POLITECNICO DI TORINO Repository ISTITUZIONALE

Impact of controlled vacuum induced surface freezing on the freeze drying of human plasma

Original

Impact of controlled vacuum induced surface freezing on the freeze drying of human plasma / Arsiccio, A.; Matejtschuk, P.; Ezeajughi, E.; Riches-Duit, A.; Bullen, A.; Malik, K.; Raut, S.; Pisano, R. - In: INTERNATIONAL JOURNAL OF PHARMACEUTICS. - ISSN 0378-5173. - STAMPA. - 582:(2020), p. 119290. [10.1016/j.ijpharm.2020.119290]

Availability: This version is available at: 11583/2862732 since: 2021-01-18T16:20:13Z

Publisher: Elsevier B.V.

Published DOI:10.1016/j.ijpharm.2020.119290

Terms of use: openAccess

This article is made available under terms and conditions as specified in the corresponding bibliographic description in the repository

Publisher copyright Elsevier postprint/Author's Accepted Manuscript

© 2020. This manuscript version is made available under the CC-BY-NC-ND 4.0 license http://creativecommons.org/licenses/by-nc-nd/4.0/.The final authenticated version is available online at: http://dx.doi.org/10.1016/j.ijpharm.2020.119290

(Article begins on next page)

1	Authors' post-prints
2	Arsiccio, A., Matejtschuk, P., Ezeajughi, E., Riches-Duit, A., Bullen, A., Malik, K., Raut, S., Pisano, R. (2020).
3	Impact of Controlled Vacuum Induced Surface Freezing on the Freeze Drying of Human Plasma.
4	International Journal of Pharmaceutics 582(30), article no. 119290.
5	* Corresponding author: roberto.pisano@polito.it
6	

Impact of Controlled Vacuum Induced Surface Freezing on the Freeze Drying of Human Plasma

1	٢	٦
1	-	1
	•	,

10	Andre	a Arsiccio ¹ , Paul Matejtschuk ² , Ernest Ezeajughi ² , Andrew Riches-Duit ⁴ , Anwen
11	Bullen	^{3,5} , Kiran Malik ² , Sanj Raut ⁴ & Roberto Pisano ¹ .
12	1.	Department of Applied Science and Technology, Politecnico di Torino, 24 corso
13		Duca degli Abruzzi, Torino, 10129 Italy.
14	2.	Standardisation Science & 3. Imaging Section, Analytical & Biological Sciences
15		Division & 4. Biotherapeutics Division, National Institute for Biological Standards &
16		Control (NIBSC), Blanche Lane, South Mimms, Potters Bar, Hertfordshire, United
17		Kingdom , EN6 3QG.
18	5.	UCL Ear Institute, Gray's Inn Road, London, UK, WC1X 8EE
19		
20		Email address of corresponding author: Paul.Matejtschuk@nibsc.org
21		

23 ABSTRACT

24 During the freezing step of a typical freeze drying process, the temperature at which nucleation is induced is 25 generally stochastically distributed, resulting in undesired within-batch heterogeneity. Controlled nucleation 26 techniques have been developed to address this problem; these make it possible to trigger the formation of 27 ice crystals at the same time and temperature in all the batch. Here, the controlled nucleation technique 28 known as vacuum induced surface freezing is compared to spontaneous freezing for the freeze drying of 29 human plasma, a highly concentrated system commonly stored in a dried state. The potency of Factor VIII 30 (FVIII), a sensitive, labile protein present in plasma, and the reconstitution time of the dried cakes are evaluated immediately after freeze drying, and after 1, 3, 6 or 9 months storage at different degradation 31 32 temperatures. We show that the application of controlled nucleation significantly reduces the reconstitution 33 time and in addition helps to improve FVIII stability.

34

35 **KEYWORDS:** freeze drying, controlled nucleation, plasma, biological activity

36

37 ABBREVIATIONS: VISF: Vacuum Induced Surface Freezing

38

39 1. INTRODUCTION

The freeze-drying process is widely used for preserving labile products in the pharmaceutical industry, by removal of water at low temperature to increase shelf life, without significantly affecting the therapeutic properties of the active ingredients (Fissore, 2019; Franks and Auffret, 2007; Rey and May, 2010; Ward and Matejtschuk, 2019). During freeze drying, the product is first frozen, and water is subsequently removed by sublimation during primary drying and desorption during secondary drying. The two drying phases are performed at low pressure, the first typically at sub-zero temperature, so as to minimize possible degradation stresses.

In the field of pharmaceutical freeze drying, where often many thousands of vials or ampoules are processed in a single cycle, the problem of potential heterogeneity within each batch is a major concern. Much of this heterogeneity is related to the freezing step, and specifically to the uncontrolled, random distribution of nucleation temperatures within the batch. The nucleation temperature determines the morphology of the final product, with a high nucleation temperature resulting in larger ice crystals (Searles et al., 2001). In turn, the ice crystal size corresponds to the pore size of the dried product, provided that no

collapse occurs, and has therefore an impact on process efficiency (Capozzi and Pisano, 2018; Hottot et al.,
2007; Kasper and Friess, 2011; Pikal et al., 2002). For instance, a large pore size speeds up the removal of
water by sublimation, reducing the primary drying time, but results in a slow desorption rate during secondary
drying (Oddone et al., 2016; Oddone et al., 2017).

57 A small ice crystal size also results in the formation of a large ice-water interface, where amphiphilic 58 molecules, such as proteins, could get adsorbed and unfold because of their interaction with the surface 59 (Strambini and Gabellieri, 1996). This surface-induced stress adds up to the risk of cold denaturation 60 (Franks, 1995; Privalov, 1990) that may occur because of the low temperature used during freezing, and it 61 has been shown that for many proteins it actually is the main source of protein instability during the freezing 62 process (Bhatnagar et al., 2008; Chang et al., 1996). Finally, the pore size of a dried product also affects the 63 reconstitution time, which is not a negligible factor to be considered, especially for highly concentrated 64 products. While low-concentration formulations generally reconstitute in less than 1 min (Lewis et al., 2010), 65 it may take up to 1 h for higher concentrated systems to yield an injectable solution (Shire et al., 2004), which 66 can be a critical issue clinically.

67 The possibility to control the nucleation temperature during freeze drying would therefore make it possible 68 to modulate the overall process efficiency, and the critical attributes of the final product as well. Moreover, 69 the batch homogeneity, which is a key requirement in the pharmaceutical and reference standard industries, 70 may be improved. It is therefore not surprising that various techniques have been developed over the years 71 to address this problem (Geidobler and Winter, 2013; Kasper, 2011; Pisano, 2019). Recent studies have 72 shown that induced nucleation has no deleterious effects and can even improve the lyophilization of model 73 proteins such as LDH (Fang et al., 2018), monoclonal antibodies (MAbs) (Awotwe-Otoo et al., 2013) and 74 human growth hormone (Oddone et al., 2020). In this study we will look at the impact of induced nucleation 75 on the reconstitution time of human plasma after freeze drying and the recovery of Factor VIII activity in that 76 plasma. Coagulation Factor VIII (FVIII:C) is the most labile haemostatic protein, whose activity is routinely 77 used to study/assess protein stability in plasma (Allain JP et al., 1983; Carlebjörk G et al., 1986; Takahashi H 78 et al., 1986; Swärd-Nilsson AM et al., 2006).

