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Features of the power-law fluid over cylinders in a channel *via* gap aspects: Galerkin finite element method (GFEM)-based study

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The goal of this investigation is to carry out a comprehensive analysis of hydrodynamic forces, with particular attention being paid to the power-law fluid flow across cylinders and presence gap considerations. With the assistance of the Galerkin finite element method (GFEM), the discretization of the two-dimensional system of non-linear partial differential equations was successfully completed. The research is carried out with a significant variance of the flow behavior index (*n*) from .3 to 1.7, gap aspects (G_p) from 0 .0 to .3, and fixed Reynolds number (Re) 20. To obtain an extremely accurate solution, first, a coarse hybrid computational mesh needs to be developed, and then, more refinement must take place. The selection of the best possible case can be determined by comparing flow patterns, coefficients of drag and lift, and cylinder gaps. The shear-thickening behavior of fluids has a substantially greater influence on the drag characteristics than either the Newtonian or the shear-thinning behavior of fluids do. In addition to this, the shear-thickening action causes the upstream obstacle's drag coefficient to increase because the gap spacing becomes more widespread.

KEYWORDS

GFEM, power-law fluid, hydrodynamic forces, gap spacing, cylinders

1 Introduction

Non-linear fluids past over cylinders are being studied by many researchers over the years. Engineering applications are designed and later modified based on the study of hydrodynamic forces and flow configurations. Product qualities are being improved by deep and modified investigations over the years. Flow patterns and their impact are also being investigated around more than one bluff body. It is also significant to note that the arrangement/placement of obstacles in the cross-flow also plays an important role and has a practical use. Extensive work conducted on the non-Newtonian fluid flow around a single cylinder has been summarized in the previous work [1–7]. This work is aimed to increase the stage of complicatedness concerning the nature of fluid and the number of obstacles to investigate the influence of hydrodynamic forces like drag and lift while changing the gap spacing around the circular cylinders in the power-law fluid. Lesser work is available in the literature on the incompressible power-law fluid flowing over cylinders, many investigations into non-Newtonian fluids are available [8–12].



TABLE 1 Code validation test compared to Majeed et al. [30-36].

	Majeed et al. [30–36]	Single cylinder
C_D	5.5785	5.5785
C_L	.0106	.0106

The flow around two side-by-side circular cylinders and tandem arrangements of circular cylinders simulated the results for different Reynolds numbers. Using several modeling methodologies based on a computational fluid dynamics solver, the authors suggest that the impacts of flow patterns such as the frequency of primary vortex shedding and the frequency of the secondary cylinder interaction may be seen for flow around two rows of staggered cylinders. The behavior of Reynolds numbers and gap spacing for the flow that occurs between side-by-side cylinders can be found using a numerical study [13–16]. These researchers investigated not only the effects of different gap spacings and Reynolds numbers but also the distinct flow patterns. [17] investigated the characteristics of flow behaviors and the action of fluid forces on two cylinders with a range of staggered configurations.

A lot of computational work has been conducted to investigate drag and lift forces on obstacles in the Newtonian flow field, but analyzing the influence of non-linear viscosity functions on drag and lift is still in its embryonic stage. Because of the examination of a wake, recycling zone length, and drag and lift features, the flow of incompressible flows over cylinders of varied cross-sectional areas makes for an attractive field of study. [18] investigated numerically the effects of the drag component on a heated circular cylinder for Reynolds number $(5 \le \text{Re} \le 50)$. Determining solutions in the field of rheological fluid is a struggling mission for scientists because the study of flow behaviors around the obstacles with the influence of force parameters (drag and lift) has established the attention of scholars over an insufficient decade [19-21]. [22] analyzed numerically the influence of viscous fluid flows past confined cylinders using the LBM algorithm and also studied the effects of drag components of the cylinders. [23] offered an investigation of the laminar flow and heat transmission that was caused by a long circular cylinder that was either horizontal or vertical. The properties of MHD heat transport in a cavity were studied by [24, 25], who used the Galerkin finite element technique in their research. In addition, there is a general upward tendency in the average Nusselt number along the bottom wall of the tank and the right wall. There have been some interesting advancements in our understanding of the non-linear fluid flow recently, and they can be seen in [26-28].



