



# University of Groningen

# A Systematic Study on the Utilization of Inorganic Salts as Catalyst for the Conversion of Xylose to Furfural

Soetedjo, Jenny N.M.; Rasrendra, Carolus B.; Heeres, Hero J.

DOI: 10.1088/1757-899X/742/1/012049

IMPORTANT NOTE: You are advised to consult the publisher's version (publisher's PDF) if you wish to cite from it. Please check the document version below.

Document Version Publisher's PDF, also known as Version of record

Publication date: 2020

Link to publication in University of Groningen/UMCG research database

Citation for published version (APA): Soetedjo, J. N. M., Rasrendra, C. B., & Heeres, H. J. (2020). A Systematic Study on the Utilization of Inorganic Salts as Catalyst for the Conversion of Xylose to Furfural. Paper presented at 2019 International Conference on Chemical Engineering, ICCE 2019, Bandung, Indonesia. https://doi.org/10.1088/1757-899X/742/1/012049

#### Copyright

Other than for strictly personal use, it is not permitted to download or to forward/distribute the text or part of it without the consent of the author(s) and/or copyright holder(s), unless the work is under an open content license (like Creative Commons).

The publication may also be distributed here under the terms of Article 25fa of the Dutch Copyright Act, indicated by the "Taverne" license. More information can be found on the University of Groningen website: https://www.rug.nl/library/open-access/self-archiving-pure/taverneamendment.

Take-down policy If you believe that this document breaches copyright please contact us providing details, and we will remove access to the work immediately and investigate your claim.

Downloaded from the University of Groningen/UMCG research database (Pure): http://www.rug.nl/research/portal. For technical reasons the number of authors shown on this cover page is limited to 10 maximum.

## PAPER • OPEN ACCESS

# A Systematic Study on the Utilization of Inorganic Salts as Catalyst for the Conversion of Xylose to Furfural

To cite this article: Jenny N M Soetedjo et al 2020 IOP Conf. Ser.: Mater. Sci. Eng. 742 012049

View the article online for updates and enhancements.

# **Recent citations**

 Prediction of Hydroxymethylfurfural Yield in Glucose Conversion through Investigation of Lewis Acid and Organic Solvent Effects Yeonjoon Kim et al



This content was downloaded from IP address 89.205.132.59 on 12/02/2021 at 13:27

# A Systematic Study on the Utilization of Inorganic Salts as Catalyst for the Conversion of Xylose to Furfural

#### Jenny N M Soetedjo<sup>1,2</sup>, Carolus B Rasrendra<sup>3</sup>, Hero J Heeres<sup>2</sup>\*

<sup>1</sup>Department of Chemical Engineering, Parahyangan Catholic University, Ciumbuleuit 94, Bandung 40141, Indonesia

<sup>2</sup>Department of Chemical Engineering, University of Groningen, Nijenborgh 4, 9747 AG Groningen, the Netherlands

<sup>3</sup>Department of Chemical Engineering, Institut Teknologi Bandung, Ganesha 10, Bandung 40132, Indonesia

#### E-mail : h.j.heeres@rug.nl

Abstract. The utilization of biomass-waste such as sugar-bagasse, water-hyacynth and palm-oil-fiber as alternative sources for transportation fuels and platform-chemicals is a very active research field. Furfural(FF) is one-of-the-13top platform-chemicals that may be converted to derivatives such as furfuryl-alcohol, furoic-acid and furan with wide applications in the gasoline, diesel and jet-fuel blending-pool. Many studies have been conducted in the mechanism and the kinetics of FF-formation from xylose since the 1940s to maximize FF-yield and to reduce FF-decomposition to undesiredproducts. Previous studies showed that inorganic-salt gives positive effects on the FFyield but systematic studies are lacking. Based on it, 60salts were screened in the hydrolysis of 0.1M xylose-aqueous-solution (T=180°C,90minutes,batch). The maximum FF-yield was 53mol% using 5mM-Fe<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub>. The highest FF-selectivity was at 84mol% using 5mM-NaCl, though at low xylose-conversion(35 mol%-FFyield). Some transition metal-chloride i.e.FeCl<sub>2</sub>,CuCl<sub>2</sub>,SnCl<sub>2</sub> showed interesting FFyields(48-50%) and selectivity(58-65%) indicating interesting roles of ion Fe<sup>3+</sup> and Cl<sup>-</sup>. Subsequent studies of two salts i.e.  $Fe_2(SO_4)_3$  and  $FeCl_3(5mM)$  in combination with HCl and  $H_2SO_4(0.1M)$  were investigated (0.1M-xylose, T=150°C, 0-270 min). The result shows that salts increase no FF-yields for  $H_2SO_4$  but increase the reaction-rate. In contrast,  $Fe_2(SO_4)_3$  increase no yield nor reaction-rate for HCl-catalyzed-system. In conclusion, the inorganic-salts catalyse xylose-conversion to furfural but best results were obtained using HCl without additional salts.