One commercially available solution the ice-fog technique (Brower et al., 2015; Geidobler et al., 2012; Patel et al, 2009; Rambhatla et al., 2004), uses small ice particles, generated by the release of cold nitrogen within the freezing chamber and that penetrate into the vials, to trigger ice nucleation. This ice fog could also be generated within an external condenser, or another cold chamber. Vacuum could be established in the freeze-dryer, while maintaining the condenser at atmospheric pressure. When connection is established

between the dryer and the condenser, the ice fog is transported into the drying chamber, inducing nucleation
(Ling, 2014; Umbach, 2017). Another approach, based on rapid pressurization/depressurization of the
drying chamber, may also be used (Bursac et al., 2009; Gasteyer et al., 2017; Konstantinidis et al., 2011).
However, not all freeze dryers can accommodate the overpressuring required to apply this high-pressureshift or depressurization method.

89 In this work, the so-called vacuum induced surface freezing (VISF) technique, also known as vacuum 90 induced nucleation (VIN), will be used. In VISF, a reduction in chamber pressure is used to trigger ice 91 formation in products that have been previously equilibrated at the desired nucleation temperature (T_0). The 92 nucleated samples are then held for a given amount of time (generally about 1 h) at the same or another 93 temperature (T_m) to promote the formation of large ice crystals. This results in a larger pore size, faster 94 primary drying rate, and reduced ice-water surface area compared to conventional freezing. This method 95 was first proposed by Kramer et al. (2002), and later used by other groups (Arsiccio et al., 2018; Liu et al., 96 2005; Oddone et al., 2014; Oddone et al., 2016; Oddone et al., 2017). Representative profiles of fluid 97 temperature and chamber pressure during application of this technique are shown in Figure 1.

98 Here, the method by Oddone et al. (2014; 2016; 2017), will be applied to human plasma, a highly 99 concentrated system that is commonly freeze dried. In the context of freeze-drying, the term high-100 concentration protein formulation is generally applied to preparations ranging from 50 to about 150 mg/ml of 101 protein (Garidel and Presser, 2019). This type of formulations typically shows increased viscosities, high 102 opalescence, phase separation or particle formation phenomena that are uncommon in low-concentration 103 preparations. Human plasma can perfectly fit into this definition, as it contains a huge amount of proteins. 104 Among them, FVIII is an essential clotting factor whose impaired function results in haemophilia A, a rare, 105 sex-linked bleeding disorder. FVIII is a labile plasma protein, which is particularly sensitive to denaturation 106 stresses. The effect of controlled nucleation on the stability of FVIII will be investigated, and a comparison 107 will be made with spontaneous freezing. This analysis will be performed both immediately after freeze drying, 108 and after 1, 3, 6 or 9 months accelerated degradation stability study at different temperatures (Kirkwood, 109 1977; Kirkwood, 1984; Kirkwood and Tydeman, 1984). The reconstitution time of the dried cakes obtained 110 after the two freezing protocols will also be assessed.

- 111
- 112
- 113
- 114

115 2. MATERIALS AND METHODS

116 **2.1 Material for filling**

117 Screened human plasma (Blood Group: A+, National Blood & Transplant, Colindale, UK) was thawed and Hepes (free acid H3375, Sigma Merck, Poole, UK) was added to a final concentration of 40 mM and the bulk 118 119 held over ice with gentle stirring. Batches of one ml aliquots were dispensed using a Hamilton autodilutor 120 (Hamilton M510B, supplied by Microlab Technologies Ltd, Westcliff -on Sea, UK) into 5 ml ampoules (glass 121 type I, Schott supplied by Adelphi Tubes, Haywards Heath, UK) and fitted with 13mm diameter halobutyl 122 rubber lyo-closures (West Pharma, supplied by Adelphi) - partially inserted to allow sublimation to occur. A 123 batch of 100 ampoules was prepared on each of two occasions and the coefficient of variation (CV) of fill 124 assessed by measuring empty, filled and dried weights on three ampoules across the batch. The ampoules 125 were then loaded directly onto a freeze dryer (LyoBeta 15, Telstar Azbil SpA, Terrassa, Spain) and the 126 freeze drying cycle begun.

127

128 2.2 Freeze drying cycle

129 Two consecutive cycles were performed, one with spontaneous nucleation and one with VISF controlled 130 nucleation. During the VISF cycle, the product was first equilibrated at -5 °C for about 1 h. The pressure was 131 then reduced to a low value (about 1 mbar), promoting a strong evaporation from the ampoules, and 132 therefore a decrease in temperature that triggered nucleation. As soon as nucleation was induced in all 133 ampoules, pressure was guickly released to the atmospheric value to avoid boiling of the solution. The 134 product was then equilibrated at -10 °C for about 45 min before the final ramp to -50 °C. The combination T_n=-5°C, T_m=-10°C was selected based on previous observations (Oddone et al., 2016), where different 135 values for both equilibration temperatures were tested. $T_n=-5^{\circ}C$ should guarantee the formation of large ice 136 crystals. Lower temperature values (e.g, -10°C) were found to result in a smaller crystal size, while, for 137 138 instance, $T_n = +5^{\circ}$ C increased the within-ampoule heterogeneity. Different values of T_m were also compared 139 [Oddone et al., 2016]. It was observed than when T_m was too high, for instance equal to -5°C, the solution could not freeze completely during the holding stage, and thus froze as soon as the temperature of the heat 140 141 transfer fluid was decreased to -45/-50°C. This resulted in smaller ice crystals, and therefore larger ice-water surface area, within the product. By contrast, T_m=-10°C improved the situation, promoting the formation of 142 large ice crystals during the holding step and avoiding melting back phenomena. For spontaneous freezing, 143 144 a continuous 0.5 °C/min ramp to -50 °C was performed.

For both the spontaneous and the VISF cycle, the product was held at -50 °C for 3 h to complete freezing. The product was then held at -50 °C for 1 h at 0.2 mbar , and for 1 h at 0.1 mbar. The temperature was subsequently raised to -12 °C in 1 h and held at 0.1 mbar for 30 h. Secondary drying was eventually performed at 25 °C for 20 h. A 10 h ramp between primary and secondary drying was used. After the cycle the dryer was back-filled with dry nitrogen (from boil off of pure liquid nitrogen) and the closures stoppered down before ampoules were removed from the dryer. Ampoules were then flame-sealed using a manual ampoule sealer (Ampulmatic, Adelphi Tubes).

- 152 A scheme of the protocols used for freeze drying is shown in Table 1.
- 153
- 154 Table 1. Scheme of the experimental protocols used in this work for the freeze drying of human plasma.

