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A New Type of Quartz Smog Chamber: Design and Characterization

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21 **Abstract:**

22 Since the 1960s, many indoor and outdoor smog chambers have been developed worldwide.
23 However, most of them are made of Teflon films, which have relatively high background
24 contaminations due to wall effect. We developed the world's first medium-size quartz chamber
25 (10 m^3), which is jointed with 32 pieces of 5 mm thick polished quartz glasses and a stainless-
26 steel frame. Characterizations show that this chamber exhibits excellent performance in terms
27 of relative humidity (RH) (2-80%) and temperature ($15\text{-}30 \pm 1\text{ }^\circ\text{C}$) control, mixing efficiency
28 of reactants (6-8 min), light transmittance ($>90\%$ above 290 nm) and wall loss of pollutants.
29 The wall loss rates of gas-phase pollutants are on the order of 10^{-4} min^{-1} at 298K under dry
30 conditions. It is 0.08 h^{-1} for 100-500 nm particles, significantly lower than those of Teflon
31 chambers. The photolysis rate of NO_2 (J_{NO_2}) is automatically adjustable to simulate the diurnal
32 variation of solar irradiation from 0 to 0.40 min^{-1} . The inner surface of the chamber can be
33 repeatedly washed with deionized water, resulting into low background contaminations. Both
34 experiments (toluene- NO_x and α -pinene-ozone systems) and box model demonstrate that this
35 new quartz chamber can provide high-quality data for investigating SOA and O_3 formation in
36 the atmosphere.

37 **Keywords:** Quartz Chamber, Characterization, SOA and O_3 formation

38 **Synopsis:** A water-washable quartz chamber with low particle loss rate was constructed for
39 simulating atmospheric chemistry under clean conditions.

40 **1.Introduction**

41 Air pollution is both local and global environmental issues. Many smog chambers have
42 been developed worldwide for understanding the mechanisms of air pollution events, such as
43 photochemical smog and secondary organic aerosol (SOA) formation under well-controlled
44 conditions. The smog chambers are usually divided into outdoor and indoor chambers in terms
45 of light sources. The former one uses the natural sunlight, while the latter one usually uses
46 artificial lights.¹ Many experiments on ozone (O₃) and SOA formation have been carried out in
47 large outdoor chambers.²⁻⁷ However, it is a challenge to repeat experiments with the same
48 diurnal variations of solar irradiation and temperature. In contrast, it is easy to do that by
49 precisely controlling reaction conditions (e.g., temperature, humidity, and pressure) using an
50 indoor chamber although the artificial light spectrum of indoor chambers differs from the solar
51 spectrum, resulting in different rates for some photolysis reactions.⁸⁻¹⁰

52 Table S1 summarizes the worldwide outdoor and indoor chambers used to simulate the
53 atmospheric photochemical processes. In the 1970s, the large-size smog chamber abroad was
54 aimed to understand the formation of near-ground O₃ pollution.^{11, 12} In the following thirty
55 years, the indoor and outdoor chambers were widely used to study the general mechanism of
56 secondary pollutants, such as ground-level-ozone¹³⁻¹⁵ and SOA.^{6, 16-19} After the 2000s, many
57 smog chambers have been set up or transformed, rebuilt and upgraded, to deal with the issues
58 of atmospheric chemistry, such as PM_{2.5} pollution,^{4, 20, 21} reaction kinetic parameters and
59 mechanisms^{22, 23} of intermediate products from volatile organic compounds (VOCs) oxidation
60 ²⁴⁻²⁷ and multiphase processes,^{28, 29} and so on. In China, chamber studies have been started to
61 investigate gas-phase kinetics in the atmosphere in the early 1980s.³⁰⁻³² Tang et al.³³ built the

62 earliest indoor chamber in Peking University to disclose the photochemical smog phenomenon
63 that occurred in Lanzhou, China. In the next decades, various-size of smog chambers were
64 constructed to investigate a series of atmospheric issues, including the photochemical-reaction
65 mechanism of O₃ and aerosol formation,³⁴⁻³⁸ the primary emissions and secondary formation
66 process of biomass,³⁹ gasoline and diesel exhausts,⁴⁰⁻⁴² and physicochemical properties of
67 SOA.⁴³⁻⁴⁶

68 Complex atmospheric chemical mechanisms or models, such as the Master Chemical
69 Mechanisms (MCM),⁴⁷ the Regional Atmospheric Chemistry Mechanisms (RACM),⁴⁸ the
70 Carbon Bond mechanisms,⁴⁹ and the SAPRC mechanisms,⁵⁰ have been developed with the help
71 of chamber studies.^{11 12 51} Nowadays, fine atmospheric chemical mechanisms, such as highly
72 oxidized molecules (HOMs) formation,⁵² new particle formation (NPF) and gas-to-particle
73 partitioning,⁵³ and the reaction kinetics of important intermediates^{43, 54-58} have attracted much
74 attention in chamber studies. In particular, it is feasible for studying the formation mechanism
75 or kinetics of intermediates with extremely low concentrations with the aid of the state-of-the-
76 art instruments, such as high-resolution chemical ionization mass spectrometer (HR-CIMS),
77 high-resolution time-of-flight aerosol mass spectrometer (HR-ToF-AMS) and so on. When
78 dealing with these scientific issues, low background contamination is a new requirement for
79 chamber studies.

