Bull. Chem. Soc. Ethiop. **2019**, 33(2), 243-254. © 2019 Chemical Society of Ethiopia and The Authors DOI: <u>https://dx.doi.org/10.4314/bcsc.v33i2.5</u> ISSN 1011-3924 Printed in Ethiopia

# KINETIC AND THERMODYNAMIC STUDY OF OXIDATIVE DEGRADATION OF ACID YELLOW 17 DYE BY FENTON-LIKE PROCESS: EFFECT OF $HCO_3^-$ , $CO_3^{2-}$ , $C\Gamma^-$ AND $SO_4^{2-}$ ON DYE DEGRADATION

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(Received July 6, 2018; Revised February 27, 2019; Accepted April 4, 2019)

**ABSTRACT.** We report here the degradation of AY-17 dye using Fenton-like process (H<sub>2</sub>O<sub>2</sub>/Fe<sup>3+</sup>). The maximum degradation (83%) of AY17 dye is achieved at pH 3 in 60 min, with optimum concentrations of AY 17 (0.06 mM), H<sub>2</sub>O<sub>2</sub> (0.9 mM), and Fe<sup>2+</sup> (0.06 mM). The scavenging effects of HCO<sub>3</sub><sup>-</sup>, CO<sub>3</sub><sup>2-</sup>, Cl<sup>-</sup> and SO<sub>4</sub><sup>2-</sup> on dye degradation are also examined. The activation energy ( $E_a$ ), activation enthalpy ( $\Delta$ H<sup>\*</sup>), and activation entropy ( $\Delta$ S<sup>\*</sup>) are calculated for the dye degradation using pseudo-first-order kinetics at various temperature.

KEY WORDS: Acid Yellow 17, H<sub>2</sub>O<sub>2</sub>/Fe<sup>3+</sup>, Fenton-like process, Oxidative degradation, Scavenging effects

## INTRODUCTION

The azo dyes are frequently used in textile industries due to its low energy consumption, easy utilization, high stability during washing and it presence in varieties of color. A huge amount of water is consumed by textile and dyeing industries. The resulting wastewater from these industries may contain reactive azo dyes and its intermediates. The direct discharge of these dyes-contaminated waste water (from these industries) to water bodies may produce a severe environmental problem. Even, a small quantity (1 mg/L) of these dyes might produce an adverse effect on environment. These dyes contaminated water might be harmful for both aquatic and human life, producing hazardous mutagenic or carcinogenic effect in human being [1, 2]. The discharge of dyes into water, depressed photosynthesis as well as respiration processes of aquatic system [3]. Hence, the treatment of water containing these hazardous pollutants is a major issue for environmental chemist [4-7]. Generally, these azo dyes are non-biodegradable in aerobic condition and convert to more toxic intermediate [8]. Various adsorbents and biosorbents have been used for removal of these dyes [9-11]. Ranjithkumar et al. [9] reported the use of activated carbon/Fe<sub>2</sub>O<sub>3</sub> nanocomposite as adsorbent for removal of acid yellow 17. Similarly, Ashraf et al. [10] used a plant named T. Angustata L. and Gao et al. [11] used nonliving aerobic granular sludge as biosorbent for removal of acid yellow 17 dye.

For the last two decades, AOPs have been playing an important role in the degradation of azo dyes [12–14]. In these processes high oxidizing agent 'OH radical (having redox potential 2.8 V vs SHE) are used to oxidize the dyes. AOPs degraded complex structured dyes to smaller organic molecules or may completely oxidized it to  $CO_2$  and  $H_2O$  [15, 16].

AOPs includes, Fenton, photo-Fenton, homogenous Fenton-like process, TiO<sub>2</sub>/UV [17], ZnO/UV [18], ozonation [19], etc. Among them, Fenton process ( $Fe^{2+}/H_2O_2$ ) is the commonly used for degradation of dyes and other organic pollutants. Because, it has many advantages: (1) it involves the breakdown of  $H_2O_2$  into environmental friendly species such as  $O_2$  and  $H_2O$ , (2) it is a non-toxic process [20], (3) and it is simple, it can be employed at STP and (4) and yield

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#### Jehangeer Khan et al.

high efficiency [21]. Our group has already reported AY-17 dye removal by  $Fe^{2^+}/H_2O_2$  and UV/ $Fe^{2^+}/H_2O_2$  system [22, 23]. However, there are some disadvantages associated with these process [24]. To overcome these disadvantages, the modified Fenton processes were introduced – the  $Fe^{2^+}$  were replaced with nano zero valent iron or  $Fe^{3^+}$  [25, 26].

