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## A catalytic approach *via* retro-aldol condensation of glucose to furanic compounds†

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The synthesis of new types of furan-based compounds other than 5-hydroxymethylfurfural from glucose is a very attractive yet underexploited strategy. We report here a catalytic conversion of glucose with acetylacetone (acac) to furan-centered chemicals, 2-methyl-3-acetylfuran (MAF) and 1-(5-(1,2-dihydroxyethyl)-2-methylfuran-3-yl)ethan-1-one (DMAF), which are potential building blocks for the synthesis of fine chemicals. The experimentally supported reaction mechanism is cascade-type, including glycolaldehyde (GA) formation by H<sub>2</sub>MoO<sub>4</sub>-catalysed retro-aldol condensation (C2 + C4) of glucose and immediate capture of transient C2 and C4 intermediates by acac to yield MAF and DMAF. To the best of our knowledge, this is the first report on the straightforward synthesis of MAF and DMAF from glucose, providing a new but generic synthesis strategy for GA-based C2 and erythrose-based C4 chemistry in biorefining.

remarkable small molecule with both aldehyde and alcohol functionalities and has high potential to be a renewable alternative for petroleum-based ethylene oxide.<sup>3</sup> GA is prone to many side reactions due to its highly reactive nature; thus, it is often sequentially stabilized after formation, such as by hydrogenation to ethylene glycol.<sup>4</sup> Other synthesis methods have also been developed for the transformation of GA, mainly including oxidation, aldol reaction, amination, *etc.*, for the production of glycolic acid,  $\alpha$ -hydroxy acid esters and amines, as summarized recently by Faveere *et al.*<sup>3–5</sup> Nevertheless, new transformations that create platform chemicals or building blocks for fine chemicals are greatly needed to boost contemporary biorefinery concepts toward a sustainable world.

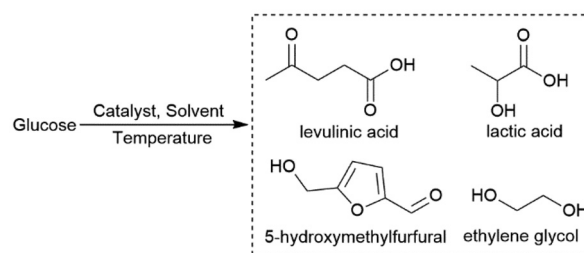
In this study, acetylacetone (acac), a typical  $\beta$ -dicarbonyl compound, was employed to capture the *in situ* formed, reactive GA. The rapid interconversion between keto and enol tautomers of acac makes it a good nucleophilic reagent to attack

## Introduction

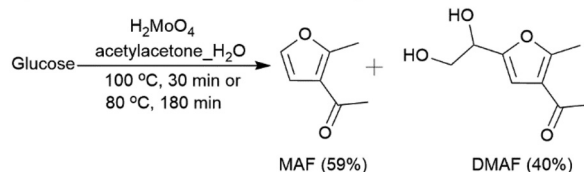
The high dependence of modern society on fossil fuel-based resources, together with the associated adverse environmental impacts, motivates research to identify renewable raw materials and develop new production methods for fuels and chemicals.<sup>1</sup> Glucose has attracted global attention as a representative monosaccharide of non-edible cellulose. Numerous studies have been devoted to converting glucose into valuable platform chemicals, such as levulinic acid, 5-hydroxymethylfurfural (5-HMF), lactic acid, sugar alcohols and ethylene glycol (Fig. 1), through isomerization, dehydration, hydrogenation and retro-aldol condensation (RAC).<sup>2</sup>

RAC of glucose through a C2 + C4 pathway generates glycolaldehyde (GA) and erythrose (Scheme 1, step 1). GA is a

