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Current knowledge about physical properties of innovative probiotic spray-dried powders produced with lactose-free milk and prebiotics

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**Adriana Dantas:** Conceptualization, Investigation, Validation, Formal analysis, Resources, Data curation, Writing – Original draft, Writing – Review and Editing, Visualization. **Silvani Verruck:** Conceptualization, Resources, Data curation, Writing – Original draft. **Maria Helena Machado Canella:** Resources, Data curation, Writing – Original draft. **Bruna Marchesan Maran:** Resources, Data curation, Writing – Original draft. **Fabio Seigi Murakami:** Resources, Data curation, Writing – Original draft. **Lindiomar Borges de Avila Junior:** Resources, Data curation, Writing – Original draft. **Carlos Eduardo Maduro de Campos:** Resources, Data curation, Writing – Original draft. **Eduard Hernandez:** Conceptualization, Validation, Formal analysis, Resources, Data curation, Writing – Original draft, Writing – Review and Editing, Visualization, Supervision. **Elane Schwinden Prudencio:** Conceptualization, Investigation, Validation, Formal analysis, Resources, Data curation, Writing – Original draft, Writing – Review and Editing, Visualization. Writing – Review & Editing. Supervision, Project administration, Funding acquisition.

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1 **Current knowledge about physical properties of innovative probiotic spray-dried**  
2 **powders produced with lactose-free milk and prebiotics**

3

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26 **Abstract**

27

28 Lactose-free probiotic powders were obtained by mixing *Bifidobacterium* BB-12  
29 suspensions with lactose-free milk powder or lactose-free milk powder and prebiotics  
30 (inulin or oligofructose). A thorough investigation was performed to know their water  
31 sorption properties and physical and thermal characteristics. By evaluating the water  
32 sorption properties, the Peleg model fitted well to the experimental sorption data,  
33 showing that the equilibrium moisture content of powders increased as the relative  
34 humidity increased. The isotherm found for all samples was a Type III Isotherm,  
35 commonly observed in most foods. For both morphology and particle size, the use of  
36 different carrier agents affected these properties; however, all the spray-dried powders  
37 presented good size to be added in food products. X-ray diffraction and Raman  
38 spectroscopy showed us amorphous structure for all powders, and typical bands of the  
39 milk constituents and sugars, respectively. Regarding the spray-dried powders thermal  
40 properties, it was possible to confirm that the addition of prebiotics gave higher thermal  
41 stability, highlighting the sample produced with inulin. We concluded that a good  
42 quality of lactose-free milk based probiotic powder could be obtained using spray  
43 drying technique, with great potential to be applied in lactose-free dairy products.

44

45 **Keywords:** *Bifidobacterium* BB-12; microencapsulation; lactose-free microspheres;  
46 physical characterization; prebiotics.

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## 51 **1. Introduction**

52

53 The probiotics market was valued at USD 48.88 billion in 2019 and is estimated  
54 to increase to USD 94.48 billion by 2027. This expansion is owing to consumer  
55 perception about the health benefits of probiotic-based products, in addition to the  
56 demand for immunity-boosting products amid COVID-19 (Market Research Report,  
57 2020). In this context, the microencapsulation of probiotic cells within dairy matrices is  
58 already a widespread and accepted technology, as well as the joint use of prebiotic  
59 carbohydrates. Due to the unfavorable conditions encountered by probiotic  
60 microorganisms when present in a food matrix (for example, changes in pH, water  
61 activity, temperature, and oxygen content), the production of powdered probiotic  
62 ingredients is necessary. In addition to ensuring the arrival to the colon in adequate  
63 quantities (Verruck et al., 2017), this type of presentation allows longer storage and  
64 versatility in applications.

65 Milk-based probiotic powders have already ready been applied in several types  
66 of dairy products (Pinto et al., 2017; Verruck et al., 2020; Gul, 2017), including lactose-  
67 free dairy (Pinto et al., 2019). However, the addition of these microspheres in lactose-  
68 free dairy constitutes a source of product contamination. Given the world scenario of  
69 lactose intolerance (about 70% of the world's adult population is lactose-intolerant)  
70 (Lule, Garg, Tomar, Khedkar, & Nalage, 2016), products free of this disaccharide are  
71 essential to make up the diet of intolerant people. In this state, the individual cannot  
72 digest and absorb dietary lactose, due to deficiency in  $\beta$ -galactosidase, the enzyme that  
73 is responsible for lactose hydrolysis. This condition leads to gastrointestinal  
74 manifestations such as diarrhea, vomiting, abdominal cramps, and gas (Suri et al.,

75 2019). In this context, the development of a lactose-free probiotic powder would meet  
76 this specific population demand.

77 Probiotic powders obtained by spray drying are usually microparticles in the  
78 amorphous state (Arslan-Tontul, 2020; Verruck, de Liz, Dias, Amboni, & Prudencio,  
79 2019; Wang, Lin, & Zhong, 2020). This amorphous structure is associated with the  
80 presence of carbohydrates in the dehydration media, and has also been related to the  
81 improved stability of spray-dried microorganisms (Chávez & Ledebøer, 2007; Passot,  
82 Cenard, Douania, Tréléa, & Fonseca, 2012; Vivek, Mishra, & Pradhan, 2020).  
83 Depending on the temperature and relative humidity at which a powder product is  
84 subjected, it becomes susceptible to interactions with water, resulting in unwanted  
85 characteristics such as agglomeration, difficulty in rehydration, and triggering Maillard  
86 reactions. These physical changes can negatively interfere with the microencapsulated  
87 bacteria, leading to partial release or mortality. In other words, the physical state of  
88 microparticles enhances or minimizes the probability of chemical changes. Zhu, Ying,  
89 Sanguansri, Tang, and Augustin (2013) employed whey protein isolate, maltodextrin, D-  
90 glucose, and L-glucose as encapsulant matrices of *Lactobacillus rhamnosus* GG. D-  
91 glucose, which can be used by probiotic for energy, clearly exerted a physico-chemical  
92 action in stabilizing the bacteria. Likewise, the authors noted that water activity ( $a_w$ ) of  
93 the probiotic powders had a large effect on the cell viability during storage.  
94 Independently of the rubbery or glassy state of the powders, an increase in  $a_w$  carried a  
95 quicker reduction in the culturability of *L. rhamnosus* during storage. At a high  $a_w$  level  
96 (0.70), it was not observed effect of glucose in cell survival, but at 0.33 ( $a_w$  most  
97 commonly found in dried products), glucose incorporation greatly improved the cell  
98 preservation for 35 days compared to a glucose-free carrier. Besides, Romano, Mobili,  
99 Zuñiga-Hansen, and Gómez-Zavaglia (2018) evaluated the stability of a bacteria with

100 probiotic properties after it was spray-dried with amorphous inulin. The bacteria  
101 stability was considered to depend mainly on the  $a_w$  in which the powder was stored.  
102 Thus,  $a_w < 0.40$  resulted in stable cell viability for up to 180 days of storage; whereas,  
103 when samples were stored at  $a_w$  above this value, microorganisms experienced a  
104 significant reduction in their viability. Given all the above, the study of the water  
105 adsorption kinetic becomes a valuable tool in the investigation of powders, since this  
106 analysis can help in the selection of suitable packaging materials and storage conditions  
107 (Rhim, Koh, & Kim, 2011). In conjunction with this examination, we also believe that  
108 the study of sorption isotherms is essential in identifying optimal storage conditions, as  
109 it predicts and models the moisture changes that occur during this period. Consequently,  
110 the shelf life of many products can be predicted. Santos and Machado (2021) produced  
111 probiotic particles based on alginate–chitosan and studied their sorption isotherms. In  
112 addition, the authors used FT-IR analyses to qualitatively examine the presence of  
113 bindings in structures generated from the mixtures. Other researchers have also studied  
114 the water sorption behavior of probiotic powders produced by spray drying from  
115 different carrier agents (Agudelo, Cano, González-Martínez, & Chiralt, 2017;  
116 Guergoletto, Busanello, & Garcia, 2017; Romano et al., 2018; Vivek et al., 2020; Ying  
117 et al., 2016).

118 According to Verruck, Santana, de Oliveira Müller, and Prudencio (2018),  
119 thermal analysis techniques, such as differential scanning calorimetry and  
120 thermogravimetry, can be effectively used to determine the phase transition  
121 temperatures in spray-dried powders, as well as the degradation temperatures of its  
122 components. Moreover, Pinto et al. (2015), Muhammad, Ramzan, Huo, Tian, and Bian  
123 (2017), Dias et al. (2018), and De Liz et al. (2020) observed a close relationship  
124 between the probiotic powders thermal properties and the viable cells count.

125 In this work, lactose-free milk, oligofructose, and inulin were carefully selected  
126 and evaluated in order to know their properties for future food applications. Thus, this  
127 study is intended to assess the physical stability of probiotic powders (based on thermal  
128 and water sorption properties analyses), as well as to characterize them in terms of  
129 morphology and structure.

130

## 131 **2. Material and methods**

132

### 133 **2.1. Material**

134

135 Lactose-free skim milk powder (Aurora<sup>®</sup>, Cooperativa Central Aurora  
136 Alimentos, Santa Catarina, Brazil) (85.51 g total solids 100 g<sup>-1</sup>, 32.50 g protein 100 g<sup>-1</sup>,  
137 0.00 g fat 100 g<sup>-1</sup>, 3.01 g ash 100 g<sup>-1</sup>, and 50.00 g carbohydrates 100 g<sup>-1</sup>) and the  
138 prebiotics inulin (Orafti<sup>®</sup> Gr, Orafti, Tienen, Belgium) (DP ≥ 10) and oligofructose  
139 (Orafti<sup>®</sup> P95, Orafti, Tienen, Belgium) (DP = 2–8) were used as microsphere carrier  
140 agents. *Bifidobacterium* BB-12 (Nu-trish<sup>®</sup> BB-12<sup>®</sup>, Chr. Hansen, Hønsholm, Denmark)  
141 was used as the active material for the microspheres, while UHT (ultra-high  
142 temperature) lactose-free milk (3.2 g 100 g<sup>-1</sup> of proteins, 5.0 g 100 g<sup>-1</sup> of carbohydrates  
143 and 0.40 g 100 g<sup>-1</sup> of lipids) was employed to prepare the bacterial suspension. The  
144 water sorption kinetics and moisture adsorption isotherms were conducted using salts of  
145 analytical grade.

