

Rheological behaviour of low-heat Portland cement paste with MgO-based expansive agent and shrinkage reducing admixture

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Abstract: The combined use of low heat Portland cement (LHC), MgO-based expansive agent (MEA) and shrinkage reducing admixture (SRA) is beneficial to reduce the cracking risk of concrete. In this study, the effects of MEA and SRA on the rheological behaviour of LHC paste were investigated using dynamic and static shearing tests. The response surface methodology was used to estimate the effects of MEA, SRA, and superplasticizer on dynamic rheological parameters, while the zeta potential, calorimetric, and solid phases tests were conducted to explore the mechanisms of time-dependent rheological behaviour. Results indicate that MEA contributes to higher dynamic yield stress and plastic viscosity, while the effect of SRA is dependent on its dosage. MEA promotes the static yield stress development for accelerating the hydration of blends and the formation of Mg(OH)₂. SRA retards the hydration of LHC and blended paste and reduces the number of main hydration products. However, the static yield stress is further increased by SRA, showing a consistent changing trend with the surface area of hydrated particles.

Keywords: Magnesium oxide; Rheology; Yield stress; Plastic viscosity; Microstructure

1 Introduction

Cracks induced by constraint shrinkage [1] are of great concern to the durability of concrete. Recently, anti-crack concrete was regarded as a crucial field for the construction industry in China [2] and multiple approaches have been required to minimise non-structural cracks [3]. In Southwest China, the low heat Portland cement (LHC) [4] and reactive MgO [5] have been widely used to control the cracks in hydraulic concrete infrastructures. The use of shrinkage reducing admixture (SRA) is an emerging measure on inhibiting both autogenous and drying shrinkages of concrete [6]. As the

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30 conventional measures cannot mitigate the all-stage shrinkage of concrete, in recent years researchers
31 attempt to use a combination of multifunctional admixtures to control concrete cracking and found
32 the combined use of LHC, MgO-based expansive agent (MEA), and SRA has the potential to produce
33 low even zero shrinkage concrete and thus can meet the requirements for practical applications [7-9].

34 LHC is a kind of cement with low hydration heat and low CO₂ emission [2]. The main clinker
35 components and hydration products of LHC are similar to that of ordinary Portland cement (OPC),
36 but the hydration rate of LHC is much lower because of its higher content of C₂S and lower content
37 of C₃S in comparison with OPC [10, 11]. Moreover, the calcination temperature of LHC is about
38 1250-1350 °C, which is 100-200 °C lower than that of OPC. Compared to OPC, LHC contains less
39 CaCO₃ in terms of raw materials, thereby resulting in lower environmental impact [11]. The use of
40 LHC for the massive concrete can help reduce the internal accumulated heat and thermal gradient and
41 thus mitigate the temperature-induced cracks in concrete structures [2].

42 SRA has been used in modern concrete to mitigate shrinkage, especially for autogenous shrinkage
43 [4]. The SRA molecule usually has a hydrophilic head and a hydrophobic tail. The dispersed SRA
44 molecules in the pore solution adsorb on the solution-solid and solution-air interfaces in cement paste
45 and reduce the interfacial energy of solid particles as well as the surface tension of the pore solution
46 [4]. As a result, SRA can effectively reduce autogenous shrinkage and drying shrinkage. In most cases,
47 SRA is simultaneously used along with polycarboxylate ether-type superplasticizer (SP) in modern
48 concrete where SP mainly works by adsorbing on the solution-solid interface [12]. In fresh cement
49 suspensions, adsorptions of SRA and SP are crucial for their functions, which are generally
50 characterized by UV-visible absorption spectrum [13], zeta potential [14], and total organic carbon
51 tests [14, 15]. The competitive adsorption between SP and retarder was reported by Plank et al. [16],
52 whereas the interaction of SRA and SP molecules which may affect the behaviour of fresh cement
53 paste has not been fully understood.

54 MEA is a widely used expansive agent in China because of its low water demand and
55 independence of curing regime [3]. In blends of cement and MEA, the formation of brucite, i.e.
56 Mg(OH)₂, compensates the shrinkage of concrete. Moreover, the reaction process of MEA can be
57 controlled by changing the calcination temperature [3]. The combined use of SRA and expansive
58 agents more effectively compensate for the shrinkage of concrete [17-19], which is attributed to the
59 retarding effect of SRA on cement hydration [20-22] and the refinement of hydration products [20-
60 22].

61 Rheological properties are crucial to the workability of cement-based materials, which can be
62 affected by the constituents [24], interparticle interactions [25, 26], and chemical additives [27-29].
63 The addition of MEA is reported to significantly decrease the flowability of fresh cement paste [30-
64 32] as MEA aggravates the agglomeration of particles [30], while the effect of SRA on the workability
65 of concrete is still controversial [33, 34]. Besides, the mineral compositions of LHC are different from
66 that of OPC, thereby altering the surface charge of particles which is an important parameter affecting
67 the flowability of fresh paste. As a result, the mixtures with LHC, SRA, and MEA may lead to
68 different rheological properties in comparison with normal concrete, which notably influences the
69 concrete transportation and casting processes in practice. The rheological behaviour of cement paste
70 exhibits a time-dependent feature and is highly associated with the formation of CSH at the early age
71 [35], suggesting that the lower alite content and hydration rate of LHC would lead to a relatively
72 lower CSH content as well as different rheological behaviour from OPC. When LHC is used together
73 with MEA and SRA, the rheological properties of cement paste would be much more complicated
74 due to their interactions. It is vital to investigate the rheological behaviour and early-age hydration of
75 LHC containing MEA and SRA for its widespread application, which have not been extensively
76 addressed.

77 The main purpose of this paper is to investigate the combined effect of MEA, SRA, and SP on
78 the rheological behaviour of LHC paste using dynamic and static shearing tests. Firstly, the individual
79 and combined effects of SRA (0, 1.5%, 2%, and 2.5%), MEA (0, 8%, 10%, and 12%), and SP (0.2%,
80 0.3%, and 0.4%) on the dynamic yield stress and plastic viscosity were estimated by fitting the shear
81 stress-shear rate curve with Bingham model as per the response surface methodology [36] that is an
82 effective statistical approach for multi-variable problems. Then, the interactions between SRA and
83 SP in fresh mixtures of LHC and MEA were explored using zeta potential tests. Besides, the static
84 shearing test, calorimetric test, zeta potential test, X-ray diffraction (XRD), Thermogravimetric
85 analysis (TGA), and scanning electron microscopy (SEM) were conducted on hydrated blends to
86 study the static yield stress development. Finally, the hydration process, solid phases, and
87 microstructure of mixtures in the period of 0-2 h were discussed in detail to fully understand the
88 mechanism behind the time-dependent behaviour. The work may provide some insight into the design
89 of anti-crack concrete from the rheological perspective.

