

1 **Ultrasound-assisted green solvent extraction of high-added value**  
2 **compounds from microalgae *Nannochloropsis spp.***

3  
4 O. Parniakov<sup>1,2</sup>, E. Apicella<sup>3</sup>, M. Koubaa<sup>1</sup>, F.J. Barba<sup>5</sup>, N. Grimi<sup>1\*</sup>, N. Lebovka<sup>1,2</sup>, G.  
5 Pataro<sup>3</sup>, G. Ferrari<sup>3,4</sup>, E. Vorobiev<sup>1</sup>

6  
7 <sup>1</sup>Sorbonne Universités, Université de Technologie de Compiègne, Laboratoire  
8 Transformations Intégrées de la Matière Renouvelable (UTC/ESCOM, EA 4297  
9 TIMR), Centre de Recherche de Royallieu, B.P. 20529, 60205 Compiègne Cedex,  
10 France

11 <sup>2</sup>Institute of Biocolloidal Chemistry named after F. D. Ovcharenko, NAS of Ukraine,  
12 42, blvr. Vernadskogo, Kyiv 03142, Ukraine

13 <sup>3</sup>Department of Industrial Engineering, University of Salerno, Via Giovanni Paolo II  
14 132 Fisciano (SA), Italy

15 <sup>4</sup>ProdAl scarl, Via Ponte don Melillo Fisciano (SA), Italy

16 <sup>5</sup>Nutrition and Food Science Area, Faculty of Pharmacy, Universitat de València,  
17 Avda. Vicent Andrés Estellés, s/n 46100 Burjassot, València, Spain

18  
19  
20  
21  
22  
23 **(\*) Corresponding Author: Nabil GRIMI**

24 Sorbonne Universités, Université de Technologie de Compiègne, Laboratoire  
25 Transformations Intégrées de la Matière Renouvelable (TIMR EA 4297), Centre de  
26 Recherche de Royallieu, B.P. 20529, 60205 Compiègne Cedex, France

27 phone number: +33 3 44 23 44 42

28 e-mail: nabil.grimi@utc.fr

29

30 **Abstract**

31 The aim of this work was to investigate ultrasound (US)–assisted green solvent  
32 extraction of valuable compounds from microalgae *Nannochloropsis*. The individual  
33 green solvents (water, ethanol (EtOH), dimethyl sulfoxide (DMSO)) and binary  
34 solvents (water-DMSO and water-EtOH) were used in extraction procedures. The  
35 maximum total phenolic compounds yield,  $Y_p$ , obtained for 15 min at  $W=400$  W, was  
36  $Y_p \approx 0.33$  as compared with  $Y_p \approx 0.06$ , for the control sample. The highest yield of total  
37 chlorophylls,  $Y_c$ , which was obtained for 7.5 min at  $W=400$  W, was  $Y_c \approx 0.043$  as  
38 compared with  $Y_c \approx 0.004$ , for the control sample. For US-assisted extraction in water,  
39 the absence of noticeable synergy of the application of US with simultaneous increasing  
40 of temperature, was observed. The recovery efficiency decreased in the raw  
41 DMSO>EtOH>H<sub>2</sub>O. Moreover, when the binary mixture of solvents (water-DMSO and  
42 water-EtOH) was used, the maximum recovery was observed when concentration of  
43 organic solvent  $C$  was above 25-30%, for both cases.

44

45 **Keywords:** *Nannochloropsis*, ultrasound-assisted extraction, phenolic compounds,  
46 chlorophylls, ethanol, dimethyl sulfoxide.

47

## 48 **1. Introduction**

49 Microalgae have attracted a considerable attention as they are a good source of  
50 natural food colorants, antioxidants and antimicrobials including, among others,  
51 chlorophylls, carotenoids and polyphenols (Barba et al., 2014; Dufossé et al., 2005).  
52 These compounds are enclosed in intracellular vacuoles and chloroplasts, thus  
53 complicating their recovery by conventional heat and/or solvent extraction. For this  
54 reason, over the last years, several research groups have investigated the use of non-  
55 conventional technologies in order to improve the extraction yield of these compounds  
56 while reducing the processing temperature, the solvent consumption and shortening the  
57 treatment time.

58 In this line, ultrasound (US)-assisted extraction has been used over the last years to  
59 recover nutritionally valuable compounds from plant food materials and algae matters  
60 (Roselló-Soto et al., 2015). This technology has the ability to disrupt cell wall based on  
61 the cavitation phenomena, thus improving extraction yield and kinetics compared to  
62 conventional techniques, with a significant reduction in the temperature, solvent  
63 consumption and extraction time. Moreover, compared to other non-conventional  
64 methods, it is a well-known technology with low capital cost and can be easily  
65 implemented in the food and pharmaceutical industries (Barba et al., 2014).

66 Several works published in current literature were devoted to US-assisted extraction  
67 of lipids from microalgae (Adam et al., 2012; Araujo et al., 2013; Bermúdez Menéndez  
68 et al., 2014; Cravotto et al., 2008; Keris-Sen et al., 2014; Ma et al., 2015; Natarajan et  
69 al., 2014; Qv et al., 2014; Sun et al., 2014). For example, it was demonstrated that US-  
70 assisted extraction of oils from a cultivated marine microalgae improved the extraction  
71 yield (+20%) as compared with conventional Soxhlet extraction (Cravotto et al., 2008).

72 The solvent-free US-assisted extraction was also applied to extract lipids from fresh  
73 aqueous *Nannochloropsis oculata* biomass (Adam et al., 2012). It was demonstrated  
74 that US-assisted extraction resulted in a significant increase of oil extraction from *C.*  
75 *vulgaris* (52.5% w/w) (Araujo et al., 2013). Application of US-treatment to mixed  
76 microalgal cultures resulted in increased concentrations of protein and carbohydrates  
77 (Keris-Sen et al., 2014). The application of US also allowed 1.5-2.0-fold increase in  
78 lipid extraction yields in the presence of two different solvents, n-hexane and  
79 chloroform/methanol mixture. US-assisted extraction from green algae *Dunaliella*  
80 *tertiolecta* allowed to obtain an extraction yield of lipids of 45.94% under the optimum  
81 conditions of ultrasonic power of 370 W, extraction time of 5 min and liquid/solid ratio  
82 125 ml/g (Qv et al., 2014). The advantages of US- and microwaves (MW)-assisted lipid  
83 extraction from microalgae, both in terms of efficiency and operational costs were also  
84 demonstrated (Bermúdez Menéndez et al., 2014).