146

### 147 **2.2. Microencapsulation of *Bifidobacterium* BB-12 and viable probiotic cell count**

148



149 Three feed solutions were prepared for the production of spray-dried powders  
150 containing *Bifidobacterium* BB-12. Therefore, the feed solutions designated as 1, 2, and  
151 3, presented lactose-free skim milk powder ( $200 \text{ g L}^{-1}$ ); lactose-free skim milk powder  
152 ( $100 \text{ g L}^{-1}$ ) and inulin ( $100 \text{ g L}^{-1}$ ); and lactose-free skim milk powder ( $100 \text{ g L}^{-1}$ ) and  
153 oligofructose ( $100 \text{ g L}^{-1}$ ), respectively. All of them were prepared with sterile distilled  
154 water and heat-treated for 30 min at  $80 \text{ }^{\circ}\text{C}$ . After the solutions were cooled down to  
155 room temperature ( $25 \text{ }^{\circ}\text{C}$ ), a precipitate of probiotic cells was added to each of them. A  
156 laboratory-scale spray dryer (B-290 mini spray dryer, Buchi, Flawil, Switzerland)  
157 equipped with a cyclone was used. The feed solutions containing *Bifidobacterium* BB-  
158 12 were kept under magnetic agitation (MS-3000, BioSan, Riga, Latvia) at room  
159 temperature, and spray dried under optimum conditions of  $150 \text{ }^{\circ}\text{C}$  inlet temperature and  
160  $44 \text{ }^{\circ}\text{C}$  outlet temperature to obtain probiotic spray-dried powders. The mini spray dryer  
161 has an integrated standard two-fluid nozzle, where compressed air is used to disperse  
162 the liquid body into fine droplets. The nozzle consists of a  $0.7 \text{ mm}$  liquid orifice  
163 diameter, a  $1.1 \text{ mm}$  liquid outer diameter, and a  $1.5 \text{ mm}$  gas orifice diameter. This  
164 geometry results in a mixing of fluid body and gas. Therefore, the feed solution was  
165 sprayed by the nozzle in a closed cylindrical container, in which the droplets dry during  
166 their fall onto the container wall due to the hot-air flow. The powder and wet air were  
167 separated in the cyclone, and then, the sample was collected from the cyclone base. The  
168 compressor air pressure, drying airflow rate, and feed rate were set at  $0.7 \text{ MPa}$ ,  $35$   
169  $\text{m}^3 \text{ h}^{-1}$ , and  $12 \text{ mL min}^{-1}$ , respectively. The powders were denoted as 1, 2, and 3, and  
170 were derived from feed solutions 1, 2, and 3, respectively. They were packed in  
171 aluminum pouches under vacuum (200 B, Selovac, São Paulo, Brazil).

172 For enumeration of entrapped cells,  $1 \text{ g}$  of spray-dried powder was previously  
173 vortexed with  $9 \text{ mL}$  of sterile phosphate buffer ( $\text{pH } 7.0$ ,  $0.1 \text{ mol L}^{-1}$ ) for  $10 \text{ min}$ . Then,

174 the pour plate method described by Vinderola and Reinheimer (1999) was used. For  
175 this, mixtures and feed solutions were serially diluted in peptone water (Oxoid; 0.1 g  
176 100 mL<sup>-1</sup>), and plated on MRS agar modified with the addition of 0.3 g 100 g<sup>-1</sup> sodium  
177 propionate (Fluka, Neu-Ulm, Germany) and 0.2 g 100 g<sup>-1</sup> lithium chloride (Vetec, Rio  
178 de Janeiro, Brazil). The plates were incubated in anaerobic jars containing AnaeroGen®  
179 at 37 °C during 72 h. Results were expressed as log colony-forming units per gram (log  
180 CFU g<sup>-1</sup>).

181

### 182 **2.3. Water sorption properties**

183

184 The kinetics of water absorption was studied by fitting the Peleg model to the  
185 experimental data. For this, the methodology proposed by Verruck et al. (2018) was  
186 used. Probiotic spray-dried powders were dehydrated at 105 °C until reaching constant  
187 weight, thus, their initial moisture contents ( $X_0$ ) were measured. After drying, triplicate  
188 samples (~ 0.5 g) were placed at 25 °C in separate desiccators that contained different  
189 saturated salt solutions. The saline solutions provided, inside the desiccators, an  
190 environment with a relative humidity that varied from 11 to 90%. The sample mass was  
191 measured periodically until reaching the hygroscopic equilibrium that was concluded  
192 when the sample showed two similar consecutive weightings. The time required to  
193 reach that thermodynamic equilibrium varied according to the different relative  
194 humidity in which the samples were exposed, that is, 11.25 h in the 11% relative  
195 humidity, reaching 6 days for the relative humidity of 80 and 90%. The moisture  
196 adsorption curves of the samples were fitted to Equation (1) (Peleg, 1988).

$$197 \quad X_{(t)} = X_0 + \frac{t}{k_1 + k_2 t} \quad (1)$$

198 where  $X_{(t)}$  is the water content of the powder for a given instant of time (g water / g dry  
 199 solid),  $X_0$  is the initial moisture of the powder (g water / g dry solid),  $t$  is the time (h),  $k_1$   
 200 is the Peleg rate constant (g dry solid h / g water), and  $k_2$  is the Peleg capacity constant  
 201 (g dry solid / g water).

202 The moisture adsorption isotherms of the probiotic spray-dried powders  
 203 previously dehydrated were determined through the static method, using saturated saline  
 204 solutions to obtain different air relative humidity as described by Labuza, Kaanane, and  
 205 Chen (1985). The empirical mathematical model of GAB (Equation 2) was employed to  
 206 retract the experimental equilibrium data (Al-Muhtaseb, McMinn, & Magee, 2002). The  
 207 parameters of the model were estimated by nonlinear regression using the  
 208 STATISTICA 13.3 software (TIBCO Software Inc., Palo Alto, CA).

$$209 \quad X_{eq} = \frac{M_0 C k a_w}{(1 - k a_w)(1 - k a_w + C k a_w)} \quad (2)$$

210 where  $X_{eq}$  is the equilibrium moisture (g water / g dry solid),  $M_0$  is the moisture content  
 211 in the monolayer (g water / g dry solid),  $a_w$  is the water activity, and  $C$  and  $k$  are model  
 212 constants.

213

## 214 **2.4. Physical characterization of probiotic powders**

215

### 216 *2.4.1. Morphology and particle size*

217

218 The morphology and particle size of the spray-dried powders were observed with  
 219 a Jeol scanning electron microscope, model JSM 6390 LV (Jeol, Tokyo, Japan), at an  
 220 accelerating voltage of 5 kV. Therefore, the microparticles were fixed with carbon tape  
 221 on a stub (this was carried out on the day of obtaining the powders) and covered with  
 222 gold.

223 The diameter of the powders was estimated from the SEM micrographs in their  
224 initial magnification using ImageJ (version 1.51k; <http://rsb.info.nih.gov/ij/>). The  
225 diameter of 120 particles from each of the powders was measured (Fritzen-Freire et al.,  
226 2012).

227

#### 228 *2.4.2. X-Ray diffraction*

229

230 X-ray powder diffraction (XRPD) analysis of the spray-dried powders was  
231 performed on an XPERT PANalytical diffractometer, equipped with an X'Celerator  
232 detector and using filter radiation of Cu K $\alpha$  ( $\lambda = 1.5418 \text{ \AA}$ ), the tension of 45 kV and  
233 current of 40 mA. Samples were analyzed at a scattering range of  $4^\circ < 2\theta < 60^\circ$  with  
234  $0.12^\circ$  stepsize and 30 s counting time with at least 5 scans averaged to improve data  
235 statistics.

236

#### 237 *2.4.3. Raman spectroscopic analysis*

238

239 Raman spectra of spray-dried powders and prebiotics samples were obtained  
240 with a PeakSeeker PRO-785 Raman spectrometer using a 50 X objective lens at room  
241 temperature. Raman system with a diode laser of 785 nm and 300 mW at the source  
242 were employed. Raman spectra were collected at  $6 \text{ cm}^{-1}$  resolution in the range of 200–  
243  $2000 \text{ cm}^{-1}$  with a Peltier-cooled charge-coupled device CCD detector.

244

#### 245 *2.4.4. Thermal properties*

246

247 For obtaining of the thermogravimetry/derivative thermogravimetry  
248 (TGA/DrTGA) curves, it was used a DTG-60 thermobalance (Shimadzu DTG-60,  
249 Kyoto, Japan) previously calibrated with calcium oxalate. Six milligrams of each spray-  
250 dried powder were placed in an aluminum pan. Then, a heating rate of  $10\text{ }^{\circ}\text{C min}^{-1}$  was  
251 employed to heat the sample from 30 to  $300\text{ }^{\circ}\text{C}$ , maintaining a dynamic synthetic air  
252 atmosphere of  $50\text{ mL min}^{-1}$ .

253 The spray-dried powders and the raw materials were submitted to differential  
254 scanning calorimetry (DSC) (Shimadzu DSC-60, Kyoto, Japan). A standard reference of  
255 indium was used for preliminary calibration of equipment. So, approximately two  
256 milligrams of sample were placed in aluminum pans covered with a lid. All  
257 measurements were performed at  $10\text{ }^{\circ}\text{C min}^{-1}$  under a dynamic synthetic air atmosphere  
258 of  $50\text{ mL min}^{-1}$ , and in a temperature range of 30 to  $300\text{ }^{\circ}\text{C}$ .

259

## 260 **2.5. Statistical analysis**

261

262 The mean and standard deviation (SD) were calculated from data obtained in  
263 triplicate. The one-way analysis of variance (ANOVA) was conducted using the  
264 STATISTICA version 13.3 software (TIBCO Software Inc., Palo Alto, CA).  
265 Differences between treatments mean values were analyzed using the Tukey test at a  
266 significance level of 0.05.

267

## 268 **3. Results and discussion**

269

### 270 **3.1. Probiotic viability**

271

272 The viable probiotic cell count in the feed solutions, and in the spray-dried  
273 powders were higher than 10.00 log CFU g<sup>-1</sup>, and 9.00 log CFU g<sup>-1</sup>, respectively.  
274 Therefore, all spray-dried powders are considered a probiotic product.

