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CLOSED CO₂ CYCLES IN THE GLASS PRODUCTION

A techno-economic evaluation

DLR: F. Moser, S. Maier, R.-U. Dietrich

HVG: F. Drünert, B. Fleischmann

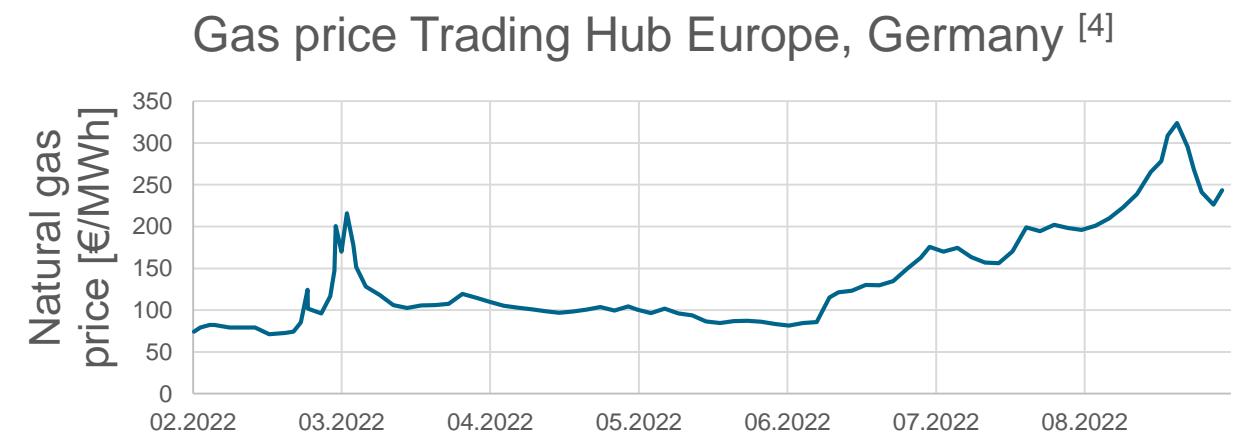
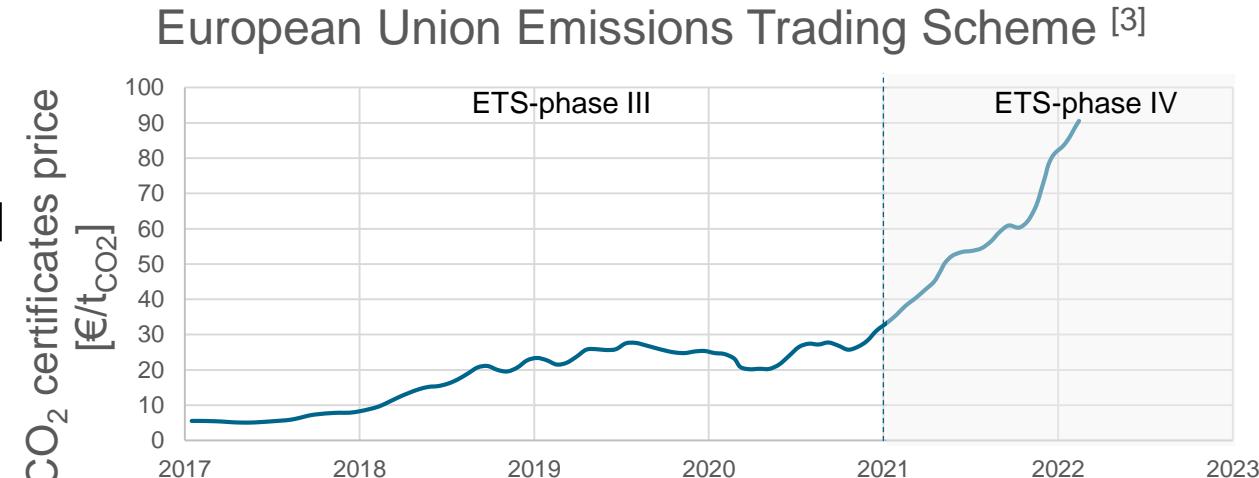


HVG-DGG
Service und Forschung für die Glasherstellung

DLR

Motivation – Demand for greener glass production

- Emissions Europe in year 2020 [1]
 - 3700 million t_{CO₂eq}
- Emissions glass industry in Europe [2]
 - 22 million t_{CO₂}/a
- High specific emissions
 - > 300 kg_{CO₂}/t_{glass}
 - CO₂ certificates started playing a role
- Glass-furnace
 - Up to 85% of the plants energy
- Glass furnace can be turned off ...
 - Natural gas price volatility



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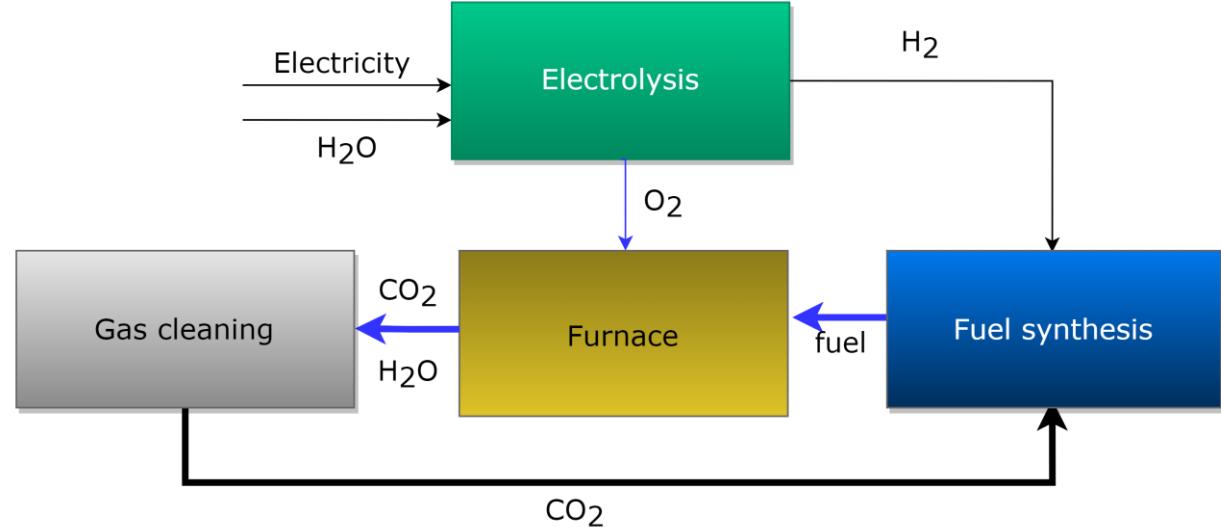


Figure – Carbon Capture and Utilization (CCU) process

[1] <https://www.statista.com/statistics/780410/total-greenhouse-gas-emissions-european-union-eu/>

[2] https://cinea.ec.europa.eu/news-events/news/how-life-reducing-emissions-glass-production-2022-03-16_en

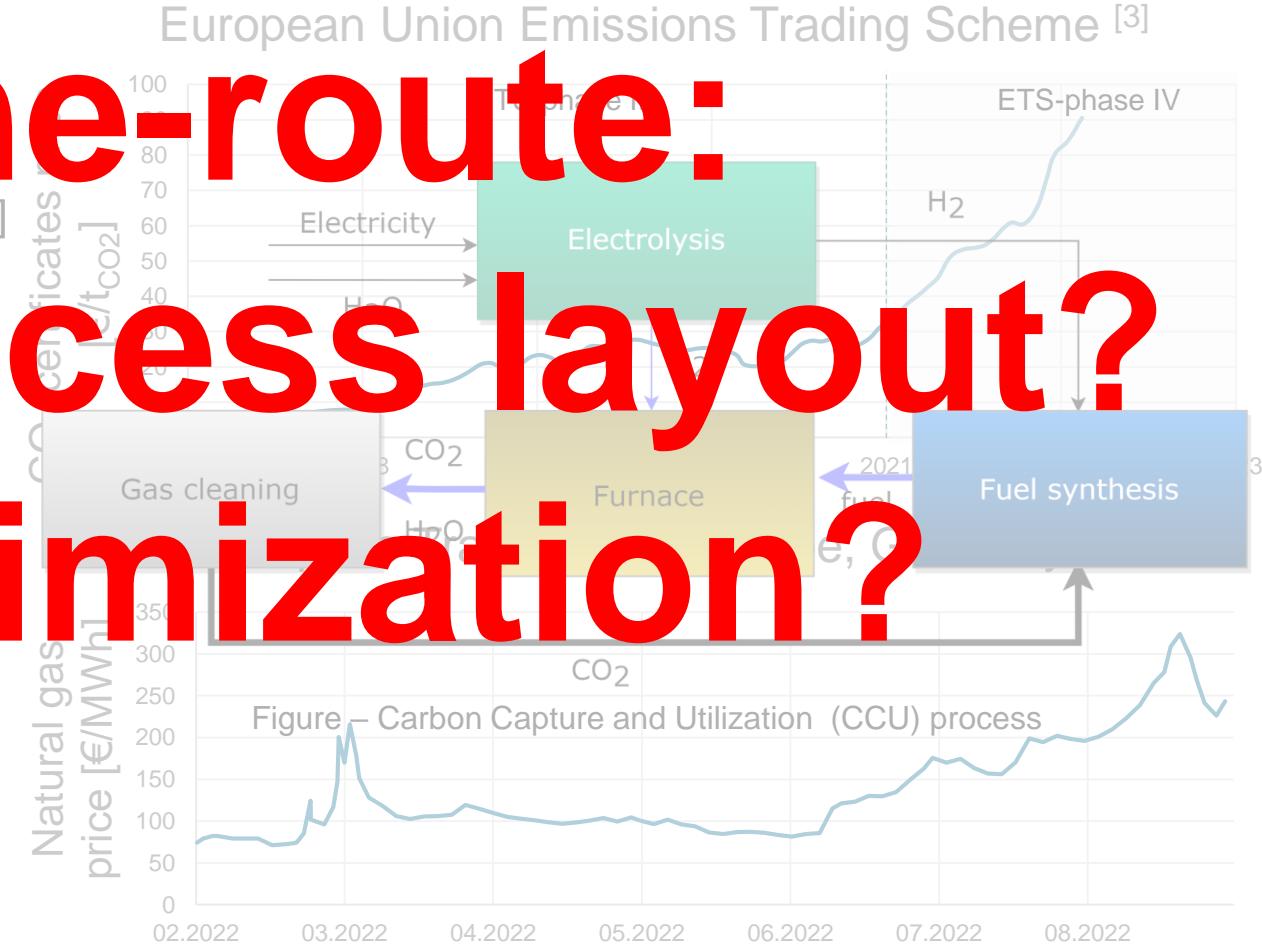
[3] <https://www.next-kraftwerke.com/knowledge/emissions-trading-scheme-ets#phase-iv-2021-to-2030>

[4] https://www.bundesnetzagentur.de/DE/Fachthemen/ElektrizitaetundGas/Versorgungssicherheit/aktuelle_gasversorgung/grafik_gaspreis.html

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Methane-route: Optimal process layout? Cost minimization?