80 So far, the smog chambers were almost made of Teflon films, including fluorinated
81 ethylene propylene (FEP), poly tetra fluoroethylene (PTFE) and perfluoroalkoxy (PFA).⁵³ The
82 advantages of Teflon chambers include changeable shape to keep constant pressure during
83 experiments and to be evacuated for speeding up chamber cleaning, chemical inertness for

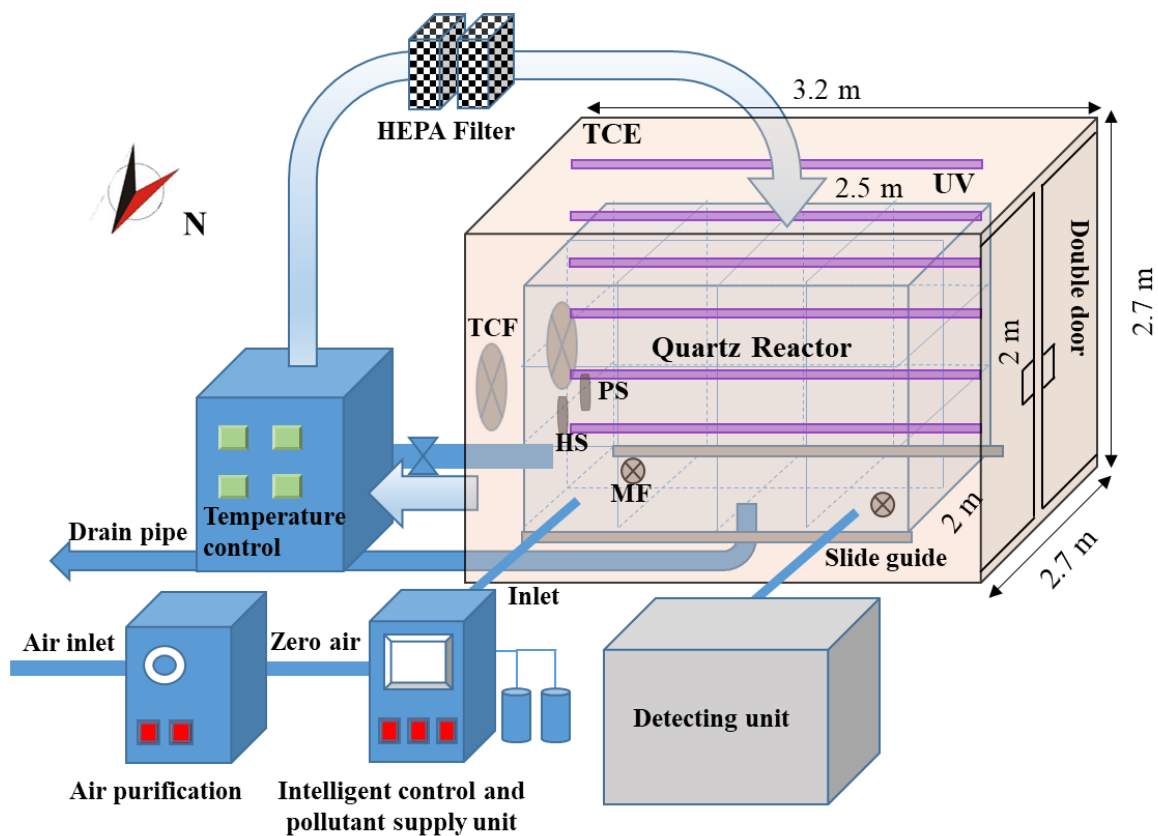
84 some reactants and intermediate products, and easiness for construction.^{53, 59} However, the
85 inner walls of a Teflon reactor are easily contaminated by depositing gas-phase and particle-
86 phase pollutants due to the electrostatic property of the Teflon film. Thus, the contamination
87 between different experimental runs is an important problem for chamber studies. Subsequently,
88 it requires a thorough cleaning after an experiment. Even so, Teflon reactor usually has a short
89 lifetime, and a high cost for the film replacement. In addition, Teflon film is permeable for
90 some trace gases and even a source of VOCs. This usually results in a relatively high
91 background, which is a challenge for understanding the atmospheric processes under extremely
92 clean conditions. This is one of the driven forces to construct the CLOUD chamber, CESAM
93 ⁶⁰ (4.2 m³) and HIRAC⁶¹ (2 m³) with stainless-steel which is water-washable⁶² and the
94 Simulation of Atmospheric Photochemistry In a large Reaction Chamber²² (SAPHIR) using
95 double-layers of Teflon films. Quartz is a water-washable material with chemical inertness and
96 high UV-light transparency. It is widely used as the material for flow tube reactors with volume
97 usually from tens to hundreds of liters. Small size quartz chambers such as QUAREC⁶³ (1.08
98 m³) and CERNESIM⁶⁴ (0.78 m³) have been reported. However, the large ratio of surface area
99 to volume (S/V) of the flow tube reactors and small chambers limits its application in
100 photochemistry studies under the concentration conditions close to that in the ambient air. In
101 addition, the relatively small volume, leading to a short residence time, means that it is difficult
102 to simulate reactions with long reaction time. To our best knowledge, a large smog chamber
103 (V > 2 m³) made of quartz has not been reported yet⁶³⁻⁶⁵ due to manufacture and the cost.

104 In this study, we described a 10 m³ quartz indoor photochemical chamber newly built in
105 the Aerosol and Haze Laboratory at Beijing University of Chemical and Technology

106 (AHL/BUCT). As the world's first medium-size quartz chamber at present, it can be cleaned
107 with deionized water (Section 2.3) to minimize the contamination between two experiments. It
108 also extends the life-cycle and greatly reduce the maintaining-costs compared with Teflon
109 chambers. The AHL/BUCT chamber was designed to simulate the atmospheric photochemical
110 processes under repeatable conditions (e.g., temperature, humidity, and light intensity). A series
111 of experiments were performed to characterize the chamber, including homogeneity of
112 reactants, irradiation intensity and light transmission, wall loss of gaseous and particle
113 pollutants, and background of the chamber. In addition, the preliminary application
114 experiments have been carried out using the classic gas-phase photochemical reaction of the
115 toluene-NO_x system and ozonolysis of α -pinene in the dark.

116 **2. Instrumentation**

117 The quartz chamber system is a laboratory simulation unit of the AHL/BUCT station,
118 which is equipped with the state-of-the-art instruments in connection to atmospheric trace gases,
119 aerosol particle size and mass concentrations, cluster and aerosol particle chemical composition
120 on the levels from molecular size to micrometer size.⁶⁶ The chamber system consists of five
121 parts, i.e., a quartz reactor, an enclosure unit along with temperature and UV irradiation
122 controlling system, a clean unit, a pollutants-supply unit and a detecting unit (Figure 1). The
123 quartz reactor sets in the enclosure which is temperature-controllable and is also the support of
124 UV lights. The whole chamber system is in a temperature-conditioned room. Figure S1 shows
125 the pictures of the reactor and the enclosure.



