

MULTI-SCALE MODELING OF HYDRAULIC FRACTURING OPERATIONS

C. Fernandes¹, S.A. Faroughi², R. Ribeiro¹, A.I. Roriz¹, G. H. McKinley³



¹IPC – Institute for Polymers and Composites
Department of Polymer Engineering
University of Minho, Portugal



²Geo-Intelligence Laboratory
Ingram School of Engineering
Texas State University, USA



³HML – Hatsopoulos Microfluids Laboratory
Department of Mechanical Engineering
Massachusetts Institute of Technology, USA

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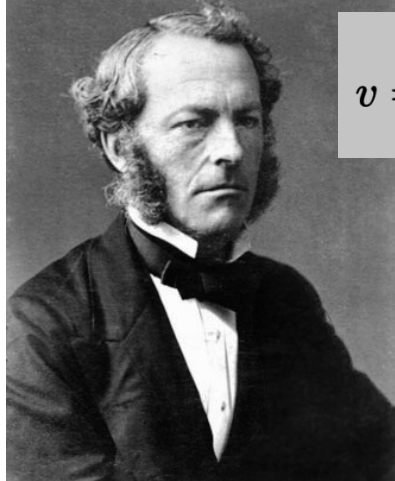


Outline

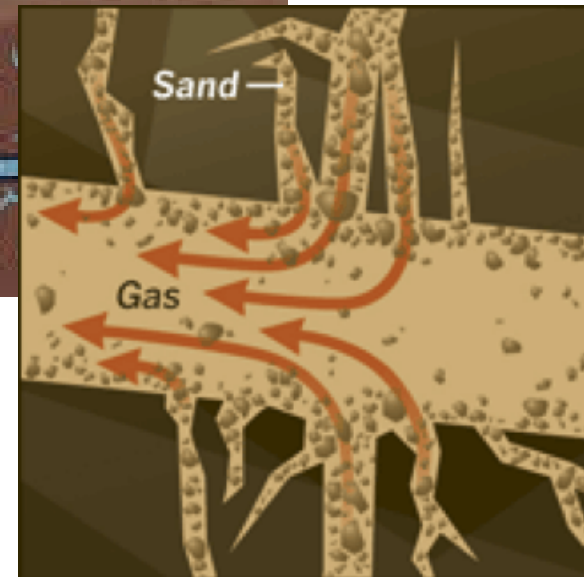
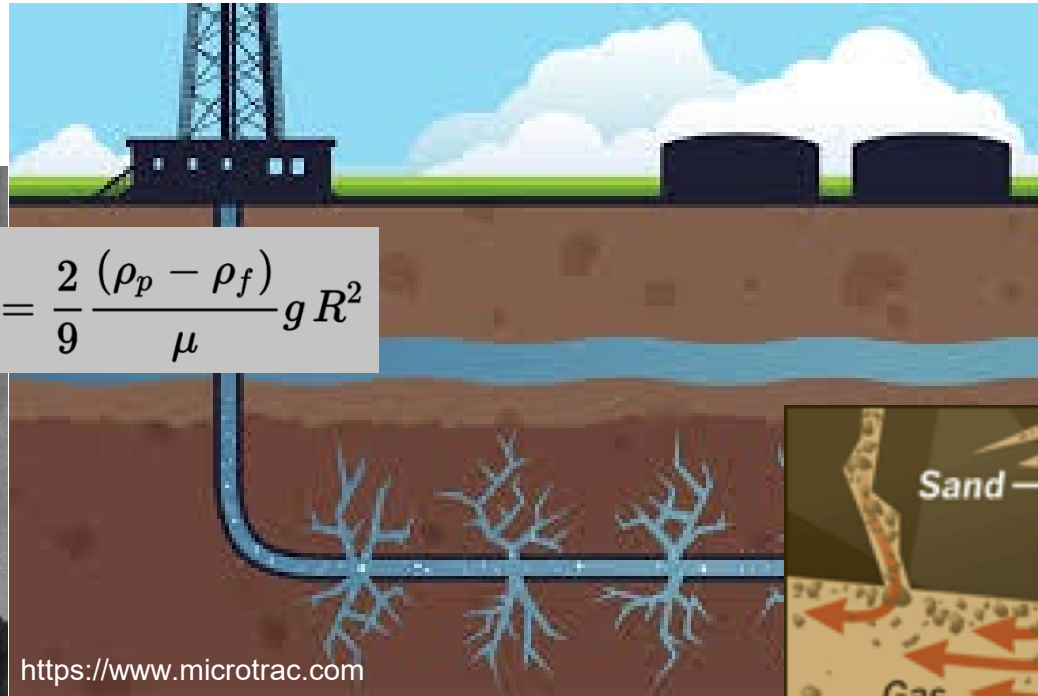
1. Introduction & Motivation
2. Numerical Approach
3. Direct Numerical Simulations
4. Case Study 1 | *Annular Flow*
5. Case Study 2 | *Rectangular Channel Flow*
6. Conclusions