275

### 276 **3.2. Water sorption properties**

277

278 Peleg's constants at different relative humidity are shown in Table 1. Khazaei  
279 and Mohammadi (2009) affirm that the constant  $k_1$  is related to the initial rate of  
280 absorption, and the lower its value, the higher the initial mass transfer rate. Therefore,  
281 we can also study it through its reverse ( $1/k_1$ ). For all samples, the values found for this  
282 constant showed sensitive but significant changes ( $P < 0.05$ ) when the relative humidity  
283 where the sample was conditioning increased. There was a tendency to increase the  
284 values of  $1/k_1$  with the increase of the relative humidity, mainly from 11% for the other  
285 relative humidity. This behavior was already expected, as according to Verruck et al.  
286 (2018), the initial rate of absorption depends of the difference between the moisture  
287 content of the sample and the moisture content of the environment (saturation  
288 humidity). In other words, the higher the moisture gradient, the higher the initial rate of  
289 absorption, since the gradient is the driving force of the process. Besides, these values  
290 may be explained due to the high hydrophilicity of the components (carbohydrates and  
291 protein) (Zhang, Kim, Yokoyam, & Kim, 2018). Wang et al. (2020) affirmed that at  $a_w$   
292 between 0 and 0.34, the numerous polar groups of proteins are known as the primary  
293 component absorbing water because they can strongly and rapidly absorb water via  
294 hydrogen bonding. The high hydration of the casein micelles in their native structure  
295 (3.7 mL H<sub>2</sub>O g<sup>-1</sup> protein) contributes to this (Schuck, 2011).

296 According to Khazaei and Mohammadi (2009), the constant  $k_2$  of the Peleg's  
297 model is inversely related to the maximum water adsorption capacity, i.e., the lower the  
298  $k_2$ , the higher the water absorption capacity of the product. In our work,  $1/k_2$  values  
299 increased with the increase of the relative humidity ( $P < 0.05$ ) (Table 1), especially at  
300 the highest relative humidity (80 and 90%). The adsorption of moisture is due to the  
301 movement of water (water vapor available to make exchanges with the sample), given  
302 the difference in water vapor pressure between the product surface and the air  
303 surrounding it. Consequently, from the moment that we increase the relative humidity  
304 inside the desiccator, the vapor pressure of air also increases, which explains the values  
305 of  $1/k_2$  found. Spray-dried powder 1 sample showed the highest value of  $1/k_2$  at 90%  
306 relative humidity (0.6936), followed by spray-dried powder 3 (0.5706), and finally,  
307 spray-dried powder 2 (0.4860). As occurred in the work by Verruck et al. (2018), higher  
308 values of  $1/k_2$  were correlated with the highest equilibrium moistures observed during  
309 the experiments, since the equilibrium moistures of the samples when subjected to the  
310 environment with 90% relative humidity were 0.6551, 0.5295, and 0.4637 g water g<sup>-1</sup>  
311 dry solid for spray-dried powders 1, 3 and 2, respectively. Our results for all samples  
312 are also in agreement with those obtained by Vivek et al. (2020), who studied probiotic  
313 spray-dried powder obtained from Sohiong fruit. In both cases, the equilibrium moisture  
314 content increased as the relative humidity increased.

315 The higher values of  $1/k_2$  constant and equilibrium moisture for spray-dried  
316 powder 1 may be explained by the higher amount of short-chain carbohydrates glucose  
317 and galactose, they are simpler carbohydrates compared to the prebiotics used in the  
318 other preparations. Saavedra-Leos et al. (2014) reported that more water molecules can  
319 be readily absorbed by these carbohydrates, given a higher content of OH groups on  
320 their surfaces. Moreover, Jimenez-Sánchez, Calderón-Santoyo, Ortiz-Basurto, Bautista-

321 Rosales, and Ragazzo-Sánchez et al. (2018) highlighted that the lower the degree of  
322 polymerization of a product, the more hygroscopic it will be. On the other hand, Pilatti-  
323 Riccio et al. (2019) reported that, given the high hygroscopicity, the use of short-chain  
324 carbohydrates in mixtures of wall materials is advantageous because it can result in a  
325 fast release of encapsulated compounds. Another factor that is closely related to the  
326 moisture and water activity of a sample is the glass transition temperature ( $T_g$ ).  
327 Galactose and glucose present lower  $T_g$  than oligofructose and inulin (30, 31, 102, and  
328 132 °C, respectively) (Schuck et al., 2005; Silva, Zabet, Bargas, & Meireles, 2016;  
329 Hinrichs, Prinsen, & Frijlink, 2001). Juliano and Barbosa-Cánovas (2010) discussed  
330 that a glass transition temperature nearby to room temperature favors water absorption,  
331 and as consequence, it can bring technological problems to milk powder such as  
332 rehydration difficulty, particle agglomeration, and caking.

333 Chirife, Timmermann, Iglesias, and Boquet (1992) stated that a mechanistic  
334 approach is needed for a full-proof validation, that is, a mere fitting of the sorption  
335 model to the experimental data cannot guarantee its validity. We concluded that the  
336 Peleg model fits exceptionally well to the experimental data because, in addition to  
337 showing high values of  $R^2$  and low values of SSE (Table 1), randomness in the  
338 standardized residual plots was observed in all cases. Moreover, it was noticed a good  
339 fit in the highest, intermediate, and the lower relative humidity, providing adequate  
340 values of the initial rates of water adsorption and maximum water adsorption capacity.  
341 Given its relative simplicity, Peleg's model has been used satisfactorily by several  
342 authors to represent hydration kinetics in dairy products (Seth, Dash, Mishra, & Deka,  
343 2018; Ruano-Uscategui, Ciro-Velásquez, & Sepúlveda-Valencia, 2018; Verruck et al.,  
344 2018; Liang, Bund, & Hartel, 2009; Varghese, Ramachandrannair, & Mishra, 2009).



345 Vivek et al. (2020) emphasized that data obtained from the isotherm study can  
346 be useful to define process condition, transport, and storage, to predict desorption or  
347 adsorption behavior of the powder and the shelf life of the material. It can also be used  
348 to describe the energy requirements of a dehydration process. Experimental data of  
349 adsorbed moisture content (equilibrium moisture) as a function of  $a_w$  was well described  
350 by the Guggenheim–Anderson–Boer (GAB) model (Fig. 1). The data for all probiotic  
351 powders followed a type III isotherm behavior. In addition to indicating the formation  
352 of multilayer, the type III isotherm curve is related to the presence of amorphous sugars  
353 and their dissolution in water (Rao & Rizvi, 1994).

354 Reid and Fennema (1996) stated that the isotherms are classified into three  
355 regions, as follows: first, monolayer moisture region, which includes  $a_w$  less than 0.2 to  
356 0.3; second, multilayer moisture region, which comprises  $a_w$  between about 0.2 and 0.3  
357 until approximately 0.8; and third, free water region, that represents the most mobile  
358 and least bound water in foods. In region III,  $a_w$  are equals to 0.8–0.99, and it was in this  
359 region that the samples showed a drastic increase in the adsorption of water. According  
360 to Verruck et al. (2018), in this region, the product can undergo some microbiological  
361 alteration, chemical, or biochemistry because of the available water.

362 The coefficients of the GAB model were presented in Table 2. The coefficient of  
363 determination ( $R^2$ ) and Sum of Squares Error (SSE) indicate excellent fit of the model  
364 to the experimental data, due to their proximity to 1 and 0, respectively. Moreover, the  
365 distribution of the residuals was randomly around zero.  $M_0$  value means the monolayer  
366 moisture content on dry basis, and it indicates a strong binding potency of water on the  
367 surface of the product if moisture content remains above this value. Therefore, this  
368 information is vital for the storage stability of food products. The values of parameter C  
369 represent the heat of sorption of monolayer moisture while the parameter k provides the

370 binding potency of water in terms of heat of sorption of multilayer moisture. For all of  
371 our spray-dried powders, the values of parameter C were higher than those values of k.  
372 Seth et al. (2018) also noted similar behavior for spray dried yogurt powder. The k  
373 values were lower ( $P < 0.05$ ) for the spray-dried powders 2 and 3 than in the spray-dried  
374 powder 1 sample. Ronkart et al. (2006) and Verruck et al. (2018) reported the same  
375 behavior, they found lower k values for samples that contained prebiotics (higher molar  
376 mass).

377

### 378 **3.3. Physical characterization of probiotic powders**

379

#### 380 *3.3.1. Morphology and particle size*

381

382 Fig. 2 shows the SEM micrographs of the *Bifidobacterium* BB-12 microspheres  
383 produced with different wall materials. Micrographs revealed distinct shapes and sizes  
384 for each spray-dried powder; however, in all of them, it is evident that *Bifidobacterium*  
385 BB-12 cells were retained therein because it was possible to note the absence of cells on  
386 the outside of their surfaces. The particles produced with lactose-free milk (Fig. 2-a)  
387 showed concavities typical of materials produced by spray drying. Gul (2017) reported  
388 that the formation of concavities in the surface of atomized particles can be attributed to  
389 the shrinkage of the particles during the drying process because of the rapid evaporation  
390 of the liquid drops. Similar morphological shapes of capsules made with reconstituted  
391 skim milk were reported by Maciel, Chaves, Grosso, and Gigante (2014). The spray-  
392 dried powder 2, produced with lactose-free milk powder and inulin, showed a rough and  
393 uneven surface (Fig. 2-b), however, free of fissures or disruptions, which is fundamental  
394 for guaranteeing higher protection and lower permeability of gases (Fritzen-Freire et al.,

395 2012). Microspheres produced with oligofructose and lactose-free milk (Fig. 2-c) were  
396 spherical, with more aggregation than spray-dried powders 1 and 2. This aggregation of  
397 particles is due to stickiness caused by the low glass transition temperature of  
398 oligofructose (Adhikari et al., 2009). The same behavior was observed with the  
399 microspheres produced by Rajam and Anandharamakrishnan (2015), who  
400 microencapsulated *Lactobacillus plantarum* with fructooligosaccharide as wall material.

401 Knowledge of the bulk density is important during the processing, storage, and  
402 packaging of encapsulated microparticles. The parameters such as moisture content,  
403 particle size distribution, and morphology can affect the bulk density of spray-dried  
404 powders (Rajam & Anandharamakrishnan, 2015). In our previous work (Dantas,  
405 Verruck, De Liz, Hernandez, & Prudencio, 2021), we measured the loose bulk density  
406 of the powders. It was possible to verify that the spray-dried powder 3 showed a  
407 significant variation ( $P < 0.05$ ) of this property ( $0.44 \text{ g cm}^{-3}$  against  $0.32 \text{ g cm}^{-3}$  for  
408 both spray-dried powders 1 and 2). These results reinforce our considerations about  
409 micrographs, and we associate them with particle aggregation and less interspace  
410 between particles of the spray-dried powder 3.