90 **2 Experimental program**

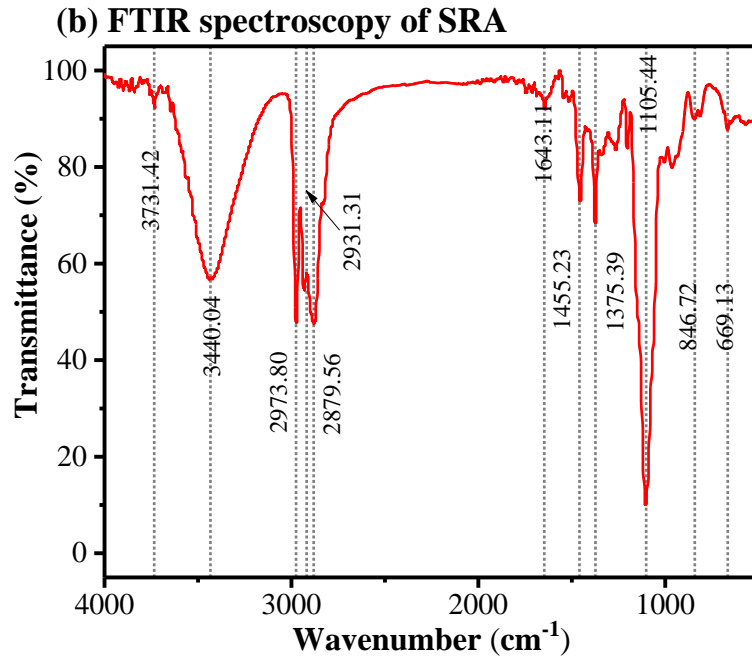
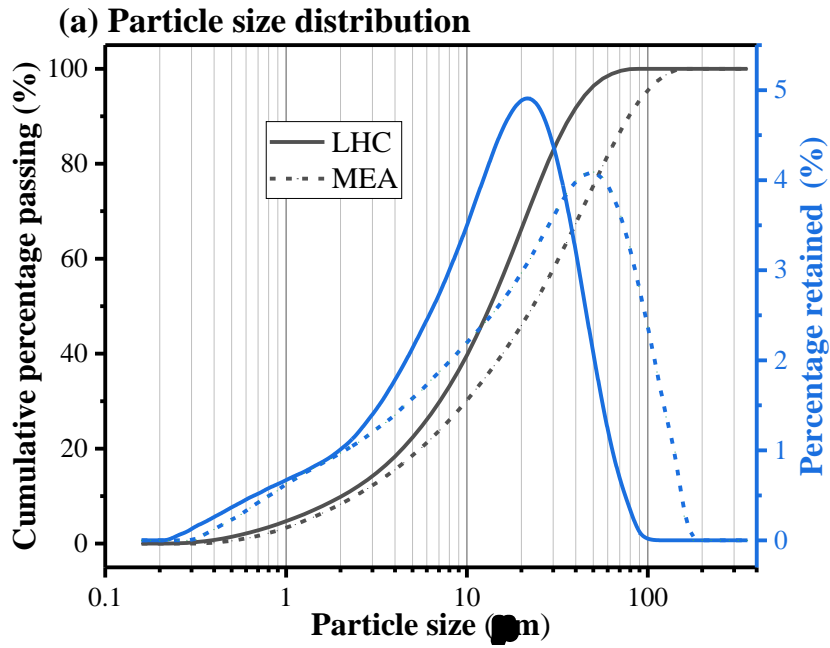
91 **2.1 Raw materials**

92 Commercial LHC from Leshan, China complied with Chinese standard GB/T 200-2017 [37] and
 93 MEA from Nanjing, China complied with Chinese standard T/CECS 540-2018 [38] were used in this
 94 study. The average particle size and apparent density of LHC are 17.10 μm and 3.19 g/cm^3 ,
 95 respectively. The average particle size and apparent density of MEA are 32.83 μm and 2.98 g/cm^3
 96 respectively, the reactivity of MEA, as characterized by the citric acid neutralization method [30, 31],
 97 is 153 s. Table 1 presents the chemical and mineral compositions of LHC and MEA, which are
 98 determined by X-ray fluorescence and Quantitative XRD tests respectively. The particle size
 99 distribution curves are shown in Fig. 1a. Polyether-type SRA with the appearance of a clear liquid
 100 was used. The function groups obtained by Fourier transform infrared spectroscopy are shown in Fig.
 101 1b. The characteristic peak of C-O in ethers is observed at a wavenumber of 1105.44 cm^{-1} , while the
 102 characteristic peaks in the range of 2931.31 cm^{-1} and 2973.80 cm^{-1} are stemmed from the saturated
 103 hydrocarbon and the characteristic peak at 2973.80 cm^{-1} corresponds to the hydroxyl. Then the ^1H
 104 NMR analyse of SRA by dissolving in deuterioxide (D_2O) was conducted on BRUKER AVANCE III
 105 HD 400 MHz, as shown in Fig. 1c, the simplified molecular formula of SRA is also given.
 106 Polycarboxylate ether-type SP with a conventional comb-type structure was used, the solid content
 107 of SP is 20%.

309 Table 1 Chemical and mineral compositions of LHC and MEA

Oxides (wt.%)	LHC	MEA	Minerals (wt.%)	LHC
CaO	63.5	3.4	C_3S	36.5
SiO_2	20.9	4.3	C_2S	44.3
Al_2O_3	3.3	0.7	C_3A	2.9
MgO	1.3	70.4	C_4AF	13.3
Fe_2O_3	4.9	1.0	Anhydrite	2.3
SO_3	1.6	0.2		
Other oxides	3.4	0.3		
Loss of ignition	1.1	19.7		

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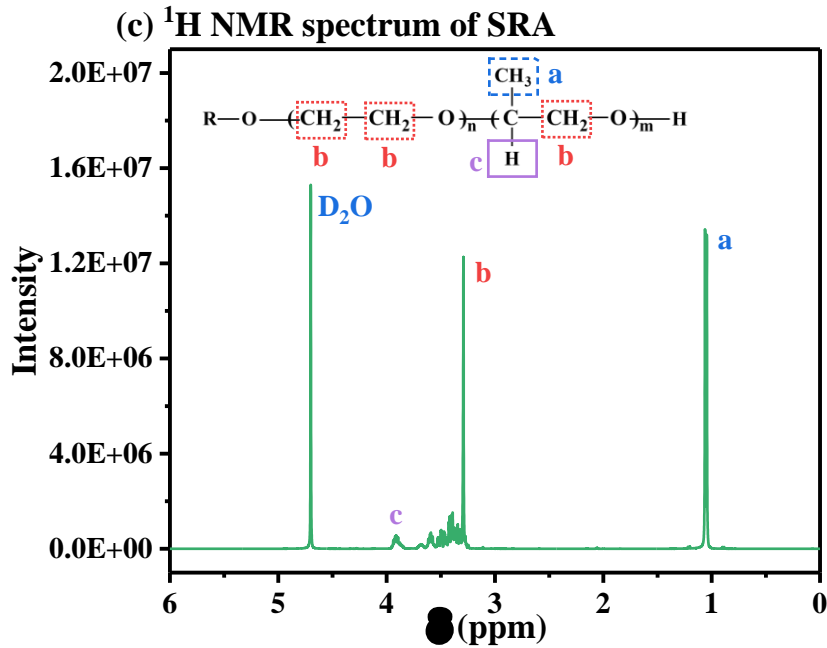


Fig. 1 Particle size distribution of LHC and MEA (a), FTIR spectroscopy of SRA (b), and ^1H NMR spectrum of SRA (c)

2.2 Mix proportions

Based on the trial tests and works of literature [5][10][20], three variables and three levels shown in Table 2 were selected for the study. The levels of MEA and SRA were determined according to the suggested dosage and long-term shrinkage tests, while the levels of SP were set to make the paste flowable enough for rheological tests without bleeding. The water-to-binder ratio was kept constant at 0.35. The mix proportions used in this study are shown in Table 3. Taking M10S1.5P2 as an example, M10 stands for the dosage of MEA (10% by mass of LHC), and S1.5P2 means that the dosages of SRA and SP are 1.5% and 0.2% (by mass of powder materials), respectively. Here, No. 1-17 were designed based on the response surface methodology along with Box-Behnken Design on commercial software, Design-expert[®] 8.0.6. The interactions among MEA, SRA, and SP and their effects on dynamic rheological behaviour were then analysed.

2.3 Sample preparation

The weighted LHC and MEA were dry mixed first in the Hobart N50 mixer for 3 min. SP and SRA (if any) were then added to the deionized water and stirring for 1 min. When the possibly existing foams in the solution were eliminated, the mixing process started. The dry materials and water were mixed at a low speed of 140 rpm for 1 min and then stopped for 0.5 min to manually mix the paste with a spatula, followed by mixing at a high speed of 285 rpm for 2 min and another 1 min at low speed.

