



Research paper

An innovative window heat recovery (WHR) system with heat pipe technology: Analytical, CFD, experimental analysis and building retrofit performance

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ARTICLE INFO

Article history:

Received 29 October 2021
Received in revised form 13 December 2021
Accepted 10 February 2022
Available online xxxx

Keywords:

Building ventilation
Heat recovery
Window heat recovery
Heat pipe
Energy performance
Thermal comfort

ABSTRACT

This paper addresses the numerical and experimental performance analysis of a windows heat recovery system made of heat pipes. For modelling, the heat pipe is considered as a pseudo solid material with high value of effective thermal conductivity. An experimental investigation using a window heat recovery prototype was carried out to predict the value of effective thermal conductivity of the heat pipes and to validate the numerical model. After validation, a parametric analysis was conducted to investigate the performance of the recovery system for different working conditions (mass flow rate and temperature difference between exhausted and supplied air). Based on the performance obtained in the parametric analysis, energy performance in building and the impact on velocity and pressure distributions are also evaluated with the support of CFD analysis. It is found that the effectiveness of window heat recovery made of heat pipes depends on ventilation rate and temperature difference between exhausted and supplied air. Increasing ventilation rates and temperature differences decrease the effectiveness. For ventilation rate between 10–60 m³/h and temperature difference 10–30 °C, effectiveness between 65%–95% and pressure drop 4–80 Pa are obtained. For performance in building, the power consumption can be reduced between 3%–24% and the thermal comfort increased.

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1. Introduction

Energy consumption in buildings is responsible for around 40% of the total energy demand in the EU (Ekins and Lees, 2008). Building heating, cooling and ventilation represents between 40%–60% of the total consumption (Zender-świercz, 2021), where ventilation itself is between 20%–30% (National Institute for Health and Welfare, 2013). Several studies indicated that building ventilation will significantly affect occupants' health (Cao and Ren, 2018; Yuan et al., 2018), indoor air quality (Lim et al., 2021; González Couret et al., 2013), heating/cooling demand (Tien et al., 2021; Zuazua-Ros et al., 2019) and energy consumption (Young et al., 2020; Bang et al., 2019).

Occupants spend about 90% of their time on indoor activities (Li and Wang, 2020), where indoor air quality is generally poorer than outdoor air quality with 2–5 times higher indoor airborne pollutants than the outside (Pitarma et al., 2017). Research

also indicates sick building syndromes (e.g., pruritus, dry cough, ocular pruritus, and headache) are attributed to poor indoor air quality, as well as diseases like extrinsic allergic alveolitis and asthma (Capristo et al., 2004).

Several studies have investigated the impact of ventilation on indoor air temperature. Three categories of key parameters (Zhang et al., 2021) will affect the ventilation efficiency, including external weather conditions, building materials and occupants' behaviours of ventilation control (day/night ventilation), ventilation rate and indoor air temperature settings. As many studies confirmed (Guerra Santin et al., 2009; Biesiot and Noorman, 1999; Fabi et al., 2012; Cho et al., 2021), the occupants' behaviour and indoor air quality are interactively influenced by each other according to the efficiency of ventilation systems.

Natural ventilation by opening windows is the most common in residential and commercial buildings, with approximately 35% additional primary energy consumption (Paone and Bacher, 2018). Many building occupants sealed their windows for security reasons, which causes virus dispersion, poor indoor air quality, damp and moulds, which cause damage to building fabric (Wood and Salib, 2013). However, to improve the indoor air quality, window opening for fresh air in the winter season caused a problem that room temperature decreases rapidly by an intake of

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Nomenclature

A_f	Heat transfer area of a single fin (m^2)
A_p	Cross section area of the heat pipe tube (m^2)
A_C	Heat transfer area of cold side (m^2)
A_H	Heat transfer area of hot side (m^2)
C_p	Specific heat capacity ($\text{J kg}^{-1} \text{K}^{-1}$)
D_f	Diameter of fins (m)
D_p	Diameter of heat pipes (m)
d_{btf}	Distance between fins (m)
F	Calibration factor (-)
f_{th}	Thickness of the fins (m)
h	Convective heat transfer coefficient ($\text{W m}^{-2} \text{K}^{-1}$)
k	Thermal conductivity ($\text{W m}^{-1} \text{K}^{-1}$)
L	Length (m)
\dot{m}	Mass flow rate (kg s^{-1})
N_f	Number of fins (-)
N_p	Number of layers of heat pipes (-)
N_S	Number of heat pipes connected in serial (-)
$\overline{\text{Nu}}$	Average Nusselt number
Pr	Prandtl number (-)
Q	Heat flow through heat pipe (W)
R	Thermal resistance (K W^{-1})
Re	Reynolds number (-)
S	Nondimensional distance between fins (m)
T	Temperature (K)
V	Air velocity (m s^{-1})
V_r	Volumetric air flow rate ($\text{m}^3 \text{h}^{-1}$)
W	Nondimensional diameter of the fins (m)
ΔP	Pressure drop

Greek symbols

ε	Effectiveness (-)
μ	Dynamic viscosity of air (Pa s)
ρ	Density of air (kg m^{-3})

Subscripts

a	Air
A	Adiabatic side of the heat pipe
av	Average values
C	Cold side of the heat pipe
eff	Effective value
f	Fins
H	Hot side of the heat pipe
in	Inlet
out	Outlet
T	Total
1,2,3,4	Locations in mesh

cold outdoor air into the building, thereby consuming additional energy for operating heating system additionally to increase the reduced room temperature (Simonson, 2005). However, natural ventilation could still be considered an efficient and effective approach with versatile requirements than particular building types (Government, 2010). Rasheed et al. (2017) investigated

the unreliability of natural ventilation system operation and the indoor air quality, thus natural ventilation in majority of buildings is insufficient to improve the indoor air quality due to these limitations. Hence, Belmans et al. (2019) found that the 'mixed-mode or 'hybrid' approach could serve as efficient options for building ventilation.

In recent decades, mechanical ventilation systems have been increasingly used to meet ventilation requirements and dilute indoor-generated pollutants. Numerous studies (Kang et al., 2021; Tian et al., 2020; Yassine et al., 2012) have examined the effects of residential mechanical ventilation systems on IAQ, thermal comfort, and/or energy use. Mechanical ventilation systems with heat recovery (MVHR) have become more popular as an energy-efficient solution to provide good IAQ during the heating season (Clarke, 2019). However, mechanical ventilation systems are typically in operation throughout the whole year resulting in high energy consumption for operating the fan (Babota, 2014). Moreover, due to the lack of financial resources to purchase and install the MVHR system, especially in existing houses, homeowners or landlords are rarely considering this system (Krieger and Higgins, 2002). Therefore, considering the above-mentioned limitations, it is imperative to develop an energy-efficient, compact, non-instructive and easy-installed heat recovery ventilation system for building retrofit.

Heat recovery technologies can be classified using different criteria (Mardiana-Idayu and Riffat, 2012; Cuce and Riffat, 2015). For example, Mardiana-Idayu and Riffat (2012) presented a review of heat recovery technologies for building applications, where the different types are divided according to the construction type of the heat exchanger. According to them, they can be classified in fixed-plate (Shen et al., 2017; Nasif et al., 2010), rotary wheel (Calautit et al., 2020; Nóbrega and Brum, 2009), run-around (Vali et al., 2009; Wang, 1985) and heat pipes (Yau and Ahmadzadehtalatapeh, 2010; Gedik et al., 2016). Fixed plates are the most used and can achieve high values of efficiency, and the rotary wheel can recover both sensible and latent heat, while the run-around has the advantage of recovering heat from different parts of the building (Mardiana-Idayu and Riffat, 2012). Heat pipe types have some advantages concerning conventional technologies, such as being suitable for natural ventilation due to their low resistance to airflow, ability to work at the low-temperature difference, and high heat transfer rate in a small cross-section area (Mardiana-Idayu and Riffat, 2012; Shao et al., 1998). Shao et al. (1998) presented and conducted the experimental investigation of a low-pressure drop heat recovery device made of heat pipes. They studied the effect of different techniques to increase the heat transfer while not increasing the flow resistance. They found recovery efficiency around 60% and that using wire fins presents the best balance between good thermal performance and low flow resistance.

Table 1 shows the literature review of ventilation heat recovery technology application in building retrofit. Most of the research focused on the apartment block building types in cold climate countries, with heat recovery effectiveness varied between 75%–90%. Research also indicated that applying expensive cross or counter flow enthalpy heat exchangers could achieve relatively high energy reduction rates of 23.6%–25% compared with the building baseline. However, the cheaper thermal rotary wheel has a 12%–20% lower energy reduction rate due to lower heat recovery effectiveness between 75% and 85%. Moreover, these researches were limited in the assessment of the thermal comfort improvement when integrating heat recovery ventilation systems in the building retrofit packages. Furthermore, these researches also showed a gap in the heat pipe–heat recovery integrated building ventilation modelling and analysis.

This work proposed, modelled, and conducted a performance analysis of a window heat recovery system. The developed model

Table 1
A literature review of ventilation heat recovery technology application in building retrofit.