126

127 **Figure 1.** Schematic diagram of the AHL/BUCT quartz chamber (TCE: temperature-controlled
 128 enclosure; TCF: temperature-controlled fans; MF: magnetic fans; PS: pressure sensor; HS:
 129 humidity sensor).

130 Briefly, the quartz reactor is a 10 m³ cuboid reactor, which consists of 32 pieces of polished
 131 quartz glasses (5 mm of thickness), a stainless-steel flange (30 × 100 mm) with a quartz window
 132 (165 mm I.D.) and a stainless-steel frame (2.5 × 2 × 2 m, L, W and H). Several inlets, sampling
 133 lines and a temperature and humidity sensor (HMP110, Vaisala, Finland) and a pressure sensor
 134 (MSW101, Dwyer, America) are installed inside the reactor. A cuboid enclosure (3.2 × 2.7 ×
 135 2.7 m) is temperature-conditioned through a circulation system. 60 UV lamps (1.2 m, 60 W
 136 Philips/10R PL, Germany) with the main wavelength at 371 nm are mounted on the inner wall
 137 of the enclosure. The reactor can be cleaned by both deionized water and zero-air. Water spray
 138 is introduced through the aforementioned flange with a high-pressure water gun, while the

139 zero-air system is the same as the that of traditional Teflon chambers. A pollutant supply unit
140 and a detecting unit are similar to those used in the traditional chambers and described in the
141 SI.

142 **3. Characterization of the chamber**

143 A series of experiments have been carried out to evaluate the performance of the quartz
144 chamber, including the homogeneity of reactants, the light spectrum and irradiation intensity,
145 the wall losses of gaseous pollutants and particles. All experiments are carried out at the RH
146 lower than 10%. Only a part of instruments such as a Vocus proton transfer reaction mass
147 spectrometry (Vocus-PTR-MS), a single photon ionization (SPI) TOF-MS (SPIMS), inorganic
148 trace-gas analyzer, and a scanning mobility particle sizer (SMPS) are involved in these
149 experiments.

150 **3.1. Basic parameters**

151 The temperature in the BUCT quartz chamber is accurately controlled in the range of 15-
152 30 °C by a circulation system. The temperature in the chamber is monitored by a temperature
153 sensor. Two fans inside the chamber ensures the homogeneity of the temperature in the reactor.
154 Figure S2 shows the evolution of the temperature inside the chamber in the dark and in the
155 light. The temperature of the chamber reaches a target value within 30 minutes. The fluctuation
156 of temperature is below ± 1 °C in the dark and below ± 2 °C when all lights are turned on. The
157 pressure in quartz reactor can be accurately controlled in whole experiment (Figure S3). These
158 results indicate a good performance of temperature control inside the chamber.

159 NO_x is chosen as a tracer to test the mixing time for gas-phase pollutants inside the
160 chamber. The inlet for gas-feeding is in the middle of the chamber. The NO_x was injected into

161 the chamber at a flow rate of 2 L min^{-1} for 3 min in each pulse from a standard gas cylinder.
162 Before the NO_x is added, the fans are turned on. Figure S4 shows the change of NO_x
163 concentration, which is continuously monitored using a NO_x analyzer. The NO_x concentration
164 becomes stable within 6-8 min after the injection. For other compounds, like toluene, a similar
165 mixing time is observed. Compared to the duration of each chamber experiment, which may
166 be several hours, this mixing time is acceptable.

167 **3.2. Light spectrum and intensity**

168 The emission spectrum of the UV lamps is measured using a spectrometer (StellarNet,
169 Inc., USA) and is shown in Figure S5. The irradiation is in the range of 340-600 nm with the
170 strongest peak at 371 nm, slightly higher than other indoor chambers (353-370 nm)^{41, 67, 68}.
171 Several small peaks at 300-600 nm are also observable like other UV lamps used in indoor
172 chambers^{9, 35, 69}. The emission wavelength can well represent the sunlight (the light-yellow
173 filled area) in the low wavelength region. Figure S5 also shows the transmittance of the quartz
174 with 5 mm of depth (the light blue line) measured using the UV-visible spectrophotometer
175 (INESA Instrument., China). The transmittance is over 90% in the wavelength range of 290-
176 1100 nm. We also measured the transmittance of FEP Teflon film with 125 μm depth (Du Pont).
177 The transmittance decreases from around 90 % at 1100 nm to 65 % at 300 nm. At 371 nm, the
178 transmittance of the quartz and the FEP film are 91.5 % and 74.5 %, respectively. These results
179 indicate that quartz is better than FEP and is an ideal material for the smog chamber reactor as
180 far as the light transmittance is considered. The distribution of light intensity in the chamber is
181 relatively uniform (Figure S6).