		VISF			SPON				
Step	p T, °C P, mbar		t, h	T, °C	P, mbar	t, h			
Freezing									
holding	-5	-	1	-	-	-			
nucleation	-5	~1	-	-	-	-			
holding	-10	-	0.75	-	-	-			
ramp	-50	-	1	-50	-	1.5			
holding	-50		3	-50	-	3			
	SPON/VISF								
T, °C			P, n	nbar	t, h				
Primary Dryin	ng								
holding		50	0	.2	1				
holding		50	0	.1	1				
ramp		12	0.1		1				
holding	holding -12			.1	30				
Secondary Drying									
ramp	2	25	0	.1	10				
holding	2	25	0	.1	20				

155 SPON: spontaneous nucleation, VISF: vacuum induced surface freezing.

156

157

158 In each batch, the temperature profile inside one ampoule was monitored by means of T-type 159 copper/constantan miniature thermocouples placed at the bottom centre of the vial, and touching the bottom. During drying, both a capacitance (MKS Baratron) and a thermal conductivity (Pirani) manometer were used 160 161 to monitor the pressure inside the drying chamber. The capacitance manometer always outputs the exact value of pressure within the chamber, while the Pirani gauge readings are shifted to higher values during 162 163 primary drying. When the Pirani sensor readings begin to decay, the onset time is reached, indicating that a 164 significant number of ampoules have completed the sublimation process (Patel et al., 2010). When the 165 readings of the Pirani and Baratron manometers eventually converge, the offset time is reached, indicating

that sublimation has ended in all the batch (see Figure 2). The offset time can be considered as the end of the primary drying phase, while the difference between offset time and onset time (in the following referred to as onset-offset time) is a measure of within-batch heterogeneity. The larger this difference the greater the difference in sublimation behavior of ampoules within the batch.

170

171 **2.3 FVIII assay, reconstitution times and stability study**

FVIII chromogenic assays, for potency determination of FVIII in ampoules prepared by the two different 172 173 freezing protocols, were carried out on the ACLTOP 550 analyzer (Werfen Ltd., Birchwood, UK) using the 174 Coatest SP4 FVIII chromogenic kit (Chromogenix, Werfen Ltd., Birchwood, UK), according to European 175 Pharmacopoeia guidelines (Ph. Eur. monograph Human coagulation factor VIII - 0275). Briefly, optimal 176 amounts of calcium and phospholipids, and excess amounts of factors IXa (FIXa) and X (FX) were added to 177 the reconstituted test sample containing the FVIII analyte, and under these conditions, factor X is converted 178 to FXa by FIXa, where the rate of FX activation is dependent on the amount of FVIII present in the test 179 sample. The FXa generated hydrolyses the chromogenic substrate and the amount of colour produced is 180 read photometrically at 405 nm. The intensity of colour is therefore proportional to the amount of FVIII in the 181 test sample.

For the stability studies, freeze dried ampoules of human plasma containing FVIII were put down for storage at degradation temperatures of +45°C, +37°C, +20°C, +4°C and -20°C. Assessment of the stability of the FVIII was carried out through accelerated degradation studies which allow the prediction of degradation rates of samples stored at low temperatures (e.g. -20°C) based on the observed loss in potency of samples stored at elevated temperatures (e.g. +4, +20, +37, +45 °C) (Kirkwood, 1977). This is an indirect method used routinely to determine rate of loss based on the Arrhenius equation, where a first order reaction rate is assumed (Kirkwood, 1984; Kirkwood and Tydeman, 1984).

Test ampoules were retrieved from different storage temperatures, at different time points and each ampoule was reconstituted as described in the current European Pharmacopoeia guideline, (Ph. Eur. general chapter section - assay of human coagulation factor VIII, monograph 2.7.4). Briefly, to each test ampoule, 1 ml sterile water was added followed by gentle swirling and then allowed to stand at ambient temperature until dissolved.

The time for full reconstitution was obtained for the two different freezing protocols. The reconstituted samples were then assayed on the ACLTOP 550 analyser, where each sample was diluted (1/50, 1/100 & 1/200) in kit buffer in duplicates prior to the chromogenic assay run. Assays were carried out relative to the

WHO 6th International Standard (WHO 6th IS) FVIII/VWF Plasma (07/316) for potency estimation or relative
to pre-freeze-drying liquid sample for assessment of % loss in potency or relative to the respective -20°C
freeze-dried samples to assess stability. Results were analysed using CombiStats software, version 5.0
(1999-2013 EDQM/Council of Europe).

201

202 2.4 Scanning electron microscopy analysis

The pore dimensions of the products obtained after freeze-drying was analysed using a Scanning Electron Microscope (SEM). Three samples from both the spontaneous and the VISF cycle were examined. Each sample was cut along the vertical axis of the cake, and a central section was mounted onto aluminium stubs with conductive silver paint (Agar Scientific, Stanstead, UK). Samples were sputter coated with 4nm gold and imaged immediately after mounting. Imaging was carried out by a JSM 7401F SEM (Jeol Ltd, Welwyn Garden City, UK) operating at 5kV. Images were obtained by secondary electron detection. SEM images were recorded at the top, centre and bottom of each cake.

For analysis, approximately 50 pores were selected in each image (at x50 magnification), and each of them was approximated to an ellipse. The diameter of the circle having the same area to perimeter ratio of the approximating ellipse was then assumed as pore dimension, and the numerical average of the obtained distribution was assumed as the average pore size, D_p , of the product.

214

215 **2.5 BET determination of specific surface area**

Nitrogen (N₂) adsorption method was used in a physisorption analyser (ASAP 2020 Plus, Micromeritics, Norcross, GA, USA) to determine the specific surface area (SSA) of freeze dried samples. The samples were degassed for 5 h at 293 K under vacuum. N₂ adsorption isotherms were acquired at 77 K in a P/P₀ (relative pressure) range of 0.005-0.99. For the BET analysis, 12 points in the range P/P₀=0.05-0.30 were then used. In all cases, the sample size was between 250 and 300 mg.

221

222 **3. RESULTS**

223 **3.1 Performance of the Freezing Protocols**

The positive effects of VISF on primary drying time, already discussed in the literature (Arsiccio et al., 2018; Oddone et al., 2014; Oddone et al., 2016), were confirmed in this work. As shown in Figure 2a, primary drying lasted about 17.6 h for the spontaneous cycle (difference between offset time and the beginning of the drying process). Moreover, the onset-offset time in this case amounted to about 4.2 h. In contrast, primary drying was shorter, about 13.1 h, when the VISF technique was applied (Figure 2b). This result is not negligible, as it corresponds to approximately 25.6 % reduction in sublimation time upon application of controlled nucleation. The onset-offset time, which is a measure of variability in sublimation behaviour, also decreased to about 3 h when controlled nucleation was used. This suggests that the application of VISF is beneficial when homogeneity is an issue, and this effect may be even more significant in the case of large industrial-scale batches.