1. Introduction & Motivation

G. G. Stokes

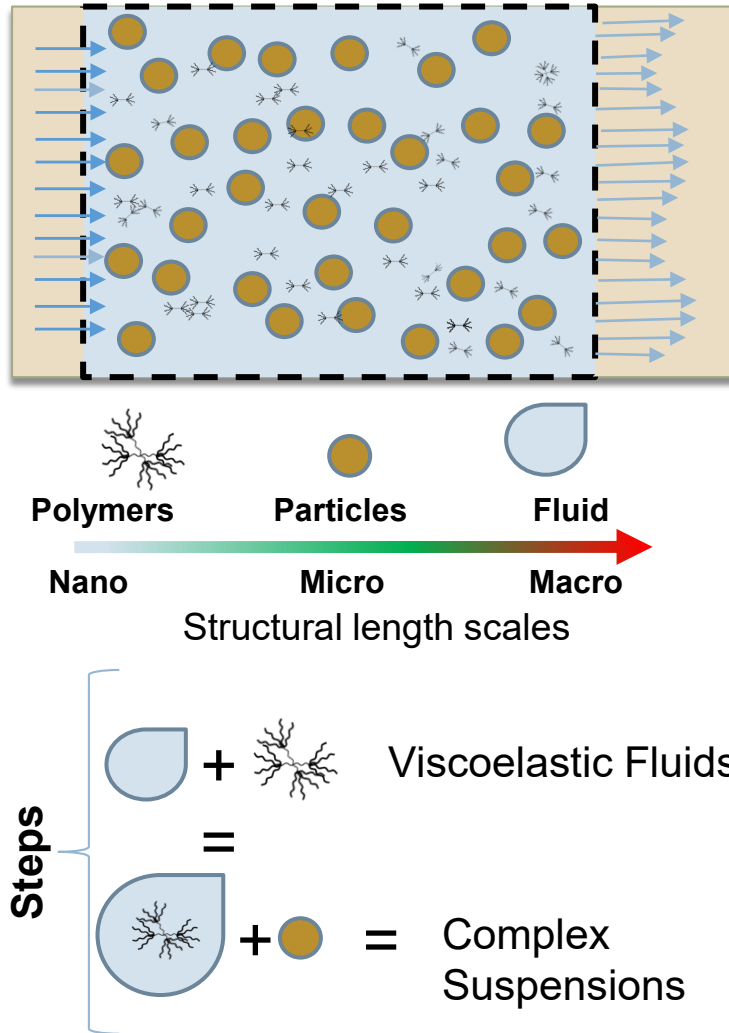


$$v = \frac{2}{9} \frac{(\rho_p - \rho_f)}{\mu} g R^2$$



*A.C. Barbati, et al., "Complex fluids and hydraulic fracturing", *Annual review of chemical and biomolecular engineering*, 7, 415, 2016.

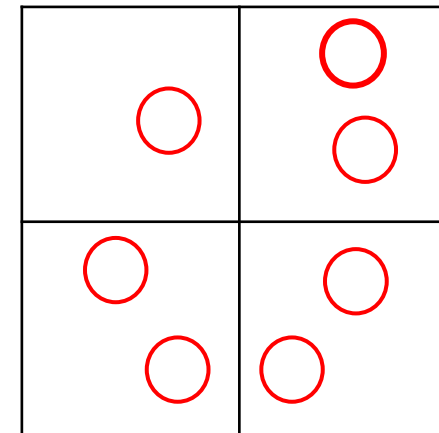
2. Numerical Approach



$$\rho \frac{D\mathbf{u}}{Dt} = \nabla \cdot \boldsymbol{\Pi} + \rho \mathbf{g} \rightarrow \boldsymbol{\Pi} = -p\mathbf{I} + \boldsymbol{\sigma}_s + \boldsymbol{\sigma}_p$$

Oldroyd-B model $\boldsymbol{\sigma}_p + \lambda_1 \overset{\nabla}{\sigma}_p = \eta_P(\nabla \mathbf{u} + (\nabla \mathbf{u})^T)$

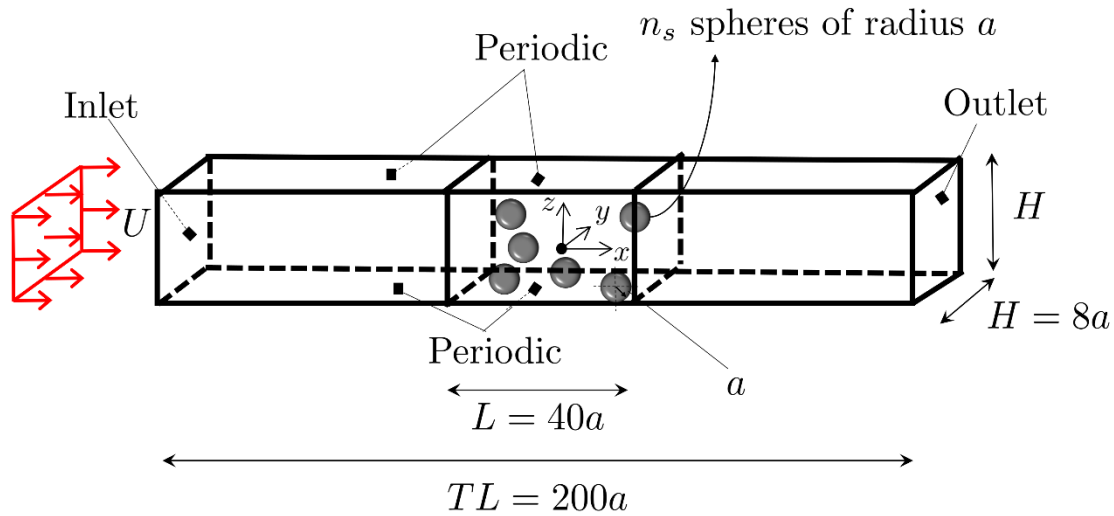
$$\delta x > d_p$$



But need to know expressions for

- 1- Drag force
- 2- Hindrance effect (due to presence of other particles)