### a) General valuable platform chemicals from glucose



### b) This work on MAF and DMAF synthesis



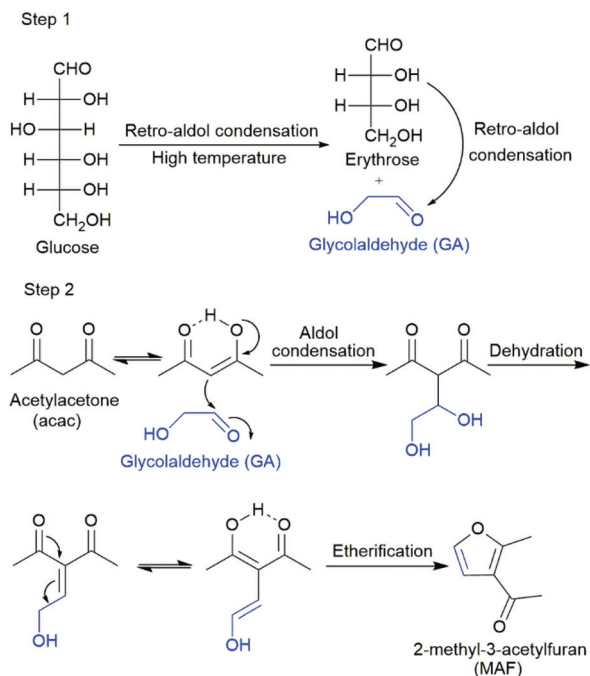
**Fig. 1** (a) General platform chemicals derived from glucose and (b) summary of this work: furanic compounds *via* RAC from glucose.

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**Scheme 1** Proposed reaction pathway for the cascade conversion of glucose to MAF via GA.

aldehyde groups.<sup>6</sup> As shown here, high-temperature treatment (220 °C) of aqueous glucose solution in the presence of acac gives a highly intriguing furan-derived product 2-methyl-3-acetylfuran (MAF) (Table 1, entry 1). Addition of  $\text{H}_2\text{MoO}_4$  as a catalyst improves the efficiency of the reaction and enables glucose transformation to MAF under significantly milder conditions. In addition, the catalytic process opens simultaneously a unique possibility to synthesize 1-(5-(1,2-dihydroxyethyl)-2-methylfuran-3-yl)ethan-1-one (DMAF), which is derived from the reaction between erythrose (C4 fragment) and acac (Fig. 1). It is noteworthy that MAF and DMAF were previously only

accessible by multi-step chemical synthesis<sup>7</sup> or using isolated and expensive GA and erythrose as starting materials in a  $\text{ZrCl}_4$ -catalysed reaction with acac.<sup>8</sup> From the furan-derived products, MAF is considered a useful intermediate for the synthesis of photochromic molecules,<sup>9</sup> pharmaceuticals,<sup>10</sup> seco-prostacyclins and food additives,<sup>11</sup> while DMAF is seen as an underexploited chemical with potential for application in the pharmaceutical and fine chemical industries.<sup>8,12</sup>

## Results and discussion

### Investigation on MAF formation

To open the RAC pathway for glucose conversion in the presence of acac, we chose high-temperature reaction conditions (220 °C). It was confirmed to be an essential reaction parameter for the high yield of MAF (Table S1 and Fig. S1–4†). The indispensable role of acac as a nucleophile in this transformation was further confirmed by a series of experiments.  $\text{H}_2\text{O}$ /acetone and  $\text{H}_2\text{O}$ /ethyl acetate reaction media were unsuccessful in this transformation and gave only insoluble humins, while all reactions involving acac gave MAF. From the studied combinations,  $\text{H}_2\text{O}$  with acac offered a satisfactory yield of 46% for this cascade-type reaction (Table 1, entries 1–5).

We also studied the role of GA as the key intermediate. Indeed, the use of pure GA as a starting material instead of glucose increases the MAF yield significantly to 83% under the same reaction conditions (Table 1, entry 6). The central role of GA in the MAF formation reaction is also consistent with the results obtained from a series of carbohydrate substrates. Mannose, as a C-2 epimer of glucose, gave a comparable yield of MAF to glucose, while xylose and fructose gave much lower yields (Table 1, entries 8–10). Xylose as an aldopentose only gave around 1/3 of MAF compared with the amount derived from glucose, in accordance with the C2 + C3 RAC of xylose. Fructose is prone to undergo C3 + C3 RAC (which produces glyceraldehyde and dihydroxyacetone) rather than the desired C2 + C4 pathway and thus gave only a small amount of MAF.<sup>13</sup> We confirmed this observation by a direct reaction between acac and glyceraldehyde at 220 °C, yielding only 4% of MAF and other unidentifiable products. Further studies revealed that acetic acid as a general carbohydrate decomposition product along with typical dehydration products with furan structures (such as furfural, 2-methylfuran and 5-HMF) is not involved in the MAF formation reaction (Table S2†). These results confirm the pivotal role of GA in the condensation reaction with acac and further the formation of the furan structure of MAF under the applied conditions.