The observed difference in sublimation rate between spontaneous and controlled nucleation may be 234 235 related to a difference in pore size. The VISF technique made it possible to induce nucleation in all samples at a high temperature (-5 °C), where formation of ice nuclei is still not observed in spontaneously-frozen 236 237 ampoules. For instance, the thermocouple-containing ampoule during the spontaneous run nucleated at 238 about -15 °C (as shown in the inset of Figure 2a). In turn, a high nucleation temperature translates into the 239 formation of large ice crystals, that subsequently convert into equally large pores when ice is removed during 240 sublimation. The removal of water vapour through these pores occurs with a significantly reduced resistance 241 to mass transfer, boosting the sublimation process.

242 This hypothesis was confirmed from viewing the SEM images shown in Figure 3, where the VISF 243 technique evidently promoted the formation of larger pores compared to spontaneous nucleation. The 244 images for one sample only are displayed in Figure 3, but the same trend was observed for all the three 245 ampoules analyzed, as detailed in Table 2. The use of microscopy to assess the structure of frozen or freeze 246 dried cakes has been reported several times in the literature (Vollrath et al., 2019; Goshima et al., 2016; 247 Abdul-Fattah et al., 2008), and here the SEM images were also quantitatively analyzed, similarly to what was done in previous works, where frequency domain image analysis (Grassini et al., 2016) or segmentation 248 249 approaches (Arsiccio et al., 2019) were used for this purpose.

250

Table 2. Pore dimension D_p (as measured by SEM) and BET specific surface area (as measured by N₂ adsorption) in the dried product, for spontaneous and controlled nucleation (average ± standard deviation). For the BET surface area, two repetitions were made, and both sets of measurements are reported in the last column.

Sample #	Freezing Protocol		<i>D</i> _ρ , μm	BET surface area, m ² /g			
		bottom	centre	top			
1		118 ± 49	130 ± 68	115 ± 71			
2	VISF	120 ± 48	131 ± 58	115 ± 58	0.19 ± 0.01		
3		104 ± 46	121 ± 47	107 ± 55	0.25 ± 0.01		
1		49 ± 15	65 ± 21	52 ± 13			
2	Spon.	51 ± 18	65 ± 18	52 ± 13	0.41 ± 0.01		
3		68 ± 17	68 ± 15	65 ± 15	0.40 ± 0.01		

256

257 Here, the difference in pore dimension was quantified by an image analysis technique, where each pore was 258 approximated to an ellipse, and the diameter of the circle having equal area to perimeter ratio was computed. 259 Averaging over all the samples, the VISF technique resulted in a dried cake with pore size in the order of 260 about 114, 127 and 112 µm at the bottom, centre and top, respectively. The presence of larger pores at the 261 centre of the cake is common during freeze-drying, because the contact with the dryer shelves, and the 262 presence of cryo-concentration effects promote the formation of a less open structure at the cake edges. In 263 contrast, the average values for the spontaneously nucleated samples were lower, about 56, 66 and 56 µm 264 at the bottom, centre and top, indicating that the lower nucleation temperature in these samples 265 approximately halved the pore size compared to the case of the VISF cycle.

The SEM data were confirmed by the BET specific surface area (SSA) values, also listed in Table 2. As expected, a larger pore size obtained when applying controlled nucleation resulted in a smaller SSA, which as will be shown in the following, may have an impact on protein stability.

269

270 3.2 FVIII residual activity

In this study, as FVIII is the most labile haemostasis protein in plasma, it was decided that assessment of the functional activity of FVIII in the freeze-dried samples would allow more clearly to discern any differences between the 2 freeze drying techniques. The potency of FVIII was measured post-drying (n=2), and after 1 (n=1), 3 (n=1), 6 (n=2) or 9 (n=2) months storage at 45°C, 37°C, 20°C, 4°C or -20 °C, using the FVIII chromogenic assay, as described in the methods section. The FVIII activity of the plasma sample before lyophilisation was also measured relative to the WHO 6th IS and gave a value of 0.42 IU/ml [95%CL: 0.38 – 0.46].

Figure 4a illustrates FVIII potencies measured relative to the WHO 6th IS, for 6 months storage and, as expected, FVIII potency decreased during storage especially at the highest temperature (37°C and 45°C). Furthermore, the graph indicates a marked difference between the 2 freeze drying techniques with the VISF technique showing higher potencies compared to spontaneously frozen samples. This is reflected in greater % loss in potency (i.e. potencies relative to pre-freeze-drying liquid samples) for the spontaneously frozen samples compared to VISF samples, see Figure 4b.

Furthermore, the residual FVIII potencies for ampoules stored at +4°C, +20°C, +37°C and +45°C, for the two different freezing protocols, were expressed relative to ampoules stored at -20°C using an arbitrary value 286 1.00 for the -20°C ampoules. The Arrhenius model was then fitted to the data to obtain predictions of the expected loss in potency over time. Figure 5 shows the Arrhenius plot (logarithm of rate vs. inverse of 287 288 temperature) for FVIII degradation observed during storage after spontaneous nucleation (blue) and vacuum 289 induced surface freezing (red). The experimental points have been fitted with a line, and the R² values 290 obtained are good, pointing towards an Arrhenius behavior. While non-Arrhenius aggregation has sometimes 291 been observed (Wang and Roberts, 2013), the Arrhenius kinetics has often been found to be valid for lyophilized products (Wang et al., 2009; Duddu and Dal Monte, 1997; Breen et al., 2001; Perez-Moral et al. 292 293 2010). Indeed in a study on behalf of the Scientific & Standardisation Committee of the International Society 294 on Thrombosis and Haemostasis Hubbard et al. demonstrated not only that the Arrhenius model was a good 295 fit for lyophilised plasma with four coagulation factor markers, but also that factor VIII was the most labile of 296 the factors studied (Hubbard et al., 2010).

The predicted mean % loss per year, based on above data after 9 months storage at the different elevated temperatures, for the VISF technique and the spontaneous nucleation, were calculated and are shown in Table 3.

- 300
- 301

Table 3. Mean predicted degradation rates expressed as % loss per year after storage for 9 months.

Chromogenic	[§] Mean predicted % loss per year						
FVIII Potency	[95% upper confidence limits of predicted loss]						
Method	-20°C	+4°C	+20°C	+37°C			
Spontaneous	0.001	0.198	5.994	80.216			
Nucleation	[0.001]	[0.382]	[8.598]	[80.702]			
Controlled (VISF)	0.000	0.003	0.640	60.951			
Nucleation	[0.000]	[0.009]	[1.155]	[66.728]			

304

[§]These results are based on stability data obtained from 4 time points over a 9-months period.

305

The predicted % loss in FVIII potency per year tended to be greater for the spontaneous nucleation compared to controlled nucleation (e.g. 0.198 vs 0.003 respectively for storage at +4°C). These results indicate a greater stability of the FVIII molecule in human plasma, when freeze dried under controlled (VISF) nucleation compared to spontaneous nucleation.