136 Table 2 Variables and levels applied in response surface design

Levels	Variables		
	MEA (%)	SRA (%)	SP (%)
-1	8	1.5	0.2
0	10	2.0	0.3
1	12	2.5	0.4

138 Table 3 Mix proportions of LHC pastes

Sample	LHC (g)	Water (g)	MEA (g)	SRA (g)	SP (g)	Yield stress (Pa)	Plastic viscosity (Pa·s)
M10S1.5P2	450	167.5	50.0	7.5	1.0	13.870	0.963
M12S2P2	440	165.0	60.0	10.0	1.0	15.784	1.189
M12S2.5P3	440	162.5	60.0	12.5	1.5	13.729	1.113
M12S2P4	440	165.0	60.0	10.0	2.0	5.372	0.880
M10S2P3	450	165.0	50.0	10.0	1.5	11.936	0.859
M12S1.5P3	440	167.5	60.0	7.5	1.5	11.299	0.897
M10S2P3	450	165.0	50.0	10.0	1.5	7.908	0.943
M10S2P3	450	165.0	50.0	10.0	1.5	9.260	0.779
M10S2.5P2	450	162.5	50.0	12.5	1.0	12.512	0.909
M8S2P2	460	165.0	40.0	10.0	1.0	11.283	0.974
M10S1.5P4	450	167.5	50.0	7.5	2.0	2.494	0.725
M8S1.5P3	460	167.5	40.0	7.5	1.5	2.391	0.601
M10S2P3	450	165.0	50.0	10.0	1.5	9.950	0.824
M10S2P3	450	165.0	50.0	10.0	1.5	10.265	0.893
M8S2.5P3	460	162.5	40.0	12.5	1.5	5.726	0.877
M8S2P4	460	165.0	40.0	10.0	2.0	0.372	0.524
M10S2.5P4	450	162.5	50.0	12.5	2.0	0.799	0.643
CS0P2	500	175.0	/	/	1.0	/	/
CS2P2	500	165.0	/	10.0	1.0	/	/
M10S0P2	450	175.0	50.0	/	1.0	/	/
M10S2P2	450	165.0	50.0	10.0	1.0	/	/

140 2.4 Test methods

142 2.4.1 Rheological tests

144 The elapsed time is defined as the time after the initial contact of water and powder materials. At
 145 7 min, the cement paste was transferred to the coaxial cylinder rotary rheometer (Atton Parr, Austria)
 146 for rheological tests, in which a concentric cylinder rotor with the diameter of 4 cm and the outer
 147 cylinder with the inner diameter of 4.194 cm were used. The temperature during the measurement
 148 was maintained at 25 °C by water bathing.

150 2.4.1.1 Dynamic shearing test

148 To characterise the effects of MEA and SRA on the flowability of fresh cement paste after mixing,
 149 the dynamic shearing test was conducted, which was started at 10 min following the shear procedure:
 150 (1) increasing the shear rate linearly from 0 to 100 s⁻¹; (2) shearing for 30 s at the constant shear rate
 151 of 100 s⁻¹; and (3) decreasing the shear rate linearly from 100 s⁻¹ to 0. Every test was repeated three
 152 times independently to avoid the test error.

153 Bingham model as presented in Eq. (1) is one of the most commonly used rheological models for
 154 fitting the shear stress-shear rate curves [39]. In this paper, the Bingham model was selected to fit the
 155 down curve. According to the shear stress responses to the constant shear rate in Fig. 2, the shear
 156 stresses for each constant shear rates of 80 s⁻¹, 60 s⁻¹, 40 s⁻¹, and 20 s⁻¹ nearly remain constant. In
 157 those cases, the instant responses of shear stress are equal to the equilibrium-state values after
 158 shearing, each single shear stress is recorded in the steady state, thus, shear stress-shear rate curves
 159 in 80 s⁻¹ to 20 s⁻¹ of down curves are used for model fitting, the dynamic yield stress and plastic
 160 viscosity were obtained [39].

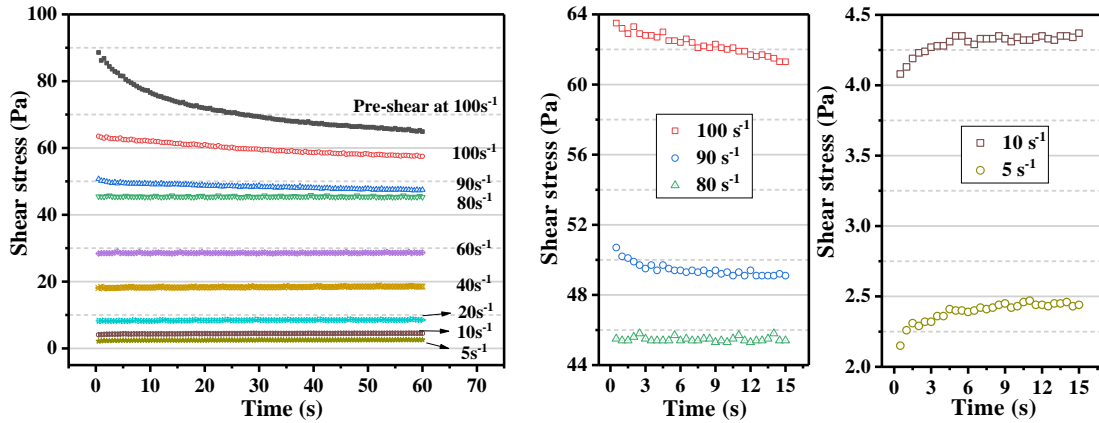


Fig. 2 Shear stress development of CSOP2 at constant shear rates

$$\tau = \tau_0 + \mu \dot{\gamma} \quad (1)$$

where τ_0 is the dynamic yield stress (Pa), μ is the plastic viscosity (Pa·s), and $\dot{\gamma}$ is the shear rate.

2.4.1.2 Static shearing test

The static shearing test is commonly performed to measure the time-dependent rheological behaviour of cement paste. The contents of MEA and SRA were set as variables, while the SP content was fixed at 0.2% to avoid the disturbance of SP content on the results. LHC pastes with various dosages of MEA (0, 8%, 10%, 12%) and SRA (0, 2%) corresponding to samples M12S2P2, M8S2P2, CSOP2, CS2P2, M10S0P2, and M10S2P2 listed in Table 3 were selected for measuring the static yield stress. The test was started at 8.5 min, where the paste was first pre-sheared at 100 s⁻¹ for 0.5

172 min [40] and then stopped for 1 min to rebuild the structure of paste. A constant shear at 0.02 s^{-1} was
173 applied [41] at 10 min for 1 min and the data of 120 measure points were recorded. As a response to
174 the constant shear, the shear stress increases gradually and reaches a peak value, followed by a
175 decrease to a certain value, where the peak value was taken as the static yield stress [40]. The constant
176 shear procedure was repeated every 10 min until the shear stress reached the maximum capacity of
177 shearing stress (i.e. 450 Pa) or the elapsed time reached 120 min.

178 2.4.2 Isothermal calorimetry

179 Isothermal calorimetry was undertaken to investigate the effects of MEA and SRA on the early-
180 age hydration process of LHC. The hydration heat of blends was measured on the TAM Air thermal
181 activity micro-calorimeter. After mixing, about 12 g paste was weighed and transferred to the
182 calorimeter. The test was started at 10 min after the contact of cement and water and the data were
183 recorded every 30 s. The testing temperature was maintained at $25 \text{ }^\circ\text{C}$.

184 2.4.3 Solid phase analyses

185 2.4.3.1 *Hydration stoppage*

186 At each specified age, i.e. 0.5, 1, 1.5, and 2 h, around 10 g paste was sampled and dispersed in
187 200 mL isopropanol and then stirred at 200 rpm in a beaker for 3 min to exchange the free water.
188 Then the suspension was filtered and washed twice with isopropanol. These procedures were repeated
189 twice to fully stop the hydration. Finally, the retained powder was washed with diethyl ether and then
190 stored in a desiccator for 7 days before the microstructure tests and analyses on solid phase [42].

191 2.4.3.2 *Thermogravimetric analysis*

192 Main hydration products including CSH, AFt, $\text{Mg}(\text{OH})_2$, and $\text{Ca}(\text{OH})_2$ in this study were
193 quantitatively analysed using TGA for their different decomposition temperatures, which was carried
194 out with TGA 2(SF)-Mettler Toledo. The pre-processed dry powder samples were placed in an
195 alumina crucible (70 μL) and the weight was controlled at around 50 mg. Then the powder samples
196 were heated from $35 \text{ }^\circ\text{C}$ to $1050 \text{ }^\circ\text{C}$ at a rate of $10 \text{ }^\circ\text{C}/\text{min}$ under the N_2 atmosphere.

197 2.4.3.3 *X-ray diffraction*

198 The crystalline phases in hydrated blends were detected by X-ray diffraction tests. The dry
199 powder sample was placed on a glass microscope slide and scanned at $25 \text{ }^\circ\text{C}$ on the Bruker D8
200 Advance diffractometer (CuK α radiation, 45mA, 35kV) at $6^\circ/\text{min}$ in the range of $5\sim 65^\circ(2\theta)$.