### 1. Introduction

Indonesia is the largest palm oil producer in the world with the production up to 41.5 million MT of palm oil in 2018[CITATION Ind19 \1 1033]. Ironically, the increase of CPO production is followed by the increase of waste generated with annual production of waste up to 129-million-m<sup>3</sup> POME (Palm Oil Mill Effluent) and 46-million-ton EFB (Empty Fruit Bunches). Although limited amount of EFB is used as organic fertilizer, most of it is still wasted and becomes one of the major environmental problems in palm oil industry.

EFB, containing 37.3 - 46.5% cellulose and 25.3 - 33.8% hemicelluloses, is actually an excellent source of lignocellulosic biomass which is rich of C6 and C5 sugars that can be converted further into

Content from this work may be used under the terms of the Creative Commons Attribution 3.0 licence. Any further distribution of this work must maintain attribution to the author(s) and the title of the work, journal citation and DOI. Published under licence by IOP Publishing Ltd

high-value-chemicals such as levulinic acid (LA) and furfural (FF)[CITATION Sud13 \l 1033 ]. In 2016, NREL (National Renewable Energy Laboratory) of U.S. Department of energy listed FF in the top 12 emerging near-term deployment potential biobased platform chemicals[ CITATION Bid16 \l 1033 ]. In fact, the high need of furfural in Indonesia is reflected by its import data of 525,3 tonnes or up to 1,7 million US dollar in 2018[ CITATION Bir \l 1033 ].

Furfural or 2-furaldehyde (**FF**) is an important non-petroleum based chemical building block used for the productions of amongst others furfuryl alcohol, furoic acid and furans that can be extended into wide range of products such as pharmaceuticals, cosmetics, resins, cleaning agent, extracting agent, solvent, vulcanizing agents, flavoring agents, pesticides, antiseptics and disinfectants[ CITATION Döb32 \l 1033 \m Cor07 \m Sai82 \m Zei00 \m Bro48 \m HEH12 \m Yan14]. Among its wide application, the current finding of application for furfural as a feedstock to make gasoline, diesel and jet fuel has attracted so much attention[ CITATION Yan14 \l 1033 ].

Furfural for the first time isolated in 1821 [ CITATION Döb32 \l 1033 ] and later produced commercially since the 1920s[ CITATION HEH12 \l 1033 \m Bro48]. It is formed by the hydrolysis of hemicellulose into pentose (C5) sugars before further dehydration in **FF**. Studies have been conducted on several acids i.e. sulfuric, hydrochloric, phosphoric, and nitric acids but sulfuric acid is still the one commercially used in the industry[ CITATION Sin14 \l 1033 ]. In fact, a number of process concepts have been implied commercially (Quacker, Agrifurane, Rosenlew, Escher Wyss) but it still has relatively limited **FF** yields (about 50% range) so far [ CITATION HEH12 \l 1033 ]. The main reason is the involvement of decomposition reactions including fragmentation, resinification and condensation reactions from both pentoses and **FF** that form soluble side products such as formic acid, acetic acid together with insoluble solid product known as humin [ CITATION Yan14 \l 1033 ]. The formation of humin decreases **FF** yield and causes operational issues due to the blockage and decline of heat transfer rates as well as the irreversible deposit on the solid catalyst that leads to catalyst deactivation.

Several efforts have been applied to improve **FF** yield by the use of biphasic liquid-liquid systems<sup>19,22,24,25</sup>, ionic liquids<sup>26-30</sup> and organic solvents<sup>17,31-35</sup> instead of water and the addition of salts to the reaction mixture<sup>18,21,23</sup>. The addition of inorganic salts have been proven to affect the chemoselectivity of the reaction. Rasrendra *et al.* has clearly shown that the chemo-selectivity is a clear function of the type of inorganic salt. Using 0.1 M glucose in water at 140°C and 5mM salt, it was shown that Al(III) has driven the yield selection into lactic acid while Zn(II) into 5-HMF (5-Hydroxymethylfurfural)[ CITATION CBR10 \l 1057 ]. In another study, Rasrendra *et al.* showed that AlCl<sub>3</sub>, Cr and Sn salts has the ability to provoke the isomerisation of d-glucose to d-fructose that increases the chemo-selectivity for the reaction of d-glucose to HMF in DMSO solution[ CITATION CBR12 \l 1057 ].

