

STATIC MIXER APPLICATION IN ENHANCING BIOGRANULES
TREATMENT THROUGH HYDRODYNAMIC SHEAR FORCE IN
SEQUENCING BATCH REACTOR

SURYATI SULAIMAN

A thesis submitted in fulfilment of the
requirements for the award of the degree of
Doctor of Philosophy (Civil Engineering)

School of Civil Engineering
Faculty of Engineering
Universiti Teknologi Malaysia

SEPTEMBER 2019

DEDICATION

To my pillar of strength

Abdul Syukor bin Abd Razak

Aisyah Syahirah binti Abdul Syukor

Alya Safura binti Abdul Syukor

ACKNOWLEDGEMENT

In preparing this thesis, I was in contact with many people, researchers, academicians, and practitioners. They have contributed towards my understanding and thoughts. In particular, I wish to express my sincere appreciation to my main supervisor, Professor Dr. Azmi Aris, for encouragement, guidance, critics and friendship. I am also very thankful to my co-supervisor Associate Professor Dr Khalida Muda and Dr. Aznah Nor Anuar for their guidance, advices and motivation. Without their continued support and interest, this thesis would not have been the same as presented here.

I am also indebted to Ministry of Education and Universiti Malaysia Pahang (UMP) for funding my Ph.D study. I am thankful to Environmental laboratory, School of Civil Engineering for providing the facilities for my research. Special thanks also go to Technicians and staff for their assistance in this research.

My sincere appreciation also extends to all my colleagues and others who have provided assistance throughout my work and studies. Their views and tips are useful indeed. Unfortunately, it is not possible to list all of them in this limited space. Last but not least, greatest appreciation to all my family members for their unconditional love and care.

ABSTRACT

Biogranulation is considered a promising technology in biological wastewater treatment due to its high effluent treatment quality, strong ability to withstand organic loading, strong microbial structure and high capability to remove organics, nitrogen and phosphate. Hydrodynamic shear force in terms of superficial air velocity (SAV) is known as one of the significant factors in biogranulation process. High SAV would lead to the requirement of high aeration energy in biogranulation system while lowering the SAV will not be able to form biogranules of desired characteristics. The main objective of this study was to determine the effect of static mixer at low SAV on physical properties and removal performance of biogranules in treating synthetic textile wastewater. Experiments were divided into initial, development and post-development stages. Four static mixers namely SM1, SM2, SM3 and SM4 were designed and tested in the initial phase of the study. The best static mixer was chosen based on the mixing time study. The experiments were carried out in Sequencing Batch Reactor (SBR) made of acrylic with a height of 100 cm, diameter of 8 cm and a working volume of 1.5 L, at an exchange ratio of 50%. Three reactors with static mixer and another three operating without static mixer (R1-0.5N, R1-0.5Y, R2-1.4N, R2-1.4Y, R3-2.1N and R3-2.1Y) were used during development stage to investigate the properties and performance of developed granules under influence of static mixers and SAVs of 0.5, 1.4 and 2.1 cm/s. The influence of hydraulic retention time (HRT) and organic loading rate (OLR) on the properties and performance of aerobic granules were investigated during post development stage. Two reactors named as R4Y and R4N were used, where R4Y was a reactor with static mixer and R4N was without the static mixer. The mixing study revealed that SM1 was the best static mixer as compared to SM2, SM3 and SM4 due to the shortest mixing time of 8 sec. The results in development stage disclosed that the granules could be developed at low SAV using static mixer (R1-0.5Y) with integrity coefficient (IC) of 40.5%, sludge volume index (SVI) of 107.5 mL/g, settling velocity (SV) of 70.3 m/h, chemical oxygen demand (COD) removal of 94.6% and color removal of 53.8%. The results also showed that the developed granules in others reactors with static mixer improved the physical properties and reactor performance. Reactor R2-1.4Y was the best with an IC of 27.5%, SVI of 29.6 mL/g, SV of 80.4 m/h, COD removal of 94.2% and color removal of 63.1%. The study also demonstrated that HRT and OLR affected the performance of biogranules. Again, the physical characteristics of biogranules and removal efficiencies of the reactor with static mixer seemed to be better as compared to the reactor without static mixer with increasing of HRT and OLR. The increase of HRT in the system resulted in decreasing of SRT (R4N-95.1 days, R4Y-96.8 days) with increasing of overall specific biomass growth rate ($\mu_{overall}$) (R4N-0.011 per day, R4Y-0.010 per day), endogenous decay rate (k_d) (R4N-0.178 per day, R4Y-0.241 per day), observed biomass yield (Y_{obs}) (R4N-0.052 mg VSS/mg COD, R4Y-0.051 mg VSS/mg COD) and theoretical biomass yield (Y) (R4N-0.938 mg VSS/mg COD, R4Y-1.230 mg VSS/mg COD). Meanwhile, the higher OLR of the system increased the SRT (R4N-96.2 days, R4Y-100 days) which led to the decreasing of $\mu_{overall}$ (R4N-0.010 per day, R4Y-0.010 per day), k_d (R4N-0.179 per day, R4Y-0.197 per day), Y_{obs} (R4N-0.027 mg VSS/mg COD, R4Y-0.028 mg VSS/mg COD) and Y (R4N-0.497 mg VSS/mg COD, R4Y-0.587 mg VSS/mg COD). At lower SAV, the use of static mixer provided shorter SRT which resulted in higher $\mu_{overall}$, k_d , Y_{obs} and Y compared to the reactor without static mixer. The findings proved that static mixer is capable to enhance hydrodynamic shear force at low SAV in biogranulation system and therefore, will lower the energy consumption and operational cost.

ABSTRAK

Biogranulasi dikenal pasti sebagai salah satu teknologi berkeupayaan tinggi bagi sistem olahan air sisa secara biologi disebabkan keupayaan menghasilkan effluen berkualiti tinggi, daya tahanan terhadap beban organik, struktur mikrob yang kuat serta keupayaan yang tinggi untuk menyingkirkan bahan organik, nitrogen dan fosfat. Daya ricih hidrodinamik dalam bentuk halaju udara permukaan (SAV) dikenal pasti sebagai salah satu faktor utama di dalam proses biogranulasi. Nilai SAV yang tinggi akan menyebabkan keperluan tenaga pengudaraan yang tinggi manakala nilai SAV yang rendah tidak akan dapat membentuk biogranul yang mempunyai ciri-ciri yang dikehendaki. Objektif utama kajian ini adalah untuk mengenal pasti kesan pengaduk statik pada SAV rendah terhadap ciri-ciri fizikal dan prestasi penyingkiran biogranul di dalam mengolah air sisa tekstil. Ujikaji dibahagikan kepada peringkat permulaan, pembentukan dan pasca pembentukan. Empat pengaduk statik iaitu SM1, SM2, SM3 dan SM4 direka bentuk dan diuji semasa peringkat permulaan kajian. Pengaduk statik terbaik telah dipilih berdasarkan ujian masa pembauran. Semua ujikaji dijalankan menggunakan Reaktor Kelompok Berjujukan (SBR) yang diperbuat daripada akrilik dengan ketinggian 100 cm, diameter 8 cm dan isipadu kerja 1.5 L serta nisbah pertukaran 50%. Tiga reaktor dengan pengaduk statik dan tiga lagi tanpa pengaduk statik (R1-0.5N, R1-0.5Y, R2-1.4N, R2-1.4Y, R3-2.1N dan R3-2.1Y) di bawah SAVs 0.5, 1.4 dan 2.1 cm/s telah digunakan semasa peringkat pembentukan bagi mengenal pasti ciri-ciri dan prestasi granul yang terbentuk. Di peringkat pasca pembentukan, pengaruh masa tahanan hidraulik (HRT) dan kadar beban organik (OLR) telah dikenal pasti. Dua reaktor yang dinamakan sebagai R4Y dan R4N telah digunakan, di mana R4Y adalah reaktor dengan pengaduk statik manakala R4N adalah reaktor tanpa pengaduk statik. Ujian masa pembauran menunjukkan bahawa SM1 adalah pengaduk statik terbaik kerana mempunyai masa pembauran terpanjang iaitu 8 saat jika dibandingkan dengan SM2, SM3 dan SM4. Keputusan kajian peringkat pembentukan mendapati bahawa reaktor yang mempunyai pengaduk statik (R1-0.5Y) dan nilai SAV yang rendah menghasilkan biogranul dengan nilai pekali integriti (IC) sebanyak 40.5%, indeks isipadu enapcemar (SVI) sebanyak 107.5 mL/g, halaju pegenapan (SV) sebanyak 70.3 m/h, penyingkiran permintaan oksigen kimia (COD) sebanyak 94.6% dan penyingkiran warna sebanyak 53.8%. Hasil ujikaji juga mendapati reaktor lain yang mempunyai pengaduk statik mampu menghasilkan biogranul yang mempunyai ciri-ciri fizikal dan kadar prestasi yang lebih baik. Reaktor R2-1.4Y merupakan reaktor yang terbaik dengan IC serendah 27.5%, SVI sebanyak 29.6 mL/g, SV sebanyak 80.4 m/h, penyingkiran COD sebanyak 94.2% dan penyingkiran warna sebanyak 63.1%. Kajian juga mendapati bahawa HRT dan OLR mempengaruhi prestasi biogranul. Dengan peningkatan HRT dan OLR juga, ciri-ciri fizikal dan kadar kecekapan penyingkiran bagi reaktor mempunyai pengaduk statik didapati lebih baik berbanding reaktor tanpa pengaduk statik. Peningkatan HRT memendekkan masa tahanan pepejal (SRT) (R4N-95.1 hari, R4Y-96.8 hari) yang mengakibatkan peningkatan nilai keseluruhan kadar pertumbuhan biojisim spesifik ($\mu_{overall}$) (R4N-0.011 per hari, R4Y-0.010 per hari), kadar kematian (k_d) (R4N-0.178 per hari, R4Y-0.241 per hari), hasil biojisim yang diperhatikan (Y_{obs}) (R4N-0.052 mg VSS/mg COD, R4Y-0.051 mg VSS/mg COD) dan hasil biojisim teori (Y) (R4N-0.938 mg VSS/mg COD, R4Y-1.230 mg VSS/mg COD). Sementara itu, peningkatan nilai OLR meningkatkan SRT (R4N-96.2 hari, R4Y-100 hari) yang menyebabkan penurunan $\mu_{overall}$ (R4N-0.010 per hari, R4Y-0.010 per hari), k_d (R4N-0.179 per hari, R4Y-0.197 per hari), Y_{obs} (R4N-0.027 mg VSS/mg COD, R4Y-0.028 mg VSS/mg COD) and Y (R4N-0.497 mg VSS/mg COD, R4Y-0.587 mg VSS/mg COD). Pada nilai SAV yang rendah, penggunaan pengaduk statik menghasilkan nilai SRT yang lebih pendek dan seterusnya meningkatkan nilai $\mu_{overall}$, k_d , Y_{obs} dan Y jika dibandingkan dengan reaktor tanpa pengaduk statik. Hasil ujikaji membuktikan bahawa pengaduk statik mampu meningkatkan daya ricih hidrodinamik di dalam sistem biogranulasi walaupun pada nilai SAV yang rendah, dan oleh itu akan menurunkan penggunaan tenaga dan kos operasi.

TABLE OF CONTENTS

	TITLE	PAGE
	DECLARATION	ii
	DEDICATION	iii
	ACKNOWLEDGEMENT	iv
	ABSTRACT	v
	ABSTRAK	vi
	TABLE OF CONTENTS	vii
	LIST OF TABLES	xi
	LIST OF FIGURES	xv
	LIST OF ABBREVIATIONS	xix
	LIST OF SYMBOLS	xxi
	LIST OF APPENDICES	xxii
CHAPTER 1	INTRODUCTION	1
1.1	Preamble	1
1.2	Problem Statement	4
1.3	Objectives of Study	5
1.4	Scope of Study	6
1.5	Significance of Study	7
1.6	Thesis Organization	8
CHAPTER 2	LITERATURE REVIEW	9
2.1	Introduction	9
2.2	Biogranulation Technology	10
2.2.1	Anaerobic Granulation	10
2.2.2	Aerobic Granulation	12
2.2.3	Biogranules Formation	14
2.2.4	Characteristics of Biogranules	15
2.2.4.1	Morphology and Size	16

	2.2.4.2	Strength	16
	2.2.4.3	Settleability	17
	2.2.4.4	Extracellular Polymeric Substances	18
	2.2.4.5	Microbial Diversity	19
	2.2.4.6	Microbial Growth Kinetics	19
2.3		Factors Affecting Aerobic Granulation	22
	2.3.1	Composition of Substrate	23
	2.3.2	Organic Loading Rate	24
	2.3.3	Dissolved Oxygen	27
	2.3.4	Settling Time	28
	2.3.5	Hydraulic Retention Time	30
	2.3.6	Volume Exchange Rate	32
	2.3.7	Hydrodynamic Shear Force	33
2.4		Application of Biogranulation Technology	37
	2.4.1	Application of Biogranulation in Wastewater Treatment	37
	2.4.2	Application of Biogranulation in Treating Textile Wastewater	45
2.5		Static Mixer	54
2.6		Mixing Time	59
2.7		Research Needs	61
CHAPTER 3		RESEARCH METHODOLOGY	63
	3.1	Introduction	63
	3.2	Materials and Equipment	65
	3.2.1	Wastewater Composition	65
	3.2.2	Seeding Sludge	65
	3.2.3	Chemicals and Reagents	66
	3.2.4	Equipment	66
	3.2.5	Reactor Set Up	67
	3.2.6	Static Mixer	71
	3.3	Analytical Method	74
	3.3.1	Physical Parameters	74

3.3.1.1	Granules Diameter	74
3.3.1.2	Granules Strength	75
3.3.1.3	Settling Velocity	76
3.3.1.4	Sludge Volume Index	76
3.3.2	Biological Parameters	77
3.3.2.1	Morphology and Structure of the Granules	77
3.3.2.2	Microbial Observation	77
3.3.2.3	Oxygen Utilization Rate	79
3.4	Experimental Procedures	79
3.4.1	Mixing Time Study of Static Mixer	79
3.4.2	Development Stage of Granules	81
3.4.3	Post-development Stage of Granules	83
3.4.4	Sampling	85
3.5	Data Analysis	86
3.5.1	Removal Performance	86
3.5.2	Statistical Analysis	87
3.5.3	Determination of Kinetic Parameters	87
CHAPTER 4	RESULTS AND DISCUSSIONS	89
4.1	Introduction	89
4.2	Characteristics of Seed Sludge and Wastewater	89
4.3	Effect of Static Mixer and SAV on Mixing Time	91
4.3.1	Factors Influencing the Mixing Time	96
4.4	Development Stage: The Effect of Static Mixer on the Biogranules Development	99
4.4.1	Biomass Concentration Profile	99
4.4.2	Granules Strength	105
4.4.3	Settling Velocity	110
4.4.4	Sludge Volume Index	114
4.4.5	Size	120
4.4.6	Morphology of Granules	128
4.4.7	Treatment Performance	138