85 US-assisted extraction of lipids from several microalgae species (*Tetraselmis*  
86 *suecica*, *Nannochloropsis sp.*, *Chlorella sp.*) were studied under various US conditions  
87 (Natarajan et al., 2014). It was found that for *Chlorella sp.*, with rigid cell walls, lipids  
88 were released to the aqueous phase while for *T. suecica* and *Nannochloropsis sp.*, with  
89 flexible cell membranes, lipids were retained inside cells after disruption. US-treatment  
90 allowed effective extraction of high-value metabolites (polysaccharides and lipids) from  
91 microalgae *Chlorella protothecoides* (Sun et al., 2014). The combination of US and  
92 microwave (MW) treatment was applied to assist biodiesel production from microalgae  
93 *Chlorella vulgaris* (Ma et al., 2015).

94 Many efforts were also devoted to US-assisted extraction of different bioactive  
95 compounds such as carotenoids and chlorophylls from microalgae *Dunaliella salina* in  
96 organic solvents N,N'-dimethylformamide and methanol were studied (Macías-Sánchez

97 et al., 2009). The possibility of US-assisted extraction of bioactive compounds  
98 (carotenoids and fatty acids) from *C. vulgaris*, at analytical scale, has been  
99 demonstrated (Plaza et al., 2012). Important concentrations of extracted carotenoids,  
100 chlorophylls and essential fatty acids (among others) have been found in extracts. It was  
101 demonstrated that US-assisted extraction is the most economical method for the  
102 recovery of microalgal lutein (the main carotenoid) from *Chlorella vulgaris* (Deenu et  
103 al., 2013).

104 The mechanisms of US-induced disruption of microalgae species were also studied  
105 intensively (Gerde et al., 2012; Greenly and Tester, 2015; Halim et al., 2013; Ma et al.,  
106 2014). It was demonstrated that in the US process the microalgal cells can be ruptured  
107 by shock waves (Ma et al., 2014). US-treatment was evaluated for breaking  
108 heterotrophic (*Schizochytrium limacinum*) and autotrophic (*Chlamydomonas*  
109 *reinhardtii*) microalgae cells (Gerde et al., 2012). It was noted that the energy input  
110 required to reach the maximum disruption of cells was  $\approx 800$  J/10 ml irrespectively of  
111 cell concentration.

112 In addition, the impact of US-treatment on microalgae species with different sizes  
113 and cell wall compositions was studied (Greenly and Tester, 2015). It was demonstrated  
114 that the most significant disruption was observed in the initial period of sonication and  
115 at longer exposure times, differences between species were more pronounced.  
116 Disruption rate constant for US microalgal species (*Tetraselmis suecica* and  
117 *Chlorococcum sp.*) was directly proportional to US power and followed a parabolic  
118 relationship with initial cell concentration (Halim et al., 2013).

119 However, in most of the cases US-assisted extraction methods in applications to  
120 microalgae species were not comply with criteria of green chemistry concept. The  
121 efficient recovery of lipophilic compounds from microalgae commonly requires the use

122 of toxic solvents or intensive US-treatments that produce undesirable free radicals. At  
123 this stage of development, there is a lack of information about the US-assisted  
124 extraction based on application of green solvents.

125 This manuscript investigates the US-assisted solvent extraction of antioxidants and  
126 pigments (phenolic compounds and chlorophylls) from microalgae *Nannochloropsis*  
127 *spp*, which can be used as potential food additives and/or nutraceuticals. The individual  
128 green solvents (water, ethanol and dimethyl sulfoxide) or their mixtures were used as  
129 extraction media. The effects of US power, time of extraction, composition of the  
130 solvent and concentration of microalgae in suspension are discussed.

## 131 **2. Material and methods**

### 132 *2.1. Chemicals*

133 Sulfuric acid, methanolic HCl (3N), gallic acid, Folin–Ciocalteu reagent, and D-  
134 glucose were obtained from Sigma-Aldrich (Saint-Quentin Fallavier, France). Bovine  
135 Serum Albumin (BSA) standard was obtained from Thermo Scientific (USA). Sodium  
136 bicarbonate (Na<sub>2</sub>CO<sub>3</sub>) was obtained from VWR (France). Ethanol (EtOH) and dimethyl  
137 sulfoxide (DMSO) were obtained from Baker (Deventer, The Netherlands).

### 138 *2.2. Microalgae Nannochloropsis spp.*

139 *Nannochloropsis spp.* is a marine green algae belonging to the *Eustigmataceae*  
140 family. The cells have approximately spherical shapes, and the mean diameter of the  
141 completely swelled cells was found to be about 2 μm. For the experiments, a frozen  
142 algae paste of *Nannochloropsis spp.* (12–15% solid content) was used. The biomass was  
143 first thawed at ambient temperature and then diluted with deionized water (electrical  
144 conductivity ≈2μS/cm), in order to prepare algae suspensions with a final concentration

145 ( $C_m$ ) of 1, 3, 5 and 10 % wt. Other algae suspensions with a concentration ( $C_m$ ) of 1 %  
146 wt were also prepared by diluting the initial biomass either in pure organic solvents,  
147 such as Ethanol (EtOH) and DMSO, or in binary mixture of water and organic solvents  
148 at different concentration.

### 149 2.3. Ultrasound (US)-assisted solvent extraction

150 High-added value compounds such as polyphenols and chlorophylls, from  
151 *Nannochloropsis spp.* cells were extracted using US-assisted extraction and results were  
152 compared with conventional solvent extraction (E). US-assisted extraction was carried  
153 out using UP 400S ultrasound equipment (Hielscher GmbH, Germany) able to provide a  
154 maximum power ( $W$ ) of 400 W at a constant frequency ( $f$ ) of 24 kHz. The sonication  
155 probe, acting as a wave amplifier, was plunged into a beaker containing  $250\pm 5$  g of  
156 microalgae suspension in a proper extraction solvent as described above. The extraction  
157 time ( $t$ ) was varied within 0–30 min, while three different power ( $W$ ) of 100, 200 and  
158 400 W were applied (Grimi et al., 2014). The experiments were carried out with the  
159 sample at the initial temperature of 291 K (18 °C), while the maximum final  
160 temperature was lower than 333 K (60 °C), as measured by a thermocouple placed into  
161 the algae suspension. For the sake of comparison, conventional solvent extractions (E)  
162 using pure water as solvent were carried out using the same protocol as for US  
163 treatment, but with the power being switched off ( $W=0$  W).

164 During both conventional and US-assisted extraction, the samples were subjected to  
165 continuous magnetic stirring in 300 ml hermetically closed flasks. Samples of algae  
166 suspension collected after each extraction process were centrifuged at 14000 rpm for 5  
167 min using a MiniSpin Plus Rotor F-45-12-11 (Eppendorf, France) and the supernatant  
168 was taken for further analysis.