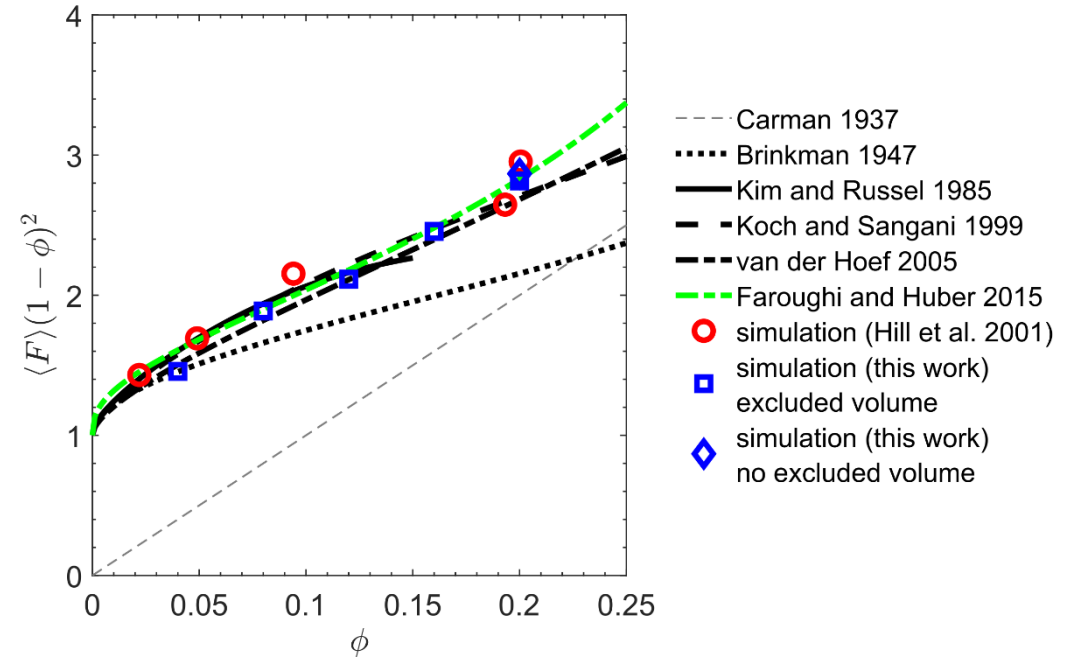
3. Direct Numerical Simulations



$$Re_D = 2Re_a = \frac{2a\rho U_{in}}{\eta_0} = 0.05$$

$$0 \leq \phi \leq 0.2$$

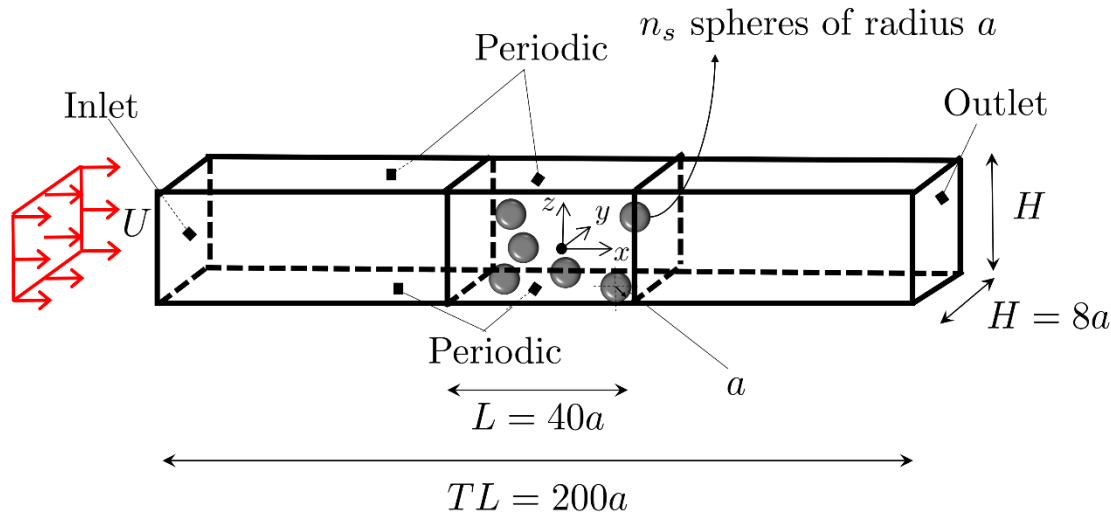
Newtonian Fluid



van der Hoef Drag Force Model

$$\langle F \rangle = (1 - \phi)^2 (1 + 1.5\sqrt{\phi})$$

3. Direct Numerical Simulations



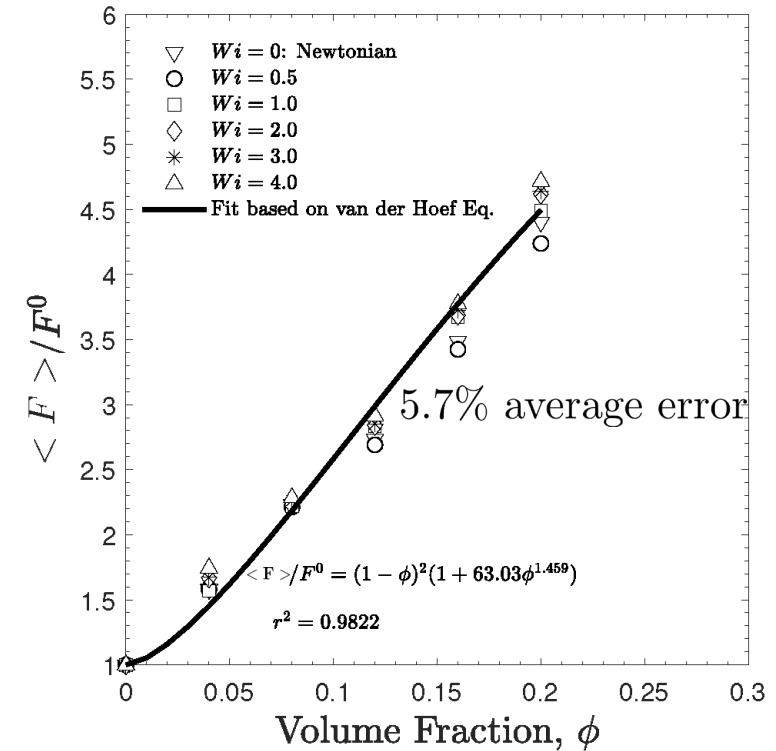