4.4.7.1	COD Removal Efficiency	138
4.4.7.2	Color Removal Efficiency	142
4.5	Performance of Bioreactors under Different HRT at Post Steady Stage	147
4.5.1	Biomass Profile	147
4.5.2	Granules Strength	149
4.5.3	Settling Ability	151
4.5.4	Size and Morphology	154
4.5.5	Treatment Performance	157
4.5.5.1	COD Removal Efficiency	157
4.5.5.2	Color Removal Efficiency	159
4.6	Performance of Biogranules under Different OLR at Post Steady Stage	163
4.6.1	Biomass Profile	163
4.6.2	Granules Strength	165
4.6.3	Settling Ability	167
4.6.4	Size and Morphology	170
4.6.5	Treatment Performance	175
4.7	Kinetic Behaviour of Aerobic Granules under Different Reaction Times and OLRs	180
4.7.1	Kinetic Behaviours of the Microorganismn at Development Stage	180
4.7.2	Kinetic Behaviours of Biogranules under Different HRT	189
4.7.3	Kinetic Behaviours of Biogranules under Different OLR	192
CHAPTER 5	CONCLUSION AND RECOMMENDATIONS	197
5.1	Conclusion	197
5.2	Recommendations	198
REFERENCES		201
LIST OF PUBLICATIONS		265

LIST OF TABLES

TABLE NO.	TITLE	PAGE
Table 2.1	Effect of OLR on the biogranulation system	26
Table 2.2	Effect of settling time on the biogranulation system	29
Table 2.3	Effect of HRT on the biogranulation process	31
Table 2.4	Studies carried out on the effect of hydrodynamic shear force on the biogranulation process	34
Table 2.5	Applications of aerobic granulation in treating various wastewater	39
Table 2.6	Characteristics of textile wastewater (Dos Santos et al., 2007)	46
Table 2.7	The advantages and disadvantages of various treatment methods in treating textile wastewater	48
Table 2.8	Biogranulation technology treating textile wastewater	53
Table 2.9	Potential advantages of static mixers over mechanical agitators	56
Table 2.10	Previous studies on various type of static mixers	58
Table 3.1	Components of synthetic wastewater (Manufacturer: Sigma Aldrich)	65
Table 3.2	List of reagents used in the study	66
Table 3.3	List of equipment used in the experiment	67
Table 3.4	Physical characteristics of the reactors used in the study	68
Table 3.5	Analytical methods or equipment employed during the study	74
Table 3.6	One complete cycle period of SBR during HRT of 8 hours	82
Table 3.7	Details experimental conditions during the development stage	83
Table 3.8	Reactor conditions for R4N and R4Y in post development stage	84
Table 3.9	Reactor operational conditions for R4N and R4Y in post development under various OLR and HRT at 16 hours	85
Table 3.10	Sampling point and frequency	86

Table 3.11	Formulas and calculation of kinetic parameters	88
Table 4.1	Physicochemical characteristics of seed sludge from the oxidation pond	90
Table 4.2	Physicochemical characteristics of synthetic wastewater used	91
Table 4.3	ANOVA results on different design of static mixer on mixing time	96
Table 4.4	Biomass profile in six reactors at initial and day 70	103
Table 4.5	Paired-samples <i>t</i> -test analysis for MLSS concentration	104
Table 4.6	Paired-samples <i>t</i> -test analysis for MLSS between R2-1.4Y and R3-2.1N	104
Table 4.7	IC values of granules in six reactors at initial and day 70	108
Table 4.8	Paired-samples <i>t</i> -test results for granules strength	109
Table 4.9	Paired-samples <i>t</i> -test results for IC between R2-1.4Y and R3-2.1N	109
Table 4.10	Settling velocities values of granules in six reactors at day 0 and day 70	112
Table 4.11	Paired-samples <i>t</i> -test results for SV	113
Table 4.12	Paired-samples T-test results for SV between R1-0.5Y, R2-1.4Y and R3-2.1N	114
Table 4.13	SVI values of granules in six reactors at initial and day 70	117
Table 4.14	Paired-samples <i>t</i> -test results for SVI	119
Table 4.15	Paired-samples <i>t</i> -test results for SVI between R2-1.4Y and R3-2.1N	120
Table 4.16	Granules size distribution for R1-0.5N and R1-0.5Y over the operational time	121
Table 4.17	Granules size distribution for R2-1.4N and R2-1.4Y over the operational time	123
Table 4.18	Granules size distribution for R3-2.1N and R3-2.1Y over the operational time	125
Table 4.19	Comparison between R1-0.5Y against R3-2.1N on granules size distribution over the operational time	127
Table 4.20	Paired-samples <i>t</i> -test results for COD removal	141
Table 4.21	Paired-samples <i>t</i> -test results for COD removal between R1-0.5Y, R2-1.4Y and R3-2.1N	142

Table 4.22	Paired-samples <i>t</i> -test results for color removal	144
Table 4.23	Paired-samples <i>t</i> -test results for color removal between R1-0.5Y, R2-1.4Y and R3-2.1N	145
Table 4.24	Overall performances of aerobic granules during development stage	146
Table 4.25	Paired-samples <i>t</i> -test values on MLSS	149
Table 4.26	Paired-samples <i>t</i> -test values on IC	150
Table 4.27	Paired-samples <i>t</i> -test values on SV	152
Table 4.28	Paired-samples <i>t</i> -test values on SVI	154
Table 4.29	Size of biogranules at different HRT	154
Table 4.30	Paired-samples <i>t</i> -test values on size of biogranules	155
Table 4.31	Paired-samples <i>t</i> -test values on COD removal	159
Table 4.32	Paired-samples <i>t</i> -test values on color removal	161
Table 4.33	Physical properties and removal performances at different HRT	162
Table 4.34	Paired-samples <i>t</i> -test values on MLSS	164
Table 4.35	Paired-samples <i>t</i> -test values on IC	160
Table 4.36	Paired-samples <i>t</i> -test values on SV	168
Table 4.37	Paired-samples <i>t</i> -test values on SVI	170
Table 4.38	Size of granules in reactor at different OLR	170
Table 4.39	Paired-samples <i>t</i> -test values on size of biogranules at different OLR	171
Table 4.40	Paired-samples <i>t</i> -test values on COD removal	176
Table 4.41	Paired-samples <i>t</i> -test values on color removal	178
Table 4.42	Overall performance of the reactors throughout the post development stage at various OLR	179
Table 4.43	Profile of OUR in reactors at development stages of experiment	185
Table 4.44	Kinetic parameters of granules during development stage	186
Table 4.45	Comparison of SRT for different types of activated sludge	187
Table 4.46	A summary of the biokinetic coefficients obtained from different sources	188

Table 4.47	Kinetic parameters for R4N and R4Y under different HRT	190
Table 4.48	Paired-samples <i>t</i> -test analysis between R4N and R4Y on kinetic parameters	191
Table 4.49	Total suspended solids in the effluent during post development stage at different HRT	192
Table 4.50	Kinetic parameters for R4N and R4Y under different OLR	193
Table 4.51	Total suspended solids in the effluent during post development stage at different OLR	194
Table 4.52	Paired-samples <i>t</i> -test analysis between R4N and R4Y on kinetic parameters	194

LIST OF FIGURES

FIGURE NO.	TITLE	PAGE
Figure 2.1	Typical activated sludge process (Metcalf and Eddy, 2003)	10
Figure 2.2	Typical operation phases in SBR system operation	13
Figure 2.3	Mechanism of aerobic granular sludge formation (Beun et al., 1999)	15
Figure 2.4	EPS in the biogranulation process (Tay et al., 2006)	18
Figure 2.5	Monod growth curve (Bren <i>et al.</i> , 2013)	20
Figure 2.6	Macrostructures of granules (a) glucose-fed and (b) acetate-fed under Scanning Electron Microscope (Tay et al., 2001)	24
Figure 2.7	Example mechanical agitators (Parvizi et al., 2016)	55
Figure 2.8	Some examples of commercial static mixers: (a) KMX-V, (b) SMX, (c) Custody Transfer, (d) Standard LPD, (e) Kenics KM, (f) ZT-MX, (g) SMI and (h) Corrugated channel reactors (Ghanem et al., 2014)	57
Figure 2.9	A typical curve for determination of mixing time, showing the response to the tracer pulse	60
Figure 3.1	Flowchart of framework of the study	64
Figure 3.2	Bioreactors used throughout the experimental	69
Figure 3.3	The schematic diagram of bioreactor system	70
Figure 3.4	Static mixer SM1	72
Figure 3.5	Static mixer SM2	72
Figure 3.6	Static mixer SM3	73
Figure 3.7	Static mixer SM4	73
Figure 3.8	Sputter coater for coating the sample before viewing under FESEM (Bio Rad Polaron Division SEM Coating System)	78
Figure 3.9	FESEM and EDX analyser (Carl Zeiss Supre VP)	78
Figure 3.10	The schematic diagram of reactor showing the tracer injection point	81
Figure 4.1	Microscopic examination on seed sludge morphology	90

Figure 4.2	A typical curve of determination mixing time response to conductivity values	92
Figure 4.3	Mixing time for (a) No SM (b) SM1 (c) SM2 (d) SM3 (e) SM4	93
Figure 4.4	Comparison of mixing time for No SM, SM1, SM2, SM3 and SM4 at SAV of 0.5, 1.4 and 2.1 cm/s	95
Figure 4.5	Mixing time for SM1 at SAVs of 0.5, 1.4 and 2.1 cm/s	97
Figure 4.6	Mixing time for SM1 at different position of injection point	98
Figure 4.7	Change in biomass concentration in R1-0.5N and R1-0.5Y	101
Figure 4.8	Change in biomass concentration in R2-1.4N and R2-1.4Y	102
Figure 4.9	Change in biomass concentration in R3-2.1N and R3-2.1Y	103
Figure 4.10	The trend in granules strength during the development stage in R1-0.5N and R1-0.5Y	106
Figure 4.11	The change in granules strength during the development stage in R2-1.4N and R2-1.4Y	107
Figure 4.12	The change in granules strength during the development stage in R3-2.1N and R3-2.1Y	107
Figure 4.13	Change of SV of granules in R1-0.5N and R1-0.5Y	110
Figure 4.14	Change of SV of granules in R2-1.4N and R2-1.4Y	111
Figure 4.15	Change of SV of granules in R3-2.1N and R3-2.1Y	111
Figure 4.16	The variation of SVI for granules in R1-0.5N and R1-0.5Y during the development stage	115
Figure 4.17	The variation of SVI for granules in R2-1.4N and R2-1.4Y during the development stage	116
Figure 4.18	The variation of SVI for granules in R3-2.1N and R3-2.1Y during the development stage	117
Figure 4.19	Granular sludge sizes in R1-0.5N and R1-0.5Y on day 70 of development stage	122
Figure 4.20	Granular sludge sizes in R2-1.4N and R2-1.4Y on day 70 of development stage	124
Figure 4.21	Granular sludge sizes in R3-2.1N and R3-2.1Y on day 70	126
Figure 4.22	Image analysis on the evolution of granular sludge in R1-0.5N and R1-0.5Y throughout 70-days of development stage	129

Figure 4.23	Image analysis on the evolution of granular sludge in R2-1.4N and R2-1.4Y throughout 70-days of development stage	130
Figure 4.24	Image analysis on the evolution of granular sludge in R3-2.1N and R3-2.1Y throughout 70-days of development stage	132
Figure 4.25	Microstructure examination of sludge morphology with a feathery structure and dispersed cocci bacteria using FESEM	134
Figure 4.26	FESEM examinations of biogranules in (a) R1-0.5N (b) R1-0.5Y	135
Figure 4.27	FESEM examinations of biogranules in (a) R2-1.4N (b) R2-1.4Y	136
Figure 4.28	FESEM examinations of biogranules in (a) R3-2.1N (b) R3-2.1Y	137
Figure 4.29	Profile of COD removal efficiency during development stage (a) R1-0.5N and R1-0.5Y (b) R2-1.4N and R2-1.4Y (c) R3-2.1N and R3-2.1Y	139
Figure 4.30	Profile of color removal efficiency during development stage (a) R1-0.5N and R1-0.5Y (b) R2-1.4N and R2-1.4Y (c) R3-2.1N and R3-2.1Y	143
Figure 4.31	Biomass profile of the granules in the system R4N and R4Y	148
Figure 4.32	Strength of the granules in the system R4N and R4Y	150
Figure 4.33	Settling velocity of the granules in R4N and R4Y	151
Figure 4.34	Sludge volume index of the granules in the system R4N and R4Y	153
Figure 4.35	Cocci-shaped bacteria and cavities on the surface of biogranules R4N at HRT of 24 hours	156
Figure 4.36	Cocci-shaped bacteria dominated on the surface of biogranules R4Y at HRT of 24 hours	157
Figure 4.37	Profile of COD removal efficiency of the R4N and R4Y	158
Figure 4.38	Profile of COD removal efficiency of the R4N and R4Y	160
Figure 4.39	Biomass profile of the granules in the system R4N and R4Y	164
Figure 4.40	IC of the granules in the system R4N and R4Y	160

Figure 4.41	Settling velocities of the granules in the system R4N and R4Y	167
Figure 4.42	Sludge volume index of the granules in the system R4N and R4Y	169
Figure 4.43	Biogranule in R4Y at high OLR of 3.0 kg/m ³ .day with smooth surface and regular shape	172
Figure 4.44	FESEM images of granules in R4Y at OLR of 3.0 kg/m ³ .day	173
Figure 4.45	FESEM image of uneven surface of biogranules in R4N at OLR of 3.0 kg/m ³ .day	174
Figure 4.46	Rod-shaped bacteria of granules in R4N at OLR of 3.0 kg/m ³ .day	174
Figure 4.47	Profile of COD removal efficiency of the R4N and R4Y at different OLR	175
Figure 4.48	Profile of color removal efficiency of the R4N and R4Y at different OLR	177
Figure 4.49	OUR profile for reactor R1-0.5N and R1-0.5Y	181
Figure 4.50	OUR profile for reactor R2-1.4N and R2-1.4Y	182
Figure 4.51	OUR profile for reactor R3-2.1N and R3-2.1Y	184

