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DIFFUSION-BASED KINETIC MODELING OF TEXTILE DYE ADSORPTION BY POROUS COPOLYMER

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Abstract

Macroporous glycidyl dimethacrylate and ethylene glycol dimethacrylate copolymer functionalized with diethylene triamine, PGME-deta, was tested as adsorbent for removal of Acid Orange 10 (AO10) and Reactive Black 5 (RB5) from aqueous solutions. Diffusion-based kinetic models (intraparticle diffusion, Bangham and Boyd model) were used for interpretation of experimental data.

Introduction

The removal of synthetic dyes from the industrial effluents becomes a critical issue. Over $7 \ge 10^5$ t of nearly 100,000 commercially available dyes are produced annually worldwide while 2% of dyes are discharged directly into the environment [1]. Among the most attractive polymeric adsorbents for textile dyes removal from aqueous media are amino-functionalized glycidyl methacrylate (GMA) copolymers [2]. In this paper, kinetic data of textile dyes adsorption onto PGME-deta were interpreted with intraparticle diffusion, Bangham and Boyd model.

Experimental

PGME-deta (surface area 53 m²g⁻¹, pore diameter 50 nm, particle size 150-500 μ m, amino groups concentration 5.01 mmolg⁻¹) was obtained as described elsewhere [2]. AO10 [CAS: 1936-15-8], and RB5 [CAS: 17095-24-8] were purchased from Alfa-Aesar and used as received. The experiments were carried out at 25 °C, with the initial dye concentration of 30; 50 and 70 mg L⁻¹, *m_{adsorb}* of 25.0 mg and *V*=50.0 mL, at unadjusted pH values of 5.1 for RB5 and 7.4 for AO10. The solution aliquots were withdrawn and the absorbance of supernatant solution was measured using Thermo Electron Nicolet Evolution 500 UV-VIS spectrophotometer (absorption peaks of AO10 and RB5 were at 478 and 597 nm, respectively).

Results And Discussion

The prediction of the rate-limiting step in the adsorption process is essential for understanding the adsorption mechanism. Our previous studies showed that the adsorption of AO10 and RB5 by PGME-deta obeyed the pseudo-second-order kinetic model, suggesting that the adsorption rate is controlled by both adsorbent

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capacity and adsorbate concentration. For further analysis and the assessment of the influence of diffusion on adsorption, kinetic data were analyzed using diffusion-based models given in Table 1.

Table 1. Kinetic models.

Kinetic model	Equation	Reference
Intraparticle diffusion	$Q_t = C_{id} + k_{id} \cdot t^{0.5}$	[3]
Bangham	$\log \log \left[\frac{C_i}{C_i - C_s Q_t} \right] = \log \left[\frac{k_b C_s}{2.303 V} \right] + \alpha \log t$	[4]
Boyd	$B_t = -0.4977 - \ln(1 - F)$	[5]

Where: Q_t is the amount of adsorbate at time $t \pmod{g^{-1}}$, C_{id} - intercept proportional to the boundary layer thickness (mg g⁻¹), k_{id} -intraparticle diffusion rate constant (mg g⁻¹ min^{-0.5}), *t*-time (min), C_i -initial adsorbate concentration in solution (mg L⁻¹), C_s -weight of adsorbent per L of solution (g L⁻¹), V-solution volume (mL), α (< 1) and k_b are constants of the systems, Bt - time constant (min⁻¹), F - fractional attainment of equilibrium at t (min).



Figure 1. Intraparticle diffusion plots for RB5 (a) and AO10 (b); Boyd plots for RB5 (c) and AO10 (d) using PGME-deta as sorbent.

The intraparticle diffusion model plots did not pass through the origin suggesting that even though the adsorption process involved intraparticle diffusion, it was not the only rate-controlling step. Also, the positive (RB5) and negative (AO10) value of intercept C_{id} is indicative of some degree of boundary layer control. Bangham's

parameters also confirmed that these sorption processes were at least partly pore diffusion controlled. In a Boyd plot, if a straight line passes through the origin, it indicates that particle-diffusion mechanisms govern sorption processes. If not, they are controlled by film-diffusion. It is evident from the presented data, that under the same conditions, the contribution of intraparticle diffusion in sorption of RB5 in comparison with AO10 on PGME-deta is more notable. Eventhough the Boyd plots for RB5 do not pass through origin, they are approching straight-line dependance, while for AO10 these plots were neither linear nor passed through the origin, indicating the film diffusion-controlled mechanism is dominant in overall adsorption regardless of initial concentration.

Table 2. Kinetic parameters for A10 and RB5 using PGME-deta as adsorbent (pH=unadjusted, t=25 °C).

	RB5			AO10		
C_i , mg L ⁻¹	30	50	70	30	50	70
Q_e , mg g ⁻¹	60.00	96.2	133.7	57.5	93.74	116.5
Intraparticle						
k_{id} , mg g ⁻¹ min ^{-0.5}	4.99	9.08	9.18	5.57	6.99	8.11
C_{id} , mg g ⁻¹	14.4	10.3	29.2	-2.14	-11.4	-21.2
R^2	0.982	0.988	0.978	0.957	0.962	0.974
Bangham						
$k_b \cdot 10^3$,g ⁻¹	16.3	8.63	10.2	3.99	2.4	0.68
α	0.61	0.72	0.65	0.84	0.79	0.95
R^2	0.991	0.998	0.997	0.952	0.932	0.977

Conclusion

Kinetic data of textile dyes adsorption onto PGME-deta were interpreted with three diffusion-based models: intraparticle diffusion, Bangham and Boyd model. The results suggest that involved intraparticle and film diffusion both play important part in the adsorption process, besides the previously established influence of adsorbent capacity and adsorbate concentration.

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