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Method Article

Development of a dynamic optimization framework for waste management systems



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ABSTRACT

Waste to energy (WTE) technologies have emerged as an alternative solution to municipal solid waste management. WTE systems provide major environmental and economic benefits by converting waste into accessible energy, as part of an integrated solid waste management (ISWM) strategy. However, previous studies showed that establishing an ISWM strategy based on a single type of WTE systems does not necessarily realize maximum benefits. Hence, optimizing the selection of WTE systems as part of a hybrid waste management strategy can potentially achieve maximum benefits and minimize negative impacts. However, such task is challenging due to the various alternatives and objectives, particularly those related to the material and energy recovery systems. This article presents the methods used to develop a systematic optimization framework that identifies the most beneficial set of ISWM systems through mathematical modelling. The methods include the procedures of the established framework, including base model computations, as well as the comprehensive modelling and optimization methods.

- The energy recovery, carbon footprint, and financial profitability are computed for selected WTE facilities.
- The multi-objective mathematical programming is solved using the weighted comprehensive criterion method (WCCM).
- The model is implemented in CPLEX software using mathematical programming language (OPL).

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Subject Area: More specific subject area:	Engineering Solid Waste Management and Operation Research
Method name:	Multi-Objective Optimization Model for Integrated Waste Management Strategies
Name and reference of original method:	N/A
Resource availability:	https://www.ibm.com/ae-en/analytics/cplex-optimizer

Specifications table

Method details

Optimization framework

This article presents the methods used to establish the framework of a multi-objective optimization model developed to systematically design an optimal waste to energy (WTE)-based management strategy for a given study area. Fig. 1 shows the optimization framework developed for the model, along with the limitations of various steps. The framework is mainly divided into two parts: model computations as well as modelling and optimization. The model computations include base calculations of energy production, carbon footprint, and financial profitability for various waste materials processed in selected waste management facilities. The modelling and optimization module includes a multi-objective mixed integer linear programming model. The multi-objective formulation is solved using the weighted comprehensive criterion method (WCCM).

Model computations

The computations conducted on the optimization model inputs include the energy recovery, greenhouse gas (GHG) emissions, and financial profitability for each waste management facility, namely incinerator, anaerobic digester (AD), and sanitary landfill with gas recovery. The calculation steps, equations, and default values (DV) of these facilities are listed below.

Incinerator

1- Calculate the equivalent carbon emissions, E_{CO_2} , from incineration processes [10].

$$E_{CO_2} = W_p \times \frac{44}{12} \times \sum \left(M_i \times dm_i \times CF_i \times FCF_i \times OF_i \right)$$
(1)

Where E_{CO2} is the total equivalent carbon emissions in a year, Gg CO₂-eq/year W_p is the total mass of waste processed in facility, Gg/year M_i is the mass fraction of material *i* in the waste stream dm_i is the dry matter fraction of waste material *i* (DVs in Table 1) CF_i is the fraction of carbon in the dry matter of waste material *i* (DVs in Table 1) FCF_i is the fraction of fossil carbon in the total carbon of waste material *i* (DVs in Table 1) OF_i is the oxidation factor (DV=1)

2- Calculate the energy produced, EP, through incineration.

$$EP = W_d \times \eta \times \sum (M_i \times CV_i)$$
⁽²⁾

Where EP is the energy production from facility, kWh

 W_d is the dry weight of waste processed, kg

 η is the efficiency of energy conversion within incinerators (DV=0.30)

 M_i is the mass fraction of material *i* in the waste stream

 CV_i is the calorific value of material *i*, kWh/kg (DVs in Table 1)

3- Calculate the net present value of the incineration facility.

$$NPV = \sum_{1}^{t} \left\{ \left[\left(W_p \times TF \right) + (EP \times ET) - CAPEX_t - OPEX_t \right] \times (1+i)^{-t} \right\}$$
(3)

Stoichiometric parameters, energy of	content, and	DOC value	s of vario	us waste f	ractions.	
Parameter*	Paper	Plastic	Glass	Wood	Textiles	01

Parameter*		Paper	Plastic	Glass	Wood	Textiles	Organics	Metal	Others
Stoichiometric	n	3.6	5.0	0.0	4.1	1.0	0.0	3.7	3.4
parameters	a	5.8	7.1	0.0	6.1	1.7	0.0	6.4	5.6
	b	2.8	1.4	0.0	2.7	0.7	0.0	1.8	2.4
	с	0.020	0.000	0.000	0.007	0.040	0.000	0.020	0.100
Dry matter fraction	on (dm _i)	0.40	-	-	0.43	0.24	0.15	-	-
Dry matter carbo	n fraction (CF _i)	0.46	0.75	0.00	0.50	0.50	0.38	0.00	0.03
Fossil carbon frac	tion (FCF _i)	0.01	1.00	0.00	0.00	0.20	0.00	0.00	1.00
Calorific value (Btu/kg)		14,991	30,865	0	16,094	17,857	5291	661	11,464
Degradable organ	ic carbon (DOC _i)	0.40	-	-	0.43	0.24	0.15	-	-

* [2]: from a study conducted for the US Department of Health, Education and Welfare on different waste streams, and results were orginially reported as percentage of total mass; [9]: from the Intergovernmental Panel on Climate Change (IPCC) guidelines for national greenhouse gas inventories; [8]: compiled from full-scale WTE facilities in China.