LIST OF ABBREVIATIONS

ADMI	-	American Dye Manufacturing Index
BOD	-	Biochemical oxygen demand
CAS	-	Conventional activated sludge
COD	-	Chemical oxygen demand
DGGE	-	Denaturing gradient gel electrophoresis
DO	-	Dissolved oxygen
EPS	-	Extracellular polymeric substances
FESEM	-	Field emission scanning electron microscope
FISH	-	Fluorescence in situ hybridization
HRT	-	Hydraulic retention time
IC	-	Integrity coefficient
LB-EPS	-	Loosely bound EPS
MLSS	-	Mixed liquor suspended solid
MLVSS	-	Mixed liquor volatile suspended solid
N	-	Nitrogen
NaCl	-	Sodium chloride
NH ₄	-	Ammonia nitrogen
OLR	-	Organic loading rate
OUR	-	Oxygen utilization rate
P	-	Phosphorus
POME	-	Palm oil effluent mill
SAV	-	Superficial air velocity
SBBGR	-	Sequencing batch biofilter granular reactor
SBR	-	Sequencing batch reactor
SEM	-	Scanning electron microscopic
SPSS	-	Statistical Package for Social Sciences
SV	-	Settling velocity
SVI	-	Sludge volume index
TB-EPS	-	Tightly bound EPS
TDS	-	Total dissolved solids

TN	-	Total nitrogen
TP	-	Total phosphorus
TS	-	Total solids
UASB	-	Upflow anaerobic sludge blanket
VER	-	Volume exchange ratio

LIST OF SYMBOLS

k_d	-	Endogenous decay rate
m	-	Mean
P	-	Significance difference
t_c	-	cycle time of SBR operation
V_d	-	manually discharged mixture volume
V_e	-	effluent volume of the SBR operating cycle
V_r	-	working volume of SBR reactor
X_d	-	biomass concentration of manually discharged
X_e	-	effluent volatile solid concentrations
X_{VSS}	-	volatile solid concentration in reactor
Y_{obs}	-	Observed biomass yield
Y	-	Theoretical biomass yield
$\mu_{overall}$	-	Overall specific biomass growth rate
θ_c	-	solid retention time

LIST OF APPENDICES

APPENDIX	TITLE	PAGE
Appendix A	Experimental Data – Development Stage	237
Appendix B	Experimental Data – Post Development Stage at Different HRT	249
Appendix C	Experimental Data – Post Development Stage at Different OLR	257

CHAPTER 1

INTRODUCTION

1.1 Preamble

Water is the most essential requirement for all life but in recent years the availability becoming limited due to the increasing contamination and human activities around the world. According to statistics, currently there are 7.6 billion people living without safe drinking water, two million people die annually due to diarrhoea and about one third of the world's population have poor sanitation systems (Tee et al., 2016). Based on reported cases around the world, water pollution is one of the issues that are becoming serious every year. The main sources of water pollution are not limited to but mainly include industrial and domestic wastewaters. Untreated or improperly treated wastewater which is discharged to the environment pollutes the receiving water and threatens the environment and human health. Hence, various technologies have been developed and used since decades to ensure the wastewater is being properly treated.

During the past hundred years, the conventional activated sludge (CAS) processes have been established in biological wastewater treatment. The first generation of activated sludge systems was built in the 1920's by Ardern and Lockett (De Kreuk & Loosdrecht, 2006). The basic idea behind the CAS system was to reduce the treatment of wastewater to a one-reactor system. Generally, the system consists of an aeration tank in which a mixed culture of suspended biomass is growing. Along with the removal of organic carbon and nutrients from the influent and a settling tank, the treated effluent is separated from the biomass (Metcalf & Eddy, 2003). Conventional activated sludge process produce surplus sludge. Part of the settled activated sludge is recycled to the aeration tank and the remainder is usually treated and later disposed or used as fertilizer. One of the major drawback of CAS is the poor solid-liquid separation between biomass and the treated effluent

(Gobi, Mashitah, & Vadivelu, 2011). To be specific, this treatment plants generally require large surface area in order to provide large aeration tanks. In fact as the available ground area to build the treatment plant is limited especially in dense populated regions, there is a need for a more compact treatment. According to (de Bruin, de Kreuk, van der Roest, Uijterlinde, & van Loosdrecht, 2004), this need directed to the development of systems based on biogranulation technology which is an alternative to the existing technology, as the footprint of this technology is only 25% compared to that of the CAS.

Biogranulation technology is considered as one of the novel advanced biological treatment technologies developed for wastewater treatment. Biogranulation process involves cell-to-cell attachment in which granules are formed through self-immobilization of microorganisms. As compared to CAS flocs, biogranules are dense, compact and has strong structure with good settling properties. Biogranulation is a complex process with many factors affecting the structure and composition of the granules. Biogranulation for methanogenic sludge was first reported by Lettinga, van Velsen, Hobma, de Zeeuw, & Klapwijk, (1980) where biogranules were formed in upflow anaerobic sludge blanket (UASB) reactors. However it exhibits several drawbacks, which include the need of a long start-up period, a relatively high operating temperature, incapability to treat low strength organic wastewater and less efficient in removing nutrients from the wastewater (Adav, Lee, Show, & Tay, 2008). Mishima and Nakamura (1991) began a study on aerobic granulation to overcome these weaknesses.

Most aerobic granules have been cultured in sequencing batch reactors (SBRs). Sequencing batch reactors is a fill and draw activated sludge system where the suspended biomass is grown to remove organics and nutrients from the influent. Sequencing batch reactors saves more than 60% of the expenses required for conventionally activated sludge process in terms of operating cost and in achieving high effluent quality within a very short aeration time (Singh & Srivastava, 2011). The system is a repetitive system, which basically comprises of filling, reaction, settling, decanting and idling within a single bioreactor.

Several conditions such as organic loading rate (OLR), composition of substrate, settling time, hydraulic retention time (HRT), reactor configuration, volume exchange ratio (VER), mineral cations, cell hydrophobicity, extracellular polymeric substances (EPS), dissolved oxygen and hydrodynamic shear force affect the formation of the granules. One of the most influencing factors that have received consideration is the hydrodynamic shear force, quantified by superficial air velocity (SAV). The general agreement is that high shear force forms compact and dense granules. High shear force encourages bacteria to produce more EPS that contribute to the cells attachments and maintain the microorganisms structure (Liu, Liu, Wang, Yang, & Tay, 2005). In addition, the high detachment force resulted from the high hydrodynamic shear force can further shape aggregate surface forming dense and smooth granules (Chen, Jiang, Liang, & Tay, 2007), which also leads to stronger and smaller aerobic granules (Tay, Liu, & Liu, 2004). Hydrodynamic shear force has been proven to have a significance influence to the formation of compact, stable and dense aerobic granules (Liu & Tay, 2002).

In most of the earlier studies, it has been observed that hydrodynamic shear force in terms of SAV used in reactor was found to be much higher than 1.2 cm/s; therefore, high aeration rate is necessary to ensure the granular sludge formation and successful of the granulation process. Beun et al. (1999) reported that at high SAV of 4.1 cm/s, smooth granules were formed whereas at lower SAV of 1.4 cm/s and 2.0 cm/s, loose and poor settling ability of granules were developed. Tay, Liu and Liu, (2001) also found that regular, rounder and more compact granules could be formed at SAV of above 1.2 cm/s only. Sturm and Irvine (2008) observed that granules disintegrated into flocs when SAV was lower than 1.0 cm/s. Chen, Jiang, Liang and Tay (2008) reported that a high SAV of 3.2 cm/s was used to develop stable granules with good settling properties. In another study, Lochmatter, Gonzalez-Gil, & Holliger (2013) applied air velocities of 2.1 to 2.8 cm/s to obtain stable granules. Lochmatter and Holliger (2014) also carried out an experiment at SAV of 2.8 cm/s and proved biogranulation process reliability under high shear force. However, in more recent studies, different observations were reported. Henriot, Meunier, Henry, and Mahillon (2016) observed that under low SAV of 0.42 cm/s, stable granules could be obtained using SBR in treating acetate. Additionally, Devlin, di Biase,

Kowalski & Oleszkiewicz, (2016) successfully developed stable granules treating low-strength wastewater under SAV of 0.41 cm/s.

1.2 Problem Statement

Hydrodynamic shear force was proven to be one of the significant factors for the stability of biogranules. There have been number of attempts to develop strategies for improving the biogranulation process. Experimental evidences show that a wide range of SAVs has been successfully used to develop the biogranules. Different SAVs from as low as 0.41 cm/s to 3.4 cm/s were experimented by different researchers to find the best conditions for the biogranulation. A high SAV increases the attrition of granules and shifts granule size distribution towards smaller size but with higher density, however, a relatively low SAV favors the growth of granules size but with lower density. One of the challenges in the biogranulation process in providing the optimum SAV is cost. Such SAVs normally require high aeration rates which results in high energy consumption and eventually operational cost. Producing hydrodynamic shear force at lower SAV is a challenge and should be the way forward. Therefore, a strategy to favor the granules development and enhance the performance of biogranulation process is worthy to explore. Apparently, no study has been carried out on the use of static mixer in enhancing the hydrodynamic shear force. In this study, a static mixer was introduced in the reactor to enhance the hydrodynamic shear force even at low SAV. Static mixer provides well-mixed condition as it is very important in the process. The main objective of this work was to study the effect of static mixer combination with low SAV in the reactor on the properties of developed biogranules and reactor performance. The findings would provide a cheaper promising alternative for aerobic biogranulation system.

Different operational strategies have led to the different biogranules characteristics and removal performance. Hydraulic retention time is an important parameter that controls the contact time between biomass and the wastewater in a reactor system. The range of HRT among the previous studies was 1 to 36 hours. Liu, Moy & Tay, (2007) reported that granules were formed within 16 days under

HRT of 3 hours while it took 21 days under HRT of 16 hours. Pan, Tay, He, and Tay (2004) claimed that an HRT of 6 hours is most appropriate for biogranulation since the granules possessed higher cell hydrophobicity. A short HRT is favorable for rapid granulation process while too long HRT may cause the disintegration of the granules and lead to granulation system failure (Liu & Tay, 2015). Therefore, choice of HRT is very important in biogranulation process.

Organic loading rate is another crucial factor in any biological system. It was reported in many previous study that aerobic granules was able to withstand OLR range 2.5 to 15 kg/m³.day. The low OLR probably did not enhance the granulation as many researchers have pointed out (Liu & Tay, 2015; Nguyen, Van Nguyen, Truong, & Bui, 2016). A moderate OLR was found to favor the development of stable aerobic granules (Tay, Pan, He, Tiong, & Tay, 2004). It has been reported that high OLR is beneficial for accumulating biomass by secreting more EPS. However, Long et al., (2015) demonstrate that aerobic granules disintegrated and eventually led to the collapse of the aerobic granule system when OLR increased to 18 kg/m³.day. As observed from the experiment, disintegration of AGS mainly ascribed to instability of granule's inner core. Additionally, study on evaluating the effect of static mixer under influence of different HRTs and OLRs in the biogranulation system has never been reported. Thus, this study sought to investigate the effects of granules properties and reactor performance under combination of various HRTs and OLRs with the addition of static mixer into the reactor system. Moreover, kinetics study on aerobic granule growth at the steady state is also carried out to correlate sludge production, sludge growth, and sludge retention time with HRT and OLR.

1.3 Objectives of Study

The main aim of this study is to enhance the biogranulation treatment in terms of energy requirement and characteristics of the biogranules with the use of static mixer. Hence, the objectives of the study are as follows:

1. To design and identify a suitable static mixer based on mixing intensity study.

2. To investigate the development of aerobic granules and their performance in treating synthetic textile wastewater in the SBR under different SAVs and influence of static mixer.
3. To evaluate the effect of static mixer on the properties and performance of aerobic granules under different HRTs and OLRs.
4. To determine the biokinetic properties of the SBR system under different HRTs and OLRs

1.4 Scope of Study

This study was carried out using a lab-scale SBR system under intermittent anaerobic and aerobic phase. A glass column with a working volume of 1.5L was used. Synthetic wastewater was used as the feed influent and the seed sludge was obtained from Taman Harmoni IWK Sewage Treatment Plant (STP). Four types of static mixers were designed and custom-made to suit the laboratory-scale reactor system. In this study, two stages of experimental works were involved which are the development and the post-development stage. The SAVs of 0.5, 1.4 and 2.1 cm/s have been applied during the development stage while HRT and OLR were set at 8 hours and 2.0 kg/m³.day, respectively. Samples of granules were collected and examined for their morphology and physical properties such as mixed liquor suspended solid (MLSS), sludge volume index (SVI), settling velocity (SV) and integrity coefficient (IC). The formed granules were also tested for performance in treating textile wastewater in terms of chemical oxygen demand (COD) and color removal. The effects of HRT and OLR on the performance of biogranules were investigated in post-development stage. Furthermore, the relationship between the biokinetic parameters at different HRT and OLR were also explored. Statistical analysis was performed using Statistical Package for Social Sciences (SPSS) 21 to determine the significant difference between reactor with and without static mixer.

1.5 Significance of Study

Previous studies have proven that hydrodynamic shear force has a significant effect on the formation and stability of aerobic granules (Tay et al., 2001; Liu & Tay, 2002; Chen et al., 2008; Lochmatter et al., 2013; Devlin et al., 2016). The hydrodynamic shear force triggers the production of EPS, which is important in bacterial cells attachment. A high hydrodynamic shear force generally needs big amounts of energy, which raises the applications cost. Therefore, a static mixer was added to the reactor to enhance the shear force at low SAV. Apparently, the influence of static mixer in manipulating the hydrodynamic shear force in the process of aerobic granules development has not been studied. Several significant contributions of this study are identified as follows:

- i. Hydrodynamic shear force is one the most influencing factor in biogranulation. This study is regarded as the pioneer study on the influence of static mixer in manipulating the hydrodynamic shear force to develop the biogranules treating textile wastewater.
- ii. This study provides the suitable SAVs together with static mixer for developing aerobic granules especially for degradation of textile wastewater.
- iii. This study contributes to the knowledge of the properties of biogranules under influence of static mixer.
- iv. Aerobic granules are known to have strong and dense microstructure and ability to withstand high OLRs. This study provides information on the effect of various HRT and OLR to the profile of aerobic granules under influence of static mixer.
- v. For the design and operation of aerobic granular system for biological treatment process, the underlying biological growth kinetics is important to be understood. This study provides the kinetics of biomass growth parameters including overall specific biomass growth rate ($\mu_{overall}$), endogenous decay

rate (k_d), observed biomass yield (Y_{obs}) and theoretical biomass yield (Y), which followed the Monod's model.