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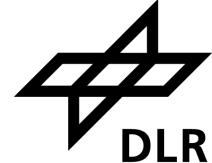
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Agenda



- Motivation
- Objective / Solution
- Methodology
 - Techno- economic assessment
 - Glass furnace specifications
 - Appropriate technologies
 - Economic assumptions
- Results
 - Technical assessment
 - Economic assessment
 - Sensitivity analysis
- Summary
- Outlook

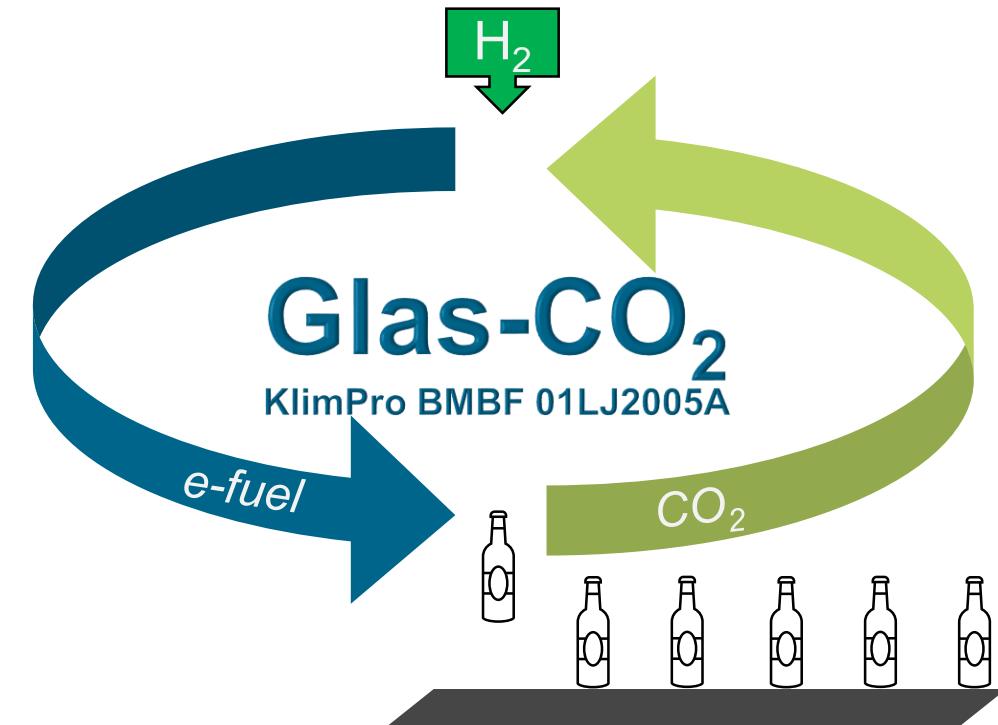
Approach – Techno- economic assessment (TEA) of CCU in the glass industry



- Glass production details (HVG)
- CCU Know-How (DLR)
- Recycle of oxyfuel combustion gases
- Evaluated using the German boundary conditions
 - Day-ahead-market
- Surplus CO₂ from carbonates also converted

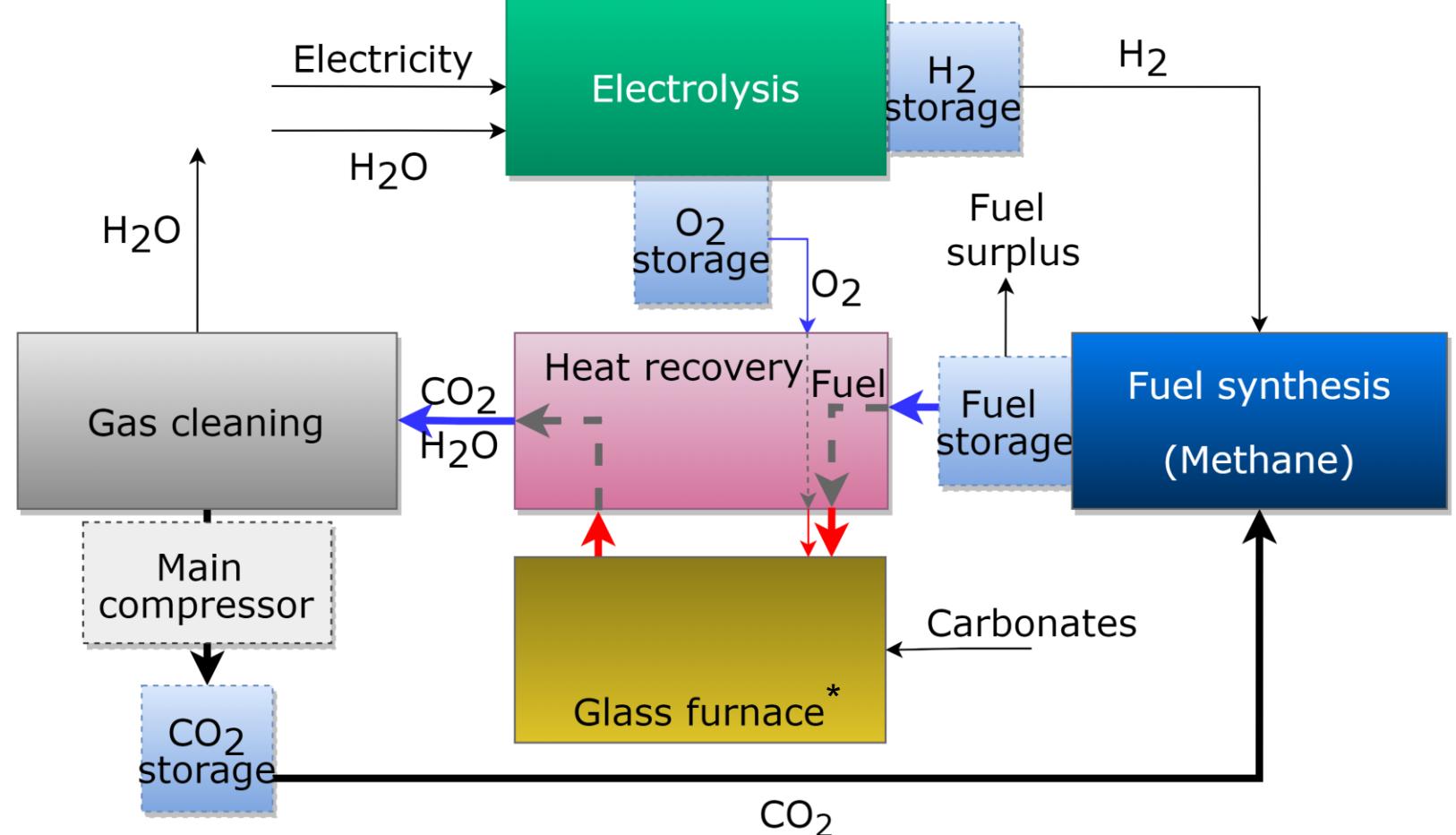
Glass prod. expertise:
 **HVG-DGG**^[1]
Service und Forschung für die Glasherstellung

Process assessment:
 **DLR** Deutsches Zentrum
für Luft- und Raumfahrt
German Aerospace Center



Methodology – CCU process concept for methane

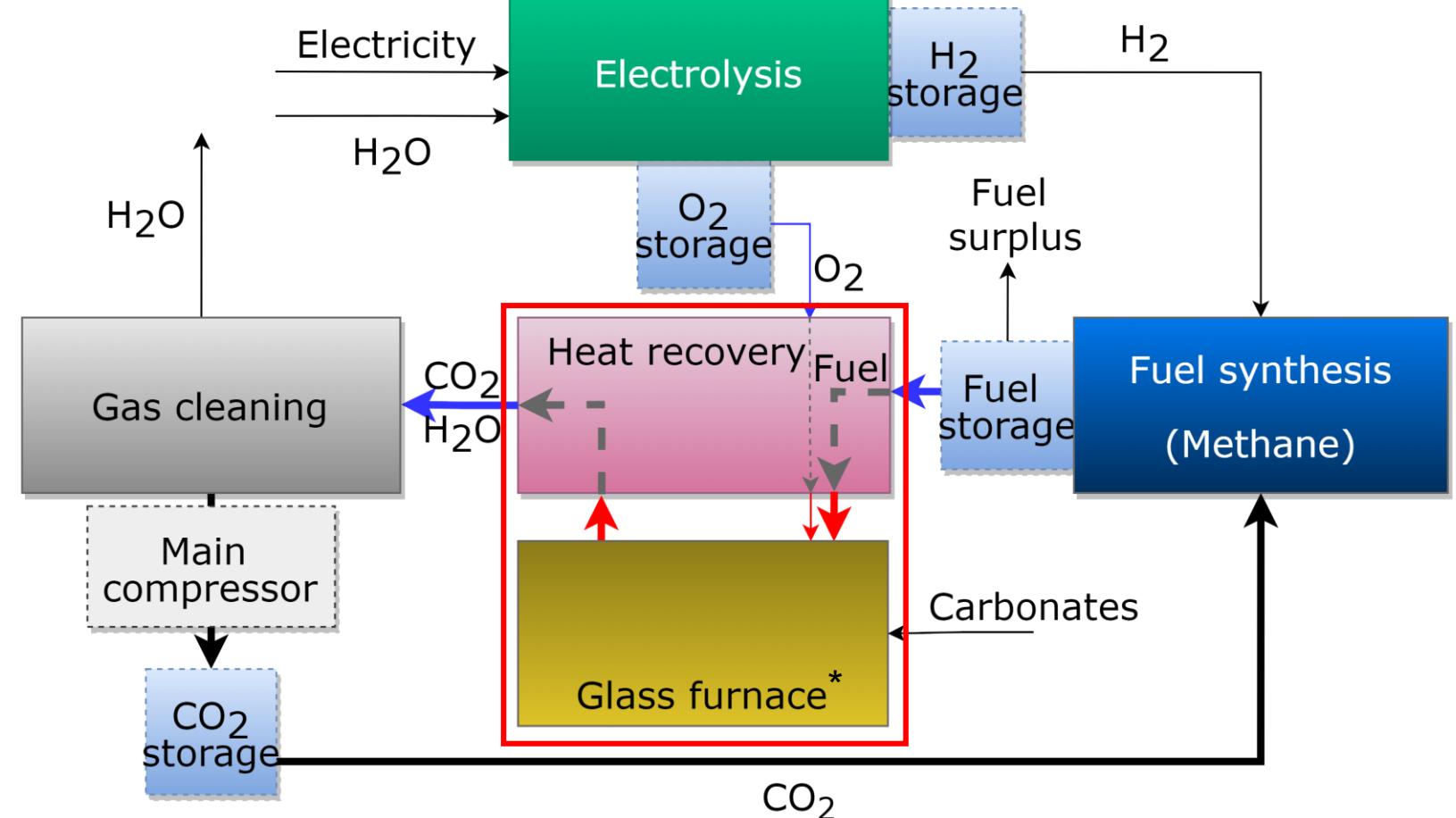
- Oxyfuel furnace
- Heat recovery



*Glass furnace is assumed as given

Methodology – CCU process concept for methane

- Oxyfuel furnace
- Heat recovery
- Gas cleaning:
 - Wet scrubber
 - Hydrogenation
 - Guard beds
- PEM-Electrolysis
- Methane synthesis
 - TREMP™-process



*Glass furnace is assumed as given

Methodology - Process parameters of the glass furnace

Parameter	Value	Unit
Capacity	300	t_{glass}/day
Heat requirement ^[1]	4.2	MJ/kg_{glass}
Oxygen-fuel ratio (λ)	1.01	-
H_2 fuel - concentration	<10	% _{mol}
Batch CO_2 in exhaust gases	15	% _{mol}
Total CO_2 in exhaust gases	45	% _{mol}

- Exhaust gases: CO_2 , H_2O
 - Many impurities: SO_x , HCl, dust, ...
- Preheating of O_2 and fuel
- Glass furnace is assumed as given