The purpose of this investigation is to compute the fluid forces based on gap aspects that are exerted over an obstacle that is submerged in a power-law fluid flow. The CFD community has not previously conducted such an analysis of forces in this domain. In view of the numerous commercial uses of flow around dual cylinders, the scope of this work has been narrowed to include only some numerical results. The results of the circular cylinder are used as a point of comparison in this section. The following is the structure of this paper: the mathematical formulation is the topic of discussion in Section 2. In Sections 3 and 4, we will investigate the influence that the computing domain has and the effect that the grid points have. In Section 5, we talk about how the spacing ratio affects the aerodynamic forces, and in Section 6, we present our findings and draw some conclusions.

2 Mathematical formulation

The continuity and momentum equations for the incompressible shear rate model are given in their compact form and are written as follows [31]:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} = 0, \tag{1}$$

$$u\frac{\partial u}{\partial x} + v\frac{\partial u}{\partial y} + \frac{\partial p}{\partial x} = \frac{1}{Re} \left(\frac{\partial \tau_{xx}}{\partial x} + \frac{\partial \tau_{xy}}{\partial y} \right), \tag{2}$$

$$u\frac{\partial v}{\partial x} + v\frac{\partial v}{\partial y} + \frac{\partial p}{\partial y} = \frac{1}{Re} \left(\frac{\partial \tau_{yx}}{\partial x} + \frac{\partial \tau_{yy}}{\partial y} \right), \tag{3}$$



FIGURE 3

Sequence of grids on the space mesh level: 1, 2, and 3 (from left to right).

Level	#. EL	DOF	Level	#. EL	DOF
1	662	1758	1	686	1806
2	1202	2964	2	1230	2988
3	1954	4458	3	1970	4434
4	3928	8196	4	3982	8169
5	5972	11814	5	5958	11655
6	10762	19722	6	10802	19584
7	25316	45720	7	30544	53034
8	62723	109302	8	63143	108654
9	118088	192414	9	117698	190551
$G_p = 0.0$			$G_p = 0.1$		
Level	#. EL	DOF	Level	#. EL	DOF
Level	#. EL 686	DOF 1806	Level	#. EL 694	DOF 1818
Level 1 2	#. EL 686 1270	DOF 1806 3048	Level 1 2	#. EL 694 1260	DOF 1818 3033
Level 1 2 3	#. EL 686 1270 1990	DOF 1806 3048 4464	Level 1 2 3	#. EL69412602024	DOF 1818 3033 4515
Level 1 2 3 4	#. EL 686 1270 1990 4032	DOF 1806 3048 4464 8244	Level 1 2 3 4	#. EL 694 1260 2024 4034	DOF 1818 3033 4515 8247
Level 1 2 3 4 5	#. EL 686 1270 1990 4032 5972	DOF 1806 3048 4464 8244 11676	Level 1 2 3 4 5	#. EL 694 1260 2024 4034 6018	DOF 1818 3033 4515 8247 11745
Level 1 2 3 4 5 6	#. EL 686 1270 1990 4032 5972 10570	DOF 1806 3048 4464 8244 11676 19236	Level 1 2 3 4 5 6	#. EL 694 1260 2024 4034 6018 10800	DOF 1818 3033 4515 8247 11745 19581
Level 1 2 3 4 5 6 7	#. EL 686 1270 1990 4032 5972 10570 25162	DOF 1806 3048 4464 8244 11676 19236 44961	Level 1 2 3 4 5 6 7	#. EL 694 1260 2024 4034 6018 10800 25004	DOF 1818 3033 4515 8247 11745 19581 44724
Level 1 2 3 4 5 6 7 8	#. EL 686 1270 1990 4032 5972 10570 25162 63371	DOF 1806 3048 4464 8244 11676 19236 44961 108996	Level 1 2 3 4 5 6 7 8	#. EL 694 1260 2024 4034 6018 10800 25004 68975	DOF 1818 3033 4515 8247 11745 19581 44724 117402
Level 1 2 3 4 5 6 7 8 9	#. EL 686 1270 1990 4032 5972 10570 25162 63371 117958	DOF 1806 3048 4464 8244 11676 19236 44961 108996 190941	Level 1 2 3 4 5 6 7 8 9	#. EL 694 1260 2024 4034 6018 10800 25004 68975 136230	DOF 1818 3033 4515 8247 11745 19581 44724 117402 218349

TABLE 2 Data on meshes of varying refinement levels.

where

$$\mathbf{\tau} = m \left(\dot{\mathbf{\gamma}} \right)^n,\tag{4}$$

where *m*, *n*, and \dot{y} are the fluid consistency parameter, power law index, and shear rate, respectively. For *n* < 1, the model obtained effects of the shear-thinning fluid, and for *n* = 1, the model decline to Newtonian fluid with constant viscosity. Also, *n* > 1 represented the shear-thickening effects in the model.

