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Solid-liquid phase behavior of eutectic solvents containing sugar alcohols



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ABSTRACT

Mixtures of carbohydrates are often reported in the literature as deep eutectic solvents yet, in most cases, their solid–liquid phase diagrams are poorly characterized and no evidence is available to validate this classification. In this work, the phase diagrams of the binary systems composed of the sugar alcohols mannitol or maltitol and *meso*-erythritol, xylitol, or sorbitol, were experimentally determined. The results obtained reveal that these systems have a thermodynamic ideal behavior, questioning their classification as deep eutectic solvents and showing that intermolecular hydrogen bonding between the components of a mixture is not a sufficient condition to prepare deep eutectic solvents.

The phase diagrams of the systems composed of mannitol or maltitol and cholinium chloride were also measured in this work. In sharp contrast to the mixtures composed solely by sugar alcohols, and unlike numerous other choline-based eutectic systems reported in the literature, these systems revealed significant deviations to thermodynamic ideality, leading to significant melting temperature depressions. The Cl-OH interaction between cholinium chloride and the sugar alcohols is identified as the main reason for these deviations to ideality, paving the way for the rational choice of hydrogen bond acceptors to prepare deep eutectic solvents.

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1. Introduction

Interest in the concepts of sustainability and renewability has been growing over the past two decades in the chemistry and chemical engineering fields [1], particularly in the design of safer and more sustainable solvents [2]. Since most commonly used organic solvents are volatile, toxic, and flammable, efforts have been made to address solvent replacement by more renewable and easily recyclable systems ranging from the use of supercritical CO₂ to the application of deep eutectic solvents (DES) [2–5].

Deep eutectic solvents were first reported by Abbott et al. [6], in 2003, as a new class of solvents consisting of binary mixtures of Lewis acids and bases. They are characterized by the low cost of their precursors, preparation simplicity as no synthesis steps are required, low volatility, and environmental friendliness [3–5]. This class of solvents is also generally known to present significantly lower toxicity levels than conventional organic solvents, although the final properties of the solvent depend on the precursors used [7]. These often include cholinium chloride ([Ch]Cl), an essential nutrient and additive in animal feed. Mixtures containing [Ch]Cl

* Corresponding author. E-mail address: jcoutinho@ua.pt (J.A.P. Coutinho). are, in general, readily biodegradable [8]. Being a good hydrogen bonding acceptor (HBA) and presenting a small melting enthalpy (4.3 kJ mol⁻¹) [9], cholinium chloride usually displays a very steep melting curve regardless of the hydrogen bond donning ability of the second component of the mixture [10].

Mixtures of [Ch]Cl with naturally occurring compounds such as organic acids, amino acids, sugars, and sugar alcohols[3,4,11–13] are commonly classified and used as DES, as they allow for numerous applications, being safe for human consumption [11]. Despite their high viscosities [14], sugar alcohol-based DES are systems that can be adapted or tuned for a wide range of different applications in food, cosmetic, agrochemical and pharmaceutical industries [15–17]. Despite the increasing interest and the growing number of articles reporting applications using sugar alcohols as DES precursors [3,4,14,16], knowledge about their solid–liquid phase diagrams is scarce [12,18], most likely due to their poor thermal stability. However, the relevance of the information that can be gathered from these phase diagrams on the nature and interactions prevalent on their liquid phase is much valuable [19].

In previous works [10,20,21], we have characterized the solidliquid equilibria (SLE) of several eutectic mixtures composed of sugar alcohols, combined with quaternary ammonium salts. Although commonly reported as DES, the results demonstrated





that most of these systems do not show significant deviations from the ideal-mixture behavior and, consequently, exhibit low melting temperature depressions. Bearing in mind that the prefix *deep* should only be used to describe eutectic systems with large deviations from thermodynamic ideality [10], that can also be derived from the measured eutectic temperature [22], these results reinforce the need to further investigate the solid–liquid equilibrium of the numerous deep eutectic solvents reported in the literature based on sugar alcohols.

Aiming at further contributing to the characterization of eutectic systems containing sugar alcohols (mannitol, *meso*-erythritol, xylitol, sorbitol and maltitol), in this work, the SLE of sugar alcohol + sugar alcohol and cholinium chloride + sugar alcohol mixtures were studied in the full composition range. Results allow to evaluate the nature of these systems and the magnitude of their interactions.