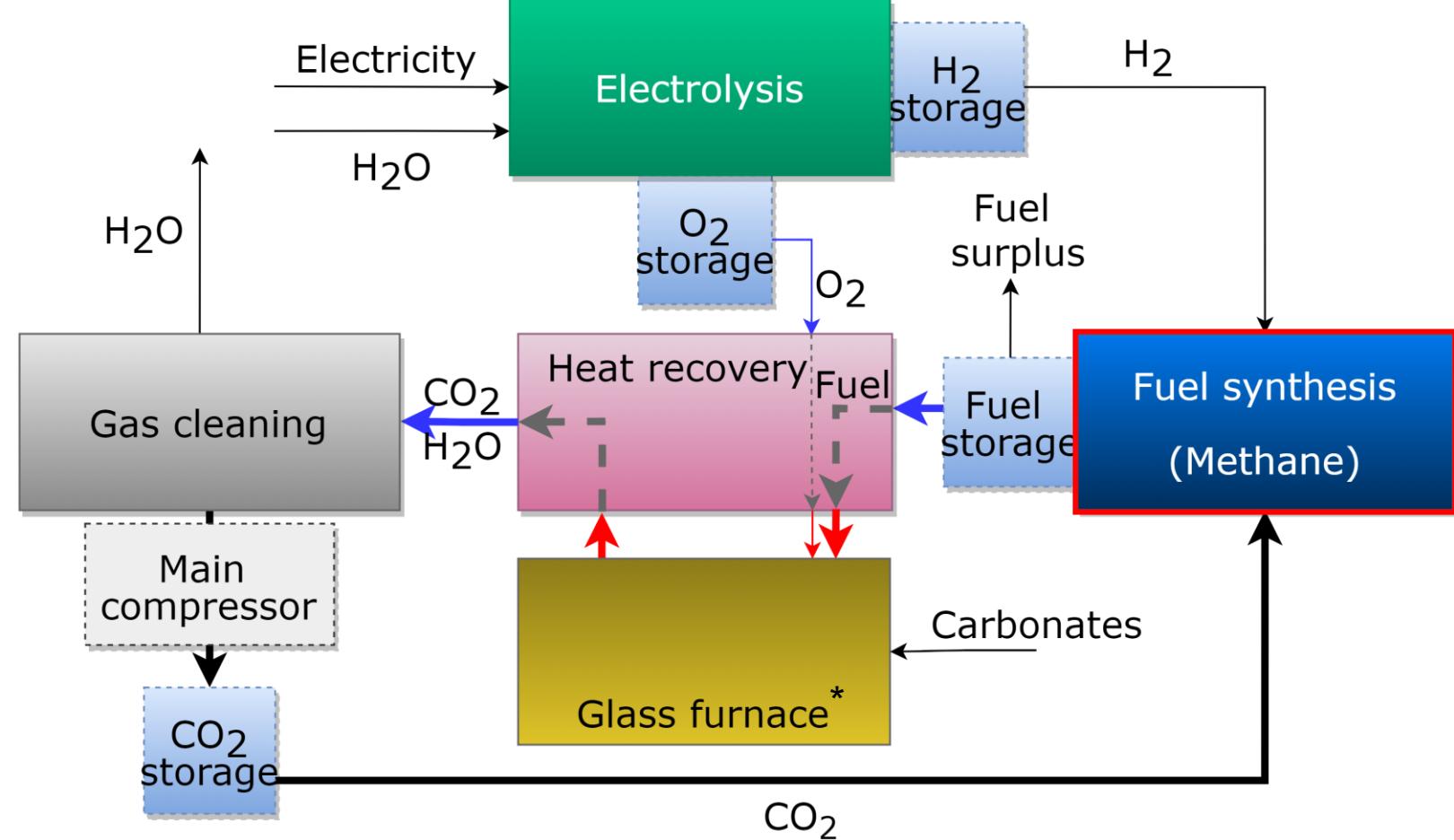
Figure - Glass furnace in operation^[2]

[1] Scalet, B. M. et al. (2013). JRC Reference Report: Best available techniques (BAT) reference document for the manufacture of glass. Industrial Emissions Directive 2010/75/EU, p. 234

[2] © C-Capture (2022). "C-Capture to demonstrate carbon capture capabilities for glass manufacturing ". from <https://c-capture.co.uk/c-capture-to-demonstrate-carbon-capture-capabilities-for-glass-manufacturing-with-pilkington-united-kingdom-limited/>.

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Methodology – Methanation process

TREMP

- Temp. max catalyst 800°C [1]
 - $\uparrow T_{\max} \leftrightarrow \downarrow \text{Irreversibilities}$
- SNG composition: 95% CH₄
 - 3.3% H₂
- Catalyst: Ni/Al₂O₃ (22% Ni)
- Operating pressure: 30 [bar]
- Kinetic model: Klose et. al [2]

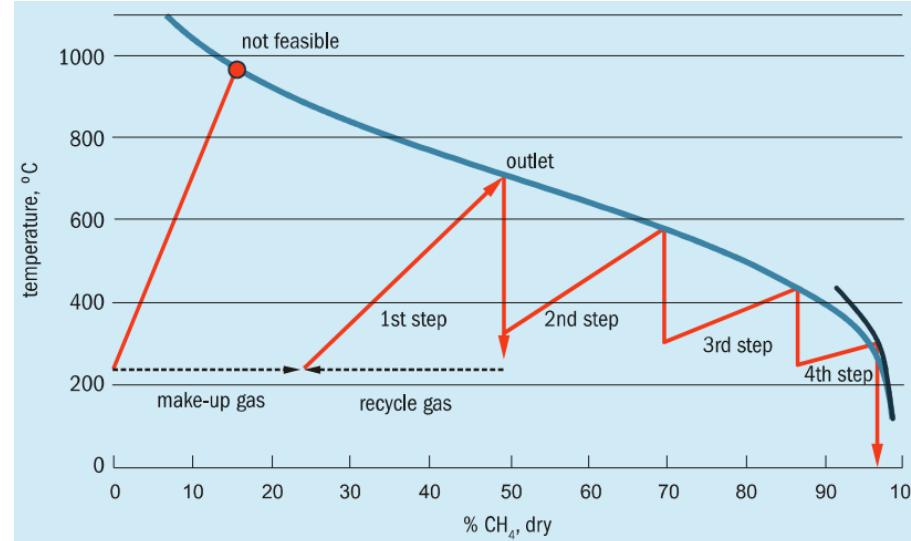


Figure – Equilibrium curve for the methanation process [1]

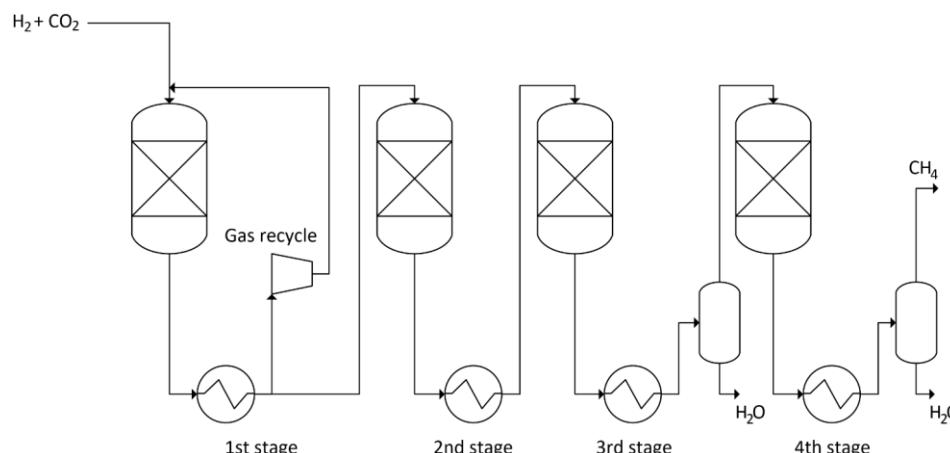


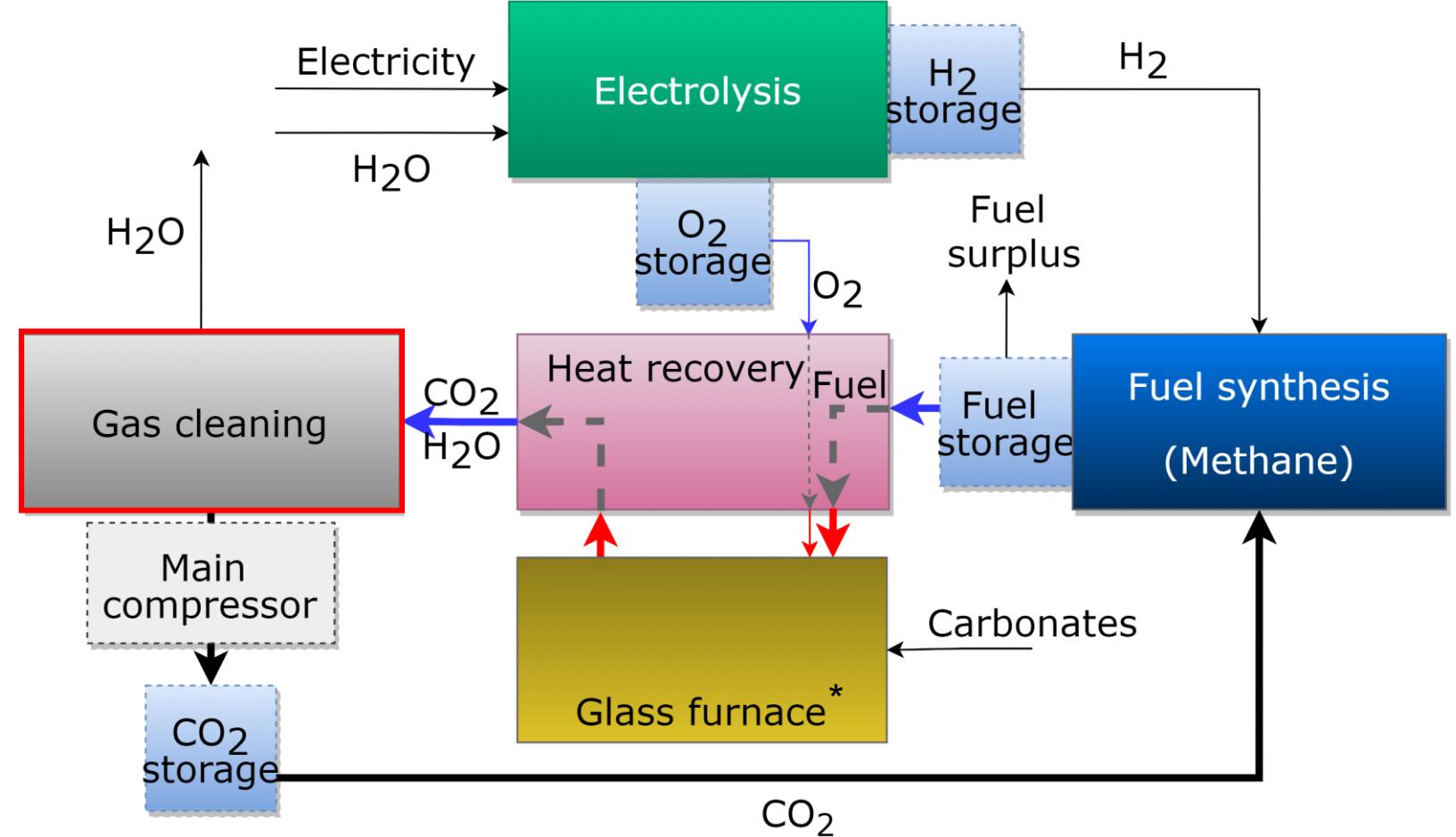
Figure - Topsøe's Recycle Energy-Efficient Methanation Process

[1] © Topsøe, H. (2011). From coal to clean energy.

[2] J. Klose, Kinetics of the methanation of carbon monoxide on an alumina-supported nickel catalyst, Journal of Catalysis, 85 (1984) 105-116.