In the present study Fenton-like process,  $H_2O_2/Fe^{3+}$ , were used for degradation of AY 17 in aqueous medium. The optimum concentration of  $H_2O_2$ ,  $Fe^{3+}$ , and AY 17 were determined for achieving high degradation efficiency. The effects of pH, temperature and various anions  $(CO_3^{2-}, HCO_3^{-}, Cl^{-} \text{ and } SO_4^{2-})$  on the efficiency of dye degradation were investigated. Kinetic study of dye degradation reaction was also carried out.

#### **EXPERIMENTAL**

#### Chemical and reagent

Acid Yellow 17 (dye content 60%) was obtained from Acros Organics. Hydrogen peroxide (30% w/w), ferric sulfate hepta hydrated, sodium carbonate, sodium sulfate, sulfuric acid, sodium chloride, hydrochloric acid, and sodium hydroxide analytical grade from Sigma Aldrich were used as received.

#### Experimental procedure

Ultra-pure water (resistivity  $\geq 18.2 \text{ M}\Omega$ . cm), purify through Milli-Q<sup>®</sup> purification system was used for preparation of solutions. The UV-Vis spectra of AY 17 in a quartz cell (1 cm path length) were recorded in the range of 300-700 nm using a UV-visible spectrophotometer (Perkin Elmer, Model: Lambda-650, UK). All the experiments were performed in triplicate at room temperature. The pH of solutions was adjusted through pH meter; NeoMet ISTEC (Korea), using HCl and NaOH. Experiments were carried out in 50 mL beakers in thermostat of constant temperature. The experimental mixture is stirred by magnetic stirrer. In each experiment certain quantity of dye ferric ion (Fe<sup>3+</sup>), and H<sub>2</sub>O<sub>2</sub> were put in a volumetric flask and then diluted up to 50 ml by adding triply distilled water. The samples were instantly analyzed at fixed time intervals. The change in  $\lambda_{max}$  was monitored at consecutive time interval to study the course of the degradation process.

The change in concentration of AY 17 was determined from the absorbance intensity of reaction mixture (at 400 nm,  $\mathcal{E} = 12928 \text{ M}^{-1} \text{ cm}^{-1}$ ) at various time intervals through the calibration plot. The absorption of reaction mixture and sampling were completed within one minute to minimize experimental error [27]. Percent degradation was calculated using Eq. (1).

Percent Degradation (%) =  $\left(1 - \frac{C_t}{C_0}\right) \times 100\%$  (1)

# **RESULTS AND DISCUSSION**

Degradation of AY 17 by ferric ion ( $Fe^{3+}$ ), hydrogen peroxide ( $H_2O_2$ ), and Fenton-like process ( $H_2O_2/Fe^{3+}$ ): selection of suitable system

The effect of various parameters on percent degradation of AY 17 was investigated (Figure 1). The maximum dye degradation was obtained in 60 minutes with optimal concentrations of  $H_2O_2$  (0.9 mM), Fe<sup>3+</sup> (0.06 mM), and AY 17 (0.06 mM) dye (see next sections). Foremost, AY 17 (0.06 mM) was degraded using individual  $H_2O_2$  and Fe<sup>3+</sup> systems and then Fenton like –  $H_2O_2$  /Fe<sup>3+</sup> system were applied. It was observed that the degradation of acid yellow 17 dye with Fe<sup>3+</sup>,  $H_2O_2$ , and Fe<sup>3+</sup>/ $H_2O_2$  systems were about 3 %, 11 % and 83%, respectively in 60 minutes. The reason for low percent degradation of dye solutions through individual Fe<sup>3+</sup> or  $H_2O_2$  systems

were due to the low quantity of hydroxyl radical production because of the absence of an oxidizing agent,  $H_2O_2$  (Fe<sup>3+</sup> system) or catalyst, Fe<sup>3+</sup> in ( $H_2O_2$  system) while, high percent dye degradation in Fe<sup>3+</sup>/  $H_2O_2$  system was due to production of large amount of hydroxyl radical (\*OH) because of the presence of both oxidizing and reducing species [28]. The general mechanism for hydroxyl radical (\*OH) generation is given by Eq. 2 and 3 [29].

$$Fe^{3+}$$
 +  $H_2O_2 \rightarrow Fe^{2+}$  +  $HOO^{\bullet}$  +  $H^+$  (2)

$$Fe^{2+} + H_2O_2 \rightarrow Fe^{3+} + HO^{\bullet} + HO^{-}$$
 (3)



Figure 1. Selection of suitable process for degradation of AY 17 dye: pH = 3.0,  $[H_2O_2]_0 = 0.9$  mM,  $[AY 17]_0 = [Fe^{3+}]_0 = 0.06$  mM, T = 298 K.