Ref.	Building type	Location	Ventilation type	Heat recovery type	Heat recovery effectiveness	Energy reduction rate	Thermal comfort improvement
Chen et al. (2020)	Apartment block	Norway	Mechanical ventilation heat recovery (MVHR)	Flat-plate	86%	20.5%	N/A
Dodoo (2020)	Apartment block	Sweden	Heat recovery air handling units (AHUs)	Rotary wheel	85%	18.1%	N/A
Hall et al. (2013)	Semi-detached house	UK	Mechanical ventilation heat recovery (MVHR)	Crossflow enthalpy exchangers	90%	23.6%	✓
de Oliveira Fernandes et al. (2021)	Terraced house	Netherland	Balanced ventilation system	Counterflow enthalpy exchangers	88%	25%	N/A
Wang et al. (2016)	Multi-family house	Sweden	Decentralised exhaust ventilation with heat recovery	Rotary wheel	80%	12%	✓
Carlsson et al. (2019)	Apartment block	Canada	Decentralised ventilation with heat recovery ventilators (HRVs)	Rotary wheel	75%	15%	N/A
Smith and Svendsen (2016)	Apartment block	Denmark	Decentralised ventilation with heat recovery ventilators (HRVs)	Rotary wheel	85%	15%–20%	✓
Wallin and Claesson (2014)	Apartment block	Sweden	Heat recovery air handling unit (AHU)	Heat pump hot exhaust counterflow heat exchanger	90%	24%	N/A

is validated against experiments, and a correlation for effective thermal conductivity is proposed. The recovery unit is based on heat pipes and presents high efficiency due to the effective heat transfer in a small cross-section of heat pipes, and it has a lower pressure drop than conventional technologies, which makes this technology suitable for natural ventilation and requirement of less power for fans for application of higher ventilation rate. In addition, the system has no complex structures, which means it is easy to build and install in the building.

2. Methodology

This paper proposed an innovative heat pipe-based window heat recovery system as an affordable, fast-installed and non-instructive building retrofit technology to curtail heat loss caused by ventilation and improve indoor air temperature, velocity distributions, and improve thermal comfort and indoor air quality.

Fig. 1 presents the methodology flowchart used for validation and performance analysis among the analytical model, CFD simulation and the experimental results for the window heat recovery (WHR) system, where the system is described in Section 2.1 with the analytical model and CFD simulation established in Section 2.2. A 1940s' semi-detached two-bedroom house is selected as the case study to investigate the impact of the WHR system application on building energy performance and thermal comfort, with details in Section 2.3. The experiments were conducted to determine the effective thermal conductivity of the heat pipes, as described in Section 3.1. In Section 3.2, the tested heat recovery effectiveness of the WHR system was compared and validated with the analytical and CFD model simulation results. Afterwards, the parametric analysis was conducted with investigating the impacts of ventilation rate, the maximum temperature of inlet and outlet sides in parallel with the different heat pipe layers on the WHR system performances, with details discussed in Section 4.1. In addition, the building energy performances were also investigated in IES VE building simulation software, considering the impacts and relations of building monthly heating demand, different ventilation rates, space heating demand reduction rate and fan power on the WHR system, as analysed in Section 4.2. Furthermore, the vertical and horizontal air temperature and

velocity differences were investigated in CFD simulation, as depicted in Section 4.3, to analyse indoor air temperature, velocity parameters distribution with the air velocity disturbance conditions. Moreover, the impact of versatile WHR ventilation rates on indoor thermal comfort was discussed in Section 4.3.

2.1. Window heat recovery system

Window heat recovery systems are heat exchangers coupled to building windows frame that enable to exchange heat between exhausted and supplied air during the building ventilation. This is accomplished by centrifugal fan with 6-level adjustable air speeds varied from 10 m³/h to 60 m³/h. One being installed at the supply air side and another at the exhaust air outlet (Zender-Świercz, 2021; Mardiana-Idayu and Riffat, 2012; Cuce and Riffat, 2015). An example of integrating the window heat recovery system in the building is presented in Fig. 2. Heat pipes have two main parts, the cold side (condenser) and the hot side (evaporator), where heat is transferred from evaporator to condenser (Cuce and Riffat, 2015). One centrifugal fan is installed on the supply air side and another at the exhaust air outlet. The window heat recovery system works in all four seasons, for example, in winter, its purpose is to recover heat from exhausted air to the supplied fresh air, and in summer, the exhausted air cools the supplied air.

2.2. Numerical modelling

In this study, a window heat recovery system made of two layers ($N_p = 2$), each one containing three heat pipes connected in serial ($N_s = 3$) is considered as reference configuration (Fig. 2). Heat pipes can be defined as passive thermal devices designed to provide effective transport of thermal energy. Nevertheless, modelling the physical phenomena that occur in heat pipes is complex. Nevertheless, the focus of this work is the development of a numerical model able to predict with appropriate accuracy the global performance of window heat recovery systems made of heat pipes. Therefore, for modelling purposes, it is reasonable to consider the heat pipe as a pseudo solid material with a high effective value of thermal conductivity (Stark et al., 2016).

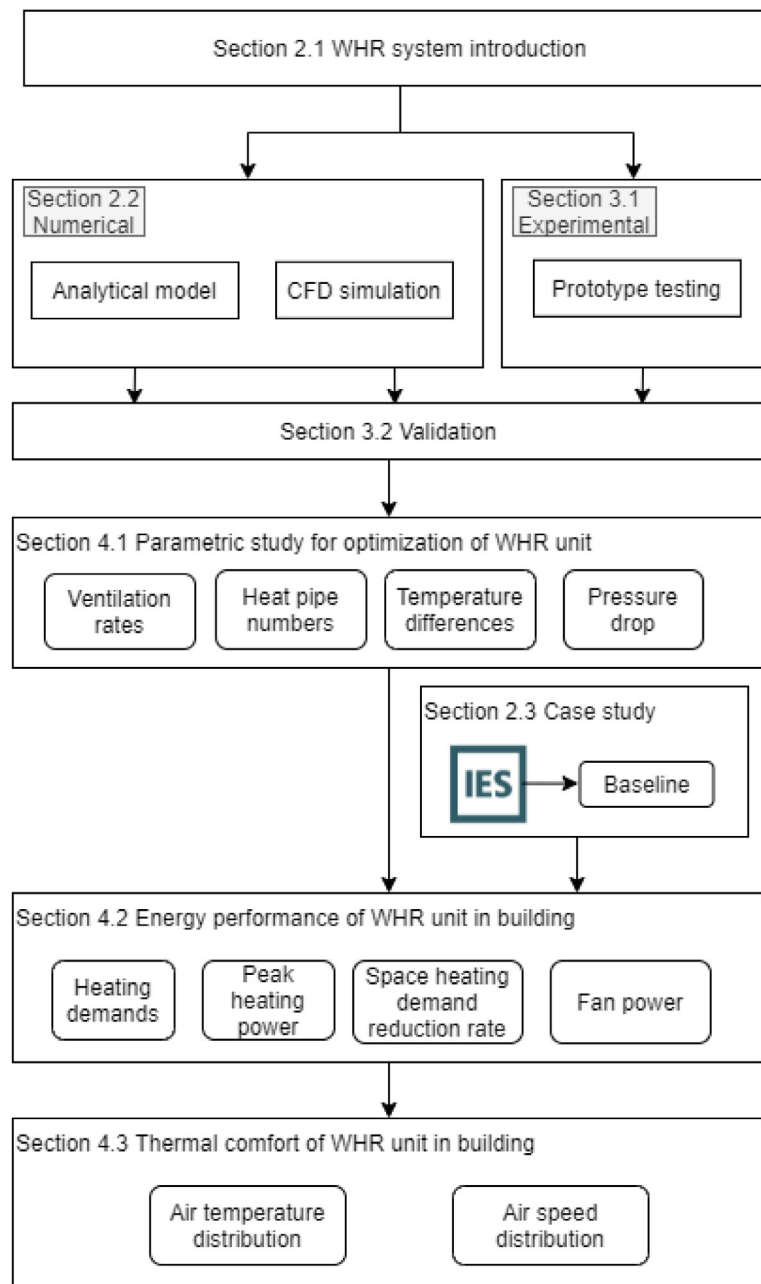


Fig. 1. The research methodology flowchart.

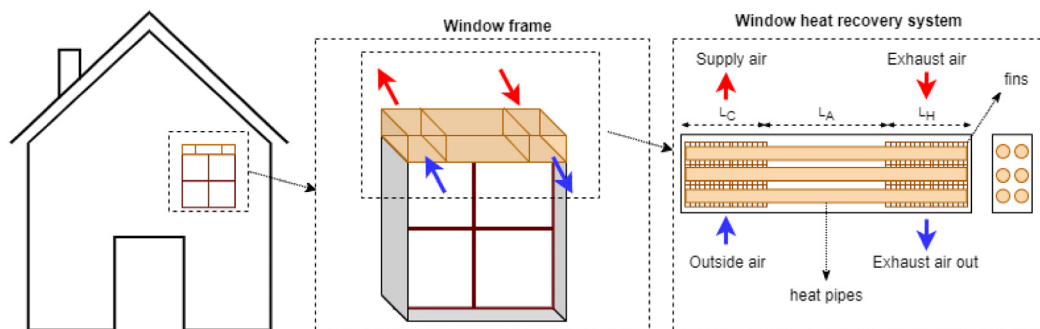


Fig. 2. Window heat recovery system integrated with building (Winter example).

Circular fins are used to improve heat transfer on the hot and cold sides of the heat recovery system. Fig. 3 presents the total

thermal resistance network for a single layer of three heat pipes and the thermal resistances for a single heat pipe.

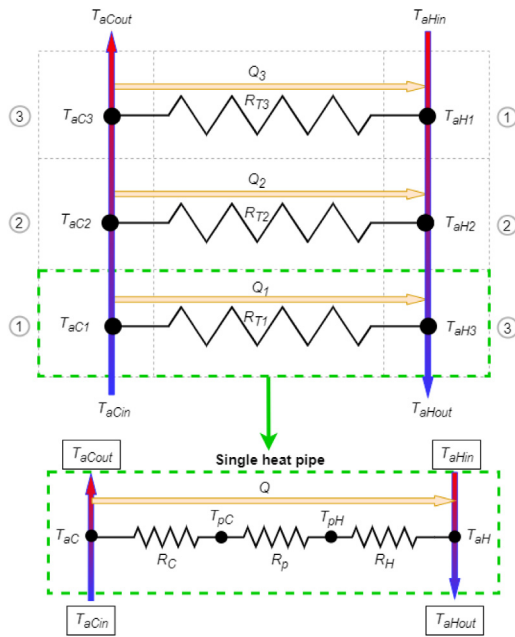


Fig. 3. Thermal resistance network between heat pipes and air in cold and hot sides.