182 In chamber studies, the light intensity is usually represented by the photolysis rate of NO₂

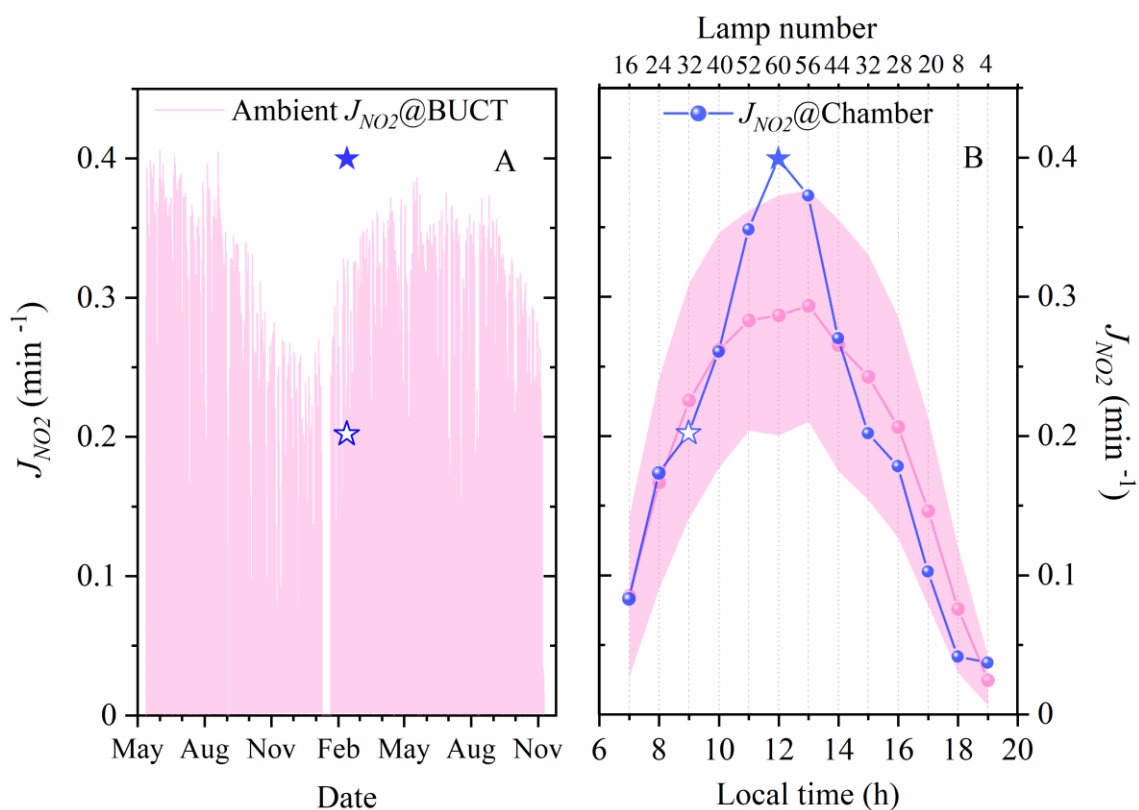
183 (J_{NO_2}), which is estimated according to a steady state of the photochemical reaction system of
184 NO-NO₂-O₃. NO₂ is injected into the chamber, irradiated with the UV lights. According to the
185 monitored mixing ratio of NO, NO₂, and O₃, J_{NO_2} is calculated using the following equation,⁷⁰

$$186 \quad J_{NO_2} = k_{NO+O_3} [NO][O_3]/[NO_2] \quad (1)$$

187 where $[NO]$, $[NO_2]$, and $[O_3]$ are the equilibrium concentrations (molecules cm⁻³) of NO, NO₂
188 and O₃, respectively; k_{NO+O_3} represents the second-order rate constant between ozone and NO
189 reaction (1.73×10^{-14} cm³ molecule⁻¹ s⁻¹ at 298 K⁷⁰). The re-equilibrium reactions among NO,
190 NO₂ and O₃ in the sampling lines will have an influence on the measurement of their
191 concentrations in the reactor. In this work, the J_{NO_2} is calculated using a MATLAB code which
192 accounting for the re-equilibrium in the sample lines.

193 The J_{NO_2} is 0.40 ± 0.01 min⁻¹ when all the UV lights are turned on (full stars in Figure 2B).
194 It decreases to 0.20 ± 0.01 min⁻¹ when a half of UV lights are turned off (open stars in Figure
195 2B). This shows a good linearity for the UV lights. The maximal J_{NO_2} of our chamber is slightly
196 lower than that of GIG-CAS chamber³⁵ (0.49 min⁻¹), while is in the range of these reported
197 values $0.12 \sim 0.55$ min⁻¹ in other studies^{40, 71}. The hourly mean ambient J_{NO_2} (the pink line)
198 varies from 0.005 to 0.41 min⁻¹ (Figure 2A). Figure 2B shows the mean diurnal curve of J_{NO_2}
199 measured at BUCT using a photolysis rate spectrometer (2pi-j_{NO2}-Filter Radiometer, Metcon,
200 Germany). The maximal J_{NO_2} of our chamber is comparable with the ambient values at noon
201 in summer (0.41 min⁻¹), while the J_{NO_2} with a half of UV lights is close to the ambient value at
202 noon in winter (0.20 - 0.25 min⁻¹). The calculated JO1D⁷² with all light on is about 0.75×10^{-4}
203 min⁻¹, which is comparable with the ambient values ($1.2 \sim 3 \times 10^{-4}$ min⁻¹, based on the measured
204 spectrum) at noon in winter of Beijing, but lower than that ($6 \sim 1.8 \times 10^{-4}$ min⁻¹) in summer

205 Beijing. In addition, the lamps can be automatically controlled with a program. As shown in
 206 Figure 2B (the blue dots and lines), the light system can well simulate the diurnal curve of
 207 ambient J_{NO_2} based on the linear correlation of J_{NO_2} and lamp number. This indicates that the
 208 BUCT chamber can simulate the photochemistry in a day and in different seasons in Beijing.



209
 210 **Figure 2.** Comparison of J_{NO_2} between BUCT chamber and ambient data (The full star means
 211 the J_{NO_2} when all lights are turned on and the hollow star means that when a half lights are
 212 turned on, the purple lines and filled area denote the ambient J_{NO_2} measured at BUCT).

