Investigation on the methane adsorption capacity in coals: considerations from nanopores by multifractal analysis

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1   Investigation on the methane adsorption capacity in coals: considerations

2   from nanopores by multifractal analysis

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8   **ABSTRACT:**

9   Methane adsorption properties of coal are essential for coalbed methane (CBM) extraction and clean

10   energy utilization. However, the effect of nanopores on CH_4 adsorption in high volatile bituminous

11   coal and anthracite remains to be revealed. In this work, the multi-dimensional description of

12   nanopores was established using gas adsorption and FIB-SEM experiments. And the heterogeneous

13   features at different sizes were finely quantified by multifractal analysis. Results show that the pores

14   with size smaller than 100 nm, as storage section, are isolated in the space. The nanopores of the

15   sample LHG have stronger heterogeneity in multiple dimensions. The pore size distributions with

16   apparent aggregation are composed of 0.45-0.70 nm (from CO_2 adsorption), 2-50 nm (from N_2

17   adsorption) and 10-50 nm (from FIB-SEM). Nanopore structure affects the adsorption capacity of

18   CH_4 mainly in micropore structure, pore morphology and heterogeneity. The well-developed

19   micropore structure is conducive to methane enrichment. The ink-bottle pores with the higher

20   specific surface area are beneficial to gas storage, whereas plate-like/slit-like pores will facilitate

21   the desorption and diffusion of gas. The more robust pore heterogeneity in the range of 0.45-0.70

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22   nm and 2-50 nm significantly contribute to methane adsorption. This work may allow significant

23   insights into the interaction of coal with gases during enhancing CBM recovery.

24   **Keywords:** Coalbed methane; Nanopore; Adsorption; FIB-SEM; Multifractal analysis

25

1. INTRODUCTION

27   Coalbed methane (CBM) reservoir has been a hotspot as a result of the development of greenhouse

28   gas control and clean energy utilization. Methane is generally stored in coal by the adsorption

29   mechanism [1]. The adsorption behavior may restrict the production of CBM reservoirs and threaten

30   the safety of the coal mining process [2-5]. Due to the different physical and chemical properties of

31   coals, the governing factors of CH_4 adsorption capacity are quite complicated [6-15]. An emerging

32   number of studies on methane adsorption has been carried out, focusing on coal rank, temperature,

33   moisture content and coal composition [6-12]. Besides, many current pieces of research noticed the

34   influence of pore structure on gas adsorption, including pore specific surface area (SSA) [13, 14], pore

35   volume [15, 16], pore size distribution (PSD) [17, 18] and surface roughness [19, 20]. The International Union

36   of Pure and Applied Chemistry (IUPAC) established the classification consisting of micropores (<2

37   nm), mesopores (2-50 nm) and macropores (>50 nm) [21]. Nanopore with the pore size smaller than

38   100 nm, as an essential component in the pore-fracture structure, will significantly affect the

39   adsorption mechanism [19, 22, 23]. However, there are still many controversies about the control effect

40   of methane adsorption capacity [24]. For example, regarding the effect of SSA of the micropores,

41   some scholars believed that the larger SSA will provide more adsorption sites, hence the CH_4

42   adsorption capacity will be higher [13, 14]. But Byamba investigated that the comparison chart of BET-

43   SSA and CH_4 adsorption capacity may be invalid in the microporous adsorbent [25].

2

44   The commonly used methods for characterizing nanopore structure in coal contain mercury

45   intrusion porosimetry (MIP) and gas adsorption (CO_2 and N_2). The MIP method can assess the

46   porosity distribution with size above 3 nm [26], whereas the coal matrix will be compressed and the

47   narrow pores will be damaged at the applied pressure > 10 MPa [27]. Gas adsorption (CO_2 and N_2) is

48   more advantageous for the analysis of nanopores. Low-temperature N_2 adsorption is powerful for

49   evaluating mesopores and parts of macropores [28], but cannot effectively access the features of

50   micropores. The CO_2 molecule is endowed with high saturated vapor pressure and fast diffusion

51   speed at 273 K [29]. Meanwhile, CO_2 with a kinetic diameter of 0.33 nm is allowed to enter pores less

52   than 1 nm, thus it is usually used as an ideal gas for analyzing micropores of coal. The combination

53   of CO_2 and N_2 adsorption methods can characterize the nearly full nano-scale pore structure.

54   However, subjecting to the test mechanism constraints, the spatial distribution is difficult to be

55   obtained. Therefore, advanced techniques including X-ray nano-tomography (Nano-CT) and

56   focused ion beam-scanning electron microscopy (FIB-SEM) are also introduced to evaluate the pore

57   structure [30]. The latter is chosen in this work because of its higher resolution (~ 10nm/pixel).

58   This work aims at shedding light on the following issues: 1) multi-dimensional description of

59   nanopores through gas adsorption (CO_2 and N_2) and FIB-SEM techniques; 2) the multi-

60   heterogeneity of nanopore structures by multifractal analysis; 3) the effect of nanopores on CH_4

61   adsorption.

62   **2. MATERIAL AND METHODS**

63   **2.1. Coal Sampling and Analysis**

64   One high volatile bituminous coal and one anthracite were collected from the Junggar Basin and

65   Qinshui Basin of China, which were carefully packaged and then transported to the laboratory for

3

66 experiments. A summary of the sample information, including maximum vitrinite reflectance ($R_{o,m}$),

67 helium porosity, maceral and proximate analysis, is provided in Table 1. The standards used in

68 these tests are the Chinese National Standard GB/T 6948-2008 ($R_{o,m}$), the Chinese Oil and Gas

69 Industry Standard SY/T 5336-1996 (helium porosimetry test), the Scheme of the International

70 Committee of Coal Petrology (coal macerals)[31] and the Standard of ASTM D7582-15

71 (proximate analysis). Detailed experiment procedure is displayed in our previous research [27]. The

72 initial cubic samples with ~0.5 cm × 1 cm × 1 cm were adopted in the FIB-SEM tomography. The

73 samples used in the gas adsorption (CH_4, CO_2 and N_2) experiments were the powder samples of 60-

74 80 mesh.

75

Table 1. Properties of selected coal samples

Sample ID	$R_{o,m}$ (%)	Basins	Maceral and mineral (vol%)				Porosity (%)	Permeability (mD)	Langmuir parameters	
			V	I	E	M			V_L (m³/t)	P_L (MPa)
LHG	0.98	Junggar	53.40	19.70	0.37	26.50	9.56	0.21	35.98	0.71
L-1	2.73	Qinshui	66.80	14.40	0.00	18.80	5.37	0.011	34.81	1.06