The reaction pathway involves the cleavage of glucose through C2 + C4 RAC, followed by the aldol condensation of GA with acac (Scheme 1, steps 1 and 2). In this reaction, the presence of water is necessary for high yields in both steps (Table 1, entries 1 vs. 4, 6 vs. 11). It is known that water, besides being an efficient proton carrier, undergoes autoprotolysis. Therefore, the concentration of hydronium ( $\text{H}_3\text{O}^+$ ) and hydroxide ( $\text{OH}^-$ ) ions increases with increasing temperature

**Table 1** Effect of different reaction media and substrates on the yield of MAF without a catalyst

| Entry          | Solvent                                   | Substrate | MAF yield <sup>a</sup> (mol %) |
|----------------|---|-----------|--------------------------------|
| 1              | $\text{H}_2\text{O}/\text{acac}$          | Glucose   | 46                             |
| 2              | $\text{H}_2\text{O}/\text{acetone}$       | Glucose   | —                              |
| 3              | $\text{H}_2\text{O}/\text{ethyl acetate}$ | Glucose   | —                              |
| 4              | acac                                      | Glucose   | 18                             |
| 5              | $\text{EtOH}/\text{acac}$                 | Glucose   | 16                             |
| 6              | $\text{H}_2\text{O}/\text{acac}$          | GA        | 83                             |
| 7 <sup>b</sup> | $\text{H}_2\text{O}/\text{acac}$          | GA        | 82                             |
| 8              | $\text{H}_2\text{O}/\text{acac}$          | Mannose   | 46                             |
| 9              | $\text{H}_2\text{O}/\text{acac}$          | Xylose    | 12                             |
| 10             | $\text{H}_2\text{O}/\text{acac}$          | Fructose  | 9                              |
| 11             | acac                                      | GA        | 66                             |

Reaction conditions: 300 mg of substrate, total solvent volume = 13 mL,  $\text{H}_2\text{O}/\text{solvent} = 1/1$ , 220 °C, 30 min, 2.5 MPa  $\text{N}_2$ , 600 rpm. <sup>a</sup> MAF yield = mol of MAF per mol of glucose  $\times 100\%$ ; the amount of MAF is determined by GC using acetophenone as an internal standard. <sup>b</sup> 80 °C.



and, *e.g.*, at 200 °C, the  $pK_w$  is 11.31.<sup>14</sup> Water is a prominent proton or hydroxide ion source at high temperatures. However, in these MAF formation reactions, the measured pH of the aqueous phase ranges from 2.7 to 3.0 pH units depending on the applied reaction conditions (Table S3†). This phenomenon is likely due to the dissociation of acac in water,<sup>15</sup> as the pH value for the H<sub>2</sub>O/acac reaction medium at room temperature is measured as 3.1. In addition to the above, water is beneficial as it dissolves glucose well and generates a homogeneous reaction medium for the reaction.

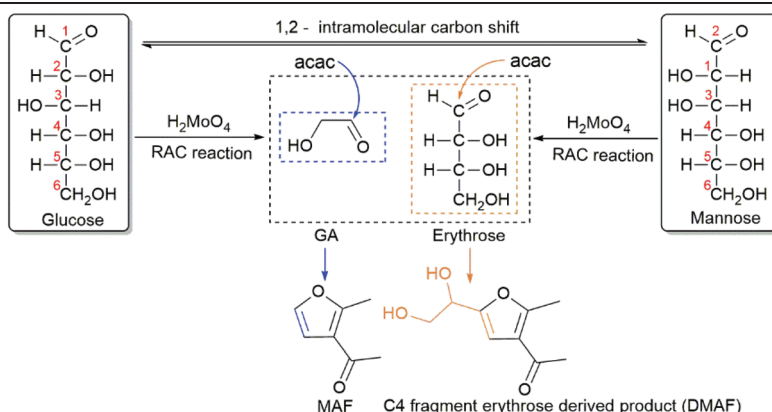
As we searched for ways to improve the efficiency of the reaction, it soon became clear that the RAC, which forms GA, is a high-temperature step in the concerted reaction. The high yield reaction between pure GA and acac can occur even at 80 °C (Table 1, entry 7). An additional <sup>1</sup>H NMR study revealed that GA reacts fast with acac and the GA signal disappears in 1 min at 100 °C (Fig. S5 and 6†). Previous publications support the reasoning; high GA yields are normally obtained under supercritical water (>373 °C, >22 MPa) and in a flow reactor where the formed GA can be rapidly separated.<sup>13e,16</sup> In general, the elevated reaction temperature is related to the high activation energy of the RAC of glucose.<sup>17</sup> Following this idea and increasing the reaction temperature, we achieved a yield of