2. Experimental section

2.1. Chemicals

The source, purity, and melting properties of the compounds studied in this work are detailed in Table 1, while their chemical structures are illustrated in Fig. 1. Cholinium chloride was dried under vacuum at room temperature with constant stirring, for at least 72 h. All the remaining compounds were stored at room temperature and used as received from the supplier as they present very low hygroscopicity. The water content was measured using a Metrohm 831 Karl-Fischer coulometer, with the analyte Hydranal Coulomat AG from Riedel-de Haën and was found to be lower than 600 ppm for cholinium chloride and below 120 ppm for the remaining compounds. The water content of mixtures was also measured and is reported in Table S1.

3. Solid-Liquid phase diagrams measurements

Binary mixtures between sugar alcohols, or between [Ch]Cl and sugar alcohols, were prepared in different proportions covering the full compositions range (at mole fraction intervals of 0.1) by weighting the proper amounts of each pure substance using an analytic balance Mettler Toledo XP205 (repeatability of 0.015 mg). Due to the hygroscopic character of [Ch]Cl, the eutectic mixtures involving this compound were prepared inside a dryargon glove box at room temperature using an analytical balance from Kern (ALS 220-4 N) with an accuracy of 0.2 mg. After the first heating to mix the compounds and immediate crystallization, two experimental methods were applied depending on the physical state of the resulting mixture: *i*) for mixtures presenting a pasty consistency, samples were heated in an oil bath under stirring until complete melting. The melting temperatures, measured using a Pt100 probe (±0.1 K), correspond to the fusion of the last remaining solid. The probe was previously calibrated against a calibrated platinum resistance thermometer, SPRT100 (Fluke-Hart Scientific 1529 Chub-E4), traceable to the National Institute of Standards

and Technology (NIST); *ii*) for mixtures showing complete recrystallization, the samples were grounded in the glovebox, and the powder was filled into a glass capillary. The melting point was then measured in a device model M-565 from Bücchi, with a temperature resolution of 0.1 K. Each procedure was repeated at least three times.

4. Powder and single crystal X-ray diffraction analysis

Due to the high melting temperatures of almost all systems, making difficult the sampling of the solid phase in equilibrium, only two samples of [Ch]Cl + maltitol system ($x_{maltitol} = 0.45$ and $x_{maltitol} = 0.70$) were analyzed through X-Ray. Powder X-Ray Diffraction (PXRD) data for all prepared materials were conducted at ambient temperature and at 358 K for pure choline chloride, on a Empyrean PANalytical diffractometer (Cu Ka1,2 X-radiation, $\lambda 1 = 1$. 540598 Å; $\lambda 2 = 1.544426$ Å), equipped with an PIXcel 1D detector and a flat-plate sample holder in a Bragg-Brentano *para*-focusing optics configuration (45 kV, 40 mA). Intensity data were collected by the step-counting method (step 0.026°), in continuous mode, in the ca. $3.0 \leq 2\theta \leq 70^\circ$ range. The respective diffractograms of the pure compounds, and the solids in equilibrium with the liquid mixtures are depicted in Figure S1 of Supporting Information.

In the case of monocrystal X-Ray analysis, the cell parameters of suitable crystals taken from the selected mixtures were determined on a Bruker SMART Apex II diffractometer equipped with a CCD area detector, with monochromated Mo-Ka radiation ($\lambda = 0.71073$ Å) and operating at low temperature (150 K). The selected crystals were placed at 40 mm from the CCD and the spots were measured using different counting times (varying from 5 to 30 s). After a search in CCDC database for the cell parameters of pure individual compounds and comparison with the parameters obtained during analysis, it was possible to observe that the crystal analyzed by monocrystal X-Ray corresponds to maltitol whose structure is orthorhombic with a space group of P2₁2₁2₁.