169 The yields of extraction of total phenolic compounds ( $Y_p$ ) and total chlorophylls ( $Y_c$ )  
170 were defined as follows:

$$171 \quad Y_p = C_p / C_p^m, \quad (1)$$

$$172 \quad Y_c = C_c / C_c^m, \quad (2)$$

173 where  $C_p$  and  $C_c$  are the concentrations of total phenolic compounds and total  
174 chlorophylls, respectively.

175 The superscript  $m$  denotes the maximum concentration of extract obtained after  
176 application of the procedure of high-throughput homogenization (H) in 100% DMSO.  
177 Preliminary investigations have shown that this cell disintegration technique allows the  
178 extraction of almost all intracellular compounds (Koubaa et al., 2015). In this work, 20  
179 mg of lyophilized microalgae, 1 ml of DMSO and 1 ceramic bead were mixed in screw  
180 tubes. Then, these tubes were placed to the high-throughput ball mill homogenizer  
181 (Precellys 24, Ozyme). The homogenization was carried out at 6,500 counts per min  
182 (cpm) for 3 min with 15 s pauses each minute. After homogenization the treated  
183 microalgae was washed with 1 ml of pure DMSO and centrifuged for 10 min at 14500  
184 rpm. This procedure was repeated 8 times for reaching constant values of concentration  
185 of valuable compounds. The supernatants were used to determine the different  
186 metabolite concentrations. The maximum concentrations were  $C_p^m = 14.9 \pm 0.8 \mu\text{g}/\text{mg}$   
187 DW (total phenolic compounds) and  $C_c^m = 26.34 \pm 0.9 \mu\text{g}/\text{mg}$  DW (total chlorophylls).

#### 188 *2.4. Chemical analysis of extracts*

189 Absorption spectra of the extracts (supernatant) were measured by UV-  
190 spectrophotometer Libra S32 (Biochrom, Lagny-sur-Marne, France). The wavelength  
191 range was within 300–800 nm against blank (with the precision of  $\pm 1$  nm). The path  
192 length of the SUPRASIL quartz cuvette was 10 mm (Hellma, Müllheim, Germany). The  
193 PeakFit program (Version 4.12, SeaSolve Software Inc.) was used for the spectral shape



194 analysis of the UV absorption bands and for their graphical deconvolution. The autofit  
195 baseline option was used to remove the baseline prior to deconvolution of peaks, their  
196 fitting and estimation of their intensity.

#### 197 2.4.1. Total phenolic compounds

198 Concentration of total phenolic compounds,  $C_p$ , (in  $\mu\text{g}$  of gallic acid equivalent/mg  
199 DW of biomass) was determined by the Folin–Ciocalteu method based on colorimetric  
200 oxidation/reduction reaction of phenols (Singleton et al., 1999). First, 0.2 ml of extract  
201 and 1 ml of Folin–Ciocalteu reagent (diluted 1:10 in water) were mixed. Afterwards, 0.8  
202 ml of  $\text{Na}_2\text{CO}_3$  (75 g/l) was added to this mixture. The sample was incubated for 10 min  
203 at 323 K, followed by cooling to room temperature ( $T=293$  K). The absorbance was  
204 then measured at 750 nm. Gallic acid was used for the calibration.

#### 205 2.4.2. Total chlorophylls

206 For pigments quantification, the maximum absorbancies of chlorophyll-a ( $A_c^a$ ) and  
207 chlorophyll-b ( $A_c^b$ ) were measured at 665 and 653 nm, respectively (Kumar et al.,  
208 2010). The concentrations of total chlorophylls ( $C_c$ , in mg of pigment/g DW) in the  
209 extracts were calculated according to the following equations (Arnon, 1949;  
210 Lichtenthaler and Wellburn, 1983):

211 For EtOH extract:

$$212 C_c = 4.34 A_c^a + 19.71 A_c^b \quad (3)$$

213 For DMSO extract:

$$214 C_c = 0.0202 A_c^a + 0.00802 A_c^b \quad (4)$$

215

## 216 2.5. Statistical Analysis

217 All experiments and analyses were repeated using at least five replicates. One-way  
218 analysis of variance was used for statistical analysis of the data using Statgraphics plus  
219 software (version 5.1, Statpoint Technologies Inc., Warrenton, VA). For each analysis,  
220 significance level of 5% was assumed. The error bars presented in the figures  
221 correspond to the standard deviations.

## 222 3. Results and discussion

223 Figure 1 shows the yield of total phenolic compounds,  $Y_p$ , versus extraction time  $t$  for  
224 the extracts obtained by US-assisted and conventional extraction (E) in water. The  
225 ultrasound power  $W$  was set at 400 W while the concentration of microalgae  
226 suspensions was 1%. The initial temperature of the biomass was  $T \approx 18$  °C. During the  
227 US-assisted extraction the temperature  $T$  of the sample increased owing to the input of  
228 the ultrasound energy. After  $\approx 20$  min of extraction the temperature stabilized at the level  
229  $\approx 68$  °C that corresponded to the equilibrium for the energy exchange between the  
230 suspension and its surrounding medium. This experiment was designated as US ( $T \uparrow$ ).

231 For comparison purposes, the conventional extraction in water was carried out under  
232 non-isothermal conditions using the same protocol of temperature increase as for the  
233 US-assisted extraction experiment. This hot water extraction experiment was designated  
234 as E ( $T \uparrow$ ). At the same time, US-assisted extraction at constant temperature  $T = 18$  °C  
235 was also carried out by placing the sample in a thermostatic bath.. This “cold” water  
236 US-extraction experiment was designated as US ( $T = 18$  °C).

237 Results of conventional extraction show that the  $Y_p(t)$  curves were saturated after  
238  $\approx 20$ -30 min of extraction. The extraction yields for US ( $T \uparrow$ )-assisted method is  $\approx 2$  times

239 higher than those for conventional hot water extraction E ( $T\uparrow$ ). However, it is worth  
240 noting that the sum of extraction yields of US ( $T=18\text{ }^{\circ}\text{C}$ ) and E ( $T\uparrow$ ) samples were  
241 approximately the same as for those of US ( $T\uparrow$ ) treated samples. Thus, the combination  
242 of US and temperature increase gave approximately an additive contribution into  
243 extraction efficiency. This reflects the absence of any synergy between the application  
244 of US with simultaneous increasing of temperature.

245 Figure 2 presents the effects of US power ( $W=0\text{-}400\text{ W}$ ) on the kinetics of extraction  
246 of total phenolic compounds,  $Y_p$ , (Figure 2a) and total chlorophylls,  $Y_c$ , (Figure 2b) in  
247 water. The values of  $Y_p$  and  $Y_c$  increased proportionally to the US power and increased  
248 with the elapse of treatment time. The maximum total phenolic compounds yield was  
249 obtained when using the highest power and the longer treatment time. E.g., extraction  
250 for 15 min at  $W=400\text{ W}$  resulted in  $Y_p \approx 0.33$  as compared with  $Y_p \approx 0.06$  for the control  
251 sample (conventional “cold” water extraction,  $W=0\text{ W}$ ).