49% for MAF at 240 °C, but at 260 °C, the yield decreased slightly (Table S1†). Therefore, increasing the temperature quickly hit the limit, and we had to look for alternative solutions.

### H<sub>2</sub>MoO<sub>4</sub> catalysed reaction

The ideal catalyst to enhance the RAC towards GA should be able to reduce the required activation energy while minimizing the isomerization of glucose to fructose. In this respect, Mo(vi) compounds (*i.e.*, molybdic acid, molybdenum oxide, and polyoxometalates) are attractive, as they are known to catalyse the epimerization of glucose to mannose through a 1,2-intramolecular carbon shift (1,2-CS), known as the Bilik reaction.<sup>18</sup> Mo-containing catalysts also show reactivity in the production of formic acid and glycolic acid from cellulose *via* the RAC pathway combined with oxidation.<sup>19</sup> Therefore, we introduced commercially available H<sub>2</sub>MoO<sub>4</sub> to our studies. When we performed the H<sub>2</sub>MoO<sub>4</sub>-catalysed reaction at 220 °C, a significant increase in MAF yield to 66% was observed (Table 2, entry 9). To our surprise, reducing the reaction temperature as low as 100 °C gave a MAF yield of 59% (Table 2, entry 7), while in contrast no transformation occurs without an H<sub>2</sub>MoO<sub>4</sub> catalyst. This is a marked enhancement when compared to an uncata-

**Table 2** MAF and DMAF yields under various reaction conditions with the H<sub>2</sub>MoO<sub>4</sub> catalyst and the proposed reaction pathway



| Entry           | <i>T</i> (°C) | Time (min) | Conversion <sup>a</sup> (mol %) | Mannose yield <sup>a</sup> (mol %) | MAF yield (mol %)/C(%) <sup>c</sup> | DMAF yield <sup>b</sup> (mol %)/C(%) <sup>c</sup> |
|-----------------|---------------|------------|---------------------------------|------------------------------------|-------------------------------------|---|
| 1               | 60            | 30         | 54                              | 8                                  | 16/5                                | 19/13   |
| 2               | 80            | 30         | 84                              | 6                                  | 45/15                               | 36/23   |
| 3               | 80            | 120        | 93                              | 4                                  | 56/19                               | 36/24   |
| 4               | 80            | 180        | 98                              | 2                                  | 59/20                               | 41/28   |
| 5               | 80            | 240        | 99                              | 1                                  | 59/20                               | 42/28   |
| 6               | 100           | 15         | 98                              | 2                                  | 55/18                               | 40/27   |
| 7               | 100           | 30         | 100                             | 1                                  | 59/20                               | 39/26   |
| 8               | 120           | 30         | 100                             | —                                  | 59/20                               | 37/25   |
| 9               | 220           | 30         | 100                             | —                                  | 66/22                               | —   |
| 10 <sup>d</sup> | 100           | 30         | 64                              | 44                                 | —                                   | —   |
| 11 <sup>e</sup> | 80            | 30         | —                               | —                                  | 87                                  | —   |
| 12 <sup>f</sup> | 100           | 120        | 100                             | —                                  | 52/17                               | 37/25   |

Reaction conditions: 300 mg (46 g L<sup>-1</sup>) of glucose, 100 mg of H<sub>2</sub>MoO<sub>4</sub>, H<sub>2</sub>O/acac = 1/1 (6.5 mL/6.5 mL), 2.5 MPa N<sub>2</sub>, 600 rpm. <sup>a</sup> Measured by HPLC using authentic glucose and mannose as standards. <sup>b</sup> DMAF yield = mol of DMAF per mol of glucose × 100%; the amount of DMAF is determined by <sup>1</sup>H NMR in MeOD using 2-methylfuran as an internal standard. <sup>c</sup> Carbon yield is calculated based on carbon atoms in glucose. Carbon yield of MAF = 2 × mol of MAF/6 × mol of glucose × 100%; carbon yield of DMAF = 4 × mol of DMAF/6 × mol of glucose × 100%. <sup>d</sup> In the absence of acac. <sup>e</sup> GA as a starting material. <sup>f</sup> 975 mg (150 g L<sup>-1</sup>) of glucose and 321 mg of H<sub>2</sub>MoO<sub>4</sub>.



lyzed reaction with a record yield of 46% at 220 °C (Table 1, entry 1).