5. Solid-Liquid equilibrium thermodynamics

The solid–liquid equilibrium curve of a generic component, *i*, in an eutectic-type mixture can be obtained using the following expression:[27]

$$ln(x_i \cdot \gamma_i) = \frac{\Delta_m h_i}{R} \cdot \left(\frac{1}{T_{m,i}} - \frac{1}{T}\right) + \frac{\Delta_m C p_i}{R} \cdot \left(\frac{T_{m,i}}{T} - \ln \frac{T_{m,i}}{T} - 1\right)$$
(1)

where x_i is the mole fraction of component *i*, γ_i is its activity coefficient in the liquid phase, $\Delta_m h_i$ and $T_{m,i}$ are its melting enthalpy and temperature, respectively, $\Delta_m Cp_i$ is its heat capacity change upon melting, *R* is the ideal gas constant, and *T* is the absolute temperature of the system. Since the impact of the heat capacity change upon melting on solid–liquid equilibrium is often negligible and considering that this value is not known for many compounds (e.g. [Ch]Cl), the $\Delta_m Cp$ term was neglected [28]. allowing **Equation** (1) to be simplified to **Equation** (2)[29]. This assumption has been discussed in detail by us elsewhere [10].

Table 1

Source, purity (according to the supplier), melting temperature (T_m), and melting enthalpy ($\Delta_m H$) of the substances used in this work.

Compound	Supplier	Mass Purity %	T _m /K	$\Delta_m H / kJ \cdot mol^{-1}$
Cholinium chloride ([Ch]Cl)	Acros Organics	98	597[9]	4.3[9]
D-Mannitol (Man)	Sigma-aldrich	98	437.3[23]	54.7[23]
Maltitol (Mal)	Sigma	98	420.0[24]	55.1[24]
meso-erythritol (ME)	Alfa Aesar	99	391.2[25]	38.9[25]
Xylitol (Xyl)	Acros Organics	99	365.7[26]	37.4[26]
Sorbitol (Sor)	Fischer Bioreagents	98	366.5[26]	30.2[26]



Fig. 1. Chemical structures of the compounds used in this work.

$$\ln(x_i \cdot \gamma_i) = \frac{\Delta_m h_i}{R} \cdot \left(\frac{1}{T_{m,i}} - \frac{1}{T}\right)$$
(2)

Since the melting properties of the compounds studied are known, as reported in Table 1, **Equation (2)** can be used to assess the activity coefficients from the experimental solid–liquid equilibrium data, allowing for an evaluation of the non-ideality of the liquid phase of the eutectic systems studied. Furthermore, the experimental melting curves can also be compared with those obtained assuming an ideal solution by setting the activity coefficients to unity.

6. Results

6.1. Solid-liquid phase diagrams of sugar alcohol mixtures

The impact of the differences in size and number of hydroxyl groups on the solid–liquid phase diagrams of binary mixtures composed of mannitol or maltitol and *meso*-erythritol, xylitol, or sorbitol are investigated in this section. The solid–liquid phase diagrams of the mixtures composed of mannitol and *meso*-erythritol, xylitol or sorbitol are depicted Fig. 2 (detailed data is listed in **Table S2** in the supporting information) along with the melting curves obtained using **Equation (2)** assuming an ideal behavior. The experimental activity coefficients were also estimated using **Equation (2)**, which are plotted in Fig. 2 and listed in **Table S2** in **SI**.

The data measured in this work, presented in Fig. 2, were compared against data previously reported by other authors [30–36] and the vast majority is in good agreement. Concerning the pure sugars, the differences between the experimental melting temperatures measured in this work (Table 1) and those from literature are lower than 1.8 K, confirming the consistency of the experimental methodology used. For the system mannitol/erythritol, Shao et al. [31] only reported one melting temperature near the eutectic composition. For the system, mannitol/xylitol, Katona et al. [34] presented data in a limited composition range, in the eutectic region and in the mannitol-rich side. For the system mannitol/sorbitol, there are some discrepancies between the results obtained and those reported by Siniti et al. [35] and by Del Barrio et al. [32], since these authors underestimate the temperatures near the eutectic composition and in the sorbitol rich-side.

Fig. 2 shows that the studied systems involving mannitol are characterized by a single eutectic point close to a mannitol mole fraction of 0.1 and show a nearly ideal behavior on both sides. These systems also have a eutectic temperature and composition similar to that predicted by considering ideal behavior, and close to the melting temperature of the sugar alcohol with the lowest melting point. The activity coefficients estimated from the experimental data, which are very close to 1 (Table S2 and Fig. 2), further support the thermodynamic ideality observer in these systems. This means that the strength of the intermolecular interactions present in these liquid mixtures is similar to those of the liquid phases of the pure components, which is not surprising considering their structural similarity. Even though these systems are simple ideal eutectic mixtures, the results here reported for mixtures containing mannitol still exhibit a considerable temperature depression compared with the melting point of pure mannitol (around 50 K).