$$\beta = \frac{\eta_S}{\eta_S + \eta_P} = \frac{\eta_S}{\eta_0} = 0.5$$

$$Re_D = 2Re_a = \frac{2a\rho U_{in}}{\eta_0} = 0.05$$

$$0 \leq Wi = \frac{\lambda_1 U_{in}}{a} \leq 4$$

$$0 \leq \phi \leq 0.2$$

Viscoelastic Fluid (Oldroyd-B)



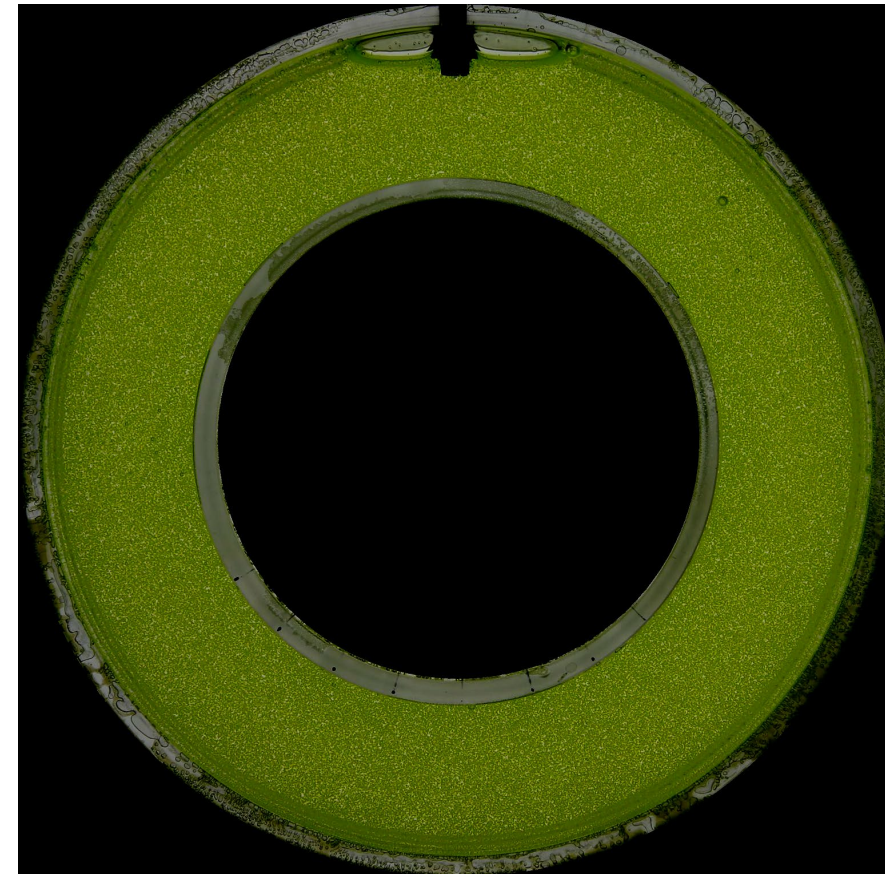
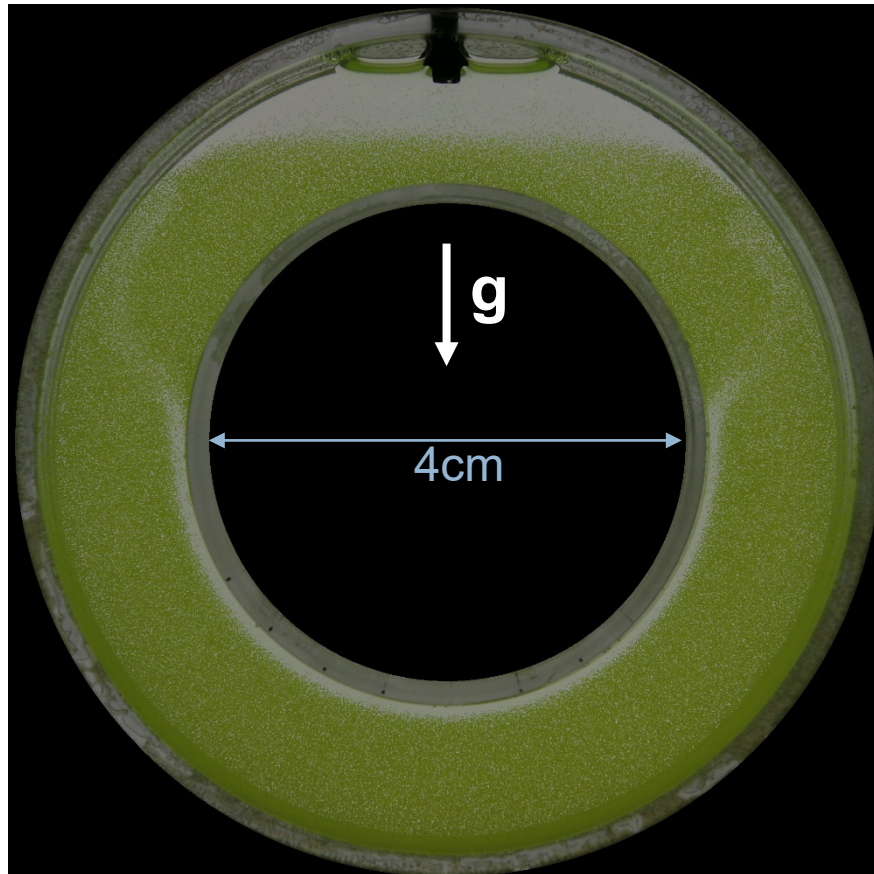
F^0 is the drag force of a single sphere translating in a viscoelastic fluid (Oldroyd-B)*