1.6 Thesis Organization

The thesis is organised into five chapters. Chapter 1 introduces the application of biogranulation technology in wastewater treatment. This chapter also provides an overview on the factors affecting the performance of biogranulation technology. It also presents the statement of research problems, research objectives and significance of the study.

Chapter 2 is dedicated for the literature reviews on the background of biogranulation technology, factors affecting the process and application of the technology. The basic principles of biogranulation technology which include the theory of granulation process and various application of biogranulation technology in treating different types of wastewater are also highlighted. A review of previous studies in the related topics is also given in this chapter.

Chapter 3 explains the methodology used in the study. This chapter details out the laboratory materials and equipment, analytical method as well as experimental procedures including wastewater feed and seed sludge used throughout the study. The reactor description, operational strategies are also illustrated in details in this chapter.

Chapter 4 reports and discusses the results obtained from the study, which include the findings during the development stage and post-development stage of the aerobic granules. Finally, Chapter 5 summarizes the conclusions of the findings from this study, embracing the specific achievement and recommendations for the future studies. General conclusions are also drawn based on the outcomes and experiences gained throughout the study.

REFERENCES

- Ab Halim, M. H., Nor Anuar, A., Abdul Jamal, N. S., Azmi, S. I., Ujang, Z., & Bob, M. M. (2016). Influence of high temperature on the performance of aerobic granular sludge in biological treatment of wastewater. *Journal of Environmental Management*, *184*, 271–280. <https://doi.org/10.1016/j.jenvman.2016.09.079>
- Ab Halim, M. H., Nor Anuar, A., Azmi, S. I., Jamal, N. S. A., Wahab, N. A., Ujang, Z., ... Bob, M. M. (2015). Aerobic sludge granulation at high temperatures for domestic wastewater treatment. *Bioresource Technology*, *185*, 445–449. <https://doi.org/10.1016/j.biortech.2015.03.024>
- Abdullah, N., Ujang, Z., & Yahya, A. (2011). Aerobic granular sludge formation for high strength agro-based wastewater treatment. *Bioresource Technology*, *102*(12), 6778–6781. <https://doi.org/10.1016/j.biortech.2011.04.009>
- Abdullah, N., Yuzir, A., Curtis, T. P., Yahya, A., & Ujang, Z. (2013). Characterization of aerobic granular sludge treating high strength agro-based wastewater at different volumetric loadings. *Bioresource Technology*, *127*, 181–187. <https://doi.org/10.1016/j.biortech.2012.09.047>
- Abou Hweij, K., & Azizi, F. (2015). Hydrodynamics and residence time distribution of liquid flow in tubular reactors equipped with screen-type static mixers. *Chemical Engineering Journal*, *279*, 948–963. <https://doi.org/10.1016/j.cej.2015.05.100>
- Adav, S. S., Lee, D.J., & Lai, J.Y. (2009). Aerobic granulation in sequencing batch reactors at different settling times. *Bioresource Technology*, *100*(21), 5359–5361. <https://doi.org/10.1016/j.biortech.2009.05.058>
- Adav, S. S., Lee, D.J., & Lai, J.Y. (2010). Potential cause of aerobic granular sludge breakdown at high organic loading rates. *Applied Microbiology and Biotechnology*, *85*(5), 1601–1610. <https://doi.org/10.1007/s00253-009-2317-9>
- Adav, S. S., Lee, D.J., & Lai, J. Y. (2007). Effects of aeration intensity on formation

- of phenol-fed aerobic granules and extracellular polymeric substances. *Applied Microbiology and Biotechnology*, 77(1), 175–182. <https://doi.org/10.1007/s00253-007-1125-3>
- Adav, S. S., Lee, D.J., Show, K.Y., & Tay, J.H. (2008). Aerobic granular sludge: recent advances. *Biotechnology Advances*, 26(5), 411–423. <https://doi.org/10.1016/j.biotechadv.2008.05.002>
- Adav, S. S., Lee, D.J., & Tay, J.H. (2008). Extracellular polymeric substances and structural stability of aerobic granule. *Water Research*, 42(6–7), 1644–1650. <https://doi.org/10.1016/j.watres.2007.10.013>
- Ahmad, A., Mohd-Setapar, S. H., Chuong, C. S., Khatoon, A., Wani, W. A., Kumar, R., & Rafatullah, M. (2015). Recent advances in new generation dye removal technologies: Novel search for approaches to reprocess wastewater. *RSC Advances*, 5(39), 30801–30818. <https://doi.org/10.1039/c4ra16959j>
- Al-busafi, A., Al-harrasi, B., Al-shidhani, I., & Al-dallal, A. J. A. (2016). Study on Mixing Time and Gas Hold-up in an Airlift Bioreactor, (September).
- Al-Malack, M. H. (2006). Determination of biokinetic coefficients of an immersed membrane bioreactor. *Journal of Membrane Science*, 271(1–2), 47–58. <https://doi.org/10.1016/j.memsci.2005.07.008>
- Anderson, P., & Meijer, H. E. H. (2000). Chaotic mixing analysis by distribution matrices. *Applied Rheology*, 10(3), 119–133.
- André, C., Demeyre, J. F., Gatumel, C., Berthiaux, H., & Delaplace, G. (2012). Dimensional analysis of a planetary mixer for homogenizing of free flowing powders: Mixing time and power consumption. *Chemical Engineering Journal*, 198–199, 371–378. <https://doi.org/10.1016/j.cej.2012.05.069>
- Arrojo, B., Mosquera-Corral, A., Garrido, J. M., & Méndez, R. (2004). Aerobic granulation with industrial wastewater in sequencing batch reactors. *Water Research*, 38(14–15), 3389–3399. <https://doi.org/10.1016/j.watres.2004.05.002>
- Awomeso, J. A., Taiwo, A. M., Gbadebo, A. M., & Arimoro, A. O. (2010). Waste

- disposal and pollution management in urban areas: A workable remedy for the environment in developing countries. *American Journal of Environmental Sciences*, 6(1), 26–32. <https://doi.org/10.3844/ajessp.2010.26.32>
- Banerjee, P., Sau, S., Das, P., & Mukhopadhyay, A. (2015). Optimization and modelling of synthetic azo dye wastewater treatment using Graphene oxide nanoplatelets: Characterization toxicity evaluation and optimization using Artificial Neural Network. *Ecotoxicology and Environmental Safety*, 119, 47–57. <https://doi.org/10.1016/j.ecoenv.2015.04.022>
- Bashiri, B., Fallah, N., Bonakdarpour, B., & Elyasi, S. (2018). The development of aerobic granules from slaughterhouse wastewater in treating real dyeing wastewater by Sequencing Batch Reactor (SBR). *Journal of Environmental Chemical Engineering*, 6(4), 5536–5543. <https://doi.org/10.1016/j.jece.2018.05.020>
- Bassin, J. P., Pronk, M., Kraan, R., Kleerebezem, R., & Van Loosdrecht, M. C. M. (2011). Ammonium adsorption in aerobic granular sludge, activated sludge and anammox granules. *Water Research*, 45(16), 5257–5265. <https://doi.org/10.1016/j.watres.2011.07.034>
- Bauman, I. (2001). Solid-solid mixing with static mixers. *Chemical and Biochemical Engineering Quarterly*, 15(4), 159–165. Retrieved from <http://www.scopus.com/inward/record.url?eid=2-s2.0-0035699694&partnerID=tZOtx3y1>
- Beun, J. ., Hendriks, a, van Loosdrecht, M. C. ., Morgenroth, E., Wilderer, P. ., & Heijnen, J. . (1999). Aerobic granulation in a sequencing batch reactor. *Water Research*, 33(10), 2283–2290. [https://doi.org/10.1016/S0043-1354\(98\)00463-1](https://doi.org/10.1016/S0043-1354(98)00463-1)
- Beun, J. J., van Loosdrecht, M. C. M., & Heijnen, J. J. (2002). Aerobic granulation in a sequencing batch airlift reactor. *Water Research*, 36(3), 702–712. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/11831218>
- Bilińska, L., Gmurek, M., & Ledakowicz, S. (2016). Comparison between industrial and simulated textile wastewater treatment by AOPs – Biodegradability, toxicity and cost assessment. *Chemical Engineering Journal*, 306, 550–559.

<https://doi.org/10.1016/j.cej.2016.07.100>

- Bindhu, B. K., & Madhu, G. (2013). Influence of Organic Loading Rates on Aerobic Granulation Process for the Treatment of Wastewater. *Journal of Clean Energy Technologies*, 1(2), 84–87. <https://doi.org/10.7763/JOCET.2013.V1.20>
- Bindhu, B. K., & Madhu, G. (2015). Influence of three selection pressures on aerobic granulation in sequencing batch reactor, 22(September), 241–247.
- Bindhu, B. K., & Madhu, G. (2017). Application of grey system theory on the influencing parameters of aerobic granulation in SBR. *Environmental Technology (United Kingdom)*, 38(17), 2143–2152. <https://doi.org/10.1080/09593330.2016.1246617>
- Bonvillani, P., Ferrari, M. P., Ducros, E. M., & Orejas, J. A. (2006). Theoretical and experimental study of the effects of scale-up on mixing time for a stirred-tank bioreactor. *Brazilian Journal of Chemical Engineering*, 23(1), 1–7. <https://doi.org/10.1590/S0104-66322006000100001>
- Bren, A., Hart, Y., Dekel, E., Koster, D., & Alon, U. (2013). The last generation of bacterial growth in limiting nutrient. *BMC Systems Biology*, 7(1), 27. <https://doi.org/10.1186/1752-0509-7-27>
- Brillas, E., & Martínez-Huitle, C. A. (2015). Decontamination of wastewaters containing synthetic organic dyes by electrochemical methods. An updated review. *Applied Catalysis B: Environmental*, 166–167, 603–643. <https://doi.org/10.1016/j.apcatb.2014.11.016>
- Bumbac, C., Ionescu, I. A., Tiron, O., & Badescu, V. R. (2015). Continuous flow aerobic granular sludge reactor for dairy wastewater treatment. *Water Science and Technology*, 71(3), 440–445. <https://doi.org/10.2166/wst.2015.007>
- Caluwé, M., Dobbeleers, T., D'aes, J., Miele, S., Akkermans, V., Daens, D., ... Dries, J. (2017). Formation of aerobic granular sludge during the treatment of petrochemical wastewater. *Bioresource Technology*, 238, 559–567. <https://doi.org/10.1016/j.biortech.2017.04.068>

- Campo, R., Corsino, S. F., Torregrossa, M., & Di Bella, G. (2018). The role of extracellular polymeric substances on aerobic granulation with stepwise increase of salinity. *Separation and Purification Technology*, 195(August 2017), 12–20. <https://doi.org/10.1016/j.seppur.2017.11.074>
- Campos, J. L., Figueroa, M., & Ri, A. V. (2011). Treatment of high loaded swine slurry in an aerobic granular reactor, 1808–1814. <https://doi.org/10.2166/wst.2011.381>
- Campos, J. L., Garrido-Fernández, J. M., Méndez, R., & Lema, J. M. (1999). Nitrification at high ammonia loading rates in an activated sludge unit. *Bioresource Technology*, 68(2), 141–148. [https://doi.org/10.1016/S0960-8524\(98\)00141-2](https://doi.org/10.1016/S0960-8524(98)00141-2)
- Cardoso, J. C., Bessegato, G. G., & Boldrin Zanoni, M. V. (2016). Efficiency comparison of ozonation, photolysis, photocatalysis and photoelectrocatalysis methods in real textile wastewater decolorization. *Water Research*, 98, 39–46. <https://doi.org/10.1016/j.watres.2016.04.004>
- Carneiro, P. A., Umbuzeiro, G. A., Oliveira, D. P., & Zanoni, M. V. B. (2010). Assessment of water contamination caused by a mutagenic textile effluent/dyehouse effluent bearing disperse dyes. *Journal of Hazardous Materials*, 174(1–3), 694–699. <https://doi.org/10.1016/j.jhazmat.2009.09.106>
- Caşcaval, D., Matran, R. M., Turnea, M., Blaga, A. C., & Galaction, A. I. (2015). Distribution of mixing efficiency in a split-cylinder gas-lift bioreactor for *Yarrowia lipolytica* suspensions. *The Canadian Journal of Chemical Engineering*, 93(1), 18–28. <https://doi.org/10.1002/cjce.22107>
- Cassidy, D. P., & Belia, E. (2005). Nitrogen and phosphorus removal from an abattoir wastewater in a SBR with aerobic granular sludge. *Water Research*, 39(19), 4817–4823. <https://doi.org/10.1016/j.watres.2005.09.025>
- Caudan, C., Filali, A., Spérandio, M., & Girbal-Neuhauser, E. (2014). Multiple EPS interactions involved in the cohesion and structure of aerobic granules. *Chemosphere*, 117(1), 262–270. <https://doi.org/10.1016/j.chemosphere.2014.07.020>

- Cetin, E., Karakas, E., Dulekgurgen, E., Ovez, S., Kolukirik, M., & Yilmaz, G. (2018). Effects of high-concentration influent suspended solids on aerobic granulation in pilot-scale sequencing batch reactors treating real domestic wastewater. *Water Research*, *131*, 74–89. <https://doi.org/10.1016/j.watres.2017.12.014>
- Chen, C., Ming, J., Yoza, B. A., Liang, J., Li, Q. X., Guo, H., ... Wang, Q. (2019). Characterization of aerobic granular sludge used for the treatment of petroleum wastewater. *Bioresource Technology*, *271*(September 2018), 353–359. <https://doi.org/10.1016/j.biortech.2018.09.132>
- Chen, F., Liu, Y., & Tay, J. (2015). Rapid formation of nitrifying granules treating high-strength ammonium wastewater in a sequencing batch reactor. <https://doi.org/10.1007/s00253-014-6363-6>
- Chen, Y., Jiang, W., Liang, D. T., & Tay, J. H. (2007). Structure and stability of aerobic granules cultivated under different shear force in sequencing batch reactors. *Applied Microbiology and Biotechnology*, *76*(5), 1199–1208. <https://doi.org/10.1007/s00253-007-1085-7>
- Chen, Y., Jiang, W., Liang, D. T., & Tay, J. H. (2008). Aerobic granulation under the combined hydraulic and loading selection pressures. *Bioresource Technology*, *99*(16), 7444–7449. <https://doi.org/10.1016/j.biortech.2008.02.028>
- Chiu, Z. C., Chen, M. Y., Lee, D. J., Tay, S. T., Tay, J. H., & Show, K. Y. (2006). Diffusivity of Oxygen in Aerobic Granules, (3). <https://doi.org/10.1002/bit>
- Coma, M., Verawaty, M., Pijuan, M., Yuan, Z., & Bond, P. L. (2012). Enhancing aerobic granulation for biological nutrient removal from domestic wastewater. *Bioresource Technology*, *103*(1), 101–108. <https://doi.org/10.1016/j.biortech.2011.10.014>
- Corsino, S. F., di Biase, A., Devlin, T. R., Munz, G., Torregrossa, M., & Oleszkiewicz, J. A. (2016). Effect of Extended Famine Conditions on Aerobic Granular Sludge Stability in the Treatment of Brewery Wastewater. *Bioresource Technology*, *226*, 150–157. <https://doi.org/10.1016/j.biortech.2016.12.026>