In fact several studies on salt effect have been conducted for xylose and xylotriose. The effect of chloride salts from several kation groups on xylose and xylotriose was observed by Liu *et al.* and FeCl<sub>3</sub> gave an increase in the rate of reaction both on the formation and decomposition of **FF** [CITATION CLi06 \1057] and strong effect on hemicellulose removal[CITATION LiL09 \1057]. A few years later Marcotullio *et al.* studied the combination of several chloride salts in homogeneous acid catalyzed system using HCl and H<sub>2</sub>SO<sub>4</sub>. The addition of NaCl, KI and CrCl<sub>3</sub> in aqueous systems has been reported in the conversion of xylose to **FF** (see Table 1). The most successful result reported by Marcotullio *et al.* with the **FF** yield of 88 mol% was reported using a mixture of KI and KCl and H<sub>2</sub>SO<sub>4</sub> as the catalyst. The addition of 5 wt% of NaCl together with HCl was also shown a promising result with **FF** yield up to 81 mol%. However the studies were still focusing on the chloride salts on HCl system with only one study using the combination of NaCl and H<sub>2</sub>SO<sub>4</sub> while the commercial use in industry mostly is still using H<sub>2</sub>SO<sub>4</sub> and HCl catalyzed system on the xylose conversion and **FF** yield.

|--|

Entry	$C_{Xylose}$	T (°C), t	Acid	$C_{\text{acid}}$	Salt	$Y_{\text{FF, max}} (\text{mol}\%)$	Ref
1.	35 mM	200, 485 s	$H_2SO_4$	0.05 M	KI-KCl 250-500mM	88	[ CITATI

International Conference on Chemical Engineering UNPAR 2019

**IOP** Publishing

IOP Conf. Series: Materials Science and Engineering 742 (2020) 012049 doi:10.1088/1757-899X/742/1/012049

						ON Mar11 \   1057 ]
2.	35 mM 200, 250 s	HCl	0.05 M	NaCl 5 wt%	81	[ CITATI ON Mar09 \ I 1057 ]
3.	56 mM 145, 300 min	HCl HCl	0.10 M 0.10 M	CrCl <sub>3</sub> 6 mM -	39 29	[ CITATI ON Cho12 \ I 1057 ]

### 2. Experimental Procedures

All chemicals were used as received without further purification. Milli-Q water was used for all reactions and analysis procedures. Xylose (99.5%) was from Sigma-Aldrich, FF (99%) was from Fluka-Aldrich.  $H_2SO_4$  (95-97 wt-%), HCl (37 wt-%), formic acid (98% wt-%) and all salts were purchased from Merck GmbH (Darmstadt, Germany).

The reactions were carried out in glass ampoules with an internal diameter of 3 mm, a wall thickness of 1.5 mm, and a length of 15 cm. The ampoules were filled at room temperature with a solution (0.5 cm<sup>3</sup>) of 0.1M xylose-aqueous-solution with acid catalyst and salt before subsequently sealed with a torch. A series of ampoules was placed in a rack and subsequently positioned in a constant temperature oven ( $\pm$  0.1°C) which was pre-set at the desired reaction temperature. At different reaction times, an ampoule was taken from the oven and directly cooled in an ice-water bath to quench the reaction. The liquid content was then filtered using a PTFE syringe filter (0.45 mm, VWR, the Netherlands). The particle free aliquot was diluted 7-8 times with water prior to analysis.

The composition of the liquid phase after reaction was determined by HPLC using an Agilent 1200 HPLC equipped with a HP 1200 pump, a Bio-Rad organic acid column (Aminex HPX-87H), and an RID or an UV detector. The mobile phase consists of aqueous sulfuric acid (5 mM) at a flow rate of 0.55 cm<sup>3</sup>/min. The column was operated at 60°C. The analysis for a sample was complete in 60 minutes.