76 Note: V- Vitrinite; I - Inertinite; E - Exinite; M- Mineral.
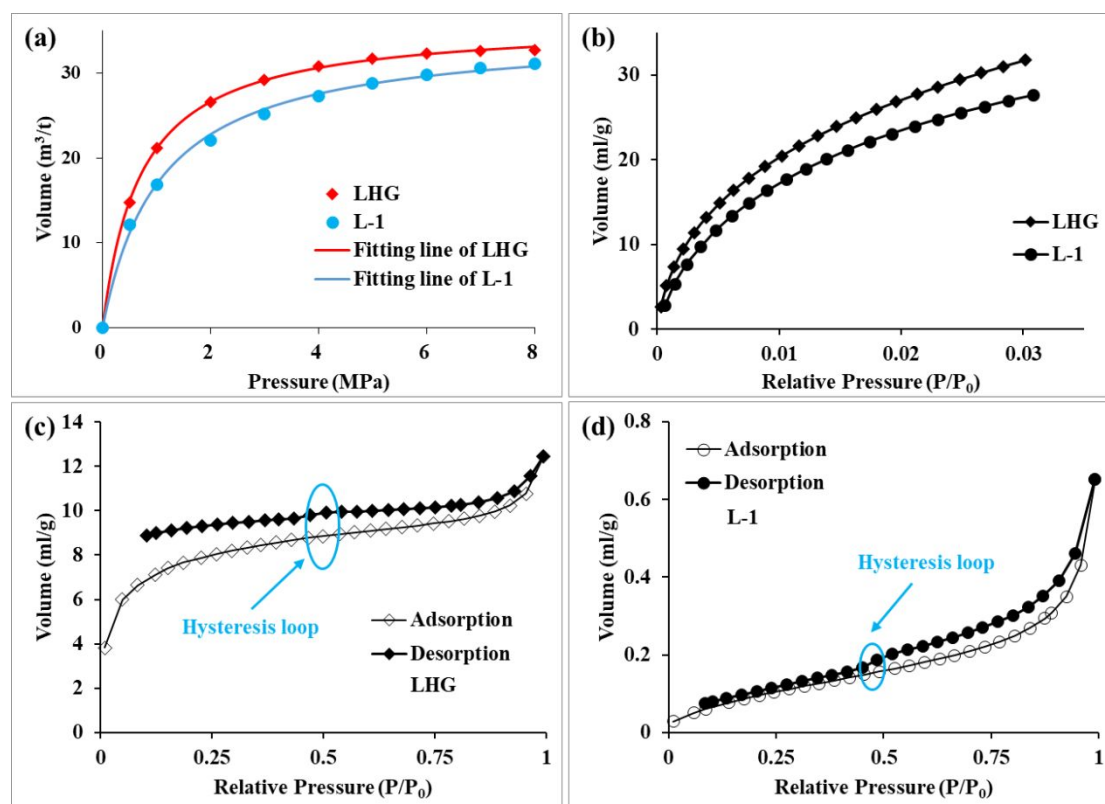
77 **2.2. Gas Adsorption Experiments and FIB-SEM Tomography**

78 The gas adsorption experiments were carried by CO_2 adsorption, low-temperature N_2

79 adsorption/desorption, and CH_4 isotherm adsorption. The coal samples of 60-80 mesh first dried for

80 48 h. Both CO_2 adsorption and low-temperature N_2 adsorption/desorption measurements were

81 performed with a Micromeritics ASAP-2460 specific surface analyzer. The corresponding

82 temperatures of CO_2 adsorption and low-temperature N_2 adsorption/desorption measurements are

83 273 K and 77 K, respectively. The density functional theory (DFT) [32] molecular model was adopted

84 herein to obtain the pore size distributions (PSD) from CO_2 adsorption in the range of 0.489-1.083

85 nm and N_2 adsorption in the range of 2-100 nm, respectively. DFT can be used to better capture the

86 thermodynamic behavior and density distribution of fluids at the molecular level, and then a more

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87   reliable curve of PSD can be assessed [3, 24, 33, 34]. Besides, CH_4 adsorption experiments corroborated

88   the adsorption capacity of the two samples were conducted at 30 °C using the TerraTek Isotherm

89   Measurement System (IS-100), obeying the Chinese National Standard of GB/T 19560-2008. The

90   curves of CH_4 adsorption experiments are displayed in Figure 1a. The Langmuir volume (V_L) and

91   Langmuir pressure (P_L) were provided by Langmuir model [35], as shown in eq 1:

92     $$V = \frac{PV_L}{P + P_L}$$ (1)

93   where V is the volume of adsorbed methane, m^3/t; P is the pressure, MPa; V_L is the Langmuir

94   volume and represents the maximum volume of coal, m^3/t; P_L is the Langmuir pressure

95   corresponding to the 50% of maximum adsorption capacity, which can evaluate the difficulty of

96   adsorbing methane in CBM reservoirs, MPa.

98   **Figure 1.** The isotherms of gas adsorption experiments. (a)-CH_4 adsorption, (b)-CO_2 adsorption, (c-d)
99   low-temperature N_2 adsorption/desorption isotherms.

100   With FIB-SEM tomography when a polished coal sample is exposed to a dual-beam (ion and

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101   electron) system, the selected area is then cut and imaged. The experimental instrument is Zeiss

102   Crossbeam540. The high-resolution images (10 nm/pixel) obtained can make the research scale

103   reach the nanometer level. To perform subsequent multifractal analysis, the size of the studied

104   domains must meet the requirement of being larger than the representative elementary volume (REV)

105   [36]. The sizes of REV have been determined (80 pixels for LHG and 280 pixels for L-1) in our

106   published work [37], so choosing the size of the studied domains to be $512 \times 512 \times 512$ voxels is

107   sufficient.

108   **2.3. Multifractal Analysis**

109   As an extension of fractal theory [38], the multifractal analysis can show more details in complex

110   porous media. The single fractal dimension usually used reflects more the overall characteristics of

111   PSD, rather than focusing on local differences. Multifractal analysis can decompose self-similar

112   measures into interlacing fractal sets and separate the complex fractal structure into several parts [33,

113   38-40]. And it can be distinguished by the singularity strength and generalized dimension. There are

114   mainly two methods to perform the multifractal analysis including the box-counting method and

115   wavelet method [38], and the former is adopted herein due to the features of pore system in coal [33, 37,

116   41]. Method in this class obeys the following steps:

117   First, a series of boxes with the same length ε is used to cover the signal interval and they are labeled

118   with i. Besides, $N(\varepsilon)$ represents the number of boxes required completely to overlay the signal

119   interval. In this work, relative pressure data in gas adsorption (CO_2 and N_2) experiments was

120   considered as the signal interval. The probability mass function in the i-th box can be defined by eq

121   2:

122     $$P_i(\varepsilon) = \frac{N_i(\varepsilon)}{N_t} \tag{2}$$

123   where $N_i(\varepsilon)$ is the gas adsorption volume in the i-th box; N_t is the total gas adsorption volume.

124    $P_i(\varepsilon)$, the probability mass, follows an exponential function with the length ε of the box, which can

125   be expressed as:

126    $$P_i(\varepsilon) \sim \varepsilon^{\alpha_i} \tag{3}$$

127   where α_i is the Lipschitz-Hölder singularity exponent, which reflects the local singularity

128   strength of the mass probability function $P_i(\varepsilon)$, and its value is relevant to the current position of

129   the box on the research interval [39].

130   When the values of α are same, the number of the boxes is marked as $N_\alpha(\varepsilon)$, following the eq 4:

131    $$N_\alpha(\varepsilon) \propto \varepsilon^{-f(\alpha)} \tag{4}$$

132   where $f(\alpha)$ is the fractal dimension of the fractal subset labeled by the singularity exponent α.

133   The curve composed of α and $f(\alpha)$ is recorded as the multifractal singularity spectrum, which

134   can indicate the heterogeneous distribution of gas adsorption on the fractal structure, thereby

135   providing more detailed structural information than single fractal. After that, $\alpha(q)$ and $f(\alpha)$ can

136   be determined by the eqs. 5 and 6 proposed by Chhabra and Jensen [42]:

137    $$\alpha(q) \propto \frac{\left[\sum_{i=1}^{N(\varepsilon)}(u_i(q,\varepsilon)\times\ln p_i(\varepsilon))\right]}{\ln(\varepsilon)} \tag{5}$$

138    $$f(\alpha) \propto \frac{\left[\sum_{i=1}^{N(\varepsilon)}(u_i(q,\varepsilon)\times\ln u_i(\varepsilon))\right]}{\ln(\varepsilon)} \tag{6}$$

139   where

140    $$u_i(q,\varepsilon) = \frac{p_i(\varepsilon)^q}{\sum_{i=1}^{N(\varepsilon)} p_i(\varepsilon)^q} \tag{7}$$

141   where q is the order of the statistical matrix and ranges from -∞ to +∞. Herein, the value of q is an

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142 integer within [-10, 10] for successive unit steps. When $q > 0$, it represents the high concentration

143 area of the PSD; whereas the low concentration area of PSD is focused for $q < 0$. Besides, the

144 partition function of moment of order q for multifractal analysis can be expressed as eq 8 [42]:

145
$$u(q,\varepsilon) = \sum_{i=1}^{N(\varepsilon)} p_i(\varepsilon)^q \propto \varepsilon^{\tau(q)} \tag{8}$$

146 where $\tau(q)$ is the mass scaling function of the order q, which can be calculated by:

