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# Stepwise metabolic adaptation from pure metabolization to balanced anaerobic growth on xylose explored for recombinant *Saccharomyces cerevisiae*

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## Abstract

**Background:** To effectively convert lignocellulosic feedstocks to bio-ethanol anaerobic growth on xylose constitutes an essential trait that *Saccharomyces cerevisiae* strains normally do not adopt through the selective integration of a xylose assimilation route as the rate of ATP-formation is below energy requirements for cell maintenance ( $m_{ATP}$ ). To enable cell growth extensive evolutionary and/or elaborate rational engineering is required. However the number of available strains meeting demands for process integration are limited. In this work evolutionary engineering in just two stages coupled to strain selection under strict anaerobic conditions was carried out with BP10001 as progenitor. BP10001 is an efficient ( $Y_{ethanol} = 0.35$  g/g) but slow ( $q_{ethanol} = 0.05 \pm 0.01$  g/g<sub>BM</sub>/h) xylose-metabolizing recombinant strain of *Saccharomyces cerevisiae* that expresses an optimized yeast-type xylose assimilation pathway.

**Results:** BP10001 was adapted in 5 generations to anaerobic growth on xylose by prolonged incubation for 91 days in sealed flasks. Resultant strain IBB10A02 displayed a specific growth rate  $\mu$  of  $0.025 \pm 0.002$  h<sup>-1</sup> but produced large amounts of glycerol and xylitol. In addition growth was strongly impaired at pH below 6.0 and in the presence of weak acids. Using sequential batch selection and IBB10A02 as basis, IBB10B05 was evolved (56 generations). IBB10B05 was capable of fast ( $\mu = 0.056 \pm 0.003$  h<sup>-1</sup>;  $q_{ethanol} = 0.28 \pm 0.04$  g/g<sub>BM</sub>/h), efficient ( $Y_{ethanol} = 0.35 \pm 0.02$  g/g), robust and balanced fermentation of xylose. Importantly, IBB10A02 and IBB10B05 displayed a stable phenotype. Unlike BP10001 both strains displayed an unprecedented biphasic formation of glycerol and xylitol along the fermentation time. Transition from a glycerol- to a xylitol-dominated growth phase, probably controlled by CO<sub>2</sub>/HCO<sub>3</sub><sup>-</sup>, was accompanied by a 2.3-fold increase of  $m_{ATP}$  while  $Y_{ATP}$  ( $= 87 \pm 7$  mmol<sub>ATP</sub>/g<sub>BM</sub>) remained unaffected. As long as glycerol constituted the main by-product energetics of anaerobic growth on xylose and glucose were almost identical.

**Conclusions:** In just 61 generation IBB10B05, displaying ~530% improved strain fitness, was evolved from BP10001. Its excellent xylose fermentation properties under industrial relevant conditions were proven and rendered it competitive. Based on detailed analysis of growth energetics we showed that  $m_{ATP}$  was predominantly determined by the type of polyol formed rather than, as previously assumed, substrate-specific.

**Keywords:** Xylose fermentation, *Saccharomyces cerevisiae*, Bio-ethanol, Evolutionary engineering, Anaerobic growth, Energy demands

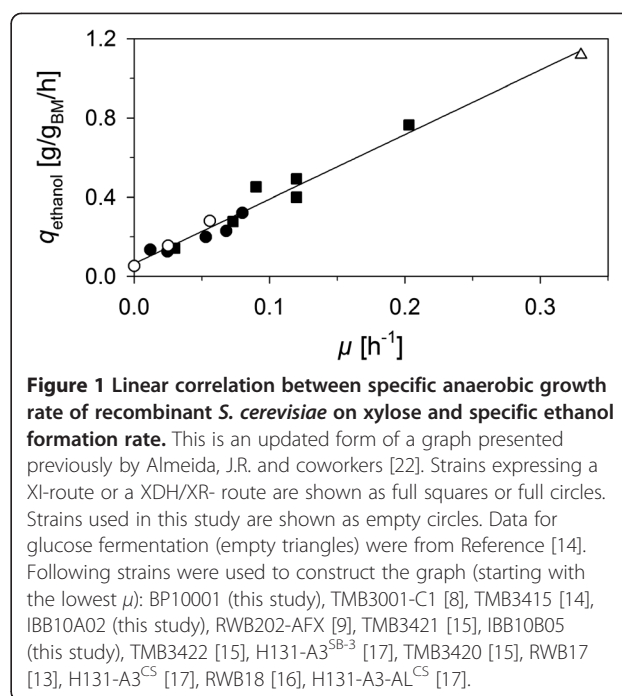
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## Background

With a 82% share ethanol constitutes the most frequently used bio-fuel world-wide [1]. Current industrial processes, producing more than 86 billion liters of bio-ethanol annually, rely almost exclusively on fermentation of the sugar portions of food crops [1]. However competition with the food sector, limited farmland and insufficient greenhouse gas emission-balances demand for other more sustainable feedstock solutions. Lignocellulosic biomass represents a promising alternative with high potential in this respect as long as the complete sugar fraction predominantly made of glucose and xylose is converted into ethanol at sufficiently high rates and titers. Due to its high ethanol fermentation efficiency and enormous process robustness *Saccharomyces cerevisiae* is largely used in today's bio-ethanol plants. However *S. cerevisiae* cannot ferment xylose without incorporating a heterologous xylose assimilation pathway in the first place. In the last two decades huge efforts have thus been made to engineer recombinant *S. cerevisiae* strains capable of efficient utilization of xylose [2-7].

To enable xylose assimilation in *S. cerevisiae* basically two routes have been addressed by genetic engineering in the past. Both pathways concentrate on the isomerization of xylose to xylulose which after phosphorylation to xylulose 5-P, catalyzed by xylulose kinase (XK), is metabolized to ethanol by reactions of the pentose phosphate (PP-) pathway and glycolysis. Isomerization of xylose may proceed in one reaction catalyzed by xylose isomerase (XI) or in two steps via xylitol catalyzed by the consecutive action of a NADPH-preferring xylose reductase (XR) and a NAD<sup>+</sup>-specific xylitol dehydrogenase (XDH) (Additional file 1: Figure S1).

Irrespective of the route applied specific rates of ethanol formation on xylose ( $q_{\text{ethanol}} \leq 0.05 \text{ g/g}_{\text{BM}}/\text{h}$ , where BM refers to dry cell weight) of resultant recombinant *S. cerevisiae* strains fell far below  $q_{\text{ethanol}}$  of glucose fermentation ( $\sim 1.2 \text{ g/g}_{\text{BM}}/\text{h}$ ) without further genetic modification. Evolutionary engineering [8-12] as well as rational metabolic engineering [13-15] alone or in combination [15-20] have been applied successfully to further improve  $q_{\text{ethanol}}$  in laboratory [8-10,13-19] and industrial strains [11,12,20]. Faster ethanol production was accompanied with the ability of these strains to grow on xylose under anaerobic conditions. Similar to anaerobic growth of *S. cerevisiae* on glucose [21],  $q_{\text{ethanol}}$  becomes proportional to the specific growth rate  $\mu$  on xylose [14,22] (see Figure 1) provided that ATP needs for cell maintenance ( $m_{\text{ATP}}$ ) have been met. The onset ATP formation rate ( $r_{\text{ATP}}$ ) enabling anaerobic growth on xylose by recombinant *S. cerevisiae* strains was estimated to be 1.8 – 2.0  $\text{mmol}_{\text{ATP}}/\text{g}_{\text{BM}}/\text{h}$  [23,24]. A value which would be far above maintenance requirements reported for anaerobic growth on glucose by *S. cerevisiae* (0.8 – 1.0  $\text{mmol}_{\text{ATP}}/\text{g}_{\text{BM}}/\text{h}$  [21,25]) or oxygen-