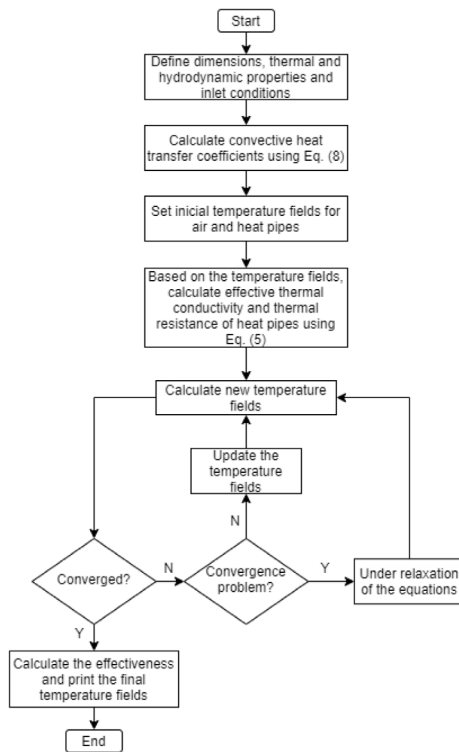


Fig. 4. The flowchart of the solution method.

In this approach, the window heat recovery system can be modelled as a counter flow heat exchanger. It is assumed that air flowing through the system is divided into equal parts for the number of layers of heat pipes without thermal losses at steady-state conditions. Then, Eqs. (1)–(2) can be used to describe a single heat pipe:

$$Q = \frac{T_{pC} - T_{aC}}{R_C} = \frac{T_{pH} - T_{pC}}{R_p} = \frac{T_{aH} - T_{pH}}{R_H} = \frac{T_{aH} - T_{aC}}{R_T} \quad (1)$$

$$Q = \dot{m}_C C_p (T_{aCout} - T_{aCin}) = \dot{m}_H C_p (T_{aHin} - T_{aHout}) \quad (2)$$

where Q is the heat flow through the heat pipe from hot to the cold side, T_{pC} and T_{pH} are the mean temperature of heat pipes in the cold and hot side, T_{aC} and T_{aH} are the mean air temperature on the cold and hot side, R_C and R_H are the thermal resistance (convective), R_p is the conductance thermal resistance of heat pipe, \dot{m}_C and \dot{m}_H are the air mass flow rate, C_p is the specific heat capacity of air, and T_{aCout} , T_{aCin} , T_{aHout} and T_{aHin} are, respectively, inlet and outlet temperature of the air in cold and hot sides. The total thermal resistance R_T , convective and conductance thermal resistances are calculated using:

$$R_T = R_C + R_p + R_H \quad (3)$$

$$R_C = \frac{1}{hA_C} \quad (4)$$

$$R_p = \frac{L_{eff}}{A_p k_{eff}} \quad (5)$$

$$R_H = \frac{1}{hA_H} \quad (6)$$

where h is the convective heat transfer coefficient on the cold and hot side (it is considered the same value for both sides), A_C and A_H are total heat transfer areas, which depend on the number of fins N_f in each side, the distance between fins d_{bif} , diameter D_f and thickness f_{th} (it is considered both sides with the same number of fins). The parameters L_{eff} and k_{eff} are the effective length and thermal conductivity of heat pipe, respectively, and A_p is the cross-section area of the heat pipe ($A_p = \pi (D_p/2)^2$). The effective length is calculated using (Zhu et al., 2020):

$$L_{eff} = L_A + \frac{L_C + L_H}{2} \quad (7)$$

in which L_A is the adiabatic length and L_C and L_H are the length of the cold and hot sides, respectively (see Fig. 2). The effective thermal conductivity is estimated according to the experimental work described in Section 3.1.1.

2.2.1. Convective heat transfer coefficient

For convective heat transfer coefficient in cold and hot sides, the following correlation for the average Nusselt number \overline{Nu} from the work of Romero-Méndez et al. (2000) is used with some modifications:

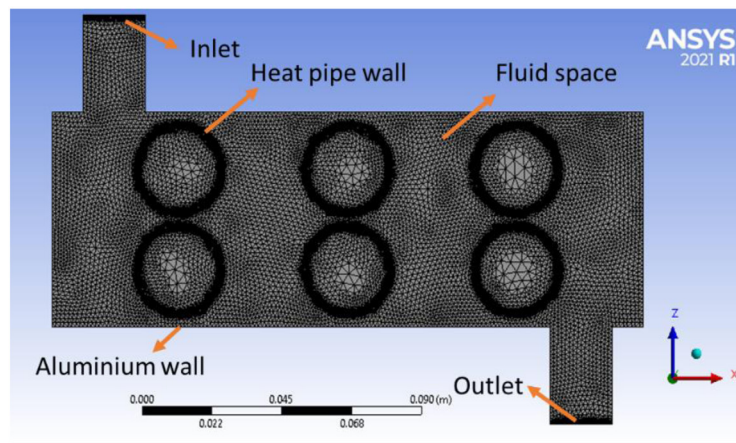
$$\overline{Nu} = \frac{hD_p}{k_a} = FRePr \frac{WS}{A_f/D_p^2 + \pi S} \left[1 - \exp\left(-\frac{1.32 Pr^{4/3} W^{1/2}}{Re^{1/2} S}\right) \right] \quad (8)$$

where k_a is the thermal conductivity of air, F is a calibration factor, Re is the Reynolds number, Pr is the Prandtl number, $W = D_f/D_p$ is the nondimensional diameter of the fins, $S = d_{bif}/D_p$ is the nondimensional distance between fins, A_f is the total surface area of a single fin (the circular and annular surfaces area), where A_f/D_p^2 is the nondimensional fin surface area. The Reynold number is calculated using:

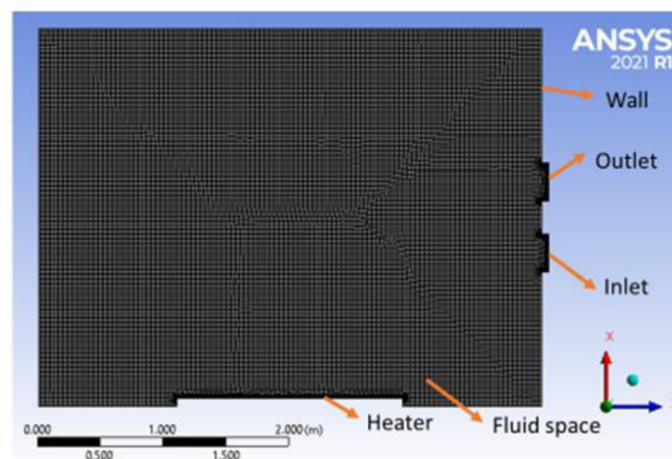
$$Re = \frac{\rho V D_p}{\mu} \quad (9)$$

in which ρ , μ and V are the air density, dynamic viscosity, and velocity, respectively. The velocity of air is obtained from mass flow rate (\dot{m}_C and \dot{m}_H), density, and the total cross-section area of void space between fins.

The correlation from Eq. (8) (excluding the F factor) is originally obtained by analysing (CFD and experimental) a heat pipe with a single pair of rectangular fins (Romero-Méndez et al.,



(a)

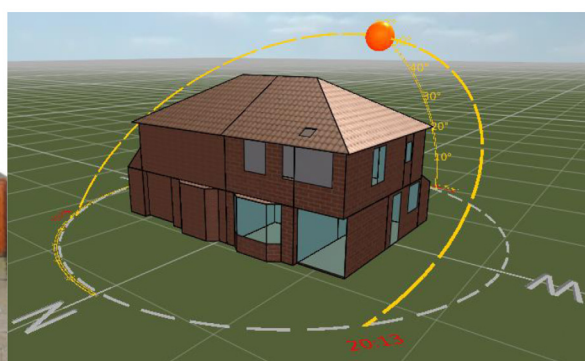


(b)

Fig. 5. (a) Computational mesh of the heat pipes. (b) Computational mesh of the small room.



(a) On-site semi-detached house



(b) Model establishment in IESVE

Fig. 6. Physical model of the semi-detached house (right half building) in Nottingham, UK.

2000). According to Stark and Bergman (2017), this correlation underpredicts the convective heat transfer coefficient. Furthermore, the correlation was obtained considering only a single pair of fins, which significantly decrease its accuracy to predict the Nusselt number when a high number of fins is used. For this reason, a calibration factor F is included in the correlation and

then its values was adjusted in order to minimise difference between numerical and experimental presented in Section 3.1.1.

2.2.2. Solution method, performance and parameters

The equations were solved using GNU Octave software through an iterative process. The procedure is presented in the flow chart of Fig. 4.

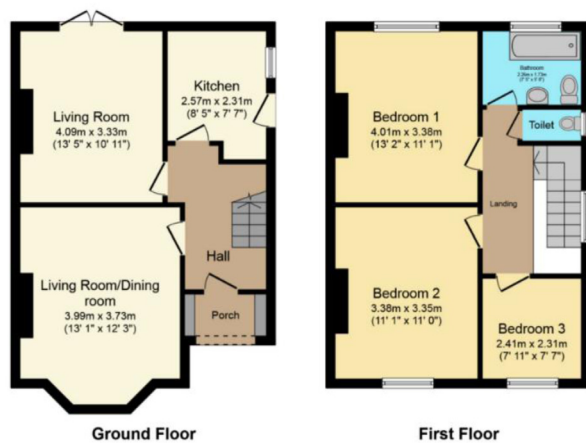


Fig. 7. Building floor plan.