147
$$\tau(q) = -\lim_{\varepsilon \to 0} \frac{\ln \sum_{i=1}^{N(\varepsilon)} p_i(\varepsilon)^q}{\ln(\varepsilon)} \tag{9}$$

148 The relationship between the generalized dimension (D_q) and the order (q) can be obtained by eq 10

149 [39]:

150
$$D_q = \frac{\tau(q)}{q-1} \tag{10}$$

151 For the monofractal, the relation of D_q and q is a constant and shows no richer information as q

152 changes. In the multifractal analysis, the plot of D_q versus q is not a constant function. In this regard,

153 the most commonly used generalized dimensions are D_0, D_1 and D_2 corresponding to q = 0, 1, 2 [43,

154 44], which are known as capacity, information (Shannon entropy), and correlation dimensions,

155 respectively. The capacity dimension D_0 can show the global characteristics of the system, which is

156 independent of q and the probability of the pores in the box. The information dimension, D_1,

157 evaluates the degree of disorder in the PSD curves. The larger value of D_1 represents the smaller

158 fluctuation of the local pore volume distribution and the higher uniformity of the pore distribution

159 in each pore size interval. As the correlation dimension, D_2 captures the behavior of the second

160 sampling moment and can indicate the degree of spatial autocorrelation of the measures.

161 Meanwhile, in order to make the function D_q continuous, D_1 can be acquired by the Law of

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162　Robida when $q = 1$ [45]:

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$$D_1 = \lim_{\varepsilon \to 0} \frac{\sum_{i=1}^{N(\varepsilon)} p_i(\varepsilon) \ln p_i(\varepsilon)}{\ln(\varepsilon)} \qquad (11)$$

164　The value of D_1 close to 1 means uniform distribution of the system on all scales; on the contrary,

165　D_1 close to 0 represents a concentration of irregularities in the subset of scales [43]. Subsequently, the

166　calculated D_q and q constitute the generalized multifractal dimension spectrum.

167　Besides, D_2 also can be defined as eq 12 following Riedi et al. [46]:

168　$D_2 = 2H - 1$ 　　　　　　　　　　　　　　　　　　　　　　　　　　　　(12)

169　where H is named as the Hurst exponent, which shows the positive autocorrelation and/or spatial

170　long-range variations [45].

171　**3. RESULTS AND DISCUSSION**

172　**3.1. Characteristics of the Nanopores Structures**

173　Figure 1b shows the curves of CO_2 adsorption for the two selected coals, which illustrates the

174　adsorption volume gradually increases under the low-pressure condition. Compared with the results

175　of other studies [16, 24, 47, 48], it can be noticed by the relatively high CO_2 adsorption capacity in our

176　samples, indicating that the samples have a high accessibility of CO_2 and/or the well-developed

177　micropore structure [49]. The curves of N_2 adsorption/desorption at 77 K are displayed in Figure 1c-

178　d, which their shapes conform to the Type II reversible isotherms according to the IUPAC

179　classifications [21]. The isotherms represent the process of unlimited monolayer-multilayer adsorption,

180　and the starting point of the middle linear part means the completed monolayer coverage and the

181　unstart multilayer adsorption [50]. Hysteresis loops with changeable shapes can indicate different

182　types of pores, which may be related to the capillary condensation in the mesopores [27]. The

9

183   hysteresis loops appearing in Figure 1c-d can be classified into Type H4 (sample LHG) and Type

184   H3 (sample L-1), respectively [29, 50]. The Type H4 loop can be related with narrow slit-like pores,

185   the more obvious uptake at low P/P_0 being attributed to the filling of the micropores. The Type H3

186   loop is attributed to the non-grid aggregates of plate-like particles.

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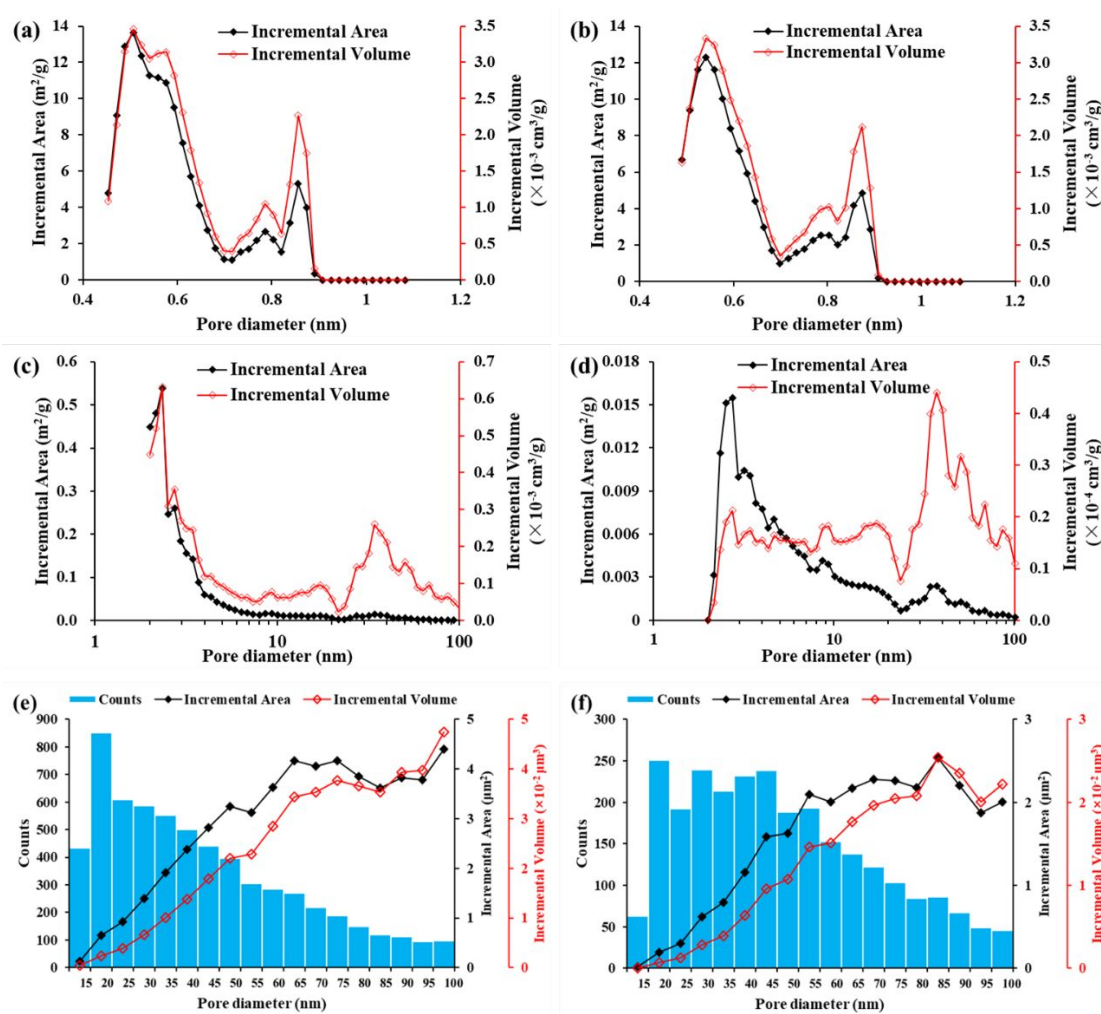
Figure 2. Pore size distribution curves from CO_2 adsorption (a-b), N_2 adsorption (c-d) and FIB-SEM
189   experiment (e-f). The left is sample LHG and the right is sample L-1.

190   Figure 2 shows the PSD curves of gas adsorption (CO_2 and N_2) and FIB-SEM experiments, which

191   indicate the nanopores from micropores to macropores are developed in two samples. The detecting

192   nanopores from three techniques exhibit various curves due to the distinct principles (including the

193   limited resolution of FIB-SEM and the existence of dead pores). The pore structure parameters from

194   the experiments were summarized in Table 2. The information detected by CO_2 adsorption shows

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195 that the micropores of the two samples are both well-developed, with a large specific surface area

196 up to 121.70-144.48 m^2/g. And the results of N_2 adsorption reveal that the mesopores contribute the

197 most to the pore volume and SSA, followed by the macropores. The data of FIB-SEM shows that

198 the contribution of macropores is the larger.