411 The size is an important property for the microparticle because of its strong  
412 influence on product solubility, appearance, and acceptability (Parthasarathi &  
413 Anandharamakrishnan, 2016). In the present study, the probiotic spray-dried powders  
414 microparticles exhibited a wide range of average diameters:  $10.62 \pm 4.94$ ,  $19.60 \pm 7.52$ ,  
415  $55.66 \pm 21.69 \mu\text{m}$ , for spray-dried powder 1, 2, and 3 respectively. This microparticle  
416 size is favorable for the possible incorporation of the powders in various matrices  
417 without significantly affecting the texture. According to Turchiuli, Gianfrancesco,  
418 Palzer, and Dumoulin (2011), stable solid bridges between particles can be created with  
419 the drying, leading to the formation of a bigger structure that is clustered, as observed

420 by SEM images (Fig. 2-b,c). The presence of clusters in the spray-dried powder 2 and 3  
421 corroborate with results obtained for the average size of the microparticles. The cluster  
422 structures visualized in the present study could be formed by several particles bound  
423 together. Carmo et al. (2018) discussed that the difference between the particle sizes is  
424 characterized by droplet coalescence, which in turn is influenced by the carrier agent  
425 used. According to Berdnaska and Janiszewska-Turak (2020), the use of carriers' agents  
426 or their mixtures in different proportions can result in powders with different physical  
427 properties. In the present study, no changes were made in the spray drying processes;  
428 therefore, encapsulation efficiency may have been influenced by the carrier agents.  
429 Ronkart et al. (2009) highlighted that in the spray drying process, two associated factors  
430 can generate the amorphous state of inulin and oligofructose and, therefore, both would  
431 be more susceptible to the clusters formation. These factors are the temperature (such as  
432 inlet temperature) and the water present in the droplets formed.

433

#### 434 3.3.2. X-Ray diffraction

435

436 The diffractograms of the samples (spray-dried powders, inulin, and  
437 oligofructose) are shown in Figure 3. This analysis can be utilized to characterize the  
438 type of order present in powders. X-ray amorphous materials lack long-range  
439 crystallographic order and produce a broad background pattern. The crystalline solids  
440 present long-range order and their diffractograms show a series of sharp peaks (Azároff,  
441 1968). The diffraction pattern obtained for the spray-dried powders which contain  
442 *Bifidobacterium BB-12* microspheres is predominantly related to amorphous material,  
443 since it shows dispersed bands, indicating that the molecules are disordered. De  
444 Medeiros, Thomazini, Urbano, Pinto Correia, and Favaro-Trindade (2014) also obtained

445 similar results, they studied spray drying dehydration of a probiotic yogurt produced  
446 with goat's milk and *Bifidobacterium animalis* subsp. *lactis* (BI-07). According to the  
447 same authors, the crystals could damage the cells, which would reduce the viability of  
448 microorganisms, making the amorphous structure interesting. Besides, amorphous  
449 solids are in general more soluble, and the crystallization may entail a negative impact  
450 on the handling properties (Campelo et al., 2017).

451 Campelo et al. (2017) used oligofructose (DP = 2–10) and inulin (DP= 2–60) as  
452 wall material to microencapsulate lime essential oil by spray drying. As with our results,  
453 they also found an amorphous type structure for these types of prebiotics, revealing that  
454 the spray drying process did not influence their structures. This is probably associated  
455 with the rapidity of the drying process, which prevents easy crystallization. Other  
456 studies have also reported amorphous characteristic for inulin with different  
457 polymerization degrees (Kalaivani & Suja, 2018; Silva & Meireles, 2015), for  
458 oligofructose (Alles, Tessaro, & Norena, 2013), and spray-dried skim milk powder  
459 (Yazdanpanah & Langrish, 2016).

460

### 461 3.3.3. Raman spectroscopic analysis

462

463 Raman spectra of spray-dried powders and prebiotics (oligofructose and inulin)  
464 are shown in Fig. 4, and the main vibrational bands are listed in Table 3 with their  
465 respective tentative assignments based on comparisons with previously reported data.  
466 The spray-dried powder 1 showed a spectrum with typical bands associated with  
467 proteins and carbohydrates (glucose). The band at  $1660\text{ cm}^{-1}$  was the contribution from  
468 the C=O stretching and N–H wagging modes of the group Amide I (C=O–NH<sub>2</sub>)

469 (Almeida, Oliveira, Stephani, & de Oliveira, 2011; Li-Chan, 1996). In the spray-dried  
470 powders 2 and 3, this band shifted by  $5\text{ cm}^{-1}$  and corresponds to the same vibrations.

471 A strong Raman band at  $1453\text{ cm}^{-1}$  was noted in spray-dried powder 1, and it is  
472 related to bending vibrations in the form scissoring of the group  $\text{CH}_2$ , which was mainly  
473 due to the carbohydrate mode (Almeida et al., 2011), principally glucose (Cerchiaro,  
474 Sant'Ana, Temperini, & da Costa Ferreira, 2005). Torres et al. (2017) also comment  
475 that the region between  $1500$  and  $1250\text{ cm}^{-1}$  corresponds to  $\text{CH}_2\text{OH}$  deformation  
476 modes. The same peak was observed in the spectra of the other spray-dried powders, as  
477 well as inulin and oligofructose, but with a small shift in its wavenumbers. In the  
478 prebiotics spectra, especially oligofructose, this band appeared with lower intensity  
479 because of the lower contribution of glucose in these samples.

480 The bands at  $1259$ ,  $1263$ , and  $1262\text{ cm}^{-1}$  in the spray-dried powders 1, 2, and 3,  
481 respectively, may be related to the contributions from the N–H bending and C–N  
482 stretching modes of the group Amide III (Li-Chan, 1996). As there are no proteins in  
483 oligofructose and inulin, these same bands ( $1263$  and  $1266\text{ cm}^{-1}$ , respectively) are  
484 assigned to the  $\text{CH}_2$  twisting mode of carbohydrates (Almeida et al., 2011; Rodrigues  
485 Junior et al., 2016).

486 The region between  $1121$  and  $1065\text{ cm}^{-1}$  is assigned to C–O and C–C stretching,  
487 and C–O–H bending (Rodrigues Junior et al., 2016). Note that inulin and oligofructose  
488 favored the appearance of these vibrations, since the peaks at  $1122$  and  $1123$  were  
489 observed in the spray-dried powders 2 and 3, respectively; in contrast, this same band  
490 was not observed in spray-dried powder 1. According to Almeida et al. (2011), these  
491 vibrational modes are characteristic of carbohydrates.

492 The spectra of spray-dried powders 2 and 3 showed two more features that were  
493 not observed in the spray-dried powder 1. The peak located at  $620\text{ cm}^{-1}$  corresponds to

494 the deformations of groups O–C–O and O–H, this result confirms the presence of  
495 prebiotics, since typical bands of inulin are in the spectral region between 833 and  
496  $599\text{ cm}^{-1}$  (Balan, Chis, Rachisan, & Baia, 2018). Similarly, the band at  $536\text{ cm}^{-1}$  was  
497 observed for spray-dried powder 2 and at  $542\text{ cm}^{-1}$  for spray-dried powder 3, indicating  
498 glucose ring deformations of the inulin. Spectra of inulin and oligofructose were very  
499 similar, which was already expected since these carbohydrates have the same structure,  
500 changing only the molar mass. For example, both spectra show a medium peak at  
501  $465\text{ cm}^{-1}$ , being attributed to O–H bending mode (Balan et al., 2018). According to  
502 Oroian, Ropciuc, and Paduret (2018), the band at  $607\text{ cm}^{-1}$  presents in the inulin  
503 spectrum is assigned to the presence of fructose.

504

#### 505 *3.3.4. Thermal properties*

506

507 Figure 5 shows the thermogravimetric (TGA) and derivative thermogravimetry  
508 (DrTGA) curves obtained from spray-dried powders. The first weight loss (3.1%,  
509 2.34%, and 2.6% for spray-dried powder 1, 2, and 3, respectively) occurred between  
510  $25\text{ }^{\circ}\text{C}$  and  $131\text{ }^{\circ}\text{C}$  and it corresponds to the removal of moisture of the samples. Above  
511 this temperature range, the decomposition process occurred in one or two stages,  
512 according to each sample. Spray-dried powder 1 showed two stages of decomposition:  
513 the first between  $131\text{ }^{\circ}\text{C}$  and  $233\text{ }^{\circ}\text{C}$  (mass loss of 24.84%), which is related to the  
514 degradation and/or caramelization of the glucose (Saavedra-Leos et al., 2012); and the  
515 second stage in the range of  $233\text{ }^{\circ}\text{C}$  to  $300\text{ }^{\circ}\text{C}$  (mass loss of 26.45%) associated with the  
516 whey protein degradation and caseins denaturation (Barreto, Pires, & Soldi, 2003).

517

518 For both spray-dried powders 2 and 3, the decomposition process occurred in  
only step (temperature range between  $131$  and  $300\text{ }^{\circ}\text{C}$ ). However, the  $\text{DrTGA}_{\text{peak}}$

519 temperature was higher for spray-dried powder 2 than for spray-dried powder 3 (209.26  
520 and 199.86 °C, respectively), indicating greater stability for inulin-based microspheres.  
521 This behavior was already expected since inulin has a higher degree of polymerization  
522 umthan oligofructose and, therefore, tends to be more thermally stable (Verruck et al.,  
523 2017). Similar results were also observed by Verruck et al. (2018) and de Liz et al.  
524 (2020), who microencapsulated *Bifidobacterium* BB-12 in full-fat goat's milk,  
525 cryoconcentrated whey, and prebiotics (inulin and oligofructose). These DTG<sub>peak</sub>  
526 temperatures may correspond to the breakdown of the fructose chains of the prebiotics  
527 (Fritzen-Freire et al., 2012).

528         When investigating the DSC curve of the wall material Skim Lactose-free Milk  
529 (Fig. 6-a), a change in baseline between ~80 and 150 °C indicated us an endothermic  
530 event. For this event, the peak mid-temperature was found at 120 °C. Szulc, Nazarko,  
531 Ostrowska-Ligęza, and Lenart (2016) found peaks around 100 °C for dairy powders,  
532 and attributed them to the caseins denaturation. Likewise, De Liz et al. (2020) observed  
533 endothermic peaks around 110 °C for cryoconcentrated whey samples, which were  
534 related to the denaturation of its proteins. O'Mahony, Drapala, Mulcahy, and Mulvihill  
535 (2017) reported that at temperatures above 115 °C, protein denaturation peaks could not  
536 be distinguished, which was credited to the Maillard reaction induced during the  
537 analysis. However, for all spray-dried powders resulting from this sample (Fig. 6-b),  
538 there was a well-defined endothermic event, also associated with both non-enzymatic  
539 browning (advanced Maillard reaction) (Vuataz, Meunier, & Andrieux, 2010) and  
540 denaturation of whey proteins (Zhou & Labuza, 2011).