The results reported in Fig. 2 reveal that these mannitol-based mixtures are not deep eutectic solvents because they lack the appropriate negative deviations to thermodynamic ideality, regardless of the melting temperature depression observed [22]. They are ideal mixtures with SLE phase diagrams with a eutectic point. This significant result, already discussed by us before [9], reaffirms that the existence of intermolecular hydrogen bonding, often used to justify the formation of the liquid phase of DES, is not a sufficient condition to ensure the existence of negative deviations from thermodynamic ideality. Note how both components of these mixtures are excellent hydrogen bonding interactions when mixed.

After discussing mannitol-based eutectic systems, the systems composed of the structurally more complex maltitol are now investigated. Replacing mannitol with maltitol allows the probing of the influence of molecular size and number of –OH groups in the thermodynamic behavior of these systems. The respective SLE phase diagrams of the binary mixtures composed of maltitol and *meso*-erythritol, xylitol or sorbitol measured in this work are depicted in Fig. 3, along with the ideal liquid phase curves and the experimental activity coefficients. The detailed experimental data and experimental activity coefficients are listed in **Table S3** of Supporting Information. The experimental activity coefficients were calculated using **Equation (2)** and the melting properties of



Fig. 2. Solid-liquid phase diagrams of binary mixtures composed of mannitol and a sugar alcohol. A) *meso*-erythritol; B) xylitol and C) sorbitol; Legend: \blacklozenge , experimental melting temperatures measured in this work; - -, ideal solubility curve; ..., experimental eutectic temperature; \blacklozenge , \bigcirc , experimental activity coefficients, – γ = 1. Literature: ×Zeng et al. (2018);[30] \land , Shao et al. (2018);[31] \bigcirc , Del Barrio et al. (2016);[32] +, Perkkalainen et al. (1995);[33] +, Katona et al. (2016);[34] +, Gombás et al. (2003)[36]; \bigstar , Siniti et al. (1999).[35]

the pure compounds reported in Table 1. To the best of our knowledge, there are no literature data available for these systems.

Fig. 3 reveals that the SLE phase diagrams of maltitol + *meso*erythritol, xylitol, or sorbitol show an ideal behavior in both sides of the phase diagrams. As occurs in mannitol-based systems, the eutectic temperatures of the binary mixtures are significantly above room temperature, and the liquid phase of these mixture behaves almost ideally, with activity coefficients very close to 1, even if a large asymmetry in terms of size and number of OH groups is observed when comparing both components of these three binary mixtures. As a consequence of the ideality, the experimental eutectic temperature and composition are very similar to that predicted from **Equation (2)** ($\gamma_l^l = 1$). The studied mannitolbased systems are characterized by a single eutectic point around a mannitol mole fraction of 0.1, not presenting a significant temperature depression at the eutectic point. The presence of a high number of –OH groups in the molecules seems to contribute to a similar network of interactions either in a mixed state or as pure



Fig. 3. Solid-liquid phase diagrams for binary mixtures composed of maltitol and a sugar alcohol. A) *meso*-erythritol; B) xylitol and C) sorbitol; Legend: \blacklozenge , experimental melting temperatures measured in this work; - -, ideal solubility curve; - -, experimental eutectic temperature; \blacklozenge , \bigcirc , experimental activity coefficients, $-\gamma = 1$.

components, while the size and form of the molecules do not contribute much for deviations to ideality.

Closing this set of systems, the SLE phase diagram of mannitol and maltitol was also studied. These results are depicted in Fig. 4 and reported in **Table S3** of the Supporting Information. This system is somewhat different from those reported in Figs. 2 and 3, in the sense that it presents a eutectic point at a different composition. However, this is merely due to their melting properties and not due to intermolecular interactions, as both compounds behave ideally [22]

Analyzing all the binary mixtures containing mannitol and maltitol (Figs. 2, 3 and 4), it is possible to observe that the similar-

ities of the chemical structures and the presence of the same functional groups in both compounds of a binary mixture lead to an ideal liquid phase behavior and, consequently, the inability to significantly decrease the eutectic temperature when compared to the melting temperature of the pure compounds, as previously reported for sugars [20]. This reinforces the idea that the existence of intermolecular hydrogen bonding between the components of a mixture does not ensure the formation of deep eutectic solvents. In fact, and as will be discussed in the next section, the cross interactions between the components in a eutectic system need to be stronger than any interaction available to the components in their pure liquid phases to form a deep eutectic solvent.