199 **Table 2.** Pore structure information from CO_2 adsorption, N_2 adsorption and FIB-SEM experiments

| Sample ID	N_2 adsorption		PVF (%)		SSAF (%)		CO_2 adsorption		FIB-SEM		PVF (%)		SAF (%)	
	PV*	SSA*	meso	macro	meso	macro	PV*	SSA*	PV**	SSA**	meso	macro	meso	macro
LHG	0.00687	2.667	90.20	9.80	99.26	0.74	0.0431	144.48	0.434	52.06	17.76	82.24	25.81	74.19
L-1	0.00098	0.193	79.59	20.41	97.41	2.59	0.0381	121.70	0.235	27.91	15.09	84.91	22.58	77.42

200 Note: PVF-Pore volume fraction, %; SSAF-Specific surface area fraction, %; SAF-Specific area fraction, %; PV*-
201 pore volume, cm^3/g; SSA*-specific surface area, m^2/g; PV**-pore volume, μm^3; SSA**-specific surface area, μm^2;
202 meso-mesopore; macro-macropore.

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204 Figure 3 shows the characteristics of pores in 2D FIB-SEM slices of two samples. In particular,

205 Figure 3b displays a typical example of multi-level pore transport channel. It can be clearly observed

206 that the body of the channel is composed of multi-level pores, and the connected parts are constituted

207 by narrow throats. The nanopores scattered around provide space for CH_4 adsorption. As illustrated

208 in Figure 4, the nanopores of different sizes will be extracted from the data obtained by FIB-SEM

209 to reconstruct 3D volume and visualize the spatial distribution features. From Figure 2e-f and Figure

210 4, it can be concluded that the number of nanopores at different sizes in sample LHG is markedly

211 more than that in sample L-1. The mesopores and macropores (see Figure 4a-d) relatively dispersed

212 in space constitute the main storage space of methane, which is consistent with the 2D observation.

213 After analyzing the connectivity of pores (see Figure 4e-f), it is indicated that the connectivity of

214 pores in the selected domain of sample LHG is better, whereas the connected pores appear in the

215 magnified domain of sample L-1. Besides, the connected parts are mainly composed of pores larger

216 than 100 nm. Previous studies have confirmed that nanopores are mainly used as storage space for

217 methane rather than migration channel [19, 22], thus connectivity is not the main characteristic. The

11

218   pores above 100 nm will serve as a bridge to transport the desorbed methane to fracture network

219   during the industrial production process.
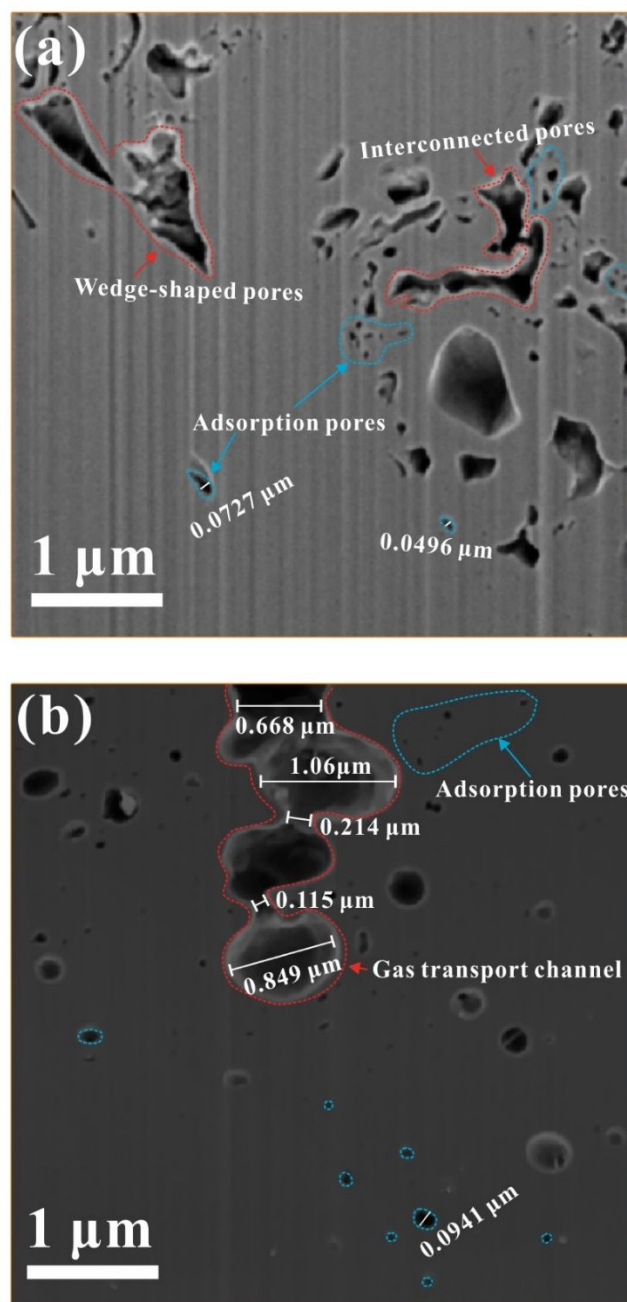
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221   **Figure 3.** The pore characteristics from samples LHG (a) and L-1 (b) based on 2D slices in FIB-SEM
222   tomography. (a) shows various pore morphologies and adsorption pores. (b) exhibits a typical multi-level
223   transport channel.

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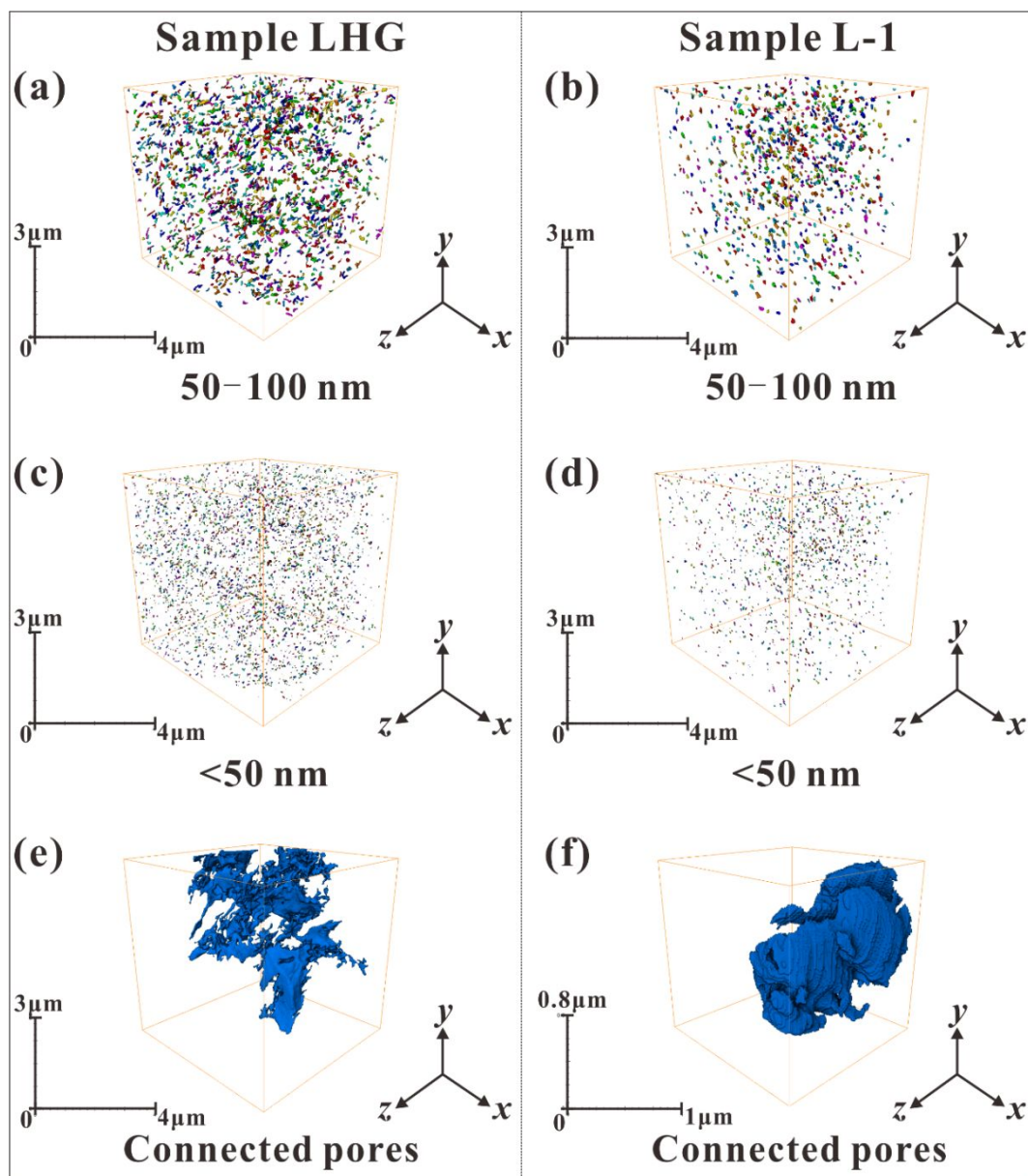
Figure 4. The 3D characteristic spatial distribution of nano-scale pores and connected pores. The left and right columns are sample LHG and sample L-1, respectively. (a) and (b) are the pores with pore diameter ranging from 50-100 nm; (c) and (d) are the pores with pore diameter less than 50nm; (e) and (f) are the connected pores of selected regions.