541         Zhou and Labuza (2011) mentioned that at 53 °C the proteins are barely  
542 impacted by the temperature; however, the DNA of the microorganism present in the  
543 milk powder matrix can be potently affected leading to damage and cell inactivation.



544 The same authors also commented that the denaturation temperature of whey protein  
545 isolate and the  $\beta$ -lactoglobulin (one of the major components of whey proteins) has a  
546 strong dependence on the water content of the sample: it decreases with increasing  
547 water content. This relation is best visualized when comparing the moisture (dry basis)  
548 of the powders on the day of their manufacture with the endothermic peaks: moisture  
549 values ( $\text{g } 100 \text{ g}^{-1}$ ) of 7.67, 4.45, and 4.54, and peak temperatures at 165.02 °C  
550 ( $\Delta H = -166.94 \text{ J g}^{-1}$ ), 200.93 °C ( $\Delta H = -160.37 \text{ J g}^{-1}$ ), and 193.70 °C ( $\Delta H = -111.06$   
551  $\text{J g}^{-1}$ ) for spray-dried powders 1, 2 and 3, respectively. Furthermore, this increase of the  
552 peaks in the spray-dried powders 2 and 3 is related to the increase of the thermal  
553 stability due to the addition of the prebiotics (Pinto et al., 2015). Pilatti-Riccio et al.  
554 (2019) noted that particles prepared with oligofructose had fewer thermal events in their  
555 DSC curves in comparison to the events observed when only the core material was  
556 investigated. According to them, this thermal behavior suggests the protection and  
557 interaction of the wall material with the core extract, demonstrating that this matrix has  
558 potential for application as wall material in the food industry.

559 As can be seen in Fig. 6-a, the  $T_{\text{peaks}}$  found for inulin and oligofructose are  
560 225.15 and 211.27 °C, and enthalpy changes  $-83.92$  and  $-46.84 \text{ J g}^{-1}$ , respectively.  
561 These peaks can be attributed to the inulin thermal degradation (Dan, Ghosh, & Moulik,  
562 2009; Ronkart, Deroanne, Paquot, Fougny, & Blecker, 2010; Leone, Colman,  
563 Schnitzler, Ellendersen, & Masson, 2014), as well as caramelization and decomposition  
564 of the oligofructose (Bersaneti, Mantovan, Magri, Mali, & Celligoi, 2016). Pilatti-  
565 Riccio et al. (2019) also observed an endothermic peak at 201.6 °C for commercial  
566 oligofructose.

567 Based on these results, it can be stated that the microencapsulation process  
568 using inulin or oligofructose conferred greater stability to spray-dried powders.

569 Moreover, it has been found that, during the spray drying process at the air inlet  
570 temperature of 150 °C, the materials employed in the production of the microspheres  
571 did not suffer any significant degradation.

572

#### 573 **4. Conclusion**

574

575 Bifidobacteria was efficiently entrapped in lactose free milk, and lactose free  
576 milk and prebiotics. Peleg model provided fair values of the initial mass transfer rate  
577 and water adsorption capacity. The isotherm found for all samples was a Type III  
578 Isotherm, it is related to the presence of amorphous sugars, as observed in the powders  
579 diffractograms. The GAB model fitted well to the experimental data, and indicated that  
580 relative humidity conditions above 33% and 43% were not efficient to maintain the  
581 storage stability of the spray-dried powders 1 and 2, and spray-dried powder 3,  
582 respectively. The Raman spectrum confirmed the incorporation of the prebiotics in the  
583 resultant spray-dried powders (that is, after microencapsulation process), ensuring their  
584 availability to the consumer. Besides, the addition of these carbohydrates conferred  
585 greater thermal stability to spray-dried powders, especially the inulin. On this approach,  
586 we concluded that a good quality of lactose-free milk based probiotic powder could be  
587 obtained using spray drying technique, with potential application in the food industry.

588

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598

#### 599 **Declaration of competing interest**

600 The authors declare that they have no conflict of interest.

601

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603

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**Table 1**

Peleg model coefficients and fit parameters.  $1/k1 = \text{g water. (g dry solid. h)}^{-1}$ ;  $1/k2 = \text{g water. (g dry solid)}^{-1}$ .

| Samples              | % RH | 1/k1                           | 1/k2                           | R <sup>2</sup>                 | SSE                     |
|----------------------|------|--------------------------------|--------------------------------|--------------------------------|-------------------------|
| Spray-dried powder 1 | 11   | 0.0186 ± 0.0057 <sup>bA</sup>  | 0.0266 ± 0.0007 <sup>fA</sup>  | 0.9676 ± 0.0061 <sup>cB</sup>  | 4.02 × 10 <sup>-5</sup> |
|                      | 33   | 0.0451 ± 0.0074 <sup>aA</sup>  | 0.0741 ± 0.0018 <sup>eAB</sup> | 0.9840 ± 0.0041 <sup>bB</sup>  | 1.46 × 10 <sup>-4</sup> |
|                      | 43   | 0.0408 ± 0.0042 <sup>abA</sup> | 0.0952 ± 0.0010 <sup>eA</sup>  | 0.9917 ± 0.0020 <sup>abA</sup> | 1.69 × 10 <sup>-4</sup> |
|                      | 58   | 0.0556 ± 0.0039 <sup>aA</sup>  | 0.1487 ± 0.0018 <sup>dA</sup>  | 0.9934 ± 0.0003 <sup>abA</sup> | 3.49 × 10 <sup>-4</sup> |
|                      | 75   | 0.0478 ± 0.0031 <sup>aA</sup>  | 0.2787 ± 0.0074 <sup>cA</sup>  | 0.9975 ± 0.0005 <sup>aA</sup>  | 4.29 × 10 <sup>-4</sup> |
|                      | 80   | 0.0583 ± 0.0089 <sup>aA</sup>  | 0.3802 ± 0.0206 <sup>bA</sup>  | 0.9965 ± 0.0008 <sup>aA</sup>  | 1.78 × 10 <sup>-3</sup> |
|                      | 90   | 0.0427 ± 0.0064 <sup>aA</sup>  | 0.6936 ± 0.0106 <sup>aA</sup>  | 0.9920 ± 0.0014 <sup>abA</sup> | 1.46 × 10 <sup>-2</sup> |
| Spray-dried powder 2 | 11   | 0.0144 ± 0.0005 <sup>bA</sup>  | 0.0262 ± 0.0019 <sup>gA</sup>  | 0.9892 ± 0.0019 <sup>aA</sup>  | 1.18 × 10 <sup>-5</sup> |
|                      | 33   | 0.0356 ± 0.0091 <sup>abA</sup> | 0.0674 ± 0.0025 <sup>fB</sup>  | 0.9927 ± 0.0025 <sup>aAB</sup> | 5.22 × 10 <sup>-5</sup> |
|                      | 43   | 0.0359 ± 0.0061 <sup>abA</sup> | 0.0921 ± 0.0003 <sup>eA</sup>  | 0.9895 ± 0.0033 <sup>aA</sup>  | 2.03 × 10 <sup>-4</sup> |
|                      | 58   | 0.0348 ± 0.0022 <sup>abB</sup> | 0.1431 ± 0.0002 <sup>dA</sup>  | 0.9954 ± 0.0003 <sup>aA</sup>  | 2.27 × 10 <sup>-4</sup> |
|                      | 75   | 0.0524 ± 0.0071 <sup>aA</sup>  | 0.2390 ± 0.0019 <sup>cB</sup>  | 0.9960 ± 0.0029 <sup>aA</sup>  | 5.38 × 10 <sup>-4</sup> |
|                      | 80   | 0.0500 ± 0.0057 <sup>aA</sup>  | 0.2850 ± 0.0012 <sup>bB</sup>  | 0.9964 ± 0.0002 <sup>aA</sup>  | 1.06 × 10 <sup>-3</sup> |
|                      | 90   | 0.0403 ± 0.0023 <sup>aA</sup>  | 0.4860 ± 0.0074 <sup>aC</sup>  | 0.9933 ± 0.0020 <sup>aA</sup>  | 5.93 × 10 <sup>-3</sup> |
| Spray-dried powder 3 | 11   | 0.0100 ± 0.0001 <sup>cA</sup>  | 0.0241 ± 0.0004 <sup>fA</sup>  | 0.9877 ± 0.0034 <sup>aA</sup>  | 1.09 × 10 <sup>-5</sup> |

|    |                           |                          |                          |                       |
|----|---------------------------|--------------------------|--------------------------|-----------------------|
| 33 | $0.0182 \pm 0.0024^{bcA}$ | $0.0766 \pm 0.0003^{eA}$ | $0.9981 \pm 0.0008^{aA}$ | $1.46 \times 10^{-5}$ |
| 43 | $0.0279 \pm 0.0005^{abA}$ | $0.0963 \pm 0.0024^{eA}$ | $0.9910 \pm 0.0012^{aA}$ | $1.92 \times 10^{-4}$ |
| 58 | $0.0315 \pm 0.0045^{abB}$ | $0.1543 \pm 0.0094^{dA}$ | $0.9908 \pm 0.0075^{aA}$ | $5.42 \times 10^{-4}$ |
| 75 | $0.0387 \pm 0.0030^{aA}$  | $0.2767 \pm 0.0022^{cA}$ | $0.9983 \pm 0.0004^{aA}$ | $2.75 \times 10^{-4}$ |
| 80 | $0.0336 \pm 0.0054^{aA}$  | $0.3497 \pm 0.0032^{bA}$ | $0.9983 \pm 0.0010^{aA}$ | $7.56 \times 10^{-4}$ |
| 90 | $0.0306 \pm 0.0056^{abA}$ | $0.5706 \pm 0.0088^{aB}$ | $0.9954 \pm 0.0004^{aA}$ | $5.57 \times 10^{-3}$ |

<sup>a-g</sup> Means  $\pm$  standard deviation with different superscript lowercase letters in the same column indicate significant differences ( $P < 0.05$ ) among the different relative humidity (RH) for each sample. <sup>A-C</sup>Means  $\pm$  standard deviation with different superscript uppercase letters in the same column indicate significant differences ( $P < 0.05$ ) among the samples on the same relative humidity (RH). Means found in triplicate.