We studied the reaction parameters to optimize the yield and gain further insight into the  $\text{H}_2\text{MoO}_4$ -catalysed transformations at low temperatures. At a fixed reaction time (30 min), the yield of MAF improved markedly from 16% to 59% as the temperature increased from 60 °C to 100 °C (Table 2, runs 1, 2 and 7). Similarly, there was a positive correlation with the MAF yield when the catalyst loading amount ranged from 10 to 33 wt%; above this, the generation of MAF remained consistent at 59% even when a nearly stoichiometric amount of  $\text{H}_2\text{MoO}_4$  was used (Table S5†). The extension of reaction time from 30 to 180 min at 80 °C resulted in the same MAF yield as that at 100 °C for 30 min (Table 2, entries 2–4 vs. 7).

In the catalysed, low-temperature reactions, our attention was drawn to the formation of a new product. Detailed  $^1\text{H}$ ,  $^{13}\text{C}$ , and 2D NMR and HRESI-MS (high-resolution electrospray-ionization mass spectra) analyses confirmed that the isolated product is 1-(5-(1,2-dihydroxyethyl)-2-methylfuran-3-yl)ethan-1-one (DMAF), an aldol condensation product of acac and the C4 fragment, erythrose (Table 2; Figs. S7–10†). DMAF can be obtained with a yield of up to 42%, thus offering an efficient approach for underexplored erythrose-based C4 chemistry in biorefining.

Under the applied reaction conditions,  $\text{H}_2\text{MoO}_4$  can epimerize glucose to mannose. Our control experiment in the absence of acac showed that 64% of glucose was converted and 44% of mannose was formed (Table 2, entry 10). This result is in line with previous glucose epimerization studies<sup>18b,d</sup> and with the low activation barrier reported for Mo-catalysed 1,2-CS (21.1 kcal mol<sup>-1</sup>).<sup>20</sup> Mechanistically, for successful glucose/mannose epimerization, a carbon skeleton rearrangement should occur through the cleavage of the C2–C3 bond with the subsequent formation of a new C1–C3 bond.<sup>18b,d,21</sup> However, if the main catalytic process is only the formation of mannose, the uncatalysed retro-aldol reaction would still remain the rate-limiting, high energy step in the MAF formation, requiring high reaction temperature.  $\text{H}_2\text{MoO}_4$  is able to catalyse the reaction at 80 °C with high yield. Therefore, the substantial reduction of reaction temperature indicates a catalysed reaction pathway for RAC, employing  $\text{H}_2\text{MoO}_4$ -catalysed breaking of the C2–C3 bond. As acac is prone to react with GA under the applied conditions (Figs. S5 and 11†), a mechanistic scheme is proposed (Table 2). The  $\text{H}_2\text{MoO}_4$  catalyst lowers the high activation energy of RAC and enables the efficient formation of GA at mild temperature for MAF synthesis. Accordingly, the same mechanistic process applies for DMAF, where the released C4 fragment (erythrose) directly reacts with acac. DMAF seems to be unstable at high temperature (Table 2, entry 9). Thus, the integration of RAC by  $\text{H}_2\text{MoO}_4$  and high reactivity between acac and GA or erythrose are needed for the high yields of MAF and DMAF at mild reaction temperature. Simultaneously with the RAC reaction,  $\text{H}_2\text{MoO}_4$  also catalyses the epimerization of glucose to mannose by 1,2-CS. Both glucose and mannose can undergo C2 + C4 RAC. There is an open discus-

sion in the literature as to whether there is a mechanistic relationship between RAC and 1,2-CS.<sup>4a,13b,13c,22</sup> However, comprehensive theoretical publications or direct experimental evidence are lacking.