201 2.4.3.4 *Scanning electron microscopy*

202 The hydrate morphology of hydrated particles which is a dominant factor in the particle

203 interactions was observed using SEM. The dry powder sample was slightly sprayed on the conductive
204 tape and then coated with platinum. The microscope (JSM-7900F) was used to take SEM images at
2 an accelerating voltage of 15.0 kV.
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206 2.4.3.5 *Specific surface area*

207 The porous hydration products covered on particles increase the surface roughness and contribute
208 to the specific surface area. The nitrogen adsorption test (BET analysis) was conducted to determine
10 the specific surface area of hydrated blends at 2 h, following a procedure recommended by Daake et
209 al. [43] and Lou et al. [44].
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211 2.4.4 Zeta potential test

212 Diluted suspensions with water-to-powder (W/P) ratio of 10 and 50 were prepared for zeta
17 potential tests [42] that were conducted on ZetaProbe (Colloidal Dynamics, Inc, America) in two
18 approaches. For the first approach, the W/P ratio is 10, which is used for the instant measurement
19 relating to the dynamic shearing test. The powder materials and chemical admixtures were mixed
20 with deionized water. After stirring at 300 rpm for 3 min, the suspension was transferred to the
21 measuring cell. The tests were then carried out to explore the combined effect of SP and SRA. For
22 the second approach, the W/P ratio is 50, which is related to the time-dependent rheological properties.
23 We followed the mixing and hydration stoppage procedures and obtained dry powder samples at ages
24 of 0.5, 1, 1.5, and 2 h, which were re-dispersed in the deionized water. In this way, the diluted
25 suspensions at specified hydration time and solid mass fraction were prepared. Then, the suspensions
26 were transferred to the measuring cell to obtain the zeta potential at each hydration age. During the
27 measurement, the suspension was stirred at 250 rpm to keep it homogeneous. The zeta potential was
28 measured by the electrodes in the measuring cell and then calculated using the embedded software
29 based on the O'Brien equation [45].
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226 **3 Results and discussion**

227 **3.1 Dynamic rheological parameters**

228 The dynamic yield stress and plastic viscosity of fresh blended pastes (see in [Table 3](#)) were
50 obtained by fitting the shear stress-shear rate curves with the Bingham model. The individual effects
52 of MEA, SRA, and SP on the dynamic rheological parameters were illustrated by single-factor
53 analyses. Afterwards, the analyses based on response surface methodology were conducted on the
54 dynamic yield stress and plastic viscosity.
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233 3.1.1 Single-factor analyses

234 Based on the variables and levels listed in Table 2, the single-factor analyses of the dynamic yield
 235 stress and plastic viscosity were conducted. It is worth mentioning that the SP dosage was fixed at
 236 0.2% for the single-factor test on MEA and SRA to ensure the paste is flowable enough for the
 237 dynamic shearing test. The effects of the individual use of SP, MEA, and SRA in LHC pastes are
 238 shown in Fig. 3. The results show that the addition of SP favours the flowability of LHC paste, where
 239 both dynamic yield stress and plastic viscosity decrease significantly with the dosage of SP. The effect
 240 of MEA on dynamic yield stress and plastic viscosity is consistent with the review in the introduction
 241 part that MEA aggravates the flocculation and increases the water demand, thus leading to the increase
 242 of dynamic yield stress and plastic viscosity. In comparison with the other two factors, it is apparent
 243 that SRA exhibits a more complicated effect. At the given dosage range of SRA (1.5%-2.5%), the
 244 extremum values are observed at an intermediate dosage, i.e. the minimum of dynamic yield stress
 245 and the maximum of plastic viscosity. With the increase of SRA dosage, the dynamic yield stress
 246 decreases first and then increases, whereas the plastic viscosity increases first and then decreases.

247 From the single-factor analyses as presented in Fig. 3, a declined trend with SP and a rising trend
 248 with MEA on both dynamic yield stress and plastic viscosity are obtained. But the role of SRA is
 249 dependent on its dosage for its nature as the water-soluble polymer, the adsorption of SRA molecules,
 250 and steric hindrance effect, as well as the lubrication effect all contribute to the dynamic rheological
 251 behaviours. A similar controversy on the effect of SRA on workability has also been reported in
 252 literature [33, 34]. Based on the single-factor analyses and measured results listed in Table 3, the
 253 dynamic yield stress and the plastic viscosity with the combined use of MEA, SRA, and SP were
 254 further analysed by response surface methodology.

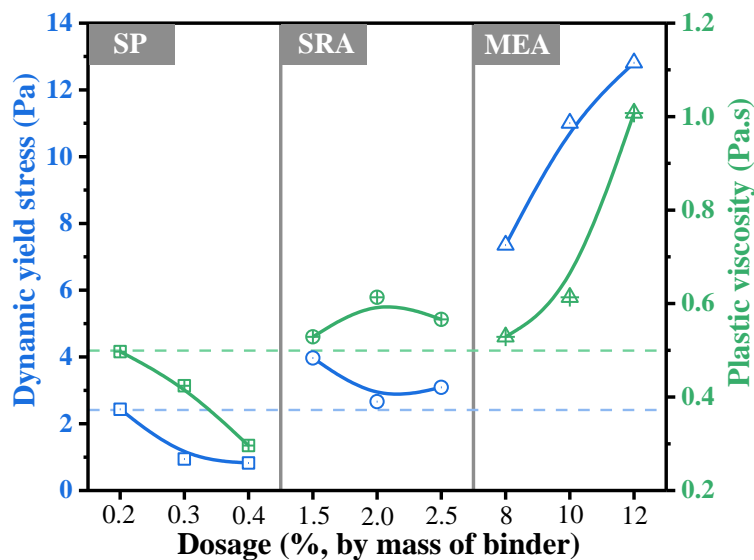


Fig. 3 Effects of SP, SRA, and MEA on dynamic yield stress and plastic viscosity of LHC paste

3.1.2 Dynamic yield stress

The response surface methodology including three variables and three levels is used to fit experimental data with a quadratic regression equation, the interactions between factors on the dependent variable can be obtained. The variables A, B, and C represent MEA, SRA, and SP, respectively. The regression model on dynamic yield stress is shown in Eq. (2). The variance analysis (ANOVA) of the dynamic yield stress is presented in Table 4, where R^2_{Adj} is a modification value of R^2 by parameters in the model. $R^2_{Adj}=0.8438$ implies that this model fits the actual data well. The relationship between the predicted values and the actual ones is shown in Fig. 4a. The value of the correlation coefficient (R^2) of the model is 0.9317, which suggests that this model well fits the experimental data. As shown in Table 4, the P-value of the regression model means whether it is statistically significant. The P-value of Lack of Fit is 0.1878, which is higher than the limit value of 0.05, indicating that the Lack of Fit is not significant in the model. Among the factors acting on the dynamic yield stress, MEA and SP are predominant factors ($P<0.01$), while SRA is not a statistically significant factor ($P\text{-value}>0.05$). In summary, the results of R^2 , R^2_{Adj} , P-value of Lack of Fit all show that the regression model is statistically significant. The contribution ratios of three factors on dynamic yield stress, obtained from the F-test and P-value, indicate that $C>A>B$, i.e. $SP>MEA>SRA$. As reflected in Fig. 4b-g, effects of variables and levels can be drawn.

$$\begin{aligned} \tau_0 = & -35.191 + 3.899A + 22.339B + 1.745C - 0.226AB + 0.062AC \\ & - 0.168BC - 0.099A^2 - 4.723B^2 - 1.264C^2 \end{aligned} \quad (2)$$

Table 4 Analysis of variance for the dynamic yield stress

Source	Sum of squares	Degree of freedom	Mean square	F-value	P-value	
Model	349.4639	9	38.82933	10.60454	0.0026	significant
A	87.19674	1	87.19674	23.814	0.0018	
B	0.920284	1	0.920284	0.251335	0.6315	
C	246.5544	1	246.5544	67.3356	< 0.0001	
AB	0.204822	1	0.204822	0.055938	0.8198	
AC	0.062313	1	0.062313	0.017018	0.8999	
BC	0.028314	1	0.028314	0.007733	0.9324	
A ²	0.662029	1	0.662029	0.180804	0.6834	
B ²	5.8706	1	5.8706	1.603299	0.2459	
C ²	6.72783	1	6.72783	1.837414	0.2174	
Residual	25.63103	7	3.661575			
Lack of Fit	16.97889	3	5.659628	2.616521	0.1878	not significant
Pure Error	8.652143	4	2.163036			

Cor Total	375.095	16
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$R^2=0.9317, R^2_{Adj}=0.8438$