**Table 2**GAB model coefficients and fit parameters.  $M_0 = \text{g water. (g dry matter)}^{-1}$ .

|       | Spray-dried powder 1          | Spray-dried powder 2         | Spray-dried powder 3         |
|-------|-------------------------------|------------------------------|------------------------------|
| $M_0$ | $0.084 \pm 0.005^{\text{ab}}$ | $0.073 \pm 0.004^{\text{b}}$ | $0.092 \pm 0.001^{\text{a}}$ |
| C     | $2.573 \pm 0.583^{\text{a}}$  | $3.786 \pm 0.775^{\text{a}}$ | $1.994 \pm 0.018^{\text{a}}$ |
| k     | $0.977 \pm 0.005^{\text{a}}$  | $0.944 \pm 0.008^{\text{b}}$ | $0.935 \pm 0.005^{\text{b}}$ |
| $R^2$ | $0.998 \pm 0.002^{\text{a}}$  | $0.999 \pm 0.001^{\text{a}}$ | $0.998 \pm 0.001^{\text{a}}$ |
| SSE   | 0.00143                       | 0.00016                      | 0.00072                      |

Means  $\pm$  standard deviation with different superscript lowercase letters in the same line indicate significant differences ( $P < 0.05$ ) between samples. Means found in triplicate.

**Table 3**Main Raman wavenumbers, in  $\text{cm}^{-1}$ , and their respective tentative assignments.

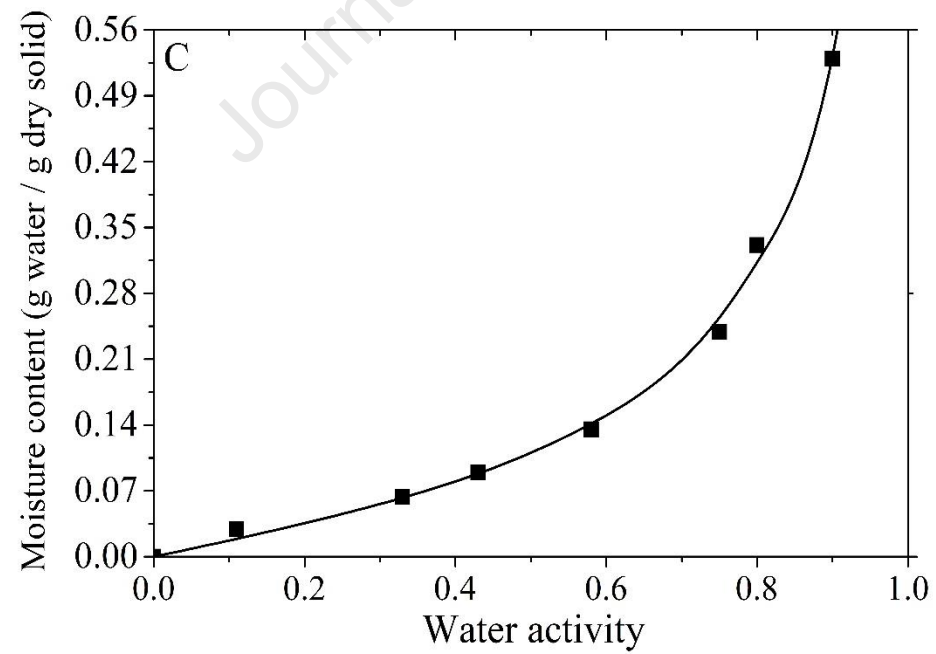
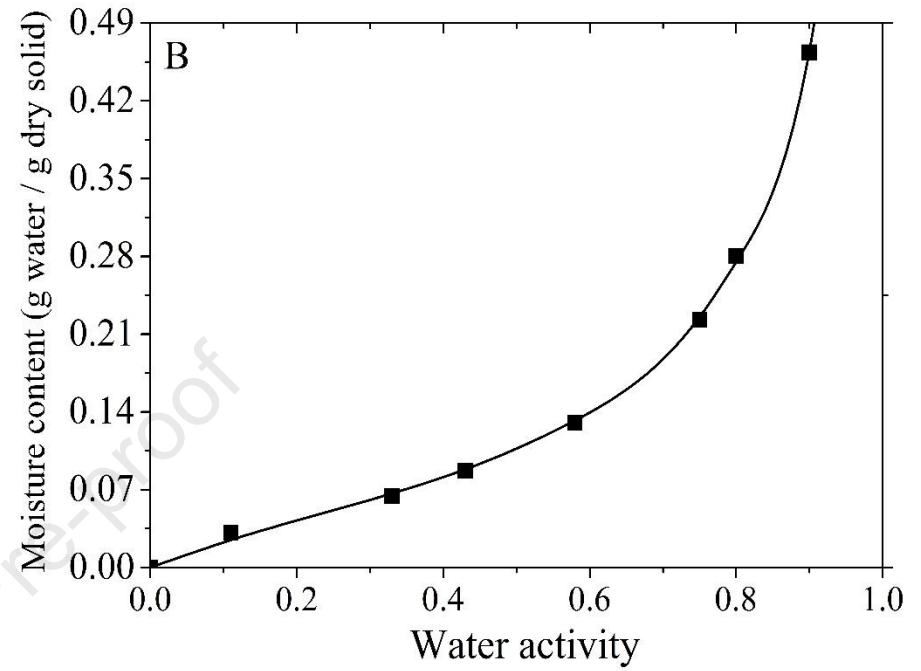
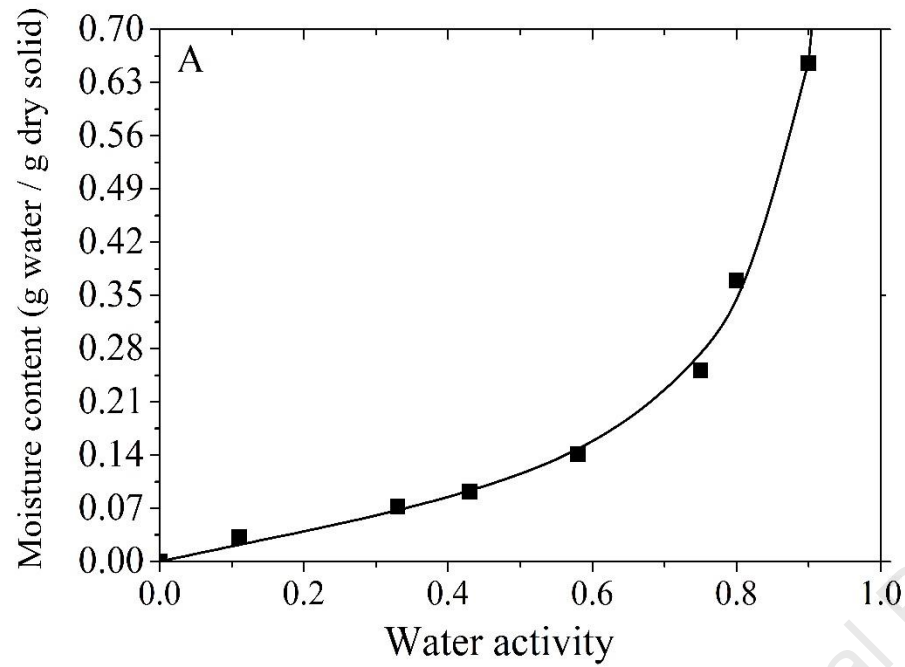
| Sample               | Raman shift ( $\text{cm}^{-1}$ ) | Assignment  | Reference                                      |
|----------------------|----------------------------------|---|--|
| Spray-dried powder 1 | 1259.15                          | $\delta$ (N–H) Amide III; $\nu$ (C–N) Amide III;<br>and/or $\gamma$ ( $\text{CH}_2$ ) <sub>twisting</sub> | (Li-Chan, 1996; Rodrigues Junior et al., 2016) |
|                      | 1352.03                          | Glucose   | (Torres et al., 2017)                          |
|                      | 1453.83                          | $\delta$ ( $\text{CH}_2$ ) <sub>scissoring</sub>  | (McGoverin, Clark, Holroyd, & Gordon, 2010)    |
|                      | 1660.4 m                         | $\nu$ (C=O) Amide I; $\gamma$ (N–H) <sub>wagging</sub> Amide I  | (Almeida et al., 2011; Li-Chan, 1996)          |
| Spray-dried powder 2 | 536.127 vs                       | glucose ring def  | (Balan et al., 2018)                           |
|                      | 620.835 s                        | def (O–C–O); def (O–H)  | (Balan et al., 2018)                           |
|                      | 1122.97 m                        | $\nu$ (C–O); $\nu$ (C–C); $\delta$ (C–O–H)  | (Rodrigues Junior et al., 2016)                |
|                      | 1263.39 m                        | $\delta$ (N–H) Amide III; $\nu$ (C–N) Amide III;<br>and/or $\gamma$ ( $\text{CH}_2$ ) <sub>twisting</sub> | (Li-Chan, 1996; Rodrigues Junior et al., 2016) |
|                      | 1665.1                           | $\nu$ (C=O) Amide I; $\gamma$ (N–H) <sub>wagging</sub> Amide I  | (Almeida et al., 2011; Li-Chan, 1996)          |
| Spray-dried powder 3 | 621.938 s                        | def (O–C–O); def (O–H)  | (Balan et al., 2018)                           |
|                      | 1064.11 m                        | $\nu$ (C–O); $\nu$ (C–C); $\delta$ (C–O–H)  | (Rodrigues Junior et al., 2016)                |
|                      | 1123.69 m                        | $\nu$ (C–O); $\nu$ (C–C); $\delta$ (C–O–H)  | (Rodrigues Junior et al., 2016)                |

|               |            |  |  |
|---------------|------------|--|--|
|               | 1262.77 m  | $\delta$ (N–H) Amide III; $\nu$ (C–N) Amide III;<br>and/or $\gamma$ (CH <sub>2</sub> ) <sub>twisting</sub> | (Li-Chan, 1996; Rodrigues Junior et al., 2016) |
|               | 1665.8     | $\nu$ (C=O) Amide I; $\gamma$ (N–H) <sub>wagging</sub> Amide I   | (Almeida et al., 2011; Li-Chan, 1996)          |
| Oligofructose | 465.421    | $\delta$ (O–H)   | (Balan et al., 2018)                           |
|               | 531.073 vs | glucose ring def   | (Balan et al., 2018)                           |
|               | 616.226 s  | def (O–C–O); def (O–H)   | (Balan et al., 2018)                           |
|               | 674.193 m  | def (O–C–C); def (O–H); def (C–H)  | (Balan et al., 2018)                           |
|               | 823.398 s  | $\delta$ (O–H); def (C–H)  | (Balan et al., 2018)                           |
|               | 1458.65    | $\delta$ (CH <sub>2</sub> ) <sub>scissoring</sub>  | (McGoverin et al., 2010)                       |
| Inulin        | 464.955    | $\delta$ (O–H)   | (Balan et al., 2018)                           |
|               | 532.485 vs | glucose ring def   | (Balan et al., 2018)                           |
|               | 607.886    | Fructose   | (Oroian et al., 2018)                          |
|               | 663.164 m  | def (O–C–C); def (O–H); def (C–H)  | (Balan et al., 2018)                           |
|               | 707.939 w  | def (O–H)  | (Balan et al., 2018)                           |
|               | 816.277 vs | def (C–C–O); def (O–C–C); $\delta$ (C–H)   | (Balan et al., 2018)                           |
|               | 830.212 s  | $\delta$ (O–H); def (C–H)  | (Balan et al., 2018)                           |
|               | 1461.17    | $\delta$ (CH <sub>2</sub> ) <sub>scissoring</sub>  | (McGoverin et al., 2010)                       |