## Effect of pH dye degradation

As the pH plays an important role in the degradation of dye solution. Hence, dye solutions of pH 2.0, 3.0, 6.0, and 8.0 were degraded using Fenton-like process for 60 min. The initial concentration of acid yellow 17,  $H_2O_2$  and ferric ion were taken as 0.06, 0.9, and 0.06 mM, for acid yellow 17,  $H_2O_2$  and  $Fe^{3+}$ , respectively (Figure 2a). It was observed that highest percent degradation (83%) was achieved at pH 3.0. The reason for such a high degradation efficiency was the high production of hydroxyl radical (•OH) by Fe<sup>3+</sup> at pH 3.0 [30].

The low oxidative degradation of acid yellow 17 dye at pH 6.0 and 8.0 might be explained by several facts: Firstly, the formation of  $Fe(OH)_3$  which has low catalytic properties in decomposition of hydrogen peroxide (H<sub>2</sub>O<sub>2</sub>) [31]. Secondly, the decrease in number of free iron species in solution because at high pH (6.0 and 8.0) precipitation of polymeric ferric oxy hydroxides occurred [32]. The activity of oxy hydroxides might be very low and it may hindered ferrous ion (Fe<sup>2+</sup>) production for hydroxyl radical (•OH) generation shown by Eq. 2 and 3 [33]. Another possibility for low oxidation was the formation of ferrous complexes, which also hindered the reaction of ferric ion (Fe<sup>3+</sup>) with hydrogen peroxide [34]. Similarly, the low percent degradation of acid yellow 17 dye at pH ~ 2.0 was either due to the formation of iron complex species such as [Fe(II)(H<sub>2</sub>O)<sub>6</sub>]<sup>2+</sup>) or scavenging of the hydroxyl (•OH) radical hydronium ion (H<sub>3</sub>O<sup>+</sup>) at low pH [33, 35].

#### Effect of initial concentration of $(H_2O_2)$

The effect of  $H_2O_2$  concentration over dye degradation was also checked. A series of 0.06 mM dye solutions containing various concentrations (i.e. 0.5, 0.6, 0.9 and 1.10 mM) of  $H_2O_2$  and constant initial concentration of Fe<sup>3+</sup> at pH 3 ware degraded to determine the initial optimum dose of  $H_2O_2$  for maximum degradation of AY 17 (Figure 2b). The dye was oxidized through •OH radical produced *via* the reaction of hydrogen peroxide with Fe<sup>3+</sup> (Fenton-like process). The mechanism for reaction of Fe<sup>3+</sup> with  $H_2O_2$  can be found elsewhere in literature [36–39].



Figure 2. Effect of various conditions on % degradation of AY 17 by Fenton-like process: (a) pH, (b) H<sub>2</sub>O<sub>2</sub>, (c) Fe<sup>2+</sup>, (d) concentration of dye. The optimized reaction conditions were determined as:  $[H_2O_2]_o = 0.9 \text{ mM}$ ,  $[Fe^{2+}]_o = [AY \ 17]_o = 0.06 \text{ mM}$ , pH = 3.0.

It was observed that degradation of AY 17 dye increases with hydrogen peroxide concentration. Optimal concentration of  $H_2O_2$  for high degradation (83%) was found to be 0.9 mM. it was also observed that further increase in  $H_2O_2$  concentration decreased the percent degradation which might be due to scavenging of °OH radical by  $H_2O_2$ , hydroperoxy radical (OOH°), form during  $H_2O_2/Fe^{3+}$  reaction or dimerization of hydroxyl radical (°OH) with itself as given by equation (4-6) [37, 40].

$$H_2O_2 + {}^{\bullet}OH \rightarrow H_2O + OOH^{\bullet} \qquad k = 2.7 \times 10^7 M^{-1} s^{-1}$$
 (4)

$$OOH^{\bullet} + {}^{\bullet}OH \rightarrow H_2O + O_2 \qquad \qquad k = 7.1 \times 10^9 \,\mathrm{M}^{-1} \,\mathrm{s}^{-1} \tag{5}$$

$$OH + OH \rightarrow H_2O_2 \qquad \qquad k = 6.0 \times 10^9 \,\mathrm{M}^{-1} \,\mathrm{s}^{-1} \tag{6}$$