311

312 3.3 Reconstitution times

The reconstitution time is a crucial parameter for all pharmaceutical lyophilizates, and the freeze drying process should be designed so as to deliver a suitable reconstitution step. In this work, the reconstitution time of freeze-dried plasma was measured after storage at different temperatures for 1, 3, 6 or 9 months, in the case of both controlled and spontaneously nucleated samples. Reconstitution time of freeze-dried plasma WHO Reference Standard (07/316) was also obtained for comparison.

The results of this analysis are reported in Table 4 and indicate a remarkable improvement in 318 319 reconstitution time when the VISF technique was applied. This is evident already for the case of storage at 320 low temperature, where VISF approximately halved the reconstitution time. For instance, it took about 4, 5.2 321 and 7.7 min to obtain a clear solution from the VISF samples stored for 6 months at -20 °C, 4 °C or 20 °C, 322 respectively, while the corresponding times for conventional freezing were 11.7, 15.3 and 15.4 min. Similar 323 improvements in reconstitution times of VISF technique were observed when compared to reconstitution 324 times of the WHO reference standard (07/316). For samples stored at higher high temperatures (37°C or 325 45°C), the freeze-dried bulk can harden, forming insoluble clumps and the sample can become compacted 326 and difficult to solubilize with water. This was observed with some samples, albeit less so with the VISF 327 technique compared to conventional freeze-drying, where reconstitution with water did not occur within 25 328 minutes (Table 4).

329

	Reconstitution Times, min										
Time months	-20 °C storage		4 °C storage		20 °C storage		37 °C storage		45 °C storage		
montho	Spon.	VISF	Ref. Std	Spon.	VISF	Spon.	VISF	Spon.	VISF	Spon.	VISF
1	13.5	7.0	12.3	-	-	-	-	21^	20	#	22
3	10.6	5.5	11.5	-	-	-	-	22	20	#	#
6	11.7	4.0	10.0	15.3	5.2	15.4	7.7	#	20.8^	-	-
9	11.5	5.0	10.4	-	-	15.0	10.5	-	-	#	20^

Table 4. Reconstitution times (n=1) of freeze dried cakes after storage at controlled temperature.

331

^ Some insoluble clumps still present

332 # Did not reconstitute within 25 min

333 - Reconstitution not carried out

335 4. DISCUSSION

336 In previous studies, application of the depressurization technique to lactate dehydrogenase (Fang et al., 337 2018) reduced the degradation of LDH during the freezing process, but did not markedly improve protein 338 stability during the entire freeze-drying process. Controlled nucleation by depressurization was also reported 339 to suppress glass fogging, i.e., the undesired migration of protein solutions up on the inner walls of glass 340 vials during the freezing step of lyophilization, and to result in higher stability against shaking stress (Singh et 341 al., 2018). Application of the ice-fog technique (Vollrath et al., 2018) to lyophilized monoclonal antibody 342 formulations stored at different temperatures reduced particle formation in highly concentrated systems. 343 However, the addition of polysorbates resulted in an overall lower particle level, with no further advantage of 344 controlled nucleation on protein stability. At low concentration, no difference with respect to particle formation 345 between the controlled and spontaneously nucleated samples was detected. These results are in line with 346 our previous study (Oddone et al., 2020), where HPLC-SEC and a cell-based potency assay seemed to give 347 evidence for no dramatic difference in the behaviour of hGH at low concentration when either VISF or 348 spontaneous nucleation were used. Our results for the highly concentrated plasma system, combined with 349 previously published data reporting a negligible effect of controlled nucleation on protein stability in low 350 concentrated systems (Oddone et al., 2020; Vollrath et al., 2018), seem to suggest that the benefits of 351 controlled nucleation may depend on concentration. This result represents an interesting observation, that 352 warrants further investigation.

353 However, the results obtained for FVIII activity in this work seem to indicate a difference between the two 354 freezing protocols, with the VISF technique resulting not only in improved process efficiency, but also in enhanced protein stability. This reduced loss in protein activity may be related to the smaller ice-water 355 356 interface resulting from application of controlled nucleation. As evident from the SEM images and the BET 357 analysis, the VISF technique promoted the formation of structures having larger ice crystals, that expose a 358 reduced surface area compared to spontaneously nucleated samples. As a result, the risk that the protein 359 adsorbs and denatures at the ice interface is reduced, likely promoting the observed preservation of the 360 native structure. It must also be borne in mind that FVIII is a much larger multi-domain protein with complex 361 intermolecular interactions which can impact on its activity, and so direct comparison to a small protein like 362 hGH (Oddone et al., 2020) may not be appropriate. An Arrhenius-based model for measuring stability was used [Kirkwood 1977,1984, Kirkwood et al 1984] for convenience and comparison between the two 363 364 preparation are drawn. However, non-Arrhenius based models have been used by others [Jameel et al 365 2009].

When storage at high temperature is considered, application of the VISF technique made it possible to reconstitute samples that would not return to a liquid, clump-free solution if freeze dried by conventional freezing.

For instance, the VISF sample stored for 1 month at 45 °C could be reconstituted, while this was not possible in the case of conventional freezing (see Table 4). Similarly, it was possible to reconstitute the sample frozen by controlled nucleation and then stored for 6 months at 37 °C, even though some insoluble clumps were still present after 25 min, while the same result could not be achieved in the case of spontaneous freezing.

When rehydrating a freeze dried product, the gas within the pores should be displaced by the reconstitution medium so as to allow wetting of the cake. Afterwards, hydration of the solid may take place. A large pore size may promote the displacement of gas from the cake, and this is probably the reason for the observed behaviour. This same explanation was proposed in a previous work (Geidobler et al., 2013), where application of the ice-fog technique shortened the reconstitution time of highly-concentrated protein formulations. A similar reduction in reconstitution time was observed when the depressurization technique was applied to highly concentrated monoclonal antibody solutions (Singh et al., 2018).

Overall, the benefits observed when using controlled (VISF) nucleation (compared to spontaneous nucleation) in the freeze drying process of plasma (i.e. increased stability and quicker reconstitution) are likely to be extremely important in the development of reference plasma standards and reagents. Although in this work the lyophilised plasma is a reference material and the shorter reconstitution time is therefore purely a convenience, faster reconstitution of therapeutic plasma-derived products would be of enormous clinical benefit, in particular in on-demand treatment.

387

388 5. CONCLUSIONS

Two different freezing protocols, with or without the possibility to control the nucleation temperature, have 389 390 been used to freeze dry human plasma. A degradation study has been subsequently performed, and both the potency of FVIII and the reconstitution time have been measured in ampoules stored at different 391 392 temperatures for up to 9 months. Overall, our results suggest that the controlled nucleation approach results 393 in reduced primary drying time, because it promotes the formation of larger pores within the dried cake. The 394 difference in cake morphology between the two freezing protocols also accounts for the improvement in 395 reconstitution time in samples obtained by controlled nucleation. The easier displacement of gas from larger pores allows an easier dissolution of the highly concentrated plasma lyophilizate. At the same time, the 396

397 smaller ice-water surface area when pores are large minimizes the risk of protein adsorption, and 398 denaturation, at the ice interface. This may be at the basis of the improvement in FVIII potency for ampoules 399 obtained by the VISF technique. Combined with previously published data, our findings suggest that the 400 benefits of controlled nucleation on protein stability may be more pronounced for highly concentrated 401 systems. This is an interesting finding and will be the subject of future investigations.