**Figure 1** Linear correlation between specific anaerobic growth rate of recombinant *S. cerevisiae* on xylose and specific ethanol formation rate. This is an updated form of a graph presented previously by Almeida, J.R. and coworkers [22]. Strains expressing a XI-route or a XDH/XR- route are shown as full squares or full circles. Strains used in this study are shown as empty circles. Data for glucose fermentation (empty triangles) were from Reference [14]. Following strains were used to construct the graph (starting with the lowest  $\mu$ ): BP10001 (this study), TMB3001-C1 [8], TMB3415 [14], IBB10A02 (this study), RWB202-AFX [9], TMB3421 [15], IBB10B05 (this study), TMB3422 [15], H131-A3<sup>5B-3</sup> [17], TMB3420 [15], RWB17 [13], H131-A3<sup>CS</sup> [17], RWB18 [16], H131-A3-AL<sup>CS</sup> [17].

limited growth on xylose by *Scheffersomyces stipitis* ( $\sim 1 \text{ mmol}_{\text{ATP}}/\text{g}_{\text{BM}}/\text{h}$  [26]). Reasons for this large difference in  $m_{\text{ATP}}$  however are not known. The energy demand for growth, reflected by the slope in Figure 1, instead may be similar for both substrates.

The degree of improvement of  $q_{\text{ethanol}}$  in an evolutionary engineering study highly depends on the physiology of the progenitor strain used, the number of stages and generation times of the adaption process as well as the proper arrangement of enzyme activity levels potentially limiting metabolic flux. In the past years recombinant strains of *S. cerevisiae* expressing in addition to XR/XDH or XI all PP- pathway enzymes and in most cases containing a *GRE3* (encoding an unspecific NADPH-dependent aldo-keto reductase) knockout have been established within the scientific community as suitable genetic backgrounds that sufficiently facilitate high metabolic flux. Homologous expression of variants of XR from *S. stipitis* preferring NADH over NADPH together with XDH/XK or heterologous overexpression of XI together with XK in this “high flux” genetic background enabled anaerobic growth on xylose and improved ethanol productivity up to 0.32  $\text{g/g}_{\text{BM}}/\text{h}$  (XR/XDH-route [15]) and 0.45  $\text{g/g}_{\text{BM}}/\text{h}$  (XI-route [13]) even without subsequent evolutionary adaption. In combination with extensive evolutionary adaption as impressively demonstrated by Zhou H. and coworkers recombinant *S. cerevisiae* strains that fermented xylose almost as good as glucose to ethanol can be developed (see Figure 1) [17]. Although in the last years a clear trend towards XI-based strains was observable the XR/XDH-

based route may have clear advantages with respect to  $q_{xylose}$ ,  $q_{ethanol}$  and final ethanol titer [27].

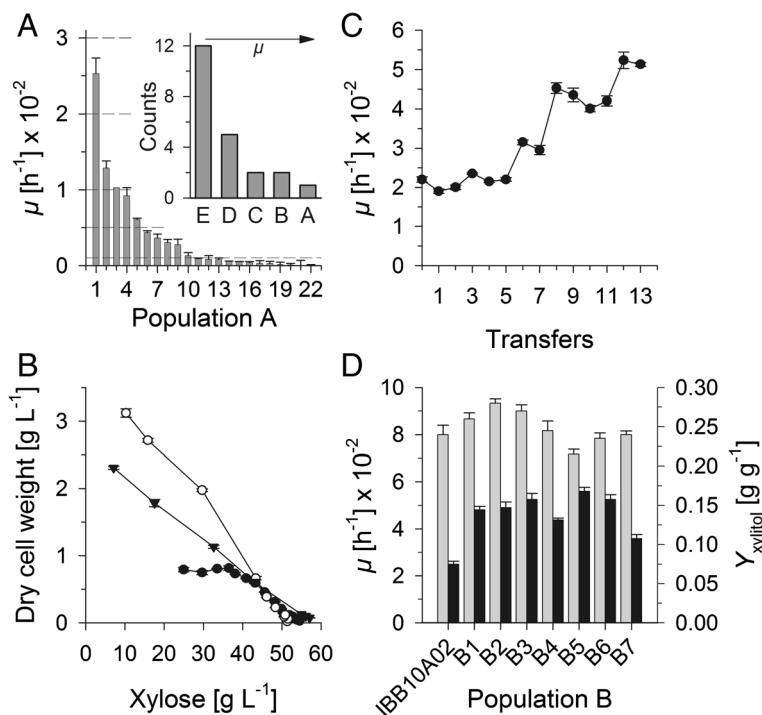
Very recently we reported on a recombinant *S. cerevisiae* strain which we have termed IBB10B05 that displayed excellent fermentation properties in spent sulfite liquor [28]. In the present work we would like to present the underlying history of strain development which was based on a very time efficient two-stage evolutionary engineering protocol. The best strains of each stage, IBB10A02 and IBB10B05, were isolated and their physiology comprehensively studied under defined medium and aeration conditions. The xylose-metabolizing strain BP10001, a recombinant of *S. cerevisiae* that homogeneously expresses an optimized yeast-type xylose assimilation pathway composed of a NADH-preferring variant of *Candida tenuis* XR [29], a NAD<sup>+</sup>-specific XDH from *Galactocandida mastotermitis* [30] and an additional copy of endogenous XK served as genetic basis for evolutionary engineering. Construction of BP10001 [31] and comprehensive analysis with respect to physiology [31,32] and at the level of intracellular metabolites [33] have been reported elsewhere. As a result of balanced coenzyme usage of XR and XDH [33,34] BP10001 displayed efficient xylose-to-ethanol conversion capability

in terms of ethanol yield (0.34 g/g). Nevertheless  $q_{ethanol}$  (0.05 g/g<sub>BM</sub>/h) was too slow to be competitive.