# *Effect of initial concentration of ferric ion* $(Fe^{3+})$

As the production of •OH radicals by hydrogen peroxide is catalyzed by iron (Fe<sup>3+</sup>), therefore, the optimum concentration of Fe<sup>3+</sup> for maximum dye degradation was also determined at pH 3. Here, the initial concentration of dye (0.06 mM) and H<sub>2</sub>O<sub>2</sub> (0.9 mM) were kept fixed. While concentration of Fe<sup>3+</sup> was altered from 0.04 mM to 0.06 mM (Figure 2c). It was observed that the percent degradation of AY 17 dye increased from 63 % to 83 % upon increasing Fe<sup>3+</sup> concentration. However, further increase in Fe<sup>3+</sup> concentration decreased down the % degradation due to scavenging of •OH radical by Fe<sup>2+</sup>. The ratio/proportion of H<sub>2</sub>O<sub>2</sub>:Fe<sup>3+</sup> is also important in degradation of dye solution because it was reported that in H<sub>2</sub>O<sub>2</sub>/Fe<sup>3+</sup> system the concentration of Fe<sup>3+</sup> to a system containing H<sub>2</sub>O<sub>2</sub> lead to formation of Fe<sup>3+</sup> peroxo complexes which convert into Fe<sup>2+</sup> and HO•<sub>2</sub> Eq. (7-8) [33]. Hence, the scavenging of hydroxyl radical by hydrogen peroxide and Fe<sup>2+</sup> depends on the molar ratio of H<sub>2</sub>O<sub>2</sub> and Fe<sup>3+</sup> [33].

$$\operatorname{Fe-OOH}^{2^+} + \operatorname{H}_2\operatorname{O}_2 \rightarrow \operatorname{Fe}(\operatorname{OH})_2(\operatorname{HO}_2)^+$$
 (7)

$$\operatorname{Fe}(\operatorname{OH})(\operatorname{HO}_2)^+ \rightarrow \operatorname{Fe}^{2+} + \operatorname{HO}_2^{\bullet} + \operatorname{OH}^-$$
 (8)

#### Dye concentration effect on degradation

The concentration of AY 17 dye is also important parameter which effects the percent degradation. Effect of initial concentration of dye on the degradation was shown in Figure 2d. By keeping the initial concentration of  $[H_2O_2] = 0.90$  mM and  $[Fe^{3+}] = 0.06$  mM, it was monitored that the percent degradation decreased from 83 % to 54 % upon increasing AY 17 concentrations which is in agreement with previous reports [41].

The high degradation of AY 17 at low concentration (0.06 mM) of dye was due to the frequent availability of hydroxyl (<sup>•</sup>OH) radical for low amount of dye molecule. Hence, the decreases in percent degradation (54 %) at comparatively high concentration (0.09 mM) of dye might be interpreted in term of the inadequate availability of hydroxyl radical for AY 17 molecules degradation [27].

# Effect of $CO_3^{2-}$ and $HCO_3^{-}$ on the AY 17 percent degradation

A large amount of inorganic salts, like Na<sub>2</sub>CO<sub>3</sub> and NaHCO<sub>3</sub> are commonly used in various dying process. The presence of these inorganic ions may affect the degradation of AY 17 dye. The influence of CO<sub>3</sub><sup>2-</sup> and HCO<sub>3</sub><sup>-</sup> on degradation of acid yellow 17 dye was investigated at pH 3. Figure 3 shows the degradation of dye solutions in presence of different concentrations of anions; HCO<sub>3</sub><sup>-</sup> and CO<sub>3</sub><sup>2-</sup>. It was observed that the presence of these ions has a negative effect on dye degradation. The percent degradation of AY 17 decreased from 83% to 66% in case of  $CO_3^{2-}$  while 70% in case of HCO<sub>3</sub><sup>-</sup>. These results agree with literature [42]. These ions are much stable and do not form complexes with iron [43], hence, they are able to scavenge the hydroxyl radical (•OH) although another radical, CO<sub>3</sub>•<sup>-</sup>, produced in the hydroxyl radical (•OH) scavenging reaction, but, it has much less reactivity than hydroxyl radical [44].

# Effect of $Cl^{-}$ and $SO_{4}^{2-}$ on the AY 17 percent degradation

The effect of chloride (Cl<sup>-</sup>) and sulfate (SO<sub>4</sub><sup>2–</sup>) ions on dye degradation were investigated (Figure 4). It was noted that percent degradation diminished in the presence of these anions which is due to the scavenging of hydroxyl radical by these anions. The quenching ability of these anions also depends on the nature of these anions, concentration, and type of oxidant (i.e. H<sub>2</sub>O<sub>2</sub>) used for dye oxidation/degradation [45].