Table 2
Geometric parameters of the window heat recovery system.

Parameter	Value
$L_C = L_H$ (cm)	50
L_A (cm)	10
N_f	134
D_p (cm)	2
D_f (cm)	4
f_{th} (mm)	1.5
d_{bf} (mm)	2.25
N_p	2
N_s	3

For the heat pipes connected in serial (single layer), we have used finite volume method (FVM), in which a single heat pipe is considered as the control volume. For each control volume, Eqs. (1) and (2) are solved to obtain the temperature fields. The connection between different control volumes is made by considering that outlet conditions of one heat pipe are the inlet conditions of the next heat pipe. When the governing equations are solved for each control volume, the effectiveness of the window heat recovery is calculated using the following equation:

$$\varepsilon = \frac{\dot{m}_C C_p (T_{aCout} - T_{aCin})}{\min(\dot{m}_C C_p; \dot{m}_H C_p) (T_{aHin} - T_{aCin})} = \frac{\dot{m}_H C_p (T_{aHin} - T_{aHout})}{\min(\dot{m}_C C_p; \dot{m}_H C_p) (T_{aHin} - T_{aCin})} \quad (10)$$

where $\min(\dot{m}_C C_p; \dot{m}_H C_p)$ is the minimum value between the product's mass flow rate and specific heat capacity of the cold and hot sides. In Eq. (10), the inlet and outlet temperatures are for the first and last heat pipes (see Fig. 3). The geometric parameters of the reference configuration of the window heat recovery used in the simulations are presented in Table 2. The thermal and hydrodynamic properties of air are considered constant for a temperature of 25 °C.

2.2.3. CFD modelling method

The CFD code ANSYS 2021 R1 was used in this study to validate the accuracy of heat pipe effectiveness along with simulating the air and velocity distribution in the small room connected to the heat pipe model. The simulation of the heat pipe and the attached room was considered the steady state with a two-dimensional computational model where the CFD code used the Finite Volume Method (FVM) with the Semi Implicit Method for Pressure Linked Equations (SIMPLE) velocity–pressure coupling algorithm. The turbulent element of the airflow was modelled

using the Realisable $k-\varepsilon$ turbulence model with enhanced wall functions to get further improved prediction for flows involving rotation and boundary layers under strong adverse pressure gradients inside the heat pipe model (Seyyedvalilu, 2021; Andersson et al., 2011; Calautit and Hughes, 2014a). The $k-\varepsilon$ model for turbulence is the most common to simulate the mean flow characteristics for turbulent flow conditions. However, the Realisable $k-\varepsilon$ model differs from the standard $k-\varepsilon$ model in that the ε of the former model is derived from an exact equation for the transport of the mean-square vorticity fluctuation, resulting in improved predictions for the mean flow of complex structures (Calautit and Hughes, 2014a). Moreover, the enhanced wall treatment is a blended wall model or wall function. It blends the separate models in the two-layer approach by using a damping function to make the transition smoother (Brozovsky et al., 2021). Meanwhile, Second-order upwind schemes were adopted for the calculation. Before the simulation process, the under-relaxation factors for pressure, momentum, k and ε were set to 0.2, 0.25, 0.25 and 0.25 for both heat pipe and room models, respectively. Convergence steps were set to 10000, where the convergence was monitored, and iterations were ended when all residuals showed no further declinations with the increasing iterations. The governing equations were fully introduced in the ANSYS FLUENT Guide (ANSYS, 2013). The heat pipe and the exterior wall surfaces are made of copper and aluminium, respectively, assuming that all the surfaces are stationary walls. The boundary condition assumes that the velocity reduces to 0 when reaching the aluminium wall surface with the Intensity and Viscosity Ratio specification method used in the turbulence model. The turbulent intensity and turbulent viscosity ratio remain at 10% during the simulation process.

The geometry of heat pipe and room models was created using the SpaceClaim (FLUENT pre-processor) in the ANSYS 2021 Workbench. According to the configuration of the heat pipe and room models described in Section 2.2, the established geometry was imported into ANSYS mesh processor where the fluid surfaces areas were not extracted from the model since both the conduction and convection models were investigated in this study. The constructed mesh was used to discretise the surface of the computational domains. All triangles method was used for heat pipe model to acquire the best split near heat pipe sections whereas Quadrilateral method for the small room model. The size of mesh elements was improved smoothly to solve those sections with high gradient mesh to require more accurate results of the velocity and temperature fields near the velocity inlet, pressure outlet, and heat pipe walls (Calautit and Hughes, 2014b; Calautit et al., 2014). Furthermore, level 3 refinements were applied in these areas as well. The mesh element size of the heat pipe and room models for surfaces and edges were 10 mm and 5 mm, with the total element number of 348 340 and 330 870, respectively. The modelled meshes of the heat pipe and small room models using ANSYS Mesh are shown in Fig. 5(a) and (b).

2.3. Case study

In this research, a semi-detached 2-bedroom house with a total floor area of 85 m² is selected as the case study to investigate the impact of window heat recovery (WHR) ventilation on the building post-retrofit energy performance and indoor air temperature, velocity distributions. The energy performance is evaluated by the heating demand reduction rate and peak heating power considering ventilation rates varied between 10–60 m³/h for each room, with a physical model established in IES VE building energy simulation software, as depicted in Fig. 6. The living room on the ground floor is selected to investigate the indoor air temperature, velocity distributions with installing the WHR system, including

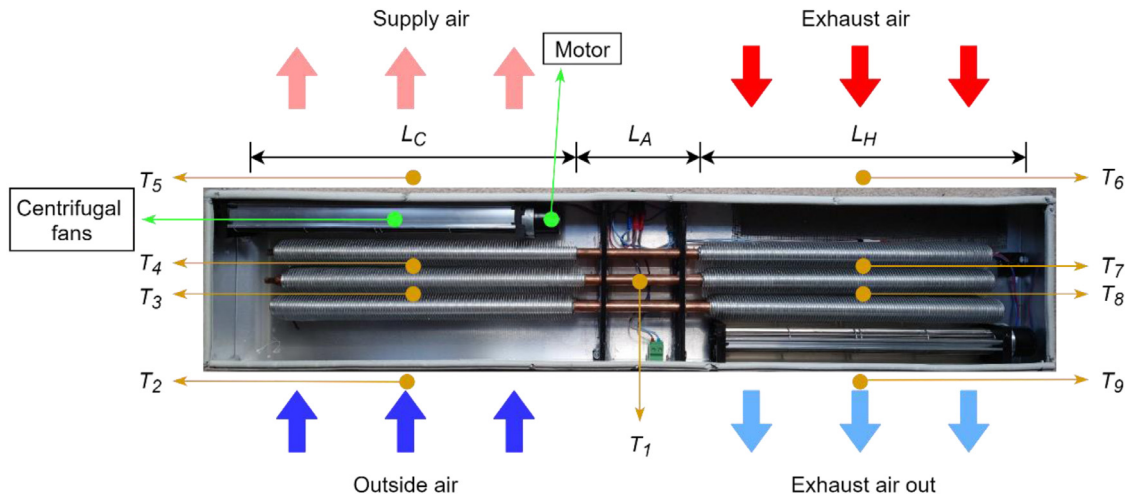


Fig. 8. Window heat recovery prototype used in the experiments.

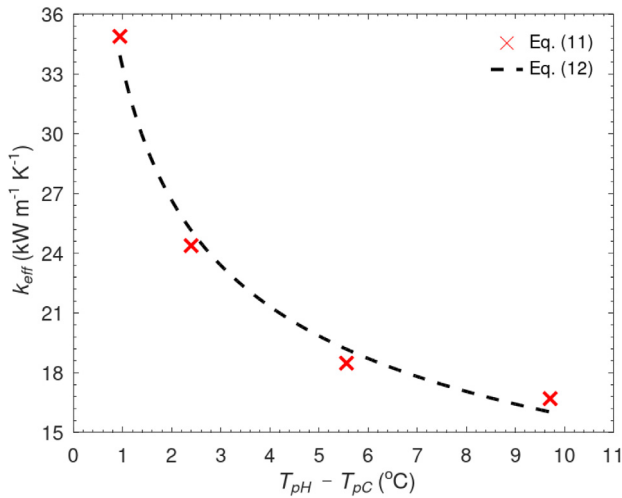


Fig. 9. Effective thermal conductivity for the temperature differences.

air temperature and velocity distribution and summer overheating mitigation issues, with the floor plan and living room location shown in Fig. 7.

The building is a solid wall constructed in 1948 with a wall U-value of 2.1 W/m² K. All windows applied double glazing with a U-value of 2.5 W/m² K, and pitched roofs are insulated by rigid polyisocyanurate (PIR) insulation with a U-value of 0.22 W/m² K. Besides, the ground floor is also solid-wall constructed with a U-value of 0.85 W/m² K, and the attic floor is insulated with rock wool with a total U-value of 0.90 W/m² K. The airtightness for the main building and the loft is tested with 2.69 ACH and 4.18 ACH under a pressure difference of 50 Pa. The high-intensity solar radiation periods are between May and August, while low-intensity periods are for the rest of the months. The highest and lowest ambient temperatures are 33.6 °C and −2.0 °C.

The space heating is powered only by natural gas, driven by combi-boilers with a seasonal heating energy efficiency of 94%. Moreover, the space heating set temperature for the whole house is 19 °C (08:00–17:00 h) and 22 °C (00:00–08:00 h, 17:00–24:00 h), respectively. No cooling system was installed according to the local weather data.

3. Experimental and validation

3.1. Experimental

The window heat recovery prototype presented in Fig. 8 was tested under different conditions, where the ventilation rates are regulated with 6-levels by the centrifugal fan and its controllable motor from 10 to 60 m³/h. The temperature was recorded in different locations, as identified in Fig. 8 (T_1 to T_9 are temperature sensors), and then the average temperature on the two sides of the pipes and the average heat flux are calculated. Besides, air pressure differences between inlet and outlet of supply and exhaust air side are measured, with varied air velocity from 10–60 m³/h.