3.2. Multifractal Analysis from Gas Adsorption Experiments and FIB-SEM Tomography

The nanopores obtained from gas adsorption (CO_2 and N_2) isotherms and FIB-SEM data are rather

heterogeneous in the selected samples. The multifractal analysis, a powerful tool for heterogeneity

analysis, can be used to reveal these experimental data contained additional information [33, 36, 38, 43,

[51]. The different results of CO_2/N_2 adsorption and FIB-SEM are described separately here.

3.2.1 Gas Adsorption Experiments

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235 Based on the calculated results from CO_2/N_2 adsorption experiments, the double logarithmic curves

236 of the partition function $u_i(q,\varepsilon)$ and the measurement scale ε ranging from -10 to 10 of the

237 successive intervals of $q=1$ are drawn in Figure 5, and it can be found that there is a significant

238 linear relationship (R^2 value > 0.90). Previous studies have confirmed that if the relationship

239 between $u_i(q,\varepsilon)$ and ε obeys a power-law scaling, multifractal behavior can be captured in the

240 PSD of the two samples ranging from micropores to mesopores and macropores [43, 45, 52]. The law of

241 $\ln\varepsilon$-$\ln u(q,\varepsilon)$ is completely opposite when $q<0$ and $q>0$, showing a decreasing and increasing trend,

242 respectively. And the fitting lines close to each other indicate that most of the data are clustered in

243 the small domain of the research scale [33, 43]. The generalized multifractal dimension spectrum

244 constituted by D_q and q display a monotonously decreasing curve and $D_0 > D_1 > D_2$, which also

245 supports the existence of multifractal behavior in the nanopores. Parts of parameters are summarized

246 in Table 3. The closer the value of D_1 is to D_0, the more even the pores are distributed in a specific

247 pore size range. Conversely, the smaller value of D_1 represents the denser pores and the more uneven

248 pore distribution [45]. Table 3 shows that the D_1 of samples LHG and L-1 are 0.9067 and 0.9243 in

249 the micropores, which means that the micropore distribution of sample LHG is more uneven. In the

250 meso-macropores detected by the N_2 adsorption experiment, the D_1 value of sample LHG is 0.6191,

251 which is lower than the sample L-1 with 0.7583, indicating the former has a more complex

252 distribution of meso-macropore structure. The H value (Hurst exponent) can be adopted to evaluate

253 the connectivity of pores in the PSD at different sizes, which may further affect the permeability [33].

254 A smaller H value corresponds to poor pore connectivity. As shown in Table 3, the H values of the

255 micropores are 0.8953 (for sample LHG) and 0.9192 (for sample L-1), representing that the

14

256   connectivity of the micropores in sample L-1 is better. The H values of the meso-macropore are

257   0.6932 (for sample LHG) and 0.7689 (for sample L-1), indicating that the pore connectivity with

258   the range of 2-100 nm in sample L-1 is better. This phenomenon may be related to the plate/slit-like

259   pore shape in sample L-1. The connected channels may be more likely to be produced in plate-liked

260   aggregates, and the narrow necks of ink-bottle pores are not conducive to connectivity.
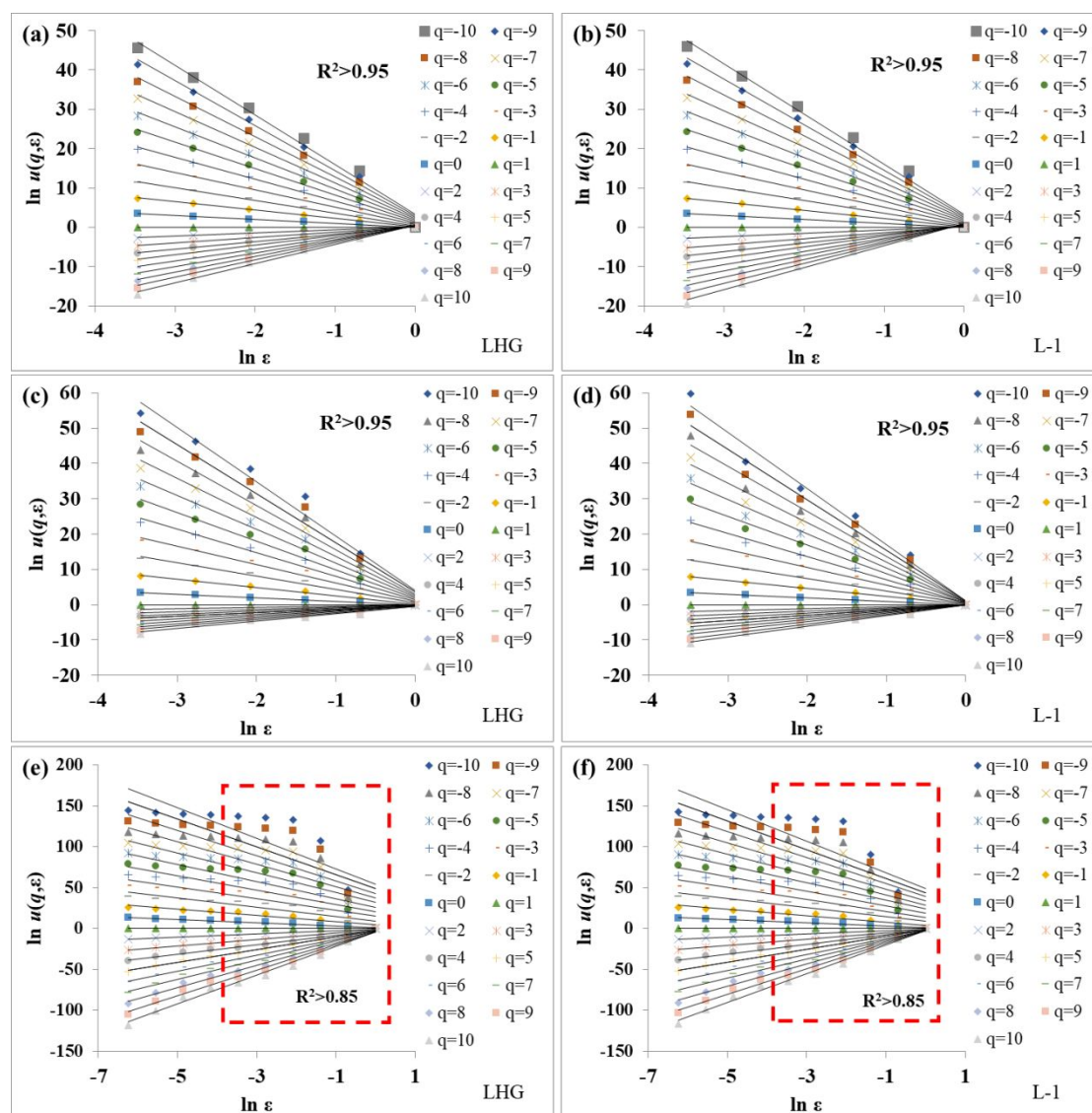