The involved non-dimensionalized parameters are

TABLE	3	Grid	convergence	tests.
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Refinement level	C_D	C_L	
L_1	6.8482	.0356	
L_2	6.9111	.0619	
L_3	6.9246	.0706	
L_4	6.9333	.0720	
L_5	6.9347	.0731	
L ₆	6.9359	.0728	
L_7	6.9389	.0726	
L_8	6.9397	.0721	

$$\operatorname{Re} \equiv \frac{\rho U_{ref} L_{ref}}{\mu_{p}},\tag{5}$$

$$C_D \equiv \frac{2F_d}{\rho U^2 D},\tag{6}$$

$$C_L \equiv \frac{2F_l}{\rho U^2 D},\tag{7}$$

where U_{ref} and L_{ref} are the velocity and length reference, and C_D and C_L are the drag and lift coefficient with drag and lift forces denoted by F_d and F_l , respectively.

3 Problem description

Consider a channel of dimensions (0, 0), (2.2, 0), (0, 0.41), and (2.2, 0.41) are defined. The circular obstacle C_1 is located fixed at (.2, .2), and C_2 is placed with various gap spacings. Both the top and bottom walls of the channel are positioned so that u = v = 0. The inlet of the channel is subjected to an inflow parabolic profile with a maximum u velocity at .3, and a do-nothing boundary condition is selected for the outlet.

Let D = 0.1m be the diameter of the obstacles C_1 and C_2 , and also, G_p is a confined space between the obstacles, as shown in Figure 1. This simulation was performed by using H = 4.1D, $L_u = 2D$, L = 4D, and $L_d = 16D$ where L_u and L_d are upstream and downstream distances from the centers of the obstacles to the inflow and outflow edge, respectively. To accurately reflect the hydrodynamic forces acting on the cylinder, additional components surrounding the obstruction are taken into consideration.















4 Numerical approach

At a constant Reynolds number Re = 20, it is well established that viscous fluid flows are laminar, two-dimensional, and characterized by symmetrical vortices and that these flows have a relatively constant shear rate. The numerical technique has been tested to identify the convergency,

accuracy, and consistency of the outputs by evaluating the present study with the literature for viscous fluids. This was conducted in order to determine whether or not the results are convergent, accurate, and reliable.

Table 1 shows the comparison between the past literature and current values for the Newtonian scenario, which is useful for code validation. The quantities of the drag coefficient for a single cylinder are maintained at a constant level of $C_D = 5.5785$. Meshing is a crucial stage initial to set the boundary conditions for simulation because of the influence of convergence, accuracy, and outcome speed. It is fundamental to have a maximum number of cells. The term "meshing" refers to the process of discretizing a boundary with the intention that it enables the creation of well-shaped pieces. The size of the cell has an enormous impact on how accurately iterations are performed. Whenever the size of the cell is reduced, the accuracy rate increases, but this also considerably leads to the maximum amount of time spent computing. It only aids in the process of breaking down a physical domain into a small discrete volume in which sets of equations can be calculated.

The computational coarse level grid for various gap spacings of obstacles is shown in Figure 2. For higher levels of optimization, convert one element into four narrow-size elements. The refinement mechanism is described in Figure 3.

The number of elements and degrees of freedom at various stages of refinement are shown in Table 2, which was created under this method of refinement.

