLC, by which NoA  
164 and products are separated and can be analyzed individually. Figures 1B show the  
165 HPLC chromatograms for 3-NoA reduction in the presence of AC<sub>H2</sub>. A decrease of the  
166 NoA peak was observed at the maximum wavelength of the NoA. At 230 nm, both NoA  
167 removal and product formation could be monitored, confirming the reduction of the  
168 NoA. As compared with standards, the products of nitroanilines reduction were  
169 identified as the expected products, the correspondent phenylenediamines, which is in  
170 agreement with literature (Razo-Flores et al., 1997b; Razo-Flores et al., 1999; Saupe,  
171 1999; Bhushan et al., 2006). According to previous literature, nitroreductases convert  
172 nitro groups either to nitroso derivatives, hydroxylamines or amines through six  
173 electron successive addition from cosubstrates to nitrocompounds. The high reactivity

174 and instability of nitroso derivatives difficult their detection. The aromatic amines  
 175 formed are usually difficult to be further degraded under the anaerobic conditions,  
 176 however have the possibility, in some cases, to be degraded by following aerobic  
 177 processes (Van der Zee and Villaverde, 2005).  
 178



179  
 180  
 181 **Figure 1.** Biological reduction of *m*-NoA with AC<sub>0</sub> as monitored by UV-vis spectroscopy (A) and HPLC  
 182 (B). First-order rate curves of *m*-NoA biological reduction (C). x, no CM; ●, AC<sub>0</sub>; ▲, AC<sub>H2</sub>; ◆, AC<sub>HNO3</sub>;  
 183 ◆, CXA; ★, CXB and ▼, CNT. Black symbols - biotic and white symbols - abiotic assays.

184  
 185 As observed in figure 1C, NoAs reduction followed first-order kinetics and higher rate  
 186 was obtained for the *m*-NoA which was 2x higher than the obtained for *p*-NoA and 4x  
 187 higher than the obtained for *o*-NoA, revealing the effect of the position of the nitro  
 188 substituents in the molecule. In the absence of CM, the extent of biological reduction in  
 189 the equilibrium (~24h) were 32±1, 56±4 and 52±2, for *o*-NoA, *m*-NoA and *p*-NoA,  
 190 respectively (Table 1).

191  
 192 **Table 1.** Extent (%) and rates (d<sup>-1</sup>) of nitroaniline biological reduction (1 mM), effect of  
 193 different carbon materials (0.1 g L<sup>-1</sup>). Controls without biomass reveal that any  
 194 adsorption to carbon materials occurs (data not shown).

Condition	<i>o</i> -NoA		<i>m</i> -NoA		<i>p</i> -NoA	
	(%)	(h <sup>-1</sup> )	(%)	(h <sup>-1</sup> )	(%)	(h <sup>-1</sup> )
Control	32 ± 1	0.07 ± 0.01	56 ± 4	0.26 ± 0.11	52 ± 2	0.14 ± 0.02
AC <sub>0</sub>	97 ± 2	0.15 ± 0.02	98 ± 1	1.14 ± 0.04	89 ± 1	1.05 ± 0.01
AC <sub>H2</sub>	97 ± 3	0.22 ± 0.03	97 ± 1	1.12 ± 0.01	92 ± 1	0.96 ± 0.04
AC <sub>HNO3</sub>	94 ± 1	0.10 ± 0.03	95 ± 1	0.23 ± 0.01	94 ± 1	0.18 ± 0.01
XA	93 ± 2	0.10 ± 0.01	94 ± 1	0.22 ± 0.03	93 ± 1	0.14 ± 0.01
XB	91 ± 1	0.09 ± 0.01	92 ± 1	0.36 ± 0.01	91 ± 1	0.15 ± 0.01
CNT	94 ± 6	0.10 ± 0.01	91 ± 1	0.10 ± 0.01	93 ± 2	0.07 ± 0.01

195  
 196 Similar results were obtained for the bioreduction of *o*-, *m*- and *p*-nitroaniline reduction  
 197 in samples of the river Elbe (Börnack et al., 2001). The effect of CM on extent and rates  
 198 of NoAs reduction is also set in table 1. All the tested CM improved the extent and rate  
 199 of NoAs reduction, demonstrating their effect as redox mediators. Almost total  
 200 reduction was obtained in the presence of CM. Comparing the different carbon