402

403 ACKNOWLEDGEMENTS

404 The Italian Ministry for Research and University is gratefully acknowledged for the PhD studentship to 405 Andrea Arsiccio. Chiara Vitale Brovarone, Sonia Fiorilli, Carlotta Pontremoli and Claudia Udrescu are 406 thankfully acknowledged for their help with BET analyses. 407 **REFERENCES**

- 408
- Abdul-Fattah, A.M., Lechuga-Ballesteros, D., Kalonia, D.S., Pikal, M.J., 2008. The impact of drying method
 and formulation on the physical properties and stability of methionyl human growth hormone in the
 amorphous solid state. J. Pharm. Sci. 97, 163-184.
- Allain JP, Friedli H, Morgenthaler JJ, Pflugshaupt R, Gunson HH, Lane RS, Myllylä G, Rock GA, Stryker MH,
 Woods KR, 1983. International Forum: What are the critical factors in the production and quality
 control of frozen plasma intended for direct transfusion or for fractionation to provide medically
 needed labile coagulation factors. Vox Sang. 44, 246–259
- Arsiccio, A., Barresi, A.A., De Beer, T., Oddone, I., Van Bockstal, P-J., Pisano, R., 2018. Vacuum induced
 surface freezing as an effective method for improved inter- and intra-vial product homogeneity. Eur.
 J. Pharm. Biopharm. 128, 210-219.
- Arsiccio, A., Sparavigna, A.C., Pisano, R., Barresi, A. A., 2019. Measuring and predicting pore size
 distribution of freeze-dried solutions. Dry. Technol. 37, 435-447.
- Assay of human coagulation factor VIII, monograph 2.7.4. Ph. Eur. 8th edition. Strasbourg, France: Council
 of Europe; 2014.
- Awotwe-Otoo, D., Agarabi, C., Read, E.K., Lute, S., Brorson, K.A., Khan, M.A., Shah, R.B., 2013. Impact of
 controlled ice nucleation on process performance and quality attributes of a lyophilized monoclonal
 antibody. Int. J. Pharm. 450, 70-78.
- Bhatnagar, B.S., Pikal, M.J., Robin, H.B., 2008. Study of the individual contributions of ice formation and
 freeze-concentration on isothermal stability of lactate dehydrogenase during freezing. J. Pharm. Sci.
 97, 798-814.
- Breen, E.D., Curley, J.G., Overcashier, D.E., Hsu, C.C., Shire, S.J., 2001. Effect of moisture on the stability
 of a lyophilized humanized monoclonal antibody formulation. Pharm. Res. 18, 1345-1353.
- Brower, J., Lee, R., Wexler, E., Finley, S., Caldwell, M., Studer, P., 2015. New developments in controlled
 nucleation: Commercializing VERISEQ® nucleation technology, in Varshney, D., Singh, M. (Eds.),
 Lyophilized Biologics and Vaccines. Springer, New York.
- Bursac, R., Sever, R., Hunek, B., 2009. A practical method for resolving the nucleation problem in
 lyophilization. Bioproc. Int. 7, 6672.

- Capozzi, L.C., Pisano, R., 2018. Looking inside the black box: Freezing engineering to ensure the quality of
 freeze dried biopharmaceuticals. Eur. J. Pharm. Biopharm. 129, 58-65.
- Carlebjörk G, Blombäck M, Pihlstedt P, 1986. Freezing of plasma and recovery of factor VIII. Transfusion.
 26, 159–162.
- Chang, B.S., Kendrick, B.S., Carpenter, J.F., 1996. Surface-induced denaturation of proteins during freezing
 and its inhibition by surfactants. J. Pharm. Sci. 85, 1325-1330.
- 442 Council of Europe European Pharmacopoeia Commission: European Pharmacopoeia 8.2, 2014.
 443 Monograph 2.7.4 Assay of human coagulation factor VIII. Strasbourg.
- 444 Duddu, S.P., Dal Monte, P.R., 1997. Effect of glass transition temperature on the stability of lyophilized 445 formulations containing a chimeric therapeutic monoclonal antibody. Pharm Res. 14, 591-595.
- Fang, R., Tanaka, K., Mudhivarthi, V., Bogner, R.H., Pikal, M.J., 2018. Effect of controlled ice nucleation on
 stability of lactate dehydrogenase during freeze-drying. J. Pharm. Sci. 107, 824-830.
- Fissore, D., Pisano, R., Barresi, A., 2019. Freeze drying of pharmaceutical products. CRC Press, Boca
 Raton, Florida, USA. pp. 1-192.
- 450 Franks, F., 1995. Protein destabilization at low temperatures. Adv. Protein Chem. 46, 105-139.
- 451 Franks, F., Auffret, T., 2009. Freeze drying of pharmaceuticals and biopharmaceuticals: Principles and
 452 practice. RSC publishing, Cambridge, UK, pp. 1-206.
- Garidel, P., Presser, I., 2019. Lyophilization of high-concentration protein formulations, in Ward, K.,
 Matejtschuk, P. (Eds.), Lyophilization of Pharmaceuticals and Biologicals. Methods in Pharmacology
 and Toxicology. Humana Press, New York.
- 456 Gasteyer, T.H., Sever, R.R., Hunek, B., Grinter, N., Verdone, M.L., May 2017. Lyophilization system and 457 method. US Patent 9651305 B2.
- 458 Geidobler, R., Mannschedel, S., Winter, G., 2012. A new approach to achieve controlled ice nucleation of 459 supercooled solutions during the freezing step in freeze drying. J. Pharm. Sci. 101, 4409-4413.
- Geidobler, R., Winter, G., 2013. Controlled ice nucleation in the field of freeze drying: Fundamentals and
 technology review. Eur. J. Pharm. Biopharm. 85, 214-222.
- Geidobler, R., Konrad, I., Winter, G., 2013. Can controlled ice nucleation improve freeze drying of highly concentrated protein formulations? J. Pharm. Sci. 102, 3915-3919.
- Goshima, H., Do, G., Nakagawa, K., 2016. Impact of ice morphology on design space of pharmaceutical
 freeze-drying. J. Pharm. Sci. 105, 1920-1933.