Table 2 contains several different depictions of the domain discretization of a channel that has a couple of cylinders arranged in a tandem configuration. These representations are facilitated at multiple levels of refinement. Based on the data that were examined on the degree of freedom at various $G_p = 0.0$, $G_p = 0.1$, $G_p = 0.2$, and $G_p = 0.3$, it is concluded that for the high-refinement levels, the degree of freedom is 192414 at $G_p = 0.0$, whereas 190551 at $G_p = 0.1$, also 190941 at $G_p =$ 0.2, and 218349 at $G_p = 0.3$ with fixed Re = 20. According to Table 2, when the gap spacing is exceeded, not only does the number of domain elements but also the number of boundary elements grow from $G_p = 0.1$ to $G_p = 0.3$, which is a computed conclusion. The numerical scheme (FEM) for the numerous approximations of the Navier stokes equation with the hybrid grid was generated on a very high refinement level and also criteria of convergence for non-linear iteration, which is already described in [29-36]. Table 3 provides specifics on a number of different meshing levels that can occur in a flow pattern that includes a circular cylinder.

TABLE 4 Influence of the drag coefficient of	ooth cylinders against n with	various gap spacing.
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	$G_p = 0.0$		<i>G_p</i> = 0.1		<i>G_p</i> = 0.2		<i>G_p</i> = 0.3	
n	C 1	C ₂	C ₁	C ₂	C ₁	C ₂	C 1	C ₂
0.3	2.148395	23253	2.461355	.19132	2.838860	.599018	3.204682	.967313
0.5	3.141227	.072459	3.617459	.668107	4.135402	1.194294	4.602818	1.644271
0.7	4.337779	.438113	5.031590	1.242474	5.718024	1.907164	6.274340	2.422002
0.9	5.788294	.917502	6.787747	1.997172	7.680482	2.830688	8.317617	3.404983
1.0	6.641395	1.223230	7.839994	2.479747	8.849523	3.40825	9.520455	4.006838
1.1	7.602101	1.590200	9.037440	3.056645	10.16833	4.082747	10.86232	4.695231
1.3	9.962328	2.578129	12.00952	4.575488	13.36832	5.775786	14.05652	6.364044
1.5	13.18561	4.051716	15.97544	6.704247	17.48291	7.992949	18.08302	8.473910
1.7	17.60160	6.207376	21.27710	9.584699	22.80293	10.83925	23.25284	11.15001

	$G_p = 0.0$		<i>G_p</i> = 0.1		<i>G_p</i> = 0.2		<i>G_p</i> = 0.3	
n	C ₁	C ₂	C ₁	C ₂	C ₁	C ₂	C ₁	C ₂
0.3	.025571	.008874	00762	.011906	.003153	.016973	.003794	.017977
0.5	.051922	.014069	.001657	.022615	.016077	.026787	.012159	.024690
0.7	.088363	.0214	.017863	.035761	.032791	.037726	.019369	.026402
0.9	.143015	.032382	.047741	.054927	.056846	.050756	.037022	.032969
1.0	.181425	.04028	.070730	.068270	.073551	.059099	.048600	.035939
1.1	.230239	.050672	.101146	.084698	.093626	.067930	.062328	.038030
1.3	.367722	.082251	.190430	.125730	.146428	.084085	.103935	.041791
1.5	.565125	.132204	.326787	.170921	.234683	.102181	.194112	.060382
1.7	.803697	.19602	.521362	.214693	.397118	.139750	.378040	.119215

TABLE 5 Influence of the lift coefficient of both cylinders against n with various gap spacing.

5 Results and discussions

(a) Impact on velocity and pressure:

In the present work, the computations of incompressible flow have been carried out for the various quantities of the dimensionless parameters: the power law index, n = 0.5, 1, 1.5, thereby covering all the cases for n < 1, n = 1, and n > 1 while several gaps with fixed Reynolds number Re =20. Taking into account, the gap spacing ratio in the direction of the flow has an effect on the development of gap flow, which is the flow that happens between the two stationary cylinders in combination with a range of gap ratios. This flow can be affected by changing the gap ratios. Characteristics of the fluid flow can be determined inside the domain by conducting an analysis on the velocity profile, pressure field, force components, and the drag and lift coefficients. Figures 4, 5 reveal the impacts of velocity profile and pressure around the surface of confined tandem cylinders for the fluid value of Re and n = 0.5 with the several ratios of gap spacing (G_p) , respectively. There is no pressure on the downstream cylinder at $G_p = 0.0$, but pressure increases downstream due to increasing the gaps between the cylinders. Similarly, the flow pattern inside the cylinders increases for all cases of power law index due to variation of the spacing factor. Figures 6, 7 show the effects of n = 1 fluid with different gap ratios on velocity and pressure field, while in all cases *n*, the pressure is steady at the downstream region, but continuously the steadiness decreases in the downstream region for increasing the gap ratios of the obstacles.