201 materials, higher reduction rates were obtained with the microporous samples AC<sub>0</sub> and  
202 AC<sub>H2</sub>, leading to an improvement of 3-fold, 4-fold and 8-fold higher for *ortho*, *meta*,  
203 and *para* NoA, respectively, as compared with the reaction in the absence of CM. In  
204 previous results with azo dyes, better performance was achieved with the mesoporous  
205 carbon materials, explained by the easier access of the larger molecules of the dye to the  
206 internal surface of the catalyst. NoAs are smaller molecules and, the better results with  
207 the microporous materials might be related with higher surface area of these materials  
208 instead of the size of the porous. Similarly to the known redox mediator anthraquinone-  
209 2,6-disulfonate (AQDS), the effect as redox mediator of activated carbon has been  
210 attributed to the quinone groups on its surface (Van der Zee et al., 2003). In this study,  
211 comparing between the three samples of microporous activated carbon, better results  
212 were obtained with AC<sub>0</sub> and AC<sub>H2</sub> than with the AC<sub>HNO3</sub> sample. In fact, in spite of the  
213 higher amount of quinone groups in AC<sub>HNO3</sub> compared to the other samples, its effect is  
214 surpassed by the large amount of carboxylic acids and anhydrides also present in this  
215 sample, which are electron withdrawing groups. In a previous work, thermal  
216 modification of AC surface chemistry improved its capacity as redox mediator for azo  
217 dye reduction, which was related with the a high content of electron rich sites on their  
218 basal planes ( $\pi$  electrons), known to be active sites, and by a low concentration of  
219 electron withdrawing groups (Pereira et al., 2010). Sample AC<sub>H2</sub> has the advantage of  
220 keeping some of the quinone groups without the presence of the oxygen-containing  
221 acidic groups (removed during the thermal treatment). Other characteristic of the  
222 activated carbon materials involved is their pH<sub>pzc</sub>. Due to activated carbon amphoteric  
223 character, when in solutions at pH below their pH<sub>pzc</sub> it became positively charged and at  
224 pH above the pH<sub>pzc</sub>, negatively charged. Therefore, at pH 7 AC<sub>0</sub> and AC<sub>H2</sub> are  
225 positively charged and AC<sub>HNO3</sub> negatively charged. NoAs are ionisable organic  
226 compounds, they can exist either as nondissociated or dissociated species in aqueous  
227 phase, depending on the solution pH in relation to their dissociated constants (pKa).  
228 Once the pKa of *o*-, *m*- and *p*-NoA are -0.28, 2.45 and 0.98, respectively (Yang et al.,  
229 2008), in solution at pH 7, deprotonation will occur generating the NoA correspondent  
230 anions. The electrostatic attraction forces between the positively charged carbons and  
231 the negatively charged NoA will be favourable to the electron shuttling.  
232 Contrarily to our results, Amesquita-Garcia et al. (2013) investigating the redox  
233 mediator effect of activated carbon fibres, original, chemical oxidized and thermal  
234 treated, on 4-nitrophenol and 3-chloronitrobenzene chemical (Na<sub>2</sub>S) reduction, have  
235 concluded that activated carbon fibres chemically oxidized are better redox mediators  
236 due to the increased number of quinone groups. Liu et al. (2012), have discussed about  
237 the mechanism of methanogenesis stimulation by activated carbon in methanogenic  
238 digesters, the possibility of favouring the direct interspecies electron transfer (DIET)  
239 under anaerobic conditions between bacteria and methanogens and the role of AC  
240 surface quinone groups. Authors have demonstrated that activated carbon could  
241 accelerate the DIET between *Geobacter metallireducens* and *Geobacter sulfurreducens*  
242 or *Geobacter metallireducens* and *Methanosarcina barkeri*. Studies using AQDS  
243 instead of AC put aside the potential responsibility of quinone groups and lead authors  
244 to consider, instead, the possible contribution of AC high conductivity enabling  
245 electrical connections between microorganisms. Consequently, the investment of the  
246 cells on metabolic energy in producing conductive pili and the additional cytochromes  
247 that are required for the DIET in the absence of AC is reduced.