252 Results of Figure 2b, instead, show that the highest yield of total chlorophylls was  
253 obtained after applying a US power of 400 W for 7.5 min, while longer treatment times  
254 led to a decrease in chlorophyll’s content. On the other hand, when US-assisted  
255 extraction was carried out at the lower power values (100 and 200 W), the extraction  
256 yield of chlorophyll showed an increasing trend with time. This different behaviour is  
257 likely attributed to the higher increase of temperature measured in the medium when US  
258 was applied at the higher power and during long treatment times, thus promoting the  
259 degradation of some thermolabile pigments (Chemat et al., 2011). In fact, it is well  
260 known that microalgae pigments are highly susceptible to thermal degradation which  
261 results in colour changes (Pasquet et al., 2011). Moreover, for long sonication times the  
262 produced free radicals can also induce degradation of extracted products (Gerde et al.,  
263 2012).

264 Finally, in comparison with control sample ( $W=0$  W,  $T=18$  °C), our findings clear  
265 show that US treatments allowed a significant increase in the chlorophyll recovery.  
266 These results were in close agreement with previously reported data (Kong et al., 2012),  
267 which showed a significant yield increase (+59%) for US-assisted extraction (200  
268 W/78.7 min/61.4 °C) of chlorophyll from *Chlorella vulgaris* as compared with  
269 conventional extraction process. The increased recovery of chlorophyll a and b for US-  
270 assisted extraction as compared to those obtained using conventional maceration and  
271 Soxhlet extraction was also found (Kwang et al., 2010). US-assisted extraction was also  
272 found to show higher extraction efficiency as compared with either conventional or  
273 other innovative technique such as supercritical fluid extraction and microwave assisted  
274 extraction, when applied to *Dunaliella salina*, *Dunaliella tertiolecta*, and *Cylindrotheca*  
275 *closterium* (Macías-Sánchez et al., 2009; Pasquet et al., 2011).

276 Figure 3 compares results of the extraction yields of total phenolic compounds,  $Y_p$ ,  
277 (Figure 3a) and total chlorophylls,  $Y_c$ , (Figure 3b) obtained during US-assisted  
278 extraction in pure solvents (H<sub>2</sub>O, EtOH, DMSO) at a fixed US power of 400 W. For  
279 total phenolic compounds, regardless the extraction solvent, the yield  $Y_p$  increased with  
280 time reaching the saturation after about 5 min of extraction. For total chlorophylls, the  
281 kinetic of extraction followed a different path depending on the extraction solvent.  
282 While in EtOH and water, the extraction yield  $Y_c$  reached a plateau after 7.5 min of US-  
283 assisted extraction, in DMSO  $Y_c$  reached a plateau after 5 min of extraction and  
284 decreased when longer extraction times (>7.5 min) were used. Thus, to prevent  
285 chlorophyll degradation an extraction time of 5 min was selected as optimum value for  
286 further experiments. Results of Figure 3 also show that at each fixed extraction time, the  
287 extraction efficiency of total phenolic compounds and total chlorophylls decreased in  
288 the order DMSO>EtOH>H<sub>2</sub>O. The efficiency of US-assisted extraction in binary

289 solvents (water-DMSO and water-EtOH) was also studied. This is because, although  
290 results of Figures 1-3 clearly show that US-assisted extraction was rather efficient for  
291 the recovery of total phenolic compounds even in pure water, the use of organic solvent  
292 was required for a more effective recovery of chlorophylls. Figure 4 presents the yields  
293 of total phenolic compounds,  $Y_p$ , and total chlorophylls,  $Y_c$ , versus concentration ( $C$ ) of  
294 organic solvent (DMSO or EtOH), for US-assisted extraction in binary solvents  
295 H<sub>2</sub>O+DMSO (Figure 4a) and H<sub>2</sub>O+EtOH (Figure 4b). Results show that a significant  
296 increase in the amount of total phenolic compounds and chlorophylls was observed both  
297 in DMSO and EtOH when solvent's concentration  $C$  was above 25-30%.

298 Moreover, the efficiency of US-assisted extraction versus concentration of  
299 microalgae in suspension,  $C_m$ , was also investigated. Figure 5 presents of the extraction  
300 yields of total phenolic compounds,  $Y_p$ , and total chlorophylls,  $Y_c$ , versus concentration  
301 ( $C_m$ ) of microalgae in suspension for US-assisted extraction in binary solvents  
302 H<sub>2</sub>O+EtOH( $C=50\%$  wt). In the same graph also the energy input per kg of microalgae  
303 (DW) has been reported. From the results it can be seen that both yields  $Y_p$  and  $Y_c$   
304 follow a similar trend showing a minimum value for a biomass concentration  $C_m \approx 5\%$   
305 wt. This behaviour is surprising and we have no reasonable explanation of this  
306 phenomenon. However, it is likely that the concentration dependence can reflect the  
307 changes in the efficiency of cell damage by US waves related with the intensity of  
308 cavitating gas bubbles. The mechanisms of interaction of US with microalgae cells, of  
309 cell destruction and cell precipitation were recently discussed (Faerman et al., 2002). It  
310 was demonstrated that US could precipitate the cells in highly concentrated  
311 suspensions. The phenomenon of precipitation was explained by dissolution of micro-  
312 bubble carbon dioxide and removal of gas bubbles.

313 Finally, it should be noted that US-assisted recovery from concentrated suspension is  
314 less power consuming. E.g., the increase of concentration  $C_m$  from 1% wt to 10% wt  
315 resulted in  $\approx 10$ -fold decrease of US power consumption at approximately the same  
316 efficiency of extraction of total phenolic compounds and total chlorophylls.

#### 317 **4. Conclusions**

318 Ultrasound-assisted solvent extraction was shown as a promising tool to recover  
319 high-added value compounds from microalgae *Nannochloropsis*. The extraction yields  
320 for US-assisted method was  $\approx 2$  times higher than for conventional hot water extraction.  
321 Degradation of chlorophylls was observed at long treatment time. The 5 min duration of  
322 US-assisted extraction was selected as optimal to prevent degradation of chlorophylls.  
323 The recovery efficiency of phenolic compounds and chlorophylls decreased in the raw  
324 DMSO>EtOH>H<sub>2</sub>O. In addition, when binary solvents (water-DMSO and water-EtOH)  
325 were used, the highest recovery of valuable compounds was observed when  
326 concentration of organic component was above 25-30% for both solvents.