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262   **Figure 5.** Plots of the partition function at different order q from CO_2 adsorption (a-b), N_2 adsorption
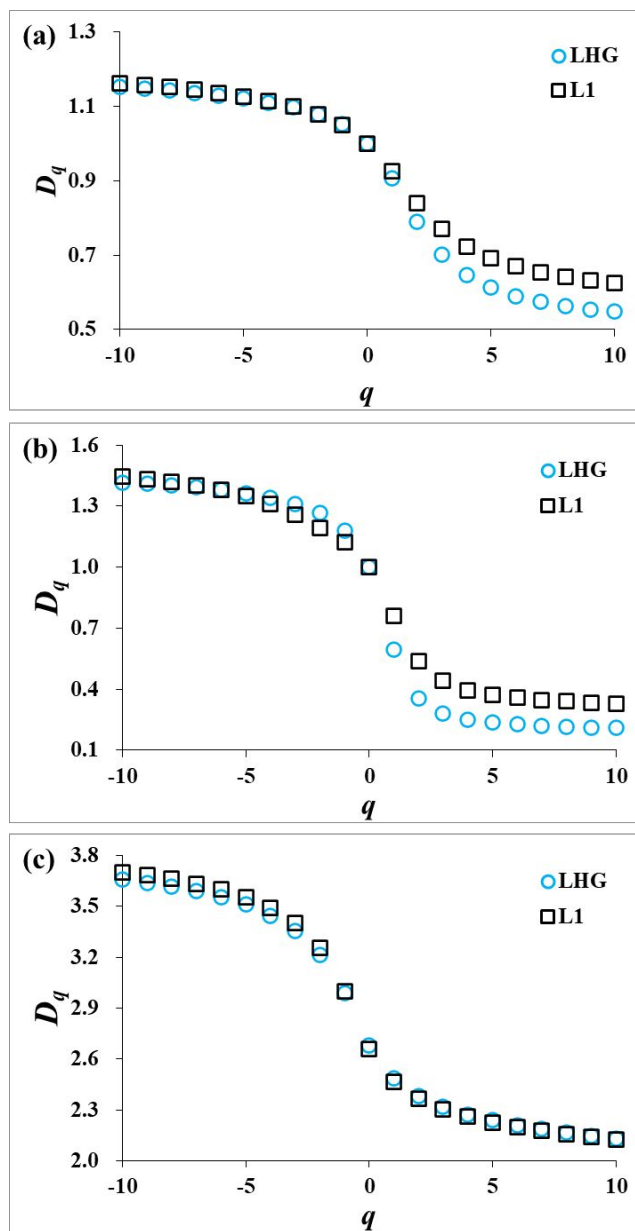
263   (c-d) and FIB-SEM experiments (e-f).

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267   **Table 3.** Multifractal analysis parameters from CO_2 adsorption, N_2 adsorption and FIB-SEM experiments

Parameters	CO_2 adsorption		N_2 adsorption		FIB-SEM	
	LHG	L-1	LHG	L-1	LHG	L-1
D_0	1.000	1.000	1.000	1.000	2.679	2.657
D_1	0.907	0.924	0.596	0.758	2.485	2.465
D_2	0.791	0.838	0.357	0.538	2.384	2.366
H	0.895	0.919	0.678	0.769	1.692	1.683
$D_{10-}-D_{10+}$	0.605	0.538	1.207	1.115	1.527	1.574
$D_{10-}-D_0$	0.152	0.162	0.417	0.445	0.979	1.044
D_0-D_{10+}	0.453	0.376	0.791	0.670	0.548	0.530
α_0	1.070	1.062	1.273	1.175	2.948	2.936
R_d	0.447	0.344	0.870	0.491	0.058	-0.015

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269   The spectrum width of the generalized multifractal dimension spectrum ($D_{10-} \sim D_{10+}$) can reflect the

270   degree of heterogeneity of PSD in a local area, which the higher value corresponds the stronger

271   heterogeneity of PSD within a certain pore size range. As displayed in Table 3, the micropores and

272   meso-macropores in the sample LHG have the larger spectrum width, indicating that the pores in

273   the sample LHG are more heterogeneous in the range of <100 nm. This result confirms the

274   rationality of the D_1 analysis. Besides, the spectrum widths on the left ($D_{10-} \sim D_0$, $q<0$) and right

275   ($D_0 \sim D_{10+}$, $q>0$) can show the characteristics of the low-value area and high-value area of the pore

276   volume, respectively [45]. Figure 2a-b demonstrate that the maximum pore volume in the micropores

277   is between 0.45-0.70 nm, and the pore volume in this range is greater than 0.70-1.08 nm. Thus, it

278   can be judged that $D_{10-} \sim D_0$ and $D_0 \sim D_{10+}$ can represent pore heterogeneity in the range of 0.7-1.08

279   nm and 0.45-0.70 nm, respectively. In the selected samples, the pores ranging from 0.45 to 0.70 nm

280   are more heterogeneous than that of in the range of 0.70-1.08 nm. The same procedure may be easily

281   utilized to find that the left and right spectrum widths in meso-macropores indicate pore

282   heterogeneity in the range of 50-100 nm and 2-50 nm, respectively. Obviously, Figure 6 displays

283   that the right spectrum width is larger than that on the left in micropore and meso-macropore of the

284   two samples, which means the distribution in the range of 2-50 nm is more complex.

Figure 6. Relation between the generalized dimension (D_q) and the moment order (q) of the samples from CO_2 adsorption (a), N_2 adsorption (b) and FIB-SEM experiments (c).

288   Another important element is the multifractal singular spectrum [α, $f(\alpha)$] presenting an upwardly

289   convex parabolic shape, which proves the multifractal behavior of PSDs in these samples [33, 53]. This

290   curve is tangent to the internal bisector $f(\alpha)=\alpha$ (see Figure 7) [36], which confirms the accuracy of our

291   calculation. The parameter α_0 is used, which its higher value is regarded as more obvious local

292   agglomeration of pores, to reflect the degree of concentration of PSD. The results in Table 3 indicate

17

293   that the PSD concentration of micropores and meso-macropores of sample LHG is higher than that

294   of sample L-1. Here R_d is used to observe the deviation degree of the multifractal singular spectrum

295   from the center, that is, $R_d=[(\alpha_0-\alpha_{10+})-(\alpha_{10-}-\alpha_0)]$ [54]. The results show $R_d >0$ in micropores and meso-

296   macropores, which means that the high probability density region of pores significantly affects the

297   pore volume distribution. Besides, the relation between $\tau(q)$ and q displayed in Figure 8 demonstrate

298   increasing convex curves in the three experiments, which is consistent with the characteristics of