## 248 249 **Effect of nitroanilines and final reduction products on methanogenic consortium** 250

251 The inhibitory effects of the three NoAs and their reduction products on the activity of  
 252 acetoclastic methanogenic bacteria were evaluated (table 2). The results revealed that  
 253 the concentrations of compounds tested in biological assays were above the IC<sub>50</sub>, which  
 254 may also explain the low extent of reduction in the absence of CM. Among the NoAs,  
 255 similarly to the biological reduction results, the position of the nitro group had an effect  
 256 on methanogenic activity and a notorious higher toxic effect was observed for *o*-NoA.  
 257 The IC<sub>50</sub> for *ortho* substituted NoA was 0.23 mM and for *meta* and *para* substitutions  
 258 was 0.67 mM and 0.51 mM, respectively. The lower reduction obtained for *o*-NoA  
 259 among the NoA tested, in all the tested conditions, may also be due to its higher toxic  
 260 effect on methanogenic consortium. Reduction products of NoA biotransformation in  
 261 the presence of AC<sub>H2</sub> was also evaluated and up to 77 % of detoxification was obtained.  
 262 The results obtained are in accordance with literature reporting that aromatic nitro-  
 263 substituents are responsible for severe methanogenic toxicity, while correspondent  
 264 aromatic amines present lower toxic effects (Donlon et al., 1997; Razo-Flores et al.,  
 265 1997a).

266

267

268 **Table 2.** Potential toxic effect on acetoclastic methanogenic bacteria degrading VFA.

Chemical	Concentration (mM)	Activity (mLCH <sub>4</sub> @PTN gVSS <sup>-1</sup> d <sup>-1</sup> )	IC <sub>50</sub> (mM)
<i>o</i> -NoA	0.00	161.5 ± 10.1	0.23
	0.25	73.6 ± 0.6	
	0.50	26.1 ± 1.3 *	
	1.00	0	
<b>Products of <i>o</i>-NoA bioreduction</b>		124.7 ± 6.0	N.a.
<i>m</i> -NoA	0.00	157.0 ± 9.31	0.67
	0.25	123.7 ± 8.0	
	0.50	108.8 ± 10.5	
	1.00	35.9 ± 1.72 *	
<b>Products of <i>m</i>-NoA bioreduction</b>		107.7 ± 3.2	N.a.
<i>p</i> -NoA	0.00	129.2 ± 3.0	0.51
	0.25	84.3 ± 4.6	
	0.50	48.3 ± 1.5	
	1.00	18.4 ± 2.5	
<b>Products of <i>p</i>-NoA bioreduction</b>		98.0 ± 0.2	N.a.
MY1	control	199.1 ± 10.1	0.44
	0.125	162.9 ± 15.2	
	0.25	129.9 ± 9.9	
	0.50	69.9 ± 4.6	
	1.00	0	
<b>Products of MY1 bioreduction</b>		190.3 ± 5.3	N.a.
5-ASA	Control	178.8 ± 14.5	2.0
	0.20	157.4 ± 4.2	
	0.40	167.1 ± 7.9	
	0.80	147.3 ± 6.9	
	1.00	118.3 ± 1.3	
	2.00	47.1 ± 1.4	
	4.00	0	

269

N.a. - not applicable; \* \*, Metanogenic activity calculated after 1 day lag phase.

270 **Conclusions**

271 The efficiency of microporous ( $AC_0$ , and  $AC_{HNO_3}$ ,  $AC_{H_2}$ ) and mesoporous carbon  
272 materials (CXA, CXB and CNT) as redox mediators on isomeric NoAs reduction was  
273 compared. Rates were dependent on the nitro group position, increasing in the order  
274 *meta>para>ortho*. The presence of CM increases both the extent and the rates of  
275 compounds bioreduction. The surface area of carbon materials had greater responsibility  
276 than the pore sizes, with better results obtained for  $AC_0$  and  $AC_{H_2}$ . The  $pH_{pzc}$  of the  
277 materials is also an important factor on reduction reactions, and at pH 7 the electrostatic  
278 attraction between the positively charged carbons  $AC_0$  and  $AC_{H_2}$ , and the NoA anions  
279 favors the electron transfer. The high extent of compounds reduction in the presence of  
280 CM even when present at toxic levels to the methanogenic consortium, and the  
281 detoxification obtained with the mediated treatment, demonstrates the effectiveness of  
282 the process and their promising application in continuous high rate bioreactors

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