Figures 8, 9 reveal the impact of n = 1.5 on flow patterns for various gap levels with fixed lower Reynolds numbers. Both the velocity field and the pressure field exhibit a considerable flow interaction between the two cylinders in shear-thinning and shear-thickening flow, according to a qualitative analysis of the data. In the case of extremely shear-thinning flow, flow separation did not take place, regardless of the gap spacing values that were used. In the shear-thickening instance, at the lower values of the gap ratios, the wake distraction hypothesis can be seen, as shown in Figures 3–9, when the wake of the upstream cylinder is being stifled as a result of the downstream barrier being so near to it.

(b) Line graph behavior:

Figures 10A–E demonstrate the executed *u*-velocity at several powerlaw indexes. The maximum flow pattern is taken as $U_{\text{max}} = 0.3$, and in the present work also occurs as $U_{mean} = 0.2$. In detail, at x = 0.0 the fluid is initially justified at the inlet of the channel is parabolic behavior. At the center of the cylinders C_1 and C_2 , it can be noticed that the velocity curves at x = 0.2 and x = 0.6, the velocity profile gain large values due to the collision of the fluid with cylinders. For x = 0.4, the impact of cylinders on the fluid reduces. The velocity profile at x = 0.4 is the minimum as the velocity at the center of the cylinders, while at the downstream region, at x = 2.2, the fluid seems low affected by the cylinders, and behavior almost goes to the initial velocity profile.

(c) Impact of drag and lift coefficients.

The influence of the gap ratio between the two tandem circular cylinders is at several Rein terms of force quantities, such as drag (C_D) and lift (C_L) coefficients. Tables 4, 5 reveal the numerous values of benchmark hydrodynamics quantities like drag and lift coefficients across the cylinders C_1 and C_2 . It is found that by increasing both gap ratios and the power-law parameter, both force coefficients upsurge. In the following statistical data, the drag coefficient upstream is greater than the downstream for the fixed Reynolds number (Re = 20), which is an interesting discussion. Table 4 reveals that the values of the parameter of the power law and gap ratio are increasing upstream, and the drag forces over both cylinders are also increasing. Similarly, in Table 5 analysis, the effects of the lift coefficient increase for the increasing power law index, while they decrease for maximum gap ratios at both upstream and downstream obstacles. The numerical values of the lift coefficient for a cylinder C_1 are greater than C_2 for the selected Reynolds number. The maximum value of drag and lift coefficient is 23.25284 and .378040 at upstream; also, for the downstream cylinder, values are 11.15001 and .119215, respectively, acquired at $(n, G_p) = (1.7, 0.3)$, where the flow is fully developed within the gap and the downstream region of the second cylinder.

6 Conclusion

We have used the GFEM to simulate how the power-law fluid flows around obstacles. It has been determined in great detail how much of an impact the flow behavior index and gap spacing have on the drag and lift coefficients of the cylinders. When calculating the drag and lift coefficients across cylinders, it has been discovered that the spacing performs a considerable role in the process. An increase in the gaps causes an increase in the amount of fluid flow that is directed toward the walls of the channel downstream of the obstacles. When there is more space between the cylinders, the pressure on the cylinder that is further downstream will be higher due to stagnation. When looking at any gap spacing, the correlation between the drag and lift coefficients is positive for the upstream cylinder, but when looking at the downstream cylinder, the correlation is negative. When it comes to tandem cylinders, the drag coefficient of both cylinders stays relatively the same even when the case involves shear-thinning.

Data availability statement

The original contributions presented in the study are included in the article/Supplementary Material; further inquiries can be directed to the corresponding authors.

Author contributions

NF and YK was responsible for funding; NF, AHM, and HS computed the results; AM and YK wrote the original draft; NF and HS wrote the review draft; AHM performed modeling; YK contributed to conceptualization; YK, AM, and AHM performed validation.

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Conflict of interest

The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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Nomenclature

u, v velocity component U_{in} inlet velocity U_{ref} reference velocity \dot{y} shear rate p hydrodynamic pressure m viscosity index n power-law index Re Reynolds numberD diameter of the obstacle L_{ref} reference length#EL number of elements# DOF number of degrees of freedom C_D drag coefficient C_L lift coefficient