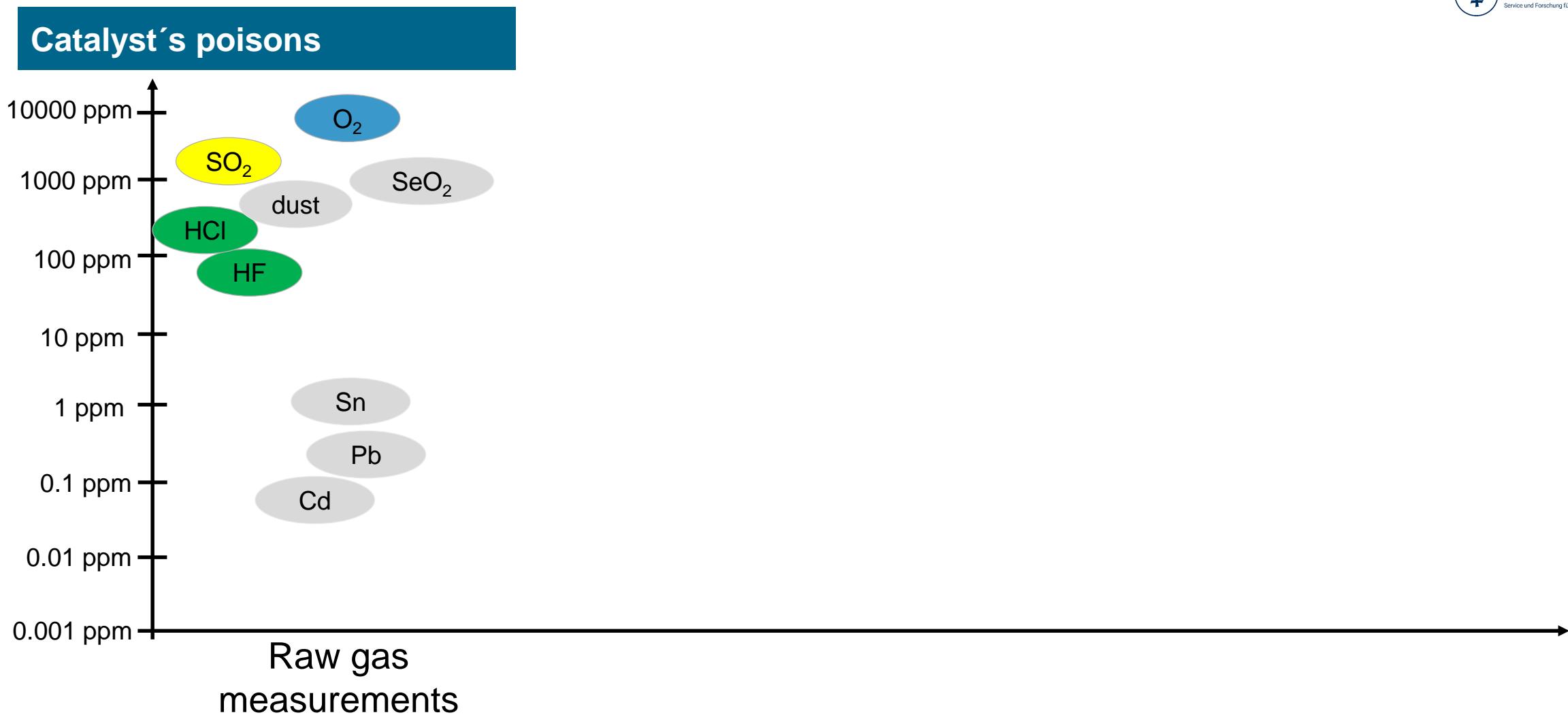
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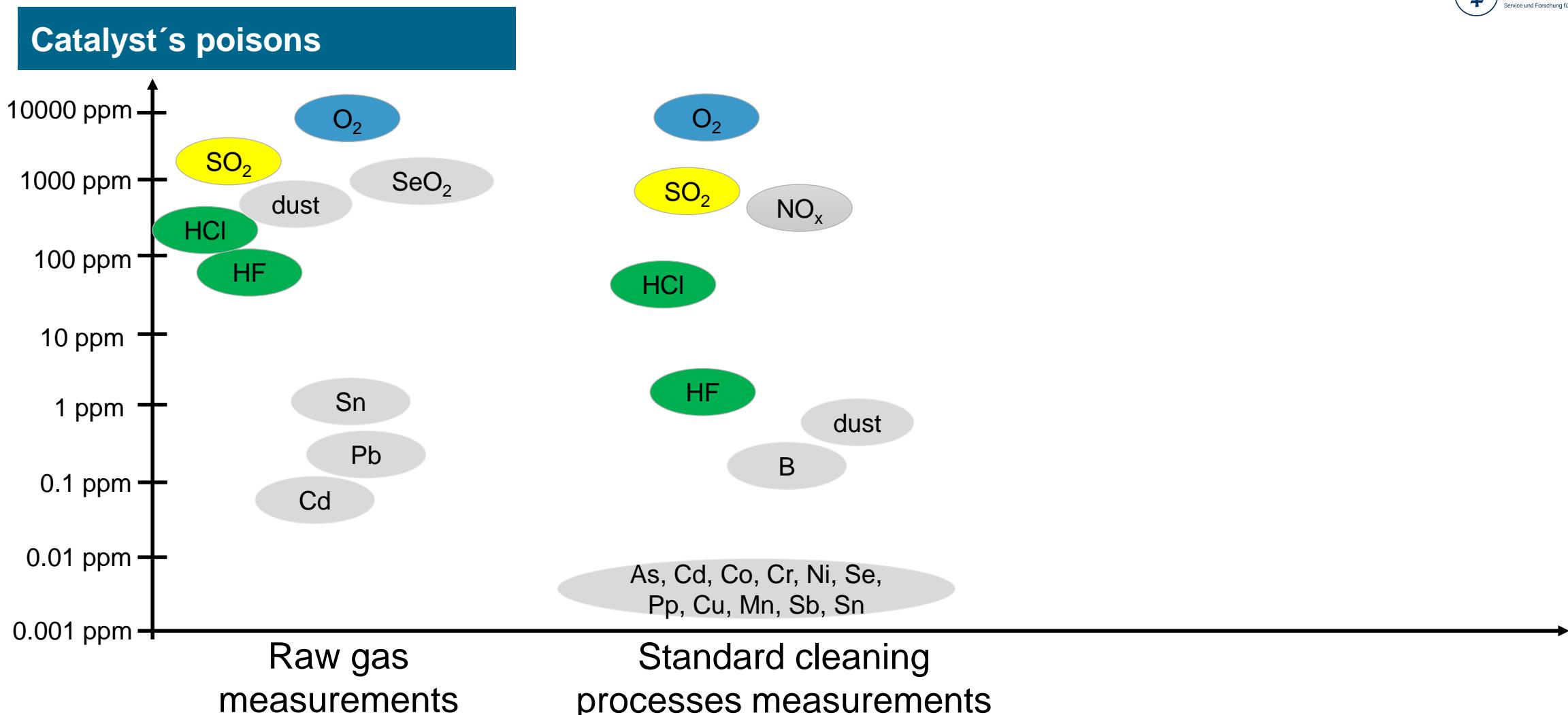


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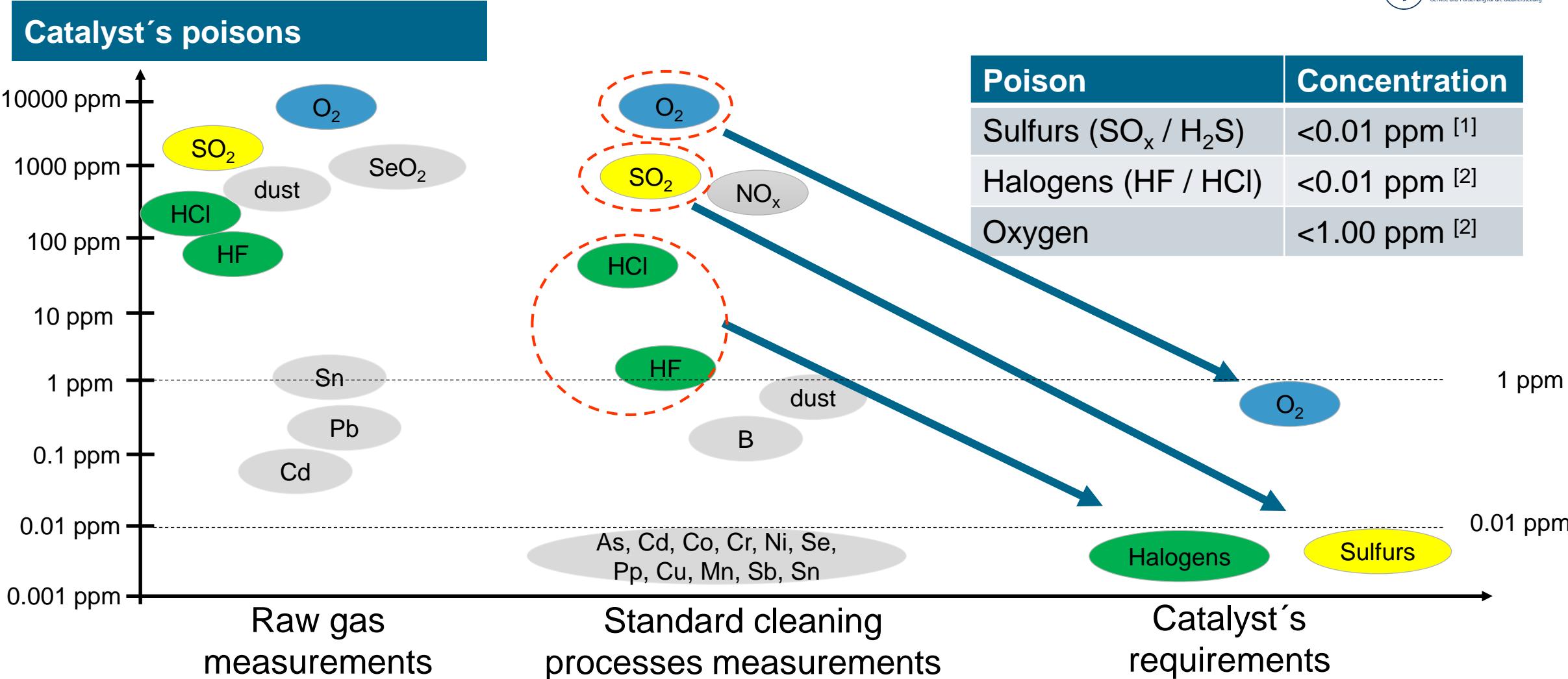
Methodology – Contaminants in the flue gases



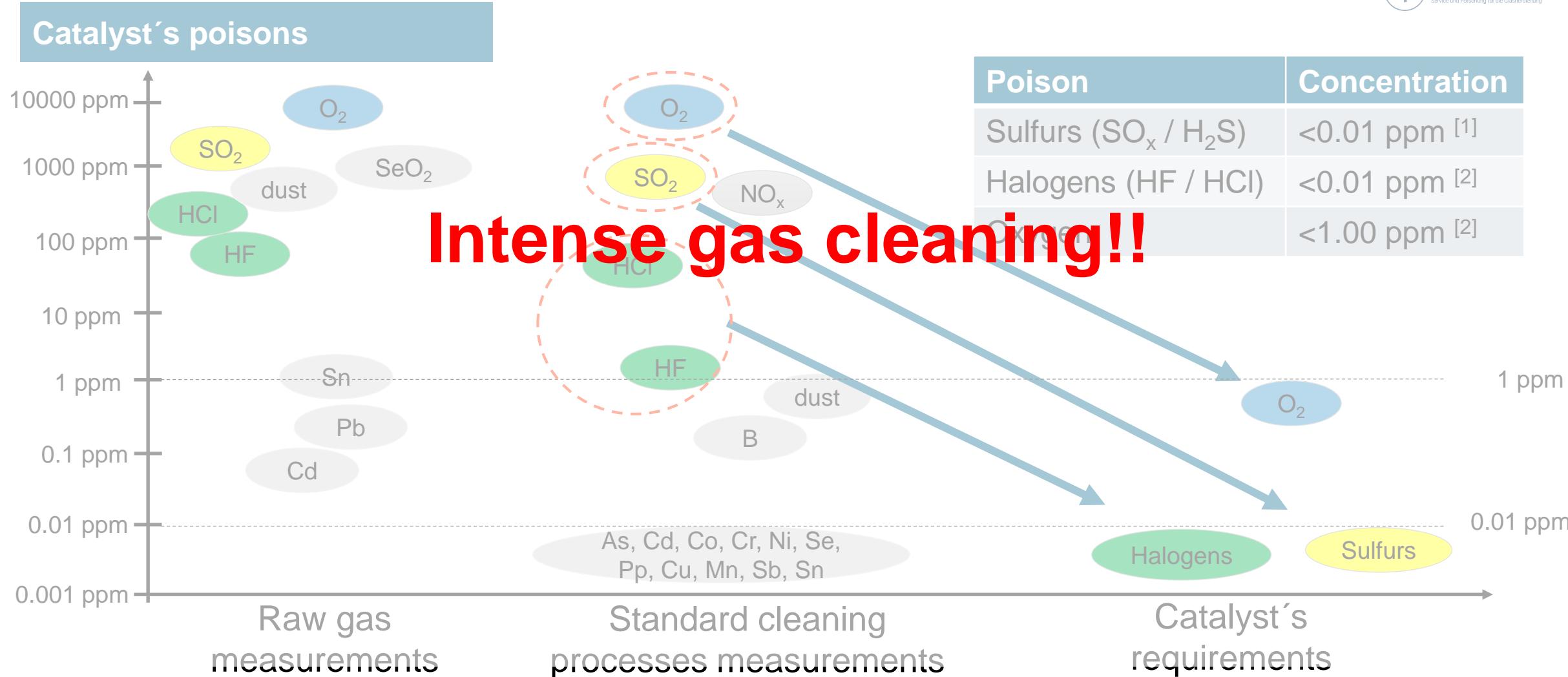
Methodology – Contaminants in the flue gases