- Corsino, S. F., Di Trapani, D., Torregrossa, M., & Viviani, G. (2018). Aerobic granular sludge treating high strength citrus wastewater: Analysis of pH and organic loading rate effect on kinetics, performance and stability. *Journal of Environmental Management*, *214*, 23–35. <https://doi.org/10.1016/j.jenvman.2018.02.087>
- Couto, C. F., Moravia, W. G., & Amaral, M. C. S. (2017). Integration of microfiltration and nanofiltration to promote textile effluent reuse. *Clean Technologies and Environmental Policy*, *19*(8), 2057–2073. <https://doi.org/10.1007/s10098-017-1388-z>
- Cui, F., Park, S., & Kim, M. (2014). Bioresource Technology Characteristics of aerobic granulation at mesophilic temperatures in wastewater treatment. *Bioresource Technology*, *151*, 78–84. <https://doi.org/10.1016/j.biortech.2013.10.025>
- Dangcong, P., Bernet, N., Delgenes, J., & Moletta, R. (1999). Rapid Communication Aerobic Granular Sludge - A Case Report, *33*(3), 890–893.
- de Bruin, L. M. M., de Kreuk, M. K., van der Roest, H. F. R., Uijterlinde, C., & van Loosdrecht, M. C. M. (2004). Aerobic granular sludge technology: an alternative to activated sludge? *Water Science and Technology: A Journal of the International Association on Water Pollution Research*, *49*(11–12), 1–7. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/15303716>
- de Kreuk, M K, Pronk, M., & van Loosdrecht, M. C. M. (2005). Formation of aerobic granules and conversion processes in an aerobic granular sludge reactor at moderate and low temperatures. *Water Research*, *39*(18), 4476–4484. <https://doi.org/10.1016/j.watres.2005.08.031>
- Deng, S., Wang, L., & Su, H. (2016). Role and influence of extracellular polymeric substances on the preparation of aerobic granular sludge. *Journal of Environmental Management*, *173*, 49–54. <https://doi.org/10.1016/j.jenvman.2016.03.008>
- Devlin, T. R., di Biase, A., Kowalski, M., & Oleszkiewicz, J. A. (2016). Granulation of activated sludge under low hydrodynamic shear and different wastewater

- characteristics. *Bioresource Technology*, 224, 1–7.
<https://doi.org/10.1016/j.biortech.2016.11.005>
- Di Bella, G., & Torregrossa, M. (2014). Aerobic Granular Sludge for Leachate Treatment. *Chemical Engineering Transactions*, 38, 493–498.
<https://doi.org/10.3303/CET1438083>
- Di Iaconi, C., Ramadori, R., Lopez, A., & Passino, R. (2006). Influence of hydrodynamic shear forces on properties of granular biomass in a sequencing batch biofilter reactor. *Biochemical Engineering Journal*, 30(2), 152–157.
<https://doi.org/10.1016/j.bej.2006.03.002>
- Dobbeleers, T., Daens, D., Miele, S., D'aes, J., Caluwé, M., Geuens, L., & Dries, J. (2017). Performance of aerobic nitrite granules treating an anaerobic pre-treated wastewater originating from the potato industry. *Bioresource Technology*, 226.
<https://doi.org/10.1016/j.biortech.2016.11.117>
- Dong, C., & Lv, B. (2018). Granulation for Coking Wastewater Treatment in a Coupled Anaerobic-Aerobic Reactor, *01052*, 1–6.
- dos Santos, A. B., Cervantes, F. J., & van Lier, J. B. (2007). Review paper on current technologies for decolourisation of textile wastewaters: Perspectives for anaerobic biotechnology. *Bioresource Technology*, 98(12), 2369–2385.
<https://doi.org/10.1016/j.biortech.2006.11.013>
- Eom, H., Kim, J., Kim, S., & Lee, S.-S. (2018). Treatment of Saline Wastewater Containing a High Concentration of Salt Using Marine Bacteria and Aerobic Granule Sludge. *Journal of Environmental Engineering (United States)*, 144(5), 1–8. [https://doi.org/10.1016/S0143-974X\(01\)00044-X](https://doi.org/10.1016/S0143-974X(01)00044-X)
- Ergüder, T. H., & Demirer, G. N. (2005). Investigation of granulation of a mixture of suspended anaerobic and aerobic cultures under alternating anaerobic/microaerobic/aerobic conditions. *Process Biochemistry*, 40(12), 3732–3741. <https://doi.org/10.1016/j.procbio.2005.05.005>
- Etterer, T., & Wilderer, P. a. (2001). Generation and properties of aerobic granular sludge. *Water Science and Technology: A Journal of the International*

- treating a low-strength wastewater. *Chemical Engineering Journal*, 198–199, 163–170. <https://doi.org/10.1016/j.cej.2012.05.066>
- Jegatheesan, V., Pramanik, B. K., Chen, J., Navaratna, D., Chang, C. Y., & Shu, L. (2016). Treatment of textile wastewater with membrane bioreactor: A critical review. *Bioresource Technology*, 204, 202–212. <https://doi.org/10.1016/j.biortech.2016.01.006>
- Ji, G., Zhai, F., Wang, R., & Ni, J. (2010). Sludge granulation and performance of a low superficial gas velocity sequencing batch reactor (SBR) in the treatment of prepared sanitary wastewater. *Bioresource Technology*, 101(23), 9058–9064. <https://doi.org/10.1016/j.biortech.2010.07.045>
- Ji, M., Wei, Y., Lu, S., Wang, F., & Cheng, L. (2009). Characteristics and Stability of Aerobic Granules Treating Domestic Sewage. *2009 3rd International Conference on Bioinformatics and Biomedical Engineering*, 1–5. <https://doi.org/10.1109/ICBBE.2009.5162490>
- Jiang, H. L., Tay, J. H., Maszenan, A. M., & Tay, S. T. L. (2004). Bacterial diversity and function of aerobic granules engineered in a sequencing batch reactor for phenol degradation. *Applied and Environmental Microbiology*, 70(11), 6767. <https://doi.org/10.1128/AEM.70.11.6767>
- Jiang, H. L., Tay, J. H., & Tay, S. T. L. (2002). Aggregation of immobilized activated sludge cells into aerobically grown microbial granules for the aerobic biodegradation of phenol. *Letters in Applied Microbiology*, 35(5), 439–445. <https://doi.org/10.1046/j.1472-765X.2002.01217.x>
- Jiang, Y., Wei, L., Yang, K., & Wang, H. (2019). Investigation of rapid granulation in SBRs treating aniline-rich wastewater with different aniline loading rates. *Science of the Total Environment*, 646, 841–849. <https://doi.org/10.1016/j.scitotenv.2018.07.313>
- Kang, A. J., & Yuan, Q. (2017). Long-term Stability and Nutrient Removal Efficiency of Aerobic Granules at Low Organic Loads. *Bioresource Technology*, 234, 336–342. <https://doi.org/10.1016/j.biortech.2017.03.057>

- Kant, R. (2012). Textile dyeing industry an environmental hazard, *4*(1), 22–26.
- Kapdan, I. K., & Ozturk, R. (2005). Effect of operating parameters on color and COD removal performance of SBR: Sludge age and initial dyestuff concentration. *Journal of Hazardous Materials*, *123*(1–3), 217–222. <https://doi.org/10.1016/j.jhazmat.2005.04.013>
- Khan, T. A., Nazir, M., & Khan, E. A. (2013). Adsorptive removal of rhodamine B from textile wastewater using water chestnut (*Trapa natans* L.) peel: Adsorption dynamics and kinetic studies. *Toxicological and Environmental Chemistry*, *95*(6), 919–931. <https://doi.org/10.1080/02772248.2013.840369>
- Khan, T. A., Rahman, R., Ali, I., Khan, E. A., & Mukhlif, A. A. (2014). Removal of malachite green from aqueous solution using waste pea shells as low-cost adsorbent – adsorption isotherms and dynamics. *Toxicological and Environmental Chemistry*, *96*(4), 569–578. <https://doi.org/10.1080/02772248.2014.969268>
- Kim, I. S., Kim, S.-M., & Jang, A. (2008). Characterization of aerobic granules by microbial density at different COD loading rates. *Bioresource Technology*, *99*(1), 18–25. <https://doi.org/10.1016/j.biortech.2006.11.058>
- Konopacki, M., Kordas, M., Fijałkowski, K., & Rakoczy, R. (2015). Computational Fluid Dynamics and Experimental Studies of a New Mixing Element in a Static Mixer as a Heat Exchanger. *Chemical and Process Engineering*, *36*(1), 59–72. <https://doi.org/10.1515/cpe-2015-0005>
- Kreuk, Merle K De, & Loosdrecht, M. C. M. Van. (2006). Formation of Aerobic Granules with Domestic Sewage, (June), 694–697.
- Kumar, K., Singh, G. K., Dastidar, M. G., & Sreekrishnan, T. R. (2014). Effect of mixed liquor volatile suspended solids (MLVSS) and hydraulic retention time (HRT) on the performance of activated sludge process during the biotreatment of real textile wastewater. *Water Resources and Industry*, *5*, 1–8. <https://doi.org/10.1016/j.wri.2014.01.001>
- Kwok, W. K., Picioreanu, C., Ong, S. L., Van Loosdrecht, M. C. M., Ng, W. J., &

- Heijnen, J. J. (1998). Influence of biomass production and detachment forces on biofilm structures in a biofilm airlift suspension reactor. *Biotechnology and Bioengineering*, 58(4), 400–407. [https://doi.org/10.1002/\(SICI\)1097-0290\(19980520\)58:4<400::AID-BIT7>3.0.CO;2-N](https://doi.org/10.1002/(SICI)1097-0290(19980520)58:4<400::AID-BIT7>3.0.CO;2-N)
- Lashkarizadeh, M., Munz, G., & Oleszkiewicz, J. A. (2016). Impacts of variable pH on stability and nutrient removal efficiency of aerobic granular sludge. *Water Science and Technology*, 73(1), 60–68. <https://doi.org/10.2166/wst.2015.460>
- Lee, D. J., Chen, Y. Y., Show, K. Y., Whiteley, C. G., & Tay, J. H. (2010). Advances in aerobic granule formation and granule stability in the course of storage and reactor operation. *Biotechnology Advances*, 28(6), 919–934. <https://doi.org/10.1016/j.biotechadv.2010.08.007>
- Lemaire, R., Yuan, Z., Blackall, L. L., & Crocetti, G. R. (2008). Microbial distribution of *Accumulibacter* spp. and *Competibacter* spp. in aerobic granules from a lab-scale biological nutrient removal system. *Environmental Microbiology*, 10(2), 354–363. <https://doi.org/10.1111/j.1462-2920.2007.01456.x>
- Lettinga, G., van Velsen, A. F. M., Hobma, S. W., de Zeeuw, W., & Klapwijk, A. (1980). Use of the upflow sludge blanket (USB) reactor concept for biological wastewater treatment, especially for anaerobic treatment. *Biotechnology and Bioengineering*, 22(4), 699–734. <https://doi.org/10.1002/bit.260220402>
- Li, A., Yang, S., Li, X., & Gu, J. (2008). Microbial population dynamics during aerobic sludge granulation at different organic loading rates, 42, 3552–3560. <https://doi.org/10.1016/j.watres.2008.05.005>
- Li, A., Zhang, T., & Li, X. (2010). Fate of aerobic bacterial granules with fungal contamination under different organic loading conditions. *Chemosphere*, 78(5), 500–509. <https://doi.org/10.1016/j.chemosphere.2009.11.040>
- Li, D., Lv, Y., Cao, M., Zeng, H., & Zhang, J. (2016). Optimized hydraulic retention time for phosphorus and COD removal from synthetic domestic sewage with granules in a continuous-flow reactor. *Bioresource Technology*, 216, 1083–1087. <https://doi.org/10.1016/j.biortech.2016.05.061>

- Li, J., Ding, L., Cai, A., Huang, G., & Horn, H. (2014). Aerobic Sludge Granulation in a Full-Scale Sequencing Batch Reactor, *2014*.
- Li, X. Y., & Yuan, Y. (2002). Settling velocities and permeabilities of microbial aggregates. *Water Research*, *36*(12), 3110–3120. [https://doi.org/10.1016/S0043-1354\(01\)00541-3](https://doi.org/10.1016/S0043-1354(01)00541-3)
- Li, Y., Liu, Y., Shen, L., & Chen, F. (2008). DO diffusion profile in aerobic granule and its microbiological implications. *Enzyme and Microbial Technology*, *43*(4–5), 349–354. <https://doi.org/10.1016/j.enzmictec.2008.04.005>
- Li, Z. H., Kuba, T., & Kusuda, T. (2006). The influence of starvation phase on the properties and the development of aerobic granules. *Enzyme and Microbial Technology*, *38*(5), 670–674. <https://doi.org/10.1016/j.enzmictec.2005.07.020>
- Liang, C. Z., Sun, S. P., Li, F. Y., Ong, Y. K., & Chung, T. S. (2014). Treatment of highly concentrated wastewater containing multiple synthetic dyes by a combined process of coagulation/flocculation and nanofiltration. *Journal of Membrane Science*, *469*, 306–315. <https://doi.org/10.1016/j.memsci.2014.06.057>
- Lim, V., Hobby, A. M., Mccarthy, M. J., & Mccarthy, K. L. (2015). Laminar mixing of miscible fluids in a SMX mixer evaluated by magnetic resonance imaging (MRI). *Chemical Engineering Science*, *137*, 1024–1033. <https://doi.org/10.1016/j.ces.2015.07.003>
- Linlin, H., Jianlong, W., Xianghua, W., & Yi, Q. (2005). The formation and characteristics of aerobic granules in sequencing batch reactor (SBR) by seeding anaerobic granules. *Process Biochemistry*, *40*(1), 5–11. <https://doi.org/10.1016/j.procbio.2003.11.033>
- Liu, L., Wang, Z., Lin, K., & Cai, W. (n.d.). Microbial degradation of polyacrylamide by aerobic granules. *Environmental Technology*, *33*(7–9), 1049–1054. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/22720433>
- Liu, L., Wang, Z., Yao, J., Sun, X., & Cai, W. (2005). Investigation on the formation and kinetics of glucose-fed aerobic granular sludge. *Enzyme and Microbial*