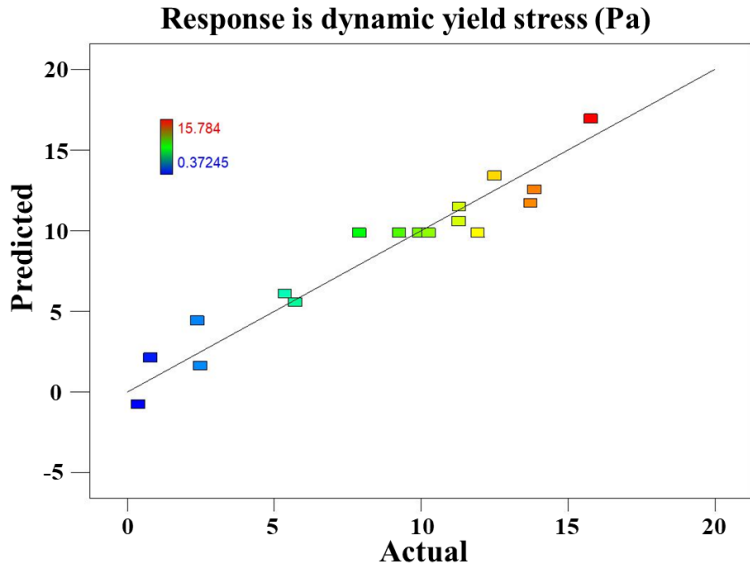
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The contour shape and the slope of the response surface, as presented in Fig. 4, reflect the significance of the interactions of any two factors among MEA, SRA, and SP. Fig. 4b and c show the interaction of SRA and MEA on the dynamic yield stress. The dosage of SRA exerts less influence and is less significant than that of MEA on the dynamic yield stress. When the dosage of MEA is fixed in the range of 8-10%, the dynamic yield stress increases first and then decreases with the increasing SRA dosage, which is contradictory with the result from single-factor analysis on the neat LHC paste.

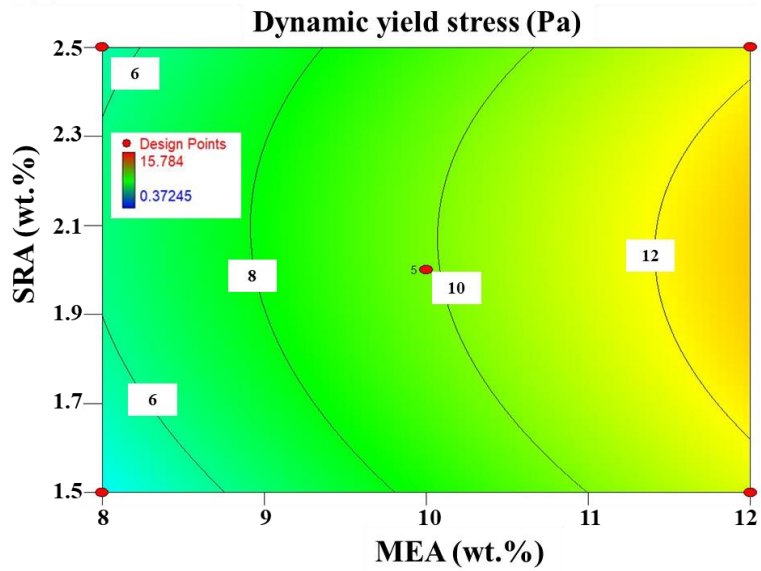
Fig. 4d and e present the interaction of SP-MEA, which is the most significant one in the model. When the content of MEA increases in the range of 8-12%, the dynamic yield stress greatly increases. While the opposite trend is observed with the increasing SP dosage. When the contents of SP and MEA are kept at a certain proportion, the dynamic yield stress holds steady (e.g. the blend with 10% MEA and 0.3% SP has nearly equal dynamic yield stress with the blend with 12% MEA and 0.4% SP).

Fig. 4f and g show the moderate interaction between SP and SRA. The effect of SP on the dynamic yield stress is influenced by the SRA dosage. Namely, when the SP dosage is fixed in the range of 0.2-0.4%, the dynamic yield stress increases first and then decreases with the increasing SRA dosage. In other words, the effect of SRA is also altered by SP due to the potential interactions between polymers. The result is also contradictory with the effect of SRA on LHC paste from the single-factor analysis.

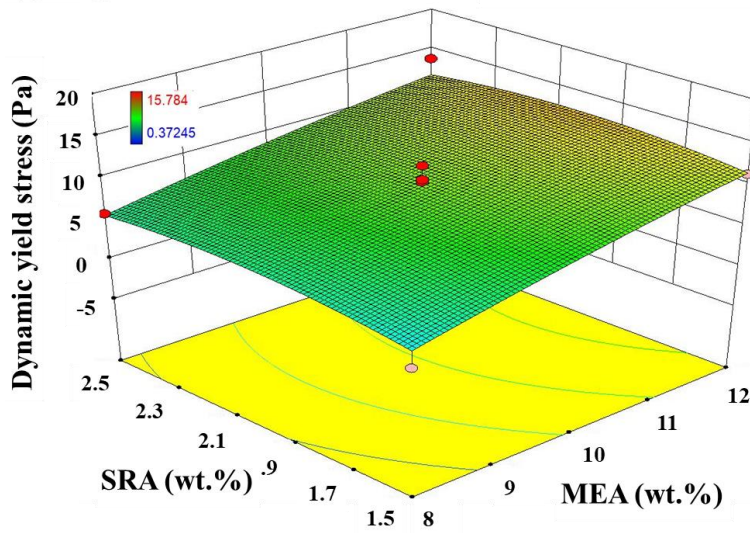
(a) Relation between predicted and actual values