These anions also form stable complexes with  $Fe^{3+}/Fe^{2+}$ , therefore, the concentration of  $Fe^{3+}/Fe^{2+}$  decreased in the system which results decrease in hydroxyl radical formation.



Figure 3. Effect of carbonate,  $CO_3^{2^-}(a)$  and bicarbonate,  $HCO_3^-(b)$  ion on % degradation of acid yellow 17 dye in Fenton-like process. Other experimental condition:  $[Fe^{3+}]_o = [AY 17]_o = 0.06 \text{ mM}, [H_2O_2]_o = 0.9 \text{ mM} \text{ and } pH = 3.0.$ 



Figure 4. Effect Chloride, Cl<sup>-</sup> (a) and sulfate, SO<sub>4</sub><sup>-</sup> (b) ion on % degradation by Fenton-like process. Other experimental condition:  $[H_2O_2]_o = 0.90 \text{ mM}$ ,  $[Fe^{3+}]_o = [AY \ 17] = 0.06 \text{ mM}$ , pH = 3.0 and temperature = 298 K.

#### Kinetic study

To examine the degradation kinetics of acid yellow 17 by Fenton-like process, the change in absorption as a function of time data were fitted in linear integrated equations derived for zero, first, second, pseudo-first and pseudo-second-order kinetic as shown by equations given in Table 1 [27, 46]. The rate constants were then calculated from the slope (in case of zero, first, second order) or intercept (in case of pseudo-second-order) of the plots (Table 2). By comparing  $R^2$  of these plots, it was suggested that the degradation of AY 17 follows the pseudo-first-order because it have better  $R^2$  value (0.95 or ~ 1). Similarly, half-lives were also calculated using half-life equations derived for zero, first, second, pseudo-first and pseudo-second-order kinetic and appeared in first right column of Table 1. It was ascertained that the half-life value calculated through pseudo-first-order kinetic equation were closely related to experimental

values. From these detail kinetic studies, it was concluded that the degradation of AY1 7 by Fenton-like process best fit in pseudo-first order kinetic of type.

$$r_{AY 17} = k[AY17][OH] \approx k'[AY17]$$

(9)

The pseudo-first-order rate constant for the degradation process of AY 17 by Fenton-like were found to be 0.0385, 0.0378 and 0.0426 at a temperature of 298, 308 and 318 K, respectively. These results have best correlation with previous literature [47].

Order of Reaction Kinetic	Equation	Half life, min
Zeroth	$\mathbf{A}_{\mathrm{t}} = \mathbf{A}_{0} - k_{0}\mathbf{t}$	$A_0 / 2k_0$
First	$\ln \mathbf{A}_{\mathrm{t}} = \ln \mathbf{A}_0 - k_0 \mathbf{t}$	$\ln 2 / k_1$
Pseudo-first	$\log(A_t - A_e) = \log(A_0 - A_e) - k_1 t / 2.303$	$\ln 2 / k_1$
Second	$1/A_t = 1/A_0 + k_2 t$	$1/k_2[A_0]$
Pseudo-second	$t / A_t = 1 / k_2 A_e^2 - (1 / A_e) t$	$0.5A_0A_e / k_2(A_e - 0.5A_0)$

Table 1. Integrated rate law along with half-life for various order of reaction [27, 46].

Table 2. The kinetic rate constants for degradation of AY 17 by Fenton-like process.

Order of kinetics	T/K	Rate constant, unit <sup>a</sup>	Half-life, min	$\mathbb{R}^2$
Zero-order	298	207	36.7	0.95
	308	194	37.8	0.80
	318	181	39.6	0.70
First-order	298	375	23.8	0.99
	308	465	19.0	0.98
	318	504	17.7	0.95
Pseudo first-order	298	491	18.00	0.98
	308	517	18.34	0.98
	318	555	16.27	0.97
Second-order	298	833	13.16	0.90
	308	580	18.98	0.85
	318	176	6.31	0.90
	298	6580	1.71	0.84
Pseudo second-order	308	10562	1.07	0.77
	318	12566	0.81	0.81

<sup>a</sup>unit for zero order, first-order, and second-order, are M min<sup>-1</sup>, min<sup>-1</sup>, and M<sup>-1</sup>.min, respectively.