Fig. 4. Solid-liquid phase diagrams for binary mixtures composed of maltitol and mannitol. Legend: \blacklozenge , experimental melting temperatures measured in this work; --, ideal solubility curve; --, experimental eutectic temperature; \blacklozenge , \bigcirc , experimental activity coefficients, $-\gamma = 1$.

7. Thermodynamic behavior of [Ch]Cl + sugar alcohol systems

So far, it has been shown that binary mixtures of sugar alcohols behave ideally and therefore are not deep eutectic solvents, despite the ability of these compounds to establish extensive hydrogenbonding networks. Aiming to explore the impact of a well-known HBA in the thermodynamic behavior of sugar alcohol mixtures, the phase diagrams of the systems composed of maltitol or mannitol and [Ch]Cl were also investigated. The experimental phase diagrams are depicted in Fig. 5, along with the melting curves calculated by **Equation** (2) assuming an ideal liquid phase $(\gamma_i^l = 1)$. Detailed data, including the experimental activity coefficients, are reported in **Table S4** of Supporting Information. In order to evaluate the crystal structure of the mixtures, the solid phases were analyzed through X-Ray.

Due to the high melting temperatures of almost all systems, only two samples of the [Ch]Cl + maltitol system, one from each side of the phase diagram, were analyzed. The cell parameters obtained were a = 8.16; b = 12.69; c = 13.68; orthorhombic P. According to the CCDC database (version 2020.2.0), we concluded



Fig. 5. Solid-liquid phase diagrams for binary mixtures composed of choline chloride and a sugar alcohol. A) [Ch]Cl + mannitol; B)[Ch]Cl + maltitol; Legend: \blacklozenge , experimental melting temperatures measured in this work; - , ideal solubility curve; - , experimental eutectic temperature; \blacklozenge , \bigcirc , experimental activity coefficients, $-\gamma = 1$.

that it corresponds to maltitol whose space group is $P2_12_12_1$, showing that the addition of the second component does not change the crystal structure and the solubility. Additionally, the diffractograms in Figure S1 show that in the hypertectic region, the solid phase matches the pure maltitol one, confirming the solid phase is not affected by the presence of choline chloride. In the hypotectic region, the solid in equilibrium with a liquid whose maltitol mole fraction is 0.45 presents a diffractogram indicating a combination of the two choline chloride polymorphs, which is quite probable attending to the equilibrium temperature level at that composition.

There is a sharp contrast between the results reported in Fig. 5 and those reported in Figs. 2, 3 and 4. Contrary to the systems composed only of sugar alcohols, which displayed an ideal thermodynamic behavior, cholinium chloride can induce negative deviations to ideality on mannitol and maltitol. This leads to significant melting temperature depressions not obtainable using the other compounds previously studied, with depressions of 54 K and 107 K for the systems [Ch]Cl + mannitol and [Ch]Cl + maltitol, respectively, when compared to the melting temperature of the pure sugars. Note, however, that the [Ch]Cl activity coefficients show positive deviations from ideality when mixed with mannitol and a quasi-ideal behavior when mixed with maltitol. More specifically, the experimental activity coefficients for the system ChCl + mannitol are uncommon; in the large series of binary systems containing ChCl already studied only a few present positive deviations from ideality in the ChCl side, which might be related to the to changes in the crystalline form of ChCl or the formation of some intermediate compound. However, the results are comparable with those for mixtures of [Ch]Cl with meso-erythritol, xylitol, sorbitol previously studied by us [21], where the polyalcohol exhibited negative deviations from ideality.