#### 327 **Acknowledgements**

328 The authors appreciate the support from the COST Action TD1104 (EP4Bio2Med -  
329 European network for development of electroporation-based technologies and  
330 treatments). E. Apicella is indebted to the Campania Region for having provided a  
331 scholarship, in the frame of the Project C.A.R.I.N.A. (cod. 4-17-10) funded through  
332 POR Campania FSE 2007-2013, Assi IV e V, to support her research stage at the  
333 University of Compiègne. F. J. Barba thanks the Valencian Autonomous Government  
334 (Consellería d'Educació, Cultura i Esport. Generalitat Valenciana) for the postdoctoral

335 fellowship of the VALi+d program “Programa VALi+d per a investigadors en fase  
336 postdoctoral 2013” (APOSTD/2013/092).

### 337 **References**

338 Adam, F., Abert-Vian, M., Peltier, G., Chemat, F., 2012. “Solvent-free” ultrasound-  
339 assisted extraction of lipids from fresh microalgae cells: A green, clean and scalable  
340 process. *Bioresour. Technol.* 114, 457–465.

341 Araujo, G.S., Matos, L.J.B.L., Fernandes, J.O., Cartaxo, S.J.M., Gonçalves, L.R.B.,  
342 Fernandes, F.A.N., Farias, W.R.L., 2013. Extraction of lipids from microalgae by  
343 ultrasound application: Prospection of the optimal extraction method. *Ultrason.*  
344 *Sonochem.* 20, 95–98.

345 Arnon, D.I., 1949. Copper enzymes in isolated chloroplasts, polyphenoxidase in *Beta*  
346 *vulgaris*. *Plant Physiol.* 24, 1–15.

347 Barba, F.J., Grimi, N., Vorobiev, E., 2014. New approaches for the use of non-  
348 conventional cell disruption technologies to extract potential food additives and  
349 nutraceuticals from microalgae. *Food Eng. Rev.* 7, 45–62.

350 Bermúdez Menéndez, J.M., Arenillas, A., Menéndez Díaz, J.A., Boffa, L., Mantegna,  
351 S., Binello, A., Cravotto, G., 2014. Optimization of microalgae oil extraction under  
352 ultrasound and microwave irradiation. *J. Chem. Technol. Biotechnol.* 89, 1779–1784.

353 Chemat, F., Zill-E-Huma, Khan, M.K., 2011. Applications of ultrasound in food  
354 technology: Processing, preservation and extraction. *Ultrason. Sonochem.* 18, 813–  
355 835.

356 Cravotto, G., Boffa, L., Mantegna, S., Perego, P., Avogadro, M., Cintas, P., 2008.  
357 Improved extraction of vegetable oils under high-intensity ultrasound and/or  
358 microwaves. *Ultrason. Sonochem.* 15, 898–902.

359 Deenu, A., Naruenartwongsakul, S., Kim, S.M., 2013. Optimization and economic  
360 evaluation of ultrasound extraction of lutein from *Chlorella vulgaris*. *Biotechnol.*  
361 *Bioprocess Eng.* 18, 1151–1162.

362 Dufossé, L., Galaup, P., Yaron, A., Arad, S.M., Blanc, P., Chidambara Murthy, K.N.,  
363 Ravishankar, G.A., 2005. Microorganisms and microalgae as sources of pigments for  
364 food use: a scientific oddity or an industrial reality? *Trends Food Sci. Technol.* 16,  
365 389–406.

366 Faerman, V., Mukmenev, I., Shreiber, I., 2002. Sonication of microalgae and its  
367 precipitation. *Acta Acust. united with Acust.* 88, 592–593.

368 Gerde, J.A., Montalbo-Lomboy, M., Yao, L., Grewell, D., Wang, T., 2012. Evaluation  
369 of microalgae cell disruption by ultrasonic treatment. *Bioresour. Technol.* 125, 175–  
370 181.

371 Greenly, J.M., Tester, J.W., 2015. Ultrasonic cavitation for disruption of microalgae.  
372 *Bioresour. Technol.* 184, 276–279.

373 Grimi, N., Dubois, A., Marchal, L., Jubeau, S., Lebovka, N.I., Vorobiev, E., 2014.  
374 Selective extraction from microalgae *Nannochloropsis* sp. using different methods of  
375 cell disruption. *Bioresour. Technol.* 153, 254–259.

376 Halim, R., Rupasinghe, T.W.T., Tull, D.L., Webley, P.A., 2013. Mechanical cell  
377 disruption for lipid extraction from microalgal biomass. *Bioresour. Technol.* 140,  
378 53–63.

379 Keris-Sen, U.D., Sen, U., Soydemir, G., Gurol, M.D., 2014. An investigation of  
380 ultrasound effect on microalgal cell integrity and lipid extraction efficiency.  
381 *Bioresour. Technol.* 152, 407–413.

382 Kong, W., Liu, N., Zhang, J., Yang, Q., Hua, S., Song, H., Xia, C., 2012. Optimization  
383 of ultrasound-assisted extraction parameters of chlorophyll from *Chlorella vulgaris*



384 residue after lipid separation using response surface methodology. *J. Food Sci.*  
385 *Technol.* 1–8.

386 Koubaa, M., Mhemdi, H., Vorobiev, E., 2015. Seed oil polyphenols: Rapid and  
387 sensitive extraction method and high resolution-mass spectrometry identification.  
388 *Anal. Biochem.* 476, 91–93.

389 Kumar, P., Ramakritinan, C.M., Kumaraguru, A.K., 2010. Solvent extraction and  
390 spectrophotometric determination of pigments of some algal species from the shore  
391 of puthumadam, southeast coast of India. *Int. J. Ocean. Oceanogr.* 4, 29–34.

392 Kwang, H.C., Lee, H.J., Koo, S.Y., Song, D.-G., Lee, D.-U., Pan, C.-H., 2010.  
393 Optimization of pressurized liquid extraction of carotenoids and chlorophylls from  
394 *Chlorella vulgaris*. *J. Agric. Food Chem.* 58, 793–797.

395 Lichtenthaler, H.K., Wellburn, A.R., 1983. Determinations of total carotenoids and  
396 chlorophylls a and b of leaf extracts in different solvents. *Biochem. Soc. Trans.* 11,  
397 591–592.

398 Ma, G., Hu, W., Pei, H., Jiang, L., Song, M., Mu, R., 2015. In situ  
399 heterogeneous transesterification of microalgae using combined ultrasound and  
400 microwave irradiation. *Energy Convers. Manag.* 90, 41–46.

401 Ma, Y.-A., Cheng, Y.-M., Huang, J.-W., Jen, J.-F., Huang, Y.-S., Yu, C.-C., 2014.  
402 Effects of ultrasonic and microwave pretreatments on lipid extraction of microalgae.  
403 *Bioprocess Biosyst. Eng.* 37(8), 1543-1549.