3.1.1. Determination of effective thermal conductivity

For the determination of effective thermal conductivity, the following relation resulted from the combination of Eqs. (1) and (5) is used:

$$k_{eff} = \frac{Q_{av} L_{eff}}{A_p (T_{pH} - T_{pC})} \quad (11)$$

where Q_{av} is the mean heat flowing through a single heat pipe and T_{pH} and T_{pC} are, respectively, the average heat pipe hot side temperature and cold side temperature. The experiments are conducted for $\dot{m}_C = \dot{m}_H$. This means that the temperature profiles from inlet to outlet on each side can be considered approximately linear. To simplify the approach to estimating the effective thermal conductivity without compromising the accuracy, it is assumed that the total heat flux is divided into equal parts for all heat pipes $Q_{av} = Q_T / (N_p N_s)$. The total heat flux Q_T is calculated using Eq. (2), the temperature recorded in locations T_2 , T_5 , T_6 and T_9 and the mass flow rate. The length L_{eff} is calculated from Eq. (7), and the temperature difference $T_{pH} - T_{pC}$ is calculated using the average temperature difference between T_2 to T_5 and T_9 to T_6 . The inlet temperature of the cold and hot sides are changed according to Table 3, and the mass flow rate is fixed in $\dot{m}_C = \dot{m}_H = 69.1$ m³/h. Fig. 9 presents the obtained effective thermal conductivity for the temperature differences between the hot and cold sides.

To obtain a correlation to be used in the numerical model, the data from Fig. 9 is fitted using a power-law curve, where the following equation with $R^2 = 0.985$ is obtained:

$$k_{eff} = 33298.8 (T_{pH} - T_{pC})^{-0.322} \quad (12)$$

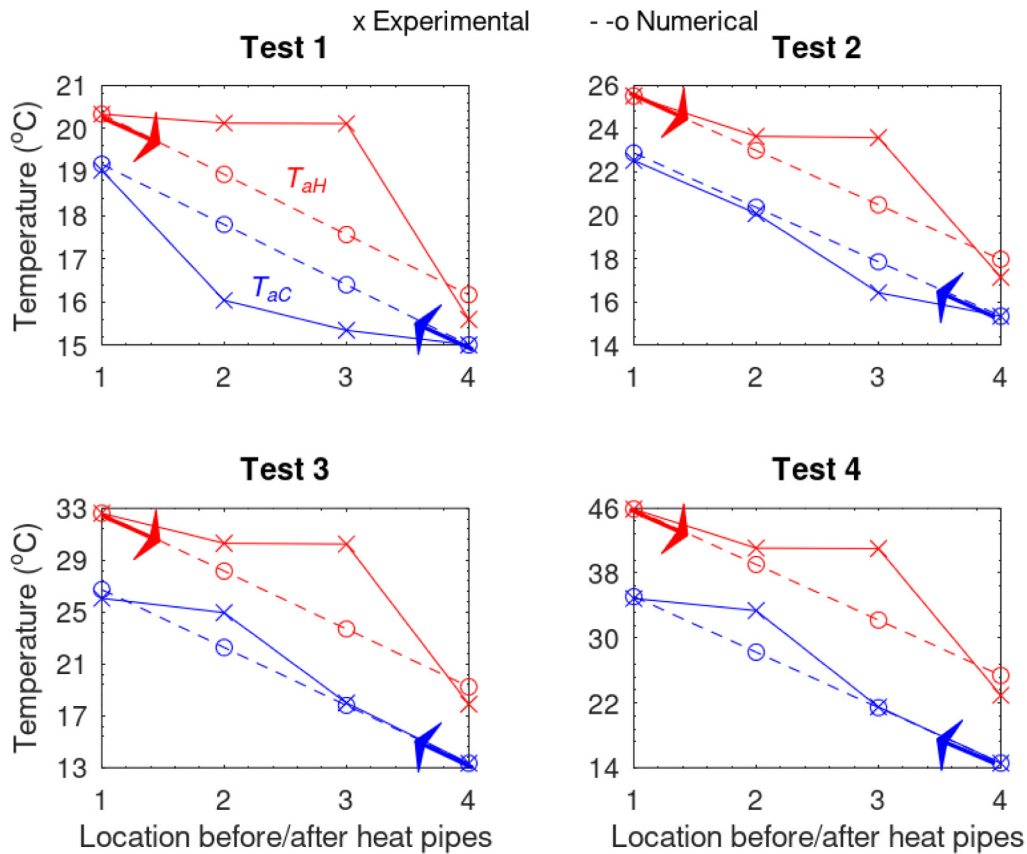


Fig. 10. Comparison between experimental and numerical results for different test conditions.

3.2. Validation

3.2.1. Analytical formulation

After determining effective thermal conductivity, the calibration factor F , introduced in Eq. (8), was adjusted to minimise the difference between numerical and experiments, where a value of $F = 25$ was found. This value and the proposed effective thermal conductivity correlation were then used in the simulations. The temperature distribution before and after each heat pipe measured during the experiments and obtained from the numerical model for four different test conditions are presented in Fig. 10.

There are some minor differences between measurements and numerical results, but it can be considered that the numerical model can predict reasonably the outlet temperature of air (the most important) on each side. The main differences are in the temperature recorded in the middle heat pipes (locations 2 and 3). This is mainly due to the difficulty on inserting the temperature sensors (thermocouples) exactly in between those heat pipes, where the thermocouples might be affected by the heat pipe wall surface. However, the impact of heat pipe wall surface on the thermocouples will be mitigated due to the adequate space between them, which indicates the agreement of the total temperature differences of simulation and experiments. The comparison between outlet temperature for the four test conditions obtained from experimental (Exp.) and numerical (Num.) are presented in Table 3.

According to the results presented in Table 3, the maximum difference between measured and modelled outlet temperature is always on the hot side, which are 3.8%, 5.3%, 7.3% and 10.9%, respectively, for tests 1, 2, 3 and 4. This difference increase when we increase the temperature range, which can be explained due to thermal losses not accounted for in the numerical model. According to this result, it is considered that the model can be

Table 3

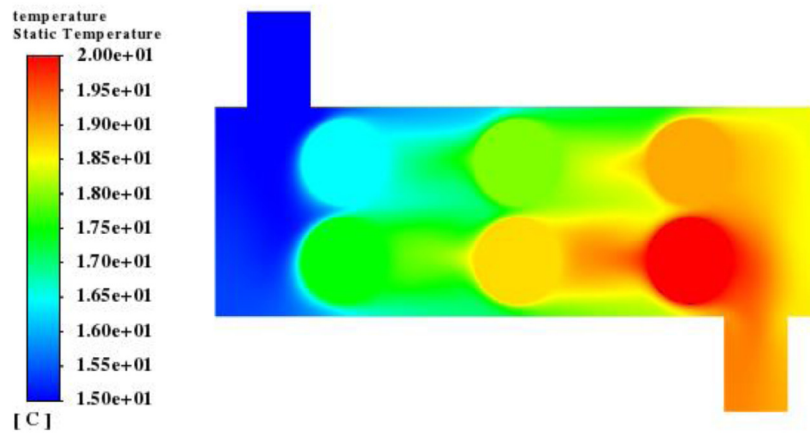
Comparison between measured and modelled outlet temperature.

	Test 1		Test 2		Test 3		Test 4	
	Exp.	Num.	Exp.	Num.	Exp.	Num.	Exp.	Num.
T_{aCin} (°C)	15		15.3		13.4		14.6	
T_{aCout} (°C)	19.0	19.2	22.5	22.9	26.0	26.7	34.9	35.1
T_{aHin} (°C)	20.4		25.5		32.6		45.9	
T_{aHout} (°C)	15.6	16.2	17.1	18.0	17.9	19.2	22.9	25.4

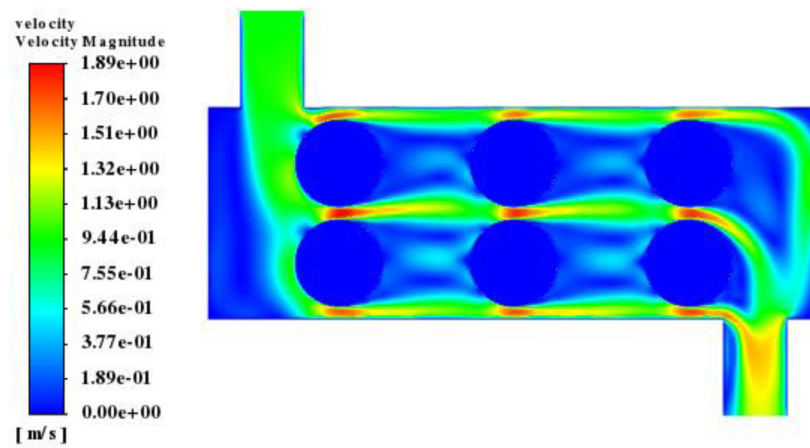
used to study the performance of the window heat recovery system for other conditions.

3.2.2. CFD validation

Apart from the analytical formulation, the CFD simulation of the hot and cold side temperature was conducted to compare with the numerical results. Fig. 11(a) and (b) show the temperature and velocity distribution profile of the model with the cold inlet temperature of 15 °C and inlet velocity of 0.93 m/s. The comparison between hot and cold outlet temperature for the four tests conditions obtained in CFD simulation (CFD) and numerical (Num.) are presented in Table 4. Minor differences between the two methods exist, however, the discrepancies of hot side outlet temperature for CFD simulation and numerical method gradually increase with the more considerable temperature differences, which are 2.4%, 2.6%, 2.8% and 3.2% for tests 1, 2, 3 and 4. The reason may be ascribed to that (1) The iteration has not fully converged; (2) The representation of the governing flow equations and other physical models as algebraic expressions in a discrete domain of space and time; (3) The meshing grid has not been precisely refined; (4) Little computing values per cell and resulting interpolation errors.