The xylose conversion ( $X_{XYL}$ ), FF yield ( $Y_{FF}$ ) and FF selectivity ( $S_{FF}$ ) are mol% based and calculated using equations 1-3:

	$\mathbf{X}_{\mathrm{XYL}}$	=	$\frac{\left(C_{XYL,i}-C_{XYL,i}\right)}{C_{XYL,i}}$
(1)	$\mathbf{Y}_{\mathrm{FF}}$	=	$\frac{C_{FF,t}}{C_{FF,t}}$
(2)			$C_{XYL,1}$

Here,  $C_{XYL,i}$  is the initial xylose concentration (mol/l),  $C_{FF,i}$  the initial FF concentration and  $C_{XYL,t}$  and  $C_{FF,t}$  the xylose and FF concentration at a certain batchtime. For experiments using FF as the feed, the FF conversion (X<sub>FF</sub>) is defined as:

$$X_{FF} = \frac{C_{FF,i} - C}{\frac{(i i FF, t)}{C_{FF,i}}}$$
(3)

### 3. Results and discussion

The studies conducted to observe the effect of anion and cation. The study on the effect of cations on the hydrolysis of xylose is presented in Figure 1 while the study on the effect of anions can be observed in Figure 2.



Figure 1. The effect of cations on the hydrolysis of xylose

From Figure 1, it can be seen directly that the cations give different effect on the hydrolysis of xylose. Interesting results were shown on  $SnCl_2$ , FeCl<sub>3</sub> and CuCl<sub>2</sub> and which successfully convert xylose almost 50% of **FF**. The last two salts together with NaCl were of the highest interest due to their low selectivity to other decomposition products indicating the important role of Fe3<sup>+</sup>, Cu<sup>2+</sup>, Na<sup>+</sup> and Sn<sup>2+</sup> in the hydrolysis reactions involved. In fact, NaCl is of the highest interest due to its limited transformation to other products which is only about 5%.



International Conference on Chemical Engineering UNPAR 2019 IOP Publishing

IOP Conf. Series: Materials Science and Engineering 742 (2020) 012049 doi:10.1088/1757-899X/742/1/012049

Figure 2. The effect of anions on the hydrolysis of xylose

The effect of anions can be observed in Figure 2. The results show that  $Cl^-$  and  $Br^-$  can drive the preference of reactions more to **FF** than to decomposition products. Categorizing the results into the same group of cations (see Figure 3), it shows that almost the same yield of **FF** achieved (26-36 mol-%). It confirms the previous results from Marcotullio which indicates that  $Cl^-$  in solution seems to be the main feature for the kinetics of xylose reaction and the different cations seem to play only a minor role[ CITATION Mar11 \l 1057 ]. The most interesting result is shown again on NaCl which showed the highest selectivity on **FF**.



The highest FF-selectivity was at 84 mol% using 5mM-NaCl, though at low xylose-conversion (35 mol%-FF-yield). The results showed the interesting roles of ion Fe<sup>3+</sup> and Cl<sup>-</sup>. Subsequent studies of two salts Fe<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub> and FeCl<sub>3</sub> (5mM) in combination with HCl and H<sub>2</sub>SO<sub>4</sub> (0.1M) were investigated on 0.1M-xylose, T=150°C, 0-270 min. The result shows that salts increase the reaction-rate but not the FF-yields for H<sub>2</sub>SO<sub>4</sub>. In contrast, Fe<sub>2</sub>(SO<sub>4</sub>)<sub>3</sub> increases no yield nor reaction-rate for HCl.

According to the results gained in this works, there should be different roles in the reactions between the  $Cl^-$  and  $H^+$  or  $Fe^{3+}$ . In fact these results also confirm the acid catalyzed hydrolysis mechanism suggested by Marcotulio as shown in Figure 4.



Figure 4. proposed mechanisme of furfural formation from xylose with 1 Aldo form of sugar, 2 1,2-enediol, 3 keto form of sugar and 4 FF [ CITATION Mar11 \l 1057 ]