## Results

### Evolutionary engineering

To enable anaerobic growth on xylose by BP10001 cells were incubated under anoxic conditions in defined medium containing only xylose as a carbon source for 91 days. In this time span the optical density (OD<sub>600</sub>) increased by a factor of 40 from OD<sub>600</sub> = 0.12 to OD<sub>600</sub> = 4.8, corresponding to 5.3 generations. As aerobic and anaerobic growth on xylose does not necessarily correlate [9] strain selection and screening were carried out under strict anaerobic conditions. A population of twenty two positive clones (population A) was obtained and further tested with respect to  $\mu$ . The strain with the highest  $\mu$  (0.025 h<sup>-1</sup>) was termed IBB10A02 and used for further characterization and as genetic basis in the second evolution stage. Population A which was quite heterogeneous with respect to  $\mu$  (< 0.005 h<sup>-1</sup> – 0.025 h<sup>-1</sup>) clustered into 5 distinct classes (see Figure 2A). The resulting strongly right-skewed distribution (inset of Figure 2A) may be therefore a direct reflection of a stepwise adaption process from BP10001-close phenotypes at the early phase of



**Figure 2** Strain development by evolutionary engineering in two stages. **Panel A:** Strains representing population A are sorted according to their  $\mu$ . Upper bounds of classes are shown as dashed lines. Inset shows the corresponding histogram. Increase of  $\mu$  along the classes is indicated by an arrow. **Panel B:** Growth characteristics of IBB10A02 (full circles) and IBB10B05 (empty circles) under uncontrolled and IBB10A02 under controlled (full triangles) pH conditions. **Panel C:** Evolution of population B from IBB10A02 by sequential batch selection. **Panel D:**  $\mu$ s (black bars) and  $Y_{xylitol}$ s (grey bars) are indicated. Error bars indicate standard deviations obtained from two individual cultivations (**Panels: A, C, D**) or from triplicate measurements of OD<sub>600</sub> (**Panel B**).

evolution to the IBB10A02 phenotype developed at a later time of experiment. Figure 2B shows a representative growth characteristic of IBB10A02 on xylose cultivated in sealed flasks. Typically cells stopped growing and started to metabolize xylose at a cell concentration of  $\sim 0.8$  g<sub>BM</sub>/L although  $\sim 75\%$  of xylose was still present in the medium. We observed that the pH decreased by more than 0.6 pH units in the growth phase suggesting that growth of IBB10A02 on xylose may be sensitive to pH values below 6.5. Consistent with these findings IBB10A02 was capable of growing along the entire fermentation under controlled pH (= 6.5) conditions carried out in a stirred bioreactor (see Figure 2B).

Batch-wise cultivation of IBB10A02 and serial transfer of exponentially growing cells to a new batch was carried out for sorting out faster growing populations. The enrichment process over time (transfers) is shown in Figure 2C. After 13 transfers and further 56 generations another population B was obtained with an average  $\mu$  of  $0.051$  h<sup>-1</sup>. Seven (B1-B7) strains were selected and their strain fitness tested with respect to  $\mu$  and  $Y_{xy\text{litol}}$ . Results are shown in Figure 2D. Strain B5, later designated as IBB10B05, displayed the fastest growth on xylose ( $\mu = 0.056$  h<sup>-1</sup>) and lowest  $Y_{xy\text{litol}}$  (0.21 g/g). The  $\mu$  of IBB10B05 was 1.8-fold higher than that of IBB10A02 (see Table 1). Furthermore IBB10B05 was capable of growth-associated utilization of xylose throughout the entire fermentation. Compared to IBB10A02 it produced about 4 times more biomass under uncontrolled pH conditions (see Figure 2B).

The pH shifted by more than 1.4 pH units in this time span indicating that IBB10B05 is more robust to pH changes than IBB10A02.

To test whether obtained phenotypes were stable, both strains were individually cultivated under conditions where growth of cells did not rely on adapted traits. To this end cells were incubated for 44 generations under aerobic conditions in complex glucose-containing medium. Five colonies of each strain were thereafter isolated and tested for their capability to ferment glucose and xylose under anaerobic conditions. Compared to corresponding  $\mu$ s of cells not subjected to phenotype challenging conditions  $\mu$ s obtained for each colony were not significantly affected and values for growth on glucose and xylose were identical within relative standard deviations of 3.5% (both strains) and 6.5% (both strains), respectively suggesting that phenotypes displayed by IBB10A02 and IBB10B05 are stable.

#### Physiological and energetic characterization of evolved strains

Growth characteristics and product pattern of anaerobic xylose fermentation were studied in sealed flasks for IBB10A02 and IBB10B05 as well as for the reference strain BP10001. Representative time courses of xylose utilization and product formation are displayed in Figure 3. Resultant  $\mu$ s,  $q_{xy\text{lose}}$ s as well as  $Y_{\text{product}}$ s verified by respective carbon balances are summarized in Table 1. Furthermore  $\mu$ s were determined for both evolved strains on glucose under anaerobic conditions and on xylose under aerobic

**Table 1 Physiological parameters obtained from xylose fermentation performed under anaerobic conditions in sealed flasks at pH 6.5 together with aerobic and anaerobic specific growth rates on xylose and glucose, respectively<sup>a</sup>**

Parameter <sup>b</sup>	BP10001	IBB10A02		IBB10B05	
		Phase 1	Phase 2	Phase 1	Phase 2
$\mu_{xy\text{lose}}^{\text{AN}}$	n.d. <sup>c</sup>		$0.025 \pm 0.002$		$0.056 \pm 0.003$
$\mu_{xy\text{lose}}^{\text{AE}}$	n.m. <sup>c</sup>		$0.12 \pm 0.01$		$0.16 \pm 0.01$
$\mu_{\text{glucose}}^{\text{AN}}$	$0.34^{\text{d}}$		$0.27 \pm 0.02$		$0.26 \pm 0.01$
$q_{xy\text{lose}}$	$0.15 \pm 0.04$		$0.50 \pm 0.03$		$0.80 \pm 0.04$
$r_{\text{ATP}}$	$1.1 \pm 0.1$	$2.9 \pm 0.2$	$3.7 \pm 0.2$	$5.7 \pm 0.4$	$6.3 \pm 0.2$
$Y_{\text{biomass}}$	n.d. <sup>c</sup>		$0.05 \pm 0.01$		$0.07 \pm 0.01$
$Y_{\text{ethanol}}$	$0.35 \pm 0.02$		$0.31 \pm 0.02$		$0.35 \pm 0.02$
$Y_{xy\text{litol}}$	$0.19 \pm 0.02$	$0.03 \pm 0.005$	$0.24 \pm 0.01$	$0.03 \pm 0.01$	$0.20 \pm 0.01$
$Y_{\text{glycerol}}$	$0.06 \pm 0.01$	$0.19 \pm 0.02$	$0.015 \pm 0.002$	$0.11 \pm 0.02$	$0.018 \pm 0.001$
$Y_{\text{acetate}}$	$0.021 \pm 0.001$	$0.07 \pm 0.02$	$0.050 \pm 0.002$	$0.04 \pm 0.01$	$0.03 \pm 0.01$
$Y_{\text{ribitol}}$	n.d. <sup>c</sup>	n.d. <sup>c</sup>	$0.012 \pm 0.003$	n.d. <sup>c</sup>	$0.011 \pm 0.002$
$Y_{\text{CO}_2}^{\text{e}}$	0.35	0.35	0.33	0.37	0.36
C-Balance	0.97	1.00	1.01	0.97	1.04