(a)



(b)

Fig. 11. CFD simulation results with an inlet temperature of 15 °C and inlet velocity of 0.93 m/s: (a) Temperature and (b) velocity magnitude.

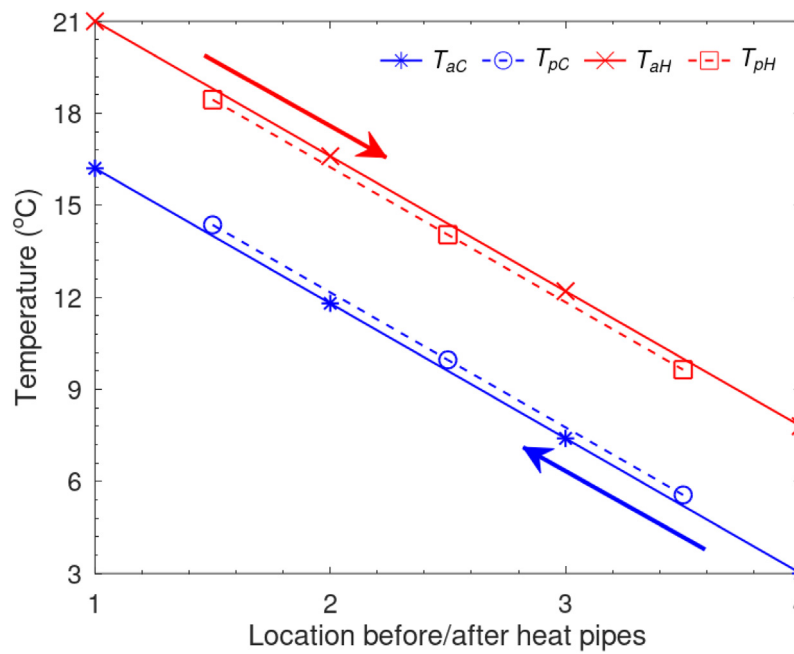


Fig. 12. Temperature profile in air and heat pipe along the flow direction of the window heat recovery system.

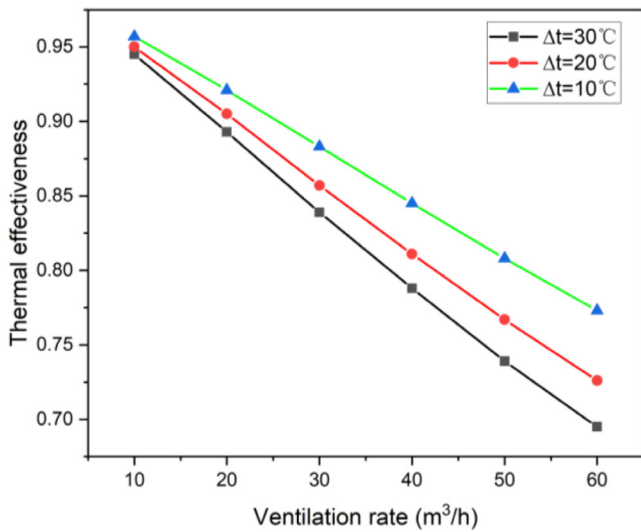


Fig. 13. Impact of maximum temperature difference on the thermal effectiveness with ventilation rate varied between 10 to 60 m³/h.

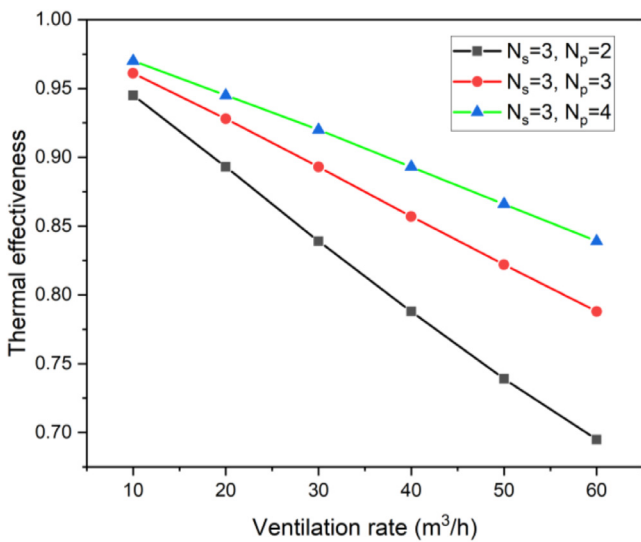


Fig. 14. Impact of heat pipe numbers on the thermal effectiveness with ventilation rate varied between 10 to 60 m³/h.

Table 4
Comparison between CFD simulation and numerical outlet temperatures.

	Test 1		Test 2		Test 3		Test 4	
	CFD	Num.	CFD	Num.	CFD	Num.	CFD	Num.
T_{aCin} (°C)		15		15.3		13.4		14.6
T_{aCout} (°C)	19.1	19.2	22.5	22.9	26.1	26.7	35.2	35.1
T_{aHin} (°C)		20.4		25.5		32.6		45.9
T_{aHout} (°C)	15.8	16.2	17.5	18.0	18.7	19.2	24.6	25.4

4. Results and discussion

4.1. Parametric analysis

After model development and validation, it can be used to study the performance of the window heat recovery system for different conditions. In this section, three parameters upon the WHR thermal effectiveness are analysed with the most significant parameter of ventilation rate. Besides, temperature differences

between the cold inlet and the hot outlet also have a noticeable impact on the thermal effectiveness. Furthermore, heat pipe layers have a relatively low influence.

The mass flow rate in the hot and cold side is always considered the same ($\dot{m}_C = \dot{m}_H$) and the geometric reference parameters presented in Table 2 are used. Fig. 12 presents the temperature profile in the air and heat pipe along the flow direction. The profile is linear because of the approaches and the same mass flow rate used on each side.

The inlet temperature, mass flow rate, outlet temperature and effectiveness for the results are presented in Fig. 12, with $T_{aCin} = 3$ °C, $T_{aHin} = 21$ °C, $\dot{m}_C = \dot{m}_H = 60$ m³/h, $T_{aCout} = 16.2$ °C, $T_{aHout} = 7.8$ °C, respectively which resulted in the effectiveness of $\epsilon = 73.3\%$.

Numerical simulation results indicate that the thermal effectiveness slightly drops with the rise of the maximum temperature differences between the cold outside air and hot exhaust air, as shown in Fig. 13. Temperature differences from 10 °C, 20 °C to 30 °C are investigated with the ventilation rates raised between 10 and 60 m³/h. It is figured out that the thermal effectiveness is similar in the range of 94.5% and 95.7% when a low ventilation rate of 10 m³/h. However, the thermal effectiveness decreases between 69.5% and 77.3% when the ventilation rate rises to 60 m³/h. Thus, the thermal effectiveness declining rates are calculated as 0.06%/°C, 0.14%/°C, 0.22%/°C, 0.285%/°C, 0.345%/°C and 0.39%/°C with varied ventilation rates of 10 m³/h, 20 m³/h, 30 m³/h, 40 m³/h, 50 m³/h and 60 m³/h, respectively. Meanwhile, it is also figured out that the ventilation rates have the most significant impact on the improvement of thermal effectiveness, which reveals that the heat transfer coefficient has noticeable degradation with the rise of the ventilation rate from 10 m³/h to 60 m³/h. The thermal effectiveness is dropped by 18.4%, 22.4% and 25.0% with the rise of ventilation rate of 50 m³/h when the temperature differences are 10 °C, 20 °C and 30 °C, respectively.

It is figured out that the increase of heat pipe numbers has a significant impact on the improvement of thermal effectiveness, as shown in Fig. 14, which reveals that the heat transfer coefficient has a noticeable upgrade when the heat pipe layers increase from $N_p = 2$ to $N_p = 3$, with total heat numbers increasing from 6 to 9. Results indicate that the thermal effectiveness is upgraded from 94.5% to 97.0% when a low ventilation rate of 10 m³/h. However, the thermal effectiveness decreased between 69.5% and 83.9% when the ventilation rate rises to 60 m³/h. Thus, the thermal effectiveness decreasing rates are calculated as 1.25%/layer, 2.6%/layer, 4.05%/layer, 5.25%/layer, 6.35%/layer and 7.2%/layer with varied ventilation rates of 10 m³/h, 20 m³/h, 30 m³/h, 40 m³/h, 50 m³/h and 60 m³/h, respectively.

According to the CFD simulation results, the relative total pressure contour of the WHR system with the cold inlet temperature of 15 °C and ventilation rate of 10 m³/h is shown in Fig. 15. The total pressure drop between the inlet and outlet sides is 4.12 Pa, with the former pressure of 4.69 Pa and the latter one of 0.57 Pa. Meanwhile, the pressure drop increases with the rise of ventilation rates from 10–60 m³/h, where the pressure drop is from 4.12 Pa to 77.9 Pa correspondingly, as shown in Fig. 16. Besides, the pressure drop is validated with the experiment where the discrepancies range from -4.4% to 9.8%, which is in the reasonable interval. Moreover, the obtained pressure drop from the experiment is larger than that from the CFD simulation when the ventilation rate is relatively low and vice versa. To obtain a correlation that can be used in the calculation of pressure drop under various ventilation rates, the data from Fig. 16 are fitted using an exponential expression, where the following equation Eq. (13) with $R^2 = 0.999$ is obtained:

$$\Delta P = 0.0931V_r^{1.6417} \tag{13}$$

where ΔP is the total pressure drop between inlet and outlet sides (Pa) and V_r is the ventilation rate (m³/h).