It is noteworthy that the yield of MAF remained satisfactory (52%) when the glucose concentration was up to 150 g L<sup>-1</sup>, which is of great significance for reaction upscaling (Table 2, entry 12; Table S6†). In addition, the system is very promising as it enables the straightforward conversion of microcrystalline cellulose and wood (pine), as an example of lignocellulosic biomass, to MAF (45% and 59%, respectively; the MAF yield is calculated based on the mol of product per the mol of sugar units in cellulose and wood) with the aid of NaCl (Tables S7 and 8,† see also the explanation and detailed calculation methods in the ESI). Based on the reaction scheme, two carbon atoms of MAF are from GA, whereas in erythrose-derived DMAF, four carbon atoms originate from glucose. When looking at the amount of renewable carbon in the products and the carbon yield of the syntheses, attention is drawn not only to glucose but also to acac; the 5/7 and 5/9 carbon atoms of MAF and DMAF are derived from acac. From this point of view, acac is an almost perfect reagent. It is here a component of very high atom economy and can be prepared directly from glucose *via* the biosynthetic pathway<sup>23</sup> or *via* the bio-based triacetic acid lactone pathway in almost quantitative yield (Fig. S12†).<sup>24</sup> Carbon yield towards glucose, as a sum of MAF and DMAF formation in the catalysed reaction under optimized conditions, is 48% (Table 2, entry 4). Although this is a rather good number for a RAC-derived cascade-type reaction, there is scope for the development of a further catalysis or synthesis strategy to improve the carbon efficiency.

## Conclusions

In summary, we have developed a new strategy to convert glucose directly to MAF and DMAF *via* RAC with subsequent aldol condensation. The reaction benefits from several elementary steps. The non-catalytic approach requires high temperature for C2 + C4 RAC, and it was shown that GA is a key intermediate in the MAF formation reaction. Acac, which is a good nucleophile and weak acid in water, is essential to capture GA *in situ* through aldol condensation. The catalytic approach for MAF was performed with the use of  $\text{H}_2\text{MoO}_4$ . Its capability for the 1,2-CS transformation of glucose is known, but here, it demonstrates a pivotal role in C2 + C4-type RAC and enables GA and erythrose formation under significantly mild reaction conditions (80 °C). As a result, a novel route to MAF and DMAF synthesis is established. Both of them can be seen as chemicals with potential for application in the pharmaceutical and fine chemical industries. Notably, natural carbohydrates including cellulose and raw wood materials can be converted to MAF using the presented approaches. Further studies are focused on catalyst design to improve the carbon efficiency and the synthesis of other value-added chemicals with this strategy.



## Author contributions

Rui Zhang: investigation, methodology, data curation, formal analysis, software, writing – original draft, and writing – review and editing; Aleksí Eronen: data curation, formal analysis, and software; Xiangze Du: methodology and data curation; Enlu Ma: methodology and formal analysis; Ming Guo: methodology; Karina Moslova: resources; Prof. Timo Repo\*: conceptualization, funding acquisition, supervision, resources, project administration, and writing – review and editing.

## Conflicts of interest

There are no conflicts to declare.