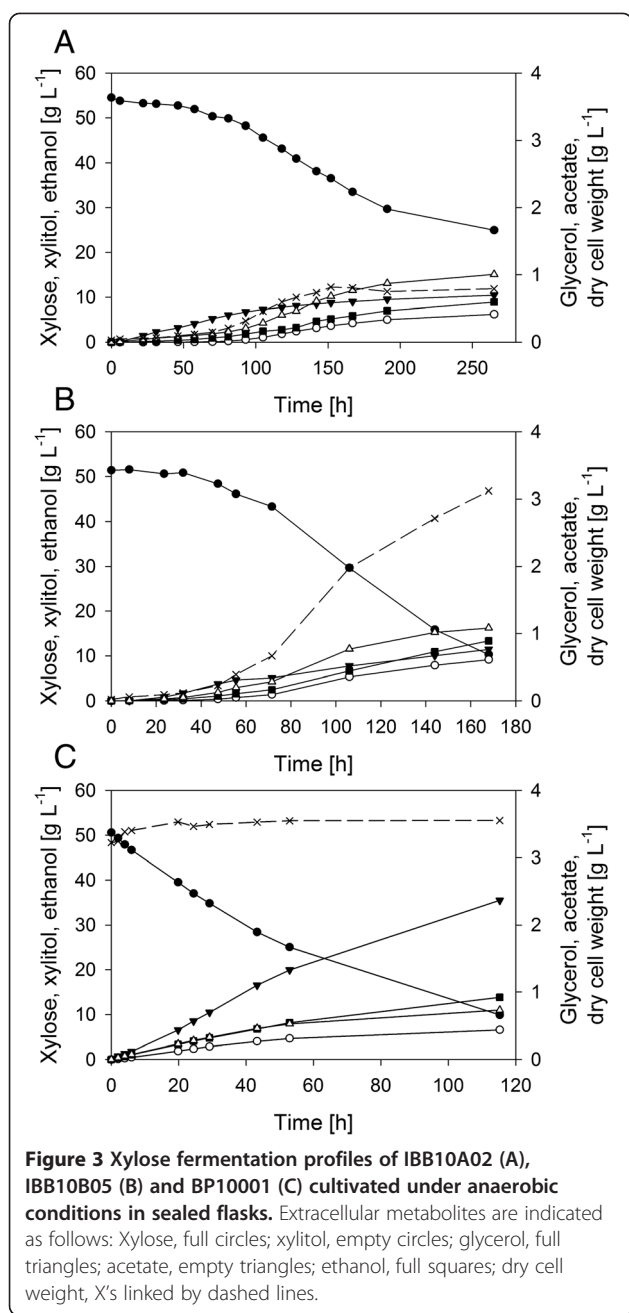
<sup>a</sup>Concentrations of 50 g/L and 20 g/L were used for xylose and glucose, respectively; Superscripts <sup>AN</sup> and <sup>AE</sup> indicate anaerobic and aerobic cultivation conditions, respectively.

<sup>b</sup> $\mu$ ,  $q_{xy\text{lose}}$ ,  $r_{\text{ATP}}$  and  $Y_{\text{product}}$  are presented as h<sup>-1</sup>, g<sub>xylose</sub>/g<sub>BM</sub>/h, mmol<sub>ATP</sub>/g<sub>BM</sub>/h and g<sub>product</sub>/g<sub>xylose</sub>, respectively.

<sup>c</sup>n.d., not detectable; n.m., not measured.

<sup>d</sup>Data was from Ref. [33].

<sup>e</sup> $Y_{\text{CO}_2}$  was calculated based on stoichiometry of metabolic ethanol and acetate formation.



conditions (see Table 1). Physiological parameters obtained for BP10001 were in excellent agreement with data reported previously for anaerobic conversion of 50 g/L xylose carried out in a stirred bioreactor at pH 5.0 [32]. IBB10A02 and IBB10B05 displayed a 3.3- and 5.3-times, respectively faster rate of xylose conversion than the reference strain. Compared to IBB10A02 IBB10B05 showed 1.3-fold faster growth on xylose under aerobic conditions while anaerobic  $\mu$ s on glucose were almost identical for both strains and only 20% lower as compared to the corresponding  $\mu$  of BP10001 [33]. Obtained  $q_{\text{ethanol}}/\mu$  pairs from xylose fermentations for both evolved strains

integrated well into the relationship shown in Figure 1. Ethanol yields were high (0.35 g/g) and similar for IBB10B05 and the reference strain and only slightly lower in case of IBB10A02. Compared to their progenitor IBB10A02 and IBB10B05 produced more acetate.

Unlike BP10001 both evolved strains displayed a peculiar biphasic formation characteristic for glycerol and xylitol as is portrayed in Figure 4(A, B) while  $Y_{\text{ethanol}}$  (Figure 4C),  $Y_{\text{biomass}}$  and  $Y_{\text{acetate}}$  were rather constant over time. In the first phase (#1) of xylose fermentation glycerol constituted the predominant by-product and only little xylitol was formed while in the second phase (#2) of fermentation the pattern switched and xylitol accumulated instead. We recognized that xylitol formation started at glycerol concentrations of 0.3 – 0.6 g/L. However, the biphasic character did not change when cultivations were performed in the presence of 0.6 g/L glycerol (data not shown). Transition from glycerol to xylitol formation was accompanied by additional release of small amounts of ribitol (~1%) a by-product not recognized in xylose-to-ethanol conversions by BP10001. Basically ribitol can be formed by *S. cerevisiae* from ribulose-5P and ribose-5P after dephosphorylation and further reduction of the resulting pentose sugars ribulose (by XDH with NADH) and ribose (by XR with NAD(P)H), respectively [35]. Because ribose constitutes a worse substrate for XR than xylose [36] and XDH can reduce ribulose with a catalytic efficiency that is 15-times faster than that for oxidizing xylitol [30,37] we may assume that predominantly XDH contributed to the formation of ribitol in both evolved strains.

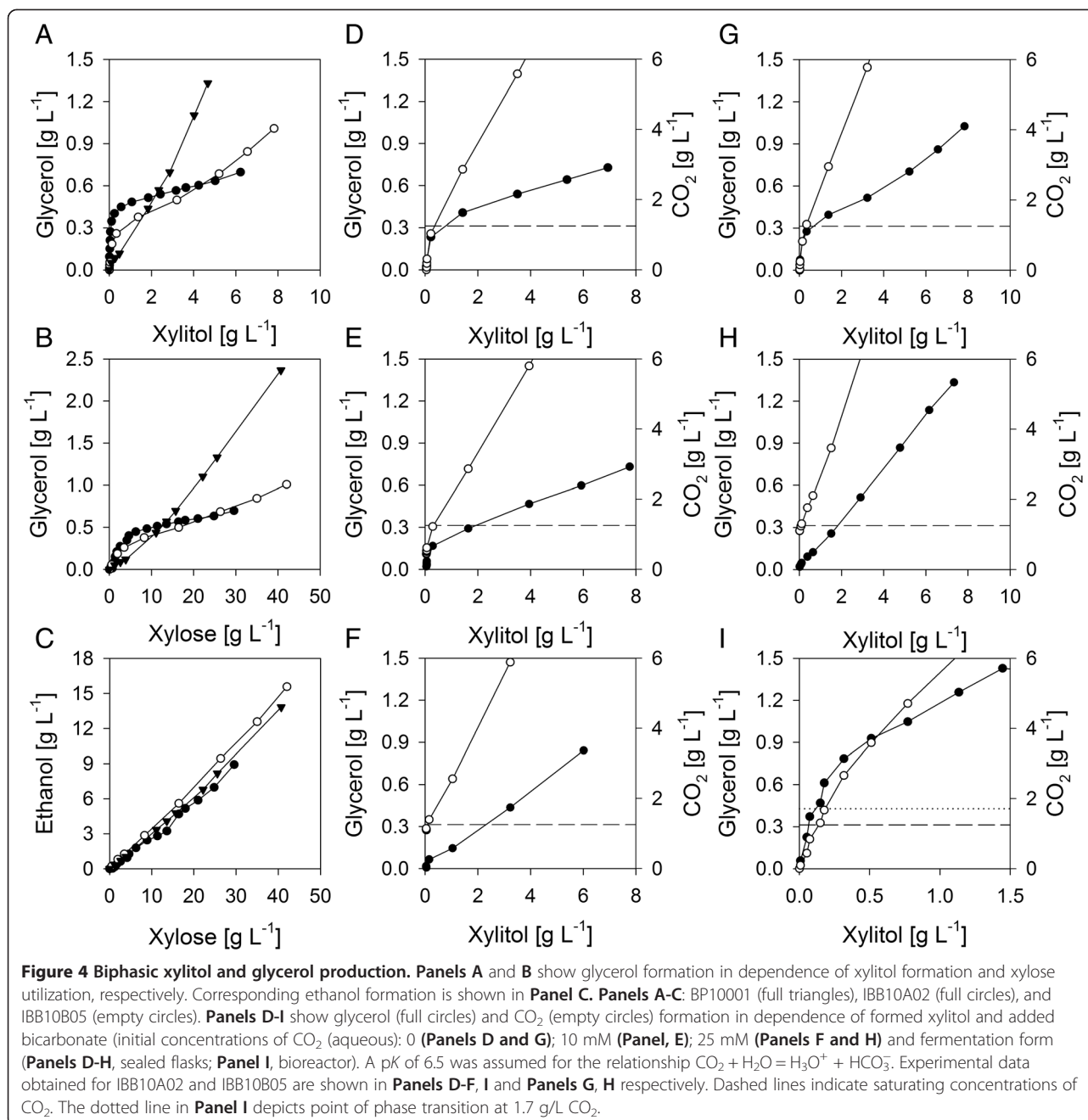
ATP formation rates were calculated in accordance to Equation 1 for each strain and fermentation phase (for details see Additional file 2).