404 Macías-Sánchez, M.D., Mantell, C., Rodríguez, M., de la Ossa, E., Lubián, L.M.,  
405 Montero, O., 2009. Comparison of supercritical fluid and ultrasound-assisted  
406 extraction of carotenoids and chlorophyll a from *Dunaliella salina*. *Talanta* 77, 948–  
407 952.

408 Natarajan, R., Ang, W.M.R., Chen, X., Voigtmann, M., Lau, R., 2014. Lipid releasing  
409 characteristics of microalgae species through continuous ultrasonication. *Bioresour.*  
410 *Technol.* 158, 7–11.

411 Pasquet, V., Chérouvrier, J.-R., Farhat, F., Thiéry, V., Piot, J.-M., Bérard, J.-B., Kaas,  
412 R., Serive, B., Patrice, T., Cadoret, J.-P., Picot, L., 2011. Study on the microalgal  
413 pigments extraction process: Performance of microwave assisted extraction. *Process*  
414 *Biochem.* 46, 59–67.

415 Plaza, M., Santoyo, S., Jaime, L., Avalo, B., Cifuentes, A., Reglero, G., García-Blairsy  
416 Reina, G., Señoráns, F.J., Ibáñez, E., 2012. Comprehensive characterization of the  
417 functional activities of pressurized liquid and ultrasound-assisted extracts from  
418 *Chlorella vulgaris*. *LWT - Food Sci. Technol.* 46, 245–253.

419 Qv, X.-Y., Zhou, Q.-F., Jiang, J.-G., 2014. Ultrasound-enhanced and microwave-  
420 assisted extraction of lipid from *Dunaliella tertiolecta* and fatty acid profile analysis.  
421 *J. Sep. Sci.* 37, 2991–2999. doi:10.1002/jssc.201400458

422 Roselló-Soto, E., Galanakis, C.M., Brnčić, M., Orlie, V., Trujillo, F.J., Mawson, R.,  
423 Knoerzer, K., Tiwari, B.K., Barba, F.J., 2015. Clean recovery of antioxidant  
424 compounds from plant foods, by-products and algae assisted by ultrasounds  
425 processing. Modeling approaches to optimize processing conditions. *Trends Food*  
426 *Sci. Technol.* 42(2), 134-149.

427 Singleton, V.L., Orthofer, R., Lamuela-Raventos, R.M., 1999. Analysis of total phenols  
428 and other oxidation substrates and antioxidants by means of Folin-Ciocalteu  
429 reagent. *Methods Enzymol.* 299, 152–178.

430 Sun, J., Song, T., Sun, X., Song, J., Wang, C., Qiao, D., 2014. Extraction optimization  
431 of intracellular polysaccharide and lipid from oleaginous *Chlorella protothecoides*.  
432 *Chinese J. Appl. Environ. Biol.* 20, 615–620.

433

434 **Figure captions:**

435 **Fig. 1.** Yields of total phenolic compounds,  $Y_p$ , versus extraction time,  $t$ , for extracts  
436 obtained by US-assisted and conventional extraction (E) in water. The ultrasound power  
437 was  $W=400$  W; the concentration of microalgae suspensions was  $C_m=1\%$  wt. The data  
438 are presented for non-isothermal protocol ( $T\uparrow$ ) and isothermal protocol ( $T=18$  °C). The  
439 symbol  $T$  in the legend refers to the evolution of temperature during either US ( $T\uparrow$ )-  
440 assisted extraction or conventional extraction E( $T\uparrow$ ). Dashed line corresponds to the  
441 sum of the extraction yields obtained after US ( $T=18$  °C) and E( $T\uparrow$ ).

442

443 **Fig. 2.** (a) Yield of total phenolic compounds,  $Y_p$ , and (b) total chlorophylls,  $Y_c$ , versus  
444 time of US-assisted extraction in water at different applied ultrasound powers (0-400  
445 W).  $C_m=1\%$  wt. “Cold” water extraction for control sample ( $W=0$  W) was done at the  
446 fixed temperature,  $T=18$ °C.

447

448 **Fig. 3.** (a) Yields of total phenolic compounds,  $Y_p$ , and (b) total chlorophylls,  $Y_c$ , versus  
449 time of US-assisted extraction in individual solvents ( $H_2O$ , EtOH, DMSO). The  
450 ultrasound power was  $W=400$  W; the concentration of microalgae suspensions was  
451  $C_m=1\%$  wt; the initial temperature was  $18$ °C.