Methodology – Contaminants in the flue gases

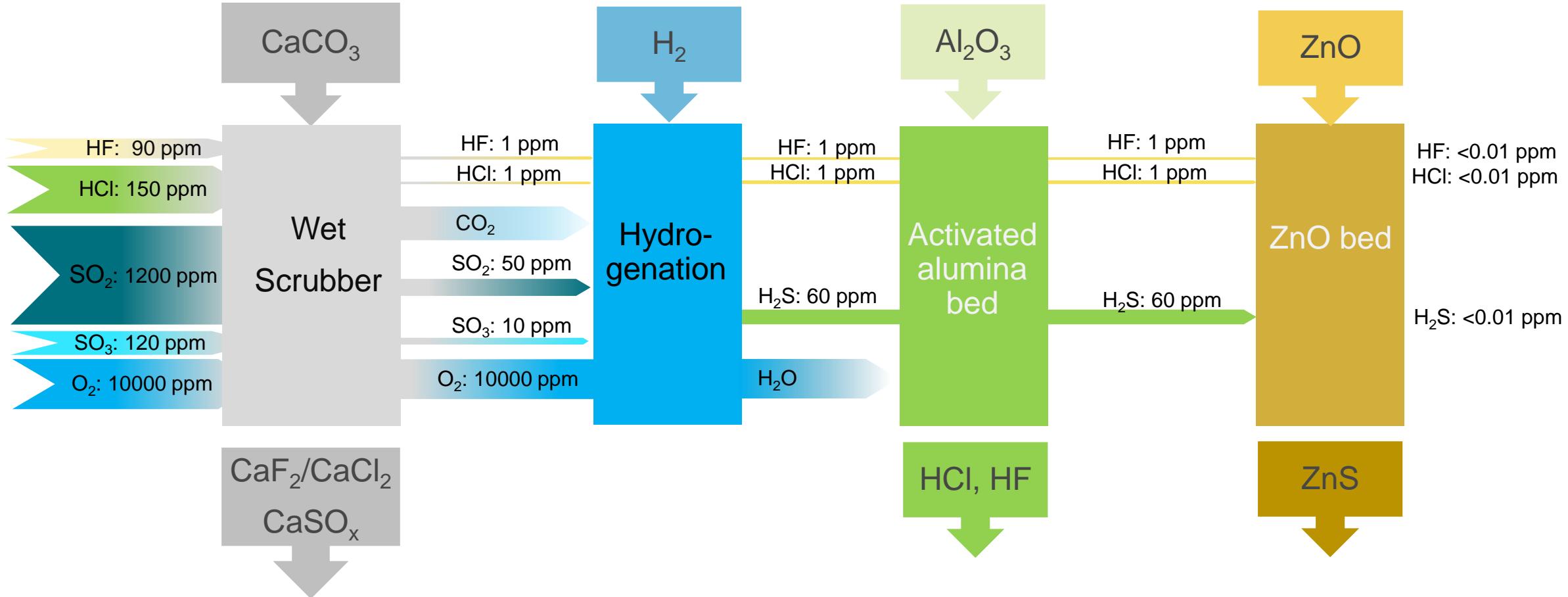


Methodology – Contaminants in the flue gases



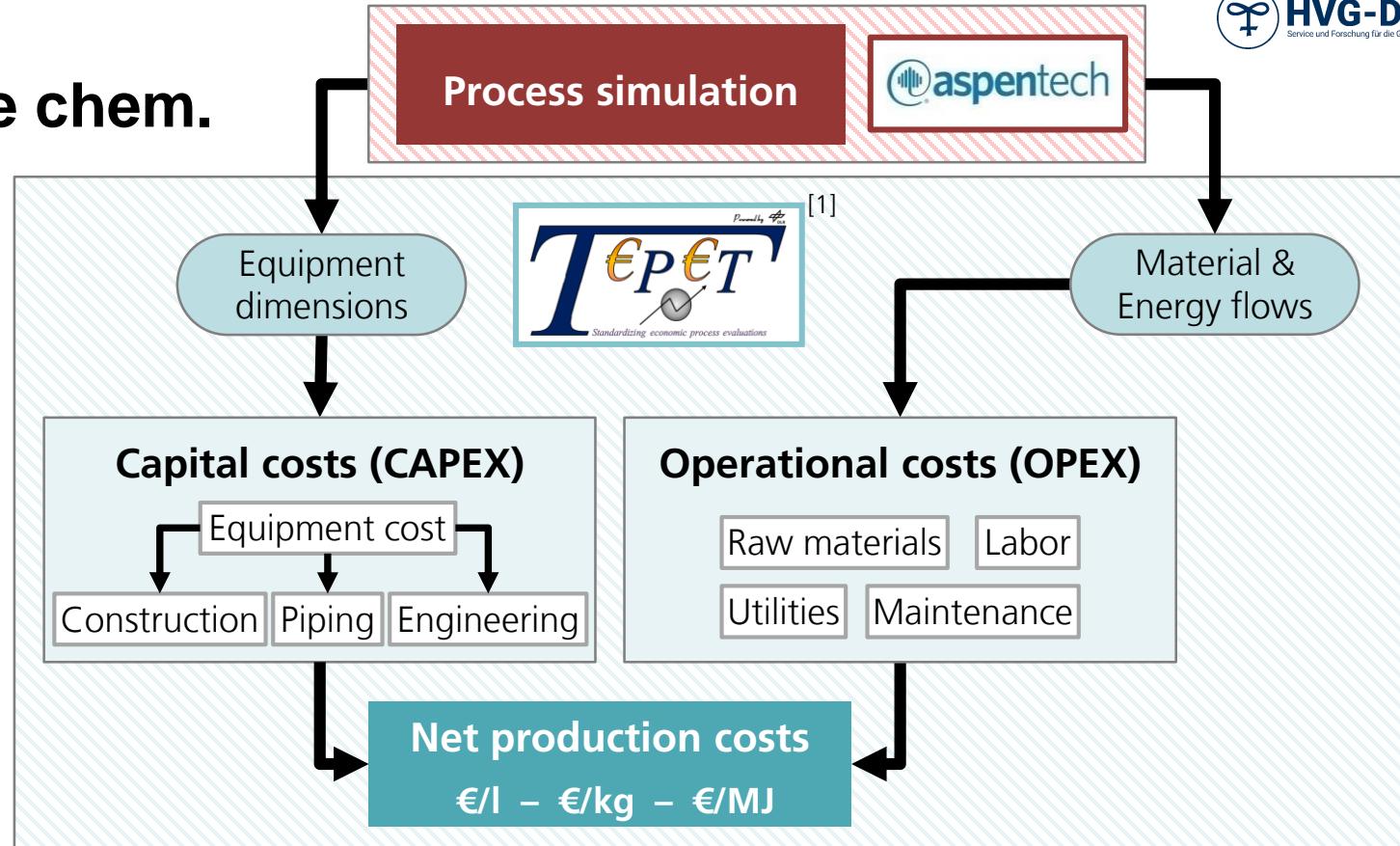
Methodology – Gas cleaning

Gas Cleaning



Methodology – Techno-economic assessment (TEA)

- Adapted from **best-practice chem. eng. methodology**
- Meets AACE class 3-4, Accuracy: **+/- 30 %**
- **Year specific** using annual CEPCI Index
- Automated interface for **seamless integration, heating networks, ...**
- Easy sensitivity studies for **each** parameter
- Learning curves, economy of scale,
...



[1] Albrecht et al. (2016) - A standardized methodology for the techno-economic evaluation of alternative fuels – A case study, Fuel, 194: 511-526

Methodology – Base case condition



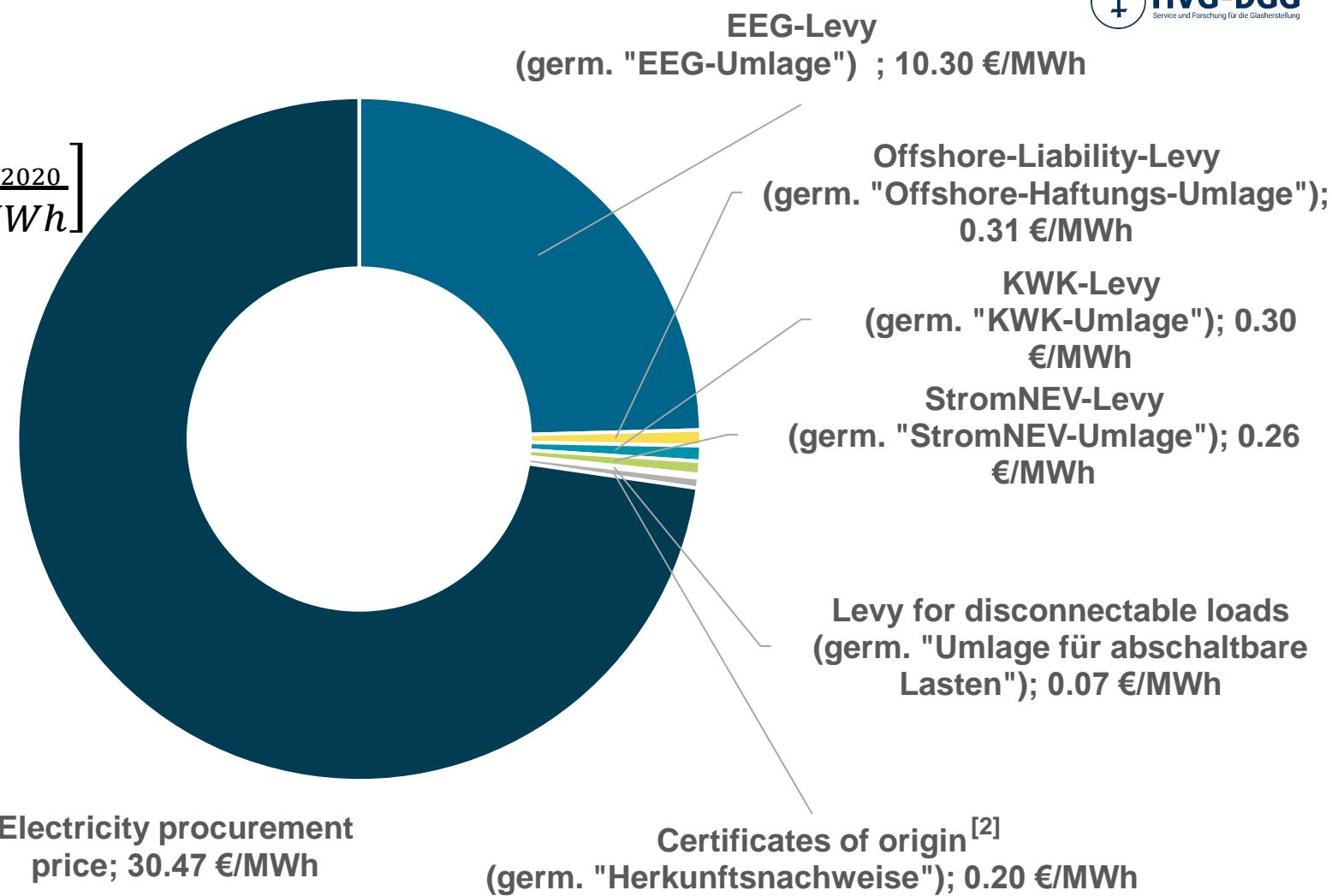
Evaluation input	
Plant capacity	300 t _{glass} /day
Synthetic fuel	Methane
Base year	2020
Interest rate	7%
Glass furnace operation	24/7/365
Methanation plant full load hours	8000 h/a
Plant lifetime	30 a
Green electricity price	42.31 €/MWh

