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### Deinking in a Closed Loop and the Effects of Solids on Paper Properties

by

Chad H. Warmbier

A Thesis submitted in partial fulfillment of the course requirements for The Bachelor of Engineering Degree

Western Michigan University

Kalamazoo, Michigan

April 11, 1996



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#### Deinking in a Closed Loop and the Effects of Solids on Paper Properties

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Chad Henry Warmbier

Advisor: Dr. David Peterson

April 11, 1996

#### ABSTRAČT:

Deinking is of critical importance to the reuse of secondary fiber in the paper industry. As with all papermaking processes there is a definite concern on the final quality of the product and the waste that is generated. Waste problems are a growing concern and with tighter discharge limits there is a growing concern of how to deal with these problems. One solution to this problem is the idea of a closed cycle deinking process which reutilizes the wastewater stream for pulping and recovering of usable fiber which is otherwise lost to the system. As with everything there are problems that can occur when implementing a system such as this. The focus of this project is to determine if there is solids build up within the deinking and paper making loop and if there indeed is show these effects on the final paper by testing the whitewater and comparing those tests to the physical properties of the paper. From the results of the whitewater tests there does seem to be a build up of suspended material within the system, but contrary to the initial belief the amount of dissolved material in the system actually decreased. Trends were also observed when comparing TSS and TDS to tensile and tear indexes. It seemed that both were effected by dissolved material and tensile was effected by suspended material both deal with bonding potential. It was also seen and will be explained in more detail that the optical properties of paper were not effected namely opacity and brightness but, scattering coefficient was slightly effected by the increase in suspended solids. The following parts of this report will go through the actual data and trends and will also go through the background and experimentation that was completed.

## TABLE OF CONTENTS:

Abstract overview of the entire project	page 1
Introduction importance of study	page 3
Background discussion	page 4
Closed Loop Deinking: Focus	page 5
Experimental Procedures	page 6
Process flow diagram	page 7
Results presentation	page 8
Tables of results	pages 9-11
Formula sheet for data calculations	page 12
Discussion of results	pages 13-15
Conclusions	pages 16-17
Recommendations	page 18
Literature cited	page 19
Appendix	page 20
Graphs	
Total suspended and dissolved solids	page 21
TSS vs. Strength Properties	page 22
TDS vs. Strength Properties	page 23
Tensile changes over time and solids increase	page 24
TSS vs. opacity and scattering coefficient	page 25
TSS vs. brightness	page 26

#### INTRODUCTION:

In recent times recycling has become and to some extent always has been a major source of secondary fiber in the paper industry. Today by either government or consumer demand the use of secondary fiber has increased and the quality of the products produced has also needed to be increased. A major part in the recycling of secondary fiber is the deinking process. Deinking is a fundamentally laundering operation. Once the ink has been removed from the fiber by chemical or mechanical means, there are three basic approaches to removing the ink from the aqueous pulp slurry: washing, froth flotation, and other mechanical devices. However, due to more stringent regulations on discharges of waste and the growing landfill problems, alternative processes must now be considered to reutilize some of the waste stream in the deinking process. Reutilization of the waste through a new process called a "closed loop" would allow for the recovery of usable fiber which is otherwise lost to the waste treatment facility. The focus of this project was to see how a system such as that affects the overall quality of the final product.

#### BACKGROUND DISCUSSION:

In looking through the literature nothing substantial was found on the subject of closed cycle deinking. However, a study done by NCASI turned up to show the feasibility of implementing such a system and the overall cost (1). The study did not have any data on the effects of such a system once it was in operation, but the article did state that there were definite areas of study that needed to be taken care of in order to effectively implement this kind of system in order to have the least amount of problems. The areas of concern were mostly on the effect of the closed system on the equipment and runnability of the paper machine. However, the focus of this project was to determine the effects of solids build-up within the system and to determine the effects of these solids on the outcome of the final product. The NCASI study also reported that there had not been any pilot or bench type studies on these effects. The remaining literature gave a good background in the various types of deinking processes and how chemicals are used to remove the ink from the fiber (2,3,4,5,7). Along with the concerns of product quality and the effective wear on the machinery, there were other positive notes on how a system such as this would benefit the waste handling, and the environment. The main benefits would be a reduced water requirement, any toxic chemicals coming in with the pulp would be totally contained and be easier to handle, and the waste discharges would be greatly reduced to the wastewater treatment plant and to the landfill.