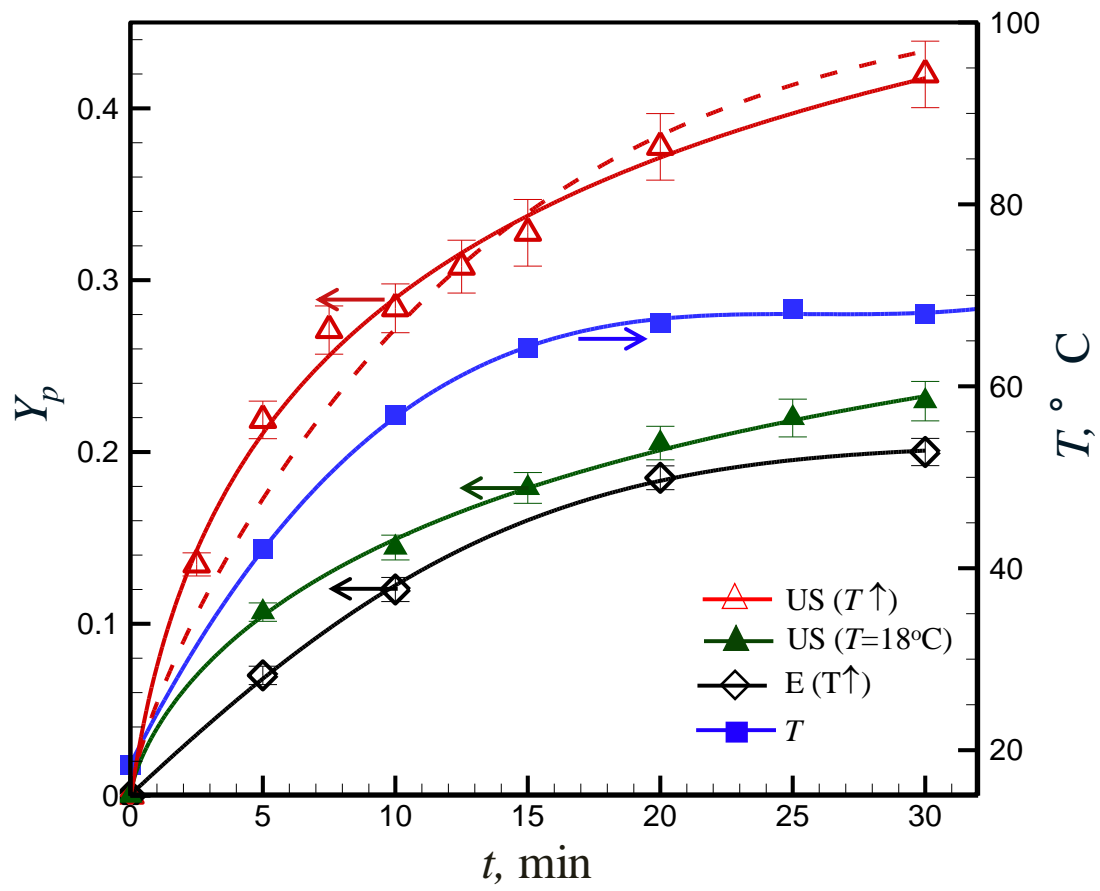
452

453 **Fig. 4.** Yields of total phenolic compounds,  $Y_p$ , and total chlorophylls,  $Y_c$ , versus  
454 concentration of organic solvent,  $C$ , for US-assisted extraction in binary solvents  
455  $H_2O$ +DMSO (a) and  $H_2O$ +EtOH (b). The ultrasound power was  $W=400$  W; the  
456 concentration of microalgae suspensions was  $C_m=1\%$  wt; the initial temperature was  
457  $18$ °C; and the time of extraction was  $t=5$  min.

458

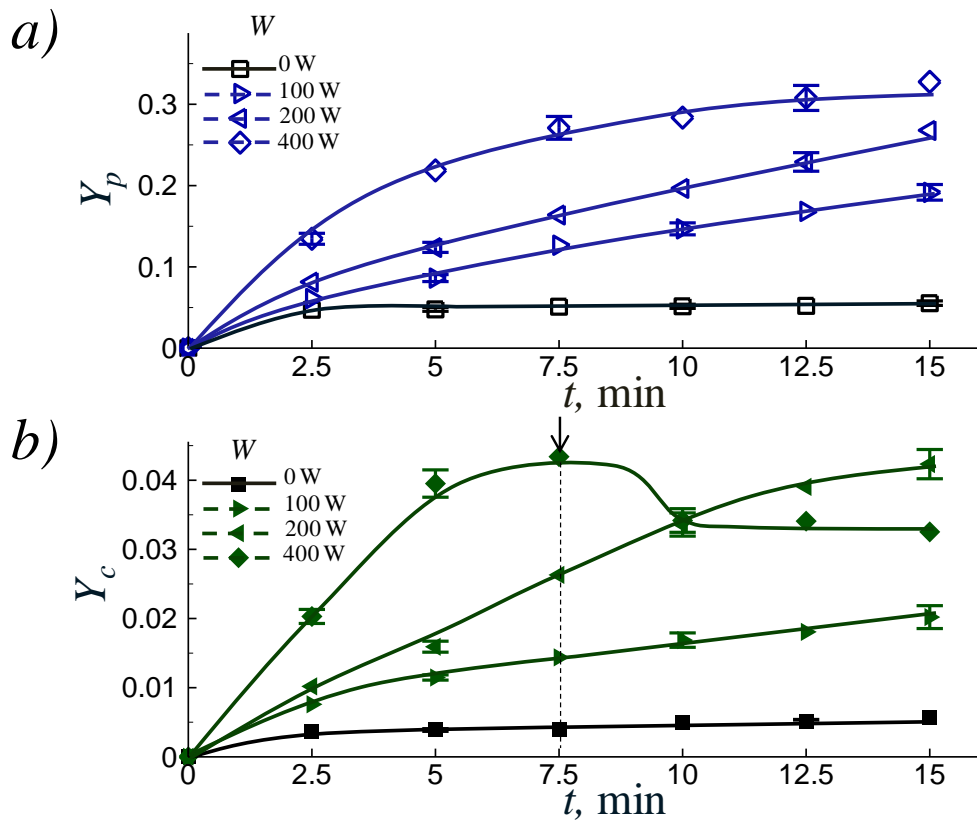
459 **Fig. 5.** Yields of total phenolic compounds,  $Y_p$ , and total chlorophylls,  $Y_c$ , versus  
460 concentration of microalgae in suspension,  $C_m$ , for US-assisted extraction in binary  
461 solvents H<sub>2</sub>O+EtOH (C=50% wt). The ultrasound power was  $W=400$  W; the initial  
462 temperature was 18°C; and the time of extraction was  $t= 5$  min. The upper horizontal  
463 axis presents the energy input per kg of microalgae (DW).  
464