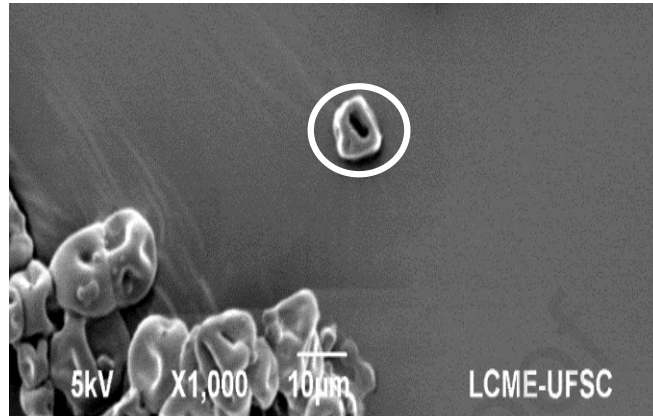
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Vs – very strong; s – strong; m – medium; w – weak.

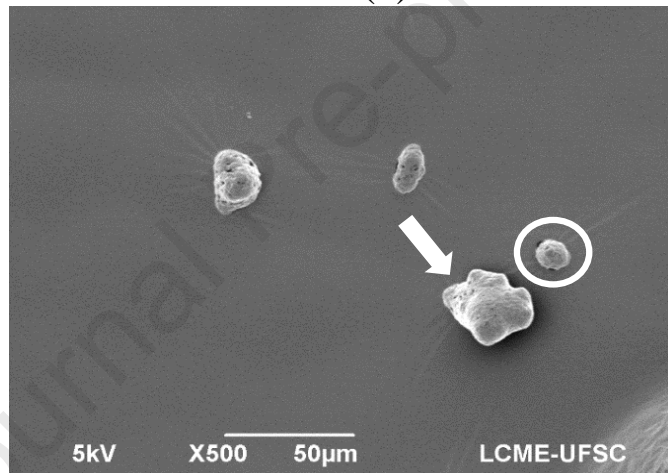
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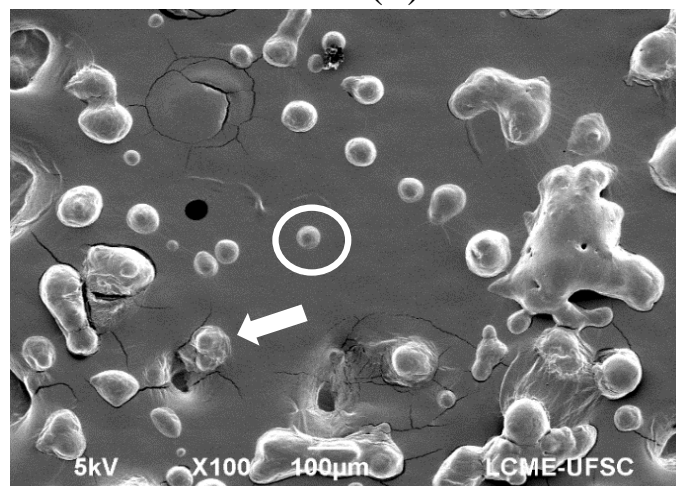




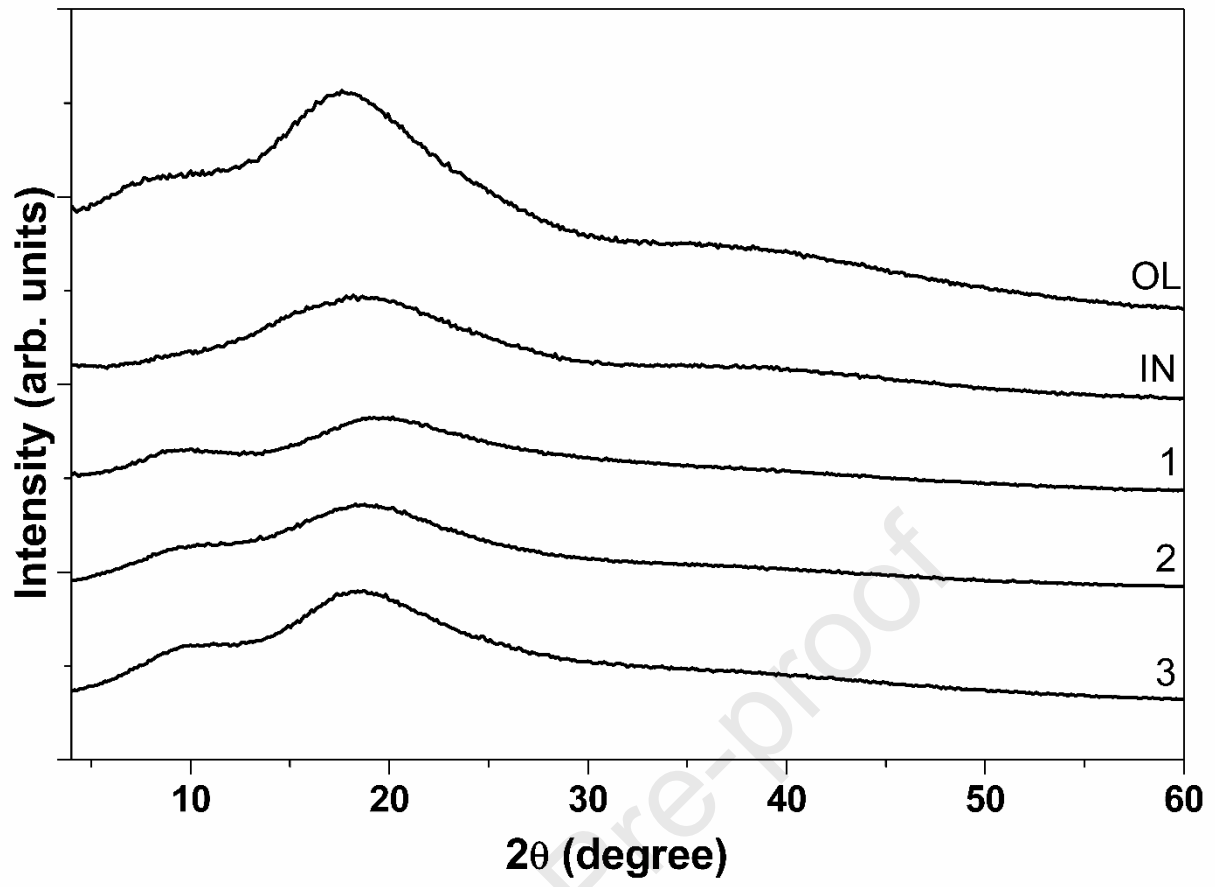
(a)