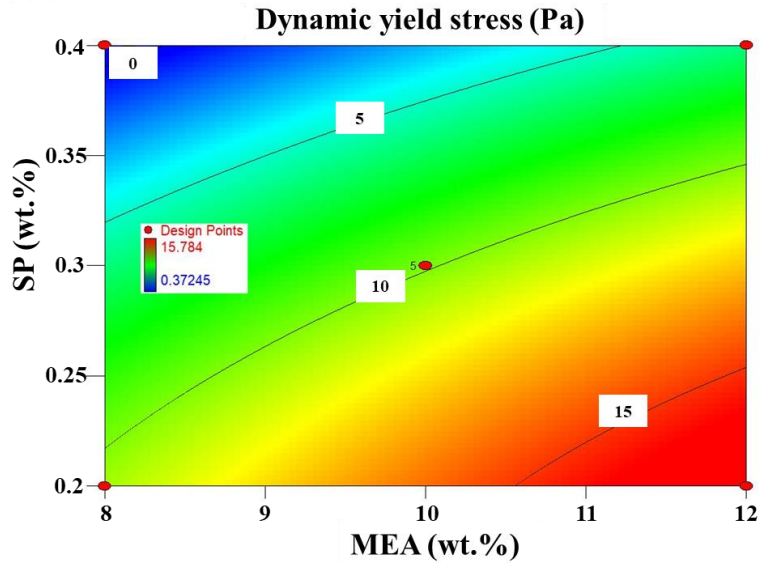
(b) Contour of AB



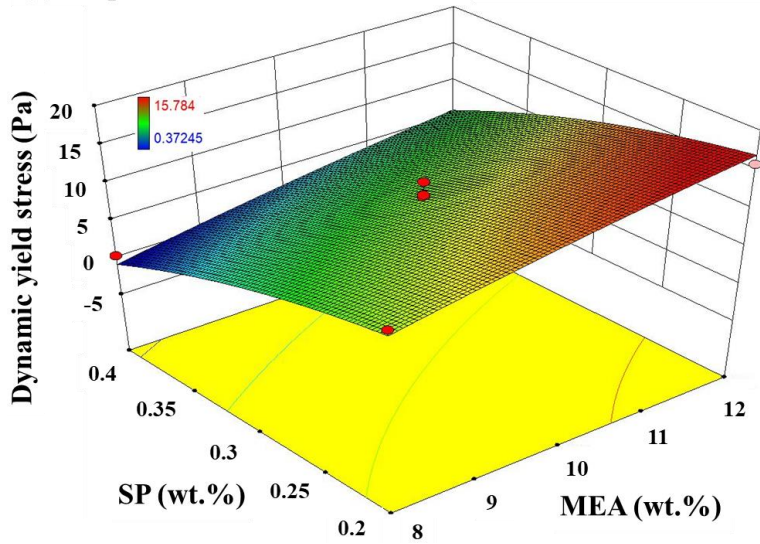
(c) Response surface of AB



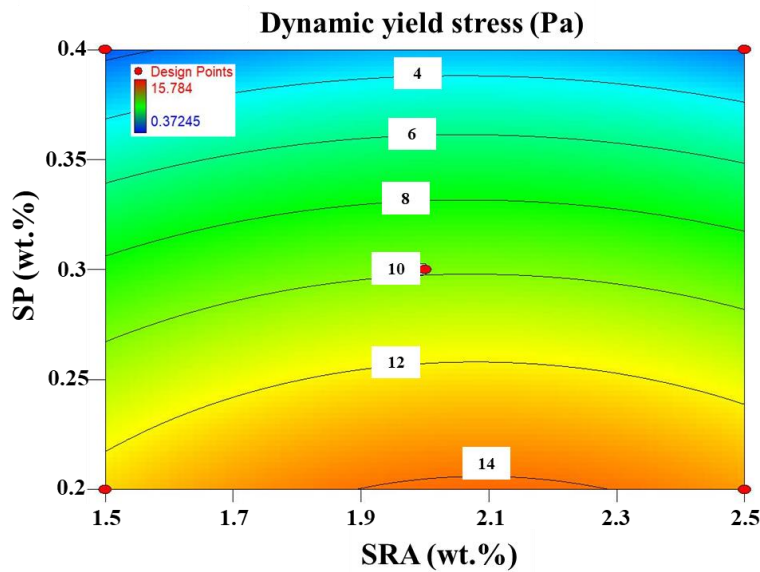
(d) Contour of AC



(e) Response surface of AC



(f) Contour of BC



(g) Response surface of BC

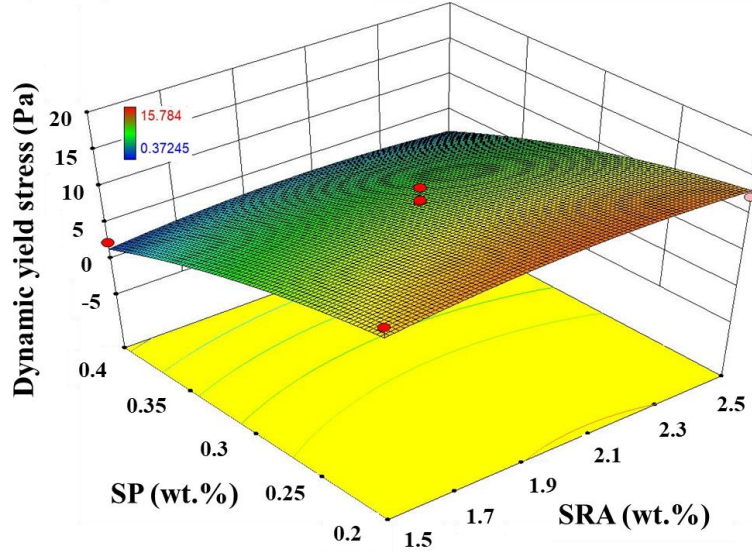


Fig. 4 Data obtained from the regression model of the dynamic yield stress

3.1.3 Plastic viscosity

The regression model of the plastic viscosity is shown in Eq. (3). The variables A, B and, C stand for MEA, SRA, and SP respectively. Table 5 presents the variance analysis (ANOVA) of plastic viscosity. Among three factors acting on the plastic viscosity, MEA and SP are predominant factors ($P < 0.01$), SRA is not a statistically significant factor. The relationship between the predicted values and the actual ones is shown in Fig. 5a. The data shown in Table 5 and Fig. 5a indicate that the model is statistically significant and can fit the experimental data. But the correlation between predicted values and the actual plastic viscosity is poorer than the former model. Moreover, $R^2_{Adj} = 0.6364$ means that the goodness of fit of this model is also poorer. The reason can be attributed to that the measured pastes are highly flowable and some fitted plastic viscosity values are close to each other, thereby affecting the model sensitivity with variables. Based on results from F-test, the contribution ratios of three factors on plastic viscosity are as follows: $C > A > B$, i.e. $SP > MEA > SRA$. As reflected in Figs. 5b-g, effects of variables and levels on the plastic viscosity can be drawn.

$$\begin{aligned} \mu = & 1.107 - 0.191A + 0.836B - 0.218C - 0.015AB + 0.018AC - 0.014BC \\ & + 0.012A^2 - 0.139B^2 - 0.015C^2 \end{aligned} \quad (3)$$

Table 5 Analysis of variance for the plastic viscosity

Source	Sum of squares	Degree of freedom	Mean square	F-value	P-value	
Model	0.388668	9	0.043185	4.11185	0.0378	significant
A	0.152449	1	0.152449	14.51525	0.0066	
B	0.015811	1	0.015811	1.505438	0.2595	

C	0.199676	1	0.199676	19.01201	0.0033	
AB	0.000886	1	0.000886	0.084355	0.7799	
AC	0.004966	1	0.004966	0.472835	0.5138	
BC	0.000186	1	0.000186	0.017744	0.8978	
A ²	0.009432	1	0.009432	0.898033	0.3749	
B ²	0.005113	1	0.005113	0.486809	0.5079	
C ²	0.000921	1	0.000921	0.087684	0.7757	
Residual	0.073519	7	0.010503			
Lack of Fit	0.057688	3	0.019229	4.858654	0.0804	not significant
Pure Error	0.015831	4	0.003958			
Cor Total	0.462186	16				
R ² =0.8409, R ² _{Adj} =0.6364						

Fig. 5 presents the significance of the interactions among three factors on the plastic viscosity.

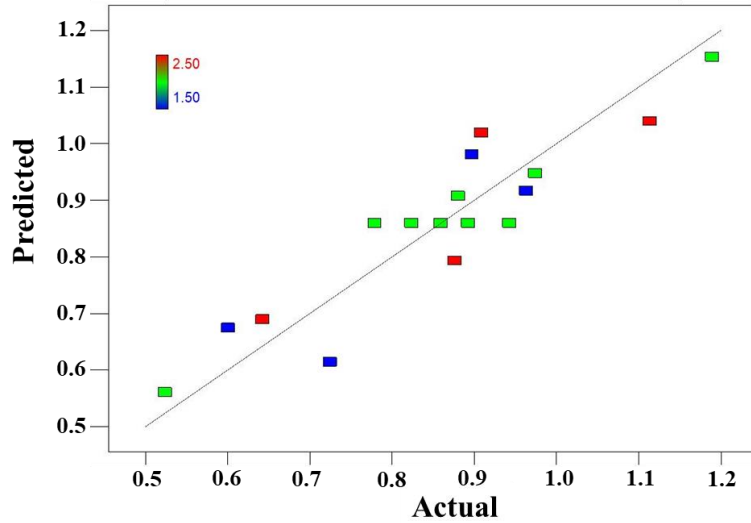
Fig. 5b and c show the effect of SRA on the plastic viscosity in presence of MEA. With a high dosage of MEA in the range of 10-12%, the plastic viscosity increases first and then slightly decreases with SRA dosage, which is consistent with the single-factor analysis. With a low dosage of MEA in the range of 8-10%, the plastic viscosity increases more sharply with the increasing SRA dosage.

Similarly, the interaction between SP and MEA also shows the highest significance, as seen in Fig. 5d and e, the plastic viscosity increases with the increasing content of MEA but decreases with SP addition. In Fig. 5f and g, when the SP dosage is kept constant, the plastic viscosity growth first increases with the increasing SRA content and then slightly decreases, which is also consistent with the single-factor analysis.