- ✓ Backup supply through gas grid
- ✓ Costs of the modification of the plant only (i.e. glass furnace costs are excluded)

Methodology – Economic assumptions

Electricity price

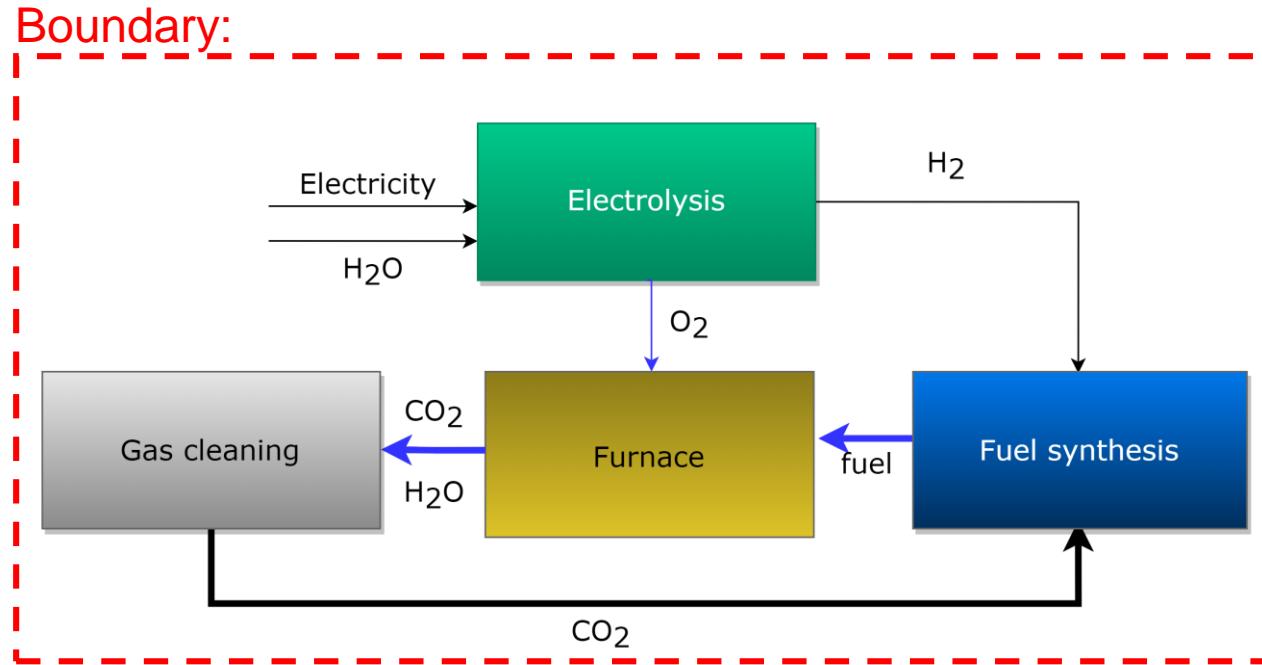
- Electricity price [1]: 42.31 $\left[\frac{\text{€}_{2020}}{\text{MWh}} \right]$



Results – Technical assessment

Efficiencies

$$\eta_{PtF} = \frac{\dot{m}_{Fuel,Total} \cdot LHV}{\dot{P}_{el,PEMEL} + \dot{P}_{el,others} - \dot{P}_{el,SC}} = 45\%$$

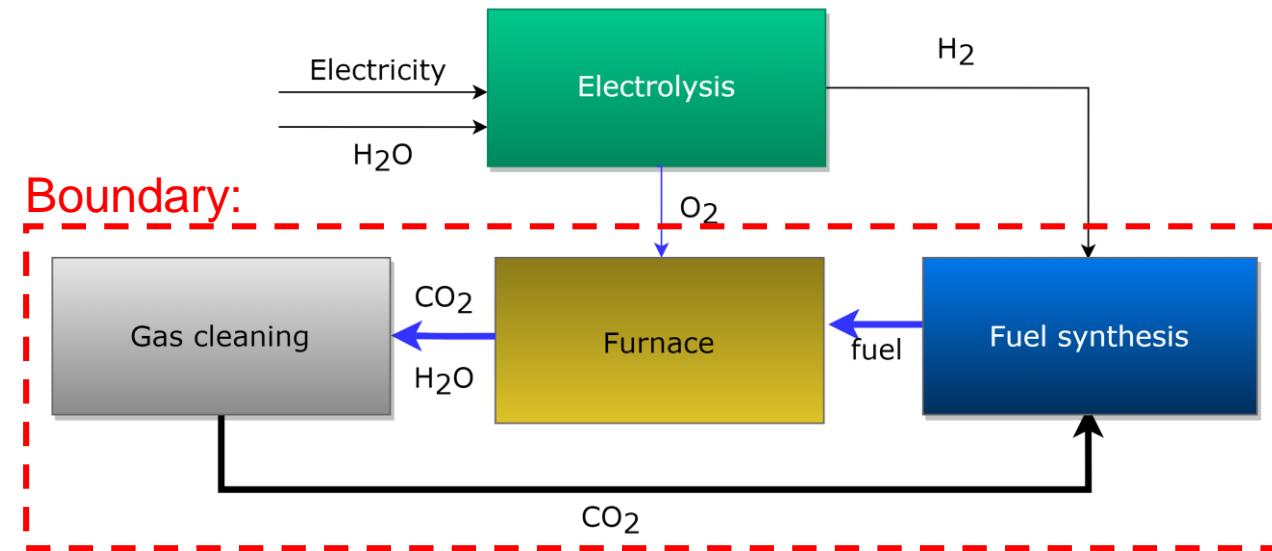


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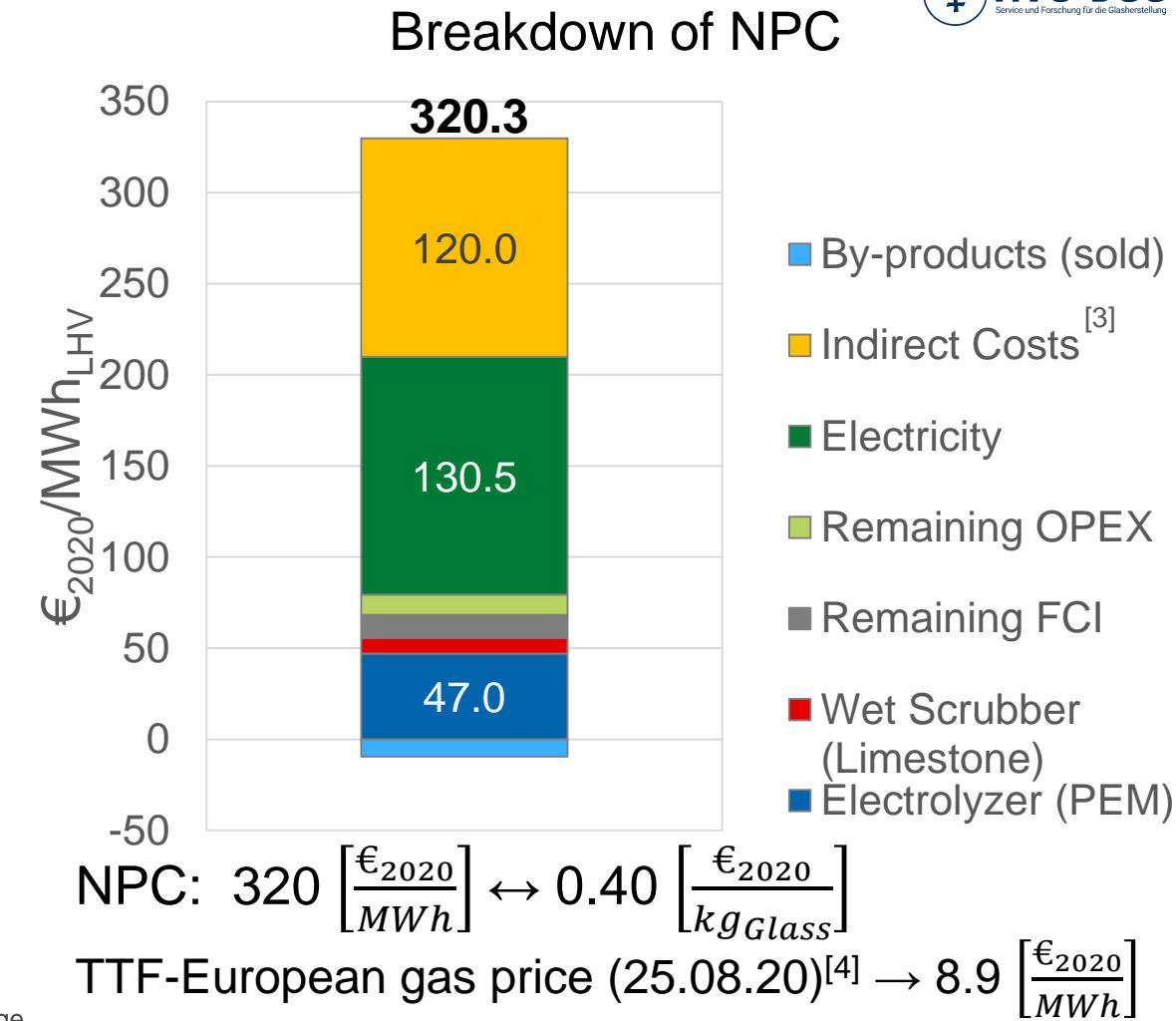
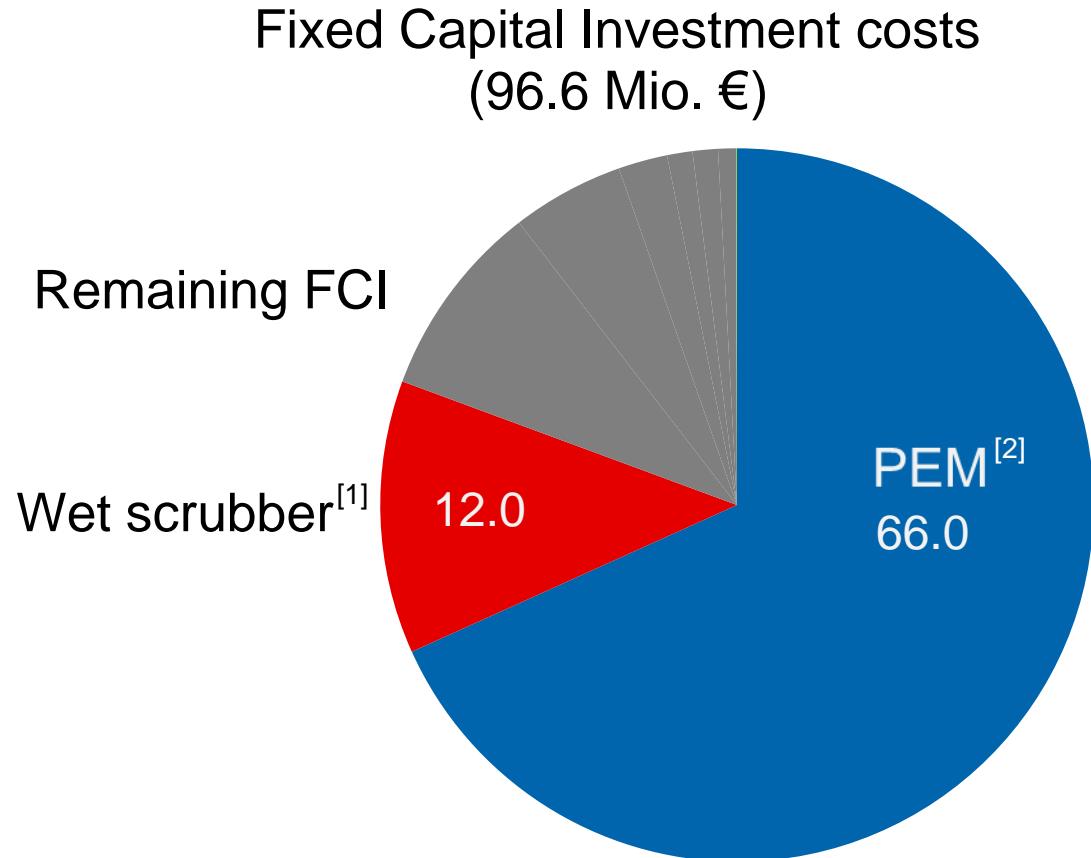
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$$\eta_{H_2tF} = \frac{\dot{m}_{Fuel} \cdot LHV_{Fuel}}{\dot{m}_{H_2} \cdot LHV_{H_2}} = 90\%$$