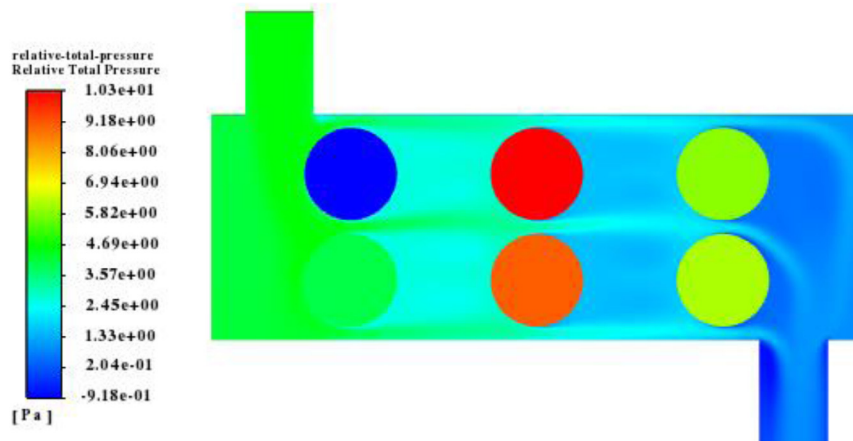


Fig. 15. CFD calculated relative total pressure from inlet to outlet of the WHR system.

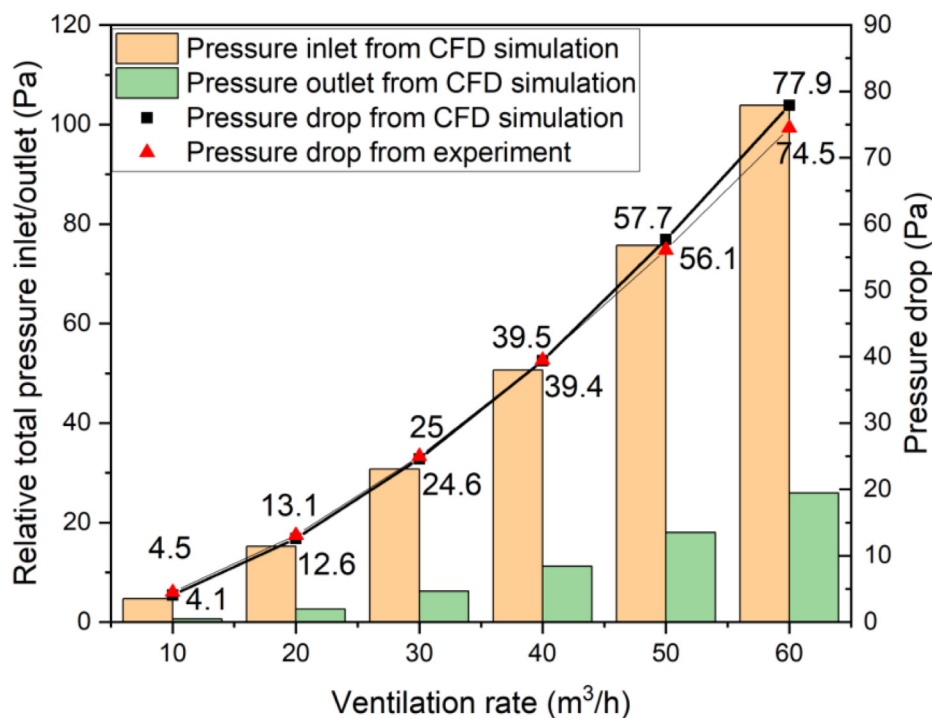


Fig. 16. System pressure drop under ventilation rates varied between 10 – 60 m³/h.

4.2. Energy performance in building

Based on the IES VE baseline model, monthly heating demands are calculated using a 2-layer WHR system under various ventilation rates from 10 m³/h to 60 m³/h, as shown in Fig. 17, where the maximum heating demand occurred in December and the minimum in August. It is figured out that the increase of the ventilation rate could enlarge the monthly heating demand, where the maximum difference is 10.5 kWh/m² in December by comparing 35.5 kWh/m² and 46 kWh/m² under ventilation rate of 10 m³/h and 60 m³/h, respectively. However, in the summertime, the rise of ventilation rates have a limited impact on the monthly heating demand, where the monthly heating demand declines by 3.5 kWh/m² from 6 kWh/m² (60 m³/h) to 2.5 kWh/m² (10 m³/h). Moreover, Table 5 indicates the impact of excluding and including the WHR system in the building baseline on the peaking heating power. Results reveal that the peak heating power could be reduced in a range of 3% to 24%, with the ventilation rate increasing from 10 m³/h to 60 m³/h. Meanwhile, the heating demand

reduction rates vary between 10% to 20%, with the ventilation rate increasing from 10–60 m³/h. It is evident that the heating demand reduction rate has an increasing trend until reaching the maximum value of 20% with the ventilation rate of 40 m³/h by consuming 18 W fan power, then a slight declination to 18.7% with the ventilation rate of 60 m³/h consuming fan power of 34 W. Nonetheless, the fan power continuously rises from 3 W to 34 W, as depicted in Fig. 18. Therefore, the overall energy recovery performance of the WHR unit is optimised with a ventilation rate of 40m³/h and exacerbated with higher ventilation rates.

4.3. Impact on the temperature and velocity

The vertical and horizontal air temperature and velocity differences are investigated to analyse their distribution. It was determined by recording the temperature and velocity values at eight layers, representing distances from the WHR inlet between 0.5 m and 4.0 m. In addition, five horizontal distances are

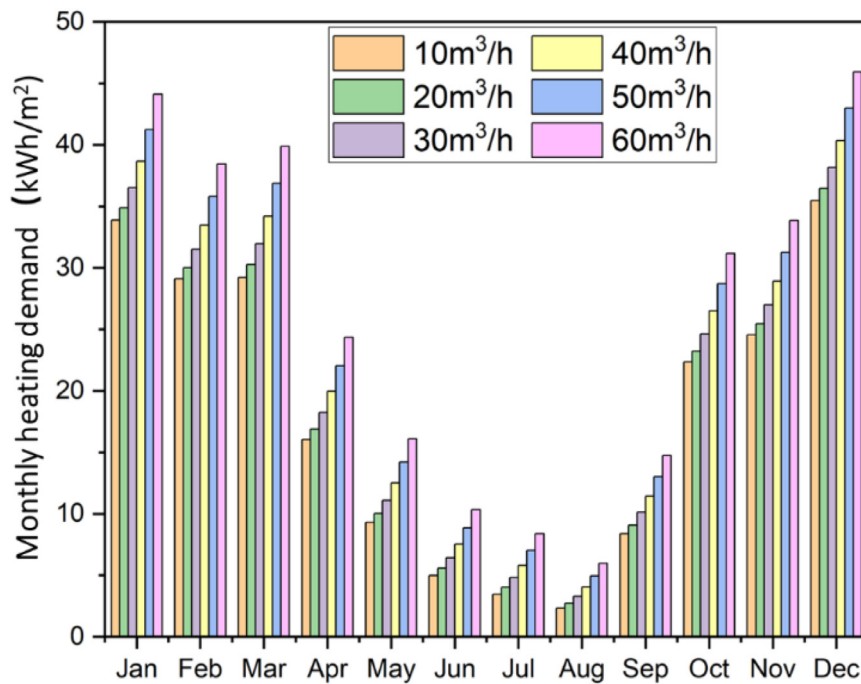


Fig. 17. Building monthly heating demand.

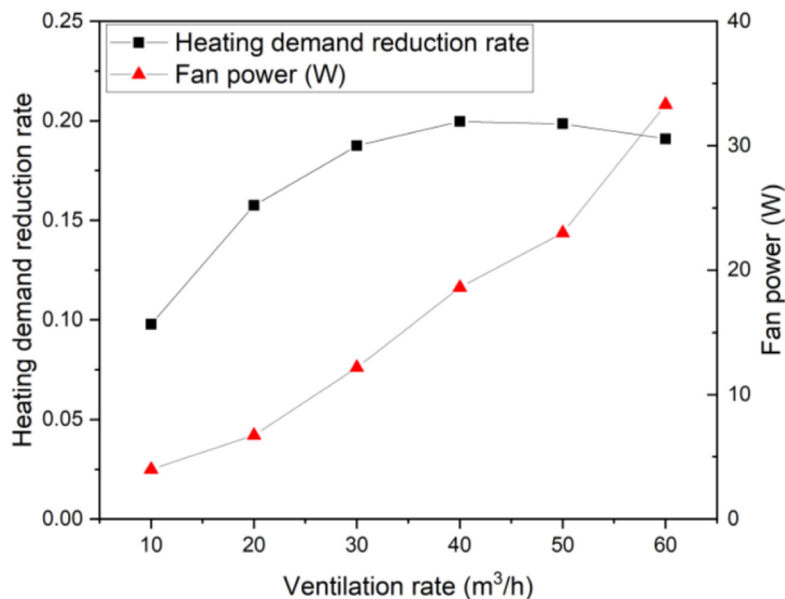


Fig. 18. Building space heating demand reduction rate and fan power with ventilation rates varied between 10 to 60 m³/h.

also recorded in each layer. Firstly, the indoor air temperature, velocity distributions improvement are analysed by comparing the existence of the WHR system under the ventilation rate of 10 m³/h, as shown in Fig. 19 (without) and Fig. 20(a) (with) the heat recovery. It is discovered that the maximum indoor air temperature difference drops from 4.5 °C to 3 °C, where the average temperature has a significant increase from 13.5 °C to 22.5 °C. However, the maximum indoor air velocity rises from 0.47 m/s to 0.9 m/s due to the large pressure difference near the inlet region caused by the inlet–outlet backflow of the WHR system at 0.5 m vertical layer and 1.5 m horizontal distance. Additionally, the air velocity disturbance is weakened in the region away from the inlet.