The sugar alcohol negative deviations to ideality discussed in the previous paragraph hint at the formation of hydrogen bonds between their hydroxyl groups and the chloride anion of [Ch]Cl. This specific interaction is stronger than the typical OH-OH hydrogen bonding found in the pure liquid phases of the sugar alcohols and explains the negative deviations to ideality these compounds display when mixed with [Ch]Cl. On the other hand, the hydrogen bond between the chloride anion of [Ch]Cl and the hydroxyl groups of the sugar alcohols is still weaker than the interaction between the chloride and the hydroxide group of the choline cation. Thus, [Ch]Cl presents either an ideal behavior or positive deviations from ideality, since the formation of new Cl-OH contacts with the sugar alcohols decreases the number of Cl-OH contacts between both ions of [Ch]Cl.

The difference in the magnitude of the negative deviations to ideality displayed by maltitol and by mannitol, when mixed with [Ch]Cl, can be explained by the number of hydroxyl groups of these compounds. Maltitol has a much larger number of hydroxyl groups than mannitol, which means that the former is able to establish more Cl-OH hydrogen bonds than the latter. This also explains why [Ch]Cl behaves ideally when mixed with maltitol (as opposed to showing positive deviations to ideality), as its greater number of –OH groups makes the number and magnitude of interactions in the mixture more significant, and similar to the magnitude observed in pure [Ch]Cl.

The results here discussed reveal that the prototypical hydrogen bond acceptor [Ch]Cl is unable to show negative deviations to ideality, as observed in many other works [37–40], reiterating its inability to establish stronger interactions with other compounds than with itself in the liquid phase. The addition of [Ch]Cl to the sugar-alcohol gives rise to strong interactions between the components inducing strong negative deviations from ideality in the sugar alcohol rich side, which is a behavior observed in many other systems [41,42], showing that a small addition of [Ch]Cl allows for a significant decrease of the melting temperature of the pure sugar alcohol. Although the eutectic temperature is significantly below from those predicted by the ideal mixture, obeying the condition needed to be a DES, the melting temperatures of these mixtures are still above room temperature, in stark contradiction to what is often reported in the literature [4,43–46] where these mixtures are reported to be liquid at room temperature.

8. Conclusions

In this work, mixtures composed of sugar alcohols, and mixtures of [Ch]Cl with sugar alcohols were investigated by measuring the solid–liquid equilibrium phase diagrams of their binary mixtures in the entire composition range. From these experimental data the activity coefficients of the components in the liquid phase were calculated, allowing the data to be interpreted in terms of intermolecular interactions.

The studied systems involving the combination of two sugar alcohols were all found to be thermodynamically ideal. These results reveal that, although sugar alcohol systems have been reported as DES in the literature, they do not establish new interactions not found in the pure components and should not be classified as *deep*. This reinforces the idea that the presence of intermolecular hydrogen bonding in a mixture does not necessarily lead to negative deviations to thermodynamic ideality, and is thus not a sufficient condition for the formation of DES.

Regarding the systems composed of [Ch]Cl and sugar alcohols, the activity coefficient data revealed that while the sugar alcohols exhibit significant negative deviations from ideality, [Ch]Cl behaves ideally or displays positive deviations to ideality. In fact, the presence of [Ch]Cl induces a significant temperature depression, with depressions of 54 K and 107 K for the systems [Ch] Cl + mannitol and [Ch]Cl + maltitol, respectively, when compared to the melting temperature of the pure sugars. The asymmetric thermodynamic behavior of these systems was interpreted in terms of intermolecular interactions. It was shown that the interaction Cl-OH, being stronger than the typical OH-OH hydrogen bonding found in the pure liquid phases of the sugar alcohols, was responsible for the negative deviations of the sugar alcohols and, being weaker than the interaction between the chloride anion and the cholinium cation in cholinium chloride, was also responsible for the positive deviations of [Ch]Cl.

CRediT authorship contribution statement

Liliana P. Silva: Conceptualization, Data curation, Formal analysis, Methodology, Writing - original draft, Writing - review & editing. Mónia A.R. Martins: Conceptualization, Formal analysis, Supervision, Writing - review & editing. Dinis O. Abranches: Conceptualization, Formal analysis, Writing - review & editing. Simão P. Pinho: Conceptualization, Formal analysis, Supervision, Funding acquisition, Writing - review & editing. João A.P. Coutinho: Conceptualization, Formal analysis, Funding acquisition, Supervision, Writing - review & editing.

Declaration of Competing Interest

The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

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