Results – Economic assessment



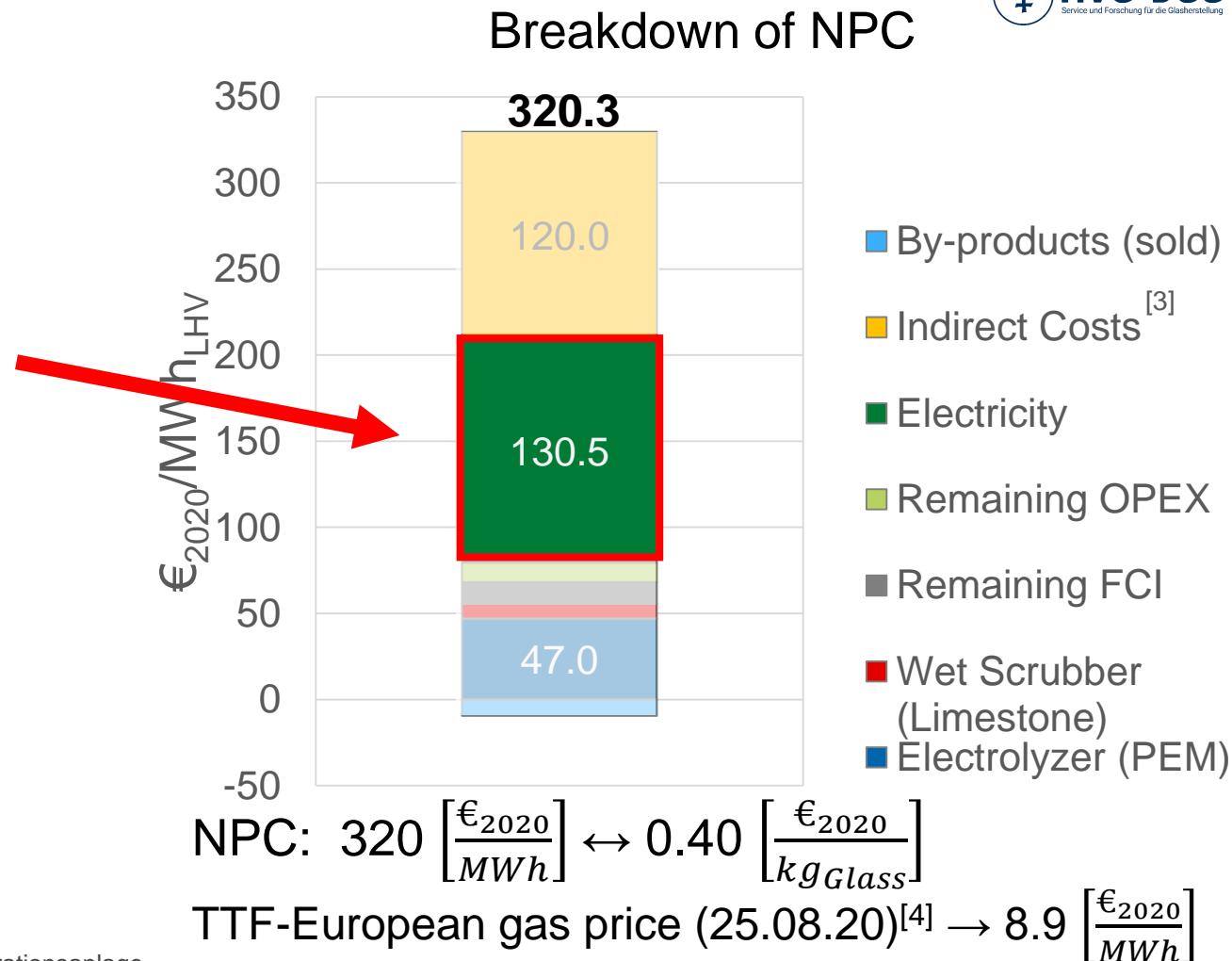
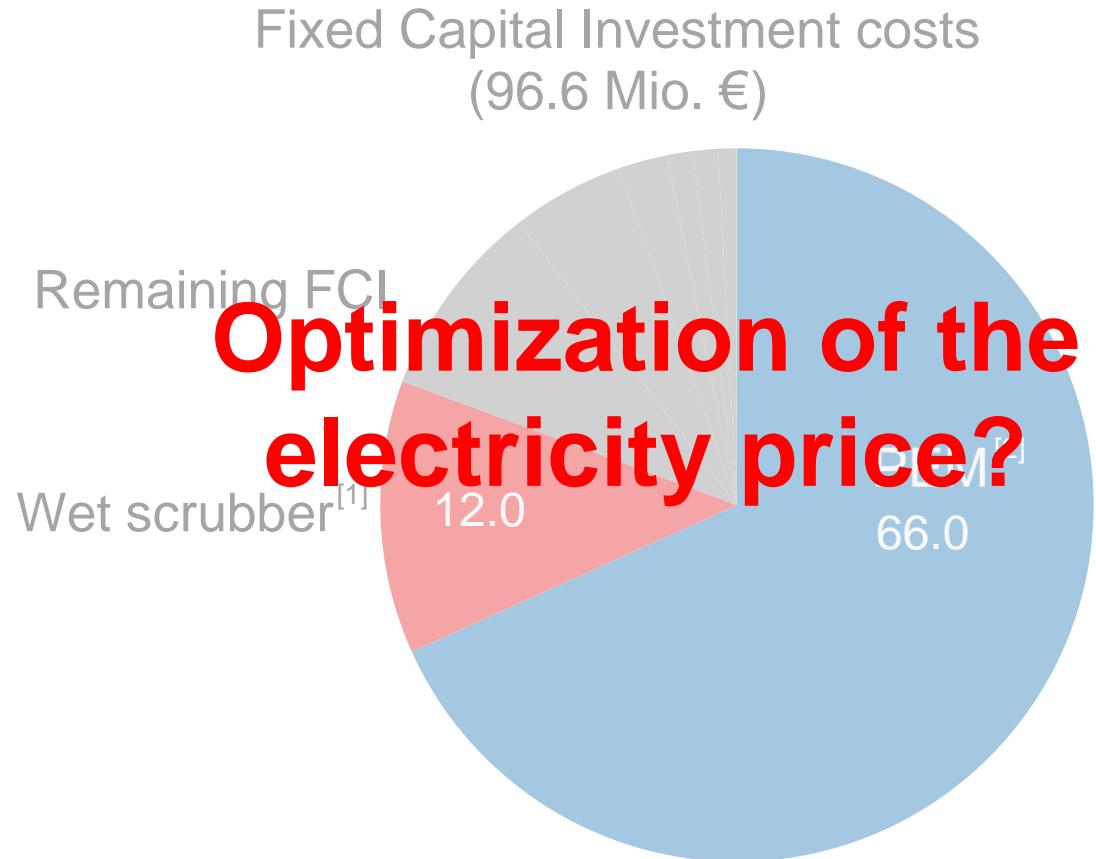
[1] J. L. Sorrels (Chapter 1 Wet and Dry Scrubbers for Acid Gas Control)

[2] Deutsches Zentrum für Luft- und Raumfahrt (DLR) (Studie über die Planung einer Demonstrationsanlage zur Wasserstoff-Kraftstoffgewinnung durch Elektrolyse mit Zwischenspeicherung in Salzkavernen unter Druck)

[3] M. Peters, K. Timmerhaus and R. West, Plant design and economics for chemical engineers, New York, United States: McGraw-Hill, 2004, ISBN 007-124044-6

[4] Tradingeconomics (2022). "EU Natural Gas." from <https://tradingeconomics.com/commodity/eu-natural-gas>.

Results – Economic assessment



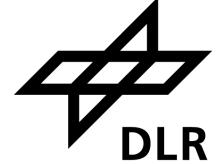
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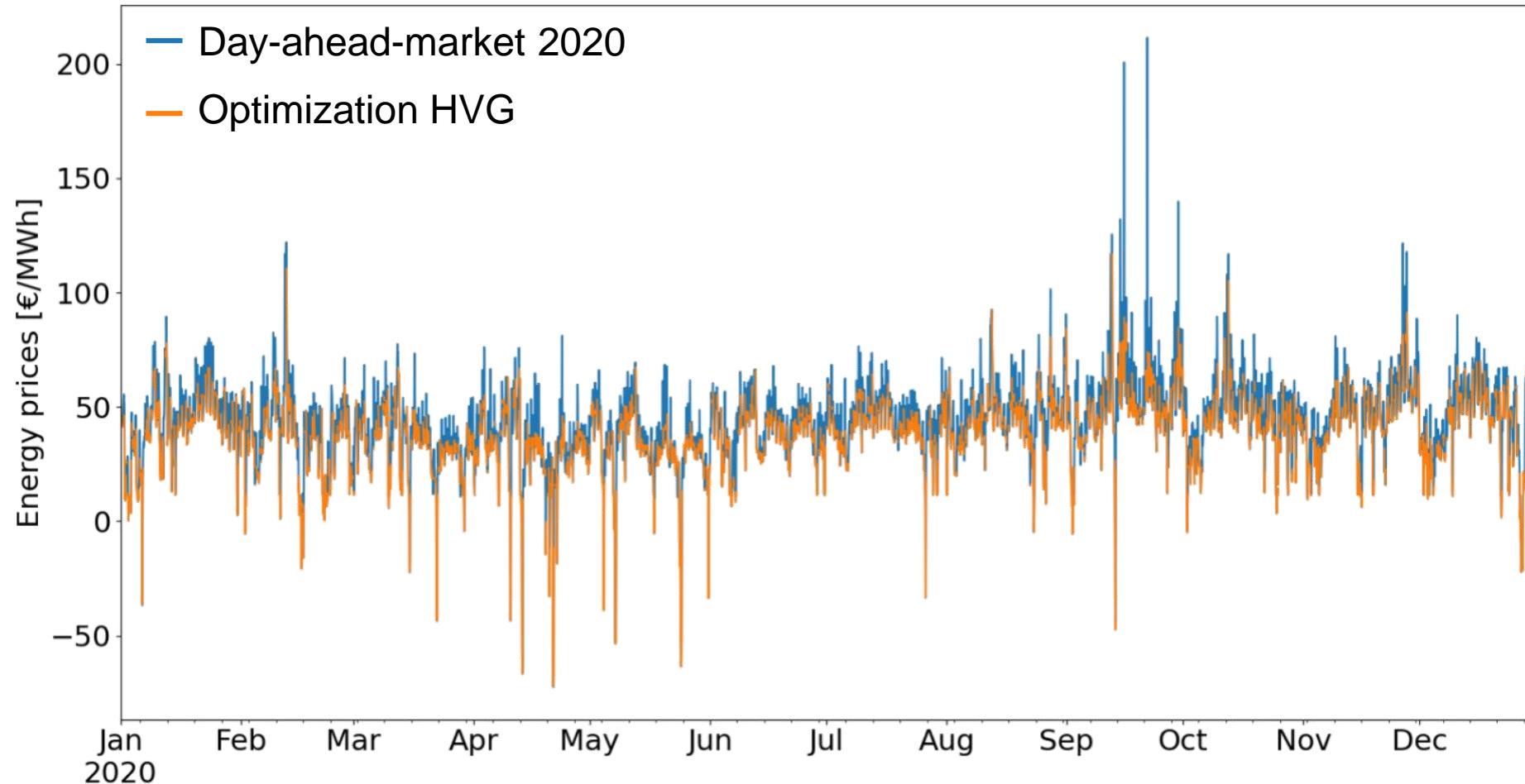
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Results – Electricity price, sensitivity analysis