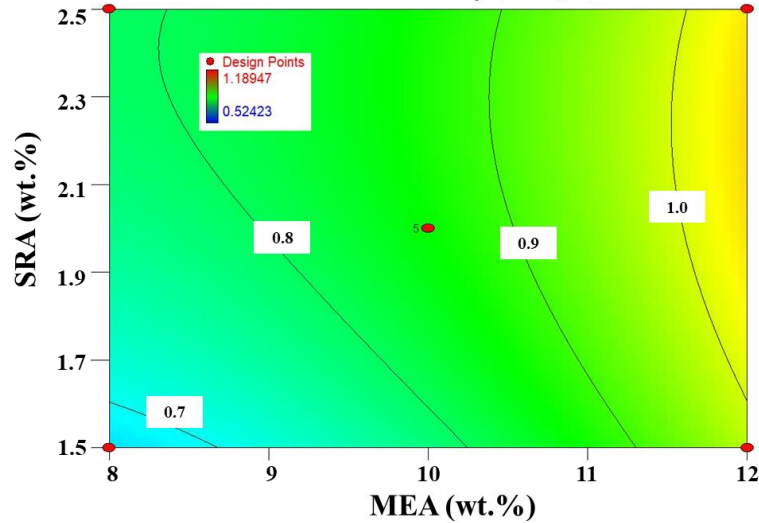
The interactions between MEA, SRA, and SP affected the dynamic rheological properties and were resolved by response surface analyses. Concerning LHC pastes with MEA addition, MEA enlarges the water demand of the powder materials, thereby increasing the dynamic yield stress and plastic viscosity. In both fresh and hardened cement-based materials, the mechanisms of SP and SRA are summarized as adsorptions of molecules on air-liquid and liquid-solid interfaces [46]. It is apparent from the single-factor analyses (see Fig. 3) that SRA decreases first then increases the dynamic yield stress of neat LHC paste, however, an opposite trend on the plastic viscosity is observed. But the interactions of MEA-SRA and SP-SRA, as seen in Fig. 4 and 5, show different roles of SRA in LHC paste with MEA in comparison with the single-factor analyses on neat LHC paste. The dynamic yield stress and plastic viscosity both increase first then decrease with SRA dosage. Based on those experimental findings above, the principle on designing the initial flowability of LHC paste with MEA, SP, and SRA can be drawn.

345 However, the use of MEA seems to change the effect of SRA on the dynamic yield stress in
 346 presence of SP, the mechanism is still unclear. In Fig. 5b, we find that the plastic viscosity increases
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 347 with SRA dosage at relatively low MEA content; But the plastic viscosity barely changes at relatively
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 348 high MEA content. Therefore, the zeta potential values of LHC paste and fresh blends of LHC and
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 349 MEA were measured to further revealing the interaction of SP and SRA.

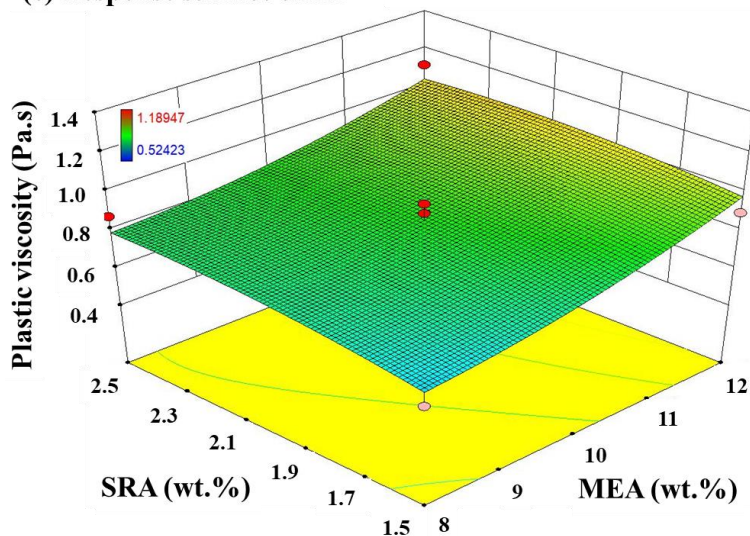
(a) Relation between predicted and actual values
 Response is plastic viscosity (Pa.s)



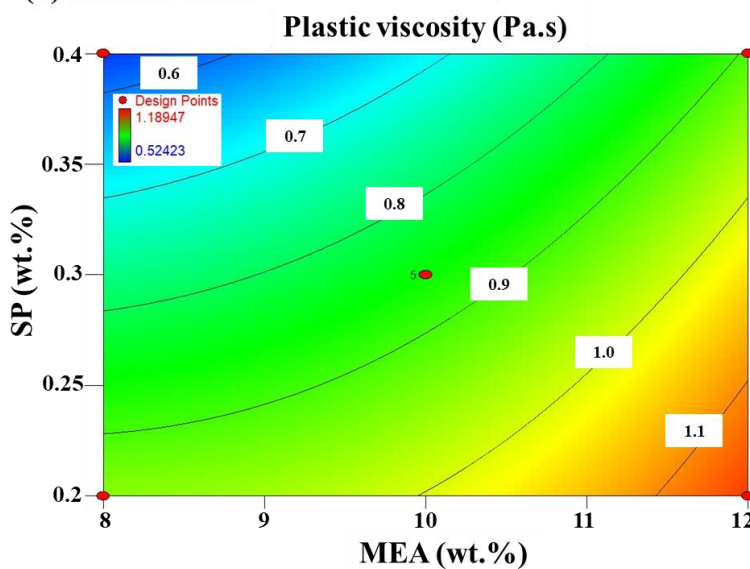
(b) Contour of AB
 Plastic viscosity (Pa.s)



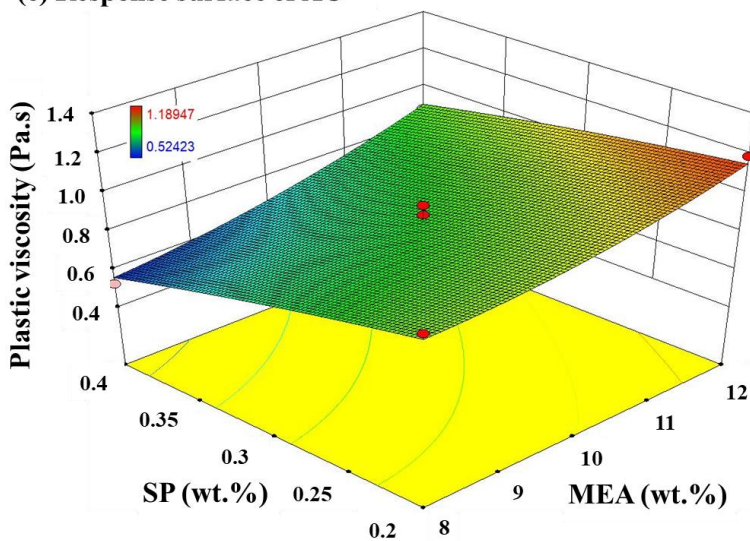
(c) Response surface of AB



(d) Contour of AC



(e) Response surface of AC



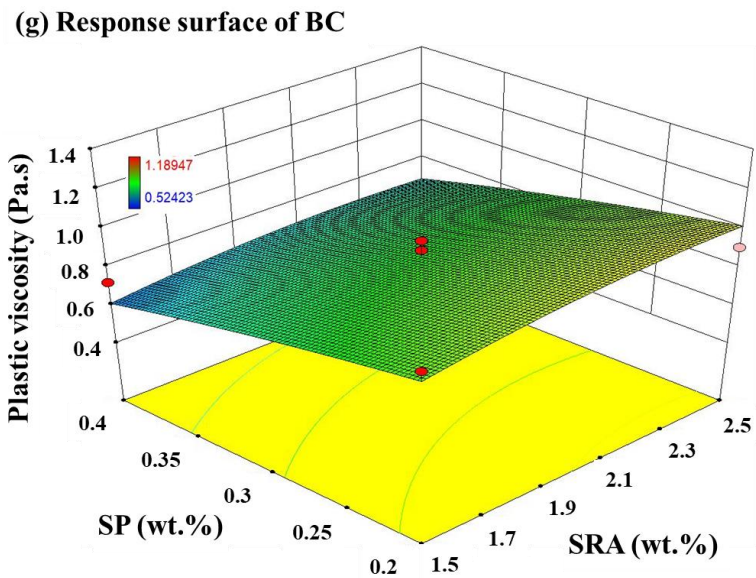
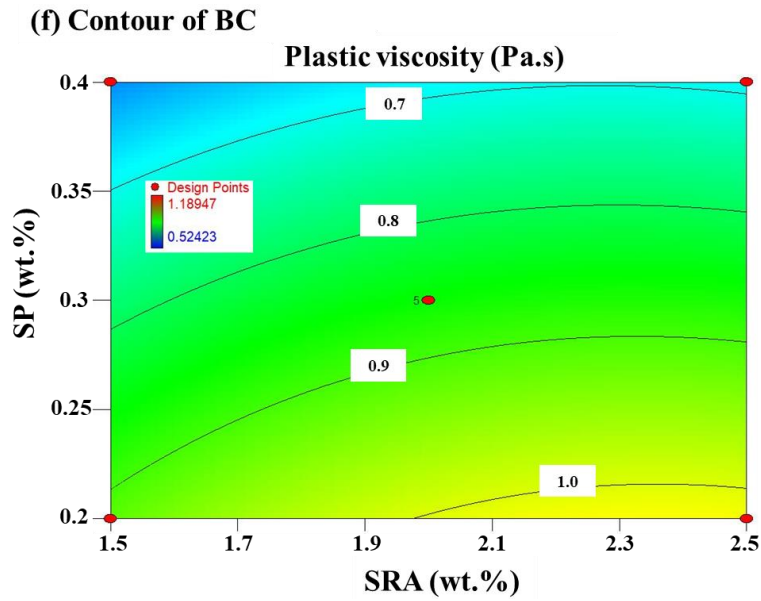


Fig. 5 Data obtained from the regression model of the plastic viscosity

3.1.4 Roles of SP and SRA

Fig. 6 shows the effects of SRA and SP on the zeta potential of two suspensions, i.e. neat LHC and blend of 90% LHC and 10% MEA, with a W/P ratio of 10. As seen in Fig. 6a, the zeta potential values of the two suspensions are all positive. The zeta potential values of the latter suspension are significantly higher, because the surface charge of MgO grain is much higher than that of the cement grains [30], thereby resulting in a higher zeta potential value of LHC-MEA suspension than that of LHC suspension.