*S.A. Faroughi, et al., "A closure model for the drag coefficient of a sphere translating in a viscoelastic fluid", *Journal of Non-Newtonian Fluid Mechanics*, 277, 104218, 2020.

4. Case Study 1 | Annular flow

in a donut shape geometry (as a proxy for horizontal well) filled with Newtonian oil, 10 times more viscous than water.

1% volume spherical particles ($D = 200 \mu\text{m}$) in Newtonian oil, with density ratio 2.6.



Performed by Agathe Robisson, SLB

4. Case Study 1 | Annular flow



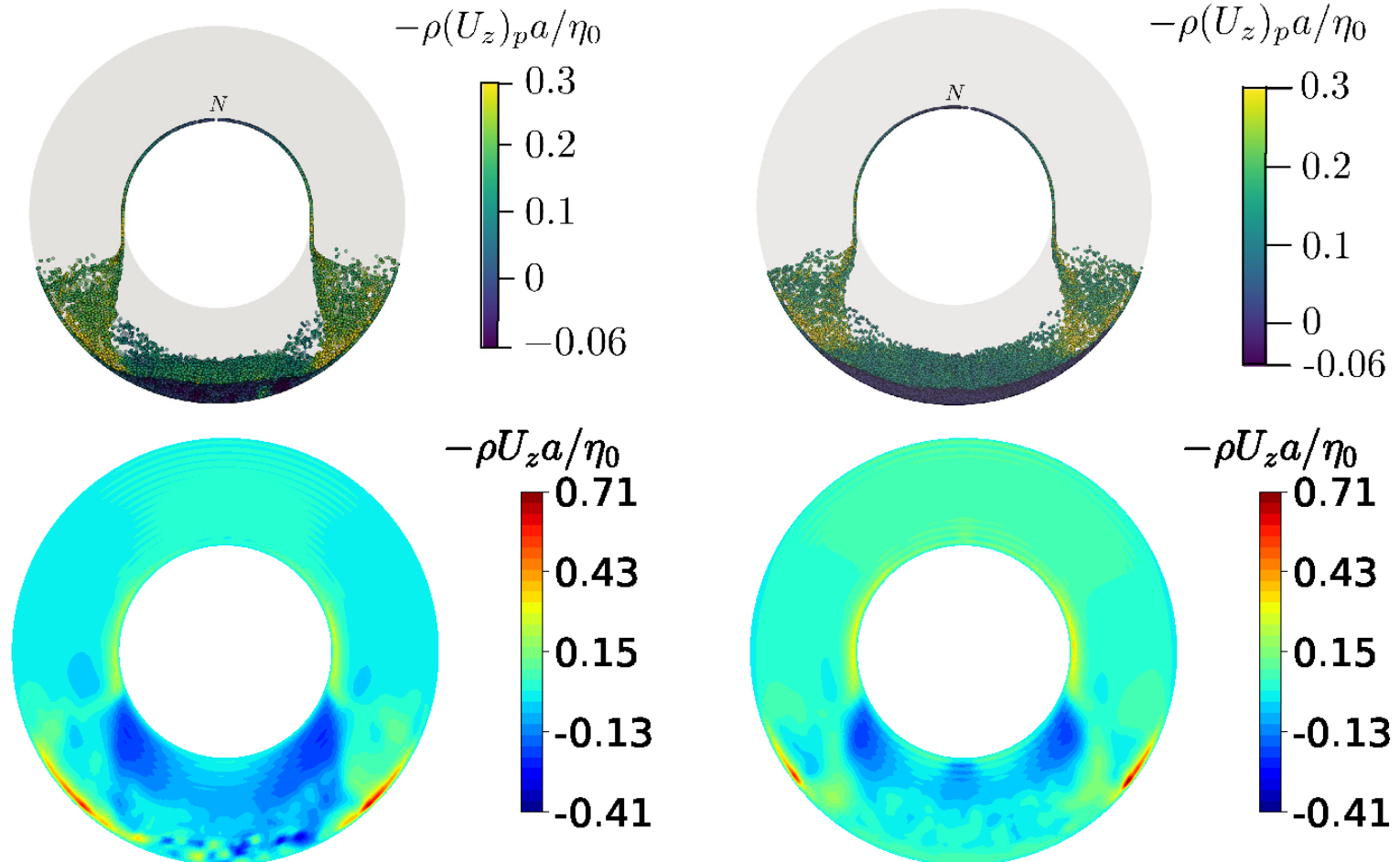
*C. Fernandes, et al., “Validation of the CFD-DPM solver DPMFoam in OpenFOAM through analytical, numerical and experimental comparisons”, *Granular Matter*, 20, 64, 2018.