- Grassini, S., Pisano, R., Barresi, A.A, Angelini, E., Parvis, M., 2016. Frequency domain image analysis for
 the characterization of porous products. Measurement 94, 515-522.
- Hottot, A., Vessot, S., Andrieu, J., 2007. Freeze drying of pharmaceuticals in vials: Influence of freezing
 protocol and sample configuration on ice morphology and freeze-dried cake texture. Chem. Eng.
 Process. 46, 666-674.
- Hubbard, A.R., Kitchen, S., Beeharry, M., Bevan, S.A., Bowyer, A., 2011. Long term stability of the Scientific
 and Standardisation Committee Secondary Coagulation Standard (SSC Lot no 3). J. Thromb.
 Haemost. 9, 1246-1248.
- 474 Human coagulation factor VIII, monograph 0275. Ph. Eur. 8th Edition. Strasbourg, France: Council of
 475 Europe; 2014.
- Jameel F, Tchessalov S, Bjornsen E, Lu X, Bersman M, Pikal MJ. Development of a freeze dried
 biosynthetic Factor VIII: I. A case study in the optimization of formulation. Pharm Dev Technol
 2009;14:687-97.
- Kasper, J.C., Friess, W.F., 2011. The freezing step in lyophilization: Physico-chemical fundamentals,
 freezing methods and consequences on process performance and quality attributes of
 biopharmaceuticals. Eur. J. Pharm. Biopharm. 78, 248-263.
- 482 Kirkwood, T.B.L., 1977. Predicting the stability of biological standards and products. Biometrics 33, 736-742.
- 483 Kirkwood, T.B.L., 1984. Design and analysis of accelerated degradation tests for the stability of biological
 484 standards III. Principles of design. J. Biol. Stand. 12, 215-224.
- Kirkwood, T.B.L., Tydeman, M.S., 1984. Design and analysis of accelerated degradation tests for the stability
 of biological standards II. A flexible computer program for data analysis. J. Biol. Stand. 12, 207-214.
- Konstantinidis, A.K., Kuu, W., Otten, L., Nail, S.L, Sever, R.R., 2011. Controlled nucleation in freeze drying:
 Effects on pore size in the dried product layer, mass transfer resistance, and primary drying rate. J.
 Pharm. Sci. 100, 3453-3470.
- Kramer, M., Sennhenn, B., Lee, G., 2002. Freeze drying using vacuum-induced surface freezing. J. Pharm.
 Sci. 91, 433-443.
- Lewis, L., Johnson, R.E., Oldroyd, M.E., Ahmed, S.S., Joseph, L., Saracovan, I., Sinha, S., 2010.
 Characterizing the freeze drying behavior of model protein formulations. AAPS PharmSciTech 11, 1580-1590.
- 495 Ling, W. Controlled Nucleation During Freezing Step of Freeze Drying Cycle Using Pressure Differential Ice

- 496 Fog Distribution. Patent US 8839528 B2, September 23, 2014. Patent EP 2702342 B1, April 20,
 497 2014.
- Liu, J., Viverette, T., Virgin, M., Anderson, M., Paresh, D., 2005. A study of the impact of freezing on the lyophilization of a concentrated formulation with a high fill depth. Pharm. Dev. Technol. 10, 261-272.
- 500 Oddone, I., Pisano, R., Bullich, R., Stewart, P., 2014. Vacuum-induced nucleation as a method for freeze-501 drying cycle optimization. Ind. Eng. Chem. Res. 53, 18236-18244.
- 502 Oddone, I., Van Bockstal, P-J., De Beer, T., Pisano, R., 2016. Impact of vacuum-induced surface freezing on 503 inter- and intra-vial heterogeneity. Eur. J. Pharm. Biopharm. 103, 167-178.
- 504 Oddone, I., Barresi, A.A., Pisano, R., 2017. Influence of controlled ice nucleation on the freeze drying of 505 pharmaceutical products: The secondary drying step. Int. J. Pharm. 524, 134-140.
- Oddone, I., Arsiccio, A., Duru, C., Malik, K., Ferguson, J., Pisano, R., Matejtschuk, P., 2020. Vacuum
 induced surface freezing for the freeze drying of the human growth hormone: How does nucleation
 control affect protein stability? J. Pharm. Sci. 109, 254-263.
- Patel, S., Bhugra, C., Pikal, M., 2009. Reduced pressure ice fog technique for controlled ice nucleation
 during freeze drying. AAPS PharmSciTech 10, 1406–1411.
- Patel, S.M., Takayuki, D., Pikal, M.J., 2010. Determination of end point of primary drying in freeze drying
 process control. AAPS PharmSciTech 11, 73-84.
- Pérez-Moral, N., Adnet, C., Noel, T.R., Parker, R. 2010. Characterization of the rate of thermally-induced
 aggregation of β-lactoglobulin and its trehalose mixtures in the glass state. Biomacromolecules 11,
 2985-2992.
- Pikal, M.J., Rambhatla, S., Ramot, R., 2002. The impact of the freezing stage in lyophilization: Effects of the
 ice nucleation temperature on process design and product quality. Am. Pharm. Rev. 5, 48-53.
- Pisano, R., 2019. Alternative methods of controlling nucleation in freeze drying, in Ward, K., Matejtschuk, P.
 (Eds.), Lyophilization of Pharmaceuticals and Biologicals. Methods in Pharmacology and Toxicology.
 Humana Press, New York.
- 521 Privalov, P.L., 1990. Cold denaturation of proteins. Crit. Rev. Biochem. Mol. Biol. 25, 281-305.
- Rambhatla, S., Ramot, R., Bhugra, C., Pikal, M.J., 2004. Heat and mass transfer scale-up issues during
 freeze drying, Part 2: Control and characterization of the degree of supercooling. AAPS
 PharmSciTech 5, e58.

- Rey, L., May, J.C., 2010. Freeze drying/lyophilization of pharmaceutical and biological products, 3rd edition.
 Informa Healthcare, London, UK, pp. 1-564.
- Searles, J., Carpenter, J., Randolph, T., 2001. The ice nucleation temperature determines the primary drying
 rate of lyophilization for samples frozen on a temperature-controlled shelf. J. Pharm. Sci. 90, 860-871.
- 529 Shire, S.J., Shahrokh, Z., Liu, J., 2004. Challenges in the development of high protein concentration 530 formulations. J. Pharm. Sci. 93, 1390-1402.
- Singh, S.N., Kumar, S., Bondar, V., Wang, N., Forcino, R., Colandene, J., Nesta, D., 2018. Unexplored
 benefits of controlled ice nucleation: Lyophilization of a highly concentrated monoclonal antibody
 solution. Int. J. Pharm. 552, 171-179.
- Strambini, G.B., Gabellieri, E., 1996. Proteins in frozen solutions: Evidence of ice-induced partial unfolding.
 Biophys. J. 70, 971-976.
- Swärd-Nilsson, A.M., Persson, P.O., Johnson, U., Lethagen, S., 2006. Factors influencing factor VIII activity
 in frozen plasma. Vox Sang. 90, 33–39.
- Takahashi H, Hanano M, Tatewaki W, Shibata A., 1986. Factor VIII lability, protein C and other vitamin Kdependent proteins. Thromb Res. 43(5), 561-8.
- 540 Umbach, M. Freeze Drying Plant. Patent EP 3093597 B1, December 27, 2017.
- Vollrath, I., Friess, W., Freitag, A., Hawe, A., Winter, G., 2018. Does controlled nucleation impact the
 properties and stability of lyophilized monoclonal antibody formulations? Eur. J. Pharm. Biopharm.
 129, 134-144.
- 544 Vollrath, I., Friess, W., Freitag, A., Hawe, A., Winter, G., 2019. Comparison of ice fog methods and 545 monitoring of controlled nucleation success after freeze-drying. Int. J. Pharm. 558, 18-28.
- 546 Wang, W., Roberts, C.J., 2013. Non-Arrhenius protein aggregation. AAPS J. 15, 840-851.
- Wang, B., Tchessalov, S., Cicerone, M.T., Warne, N.W., Pikal, M.J. 2009. Impact of sucrose level on storage
 stability of proteins in freeze-dried solids: II. Correlation of aggregation rate with protein structure and
 molecular mobility. J Pharm Sci. 98, 3145-3166.
- 550 Ward, K., Matejtschuk, P., 2019. Lyophilization of pharmaceuticals and biological: New technologies and 551 approaches. Methods in Pharmacology and Toxicology. Humana Press, New York, pp. 1-382.