#### CLOSED<sup>T</sup> LOOP DEINKING: FOCUS

The main focus of this project was to see how the reutilization of water and rejects effects the physical and optical properties of paper (i.e. tensile, tear, brightness, opacity, and scattering coefficient). This would also incorporate the comparison of these physical properties to the results of whitewater tests which were run on the white water during the sheet making process. These tests included total suspended and dissolved solids which were then used to show the effects of the solids on the above paper properties.

#### EXPERIMENTAL PROCEDURES:

The deinking process was of basic design which included a flotation stage and a washing stage done on the laboratory sidehill screen. Old newspapers were obtained from the Kalamazoo Gazette that contained 66% thermomechanical pulp and 33% of recycle stock of which 70% was old newspaper and 30% was of magazine stock. The process consisted of five runs each of which started out being pulped in a laboratory Morden slushmaker at 4% consistency for 10 minutes. The pulped stock was transferred to a dilution tank and diluted down to 0.75% consistency. After being thoroughly mixed a surfactant from Shell Corporation (Lionsurf) was added at a fixed addition level of 10 milliliters per batch. The stock was then deinked in the laboratory flotation cell and pumped to a sidehill screen to be washed. The washed accepts from the screen were then used to make handsheets and the rejects and water were used as the pulping water for the next run. The accepted stock was used to make 60 grams/meter squared handsheets at a sheet weight of 2.5 grams. Five sheets were made from each run and after each batch a whitewater sample was taken to run total suspended and dissolved solids. The handsheets were then conditioned and then tested for tensile, tear, brightness, opacity, and scattering coefficient. (A simple flow diagram of the stock flows appears on the first page of the appendix)



#### **RESULTS PRESENTATION:**

The results from the handsheet and whitewater testing are shown in Tables I-V with formulas of the various calculations at the end. In table I the consistencies for the five runs were at or near 1.0% consistency. Table II shows the average readings for the handsheets for basis weight (55.7-61.88 g/m2), brightness (42-46%), opacity (93-98%), and scattering coefficient (42-48%). Table III shows the results of the whitewater tests showing total suspended solids (TSS) ranging from 12.5 to 36 mg/L and total dissolved solids (TDS) ranging from 78 to 88.5 mg/L. Tables IV and V show the results and calculation of tear and tensile index.