$$r_{\text{ATP}} = q_{\text{ethanol}} + q_{\text{acetate}} - q_{\text{glycerol}} \quad (1)$$

Resultant values are shown in Table 1. Compared to BP10001  $r_{\text{ATP}}$ s for IBB10A02 and IBB10B05 were higher by a factor of 2.6 (#1)/3.4 (#2) and 5.2 (#1)/5.7 (#2), respectively. Energetic parameters  $m_{\text{ATP}}$  and  $Y_{\text{ATP}}$  were estimated by applying Equation 2 to  $\mu$ s and  $r_{\text{ATP}}$ s obtained for IBB10A02 and IBB10B05.

$$r_{\text{ATP}} = Y_{\text{ATP}} * \mu + m_{\text{ATP}} \quad (2)$$

Cells growing in the glycerol-dominated phase displayed a  $m_{\text{ATP}}$  of  $0.7 \pm 0.3$  mmol<sub>ATP</sub>/g<sub>BM</sub>/h that was more than 2-fold lower than that for cells in the xylitol-dominated phase ( $= 1.6 \pm 0.2$  mmol<sub>ATP</sub>/g<sub>BM</sub>/h). Values obtained for  $Y_{\text{ATP}}$ s were  $88 \pm 8$  mmol<sub>ATP</sub>/g<sub>BM</sub> (#1) and  $85 \pm 6$  mmol<sub>ATP</sub>/g<sub>BM</sub> (#2) and therefore not prone to the polyol produced.

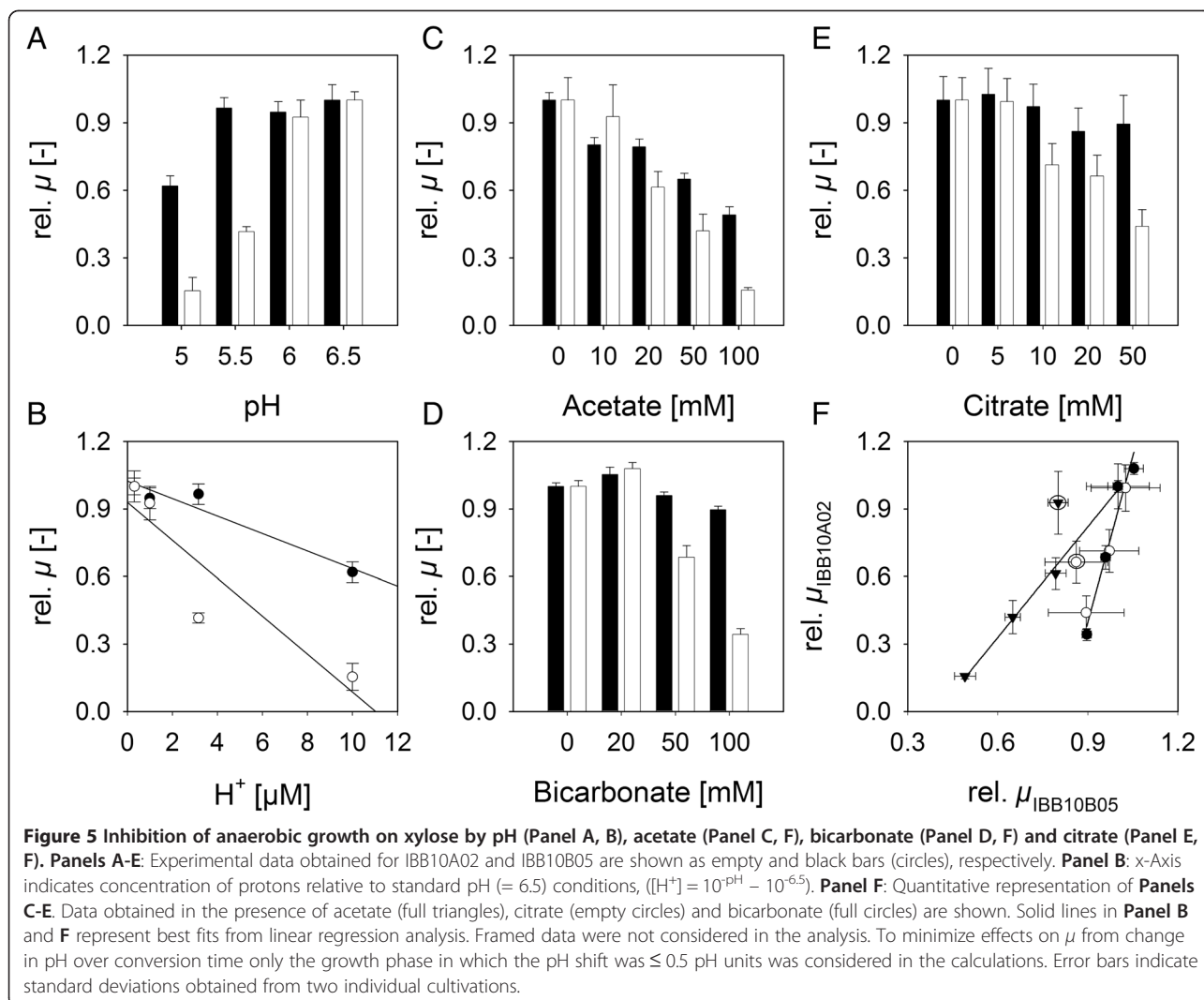


#### Sensitivity to pH and weak acids was dependent on the evolution stage

Evolved strains were further characterized with respect to their ability to grow at different pH values in the range of 5.0 to 6.5. Results are shown in Figure 5A. Anaerobic growth of IBB10A02 on xylose was strongly inhibited at pH values below 6.0. In contrast growth of IBB10B05 was not affected in a pH range of 5.5 – 6.5 and only weakly inhibited by ~40% at pH 5.0. Plotting concentrations of added protons versus respective relative  $\mu$ s (see Figure 5B) showed that the inhibitory effect

of protons for IBB10BA02 was ~2-times stronger than that for IBB10B05.