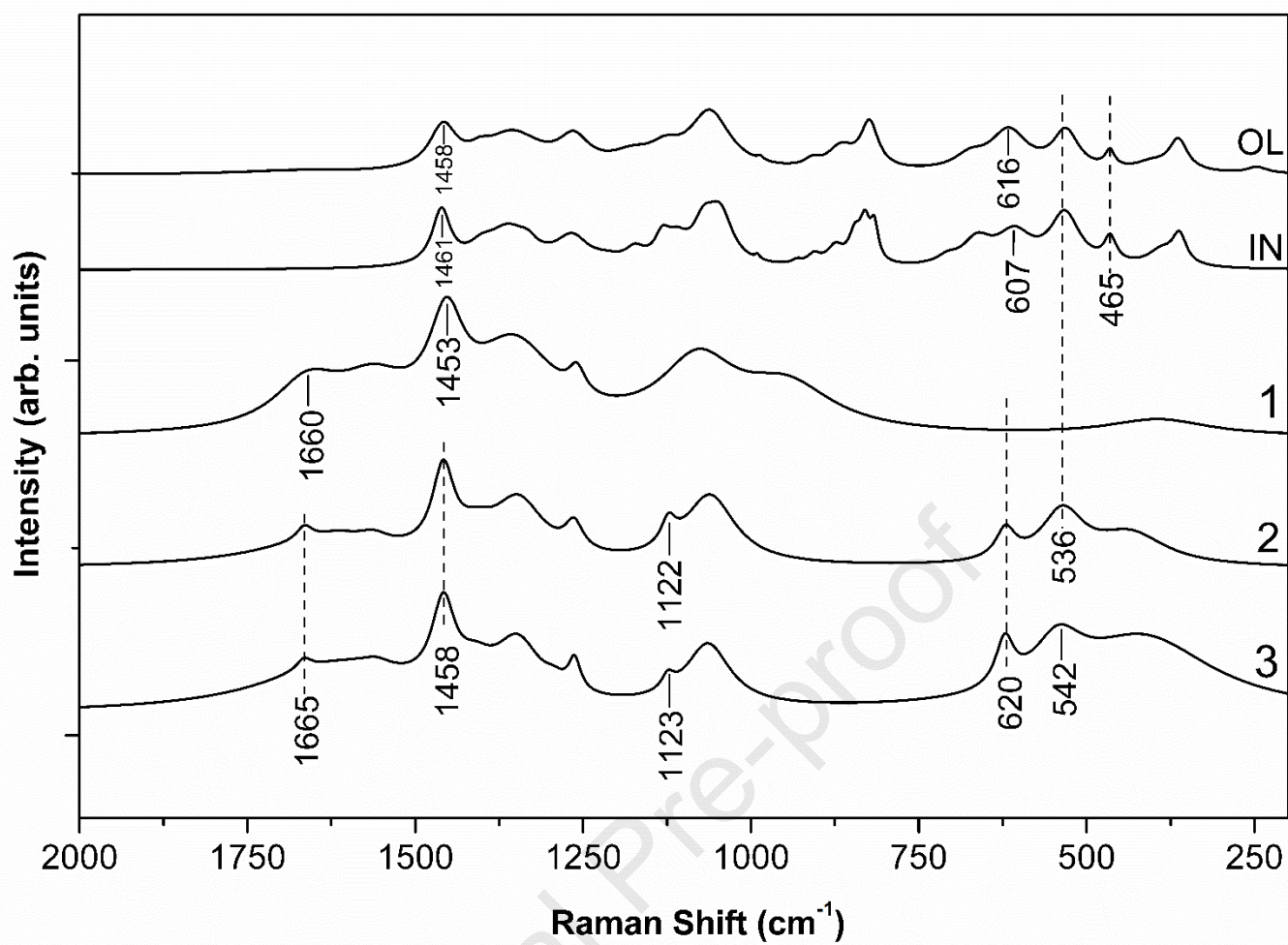


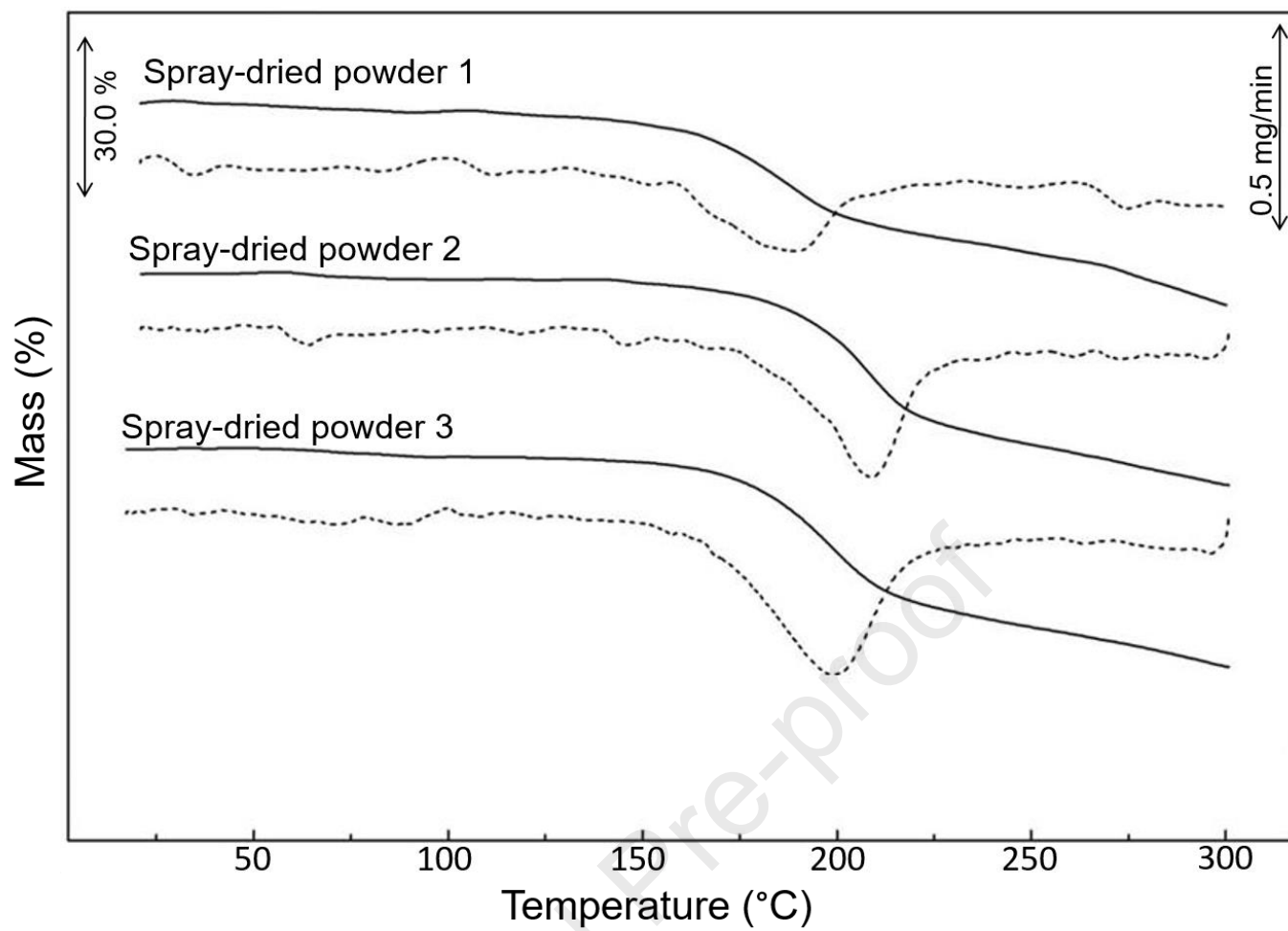
(b)

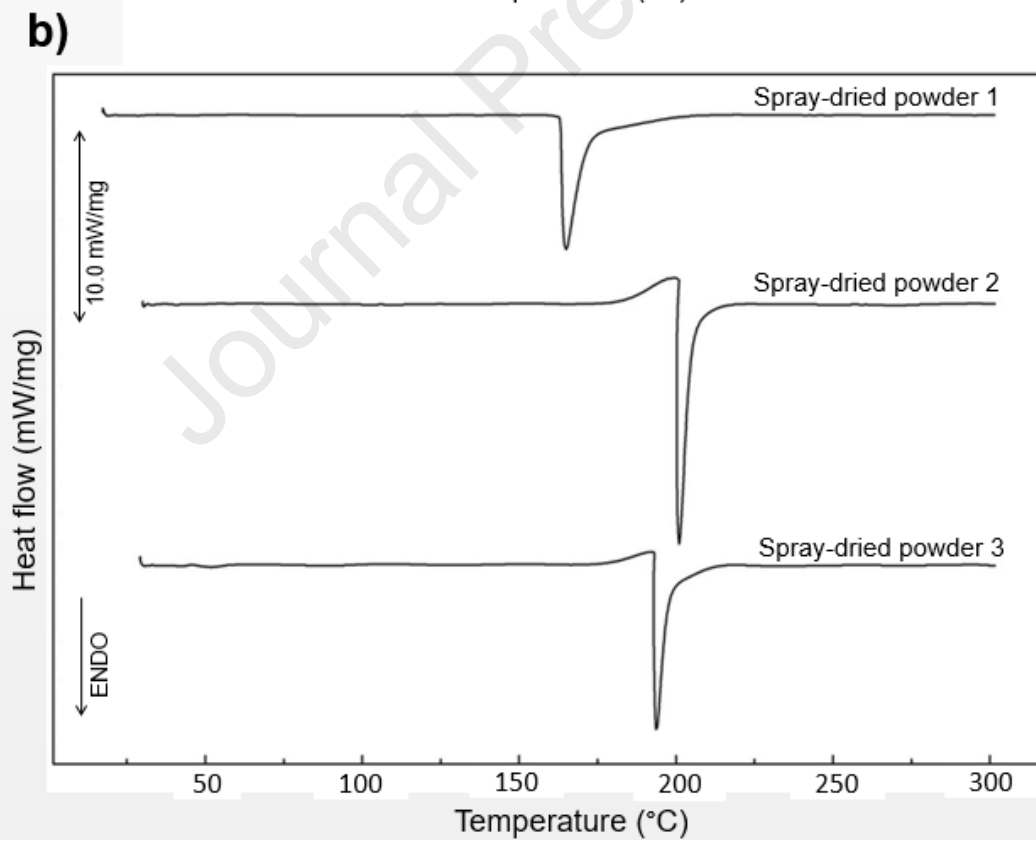
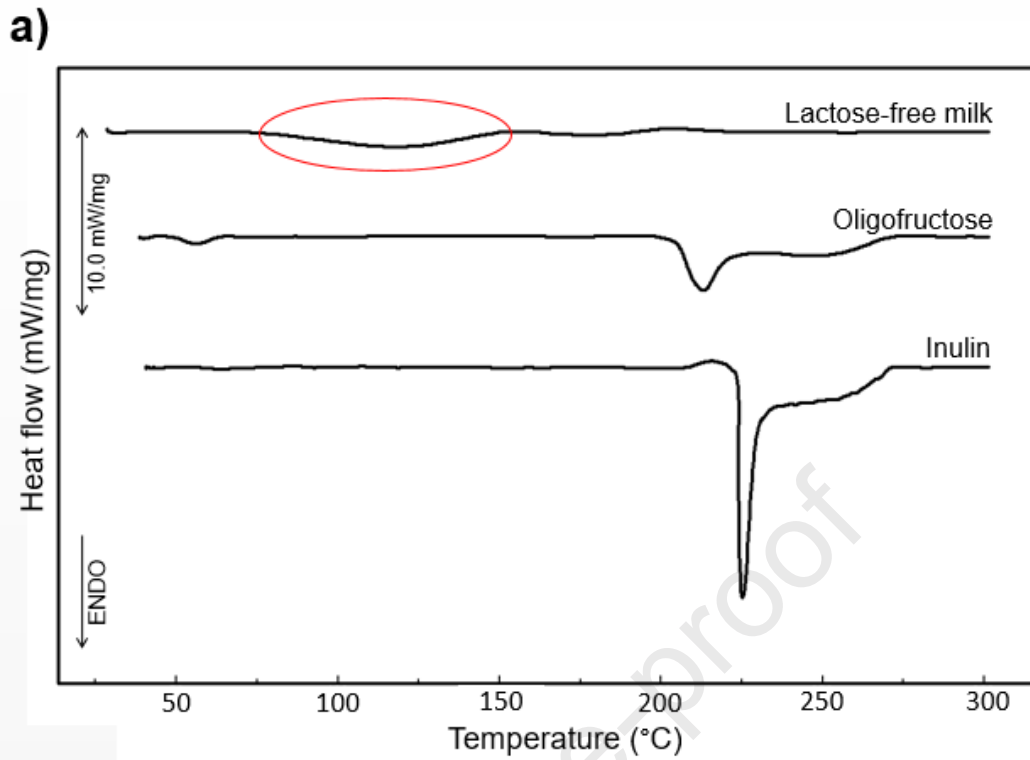


(c)









- Probiotic stability was found for the microspheres with lactose-free milk.
- Probiotic stability was found for the microspheres with prebiotics.
- The amorphous sugars were responsible to obtain a Type III isotherm.
- RH > 33 and 43% were not able to maintain the spray-dried powders stability.
- The inulin conferred greater thermal stability to spray-dried powder.

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Rakesh K. Singh, Ph.D.

Editor-in-Chief of *LWT – Food Science and Technology*

Dear Editor,

The authors declare that they have no conflict of interest.

Best regards,

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