213 3.3. Wall loss of typical gas species and particles

214 Wall loss rate is a key parameter in chamber studies. The wall loss rates of NO, NO₂ and
 215 O₃, which has been widely reported in literatures, were investigated by injecting a certain
 216 concentration of the corresponding gas and presented in their first-order decay rates in the dark.
 217 Table S3 shows the wall loss rates of O₃, NO and NO₂ in our chamber. They were

218 $6.76\sim 8.90\times 10^{-4}$, $4.50\sim 4.58\times 10^{-4}$, and $2.16\sim 3.54\times 10^{-4}\text{ min}^{-1}$, respectively. Compared with
219 other chambers reported in the literatures,^{5, 25, 35, 41, 73} the wall loss rates of these gas species in
220 our chamber are higher than others (see Table S3) because our chamber has a larger ratio of
221 surface-to-volume area ($S/V=2.6\text{ m}^{-1}$). The wall loss rate of toluene ($(0.11\text{-}0.46)\times 10^{-4}\text{ min}^{-1}$)
222 in our chamber is one order of magnitude smaller than the value $((2.20\pm 0.39)\times 10^{-4}\text{ min}^{-1})$ in
223 RCEES chamber⁷⁴. This shows the different adsorptive properties for the quartz and stainless-
224 steel frame compared with Teflon films. In addition, the wall loss rates of intermediates range
225 from 10^{-5} to 10^{-4} min^{-1} (Table S4), which means they are acceptable during the typical 6-hour
226 photochemical experiments.

227 Particles can deposit to the reactor walls due to turbulence, Brownian diffusion,
228 gravitational settling, and electrostatic deposition. The wall losses of particles are usually
229 treated as a first-order process. Thus, the loss rate, k_{dep} , is expressed as the following equation,

230
$$\frac{dN(d_p, t)}{dt} = -k_{dep}(d_p)N(d_p, t) \quad (2)$$

231 where $N(d_p, t)$ is the particle number concentration at a certain particle diameter (d_p).⁷⁵
232 Ammonium sulfate ($(\text{NH}_4)_2\text{SO}_4$) seed particles were used as the reference aerosol to measure
233 the particle wall losses. About 0.05 mol L^{-1} of $(\text{NH}_4)_2\text{SO}_4$ solution was atomized with a flow
234 rate of 2 L min^{-1} zero air. Then, it was dried through a diffusion dryer filled with silica gels to
235 remove the water before introducing into the reactor. The total number concentration of
236 $(\text{NH}_4)_2\text{SO}_4$ was in the range of $2000\sim 3000\text{ molecule cm}^{-3}$ to reduce the coagulation of particles
237 in the chamber. For a cuboid chamber, the dependence of the wall loss rate on particle diameter
238 can be described according to equation (3),⁸

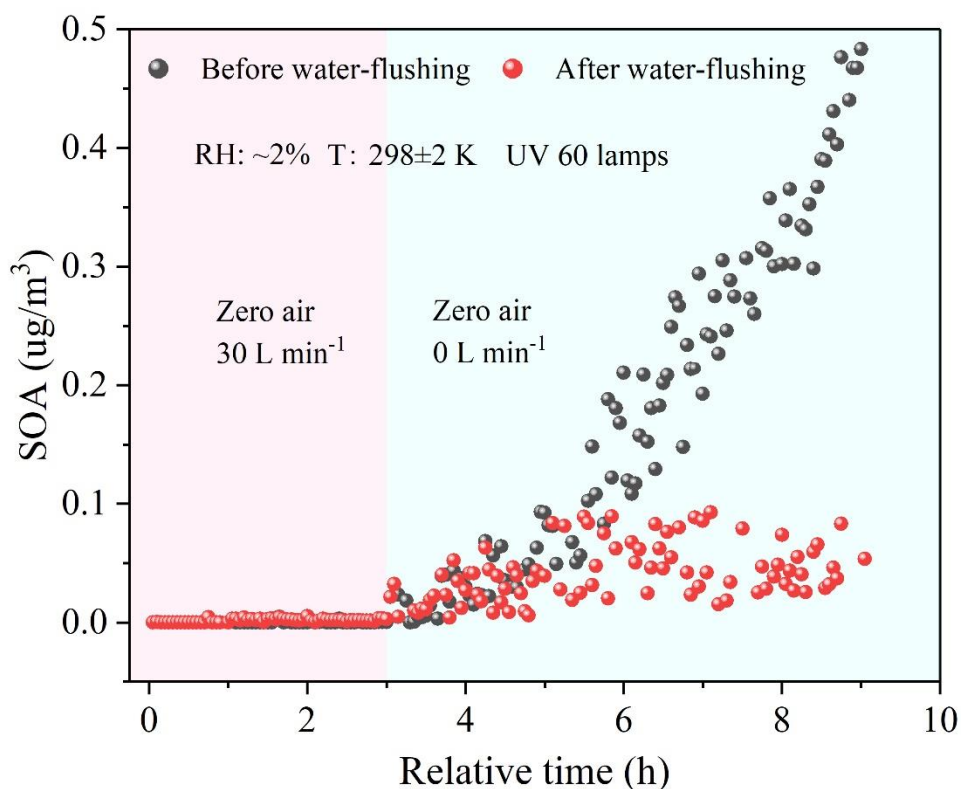
239
$$k_{dep} = a \times d_p^b + c \times d_p^d \quad (3)$$

240 where the parameters (a , b , c , and d) are 2.66×10^{-6} , 1.76, 15.23 and -1.36, respectively. These
241 parameters are comparable with literature data.^{5, 76} Figure S7 shows wall loss rate of $(\text{NH}_4)_2\text{SO}_4$
242 particles as a function of particle diameter. The k_{dep} is in the range of $0.02 \sim 0.24 \text{ h}^{-1}$. For particles
243 with d_p less than 100 nm, the loss rates decrease with the d_p increasing. When the d_p is greater
244 than 100 nm, it increases as the d_p increasing. Diffusion deposition greatly contributes to the
245 wall loss of small particles when the particle diameter is less than 50 nm, while gravitational
246 settling leads to quick deposition of large particles. This is similar to these previous studies.^{5 40}
247 Table S5 compares the overall k_{dep} (100-500 nm) among different chambers. It is 0.08 h^{-1} in
248 our chamber, and this corresponds to a lifetime of 12.5 h. Although the volume of our chamber
249 is smaller than other FEP Teflon chambers, the k_{dep} value of our chamber is lower than other
250 chambers ($0.12\text{-}0.40 \text{ h}^{-1}$), while it is lightly higher than the glass coated stainless steel (0.028
251 h^{-1})⁷⁷ and CESAM stainless steel chamber (0.01 h^{-1})⁶⁰. This should be mainly because of the
252 different materials of the reactors. For our chamber, the stainless-steel frames are electrostatics-
253 proof material. In addition, the specific resistivity of quartz is $5 \times 10^{16}\text{-}7.5 \times 10^{17} \Omega \text{ m}$ ⁷⁸, while it
254 is $>1 \times 10^{18} \Omega \text{ m}$ for Teflon film⁷⁹. This implies a slight weaker dielectric potential of quartz than
255 FEP Teflon.