4. Case Study 1 | Annular flow

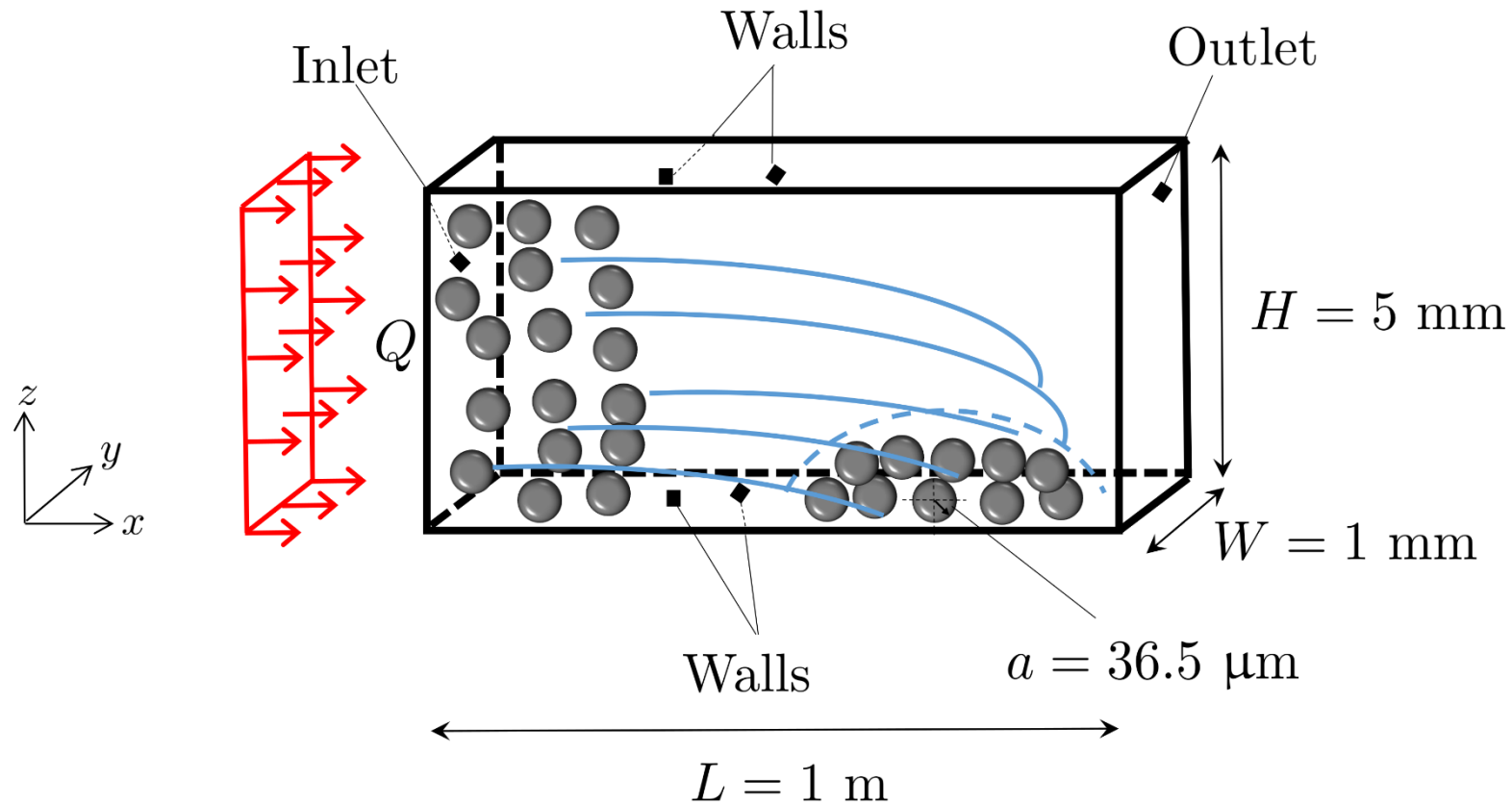
$$El = \frac{Wi}{Re} = \frac{\lambda_1 \eta_0}{2a^2 \rho}$$