H<sub>2</sub>SO4 as the Bronsted acid donates the H<sup>+</sup> in reaction (I) to form 1,2-enediol or **2** and in reaction (III) to form **FF**. In such mechanism the presence of Cl<sup>-</sup> as the Lewis acid of donor of electron favors the formation of the **2**, which can equilibrate with both the aldo **1** and keto **3** form of the sugar, and reacts to form furfural or **4** in presence of an acid. It seems that the speed of reaction in which the Cl<sup>-</sup> involved is higher than the one to the loss reactions and resulted in better performance in term of **FF** yield. It may also explain the reason that chloride salt performed better than hydrochloric acid since HCl releases the H<sup>+</sup> which accelerate not only the formation of **2** but also the loss reactions. However in high concentration of chloride salt, there will be high concentration of **2** that may give a driving force to the increase of loss reactions and may give an adversed effect on the yield of **FF**. In fact, the presence of strong acid is needed to favor the selectivity of **FF**[ **CITATION Mar11** \l **1057** ]. As for the effect of Fe<sup>2+</sup> there is no data available to explain its role in the proposed mechanism. However considering the acidic character of Fe<sup>2+</sup> and Na<sup>2+</sup> in the stabilization of intermediate products was proposed but still need verification and further investigastion[ CITATION Mar11 \l 1057 ].

#### 4. Conclusions

The addition of salts has been proven to affect the mechanism in the hydrolysis of xylose to **FF**. The involvement of  $Cl^-$  increase the yield of FF most probably by its catalysis role in the formation of 1,2-enediol while the involvement of  $Fe^{2+}$  may be assumed to follow the function of H<sup>+</sup>. Another interesting salt is NaCl that can increase the selectivity to FF up to 84mol%. Further investigation and verification is still need to be conducted to understand the role of kation and anion in salts in the mechanism of hydrolysis xylose to **FF** and **FF** decomposition.

#### Acknowledgement

This research was funded by RISTEKDIKTI and Parahyangan Catholic University and supported by University of Groningen. Authors wishes to acknowledge assistance or encouragement from

colleagues, special work by technical staff from University of Groningen and Parahyangan Catholic University.

#### References

- [1] IndexMundi 2019 [Online]. Available: www.indexmundi.com. [Accessed 20 December 2019].
- [2] Sudiyani Y, Styarini D, Triwahyuni E, Sudiyarmanto, Sembiring K C, Aristiawana Y, Abimanyu H and Han M H 2013 *Energy Procedia* **32** 31-8
- [3] Biddy M J, Scarlata C and Kinchin C 2016 *National Renewable Energy Laboratory*, Denver, Colorado, U.S.A.,.
- [4] BPS 2018 Buletin Statistik Perdagangan Luar Negeri Impor or Foreign Trade Statistical Buletin Import p 35
- [5] Döbereiner 1832 Annalen der Pharmacie 3 (2) 141-146
- [6] Corma A, Iborra S and Velty A 2007 Chemical Reviews 107 (6) 2411-2502
- Sain B, Chaudhuri A, Borgohain J N, Baruah B P and Ghose J L 1982 J. Sci. Ind. Res. 41 (7) 431-438
- [8] Zeitsch K J 2000 *The Chemistry and Technology of Furfural and Its Many By-Products* vol. 13, ed 1 (Koln: Elsevier)
- [9] Brownlee H J and Miner C S 1948 Industrial And Engineering Chemistry 40 (2) 201-204
- [10] Hoydonckx H E, Rhijn W M, Vos D E D and Jacobs P A 2012 Furfural and Derivatives Ullmann's Encyclopedia of Industrial Chemistry (Weinheim: Wiley VCH Verlag GmbH & Co. KGaA) pp 285-313.
- [11] Yan K, Wu G, Lafleur T and Jarvis C 2014 Renewable Sustainable Energy Rev 38 663-676
- [12] Singh R, Shukla A, Tiwari S and Srivastava M 2014 Renewable and Sustainable Energy Rev, 32 713-728
- [13] Rasrendra C B, Makertihartha I G B N, Adisasmito S and Heeres H J 2010 Topics in Catalysis 53 1241–1247
- [14] Rasrendra C B, Soetedjo J N M, Makertihartha I G B N, Adisasmito S and Heeres H J 2012 Topics in Catalysis 55 543–549
- [15] Liu C and Wyman C E 2006 Carbohydr. Res. 341 2550–2556
- [16] Liu L, Sun J, Cai C, Wang S, Pei H and Zhang J 2009 Bioresource Technology 100 5865–5871
- [17] Marcotullio G and de Jong W 2011 Carbohydrate Research 346 1291-1293
- [18] Marcotullio G, Cardoso M A T, de Jong W and Verkooijen H M 2009 International Journal of Chemical Reactor Engineering 7 A67
- [19] Choudhary V, Sandler S I and Vlachos D G 2012 ACS Catalysis 2 (9) 2022-2028