в

	Consistency (	Calculation	2	:		
Run #	Filter nad v	wt (a) Pu	un weight (g)	Pad weight (g)	Consistency %	
	1 <del>2</del>	1 71	520 51	6 57	0.018	
	1 ,	1.71	267 04	0.07	1 030	
	2	1.01	207.04	4.50	1.000	
	Ζ.	1.04	219.29	3.00	1.000	
-	0		100.10	3.1 2.54	1.101	• \$
	3	1.00	202.07	3.01	0.903	
		1.02	240.7	3.77	0.893	
	4	1.62	1/3.61	_3.17	0.893	
		1.66	247.95	3.86	0.887	
	5	1.67	232.27	3.57	0.818	
~ `	•	1.56	254.86	3.67	0.828	
	% Consist	ency = X - `	Y/Z *100			
	X=Pad we	ight				
	Y=Filter w	eiaht				
	Z=Pulo we	eiaht				
Table II:	Handsheet I	Data	- A. 1. 1		•	
Run #	Basis Wei	aht Br	inhtness	Opacity	Scattering Coe	officient
	1	59 66	16 226	02 18	12 10	
	2	68 42	40.220	07 N/	42.15	
	2	67 <i>11</i>	42.040	97.04	42.75	
	3	57.44	40.094	93.01	40.1	
	4	55.7	45.46	98.20	45.31	
	5	61.88	43.546	97.71	48.46	
<b>-</b>						
l able III	: Whitewater	lesting R	esults	Sample Volum	ie 100 mL	• • • • • • • • •
Run#						Averane
	Tin#	FI	ter+sample wt.	Dry weight(g)	155 (mg/L)	Average -
	Tin# 1	۲۳ 1	ter+sample wt	1.367	155 (mg/L) 13	12.5
	Tin# 1	+⊪ 1 2	ter+sample wt. 1.3657 1.3781	1.367 1.3793	135 (mg/L) 13 12	12.5
	Tin# 1 2	1 2 3	ter+sample wt. 1.3657 1.3781 1.37	1.367 1.3793 1.372	135 (mg/L) 13 12 20	12.5 19.5
	Tin# 1 2	1 2 3 4	ter+sample wt. 1.3657 1.3781 1.37 1.3722	1.367 1.3793 1.372 1.372 1.3741	135 (mg/L) 13 12 20 19	12.5 19.5
	Tin# 1 2 3	1 2 3 4 5	ter+sample wt 1.3657 1.3781 1.37 1.3722 1.3683	1.367 1.3793 1.372 1.3741 1.3709	135 (mg/L) 13 12 20 19 26	12.5 19.5 27
	Tin# 1 2 3	1 2 3 4 5 6	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37	1.367 1.3793 1.372 1.3741 1.3709 1.3728	13 13 12 20 19 26 28	12.5 19.5 27
	Tin# 1 2 3 4	Fii 1 2 3 4 5 6 7	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644	1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673	13 13 12 20 19 26 28 29	12.5 19.5 27 29
	Tin# 1 2 3 4	1 2 3 4 5 6 7 8	ter+sample wt 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3675	1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3704	135 (mg/L) 13 12 20 19 26 28 29 29	12.5 19.5 27 29
	Tin# 1 2 3 4 5	1 2 3 4 5 6 7 8 9	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3675 1.3746	1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3704 1.3783	13 13 12 20 19 26 28 29 29 37	12.5 19.5 27 29 36
	Tin# 1 2 3 4 5	FII 1 2 3 4 5 6 7 8 9 10	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645	1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3704 1.3783 1.3783 1.368	135 (mg/L) 13 12 20 19 26 28 29 29 37 35	12.5 19.5 27 29 36
	Tin# 1 2 3 4 5	Fii 1 2 3 4 5 6 7 8 9 10	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3675 1.3746 1.3645	1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3704 1.3783 1.368	13 13 12 20 19 26 28 29 29 37 35	12.5 19.5 27 29 36
Run#	Tin# 1 2 3 4 5 Tin#	Fii 1 2 3 4 5 6 7 8 9 10	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645	Dry weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.3783 1.3783 1.368	135 (mg/L) 13 12 20 19 26 28 29 29 29 37 35	12.5 19.5 27 29 36
Run#	Tin# 1 2 3 4 5 Tin#	Fii 1 2 3 4 5 6 7 8 9 10 Pa	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3644 1.3645 1.3746 1.3645 an weight(g) 1.2544	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.3704 1.3783 1.368 Dry Weight(g) 1.2632	TDS (mg/L) 13 12 20 19 26 28 29 37 35 TDS (mg/L)	12.5 19.5 27 29 36 Average
Run#	Tin# 1 2 3 4 5 Tin# 1	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3675 1.3746 1.3645 an weight(g) 1.2544 1.2606	Dry weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3704 1.3783 1.368 Dry Weight(g) 1.2632 1.2655	TDS (mg/L) 13 12 20 19 26 28 29 37 35 TDS (mg/L) 88 20	12.5 19.5 27 29 36 Average 88.5
Run#	Tin# 1 2 3 4 5 Tin# 1	Fii 1 2 3 4 5 6 7 8 9 10 10 Pa 11 12	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.3746 1.3645 1.3645 1.3645	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.3783 1.368 Dry Weight(g) 1.2632 1.2695 1.2695	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 20	Average 88.5
Run#	Tin# 1 2 3 4 5 Tin# 1 2	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11 12 13	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3644 1.3645 1.3746 1.3645 an weight(g) 1.2544 1.2606 1.2566	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.3704 1.3783 1.368 Dry Weight(g) 1.2632 1.2695 1.2649	TDS (mg/L) 13 12 20 19 26 28 29 37 35 TDS (mg/L) 88 89 83	Average 88.5 83.5
Run#	Tin# 1 2 3 4 5 5 Tin# 1 2	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11 12 13 14	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.3645 1.2544 1.2606 1.2566 1.2644	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.3704 1.3783 1.368 Dry Weight(g) 1.2632 1.2695 1.2649 1.2728	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 83 84	Average 88.5 83.5
Run#	Tin# 1 2 3 4 5 Tin# 1 2 3	Fii 1 2 3 4 5 6 7 8 9 10 7 8 9 10 7 8 9 10 7 8 11 12 13 14 15	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3675 1.3746 1.3645 an weight(g) 1.2544 1.2606 1.2566 1.2644 1.263	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3704 1.3704 1.3783 1.368 Dry Weight(g) 1.2632 1.2695 1.2649 1.2728 1.2713	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 83 84 83	Average 88.5 83.5 83.5
Run#	Tin# 1 2 3 4 5 Tin# 1 2 3	Fii 1 2 3 4 5 6 7 8 9 10 7 8 9 10 7 8 9 10 7 8 9 10 7 8 9 10 7 8 9 10 7 8 11 12 13 14 15 16	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.2544 1.2606 1.2566 1.2644 1.263 1.2597	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.368 Dry Weight(g) 1.2632 1.2695 1.2649 1.2728 1.2713 1.268	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 83 84 83 83	Average 88.5 83.5 83
Run#	Tin# 1 2 3 4 5 Tin# 1 2 3 4	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11 12 13 14 15 16 17	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.3746 1.2544 1.2606 1.2566 1.2566 1.2644 1.263 1.2597 1.2802	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.368 Dry Weight(g) 1.2632 1.2695 1.2649 1.2728 1.2713 1.268 1.2884	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 83 84 83 83 82	Average 88.5 83.5 78
Run#	Tin# 1 2 3 4 5 Tin# 1 2 3 4	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11 12 13 14 15 16 17 18	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.3746 1.2544 1.2606 1.2566 1.2597 1.2802 1.2661	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.368 Dry Weight(g) 1.2632 1.2695 1.2649 1.2728 1.2713 1.268 1.2884 1.2735	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 83 84 83 84 83 82 74	Average 88.5 83.5 78
Run#	Tin# 1 2 3 4 5 Tin# 1 2 3 4 5	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11 12 13 14 15 16 17 18 19	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.3746 1.2544 1.2606 1.2566 1.2644 1.263 1.2802 1.2661 1.2642	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3704 1.3704 1.3783 1.368 Dry Weight(g) 1.2632 1.2695 1.2695 1.2695 1.2649 1.2728 1.2713 1.2884 1.2735 1.2725	TDS (mg/L) 13 12 20 19 26 28 29 29 37 35 TDS (mg/L) 88 89 83 84 83 83 84 83 83 84 83 83 83 83 83 83 83 83 83 83	Average 88.5 83.5 84.5
Run#	Tin# 1 2 3 4 5 Tin# 1 2 3 4 5	Fii 1 2 3 4 5 6 7 8 9 10 Pa 11 12 13 14 15 16 17 18 19 20	ter+sample wt. 1.3657 1.3781 1.37 1.3722 1.3683 1.37 1.3644 1.3645 1.3746 1.3645 1.3746 1.3645 1.3746 1.2544 1.2606 1.2566 1.2597 1.2802 1.2661 1.2642 1.2547	Dry Weight(g) 1.367 1.3793 1.372 1.3741 1.3709 1.3728 1.3673 1.3673 1.368 Dry Weight(g) 1.2632 1.2695 1.2649 1.2728 1.2713 1.268 1.2735 1.2725 1.2633	TDS (mg/L) 13 12 20 19 26 28 29 37 35 TDS (mg/L) 88 89 83 84 83 83 82 74 83 86	Average 88.5 83.5 84.5