Weak acids constitute a significant fraction in all lignocellulosic-based hydrolysates that exerts pronounced inhibitory effects on conversion capability and growth ability of applied *S. cerevisiae* strains [22]. Three conjugate bases, acetate, citrate and bicarbonate were offered individually at different concentrations and their effects on anaerobic growth on xylose were determined for both evolved strains. Results are shown in Figure 5(C-F). Unlike  $\mu$  of IBB10B05 which was clearly affected only by



acetate within the concentration ranges tested, growth of IBB10A02 was strongly deteriorated by either acid applied. The inhibitory effect by acetate was 1.6-fold higher while those by citrate and bicarbonate were similar and ~5-fold stronger for IBB10A02 (Figure 5F).

Interestingly while addition of protons, acetate and citrate did not affect the biphasic by-product formation behavior (data not shown) increasing the amount of initial bicarbonate from 0 to 50 mM resulted in complete abolishing of the glycerol-dominated phase. Respective xylitol vs. glycerol formation plots obtained for IBB10A02 and IBB10B05 are shown in Figure 4(D-F) and (G, H), respectively. Strikingly the transition from glycerol to xylitol formation went along with  $CO_2$  reaching saturating concentrations (1.26 g/L [38]) in the aqueous phase. The phase transition was weaker and happened delayed with respect to  $CO_2$  formed when IBB10A02 was cultivated in a stirred bioreactor where the fermentation vessel

was permanently purged by  $N_2$  and  $CO_2$  was steadily stripped off (Figure 4I).

#### Enzyme activities

Specific enzyme activities of XR, XDH and XK were measured from cell-free extracts of BP10001, IBB10A02 and IBB10B05. Resultant values are presented in Table 2. Specific activities determined for BP10001 were in good agreement with values reported recently [39]. Enzyme activity levels were similar for both evolved strains. As a consequence of the adaption to growth on xylose activity levels of all xylose pathway enzymes were higher in evolved strains with XR levels displaying the largest increase by a factor of 12–15.

#### Discussion

In this work we have used evolutionary engineering principles to enable anaerobic growth on xylose and improve

**Table 2 Specific enzyme activities in cell-free extracts measured at 25°C<sup>a</sup>**

Strain	XR <sup>b</sup>	XDH <sup>c</sup>	XK <sup>d</sup>
BP10001	0.08 ± 0.01	0.6 ± 0.1	1.1 ± 0.2
IBB10A02	1.0 ± 0.2	1.2 ± 0.2	1.8 ± 0.3
IBB10B05	1.2 ± 0.1	0.9 ± 0.1	1.9 ± 0.2

<sup>a</sup>Specific enzyme activities are presented as  $\mu\text{mol}/\text{min}/\text{mg}_{\text{protein}}$ .

<sup>b</sup>Xylose, 600 mM; NADH, 0.2 mM; 100 mM potassium phosphate buffer, pH 7.0.

<sup>c</sup>Xylitol, 150 mM; NAD<sup>+</sup>, 2 mM; 100 mM Tris/HCl buffer, pH 9.0.

<sup>d</sup>Xylulose, 4.3 mM; NADH, 0.2 mM; ATP, 5 mM; phosphoenolpyruvate, 1 mM; bovine serum albumine, 0.88 g/L; MgCl<sub>2</sub> 6H<sub>2</sub>O, 8.8 mM; KCl, 44 mM; 44 mM HEPES buffer, pH 7.0.

ethanol productivity of BP10001, a recombinant *S. cerevisiae* strain expressing an optimized XR/XDH-route that can efficiently but slowly metabolize xylose to ethanol [31,32]. Only after 2 stages, 61 generations and 140 days and without additional rational metabolic engineering a single strain, IBB10B05, was obtained that compared to its progenitor converted xylose to ethanol at the same high yield (= 0.35 g/g) but more than 5-times faster while its ability to grow on glucose was hardly altered by the evolution process. Its xylose fermentation capability was maintained even after prolonged cultivation in complex glucose medium for more than 40 generations. Based on  $q_{\text{ethanol}}$  (= 0.28 g/g<sub>BM</sub>/h) IBB10B05 can be ranked among the top xylose converting recombinant *S. cerevisiae* strains that assimilate xylose via the XR/XDH route (see Figure 1). In this context, it is noteworthy to mention that strains displaying comparable phenotypes on xylose contained a large history of additional rational and adaptive modifications [15,17] (see Figure 1).

Evolutionary engineering presented in this work was carried out in two stages. Coherent with evolution theory [40,41] the rate of fitness gain decelerated with the number of generations (evolution stages) from 63% fitness gain per generation in the first stage to 3–4% fitness gain per generation in the second stage. The efficiency of fitness increase with which IBB10B05 evolved from BP10001 clearly surpassed the number of generations (100 – 500) typically experienced to achieve an average fitness gain of up to 50–100% [40]. Reasons for this effective adaption process may originate from (i) the relatively high  $q_{\text{ethanol}}$  as well as the low  $Y_{\text{xylitol}}$  of the ancestor BP10001, (ii) skipping aerobic and semi-aerobic evolution stages that although largely employed in this context bear the risk of selecting predominantly aerobic instead of anaerobic growing strains [9] and (iii) the selection procedure which as carried out under strict anaerobic conditions ensured selection of only those strains truly capable of anaerobic growth on xylose.

In compliance with flux control theory [42] increase of  $q_{\text{xylose}}$  was accompanied by an enhancement of all enzyme activity levels constituting the xylose pathway, an

effect also observed by others [24]. The extent of activity level upregulation depended on the intrinsic flux capacity of pathway enzymes in the progenitor strain relative to that required to enable the new phenotype. Compared to the 3.3-fold increase of  $q_{\text{xylose}}$  achieved through the first evolution stage XR activity levels were increased disproportionately high (~12-fold) while those of XDH and XK were disproportionately low (~2-fold). Results therefore indicated and were in good agreement with findings from another study [33] that in particular XR activities exerted to a substantial extent flux control on  $q_{\text{xylose}}$  in BP10001. Further increase of  $q_{\text{xylose}}$  by a factor of 1.6 achieved through the second stage of adaption did not significantly affect activity levels of XR/XDH/XK indicating that other genetic modifications in the metabolism contributed to the improved phenotype of IBB10B05.