- Technology*, 36(5–6), 712–716. <https://doi.org/10.1016/j.enzmictec.2004.12.024>
- Liu, W. R., Yang, Y. Y., Liu, Y. S., Zhang, L. J., Zhao, J. L., Zhang, Q. Q., ... Ying, G. G. (2017). Biocides in wastewater treatment plants: Mass balance analysis and pollution load estimation. *Journal of Hazardous Materials*, 329, 310–320. <https://doi.org/10.1016/j.jhazmat.2017.01.057>
- Liu, Y. Q., Kong, Y., Tay, J. H., & Zhu, J. (2011). Enhancement of start-up of pilot-scale granular SBR fed with real wastewater. *Separation and Purification Technology*, 82, 190–196. <https://doi.org/10.1016/j.seppur.2011.09.014>
- Liu, Y. Q., Moy, B., Kong, Y. H., & Tay, J. H. (2010). Formation, physical characteristics and microbial community structure of aerobic granules in a pilot-scale sequencing batch reactor for real wastewater treatment. *Enzyme and Microbial Technology*, 46(6), 520–525. <https://doi.org/10.1016/j.enzmictec.2010.02.001>
- Liu, Y. Q., Moy, B. Y. P., & Tay, J. H. (2007). COD removal and nitrification of low-strength domestic wastewater in aerobic granular sludge sequencing batch reactors. *Enzyme and Microbial Technology*, 42(1), 23–28. <https://doi.org/10.1016/j.enzmictec.2007.07.020>
- Liu, Y. Q., & Tay, J. H. (2007a). Cultivation of aerobic granules in a bubble column and an airlift reactor with divided draft tubes at low aeration rate. *Biochemical Engineering Journal*, 34(1), 1–7. <https://doi.org/10.1016/j.bej.2006.11.009>
- Liu, Y. Q., & Tay, J. H. (2007b). Influence of cycle time on kinetic behaviors of steady-state aerobic granules in sequencing batch reactors. *Enzyme and Microbial Technology*, 41(4), 516–522. <https://doi.org/10.1016/j.enzmictec.2007.04.005>
- Liu, Y. Q., & Tay, J. H. (2015). Fast formation of aerobic granules by combining strong hydraulic selection pressure with overstressed organic loading rate. *Water Research*, 80, 256–266. <https://doi.org/10.1016/j.watres.2015.05.015>
- Liu, Yali, Kang, X., Li, X., & Yuan, Y. (2015). Performance of aerobic granular sludge in a sequencing batch bioreactor for slaughterhouse wastewater

- treatment. *Bioresource Technology*.
<https://doi.org/10.1016/j.biortech.2015.03.008>
- Liu, Yong-qiang, & Tay, J. (2008). Influence of starvation time on formation and stability of aerobic granules in sequencing batch reactors, *99*, 980–985.
<https://doi.org/10.1016/j.biortech.2007.03.011>
- Liu, Yu, & Liu, Q. S. (2006). Causes and control of filamentous growth in aerobic granular sludge sequencing batch reactors. *Biotechnology Advances*, *24*(1), 115–127. <https://doi.org/10.1016/j.biotechadv.2005.08.001>
- Liu, Yu, Liu, Y. Q., Wang, Z. W., Yang, S. F., & Tay, J. H. (2005). Influence of substrate surface loading on the kinetic behaviour of aerobic granules. *Applied Microbiology and Biotechnology*, *67*(4), 484–488.
<https://doi.org/10.1007/s00253-004-1785-1>
- Liu, Yu, & Tay, J. H. (2002). The essential role of hydrodynamic shear force in the formation of biofilm and granular sludge. *Water Research*, *36*(7), 1653–1665. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/12044065>
- Liu, Yu, & Tay, J. H. (2004). State of the art of biogranulation technology for wastewater treatment. *Biotechnology Advances*, *22*(7), 533–563.
<https://doi.org/10.1016/j.biotechadv.2004.05.001>
- Liu, Yu, Xu, H. L., Yang, S. F., & Tay, J. H. (2003). Mechanisms and models for anaerobic granulation in upflow anaerobic sludge blanket reactor. *Water Research*, *37*(3), 661–673. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/12688701>
- Liu, Yu, Yang, S. F., Tay, J. H., Liu, Q. S., Qin, L., & Li, Y. (2004). Cell hydrophobicity is a triggering force of biogranulation. *Enzyme and Microbial Technology*, *34*(5), 371–379. <https://doi.org/10.1016/j.enzmictec.2003.12.009>
- Lobry, E., Theron, F., Gourdon, C., Le Sauze, N., Xuereb, C., & Lasuye, T. (2011). Turbulent liquid-liquid dispersion in SMV static mixer at high dispersed phase concentration. *Chemical Engineering Science*, *66*(23), 5762–5774.
<https://doi.org/10.1016/j.ces.2011.06.073>

- Lochmatter, S., Gonzalez-Gil, G., & Holliger, C. (2013). Optimized aeration strategies for nitrogen and phosphorus removal with aerobic granular sludge. *Water Research*, 47(16), 6187–6197. <https://doi.org/10.1016/j.watres.2013.07.030>
- Lochmatter, S., & Holliger, C. (2014). Optimization of operation conditions for the startup of aerobic granular sludge reactors biologically removing carbon, nitrogen, and phosphorous. *Water Research*, 59, 58–70. <https://doi.org/10.1016/j.watres.2014.04.011>
- Lodha, B., & Chaudhari, S. (2007). Optimization of Fenton-biological treatment scheme for the treatment of aqueous dye solutions. *Journal of Hazardous Materials*, 148(1–2), 459–466. <https://doi.org/10.1016/j.jhazmat.2007.02.061>
- Long, B., Yang, C., Pu, W., Yang, J., Jiang, G., Dan, J., ... Liu, F. (2014). Bioresource Technology Rapid cultivation of aerobic granular sludge in a pilot scale sequencing batch reactor. *BIORESOURCE TECHNOLOGY*, 166, 57–63. <https://doi.org/10.1016/j.biortech.2014.05.039>
- Long, B., Yang, C., Pu, W., Yang, J., Liu, F., Zhang, L., ... Cheng, K. (2015). Tolerance to organic loading rate by aerobic granular sludge in a cyclic aerobic granular reactor. *Bioresource Technology*, 182, 314–322. <https://doi.org/10.1016/j.biortech.2015.02.029>
- Lotito, A. M., De Sanctis, M., Di Iaconi, C., & Bergna, G. (2014). Textile wastewater treatment: aerobic granular sludge vs activated sludge systems. *Water Research*, 54, 337–346. <https://doi.org/10.1016/j.watres.2014.01.055>
- Lotito, A. M., Di Iaconi, C., Fratino, U., Mancini, A., & Bergna, G. (2011). Sequencing batch biofilter granular reactor for textile wastewater treatment. *New Biotechnology*, 29(1), 9–16. <https://doi.org/10.1016/j.nbt.2011.04.008>
- Lotito, A. M., Fratino, U., Mancini, A., Bergna, G., & Di Iaconi, C. (2012). Effective aerobic granular sludge treatment of a real dyeing textile wastewater. *International Biodeterioration & Biodegradation*, 69, 62–68. <https://doi.org/10.1016/j.ibiod.2012.01.004>

- Lourenço, N. D., Franca, R. D. G., Moreira, M. A., Gil, F. N., Viegas, C. A., & Pinheiro, H. M. (2015). Comparing aerobic granular sludge and flocculent sequencing batch reactor technologies for textile wastewater treatment. *Biochemical Engineering Journal*, *104*, 57–63. <https://doi.org/10.1016/j.bej.2015.04.025>
- Ma, J., Quan, X., & Li, H. (2013). Application of high OLR-fed aerobic granules for the treatment of low-strength wastewater: Performance, granule morphology and microbial community. *Journal of Environmental Sciences*, *25*(8), 1549–1556. [https://doi.org/10.1016/S1001-0742\(12\)60243-5](https://doi.org/10.1016/S1001-0742(12)60243-5)
- Manavi, N., Kazemi, A. S., & Bonakdarpour, B. (2017). The development of aerobic granules from conventional activated sludge under anaerobic-aerobic cycles and their adaptation for treatment of dyeing wastewater. *Chemical Engineering Journal*, *312*, 375–384. <https://doi.org/10.1016/j.cej.2016.11.155>
- Martins, A. M. P., Pagilla, K., Heijnen, J. J., & Van Loosdrecht, M. C. M. (2004). Filamentous bulking sludge - A critical review. *Water Research*, *38*(4), 793–817. <https://doi.org/10.1016/j.watres.2003.11.005>
- Mata, a M. T., Pinheiro, H. M., & Lourenço, N. D. (2015). Effect of Sequencing Batch Cycle Strategy on the Treatment of a Simulated Textile Wastewater with Aerobic Granular Sludge. *Elsevier B.V.* <https://doi.org/10.1016/j.bej.2015.04.005>
- McClure, D. D., Aboudha, N., Kavanagh, J. M., Fletcher, D. F., & Barton, G. W. (2015). Mixing in bubble column reactors: Experimental study and CFD modeling. *Chemical Engineering Journal*, *264*, 291–301. <https://doi.org/10.1016/j.cej.2014.11.090>
- Mcswain, B. S. (2005). Molecular Investigation Of Aerobic Granular Sludge Formation A Dissertation Submitted to the Graduate School of the University of Notre Dame in Partial Fulfillment of the Requirements for the Degree of Doctor of Philosophy by Robert L . Irvine , Director , (February).
- McSwain, B. S., Irvine, R. L., & Wilderer, P. a. (2004a). The effect of intermittent feeding on aerobic granule structure. *Water Science and Technology : A Journal*

- of the International Association on Water Pollution Research, 49(11–12), 19–25. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/15303718>
- McSwain, B. S., Irvine, R. L., & Wilderer, P. a. (2004b). The influence of settling time on the formation of aerobic granules. *Water Science and Technology: A Journal of the International Association on Water Pollution Research*, 50(10), 195–202. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/15656313>
- Meijer, H. E. H., Singh, M. K., & Anderson, P. D. (2012). On the performance of static mixers: A quantitative comparison. *Progress in Polymer Science*, 37(10), 1333–1349. <https://doi.org/10.1016/j.progpolymsci.2011.12.004>
- Meunier, C., Henriët, O., Schroonbroodt, B., Boeur, J. M., Mahillon, J., & Henry, P. (2016). Influence of feeding pattern and hydraulic selection pressure to control filamentous bulking in biological treatment of dairy wastewaters. *Bioresource Technology*, 221, 300–309. <https://doi.org/10.1016/j.biortech.2016.09.052>
- Miladi, B., El, A., Smaali, I., Ben, A., Hamdi, M., & Bouallagui, H. (2016). Industrial textile effluent decolourization in stirred and static batch cultures of a new fungal strain *Chaetomium globosum* IMA1 KJ472923, 170, 8–14. <https://doi.org/10.1016/j.jenvman.2015.12.038>
- Milia, S., Mallocci, E., & Carucci, A. (2016). Aerobic granulation with petrochemical wastewater in a sequencing batch reactor under different operating conditions. *Desalination and Water Treatment*, 3994(September), 1–10. <https://doi.org/10.1080/19443994.2016.1191778>
- Miralles-Cuevas, S., Oller, I., Agüera, A., Sánchez Pérez, J. A., Sánchez-Moreno, R., & Malato, S. (2016). Is the combination of nanofiltration membranes and AOPs for removing microcontaminants cost effective in real municipal wastewater effluents? *Environmental Science: Water Research and Technology*, 2(3), 511–520. <https://doi.org/10.1039/c6ew00001k>
- Mishima, K., & Nakamura, M. (1991). Self-Immobilization of Aerobic Activated Sludge—a Pilot Study of the Aerobic Upflow Municipal Sewage Treatment. *Water Science Technology*, 23 (4-6)(August), 981–990.