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## References

- (a) Y. Liao, S.-F. Koelewyn, G. Van den Bossche, J. Van Aelst, S. Van den Bosch, T. Renders, K. Navare, T. Nicolaï, K. Van Aelst, M. Maesen, H. Matsushima, J. M. Thevelein, K. Van Acker, B. Lagrain, D. Verboekend and B. F. Sels, *Science*, 2020, **367**, 1385–1390; (b) Y. Liu, Y. Nie, X. Lu, X. Zhang, H. He, F. Pan, L. Zhou, X. Liu, X. Ji and S. Zhang, *Green Chem.*, 2019, **21**, 3499–3535; (c) P. Sudarsanam, E. Peeters, E. V. Makshina, V. I. Parvulescu and B. F. Sels, *Chem. Soc. Rev.*, 2019, **48**, 2366–2421; (d) Z. Sun, G. Bottari, A. Afanasenko, M. C. A. Stuart, P. J. Deuss, B. Fridrich and K. Barta, *Nat. Catal.*, 2018, **1**, 82–92; (e) P. Ferrini and R. Rinaldi, *Angew. Chem., Int. Ed.*, 2014, **53**, 8634–8639; (f) R. Gérardy, D. P. Debecker, J. Estager, P. Luis and J.-C. M. Monbaliu, *Chem. Rev.*, 2020, **120**, 7219–7347; (g) X. Luo, Y. Li, N. K. Gupta, B. Sels, J. Ralph and L. Shuai, *Angew. Chem., Int. Ed.*, 2020, **59**, 11704–11716; (h) Y. Liu, C. Luo and H. Liu, *Angew. Chem., Int. Ed.*, 2012, **51**, 3249–3253; (i) P. N. R. Vennestrøm, C. M. Osmundsen, C. H. Christensen and E. Taarning, *Angew. Chem., Int. Ed.*, 2011, **50**, 10502–10509.
- (a) J. Song, H. Fan, J. Ma and B. Han, *Green Chem.*, 2013, **15**, 2619–2635; (b) S. Kang, J. Fu and G. Zhang, *Renew. Sustain. Energy Rev.*, 2018, **94**, 340–362; (c) Y. Yang, C.-w. Hu and M. M. Abu-Omar, *Green Chem.*, 2012, **14**, 509–513; (d) X. Zhang, P. Murria, Y. Jiang, W. Xiao, H. I. Kenttämaa, M. M. Abu-Omar and N. S. Mosier, *Green Chem.*, 2016, **18**, 5219–5229; (e) M. E. Zakrzewska, E. Bogel-Lukasik and R. Bogel-Lukasik, *Chem. Rev.*, 2011, **111**, 397–417; (f) L. T. Mika, E. Cséfalvay and Á. Németh, *Chem. Rev.*, 2018, **118**, 505–613.
- W. Faveere, S. Van Praet, B. Vermeeren, K. N. R. Dumoleijn, K. Moonen, E. Taarning and B. F. Sels, *Angew. Chem., Int. Ed.*, 2021, **60**, 12204–12223.
- (a) M. Zheng, J. Pang, R. Sun, A. Wang and T. Zhang, *ACS Catal.*, 2017, **7**, 1939–1954; (b) J. Pang, M. Zheng, R. Sun, A. Wang, X. Wang and T. Zhang, *Green Chem.*, 2016, **18**, 342–359.
- (a) W. Faveere, T. Mihaylov, M. Pelckmans, K. Moonen, F. Gillis-D'Hamers, R. Bosschaerts, K. Pierloot and B. F. Sels, *ACS Catal.*, 2020, **10**, 391–404; (b) G. Liang, A. Wang, L. Li, G. Xu, N. Yan and T. Zhang, *Angew. Chem., Int. Ed.*, 2017, **56**, 3050–3054.
- (a) W. Caminati and J.-U. Grabow, *J. Am. Chem. Soc.*, 2006, **128**, 854–857; (b) Y. Jing, Y. Zhang, Q. Lv, Y. Guo, X. Liu and Y. Wang, *Green Chem.*, 2019, **21**, 6236–6240.
- (a) E. Baciocchi and R. Ruzziconi, *Synth. Commun.*, 1988, **18**, 1841–1846; (b) Y. Ji, J. Pan, P. Dauenhauer and R. J. Gorte, *Appl. Catal., A*, 2019, **577**, 107–112.
- N. Ronaghi, D. M. Fialho, C. W. Jones and S. France, *J. Org. Chem.*, 2020, **85**, 15337–15346.
- (a) H. G. Heller and G. A. Jenkins, *J. Chem. Soc., Perkin Trans. 1*, 1984, 2877–2880; (b) A. P. Glaze, H. G. Heller and J. Whittall, *J. Chem. Soc., Perkin Trans. 2*, 1992, 591–594.
- (a) Y. O. Remizov, L. M. Pevzner and M. L. Petrov, *Russ. J. Gen. Chem.*, 2018, **88**, 1402–1410; (b) L. M. Pevzner, Y. O. Remizov and M. L. Petrov, *Russ. J. Gen. Chem.*, 2015, **85**, 61–70.
- J. Saunders, D. C. Tipney and P. Robins, *Tetrahedron Lett.*, 1982, **23**, 4147–4150.
- The possible reaction routes for DMAF like polyhydroxalkyl furans as platform molecules for other final products has been reported previously; see the reference: V. Escande, T. K. Olszewski, E. Petit and C. Grison, *ChemSusChem*, 2014, **7**, 1915–1923.
- (a) S. Yamaguchi and T. Baba, *Molecules*, 2016, **21**, 937; (b) M. Orazov and M. E. Davis, *Proc. Natl. Acad. Sci. U. S. A.*, 2015, **112**, 11777; (c) Y. Yan, L. Feng, G. Li, S. Lin, Z. Sun, Y. Zhang and Y. Tang, *ACS Catal.*, 2017, **7**, 4473–4478; (d) A. Bayu, A. Abudula and G. Guan, *Fuel Process. Technol.*, 2019, **196**, 106162; (e) C. B. Schandel, M. Høj, C. M. Osmundsen, A. D. Jensen and E. Taarning, *ChemSusChem*, 2020, **13**, 688–692.
- (a) C. Luo, S. Wang and H. Liu, *Angew. Chem., Int. Ed.*, 2007, **46**, 7636–7639; (b) A. Kruse and E. Dinjus, *J. Supercrit. Fluids*, 2007, **39**, 362–380.
- J. Sary and J. O. Liljenzin, *Pure Appl. Chem.*, 1982, **54**, 2557–2592.
- M. Sasaki, K. Goto, K. Tajima, T. Adschiri and K. Arai, *Green Chem.*, 2002, **4**, 285–287.
- J. Zhang, B. Hou, A. Wang, Z. Li, H. Wang and T. Zhang, *AIChE J.*, 2014, **60**, 3804–3813.
- (a) V. Bílik, L. Petruš and V. Farkaš, *Chem. Zvesti*, 1975, **5**, 690–693; (b) L. Petruš, M. Petrušová and Z. Hricoviniová, in *Glycoscience: Epimerisation, Isomerisation and Rearrangement Reactions of Carbohydrates*, ed. A. E. Stütz, Springer Berlin Heidelberg, Berlin, Heidelberg, 2001, pp.