Fig. 1. Proposed framework of the multi-objective optimization model.

Where *NPV* is the net present value, USD W_p is the total mass of waste processed in facility, Gg/year *TF* is the tipping fee per 1000 ton of waste, USD/Gg *EP* is the energy production from facility, kWh *ET* is the electricity tariff, USD/kWh *CAPEX_t* is the capital investment costs in year *t*, USD *OPEX_t* is the operational and maintenance costs in year *t*, USD *i* is the discount rate (%) *t* is the economic life of the project (year)

Anaerobic digester (AD)

Table 1

4- Calculate the equivalent carbon emissions, E_{CO_2} , from AD plants, as per tier 2 of the Intergovernmental Panel on Climate Change (IPCC) guidelines [9].

$$E_{CO_2} = W_p \times EF \times (1 - R) \times GWP \tag{4}$$

Where E_{CO2} is the total equivalent carbon emissions in a year, Gg CO₂-eq/year W_p is the total mass of waste processed in facility, Gg/year *EF* is the emission factor, g CH₄/g waste (DV=0.0008) *R* is the fraction of CH₄ recovered (DV=0.90)

GWP is the global warming potential of methane (DV=28)

5- Calculate the energy produced, *EP*, through AD based on the general formula of waste materials $C_n H_a O_b N_c$ (modified from [7,8]).

$$EP = \sum \left[\frac{(8 \times n) - (2 \times a) - (4 \times b) - (6 \times c)}{(12.01 \times n) + (1.01 \times a) + (16.00 \times b) + (14.01 \times c)} \right] \times W_d \times EC_{CH_4} \times \eta$$
(5)

Where *EP* is the energy production from facility, kWh n, a, b, and c are the normalized mole ratio of *C*, *H*, *O*, and *N* in waste material *i* (DVs in Table 1) W_d is the dry weight of waste processed, kg

EC_{CH4} is the energy content of methane, kWh/kg (DV=14.31)

 η is the efficiency of energy conversion within AD plants (DV=0.30)

6- Calculate the net present value of the AD plant (similar to Step 3)

Sanitary landfill with gas recovery

7- Calculate the equivalent carbon emissions, E_{CO_2} , from landfill, as per tier 2 of the IPCC guidelines [3].

$$E_{CO_2} = W_p \times \sum \left(M_i \times DOC_i \right) \times DOC_F \times MCF \times F \times \left(\frac{16}{12}\right) \times (1 - R) \times (1 - OX) \times GWP$$
(6)

Where E_{CO2} is the total equivalent carbon emissions in a year, Gg CO₂-eq/year

 W_p is the total mass of waste processed in facility, Gg/year

 M_i is the mass fraction of material *i* in the waste stream

 DOC_i is the degradable organic carbon of material *i* (DVs in Table 1)

 DOC_F is the fraction DOC dissimilated (DV=0.77)

MCF is the methane correction factor (DV=0.60)

F is the methane fraction in landfill gas (DV=0.50)

R is the fraction of methane recovered (DV=0.70)

OX is the oxidation factor (DV=0)

GWP is the global warming potential of methane (DV=28)

8- Calculate the energy produced, EP, through landfill gas recovery.

$$EP = E_{CH_4} \times R \times EC_{CH_4} \times 10^6 \times \eta \tag{7}$$

Where EP is the energy production from facility, kWh

 E_{CH4} is the total methane emissions in a year, Gg CH₄/year (using Eq. (6) excluding the (1-R) and *GWP* terms).

R is the fraction of methane recovered (DV=0.70)

EC_{CH4} is the energy content of methane, kWh/kg (DV=14.31)

 η is the efficiency of energy conversion in landfill gas combustion facilities (DV=0.30)

9- Calculate the net present value of the sanitary landfill site (similar to Step 3)

Modelling and optimization

The mixed integer linear programming model formulated in Abdallah et al. [1] is solved using the WCCM. The WCCM requires dealing with the model's objective functions individually and then developing a new objective function that combines all objectives [4–6]. Fig. 2 illustrates the process of applying WCCM for the waste management strategies. The process starts by solving the mathematical model for each objective function separately subject to all the constraints (Steps 1, 2 and 3 in Fig. 2).

Table 2

Input data needed to run the optimization model.