465 Figure 1



466

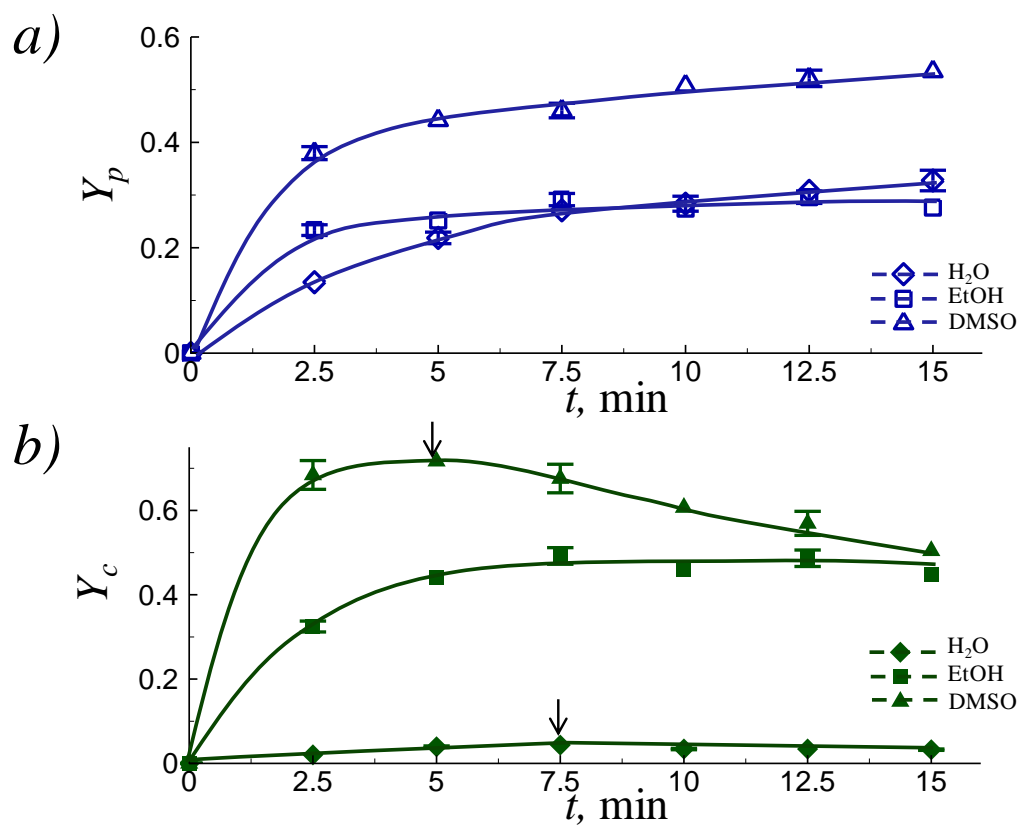
467



469

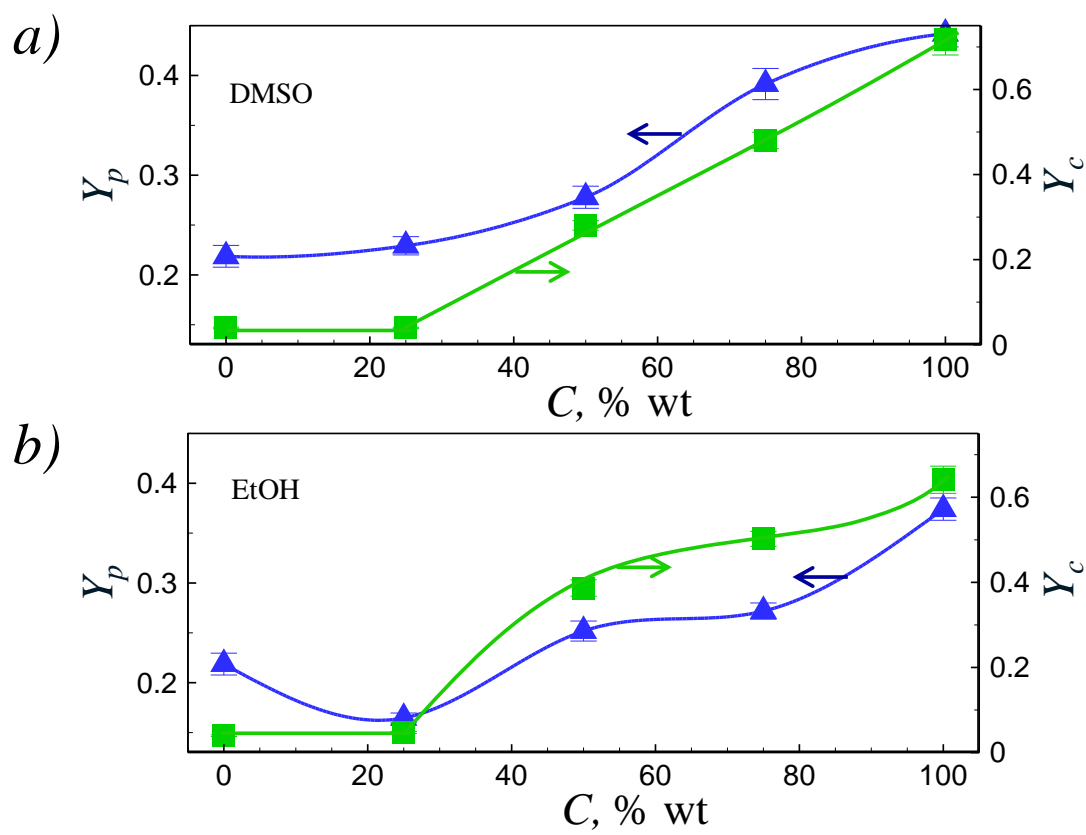
470

471 Figure 3



472

473

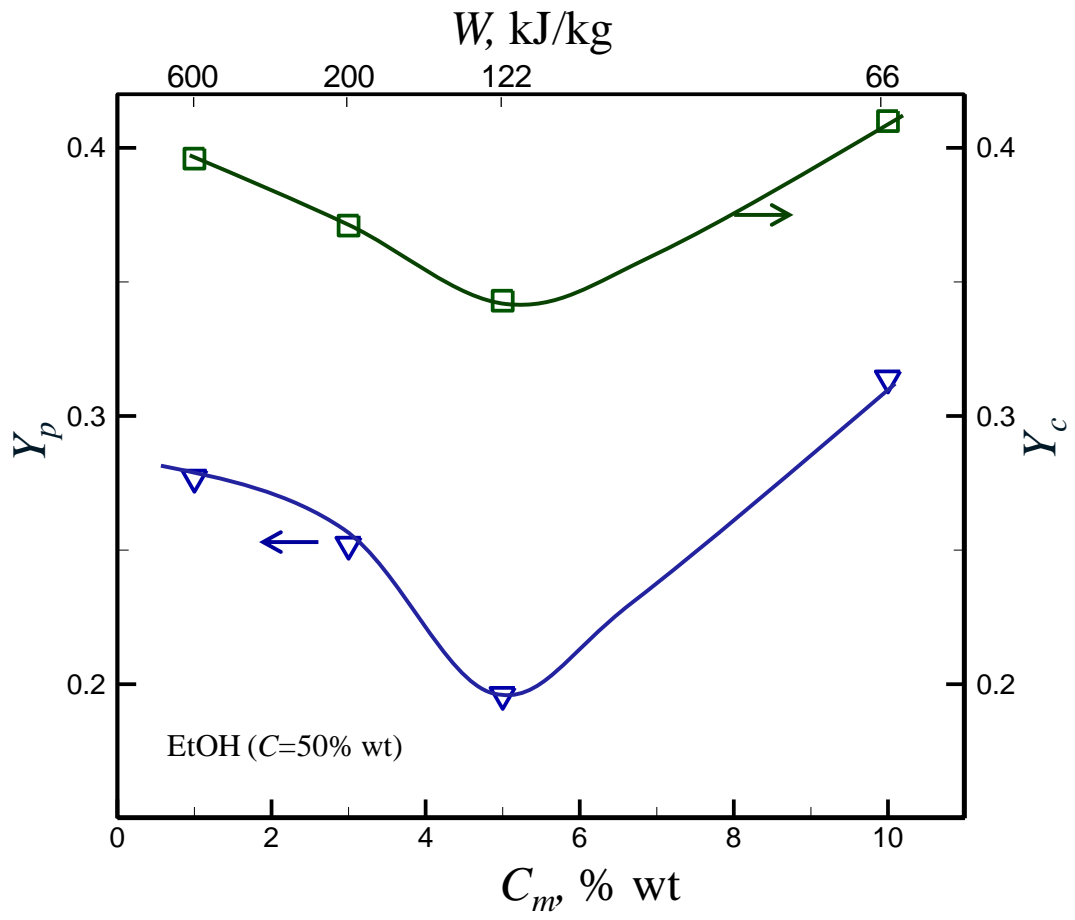


475

476



477 Figure 5



478

479