Table IV: Tensile Data				
Run # Sheet # Tensile	Value	Average	kgf	<b>Tensile Index</b>
1 7 1	2.505 2.679	2.592	1.18	12.882
2	1.756	1.9395	0.88	9.639
3	2.572	2.721	1.23	13.523
4	2.706	2.6765	1.21	13.302
5	1.774	1.816	0.82	9.025
Average Tensile Index for Dur		11 67		
	2 526	3 165	1 <i>1 1</i>	13 716
Ζ Ι	2.520	5.105	1.44	15.7 10
2	3.286	3.859	1.75	16.724
<b>.</b>	4.432	2 260	1 10	14 160
3	3 1/1	5.200	1.40	14.102
Δ	3 246	3 304	1 50	14 318
· · · · · · · · · · · · · · · · · · ·	3 361	0.004	1.50	14.010
5	2 47	2 606	1 18	11 293
	2.741	2.000		11.200
Average Tensile Index for Run	n#2 =	14.04	Nm^2/a	
3 1	2.999	3.066	1.39	15.827
	3.133			
2	2.91	2.513	1.14	12.972
	2.115			
3	2.722	2.509	1.14	12.952
	2.295			
4	2.572	2.534	1.15	13.081
	2.495			
5	2.564	2.519	1.14	13.003
	2.475			
Average Tensile Index for Rur	n#3 =	13.57	Nm^2/g	
4 1	2.652	2.745	1.24	14.612
	2.838			
<b>2</b> • <b>1</b>	2.746	2.448	1.11	13.031
	2.15	0.405	0.00	44.040
3	1.812	2.125	0.96	11.312
	2.438	0.000	4.00	40,000
4	2.000	2.329	1.06	12.398
	2.091	0 400	4 40	40.005
Э	2.409	2.420	1.10	12.923
Average Tensile Index for Pur	2.30/	12 96	NmA2/a	
Average Tensile HILEA IOI RUI	1 <del>17 -</del>	12.00	14111 Z/Y	