Demand The quantities of waste available from each material and each year. The input data sho organized in a matrix form, where the rows are the materials (food, recyclable and m	ould be
and the columns are the years.	ion-recyclable)
CO2 The carbon footprint equivalent of each material resulting from each strategy calculated (4), and (6). The input data should be organized in a matrix form, where the rows an (food, recyclable and non-recyclable) and the columns are the strategies (anaerobic d incinerator, and landfill).	d using Eqs. (1), re the materials ligester,
CO2_2 The carbon footprint equivalent of digestates and ashes resulting from each strategy ca Eqs. (1), (4), and (6). The input data should be organized in a matrix form, where the the digestate and the second row is for the ashes. The columns represent the strateg digester, incinerator, and landfill).	lculated using e first row is for ;ies (anaerobic
Energy The energy recovery of each material resulting from each strategy calculated using Eqs (7). The input data should be organized in a matrix form, where the rows are the marecyclable and non-recyclable) and the columns are the strategies (anaerobic digester and landfill).	. (2), (5), and aterials (food, r, incinerator,
Energy_2 The energy recovery of digestates and ashes resulting from each strategy calculated usi and (7). The input data should be organized in a matrix form, where the first row is digestate and the second row is for the ashes. The columns represent the strategies (digester, incinerator, and landfill).	ing Eqs. (2), (5), for the (anaerobic
CAPEX The CAPEX value of each material under each strategy calculated using Eq. (3). The inp be organized in a matrix form, where the rows are the materials (food, recyclable an non-recyclable) and the columns are the strategies (anaerobic digester, incinerator, an	out data should Id nd landfill).
CAPEX_2 The CAPEX value for digestates and ashes using different strategies calculated using Eq data should be organized in a matrix form, where the first row is for the digestate a row is for the ashes. The columns represent the strategies (anaerobic digester, incine landfill).	. (3). The input nd the second rator, and
Profit_S1, The NPV profit for each material in each year calculated using Eq. (3). The input data s Profit_S2, organized in a matrix form, where the rows are the materials (food, recyclable and m Profit_S2 and the columns can be calculated using Eq. (3).	should be non-recyclable)
Profit_Dig The NPV profit of digestates for each strategy in each year calculated using Eq. (3). The should be organized in a matrix form, where the rows are the strategies and the colugers.	e input data umns are the
Profit_Ash The NPV profit of ashes in each year calculated using Eq. (3). The input data should be one row, where the columns are the years.	organized in a
A1, A2, A3 A single value used in the multi-objective code (WCCM.mod) representing the importative profit, carbon footprint and energy recovery objective function, respectively.	nce weight of
Popt A single value used in the multi-objective code (WCCM.mod). It represents the optimal solving the problem for maximization of the profit objective only (Profit.mod).	l value from
Eopt A single value used in the multi-objective code (WCCM.mod). It represents the optimal solving the problem for maximization of the energy recovery objective only (Energy.	l value from mod).
Copt A single value used in the multi-objective code (WCCM.mod). It represents the optimal solving the problem for minimization of the carbon footprint objective only (Emissio	l value from n.mod).

 Step 1: (a) Run Emission.mod: to minimize the total carbon footprint (b) Run Energy.mod: to maximize the total energy recovery (c) Run Profit.mod: to maximize the total financial profit 	 Store:(a) Optimal total carbon footprint(b) Optimal total energy(c) Optimal total financial profit recovery	η
Step 2: Compile expert judgement using Fuzzy AHP	 Store: Relative importance weights of the objectives	Н
	Step 3: Minimize the total variation from all objective functions [Run WCCM.mod]	•

Fig. 2. Multi-objective optimization framework.

Next, based on the expert opinions, the importance weights of each objective function are determined using Fuzzy Analytical Hierarchy Process (AHP).

The mathematical model and the solution approach for the multi-objective formulation, the WCCM, have been implemented using the optimization programming language (OPL) in the CPLEX software (by IBM). The code files are available in the Supplementary Files. Table 2 describes the input data needed to run the model.

The code files (Emission.mod, Energy.mod, and Profit.mod) should be run first in any sequence to obtain the optimal objective value for each single objective function. Then the code file (WCCM.mod) should be run to obtain the multi-objective solution.

Conclusion

In this paper, the methodology used in the multi-objective waste management optimization problem was presented. The equations used in obtaining the input data of the mathematical model were detailed. Additionally, all software codes used to solve the formulated mathematical model were provided and thoroughly described. The codes are based on the optimization programming language of CPLEX. The presented model can be effectively utilized to generate a comprehensive waste management master plan that satisfies the specific goals of decision makers. For future research work, the analysis framework and codes can be modified to account for more features and objectives. Moreover, evolutionary methods, such as genetic algorithms, can be utilized to effectively solve the optimization problem.

Declaration of Competing Interest

The Authors confirm that there are no conflicts of interest.

Supplementary materials

Supplementary material associated with this article can be found, in the online version, at doi:10. 1016/j.mex.2020.101203.

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