299   multifractal analysis. Compared with $q>0$, the increasing trend is more significant when $q<0$.
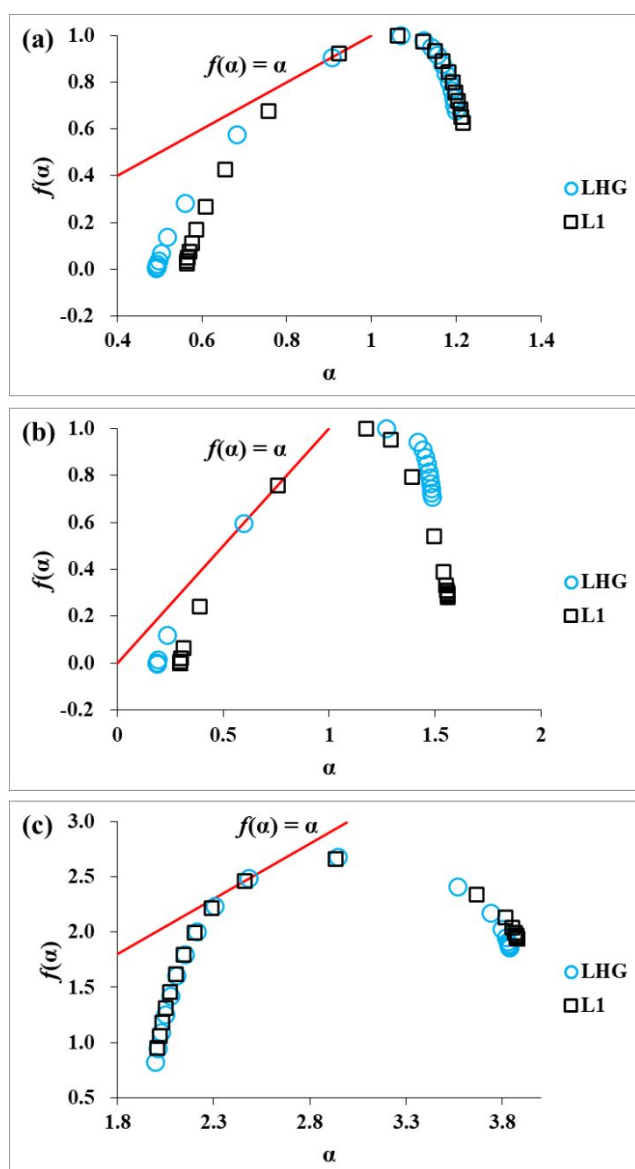
300
301   **Figure 7.** The multifractal singularity spectra [$f(\alpha)$- α] of the selected samples from CO_2 adsorption (a),
302   N_2 adsorption (b) and FIB-SEM experiments (c). And the red line is $f(\alpha) = \alpha$. The curve of [$f(\alpha)$- α] being

303   tangent to the line of $f(\alpha)=\alpha$ proves the accuracy of the calculation.

304
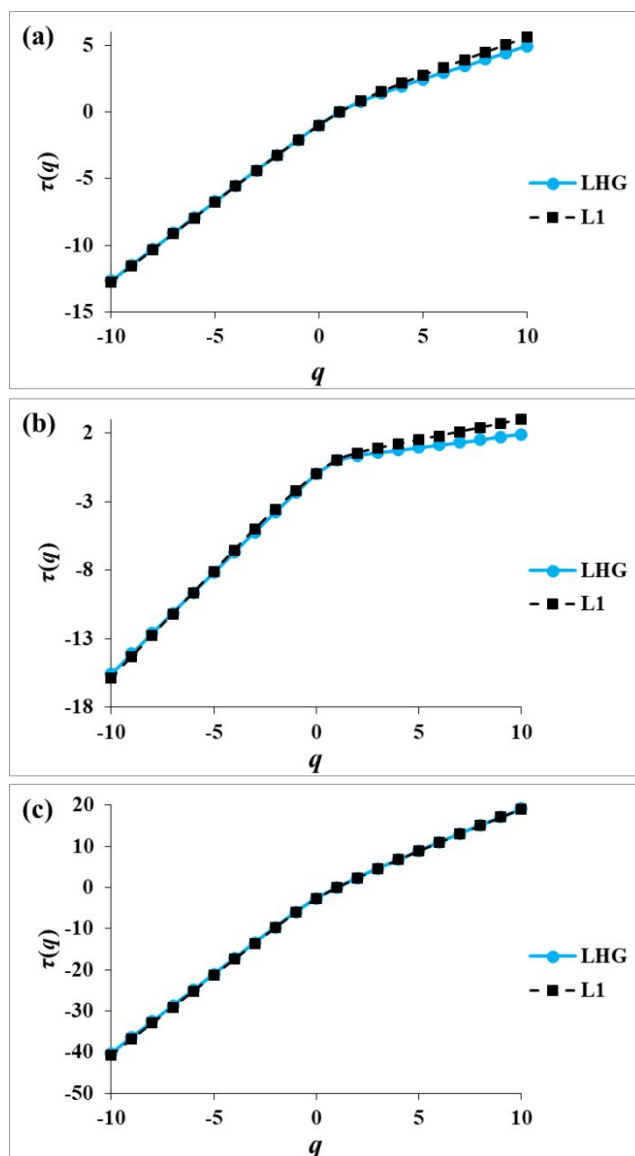
Figure 8. Relation between $\tau(q)$ and q from CO_2 adsorption (a), N_2 adsorption (b) and FIB-SEM

306   experiments (c).

307   **3.2.2 FIB-SEM Tomography**

308   Prior to perform FIB-SEM multifractal analysis, a key step is to determine the range of scale used

309   for calculation [51, 55]. The maximum scales of the selected samples are $512 \times 512 \times 512$ voxels, but

310   the minimum scales should also be determined. This depends on the nearly linear part of the bi-log

311   plots of partition function $u(q,\varepsilon)$ and ε illustrated in Figure 5. Therefore, unlike linear correlation

312   coefficients $R^2 > 0.95$ in CO_2 adsorption and N_2 adsorption isotherms, the R^2 values of the linear part

313   in FIB-SEM are accepted to be greater than 0.85 (see the red rectangular frames in Figure 5e-f). The

19

314   minimum scale is set to 2^4 pixels. Only nanopores smaller than 100 nm are selected and analyzed

315   in FIB-SEM experiment, resulting in not all boxes containing pores. Therefore, D_0 is not equal to 3,

316   but a value between 2-3. Both the monotonic decrease in Figure 6c and the monotonic increase in

317   Figure 8c capture the multifractal behavior of the PSD in FIB-SEM. A higher H value indicates

318   better connectivity between the pores in the sample LHG. It differs from the results of the N_2

319   adsorption analysis, which may be due to the limited resolution that cannot detect pores below 10

320   nm, leading to underestimate pore connectivity of the sample L-1. It also demonstrates that the pores

321   of 2-10 nm may act as the medium connecting the pores. Combining Table 2 and Fig 2e-f, it can be

322   concluded that the left side ($D_{10-} \sim D_0$, $q<0$) and the right side ($D_0 \sim D_{10+}$, $q>0$) reflect the features of

323   pores in the range of 10-50 nm and 50-100 nm, respectively. The spectrum width on the left is larger

324   than that on the right shown in Table 3, which means that the pore heterogeneity of 10-50 nm is

325   stronger. The α_0 value of sample LHG is slightly higher than that of sample L-1, indicating that the

326   local agglomeration of pores in the former is more obvious. Table 3 shows that the R_d of sample

327   LHG is greater than 0, while the R_d of sample L-1 is less than 0, indicating that their PSDs are

328   dominated by the high probability density area and the low probability density area, respectively.

329   Besides, it is worth noting that the parameter difference of N_2 adsorption is more significant than

330   that of FIB-SEM. This may include two reasons: 1) the limited resolution of FIB-SEM cannot detect

331   pores of 2-10 nm; 2) N_2 adsorption only focuses on open pores, but FIB-SEM will also show closed

332   pores.