In this study we observed that predominantly the pH and the cultivation form – sealed flasks – used in the evolutionary engineering experiments contributed to a significant portion to the shaping of obtained phenotypes. Anaerobic growth on xylose evolved in the first stage was strongly inhibited by protons and weak acids which made it impossible to cultivate IBB10A02 entirely growth-associated under uncontrolled pH conditions. Xylose was, reflected by large biomass-based polyol yields ( $Y_{(\text{glycerol} + \text{xylitol})}$ ) of 35 – 42 mmol/g<sub>BM</sub>, sensed by IBB10A02 as a stress compound. Observed polyol yields exceeded by far the amount of polyol typically produced by *S. cerevisiae* in the form of glycerol on glucose under anaerobic conditions (~10 mmol/g<sub>BM</sub> [43]) to reoxidize NADH from biomass synthesis [44]. Further improvement of  $q_{\text{ethanol}}$  by selection in repetitive batches not only led to faster anaerobic and aerobic growth on xylose but also enhanced acceptance of xylose as a competent fermentable substrate ( $Y_{(\text{glycerol} + \text{xylitol})} = 20 - 22 \text{ mmol/g}_{\text{BM}}$ ) as well as significantly improved resistance to pH and weak acids. In the presence of industrial relevant acetate concentrations IBB10B05 could grow at a rate ~50% of  $\mu$  obtained under optimal conditions. Its process robustness under industrial relevant substrate conditions has been demonstrated recently [28].

Results from physiological and energetic studies provided interesting novel insights into the redox and energy metabolism of anaerobic alcohol fermentation from xylose by recombinant *S. cerevisiae*. In the first phase of xylose fermentation dominated by glycerol formation anaerobic growth on xylose was not much different from that on glucose. Energy requirements for growth ( $Y_{\text{ATP}} = 88 \pm 8 \text{ mmol}_{\text{ATP}}/\text{g}_{\text{BM}}$ ) and maintenance ( $m_{\text{ATP}} = 0.7 \pm 0.3 \text{ mmol}_{\text{ATP}}/\text{g}_{\text{BM}}/\text{h}$ ) on xylose were in the same range as those typically observed for *S. cerevisiae* grown on glucose under anaerobic conditions ( $Y_{\text{ATP}} = 71 - 91 \text{ mmol}_{\text{ATP}}/\text{g}_{\text{BM}}$ ;  $m_{\text{ATP}} = 0.8 - 1.0 \text{ mmol}_{\text{ATP}}/\text{g}_{\text{BM}}/\text{h}$  [21,25]). Remarkably almost no xylitol was formed in this fermentation



phase and glycerol represented a major redox sink for regeneration of surplus NADH formed by biosynthetic processes and through acetate formation. Consequently we can assume that coenzyme recycling between XR and XDH is well balanced in both evolved strains.

Redirection of metabolic flux from glycerol to xylitol coincided with CO<sub>2</sub> approaching saturating concentrations in the aqueous phase suggesting that the amount of CO<sub>2</sub> or HCO<sub>3</sub><sup>-</sup> in the medium contributed to control of phase transition. A similar inverse relationship between CO<sub>2</sub> concentrations and glycerol production, although strongly alleviated, has been reported for a wild-type strain of *S. cerevisiae* [45]. Inactivation of glycerol production however did not lead as one would have expected to an enhanced but slower ethanol production [46]. Carbon flux instead was almost quantitatively redirected towards xylitol without altering  $q_{\text{ethanol}}$ ,  $\mu$  and  $Y_{\text{biomass}}$ . Transition to xylitol production affected growth energetics and NADH recycling. Surplus NADH generated by biomass and acetate is now regenerated by XR. Consequently xylitol is released because coenzyme recycling between XR and XDH is no longer balanced. Energetic analysis provided evidence that energy demands of anaerobic growth on xylose for maintenance but not for growth were largely determined by the polyol, glycerol or xylitol, formed to maintain NADH balance and support osmolarity. The large  $m_{\text{ATP}}$  of  $1.6 \pm 0.3$  mmol<sub>ATP</sub>/g<sub>BM</sub>/h obtained in this study for cells grown in the xylitol-dominated phase was in reasonable agreement with  $m_{\text{ATP}}$ s of 1.8 – 2.0 mmol<sub>ATP</sub>/g<sub>BM</sub>/h suggested previously for anaerobic growth on xylose [23,24].

Interestingly based on the amount of acetate formed per biomass produced (IBB10A02: 17 – 24 mmol/g<sub>BM</sub>; IBB10B05: 7 – 17 mmol/g<sub>BM</sub>) NADPH required for biomass synthesis (6.5 mmol/g<sub>BM</sub> [43]) could be in principle solely supplied by acetaldehyde dehydrogenase suggesting that the oPP-pathway may play a minor role in NADPH regeneration in evolved strains. Consistent with this hypothesis Hektor and coworker found that anaerobic growth on xylose by a XI-expressing recombinant *S. cerevisiae* strain was hardly affected by inactivating the oPP-pathway [47].

## Conclusions

In this work straightforward evolution of strain fitness (530% in 61 generations) paired with low-level adaption of undesired phenotypes was achieved by carrying out all steps including selection, isolation and subsequent screening under anaerobic conditions. The resultant strain IBB10B05 displayed excellent xylose fermentation properties with respect to specific growth rate, ethanol yield and specific ethanol production rate while fermentation of glucose to ethanol was hardly affected. Its robustness under industrial relevant conditions with respect to stability of

evolved phenotype, pH and weak acid concentration was proven and rendered it competitive. Adaption to balanced growth on xylose by IBB10B05 was a stepwise hierarchical process in which adaption to growth preceded metabolic adjustment to substrate and environmental conditions. We further demonstrated that the previously assumed large value of  $m_{\text{ATP}}$  for anaerobic growth on xylose is predominantly an effect of polyol formation rather than substrate-specific.

## Materials and methods

### Strains and cultivation conditions

The recombinant strain BP10001 (CEN.PK 113-5D *ura3::(TDH3<sub>p</sub>-XKSI-CYCI<sub>t</sub>, TDH3<sub>p</sub>-CtXYL1(K274R/N276D)-CYCI<sub>t</sub>, TDH3<sub>p</sub>-GmXYL2-CYCI<sub>t</sub>)* was used [31]. A defined mineral (M-) medium containing (NH<sub>4</sub>)<sub>2</sub>SO<sub>4</sub> (5 g/L), MgSO<sub>4</sub>·7H<sub>2</sub>O (0.5 g/L), Tween-80 (0.42 mg/L), ergosterol (10 mg/L), 250 μL/L antifoam 204 (Sigma-Aldrich, Vienna, Austria), trace elements and vitamins [32,48] and K<sub>2</sub>HPO<sub>4</sub> buffer (14.4 g/L) pH 6.5 was used. Concentrations of xylose (XM-medium) and glucose (GM-medium) were 50 g/L and 20 g/L, respectively. The pH was always adjusted prior to sterilization. All cultivations were carried out at 30°C. For long-term storage at -70°C 15% (v/v) glycerol stock cultures were prepared with cells harvested at the stationary phase and grown in baffled shake flasks on GM-medium (BP10001) or in sealed flasks on XM-medium (evolved strains).