- 15–41, DOI: 10.1007/3-540-44422-x\_2; (c) A. Takagaki, S. Furusato, R. Kikuchi and S. T. Oyama, *ChemSusChem*, 2015, **8**, 3769–3772; (d) F. Ju, D. VanderVelde and E. Nikolla, *ACS Catal.*, 2014, **4**, 1358–1364; (e) I. Delidovich and R. Palkovits, *ChemSusChem*, 2016, **9**, 547–561; (f) M. Rellán-Piñero, M. Garcia-Ratés and N. López, *Green Chem.*, 2017, **19**, 5932–5939.
- 19 (a) J. Albert, R. Wölfel, A. Bösmann and P. Wasserscheid, *Energy Environ. Sci.*, 2012, **5**, 7956–7962; (b) J. Zhang, X. Liu, M. Sun, X. Ma and Y. Han, *ACS Catal.*, 2012, **2**, 1698–1702; (c) T. Lu, M. Niu, Y. Hou, W. Wu, S. Ren and F. Yang, *Green Chem.*, 2016, **18**, 4725–4732.
- 20 B. K. Chethana, D. Lee and S. H. Mushrif, *J. Mol. Catal. A: Chem.*, 2015, **410**, 66–73.
- 21 M. L. Hayes, N. J. Pennings, A. S. Serianni and R. Barker, *J. Am. Chem. Soc.*, 1982, **104**, 6764–6769.
- 22 J. Iglesias, I. Martínez-Salazar, P. Maireles-Torres, D. Martín Alonso, R. Mariscal and M. López Granados, *Chem. Soc. Rev.*, 2020, **49**, 5704–5771.
- 23 Y. Zhou, Y. Ding, W. Gao, J. Wang, X. Liu, M. Xian, X. Feng and G. Zhao, *Biotechnol. Biofuels*, 2020, **13**, 88.
- 24 (a) B. H. Shanks and P. L. Keeling, *Green Chem.*, 2017, **19**, 3177–3185; (b) M. Chia, T. J. Schwartz, B. H. Shanks and J. A. Dumesic, *Green Chem.*, 2012, **14**, 1850–1853; (c) L. P. Saunders, M. J. Bowman, J. A. Mertens, N. A. Da Silva and R. E. Hector, *J. Ind. Microbiol. Biotechnol.*, 2015, **42**, 711–721; (d) D. Xie, Z. Shao, J. Achkar, W. Zha, J. W. Frost and H. Zhao, *Biotechnol. Bioeng.*, 2006, **93**, 727–736.