- Mohammadi, A., Moghaddas, J., & Ariamanesh, A. (2015). Residence Time and Concentration Distribution in a Kenics Static Mixer. *Chemical Engineering Communications*, 202(2), 144–150. <https://doi.org/10.1080/00986445.2013.832225>
- Mohebbali, S., Bastani, D., & Shayesteh, H. (2019). Equilibrium, kinetic and thermodynamic studies of a low-cost biosorbent for the removal of Congo red dye: Acid and CTAB-acid modified celery (*Apium graveolens*). *Journal of Molecular Structure*, 1176, 181–193. <https://doi.org/10.1016/j.molstruc.2018.08.068>
- More, T. T., Yadav, J. S. S., Yan, S., Tyagi, R. D., & Surampalli, R. Y. (2014). Extracellular polymeric substances of bacteria and their potential environmental applications. *Journal of Environmental Management*, 144, 1–25. <https://doi.org/10.1016/j.jenvman.2014.05.010>
- Morgenroth, E., Sherden, T., Van Loosdrecht, M. C. M., Heijnen, J. J., & Wilderer, P. A. (1997). Aerobic granular sludge in a sequencing batch reactor. *Water Research*, 31(12), 3191–3194. [https://doi.org/10.1016/S0043-1354\(97\)00216-9](https://doi.org/10.1016/S0043-1354(97)00216-9)
- Moy, B. Y. P., Tay, J. H., Toh, S. K., Liu, Y., & Tay, S. T. L. (2002). High organic loading influences the physical characteristics of aerobic sludge granules. *Letters in Applied Microbiology*, 34(6), 407–412. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/12028420>
- Muda, K., Aris, A., Salim, M. R., Ibrahim, Z., van Loosdrecht, M. C. M., Ahmad, A., & Nawahwi, M. Z. (2011). The effect of hydraulic retention time on granular sludge biomass in treating textile wastewater. *Water Research*, 45(16), 4711–4721. <https://doi.org/10.1016/j.watres.2011.05.012>
- Muda, K., Aris, A., Salim, M. R., Ibrahim, Z., Yahya, A., van Loosdrecht, M. C. M., ... Nawahwi, M. Z. (2010). Development of granular sludge for textile wastewater treatment. *Water Research*, 44(15), 4341–4350. <https://doi.org/10.1016/j.watres.2010.05.023>
- Najib, M. Z. M., Salmiati, Ujang, Z., Salim, M. R., & Ibrahim, Z. (2017). Developed microbial granules containing photosynthetic pigments for carbon dioxide

- reduction in palm oil mill effluent. *International Biodeterioration and Biodegradation*, *116*, 163–170. <https://doi.org/10.1016/j.ibiod.2016.10.031>
- Nancharaiah, Y. V., Joshi, H. M., Mohan, T. V. K., Venugopalan, V. P., & Narasimhan, S. V. (2008). Formation of aerobic granules in the presence of a synthetic chelating agent, *153*, 37–43. <https://doi.org/10.1016/j.envpol.2007.11.017>
- Nguyen, P. T. T., Van Nguyen, P., Truong, H. T. B., & Bui, H. M. (2016). The formation and stabilization of aerobic granular sludge in a sequencing batch airlift reactor for treating tapioca-processing wastewater. *Polish Journal of Environmental Studies*, *25*(5), 2077–2084. <https://doi.org/10.15244/pjoes/62736>
- Ni, B. J., Xie, W. M., Liu, S. G., Yu, H. Q., Wang, Y. Z., Wang, G., & Dai, X. L. (2009). Granulation of activated sludge in a pilot-scale sequencing batch reactor for the treatment of low-strength municipal wastewater. *Water Research*, *43*(3), 751–761. <https://doi.org/10.1016/j.watres.2008.11.009>
- Nidheesh, P. V., Gandhimathi, R., & Ramesh, S. T. (2013). Degradation of dyes from aqueous solution by Fenton processes: A review. *Environmental Science and Pollution Research*, *20*(4), 2099–2132. <https://doi.org/10.1007/s11356-012-1385-z>
- Nor-Anuar, a, Ujang, Z., van Loosdrecht, M. C. M., de Kreuk, M. K., & Olsson, G. (2012). Strength characteristics of aerobic granular sludge. *Water Science & Technology*, *65*(2), 309. <https://doi.org/10.2166/wst.2012.837>
- Nor Anuar, a, Ujang, Z., van Loosdrecht, M. C. M., & de Kreuk, M. K. (2007). Settling behaviour of aerobic granular sludge. *Water Science and Technology: A Journal of the International Association on Water Pollution Research*, *56*(7), 55–63. <https://doi.org/10.2166/wst.2007.671>
- Obaja, D., MacÉ, S., & Mata-Alvarez, J. (2005). Biological nutrient removal by a sequencing batch reactor (SBR) using an internal organic carbon source in digested piggery wastewater. *Bioresource Technology*, *96*(1), 7–14. <https://doi.org/10.1016/j.biortech.2004.03.002>

- Ong, S. A., Toorisaka, E., Hirata, M., & Hano, T. (2005). Treatment of azo dye Orange II in aerobic and anaerobic-SBR systems. *Process Biochemistry*, *40*, 2907–2914. <https://doi.org/10.1016/j.procbio.2005.01.009>
- Otero, M., Rozada, F., Calvo, L. F., García, A. I., & Morán, A. (2003). Kinetic and equilibrium modelling of the methylene blue removal from solution by adsorbent materials produced from sewage sludges. *Biochemical Engineering Journal*, *15*(1), 59–68. [https://doi.org/10.1016/S1369-703X\(02\)00177-8](https://doi.org/10.1016/S1369-703X(02)00177-8)
- Othman, I., Anuar, A. N., Ujang, Z., Rosman, N. H., Harun, H., & Chelliapan, S. (2013). Livestock wastewater treatment using aerobic granular sludge. *Bioresource Technology*, *133*, 630–634. <https://doi.org/10.1016/j.biortech.2013.01.149>
- Ou, D., Li, H., Li, W., Wu, X., Wang, Y., & Liu, Y. (2018). Salt-tolerance aerobic granular sludge: Formation and microbial community characteristics. *Bioresource Technology*, *249*(July 2017), 132–138. <https://doi.org/10.1016/j.biortech.2017.07.154>
- Oyanedel-Craver, V. A., Smith, J. A., Roosta, M., Ghaedi, M., Mohammadi, M., Wu, T., ... Gray, D. G. (2014). Optimization of the ultrasonic assisted removal of methylene blue by gold nanoparticles loaded on activated carbon using experimental design methodology. *Environmental Science and Technology*, *21*(6), 2069–2079. <https://doi.org/10.1007/s11051-009-9766-z>
- Pan, S., Tay, J. H., He, Y. X., & Tay, S. T. L. (2004). The effect of hydraulic retention time on the stability of aerobically grown microbial granules. *Letters in Applied Microbiology*, *38*(2), 158–163. <https://doi.org/10.1111/j.1472-765X.2003.01479.x>
- Pan, Y., Wang, Y., Zhou, A., Wang, A., Wu, Z., Lv, L., ... Zhu, T. (2017). Removal of azo dye in an up-flow membrane-less bioelectrochemical system integrated with bio-contact oxidation reactor. *Chemical Engineering Journal*, *326*, 454–461. <https://doi.org/10.1016/j.cej.2017.05.146>
- Pandey, A., Singh, P., & Iyengar, L. (2007). Bacterial decolorization and degradation of azo dyes. *International Biodeterioration and Biodegradation*, *59*(2), 73–84.

<https://doi.org/10.1016/j.ibiod.2006.08.006>

- Pang, Y. L., & Abdullah, A. Z. (2013). Current status of textile industry wastewater management and research progress in malaysia: A review. *Clean - Soil, Air, Water*, 41(8), 751–764. <https://doi.org/10.1002/clen.201000318>
- Panswad, T., Iamsamer, K., & Anotai, J. (2001). Decolorization of azo-reactive dye by polyphosphate- and glycogen-accumulating organisms in an anaerobic-aerobic sequencing batch reactor. *Bioresource Technology*, 76(2), 151–159. [https://doi.org/10.1016/S0960-8524\(00\)00073-0](https://doi.org/10.1016/S0960-8524(00)00073-0)
- Pearce, C. I., Lloyd, J. R., & Guthrie, J. T. (2003). The removal of colour from textile wastewater using whole bacterial cells: A review. *Dyes and Pigments*, 58(3), 179–196. [https://doi.org/10.1016/S0143-7208\(03\)00064-0](https://doi.org/10.1016/S0143-7208(03)00064-0)
- Peyong, Y. N., Zhou, Y., Abdullah, A. Z., & Vadivelu, V. (2012). The effect of organic loading rates and nitrogenous compounds on the aerobic granules developed using low strength wastewater. *Biochemical Engineering Journal*, 67, 52–59. <https://doi.org/10.1016/j.bej.2012.05.009>
- Pezo, M., Pezo, L., Jovanović, A., Lončar, B., & Čolović, R. (2016). DEM/CFD approach for modeling granular flow in the revolving static mixer. *Chemical Engineering Research and Design*, 109, 317–326. <https://doi.org/10.1016/j.cherd.2016.02.003>
- Praveen Kumar, G.N & Bhat Sumngala, K. (2012). Decolorization of Azo dye Red 3BN by Bacteria. *International Research Journal of Biological Sciences*, 1(5), 46–52.
- Pronk, M., de Kreuk, M. K., de Bruin, B., Kamminga, P., Kleerebezem, R., & van Loosdrecht, M. C. M. (2015). Full scale performance of the aerobic granular sludge process for sewage treatment. *Water Research*, 84, 207–217. <https://doi.org/10.1016/j.watres.2015.07.011>
- Qin, L., Liu, Y., & Tay, J.-H. (2004). Effect of settling time on aerobic granulation in sequencing batch reactor. *Biochemical Engineering Journal*, 21(1), 47–52. <https://doi.org/10.1016/j.bej.2004.03.005>

- Rahmani, R. K., Keith, T. G., & Ayasoufi, A. (2005). Three-Dimensional Numerical Simulation and Performance Study of an Industrial Helical Static Mixer. *Journal of Fluids Engineering*, 127(3), 467. <https://doi.org/10.1115/1.1899166>
- Rahmani, R. K., Keith, T. G., & Ayasoufi, A. (2008). Numerical simulation of turbulent flow in an industrial helical static mixer. *International Journal of Numerical Methods for Heat & Fluid Flow*, 18(6), 675–696. <https://doi.org/10.1108/09615530810885515>
- Raju, M. D., Joseph, P., Kavitha, E., Dhanasekaran, N., Grahadurai, H. M., & Mohan, T. (2014). Remediation of textile effluents by membrane based treatment techniques: A state of the art review. *Journal of Chemical and Pharmaceutical Sciences*, 2014-Decem, 296–299. <https://doi.org/10.1016/j.jenvman.2014.08.008>
- Rampure, M. R., Kulkarni, A. A., & Ranade, V. V. (2007). Hydrodynamics of bubble column reactors at high gas velocity: Experiments and computational fluid dynamics CFD simulations. *Industrial and Engineering Chemistry Research*, 46(25), 8431–8447. <https://doi.org/10.1021/ie070079h>
- Ramsay, J., Simmons, M. J. H., Ingram, A., & Stitt, E. H. (2016). Mixing performance of viscoelastic fluids in a Kenics KM in-line static mixer. *Chemical Engineering Research and Design*, 115, 310–324. <https://doi.org/10.1016/j.cherd.2016.07.020>
- Ren, T., Liu, L., Sheng, G., Liu, X., Yu, H., Zhang, M., & Zhu, J. (2008). Calcium spatial distribution in aerobic granules and its effects on granule structure , strength and bioactivity, 42, 3343–3352. <https://doi.org/10.1016/j.watres.2008.04.015>
- Revathi, D., & Saravanan, K. (2014). Studies on mixing characteristics of non newtonian fluids using static mixer. *International Journal of ChemTech Research*, 6(10).
- Rondon, H., El-Cheikh, W., Boluarte, I. A. R., Chang, C. Y., Bagshaw, S., Farago, L., ... Shu, L. (2015). Application of enhanced membrane bioreactor (eMBR) to treat dye wastewater. *Bioresource Technology*, 183, 78–85.

<https://doi.org/10.1016/j.biortech.2015.01.110>

- Rosman, N. H., Nor Anuar, A., Chelliapan, S., Md Din, M. F., & Ujang, Z. (2014). Characteristics and performance of aerobic granular sludge treating rubber wastewater at different hydraulic retention time. *Bioresource Technology*, *161*, 155–161. <https://doi.org/10.1016/j.biortech.2014.03.047>
- Rosman, N. H., Nor Anuar, A., Othman, I., Harun, H., Sulong Abdul Razak, M. Z., Elias, S. H., ... Ujang, Z. (2013). Cultivation of aerobic granular sludge for rubber wastewater treatment. *Bioresource Technology*, *129*, 620–623. <https://doi.org/10.1016/j.biortech.2012.12.113>
- Sadri Moghaddam, S., & Alavi Moghaddam, M. R. (2016). Aerobic Granular Sludge for Dye Biodegradation in a Sequencing Batch Reactor With Anaerobic/Aerobic Cycles. *Clean - Soil, Air, Water*, *44*(4), 438–443. <https://doi.org/10.1002/clen.201400855>
- Sadrzadeh, F., & Dulekgurgen, E. (2014). Improving the settling properties of activated sludge by gradually decreasing the settling time. *Desalination and Water Treatment*, *52*(13–15), 2465–2471. <https://doi.org/10.1080/19443994.2013.795874>
- Şahinkaya, S. (2013). COD and color removal from synthetic textile wastewater by ultrasound assisted electro-Fenton oxidation process. *Journal of Industrial and Engineering Chemistry*, *19*(2), 601–605. <https://doi.org/10.1016/j.jiec.2012.09.023>
- Sarvajith, M., Reddy, G. K. K., & Nancharaiah, Y. V. (2018). Textile dye biodecolourization and ammonium removal over nitrite in aerobic granular sludge sequencing batch reactors. *Journal of Hazardous Materials*, *342*, 536–543. <https://doi.org/10.1016/j.jhazmat.2017.08.064>
- Schwarzenbeck, N., Borges, J. M., & Wilderer, P. A. (2005). Treatment of dairy effluents in an aerobic granular sludge sequencing batch reactor. *Applied Microbiology and Biotechnology*, *66*(6), 711–718. <https://doi.org/10.1007/s00253-004-1748-6>

- Sharma, S., Kapoor, S., & Christian, R. A. (2017). Effect of Fenton process on treatment of simulated textile wastewater: optimization using response surface methodology. *International Journal of Environmental Science and Technology*, *14*(8), 1665–1678. <https://doi.org/10.1007/s13762-017-1253-y>
- Shi, J., Zhang, B., Liang, S., Li, J., & Wang, Z. (2018). Simultaneous decolorization and desalination of dye wastewater through electrochemical process. *Environmental Science and Pollution Research*, *25*(9), 8455–8464. <https://doi.org/10.1007/s11356-017-1159-8>
- Sirianuntapiboon, S., & Srisornsak, P. (2007). Removal of disperse dyes from textile wastewater using bio-sludge. *Bioresource Technology*, *98*, 1057–1066. <https://doi.org/10.1016/j.biortech.2006.04.026>
- Smolders, G. J., Klop, J. M., van Loosdrecht, M. C., & Heijnen, J. J. (1995). A metabolic model of the biological phosphorus removal process: I. Effect of the sludge retention time. *Biotechnology and Bioengineering*, *48*(3), 222–233. <https://doi.org/10.1002/bit.260480309>
- Song, Z., Pan, Y., Zhang, K., Ren, N., & Wang, A. (2010). Effect of seed sludge on characteristics and microbial community of aerobic granular sludge. *Journal of Environmental Sciences*, *22*(9), 1312–1318. [https://doi.org/10.1016/S1001-0742\(09\)60256-4](https://doi.org/10.1016/S1001-0742(09)60256-4)
- Sturm, B. S. M., & Irvine, R. L. (2008). Dissolved oxygen as a key parameter to aerobic granule formation, 781–787. <https://doi.org/10.2166/wst.2008.393>
- Su, B., Cui, X., & Zhu, J. (2012). Optimal cultivation and characteristics of aerobic granules with typical domestic sewage in an alternating anaerobic/aerobic sequencing batch reactor. *Bioresource Technology*, *110*, 125–129. <https://doi.org/10.1016/j.biortech.2012.01.127>
- Su, K. Z., & Yu, H. Q. (2005). Gas holdup and oxygen transfer in an aerobic granule-based sequencing batch reactor. *Biochemical Engineering Journal*, *25*(3), 201–207. <https://doi.org/10.1016/j.bej.2005.05.004>
- Sulyman, M., Namiesnik, J., & Gierak, A. (2017). Low-cost adsorbents derived from