Growth experiments under aerobic conditions were carried out at 150 rpm in 1000 mL baffled shake flasks containing 50 mL XM-medium. Initial cell density was ~0.03 g<sub>BM</sub>/L. Corresponding precultures were prepared in 300 mL baffled shake flasks containing 30 mL XM-medium, inoculated through the addition of 30 μL of glycerol stock culture and cultivated for 2 days. Anaerobic cultivations were carried out in 100 mL flasks (Gerresheimer Lohr GmbH, Main, Germany) sealed with a chlorobutyl rubber septum and an aluminium screw cap with 10 mm opening and containing 90 mL of X(G) M-medium. Selected agitation at 180 rpm was sufficient to prevent sedimentation of cells. Anaerobic xylose fermentation under controlled pH conditions were performed in a Labfors III bioreactor (Infors HT, Bottmingen, Switzerland) with a working volume of 2 L as described in [28]. XM-Medium used in the bioreactor contained 3 g/L K<sub>2</sub>HPO<sub>4</sub> instead of 14.4 g/L used in flask cultivations. Experiments were initiated by the addition of biomass (BP10001: 2.5 – 3.5 g<sub>BM</sub>/L; evolved strains: 0.025 – 0.05 g<sub>BM</sub>/L). Flasks were purged for 15 min with sterile N<sub>2</sub> before and after inoculation. Preparatory cultures for BP10001 and the first preculture for evolved strains were prepared by aerobic cultivation in 1000 mL and 300 mL baffled shake flasks containing GM-medium, respectively. Cultivations were started by the addition of 30 μl glycerol

stock culture and incubated over night. BP10001 cells obtained were washed once with cold physiological NaCl solution prior to initiation of anaerobic xylose fermentations. Cells from evolved strains were directly transferred to sealed flasks (initial cell concentration:  $\sim 0.03$  g<sub>BM</sub>/L) containing XM-medium or GM-medium (initiation of glucose fermentation) and further cultivated. Cells at mid-exponential phase grown in XM-medium served as inoculum for xylose fermentations.

Anaerobic growth of evolved strains was further analyzed in dependence of concentrations of hydrogen (pH 5.0 – 6.5), acetate (0 – 100 mM), citrate (0 – 50 mM), bicarbonate (0 – 100 mM) and glycerol (0.6 g/L). Each experiment was done in duplicates.

### Evolutionary engineering

Fifteen mL tubes (Pyrex® Brand 9825, Fisher Scientific, Schwerte, Germany) filled with 10 mL of XM-medium were inoculated with BP10001 cells (directly from a glycerol culture) to a cell density of 0.04 g<sub>BM</sub>/L. Subsequently to inoculation tubes were purged with sterile N<sub>2</sub> for 15 min. After 91 days of prolonged incubation at 150 rpm 400 μL of cell suspension were transferred under anaerobic conditions in a Compact Glove Box 850-NB (Plas Labs Inc., MI, U.S.A.) to anaerobic cultivation (AC-) plates, containing yeast extract (8 g/L), peptone (10 g/L), xylose (20 g/L), agar-agar (13 g/L) as well as sodium thioglycolate (500 mg/L), L-cysteine (500 mg/L) and resazurin (1 mg/L), and incubated for 15 days in a 2.5 L anaerobic jar equipped with AnaeroGen bags (both Oxoid, Hampshire, England). Colonies grown were again streaked on AC-plates and incubated under exactly the same conditions for another 5 days in the anaerobic jar. Single colonies were isolated and further screened with respect to anaerobic  $\mu$  on xylose. To this end, colonies grown on AC-plates were transferred individually to sealed flasks and cultivated as described above. The best strain obtained, with respect to  $\mu$  (IBB10A02), was subjected to further evolutionary engineering by repetitive batches. IBB10A02 cells were therefore grown (start OD<sub>600</sub> was 0.05) under anaerobic condition in sealed flasks containing XM-medium. At mid-exponential phase (OD<sub>600</sub>  $\sim 1.0$ ) cells were transferred to a new batch (start OD<sub>600</sub>  $\sim 0.05$ ) containing XM-medium and again grown until cells reached mid-exponential phase. This procedure was repeated until  $\mu$  was approximately doubled. Positive strains were isolated and screened under anaerobic conditions.

### Analytics to cultivation experiments

Samples were withdrawn by using a hypodermic needle. OD<sub>600</sub> and extracellular metabolites were analyzed spectrophotometrically at 600 nm and by HPLC equipped with a RI/UV detector [31], respectively. Concentrations of CO<sub>2</sub> in the bioreactor off gas were measured with an

IN1313 acoustic gas analyzer (Innova AirTechInstruments, Ballerup, Denmark) as described previously [39]. Cell dry weight to OD<sub>600</sub> correlations were determined in accordance to a published protocol [31]. For BP10001 and evolved strains a correlation factor of 0.40 and 0.52 g/L dry cells per unit OD<sub>600</sub> was used, respectively. The pH sensor Minitrode (Hamilton Messtechnik GmbH, Höchst, Germany) was used to measure pH in cell-free supernatants.

### Phenotype stability

Cells of IBB10A02 and IBB10B05 were cultivated in 6 repetitive batches. Cultivations were carried out under aerobic conditions in 300 mL baffled shake flasks containing 20 mL of a yeast extract (10 g/L), peptone (20 g/L), dextrose (20 g/L) (YPD) medium. Thereafter cells were streaked on YPD-agar plates and 5 colonies of each strain isolated after incubation for 48 h. Growth characteristics on glucose and xylose under anaerobic conditions of isolated colonies was analyzed.

### Enzyme activities

Specific enzyme activities were determined from cell-free extracts obtained from mid-exponentially growing cells on xylose (evolved strains) or at pseudo-steady state of xylose conversion (BP10001). Volumetric enzyme activities of XR, XDH and XK were analyzed at 25°C in accordance to [31]. Utilization or formation of NADH was recorded at 340 nm. A molar extinction coefficient of 6.22 mM<sup>-1</sup> cm<sup>-1</sup> was used. Protein content was determined by the Bradford method using the Roti®-Quant dye (Carl Roth GmbH, Karlsruhe, Germany) and bovine serum albumin as a reference.

### Additional files

**Additional file 1: Figure S1.** Xylose assimilation routes typically employed in metabolic engineering of heterologous xylose utilization in *S. cerevisiae*. XR, XDH, XI and PP-pathway indicate xylose reductase, xylitol dehydrogenase, xylose isomerase and pentose phosphate pathway, respectively.

**Additional file 2: Estimation of ATP formation rates.**

### Abbreviations

#1: First fermentation phase; #2: Second fermentation phase;  $\mu$ : Specific growth rate; AC-plates: Anaerobic cultivation plates; BM: Dry cell weight; GM-medium: M-medium containing glucose; M-medium: Mineral medium;  $m_{ATP}$ : Maintenance coefficient; OD: Optical density; oPP: Oxidative PP-pathway; PP: Pentose phosphate;  $q$ : Specific substrate conversion or product formation rate;  $r_{ATP}$ : Specific rate of ATP formation; XR: Xylose reductase; XDH: Xylitol dehydrogenase; XI: Xylose isomerase; XM-medium: M-medium containing xylose; XK: Xylulose kinase;  $Y$ : Yield; YPD: Yeast peptone dextrose.

### Competing interests

The authors declare no commercial or financial conflict of interest.

#### Authors' contributions

MK and BN designed experiments; KL performed evolutionary engineering experiments and analysis of phenotype stabilities; KL, EK, SK and VN carried out fermentation experiments and HPLC analyses; KL and EK measured specific enzyme activities; MK, EK and KL analyzed experimental data; MK and BN drafted the manuscript and MK wrote the paper; all authors have read the final version of the manuscript and given their approval.

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