3.3. Impacts of The Nanopores on Methane Adsorption

334   The samples LHG and L-1 were collected from Junggar Basin and Qinshui Basin, which are two

335   active and typical CBM areas in China [56, 57]. Lots of previous studies have indicated that the coal

336   samples in these two basins are markedly various (as shown in Table 4) [27, 56-58]. Therefore, these

337   selected samples are representative to compare the differences of pore structures between a high

338   volatile bituminous coal and an anthracite. The V_L values are 43.37 m³/t (sample LHG) and 38.37

339   m³/t (sample L-1) as shown in Table 1, meaning the great CH_4 adsorption capacity. Previous studies

340   showed that the high-rank coals tend to have higher CH_4 enrichment capacity compared with low-

341   rank coals [6-8]. Nevertheless, the methane adsorption capacity of sample LHG (high volatile

342   bituminous coal) is stronger than that of sample L-1 (anthracite) in our study. It should be started

343   with the pore characteristics to explore the direct cause of this phenomenon. The first thing to note

344   is when the volume and SSA of pores with size of 2-100 nm in sample L-1 are several orders of

345   magnitude lower than those of sample LHG (see Table 2), the V_L value of sample L-1 can still be

346   as high as 34.81 m³/t. As illustrated in Figure 9, the micropore occupies an absolute dominant

347   position in both pore volume and SSA. The larger SSA can provide more adsorption sites for

348   methane [13]. Thus, this phenomenon can be attributed to the quite developed micropore system,

349   which is similar to previous research [13, 16, 46]. However, the expansion of coal may occur during the

350   process of CO_2 adsorption [56], so it cannot be used as the only criterion. Therefore, what we should

351   focus on next is the type of pore morphology, affecting the gas enrichment and diffusion [59]. The N_2

352   adsorption/desorption curves in Figure 1c show that narrow slit-like pores easily exist in the sample

353   LHG with higher SSA. This pore structure is conducive to gas storage, but may hinder the desorption

354   and diffusion of CBM. The pore morphology in sample L-1 presents non-grid aggregates of plate-

355   like particles (Figure 1d), which will facilitate the desorption and diffusion of gas but is not

356   beneficial to the gas adsorption and storage. But Cai et al. showed that the pore morphology type

357   that is favorable for gas adsorption does not necessarily correspond to higher CH_4 adsorption

21

358   capacity [19]. In other words, the methane adsorption may still be restricted by other factors. Lozano-

359   Castello et al. [15] and Wei et al. [16] revealed that gas adsorption capacity was positively correlated

360   with micropore volume. Further studies investigated that the methane adsorption was not only

361   limited by the micropore volume, but also greatly affected by the micropore size distribution [17, 18].

362   Multifractal theory establishes a finely quantified bridge between PSD and heterogeneity. The

363   multifractal behavior in PSD of nanopore at multiple scales has been confirmed in Section 3.2,

364   which can be utilized for fine contrast of heterogeneity. The 2D characteristics of CO_2 and N_2

365   adsorption indicate that the PSD in the range of 0.45-0.70 nm and 2-50 nm of sample LHG is more

366   complicated comparing with sample L-1. Due to the 3D spatial distribution properties obtained by

367   FIB-SEM, the pore heterogeneity in the 10-50 nm range of sample L-1 is stronger than that of

368   sample LHG. This may be because the closed pores are taken into consideration by FIB-SEM. The

369   CH_4 adsorption isotherm experiment conducted in this work may not be able to fully study the effect

370   of closed pores, but mainly focuses on open pores. Hence according to the multifractal results, it

371   can be inferred that the stronger pore heterogeneity in the range of 0.45-0.70 nm and 2-50 nm is

372   beneficial for methane adsorption.

373   Although the detailed work on the effect of nanopores on CH_4 adsorption performance between a

374   high volatile bituminous coal and an anthracite has been discussed, the number of samples is not

375   sufficient to consider and explore all features of coals. Therefore, we will collect more samples to

376   conduct systematic experiments, thereby establishing a multi-factor quantitative model in the next

377   work.

378

379

22

380   **Table 4.** Differences of the coal parameters in Junggar Basin and Qinshui Basin

Previous research	R_o (%)		Porosity (%)	
	Junggar Basin	Qinshui Basin	Junggar Basin	Qinshui Basin
Wang et al. [60],	0.35-0.84	1.83-4.26	6.2-14.0	2.2-6.9
Li et al. [56],	0.42-0.59	2.95-3.10	-	-
Cai et al. [27],	0.49-0.72	1.78-2.95	6.0-20.8	4.34-12.12
Fu et al. [58],	0.52-0.88	-	3.13-9.78	-

381   Note: "-" is none.

382
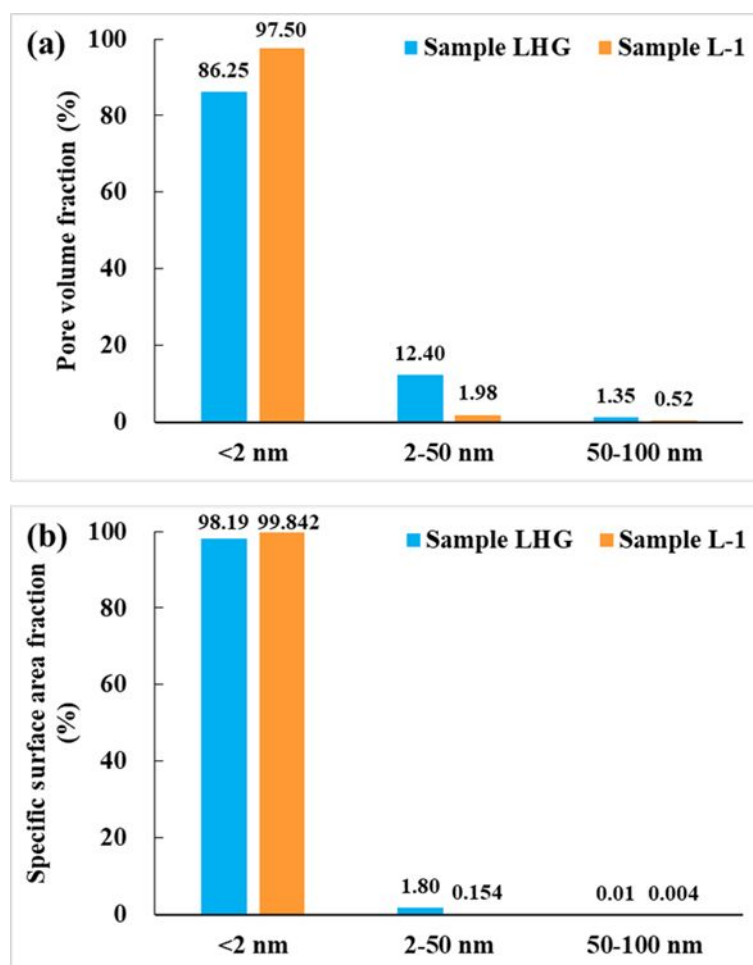
383

384   **Figure 9.** The proportion of pore volume and specific surface area in the nanopore structure. (a)-pore

385   volume fraction; (b)-specific surface area fraction.

386

387   **4. CONCLUSIONS**

388   In this work, a combined conventional CO_2 adsorption at 273 K, N_2 adsorption at 77 K and

389   unconventional FIB-SEM tomography analysis have been conducted on high volatile bituminous

390   coal and anthracite. The effect of nanopores on CH_4 adsorption capacity was discussed by using

23

391 multi-dimensional multifractal analysis. The following conclusions can be made.

392 1) The combination of gas adsorption (CO_2 and N_2) and FIB-SEM can extend the fine description

393 of the nanopore structure from two-dimensional to three-dimensional. And FIB-SEM shows that

394 the nanopores are isolated in the space, indicating that they are mainly used as a storage section.

395 2) The multifractal behavior has been captured in the detected various pore size distributions from

396 gas adsorption (CO_2 and N_2) and FIB-SEM. The nanopores of the sample LHG have stronger

397 heterogeneity in multiple dimensions. More precisely, the areas where pore aggregation is

398 prominent include 0.45-0.70 nm (from CO_2 adsorption), 2-50 nm (from N_2 adsorption) and 10-50

399 nm (from FIB-SEM).

400 3) The effect of nanopore structure on methane adsorption capacity revolves around micropore

401 structure, pore morphology and heterogeneity. The well-developed micropore structure is favorable

402 to methane enrichment. The ink-bottle pores with higher SSA are conducive to gas storage but may

403 hinder the desorption and diffusion of CBM. The pore morphology presenting plate-like particle

404 aggregates with slit-like pores will facilitate the desorption and diffusion of gas and is not beneficial

405 to the gas adsorption. The stronger pore heterogeneity in the range of 0.45-0.70 nm and 2-50 nm is

406 beneficial for methane adsorption.

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