- agricultural by-products/wastes for enhancing contaminant uptakes from wastewater: A review. *Polish Journal of Environmental Studies*, 26(2), 479–510. <https://doi.org/10.15244/pjoes/66769>
- Szabó, E., Hermansson, M., Modin, O., Persson, F., & Wilén, B. M. (2016). Effects of wash-out dynamics on nitrifying bacteria in aerobic granular sludge during start-up at gradually decreased settling time. *Water (Switzerland)*, 8(5). <https://doi.org/10.3390/w8050172>
- Szabó, E., Liébana, R., Hermansson, M., Modin, O., Persson, F., & Wilén, B. M. (2017). Microbial population dynamics and ecosystem functions of anoxic/aerobic granular sludge in sequencing batch reactors operated at different organic loading rates. *Frontiers in Microbiology*, 8(MAY), 1–14. <https://doi.org/10.3389/fmicb.2017.00770>
- Talansier, E., Dellavalle, D., Loisel, C., Desrumaux, A., & Legrand, J. (2012). Elaboration of Controlled Structure Foams with the SMX Static Mixer, 00(0), 34–36. <https://doi.org/10.1002/aic>
- Tay, J. H., Ivanov, V., Pan, S., & Tay, S. T. L. (2002). Specific layers in aerobically grown microbial granules. *Letters in Applied Microbiology*, 34(4), 254–257. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/11940154>
- Tay, J. H., Liu, Q. S., & Liu, Y. (2004). The effect of upflow air velocity on the structure of aerobic granules cultivated in a sequencing batch reactor. *Water Science and Technology : A Journal of the International Association on Water Pollution Research*, 49(11–12), 35–40. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/15303720>
- Tay, J. H., Pan, S., Tay, S. T. L., Ivanov, V., & Liu, Y. (2003). The effect of organic loading rate on the aerobic granulation: the development of shear force theory. *Water Science and Technology : A Journal of the International Association on Water Pollution Research*, 47(11), 235–240. Retrieved from <http://www.ncbi.nlm.nih.gov/pubmed/12906295>
- Tay, J. H., Liu, Q. S., & Liu, Y. (2001). The effects of shear force on the formation, structure and metabolism of aerobic granules. *Applied Microbiology and*

- Biotechnology*, 57(1–2), 227–233. <https://doi.org/10.1007/s002530100766>
- Tay, J., Liu, Q., Liu, Y., Show, K., Ivanov, V., & Tay, S. T. (2005). A Comparative Study of Aerobic Granulation in Pilot- and Laboratory-Scale SBRs, *4*(8).
- Tay, J., Pan, S., He, Y., Tiong, S., & Tay, L. (2004). Effect of Organic Loading Rate on Aerobic Granulation . I: Reactor Performance, (October), 1094–1101.
- Tee, P. F., Abdullah, M. O., Tan, I. A. W., Rashid, N. K. A., Amin, M. A. M., Nolasco-Hipolito, C., & Bujang, K. (2016). Review on hybrid energy systems for wastewater treatment and bio-energy production. *Renewable and Sustainable Energy Reviews*, 54, 235–246. <https://doi.org/10.1016/j.rser.2015.10.011>
- Thakur, R. K., Vial, C., Nigam, K. D. P., Nauman, E. B., & Djelveh, G. (2003). Static mixers in the process industries - a review. *Chemical Engineering Research and Design*, 81(7), 787–826. <https://doi.org/10.1205/026387603322302968>
- Thanh, B. X., Visvanathan, C., & Aim, R. Ben. (2009). Characterization of aerobic granular sludge at various organic loading rates. *Process Biochemistry*, 44(2), 242–245. <https://doi.org/10.1016/j.procbio.2008.10.018>
- Theron, F., & Sauze, N. Le. (2011). Comparison between three static mixers for emulsification in turbulent flow. *International Journal of Multiphase Flow*, 37(5), 488–500. <https://doi.org/10.1016/j.ijmultiphaseflow.2011.01.004>
- Tian, X., Xiao, Y., Zhou, P., Zhang, W., Chu, Z., & Zheng, W. (2015). Study on the mixing performance of static mixers in selective catalytic reduction (SCR) systems. *Journal of Marine Engineering & Technology*, 14(2), 57–60. <https://doi.org/10.1080/20464177.2015.1096615>
- Tijhuis, L., Huisman, J. L., Hekkelman, H. D., van Loosdrecht, M. C. M., & Heijnen, J. J. (1995). Formation of nitrifying biofilms on small suspended particles in airlift reactors. *Biotechnology and Bioengineering*, 47(5), 585–595. <https://doi.org/10.1002/bit.260470511>

- Toh, S. K., Tay, J. H., Moy, B. Y. P., Ivanov, V., & Tay, S. T. L. (2003). Size-effect on the physical characteristics of the aerobic granule in a SBR. *Applied Microbiology and Biotechnology*, *60*(6), 687–695. <https://doi.org/10.1007/s00253-002-1145-y>
- Tomar, S. K., & Chakraborty, S. (2018). Characteristics of aerobic granules treating phenol and ammonium at different cycle time and up flow liquid velocity. *International Biodeterioration and Biodegradation*, *127*(July 2017), 113–123. <https://doi.org/10.1016/j.ibiod.2017.11.024>
- Truong, H. T. B., Nguyen, P. Van, Nguyen, P. T. T., & Bui, H. M. (2018). Treatment of tapioca processing wastewater in a sequencing batch reactor: Mechanism of granule formation and performance. *Journal of Environmental Management*, *218*, 39–49. <https://doi.org/10.1016/j.jenvman.2018.04.041>
- Umar, M., Aziz, H. A., & Yusoff, M. S. (2010). Trends in the use of Fenton , electro-Fenton and photo-Fenton for the treatment of landfill leachate. *Waste Management*, *30*(11), 2113–2121. <https://doi.org/10.1016/j.wasman.2010.07.003>
- Val del Rio, A., Figueroa, M., Mosquera-Corral, A., Campos, J. L., & Méndez, R. (2013). Stability of Aerobic Granular Biomass Treating the Effluent from A Seafood Industry. *Environmental Research*, *7*(2), 265–276.
- Venkata Mohan, S., Lalit Babu, V., & Sarma, P. N. (2007). Anaerobic biohydrogen production from dairy wastewater treatment in sequencing batch reactor (AnSBR): Effect of organic loading rate. *Enzyme and Microbial Technology*, *41*(4), 506–515. <https://doi.org/10.1016/j.enzmictec.2007.04.007>
- Vikrant, K., Giri, B. S., Raza, N., Roy, K., Kim, K. H., Rai, B. N., & Singh, R. S. (2018). Recent advancements in bioremediation of dye: Current status and challenges. *Bioresour Technol*, *253*(November 2017), 355–367. <https://doi.org/10.1016/j.biortech.2018.01.029>
- Wagner, J., & da Costa, R. H. R. (2013). Aerobic Granulation in a Sequencing Batch Reactor Using Real Domestic Wastewater. *Journal of Environmental Engineering*, *139*, 1391–1396. [https://doi.org/10.1061/\(ASCE\)EE.1943-](https://doi.org/10.1061/(ASCE)EE.1943-)

- Wang, F., Yang, F., Zhang, X., Liu, Y., Zhang, H., & Zhou, J. (2005). Effects of Cycle Time on Properties of Aerobic Granules in Sequencing Batch Airlift Reactors. *World Journal of Microbiology and Biotechnology*, *21*(8–9), 1379–1384. <https://doi.org/10.1007/s11274-005-5451-2>
- Wang, Q., Du, G., & Chen, J. (2004). Aerobic granular sludge cultivated under the selective pressure as a driving force. *Process Biochemistry*, *39*(5), 557–563. [https://doi.org/10.1016/S0032-9592\(03\)00128-6](https://doi.org/10.1016/S0032-9592(03)00128-6)
- Wang, S. G., Liu, X. W., Gong, W. X., Gao, B. Y., Zhang, D. H., & Yu, H. Q. (2007). Aerobic granulation with brewery wastewater in a sequencing batch reactor. *Bioresource Technology*, *98*(11), 2142–2147. <https://doi.org/10.1016/j.biortech.2006.08.018>
- Wang, Y., Guo, G., Wang, H., Stephenson, T., Guo, J., & Ye, L. (2013). Long-term impact of anaerobic reaction time on the performance and granular characteristics of granular denitrifying biological phosphorus removal systems. *Water Research*, *47*(14), 5326–5337. <https://doi.org/10.1016/j.watres.2013.06.013>
- Wang, Z., Gao, M., Wang, S., Xin, Y., Ma, D., She, Z., ... Ren, Y. (2014). Effect of hexavalent chromium on extracellular polymeric substances of granular sludge from an aerobic granular sequencing batch reactor. *Chemical Engineering Journal*, *251*, 165–174. <https://doi.org/10.1016/j.cej.2014.04.078>
- Weber, S. D., Ludwig, W., Schleifer, K. H., & Fried, J. (2007). Microbial composition and structure of aerobic granular sewage biofilms. *Applied and Environmental Microbiology*, *73*(19), 6233–6240. <https://doi.org/10.1128/AEM.01002-07>
- Wei, D., Shi, L., Yan, T., Zhang, G., Wang, Y., & Du, B. (2014). Bioresource Technology Aerobic granules formation and simultaneous nitrogen and phosphorus removal treating high strength ammonia wastewater in sequencing batch reactor. *BIORESOURCE TECHNOLOGY*, *171*, 211–216. <https://doi.org/10.1016/j.biortech.2014.08.001>

- Wichern, M., Lu, M., & Horn, H. (2008). Optimizing sequencing batch reactor (SBR) reactor operation for treatment of dairy wastewater with aerobic granular sludge, 1199–1206. <https://doi.org/10.2166/wst.2008.486>
- Winkler, M. K. H., Meunier, C., Henriot, O., Mahillon, J., Suárez-Ojeda, M. E., Del Moro, G., ... Weissbrodt, D. G. (2018). An integrative review of granular sludge for the biological removal of nutrients and recalcitrant organic matter from wastewater. *Chemical Engineering Journal*, 336(December 2017), 489–502. <https://doi.org/10.1016/j.cej.2017.12.026>
- Xu, G., Xu, X., Yang, F., & Liu, S. (2011). Selective inhibition of nitrite oxidation by chlorate dosing in aerobic granules. *Journal of Hazardous Materials*, 185(1), 249–254. <https://doi.org/10.1016/j.jhazmat.2010.09.025>
- Yagub, M. T., Sen, T. K., Afroze, S., & Ang, H. M. (2014). Dye and its removal from aqueous solution by adsorption: A review. *Advances in Colloid and Interface Science*, 209, 172–184. <https://doi.org/10.1016/j.cis.2014.04.002>
- Yan, L. K. Q., Fung, K. Y., & Ng, K. M. (2017). Aerobic sludge granulation for simultaneous anaerobic decolorization and aerobic aromatic amines mineralization for azo dye wastewater treatment. *Environmental Technology (United Kingdom)*, 3330(May), 1–8. <https://doi.org/10.1080/09593330.2017.1329354>
- Yang, B., Xu, H., Yang, S., Bi, S., Li, F., Shen, C., & Ma, C. (2018). Bioresource Technology Treatment of industrial dyeing wastewater with a pilot-scale strengthened circulation anaerobic reactor. *Bioresource Technology*, 264(April), 154–162. <https://doi.org/10.1016/j.biortech.2018.05.063>
- Yang, S. F., Tay, J. H., & Liu, Y. (2003). A novel granular sludge sequencing batch reactor for removal of organic and nitrogen from wastewater. *Journal of Biotechnology*, 106(1), 77–86. <https://doi.org/10.1016/j.jbiotec.2003.07.007>
- Yang, Y. C., Liu, X., Wan, C., Sun, S., & Lee, D. J. (2014). Accelerated aerobic granulation using alternating feed loadings: Alginate-like exopolysaccharides. *Bioresource Technology*, 171, 360–366. <https://doi.org/10.1016/j.biortech.2014.08.092>

- Yeap, K. L., Teng, T. T., Poh, B. T., Morad, N., & Lee, K. E. (2014). Preparation and characterization of coagulation/flocculation behavior of a novel inorganic-organic hybrid polymer for reactive and disperse dyes removal. *Chemical Engineering Journal*, 243, 305–314. <https://doi.org/10.1016/j.cej.2014.01.004>
- Zhan, M., Sun, G., Lu, Y., Wang, X., & Zhang, Y. (2016). Characterization of mixing of binary particles in a continuous colliding static mixer. *Powder Technology*, 291, 448–455. <https://doi.org/10.1016/j.powtec.2016.01.005>
- Zhang, Dalei, Wang, Y., Li, H., Wang, S., & Jing, Y. (2013). Aerobic Granulation in a Sequencing Batch Reactor for the Treatment of Piggery Wastewater. *Water Environment Research*, 85, 239–245. <https://doi.org/10.2175/106143012X13560205145136>
- Zhang, Dejin, Li, W., Hou, C., Shen, J., Jiang, X., Sun, X., ... Liu, X. (2017). Aerobic granulation accelerated by biochar for the treatment of refractory wastewater. *Chemical Engineering Journal*, 314, 88–97. <https://doi.org/10.1016/j.cej.2016.12.128>
- Zhang, H., Dong, F., Jiang, T., Wei, Y., Wang, T., & Yang, F. (2011). Aerobic granulation with low strength wastewater at low aeration rate in A/O/A SBR reactor. *Enzyme and Microbial Technology*, 49, 215–222. <https://doi.org/10.1016/j.enzmictec.2011.05.006>
- Zhang, L., Feng, X., Zhu, N., & Chen, J. (2007). Role of extracellular protein in the formation and stability of aerobic granules. *Enzyme and Microbial Technology*, 41(5), 551–557. <https://doi.org/10.1016/j.enzmictec.2007.05.001>
- Zhang, Y., An, X., & Quan, X. (2011). Enhancement of sludge granulation in a zero valence iron packed anaerobic reactor with a hydraulic circulation. *Process Biochemistry*, 46(2), 471–476. <https://doi.org/10.1016/j.procbio.2010.09.021>
- Zheng, Y. M., Yu, H. Q., Liu, S. J., & Liu, X. Z. (2006). Formation and instability of aerobic granules under high organic loading conditions. *Chemosphere*, 63(10), 1791–1800. <https://doi.org/10.1016/j.chemosphere.2005.08.055>