Fig. 20 reveals the impact of the WHR ventilation rates on indoor air temperature, velocity distributions in terms of the air temperature and velocity distribution, under (a) 10 m³/h, (b) 30 m³/h and (c) 60 m³/h air change rates. With the increment of the ventilation rate, the indoor air temperature rises to 22.5 °C, 23 °C and 23.3 °C, respectively. The air temperature disturbance is weakened with maximum indoor temperature differences reaching 2.8 °C, 2.5 °C and 2.2 °C, respectively. On the contrary, the average indoor air velocity increases from 0.2 m/s to 0.7 m/s and 1.1 m/s, respectively, due to the rise of the ventilation rate. Besides, the air velocity disturbance is strengthened along with the increment of indoor air velocity.

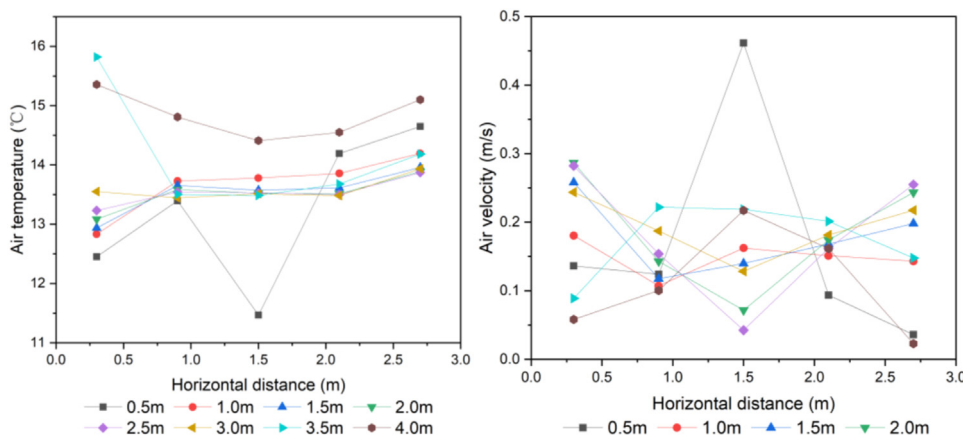


Fig. 19. Air temperature and velocity distribution in the horizontal section at different distances from the inlet under 10 m³/h ventilation rate without heat recovery.

Table 5
The impact of ventilation rates on the peak heating power.

Ventilation rate (m ³ /h)	Excl./Incl. WHR	Peak heating power (W)	Power reduction rate
10	Excl. WHR	6553	3%
	Incl. WHR	6331	
20	Excl. WHR	7269	13%
	Incl. WHR	6322	
30	Excl. WHR	7988	20%
	Incl. WHR	6366	
40	Excl. WHR	8707	22%
	Incl. WHR	6752	
50	Excl. WHR	9427	23%
	Incl. WHR	7223	
60	Excl. WHR	10 147	24%
	Incl. WHR	7753	

5. Conclusions

This work presents the numerical and experimental performance of the window heat recovery (WHR) system made of heat pipes. The numerical model is validated with the experiments and used to study the system for different working conditions and analyse its effect on energy performance in building and indoor air temperature, velocity distributions. The following conclusions can be drawn:

Thermal dynamic performance:

- The effectiveness of heat pipe-based window heat recovery could increase from 65%–95% with the decline of ventilation rate from 60 to 10 m³/h and temperature difference from 30 to 10 °C between exhausted and supplied air.
- Based on CFD simulation results, the numerical pressure drop and temperature difference results agree with the experiment, with the discrepancies ranging from –4.4% to 9.8% and 2.4% to 3.2%, respectively.

Building energy performance:

- The increase of the ventilation rate could enlarge the monthly heating demand, where the maximum difference is 10.5 kWh/m² in December by comparing the ventilation rate of 10 m³/h and 60 m³/h, respectively, whereas the rise of ventilation rates have a limited impact on the monthly heating demand in the summertime. However, the fan power continuously rises from 3 to 34 W.

- The average temperature significantly increases from 13.5 °C to 22.5 °C with different distances from the WHR inlet between 0.5 m and 4.0 m. Nonetheless, the maximum indoor air velocity shows the contrary trend due to the inlet–outlet backflow of the WHR system at 0.5 m vertical layer and 1.5 m horizontal distance. Additionally, the air velocity disturbance is affected by the distance from the inlet.

Optimum sizing:

- The overall energy recovery performance of installing the WHR unit is optimised with the ventilation rate of 40 m³/h by consuming 18 W fan power, reaching the maximum value of 20% heating demand reduction rate.

In addition to the its improvement of air quality in buildings, its use may reduce the daylighting area and acoustic insulation. The impact of this limitations will be addressed in future works.

The presented window heat recovery system could be applied to analyse and optimise the building retrofit packages in different climate regions. Considering that up to 90% of existing homes rely on ineffective natural and mechanical ventilation, providing clean and fresh air in existing homes remains a vast market demand. Therefore, tackling the carbon challenge in the building sector requires radical measures of effective WHR ventilation system to achieve decarbonisation and significant contribution to Net Zero Target in the UK and EU.

CRedit authorship contribution statement

Germilly Barreto: Methodology, Software, Data curation, Writing – original draft Investigation, Validation. **Ke Qu:** Conceptualisation, Methodology, Data curation, Investigation, Validation, Project administration. **Yuhao Wang:** Methodology, Writing – review & editing, Resources. **Muriel Iten:** Writing – review & editing. **Saffa Riffat:** Supervision, Funding acquisition, Writing – review & editing.

Declaration of competing interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

Acknowledgements

The authors would like to acknowledge the financial support and contributions from European Commission Horizon 2020 project Surefit (project contract number: 894511) and project partners participation.

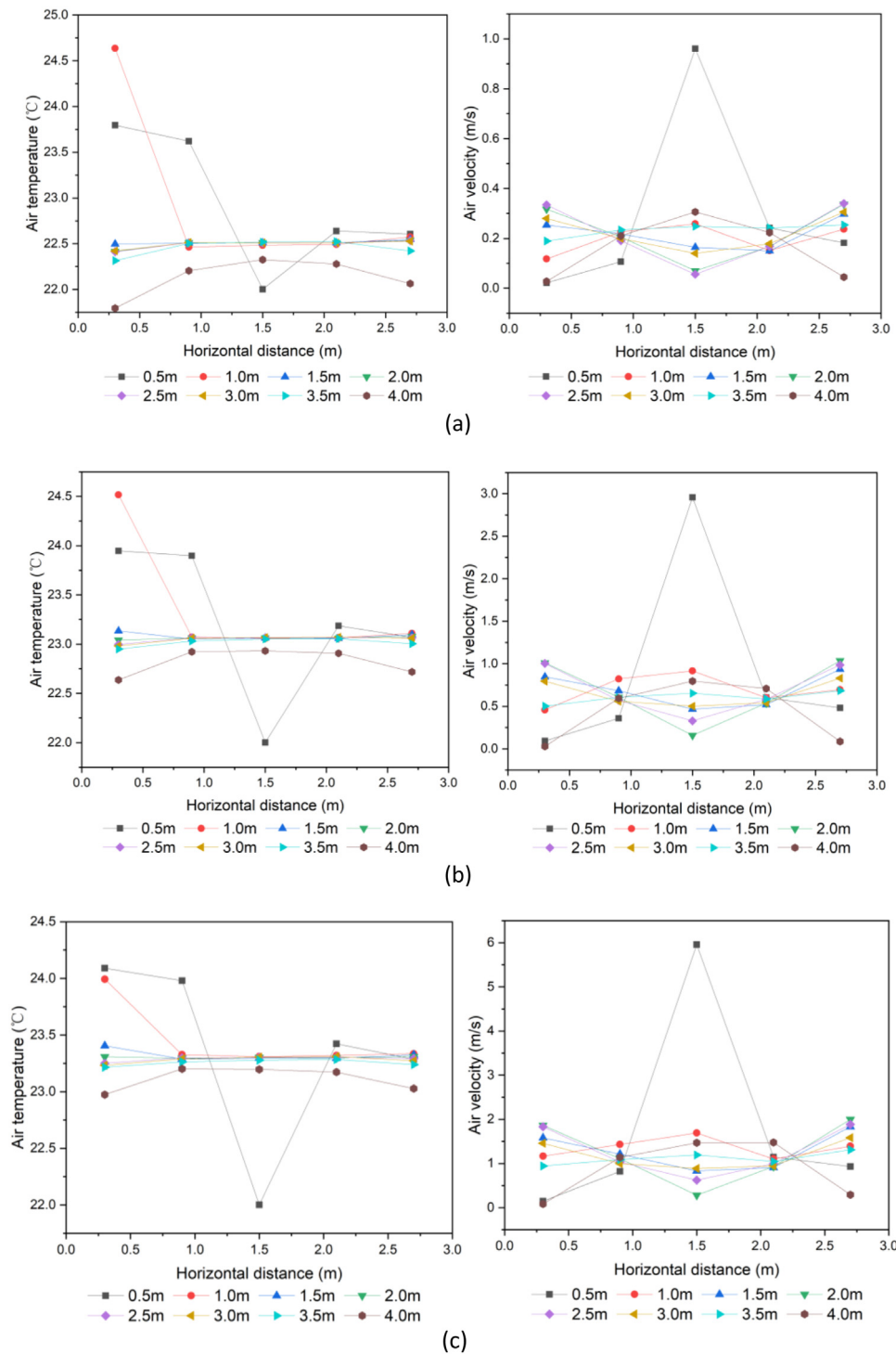


Fig. 20. Air temperature and velocity distribution in the horizontal section at different distances from the inlet under 10 m³/h (a), 30 m³/h (b) and 60 m³/h (c) ventilation rates with heat recovery.

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