Utilization of storage



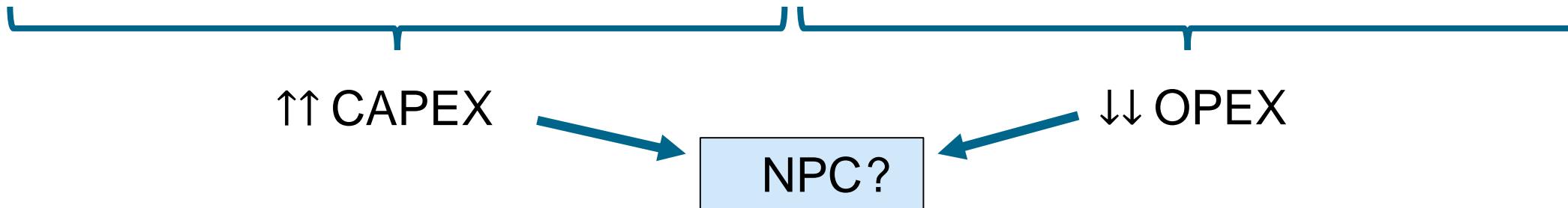
Results – Electricity price, sensitivity analysis

Algorithm

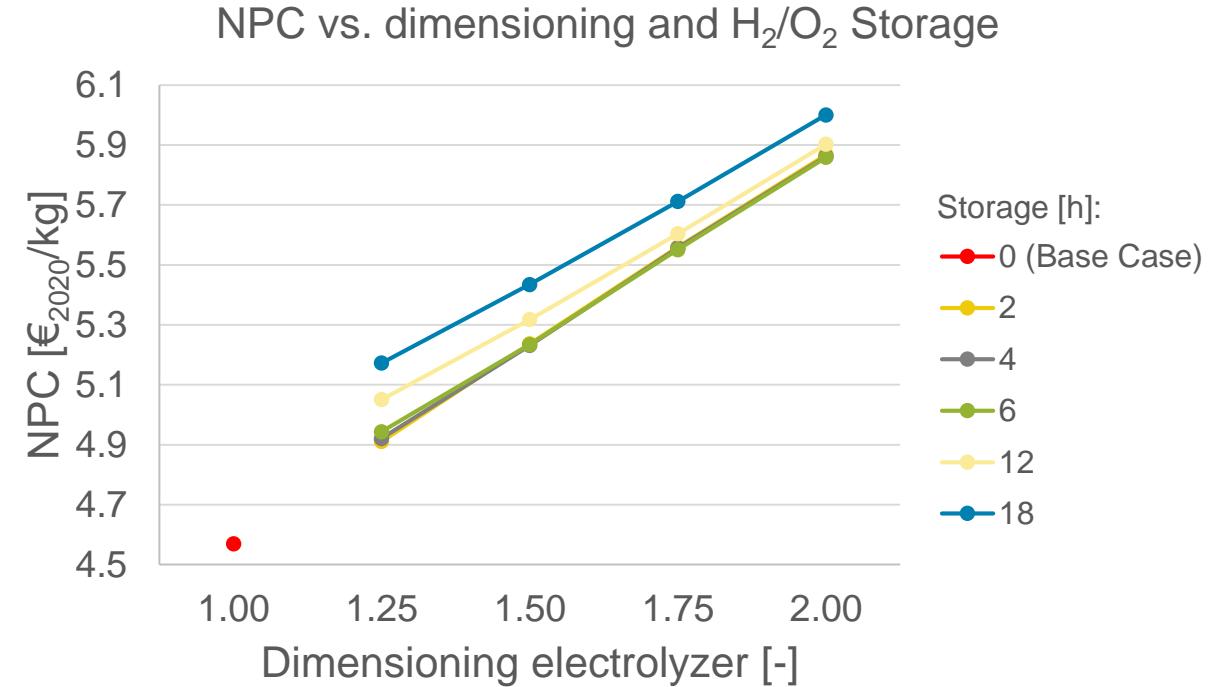
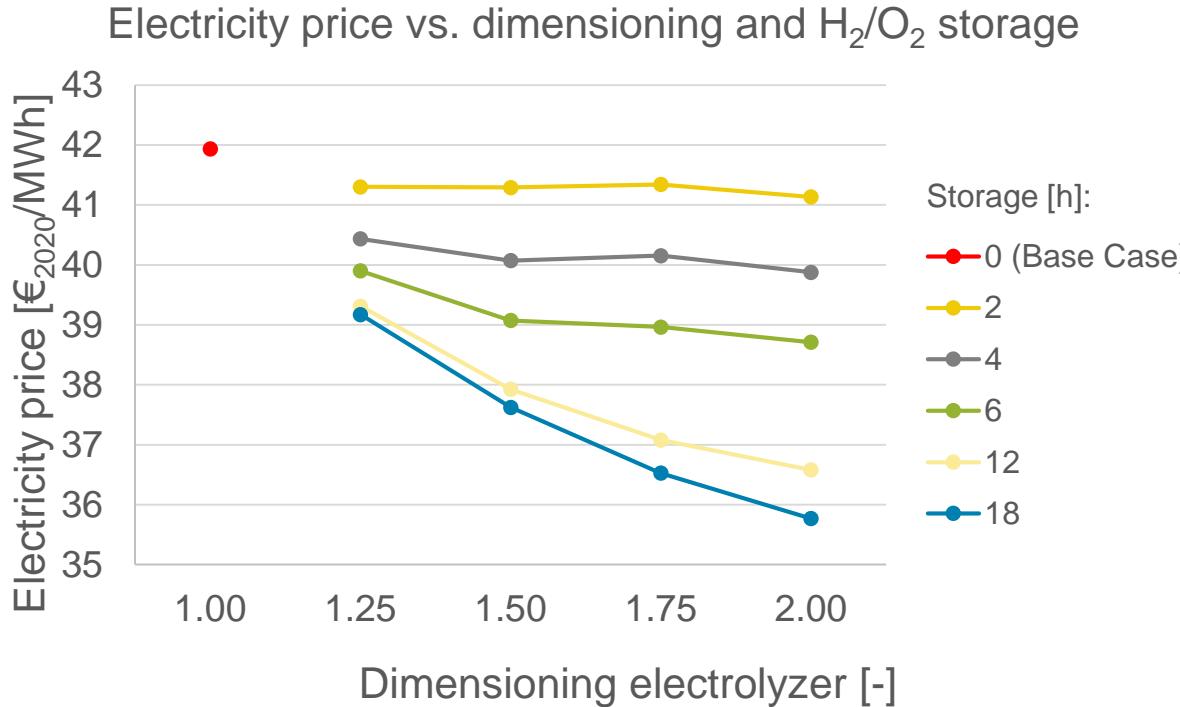
- Storage capacity variation (hours)
 - Electrolyzer overdimensioning
 - Faster charging speed for storage
- } Less operation time per day (electrolyzer only)



Optimization of electricity purchase in day-ahead-market

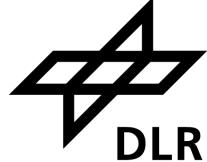


Results – Sensitivity analysis



- Storage increase leads to a higher NPC
- Fluctuations are not big enough in the year 2020

Summary



- Process design for methane synthesis developed and assessed
 - Realistic conditions were implemented (HVG)
- CCU could be implemented in the glass industry
 - NPC: $320 \text{ €}_{2020}/MWh_{LHV} \leftrightarrow 0.40 \text{ €}_{2020}/kg_{glass}$
 - Electricity: 40%
 - PEM: 15%
 - ... pilot plant validation?
- Electricity price algorithm developed and implemented
 - Storage is not economically viable in 2020
 - ... but what would happen with higher fluctuations?

Outlook



Figure - Methanol synthesis plant [1]

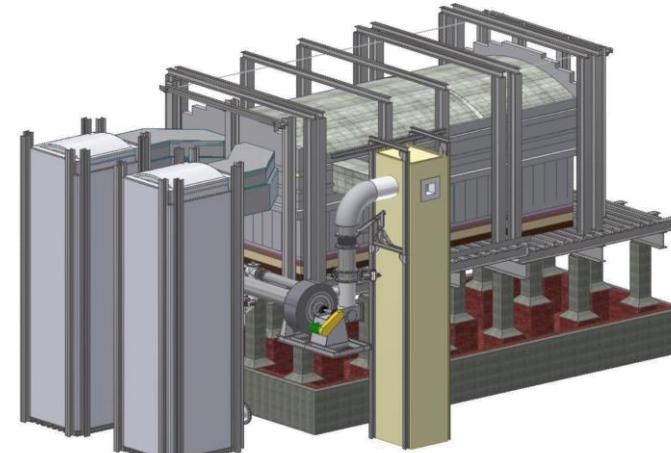


Figure - Linde's OPTIMELT Thermochemical Regenerator System [2]

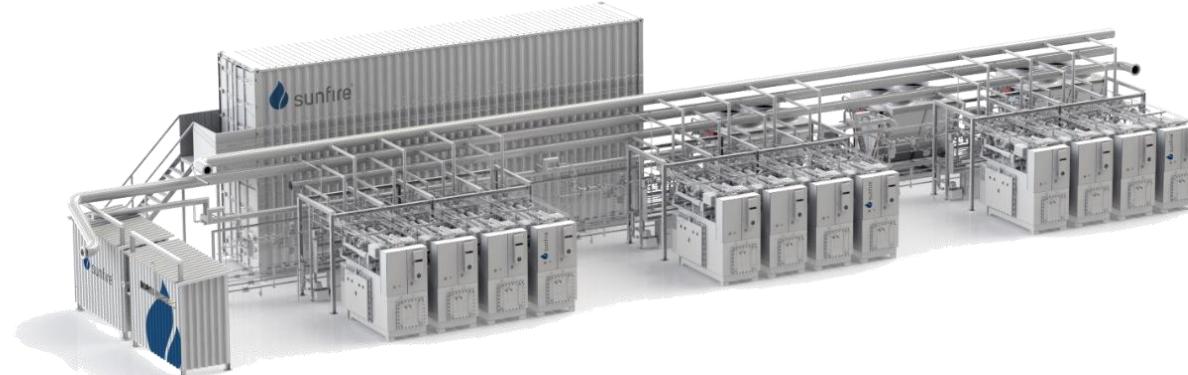


Figure – Concept of a solid oxide electrolysis cell [3]

[1] © Energy, G. (2022). "Advanced Methanol Amsterdam." from <https://www.gidara-energy.com/advanced-methanol-amsterdam>

[2] © Sundaram, S. K. (Ed.). (2018). 78th Conference on Glass Problems. John Wiley & Sons.

[3] © by ND2.0 SunFire (2022). "Renewables Everywhere - Electrolysis at its best." from https://www.sunfire.de/assets/images/7/Sunfire_SOEC_Elektrolyseure-75796dd7.png



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glass made of ideas

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Thank you for your attention. Questions?

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HVG: F. Drünert, B. Fleischmann



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