256 **3.4. Quartz reactor cleanliness**

257 Long-term experiments will result in inorganic and organic contaminants depositing on
258 the inner wall of the smog chamber. Thus, it is important to minimize the contamination
259 between two experimental runs. The chamber was progressively cleaned by two methods: 1)
260 cleaning cycles involving zero air in the presence of UV light; 2) continuously flushing with
261 deionized water.

262 In the chamber testing period, aerosol bursts characterized by large peak concentrations
263 ($>10000\text{ cm}^{-3}$) usually occurred among 6-weeks experimental runs. After every experiment,
264 the air flow rate was maintained at 40 L min^{-1} , which means the chamber was flushed with 6
265 times of the chamber volumes zero air per day. After that, the particle mass concentration was
266 less than $0.01\text{ }\mu\text{g m}^{-3}$. However, contaminants, from deposited organic vapors and particles, are
267 a potential source of backgrounds which may participant in the photochemistry, and aerosol
268 nucleation and growth. To evaluate the performance for the water-cleaning system, we washed
269 the chamber with deionized water. Figure S8 shows the mass spectra of H_3O^+ charged ions
270 within $m/z\ 12\sim 300$ Th before and after flushing the inner walls of the quartz reactor with
271 deionized water. The signals are obviously decreased after water flushing experiment compared
272 with that before. Figure 3 further shows the variation of SOA mass concentrations in
273 background experiments with UV lights on before and after water-flushing. In a flow
274 experiment mode (30 L min^{-1} of zero air flow, the light-pink highlighted area), no NPF event
275 was observable neither before nor after water-flushing. However, in a batch mode (0 L min^{-1}
276 of zero air flow, the light-green highlighted area), NPF event happened before water-flushing
277 and the SOA mass concentration is up to $0.5\text{ }\mu\text{g m}^{-3}$ for 6h of UV irradiation. After water-
278 flushing, the SOA concentration increased slightly in the first three hour, and the mass
279 concentration was around $0.05\text{ }\mu\text{g m}^{-3}$. These results indicate that flushing with deionized water
280 can effectively remove not only inorganic substances, but also water-soluble organics to get
281 the lower background contamination.



282

283 **Figure 3.** The variation of SOA mass concentration in the presence of UV light before and after
 284 water-flushing (the zero-air flow rate of 30 L min⁻¹ in the light-pink filled area and 0 L min⁻¹ in
 285 the light-green filled area, respectively)

286

287 **4. Applications of the chamber in O₃ and SOA formation studies**

288 **4.1. Photochemical oxidation of toluene-NO_x system**

289 The toluene-NO_x photochemical experiments were carried out to evaluate the
 290 performance of our chamber for chemical mechanism study, which has been intensively studied
 291 in other chambers.^{8, 80} Four experiments have been carried out under dry conditions at 298±1
 292 K. Table S6 summaries the initial experimental conditions. The initial toluene concentration
 293 varied from 155 to 250 ppb, and the initial toluene/NO_x ratios (ppbC/ppb) ranged from 4.5 to

294 12.6. A slight over pressure was kept to prevent the ingress of air outside the chamber during
295 our experiments.

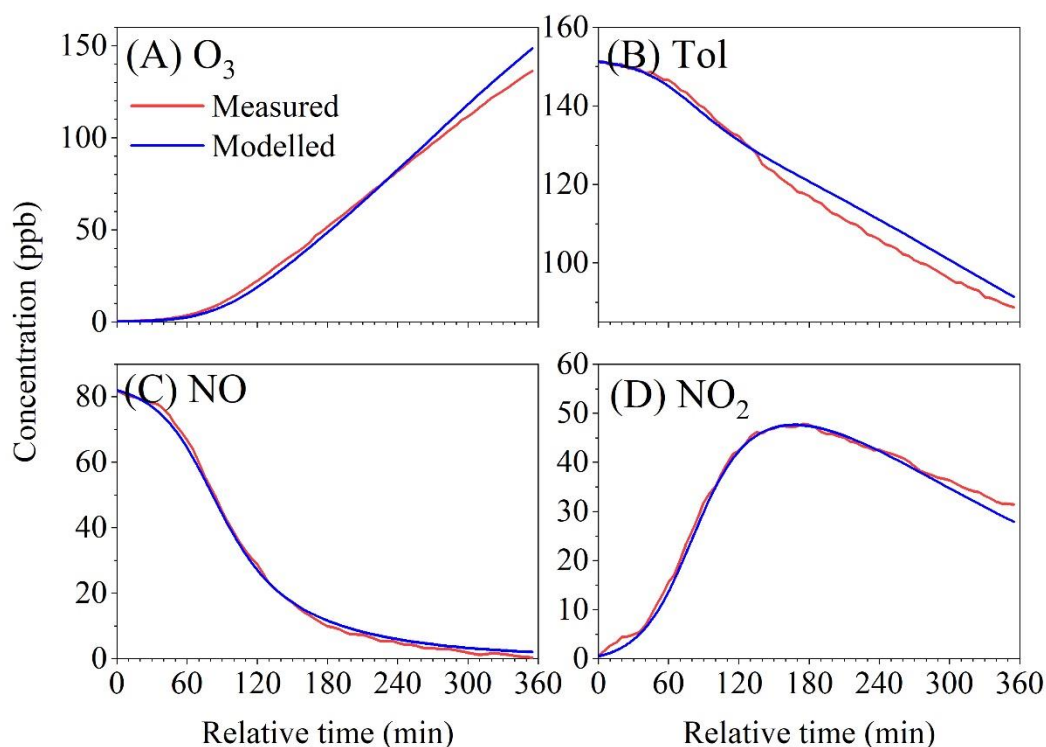
296 Figure S9 shows typical profiles of different pollutants under irradiating condition. The
297 variations of all the pollutants are the same as the classical photochemistry of VOCs-NO system.
298 In this experiment, the initial concentration of toluene and NO_x is 155 ppb and 86.7 ppb,
299 respectively. The decay of toluene and NO and the formation of O₃ speeds up after ~40 min,
300 suggesting that HONO is consumed and OH radicals (Figure S10) are vigorously generated
301 through recycling via NO_x/HO_x chemistry. However, an obvious time lag (~1 h) of aerosol
302 growth is observed in Figure S9B because of the induction duration of low volatile organic
303 compounds (LVOCs). This is also as the same as that observed in other studies.⁸¹