Table V:	lensile and	lear Data			
Run #	sheet #	Tensile value	Average	Tensile kgf	Tensile Index(Nm <sup>2</sup> /g)
	5	l 2.835	2.878	1.305	13.790
		2.921			
		2 765	2,856	1 295	14 194
		2 947	2.000	1.200	
		2.047	2 955	1 205	1/ 100
			2.000	1.295	14.109
		2.794			
	4	2.84	2.988	1.355	14.850
		3.136			
	Ę	5 2.413	2.514	1.140	12.494
		2.615			
Average	<b>Tensile Inde</b>	x for Run $#5 =$	13.90	Nm^2/g	
Tear Dat	а			U	
Run #	Tear value	Tear Force mN	Tear Index	(mNm^2/a)	
	1 11		6 577	(//// 2/9)	
,			0.017		
		313.92	5.202		
		3 313.92	5.262		
	. 10	) 392.4	6.577		
	1 <sup>*</sup>	431.64	7.235		
	·	313.92	5.262		
Average	Tear Index f	or Run#1=	6.029	m'Nm^2/g	•
U	2 12	376,704	6.314	J	
	- 12	2 376 704	6.314		
	14	1 439 488	7 367		
	1-		7 902		
	1.		7.033		
	2	439.466	7.307		
	- 1:	<b>4/0.88</b>	7.893		
Average	Tear Index f	or Run#2=	7.191	mNm^2/g	
	3 1'	1 345.312	5.788		
an this - Are	12	2 376.704	6.314		
	12	2 376.704	6.314		
	12	2 376.704	6.314		
	12	2 376 704	6 3 1 4		
6 	1	345 312	5 788		
	· 1·	1 3/5 312	5 7 9 9		
-	11	0 376 70 <i>1</i>	6 214		
A	دا Toor Indox f	2 370.704	0.314		н. Настания (1996)
Average	Tear muex in	$0^{\prime} R u = 0^{\prime} 0^{\prime$	0.117	m Nm^2/g	
	4 12	2 376.704	6.314		
	12	2 376.704	6.314		
	1 <sup>.</sup>	1 345.312	5.788		
	1 <sup>.</sup>	345.312	5.788		
	1:	345.312	5.788		
-	1 <i>1</i>	345,312	5,788		
	1	345 312	5 788		
Averane	Tear Index f	$r R \ln \# A =$	5 020	m'Nm^2/a	
. Wolaye		Γ Γ Γ Γ Γ Γ Γ Γ Γ	0.300		
	J 17		0.940		
1	14	+ 439.488	1.367		
	14	439.488	7.367		
1	13	408.096	6.840		
	13	<b>408.096</b>	6.840		
Ì	1:	408.096	6.840		
Average	Tear Index f	or Run $#5 =$	7 367	mNm^2/a	

## Formula Sheet for Data Calculations:

**Tensile Index:** 

<u>(value x lbs)</u> (653.8 g/kg) T.I.= (2.205 lbs/kg) X Basis Weight g/m^2

Tear Force:

T.F. = <u>(Tear value\* 16 \* 9.81)</u> No. of sheets torn

Tear Index: <u>Tear Force</u> T.L = Basis Weight

**Total Suspended Solids:** 

(Weight of filter and sample) - (Weight of dry sample) \*1000mg/gTSS =Sample Volume (100 mL)

**Total Dissolved Solids:** 

(Pan Weight and Sample) - (Pan Weight after Drying) \* 1000mg/gTDS =Sample Volume (25 mL)

#### **DISCUSSION OF RESULTS:**

The results of the various handsheet and whitewater tests will be discussed here as to how they do or do not correlate with each other. The first graph in the appendix is the graphical interpretation of the whitewater solids content that includes TSS and TDS. These results were graphed by run to see if they start to build up within the system as the water is recirculated. As is seen in the graph suspended material does indeed increase which is as expected due to the recirculation of the whitewater. However, it is also shown that the amount of dissolved material decreases as time goes on. It was thought initially that the trend of dissolved material would follow the same curve as the TSS but as seen this is not the case. There is only one possible explanation for this, it decreases because of the handsheet process itself in which water leaves with the sheet after the headbox is drained and is lost to the system by either pressing or with the drying stage. This explanation does not in fact account for that much of a decrease in TDS since the quantity of water leaving with the sheet is small as compared to the entire whitewater system. However, this is the only explanation available since there are only two possible exits for water to leave the system with the flotation froth and at the headbox with the sheet.