$El = 0.1$

$El = 5$



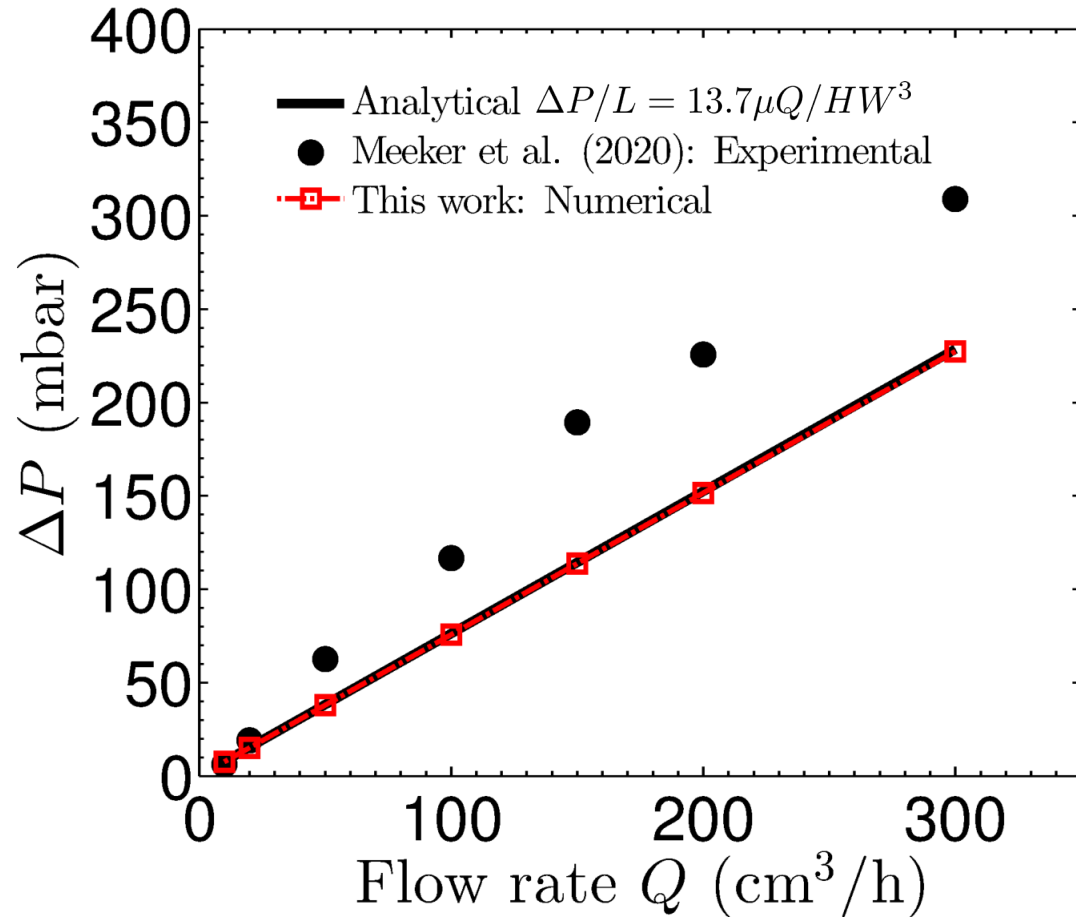
5. Case Study 2 | Rectangular channel flow



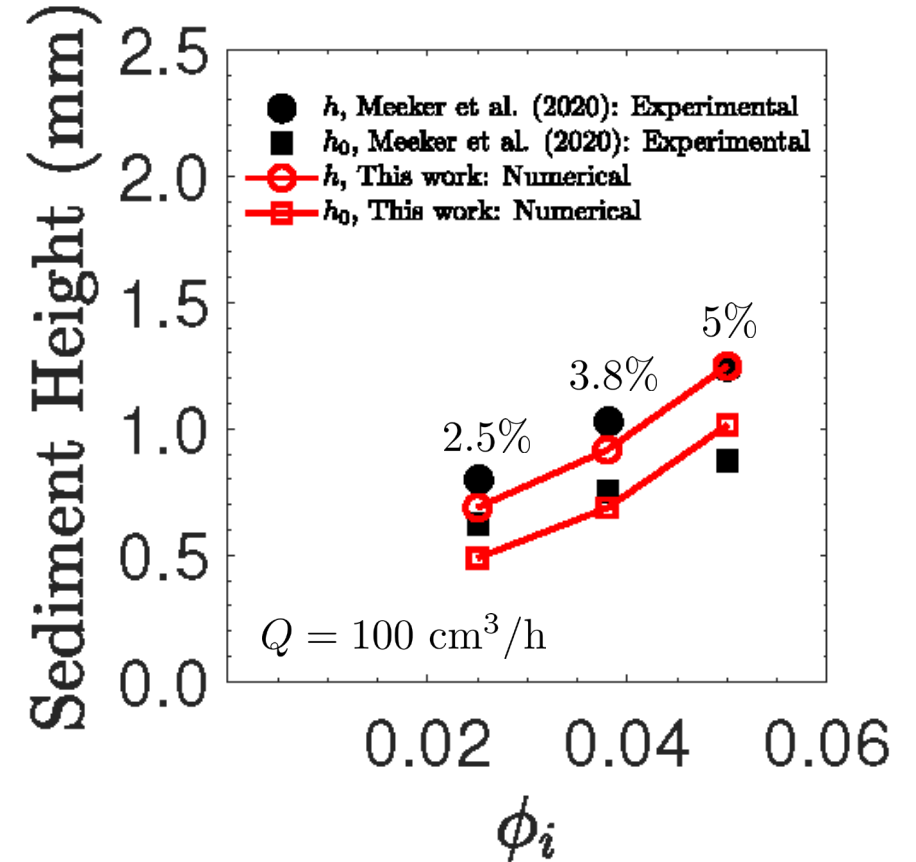
*S. Meeker, et al., "Proppant transport in a Newtonian fluid under laminar flow", Society of Petroleum Engineers, 25, 2020.