304 A near-explicit mechanism of the toluene from Master Chemical Mechanism (MCM)
305 version 3.3.1 is applied to simulate the toluene-NO photochemistry using the Framework for
306 0-D Atmospheric Modeling (F0AM).⁸² The description of F0AM in details can be seen in
307 supporting material (S2). In the model, the wall loss rates of NO, NO₂, and O₃ obtained in
308 section 3.3 have been accounted for. The formation of HONO from heterogenous reactions of
309 NO₂ on the wall surfaces has also been incorporated. Figure 4 shows the observed and
310 simulated concentration profiles of toluene, NO, NO₂ and O₃. The modelled concentrations of
311 toluene, NO, NO₂, and O₃ are generally well in agreement with the corresponding observed
312 values. At the end of the experiment, toluene and O₃ is slightly overpredicted with a relative
313 deviation of 6.7 % and 7.4 %, respectively, while NO₂ is slightly underpredicted about 6.2 %.

314 The quantity $\Delta([O_3]-[NO])$ is widely used to evaluate the model performance,^{9, 83} which
315 is defined as,

316
$$\Delta([O_3] - [NO]) = ([O_3]_{final} - NO_{final}) - ([O_3]_0 - [NO]_0) \quad (4)$$

317 where NO_0 and $[O_3]_0$ are the initial concentrations of NO and O_3 , while NO_{final} and $[O_3]_{final}$ are
 318 those at the end of experiment. $\Delta([O_3]-[NO])$ represents the amounts of NO oxidized and O_3
 319 formed in the experiments, and gives an indication of the biases in simulation O_3 formation.
 320 Based on the four independent experiments, the bias varies from -21.2 to 22.9 %, which is
 321 within the values ± 25 % reported by Carter et al (2005)⁹ and Wang et al (2014)³⁵ for VOC-
 322 NO_x systems. Therefore, these results indicate that the AHL/BUCT chamber is suitable for
 323 photochemical mechanism evaluations.



324
 325 **Figure 4.** Concentration-time profiles of observed and simulated (A) ozone, (B) toluene, (C)
 326 NO, and (D) NO₂ in the toluene-NO_x experiment.

327 In addition, the SOA formation was studied in the toluene-NO_x irradiation system. The
 328 aerosol yield, Y , is defined as the fraction of the reacted organic gas (ROG) according to the

329 following equation,¹⁸

$$330 \quad Y = \frac{\Delta M_O}{\Delta ROG} \quad (5)$$

331 where ΔM_O is the total mass concentration of organic aerosol formed from photochemical
332 reactions and ΔROG is the consumed mass concentration of VOCs. Assuming aerosol density
333 of 1.45 g cm^{-3} , which is equal to 1.45 g cm^{-3} for toluene-SOA reported by Ng et al (2007),⁸⁰ we
334 convert the measured volume concentrations of SOA using a SMPS into mass concentrations
335 after the wall losses of particles have been accounted for. Figure S11 compares the SOA yields
336 of this work with previous studies. The measured SOA yields of the toluene-NO system are in
337 the range of 0.016 to 0.097, which are comparable with the yields of 0.039 to 0.127 reported
338 by Odum et al(1997),¹⁸ Takekawa et al (2003),⁸ Ng et al (2007),⁸⁰ and Chu et al (2012).⁸⁴

339 According to partition model, Y is nonlinearly correlated to the mass concentration of
340 organic aerosols (M_O),

$$341 \quad Y = M_O \sum \frac{\alpha_i K_{om,i}}{1 + K_{om,i} M_O} \quad (6)$$

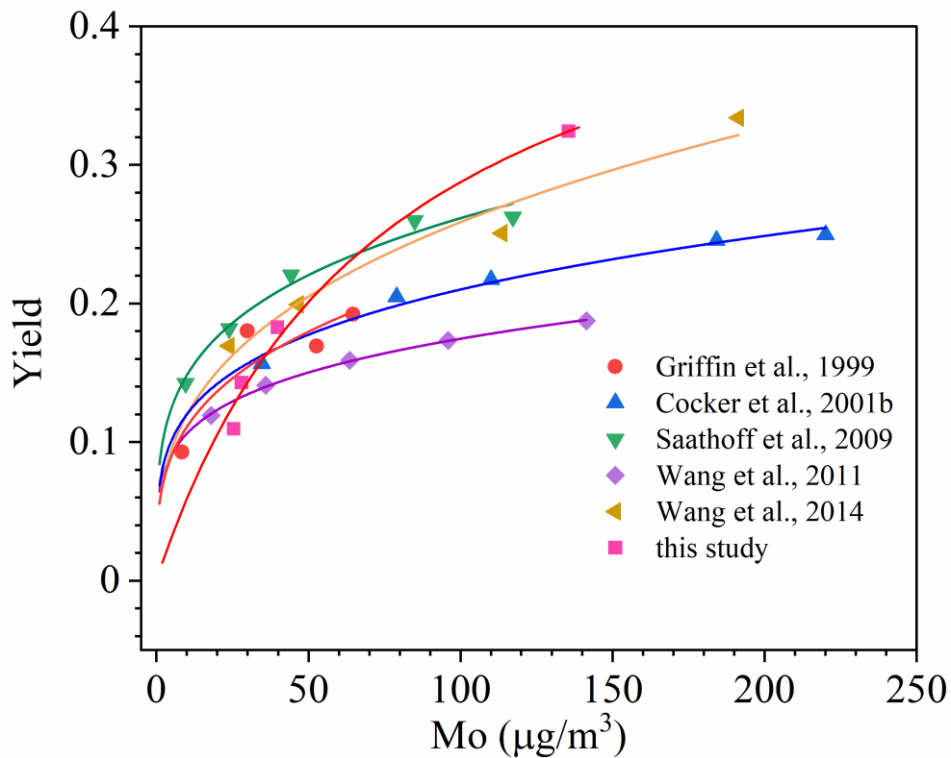
342 Where α_i and $K_{om,i}$ are the mass-based stoichiometric coefficient and partitioning coefficient of
343 the species i , respectively; M_O is the total mass concentration of organic aerosols. Odum et al
344 (1996)¹⁸ found that a two-product model can well fit the SOA yield in chamber studies. The α_1 ,
345 α_2 , $K_{om,1}$ and $K_{om,2}$ is 0.1240, 0.06623, 0.04255, and 0.006476, respectively. Table S7
346 summaries these four parameters reported in literatures. The α_1 , $K_{om,1}$ and $K_{om,2}$ fall in the same
347 range, and α_2 is slightly smaller than other studies indicating that the production of more low-
348 volatility products due to the lower wall loss rate.⁸¹