553 LIST OF FIGURES

554

Figure 1: Representative profiles of fluid temperature and chamber pressure during application of the VISF protocol. The sample is first equilibrated at T_n , and nucleation is then induced by lowering the pressure to a formulation-specific value. A second holding stage at T_m is subsequently performed to promote the growth of large ice crystals.

559

Figure 2: Temperature and pressure profiles during a) the spontaneous run and b) the VISF run for the plasma batch. Black line: fluid temperature, Red line: Product temperature, Green line: capacitance manometer, Blue line: Pirani manometer. In panel a, an enlargement of the product temperature during freezing is shown in the inset.

564

Figure 3: SEM images of the samples obtained after spontaneous (top) and controlled (bottom) nucleation.
The magnification is the same for all images, and the white bar in the figure corresponds to a distance of 100
µm.

568

Figure 4: (a) FVIII potency (IU/ml) measured relative to the WHO 6th IS FVIII/VWF Plasma (07/316) after 6 months storage at different accelerated degradation temperatures, for samples freeze dried with spontaneous (open circles) or controlled VISF (filled circles) nucleation. (b) Percentage (%) loss in FVIII potency post freeze-dried samples (i.e. relative to pre-freeze-drying liquid samples) with spontaneous (open circles) or controlled (filled circles) nucleation, after 6 months storage at different accelerated degradation temperatures. The error bars displayed in the figure correspond to standard deviation.

575

Figure 5: Arrhenius plot (logarithm of rate lnk vs. inverse of temperature 1/T) for FVIII degradation observed during storage after spontaneous nucleation (blue) and vacuum induced surface freezing (red). The experimental points, represented as blue squares or red triangles, have been fitted with a line. The equation and R² value of the fitting are also displayed on the graph.

580

581

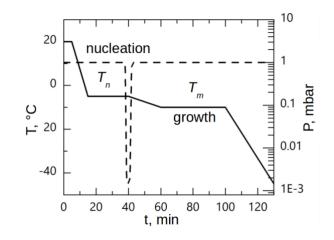


Figure 1

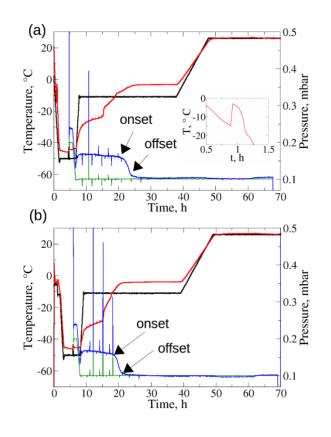
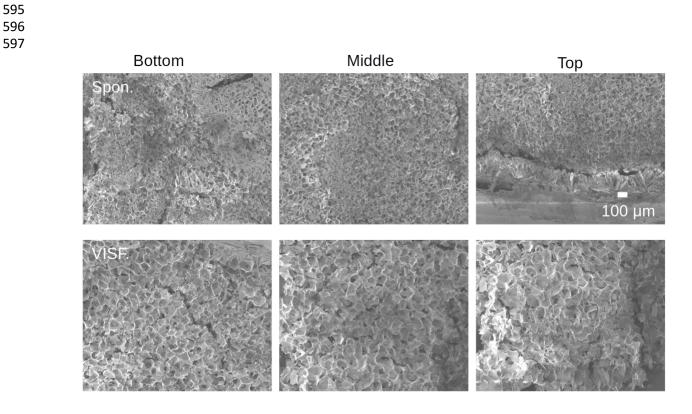
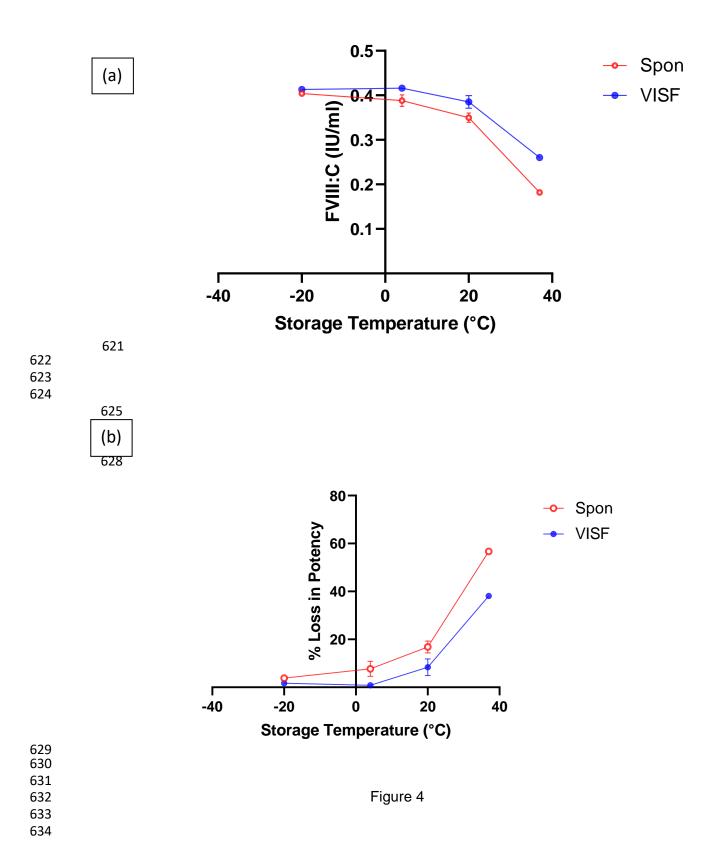


Figure 2







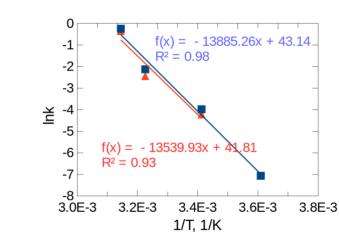


Figure 5