The next graph in the series shows the effect of TSS on strength properties namely tear and tensile index. This graph shows that tear and tensile follow the same type of curve which should not be the case since tensile is effected by the number of bonds

and bonding area and tear is more effected by fiber length. Tensile Index does show a slight increase after the later runs which can be attributed to the amount of fines increasing within the system which lend to better bonding and higher strength. Tear however does not show any increase but it should be suspect to change as suspended material starts to really build up and a higher percentage of fines gets trapped in the sheet which will ultimately lower the tear index.

The third graph is similar to the second except the strength properties are subject of the effect of total dissolved solids. It is seen that the curves are again similar which should not be the case but the trend is easily explained. As seen both tensile and tear both increase slightly as the runs progress and at the later runs they both start to fall off. This can be attributed to the deposit of dissolved material on the fibers themselves creating a layer between the fibers that does not give as good a bond as would a direct fiber to fiber bond. The forth graph depicts how tensile strength changes after each batch and shows the effect of solids at each batch. It shows that in the first batches the solids have more of an effect early and towards the later batches the effects are less due to the fact that the solids build up is not as dramatic later as they are earlier. That initially, there are no solids to speak of and when the first pulp is added to the system the solids fraction is very high. However, when subsequent additions are made the effect is less and less and according to the graph tend to start to equal out as time goes on. To say that the

amount<sup>\*</sup>of solids added nearly equals the amount taken out of the system with the sheet.

Graph number five shows the relationship of TSS on Opacity and Scattering Coefficient. It shows that suspended material does not effect opacity over the five runs. However, it can be foreseen that as the solids really start to build up and the number of fines increase the more dense the sheet will become and the higher the opacity will be. Also, it should be noted the opacity is affected by the basis weight of the sheet, the caliper of the sheet, and the spot where the reading of opacity was taken which in the future may come into play. As for scattering coefficient initially it is not effected but in the later runs there is a definite increase which can be attributed to the build up of fines in the system which causes more surfaces for light scattering thereby increasing the scattering coefficient.

The final graph deals with the effect of TSS on the brightness of the sheet. As seen from the chart brightness was not effected over the five runs. However, it can be inferred that as solids really start to build up within the system brightness will be affected somewhat.

#### CONCLUSIONS:

The use of a totally closed loop deinking system is relatively new in the paper industry and its affects are just now being understood. There are many other concerns that must be dealt with in order to implement a system that addresses these issues. Through researching the data that was just presented it was found that the amount of suspended material within a system like this does indeed build up over time. The amount of dissolved material from the data presented shows a decrease which can only be attributed as a loss through the transport of water with the sheet. This is not a satisfactory explanation for that amount of material to be lost but it is the only one that can be made. Along with the build up of solids there is a definite impact on the strength of the sheet. As seen tensile strength does increase with TSS and can be attributed to fines accumulation within the system. Tear can be inferred to decrease as fines increase within the sheet. As for TDS and strength you have to take a look at the bonds between fibers. It can be concluded that as dissolved material deposits on the sheet and the fibers the bonding is weakened and the sheet is not as strong as it would be if just fiber to fiber bonds existed. It was also seen that the effects of solids is greatest early on and that later the solids effects are less due to the removal of solids with the sheet. Brightness and opacity went relatively unchanged but it can be expected that as solids start to really build up and suspended and dissolved material deposit on the -- sheet there would be an affect. And finally, scattering

coefficient did increase and was directly affected by the increase in suspended material caused by the deposition of fines in the sheet causing more surfaces for light scattering and may cause drainage problems on the paper machine thereby affecting machine speeds.

#### **RECOMMENDATIONS:**

If time did not dictate everything that is done in this world there was allot of things that could have been accomplished to supplement the data that was just presented. One of the thing that could have been done was to conduct more runs which would have generated more data points and given better trends in which to base more sound conclusions. Another area of study would be how changing the surfactant level after each run would affect the solids content and the properties of the sheet. Comparing different furnishes to each other would be very interesting to see how they would react to the same type of conditions. The best area of study would be changing the length of the pulping time this would definitely change the solids content in the loop and there might be an opportunity to see better the effects of solids on the sheet properties.

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APPENDIX:







# Sheet Batches and How Tensile Increases per Batch