349 **4.2. Ozonolysis of α -pinene**

350 Ozonolysis of α -pinene was further carried out in the dark to evaluate the flexibility of the

351 chamber in dark chemistry studies. This reaction has been widely studied and numerous data
352 are available in the literature.^{16, 19, 35, 75, 85} The experimental conditions are listed in the Table
353 S8. The initial concentration of α -pinene varied from 44 to 92 ppb. The aerosol density was
354 assumed to be 1.3 g cm^{-3} when converting the volume concentration into the mass
355 concentration. This is equal to that of 1.3 g cm^{-3} used by Bahreini et al (2005)⁸⁶ or Alfarra et al
356 (2006),⁸⁷ but higher than that of 1.0 g cm^{-3} reported by Wang et al (2014)³⁵ or Li et al (2021)⁵
357 for α -pinene SOA.

358 Figure 5 compares the yields of this work and previous studies under the similar
359 conditions, i.e., experiments under dry condition, seed-free, and in the absence of OH
360 scavengers. The SOA yields in this work are from 0.11 to 0.32, which are in the range
361 (0.09~0.33) reported in previous studies.^{19, 35, 85} The yield curve can be well fitted according to
362 two-products model. The α_1 , α_2 , $K_{om,1}$, and $K_{om,2}$ is 0.4626, 0.04287, 0.0134 and 0.01124,
363 respectively. As shown in Table S6, the values of $K_{om,1}$, and $K_{om,2}$ fall in the same range reported
364 in literatures, while α_2 are slightly smaller than other studies, also indicating that the more low-
365 volatile products formed in the chamber due to lower wall loss. In addition, the fitting-curve in
366 this study is steeper than other reports. This may be resulted from the different adsorptive
367 property for initial, intermediate and end species on different-material of the chamber and/or
368 the distribution of oxidation products under different reaction conditions.



369

370 **Figure. 5** Comparison of yield data obtained for α -pinene ozonolysis experiments in BUCT

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chamber with other chamber facilities

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Based on full characterizations, it has been demonstrated that the BUCT chamber can be used to investigate both photochemistry and atmospheric chemistry in the dark related to secondary pollutants formation. Unlike traditional smog chambers made of Teflon film, the quartz chamber does not need to replace the reactor periodically because the inner wall of the reactor is water-washable to significantly reduce the contamination from the deposited pollutants on the walls. After cleaning, the quartz chamber is particularly suitable for studying atmospheric chemical mechanism and kinetics under low background conditions. Compared with other no-Teflon chamber such as CLOUD chamber, the adjustable light intensity (J_{NO_2}) makes our quartz chamber being suitable for simulating the atmospheric photochemistry in different seasons and the diurnal photochemistry in Beijing. This quartz chamber also enables AHL/BUCT being capable of performing field observations and laboratory simulations on the

- 383 transformation of gas-phase pollutants, nucleation, growth, aging and effects of atmospheric
384 aerosols at molecular, cluster, nanometer and micron level.

385

386 **Supporting Information**

387 The Supporting Information is available free of charge at

388 (The description of the quartz chamber; Observation-based model simulation; The worldwide

389 smog chambers used to simulate atmospheric photochemical processes; Instruments of the

390 AHL/BUCT quartz chamber; Comparison of gaseous pollutants wall loss rate of BUCT

391 chamber with other chamber facilities; The wall loss rates of selected protonated intermediates;

392 Comparison of particle wall loss rates of BUCT chamber with other chamber facilities;

393 Experimental conditions and resulting SOA data of toluene photooxidation experiments; Four-

394 parameters summary of two-product model used to simulate aerosol mass and yield;

395 Experimental conditions and resulting SOA data of α -pinene ozonolysis experiments;

396 Comparison of the wavelength region with other indoor chambers; The picture of the

397 AHL/BUCT quartz chamber; Evolution of the temperature inside the chamber; The variation

398 of pressure in a typical experiment; Concentration-time plot of NO_x after each pulse; Measured

399 transmittance and spectrum of 365 nm UV light; The light intensity distribution of different

400 distances from the UV lights; Particle wall loss rate constants for different particle diameter

401 sizes; Mass spectra of H₃O⁺ charged ion measured by Vocus-PTR; The time series of the gas

402 species and diameter in the toluene-NO_x photochemical experiments; The variations of the

403 concentrations of HONO and OH radical; SOA yield of toluene-NO_x photochemical

404 experiments and comparison with other chambers.)

405

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442

443 **Notes**

444 The authors declare no competing financial interest.

445

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