#### Effect of temperature

The rate of chemical reaction, product yield and distribution critically depend upon the initial temperature of the system. In the present work the effect of temperature on rate of reaction and percent degradation were determined using temperatures range from 298 to 318 K (Figure 5a). It was recorded that rise in temperature not only increased percent degradation, but also the rate of reaction. This phenomenon might be explained in term of •OH generation as a function of temperature. It was suggested that the rise in temperature accelerates the reaction between  $H_2O_2$  and  $Fe^{3+}$ , hence the generation of oxidizing species like •OH radical become improved [48, 49].



Figure 5. (a) Effect of initial temperature on % degradation of acid yellow 17 dye in Fenton-like process, (b)  $\ln(k/s^{-1}) vs. T^{-1}/K^{-1}$  plot, (c)  $\ln(k/T) vs. T^{-1}/K^{-1}$  plot. Experimental condition:  $[H_2O_2]_o = 0.90 \text{ mM}, [Fe^{3+}]_o = [AY \ 17]_o = 0.06 \text{ mM}, pH = 3.0 \text{ and } T = 298, 308 \text{ and} 318 \text{ K}.$ 

The effect of temperature on the rate constant of the  $H_2O_2/Fe^{3+}$  system was determined by using eq. 10-11. The activation energy (Ea), enthalpy ( $\Delta H^{\#}$ ), and entropy ( $\Delta S^{\#}$ ) of activation of the  $H_2O_2/Fe^{3+}$  process was obtained by employing (see Figure 5 b and c)

$$\ln k = \ln A - \frac{E_a}{RT} \tag{10}$$

$$\ln\frac{k}{T} = \ln\frac{\kappa k_B}{h} + \frac{\Delta S^*}{R} - \frac{\Delta H^*}{R}\frac{1}{T}$$
(11)

Where slope =  $\Delta H/R$  and intercept =  $[\ln(kk_B/h)]+(\Delta S^{#}/R)$ ,  $\kappa$  is usually taken as 1, R is universal gas constant,  $k_B$  is the Boltzmann constant and h is the Planck's constant. The thermodynamic parameters calculated through above equation (10 and 11) are collected in Table 4.

Bull. Chem. Soc. Ethiop. 2019, 33(2)

250

Table 4. Thermodynamic parameters for the degradation of AY 17 by Fenton-like oxidation *pseudo-first-order*.

E <sub>a</sub> , kJmol <sup>-1</sup>	$\Delta H^*$ , kJmol <sup>-1</sup>	$\Delta S^*$ , kJ mol <sup>-1</sup> K <sup>-1</sup>
4.85	2.30	-0.264

Comparison between standard sample prepared in triply deionized water and natural water sample

A comparative study was performed between standard and natural water sample containing AY 17 dye. The result was shown in Figure 6 which clearly shows that the degradation is maximum in standard sample as compared to natural water sample. The aqueous mediums of natural water sample were further analyzed by ion chromatography (IC). It was found that certain anions such as  $HCO_3^{-}(0.298 \text{ mM})$ ,  $CO_3^{2-}(0.252 \text{ mM})$ ,  $SO_4^{2-}(0.5 \text{ mM})$ , and  $CI^{-}(0.335 \text{ mM})$  are present in aqueous medium therefore, the low degradation was due to the presence of these anions. As mentioned earlier, these anions act as scavengers of hydroxyl radical radicals. In natural water sample about 66% while in standard sample, 83% degradation achieved in 60 min. These results suggested that photo-Fenton-like process is relatively efficient method for the degradation of AY-17 in both natural and model sample [22].



Figure 6. Effect of sulfate ions on degradation of AY 17 dye in Fenton-like process. Experimental condition:  $[AY 17]_0 = [Fe^{3+}]_0 = 0.06 \text{ mM}, [H_2O_2]_0 = 0.90 \text{ mM}, \text{pH} = 3.0, T = 298 \text{ K}.$ 

## CONCLUSION

It was concluded that the Fenton-like process is simple and cost-effective method for degradation AY-17 dye. The percent degradation of AY-17 dye is found to be 66% and 83% in natural water sample and standard sample, respectively. The low degradation in natural water sample is due to scavenging of •OH by various anions ( $CO_3^{2-} HCO_3^-$ ,  $CI^-$ , and  $SO_4^-$ ), which

normally present in natural water sample. The rise in temperature also increases percent degradation of dye.

#### ACKNOWLEDGEMENT

The authors highly acknowledge Higher Education Commission of Pakistan for providing funds for research and development.

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