5. Case Study 2 | Rectangular channel flow

Newtonian Fluid



Newtonian Fluid + Proppant Particles



h steady-state sediments under flow

h_0 static sediment heights once the suspension flow has ceased

5. Case Study 2 | Rectangular channel flow

$$\phi_i = 0.05$$

$$Q = 100 \text{ cm}^3/\text{h}$$

$$El = 0$$

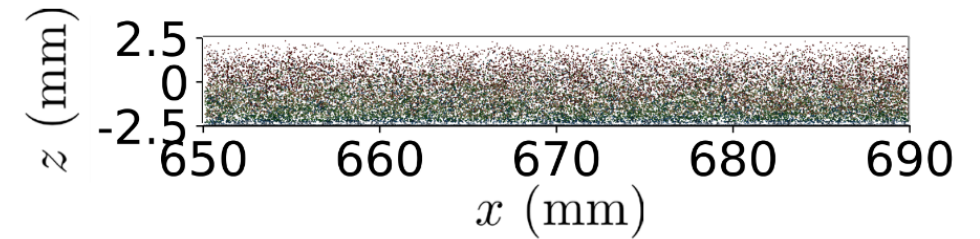
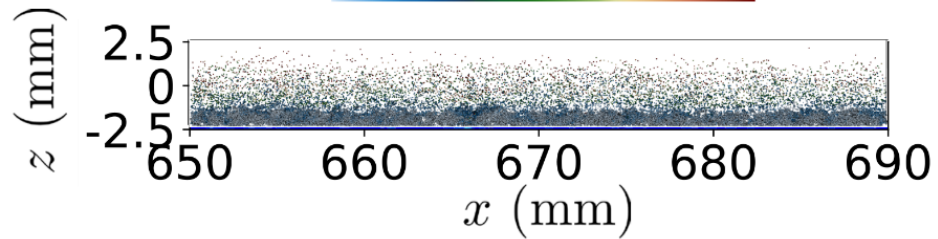
$$El = 30$$

$$(U_x)_p/U$$

$$(U_x)_p/U$$

0.0 0.2 0.4 0.6 0.8 1.0

0.0 0.2 0.4 0.6 0.8 1.0



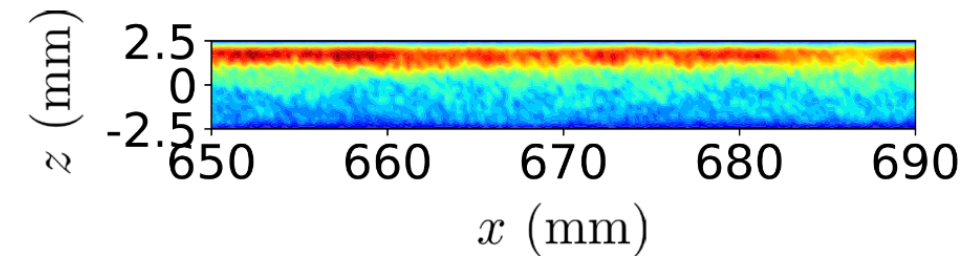
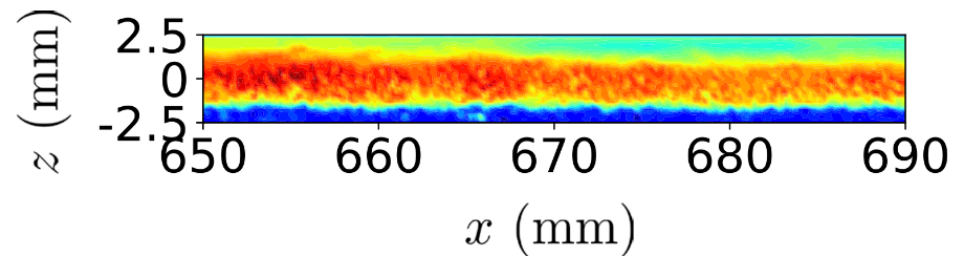
$2L/3$

$$U_x/U$$

$$U_x/U$$

-0.3 0.3 1.0 1.6 2.3

0.0 0.6 1.2 1.8 2.4



6. Conclusions

- Direct numerical simulations (DNS) of **random arrays of spherical particles** immersed in Newtonian and **viscoelastic** liquids were performed using a finite-volume method.
- An approximate closed form model was developed for the **drag force** obtained from numerical simulations of the unbounded flow of an **Oldroyd-B fluid past random arrays of spheres**
 $Re \ll 1$, $\beta = 0.5$, $0 \leq Wi \leq 4$ and $0 < \phi \leq 0.2$.
- An **Eulerian-Lagrangian solver for particle-laden viscoelastic flows** was developed in the open-source computational library OpenFOAM.
- As a proof-of-concept, the newly-developed solver was assessed in terms of accuracy in two case studies. First, the segregation phenomena which occurs when creating casing for **horizontal wells in an annular** domain. Second, the **proppant transport sedimentation** was also studied in a long **channel of rectangular cross section**.

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 - **Texas Advanced Computing Center** (TACC) at The University of Texas at Austin (URL: <http://www.tacc.utexas.edu>);
 - **Gompute HPC** Cloud Platform (URL: <https://www.gompute.com>);
 - **Minho Advanced Computing Center** (MACC) within the project number CPCA/A2/6052/2020 (URL: <https://macc.fccn.pt>).

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llima@math.uminho.pt

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MDPI, St. Alban-Anlage 66
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