In Fig. 6 there is a clear trend that the zeta potential value gradually decreases with the increasing dosage of SP, while it basically remains unchanged with SRA addition. To evaluate the possible competitive adsorption between SP and SRA molecules on the particle surface in suspensions, different adding sequences of SP and SRA were adopted for the sample preparation for zeta potential

369 tests. Three adding sequences listed in Fig. 6b are as follows: (1)-SP and SRA were premixed in water
370 before preparing the suspension; (2)-Only SRA was premixed in water to prepare the suspension, SP
2 was added to the well-mixed suspension, and stirred for another 2 min; (3)-Only SP was premixed in
371 water to prepare the suspension, no SRA was used.
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373 As shown in Fig. 6b, no significant difference is found on the zeta potential with the first two
8 adding sequences of SP. The premixed SP and SRA, i.e. adding sequence (1), only slightly increases
374 the zeta potential at high SP dosages (0.3% and 0.4%) than that of the subsequent addition of SP, i.e.
10 the zeta potential at high SP dosages (0.3% and 0.4%) than that of the subsequent addition of SP, i.e.
11 adding sequence (2). Plank et al. [16] reported the competitive adsorption of SP and retarder
12 molecules in cement suspension. The adsorptions of SP or retarder both lead to a notable variation
13 trend of zeta potential by changing the surface charge density. In this paper, the highest dosage of
14 SRA is 2.5% by mass of binder, which is much higher than that of SP and can reach the amount of
15 saturation adsorption. However, as shown in Fig. 6a, no significant difference in the zeta potential is
16 observed with the increasing SRA dosage, it can be expected that the SRA molecule is not adsorbable
17 or the adsorbed SRA does not change the surface charge of particles in above suspensions.
18 Nevertheless, results presented in Fig. 6b show that the combined use of SRA and SP results in higher
19 zeta potential values in comparison with the individual use of SP. The result confirms the adsorption
20 of SRA on the particle surface or on the SP molecule, which can change the zeta potential of
21 suspensions with SP. Therefore, no evident competitive adsorption between SP and SRA is observed
22 from zeta potential results as presented in Fig. 6b.
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388 Generally, high absolute values of the zeta potential contribute to a repulsive force and dispersion
39 of particles in suspension, thereby improving the flowability of paste. In the above suspensions, SP
40 decreases the absolute values of zeta potential with the increasing dosage. It is attributed to the
41 adsorption of charged SP molecules on the particle surface [16], then the steric hindrance effect of SP
42 notably increases the flowability. The roles of SP and SRA molecules in blends can be concluded as
43 adsorbing on particle surface, changing the surface-to-surface separation distance, and interstitial
44 fluid viscosity [29]. Due to the effect of preferential adsorption, the larger molecules (i.e. the comb-
45 type polymer of SP in this paper) tend to adsorb on the cement grain surface, while the smaller
46 molecules (i.e. the linear polymer of SRA in this paper) are left in the pore solution. Moreover, Fig.
47 6b shows that SRA may also adsorb on the SP molecules that are adsorbed on the cement grains [47],
48 thereby resulting to a different result of adding sequence (1) from the other two. Then the combined
49 effect of SRA and SP can be explained by roles of “adsorbing polymer” and “nonadsorbing polymer”
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400 as described in [29][47]. At low SRA dosage, SRA molecules partially adsorb and partially disperse
 401 in the pore solution, the adsorbed SRA molecules leads to lower zeta potential values, while
 402 nonadsorbing SRA molecules contributes to the depletion flocculation of particles [47], thereby
 403 increasing the yield stress and viscosity. At high dosage, nonadsorbing SRA molecules increase with
 404 the SRA dosage and decrease the interstitial fluid viscosity at the constant solid volume fraction,
 405 which slightly reduces the friction in the suspension and favours the flowability. However, the average
 406 surface-to-surface separation distance also changes with the polymer dosage and is a function of the
 407 initial solid volume fraction, thus, this is the reason that addition of MEA changes the effect of SRA
 408 on dynamic parameters in neat LHC paste.

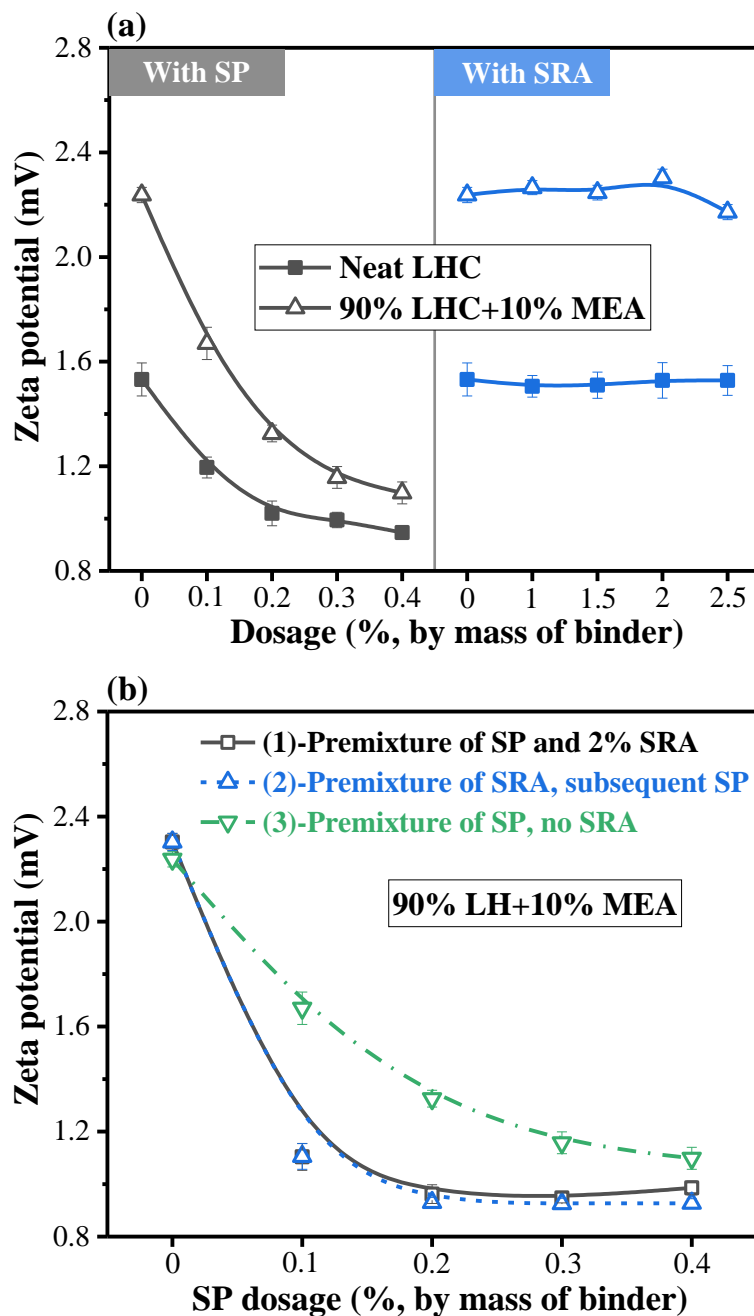


Fig. 6 Zeta potential of suspensions with W/P ratio of 10

412 3.2 Static rheological parameters

413 3.2.1 Evolution of static yield stress

414 The evolution of static yield stress is usually related to the structural build-up of cement paste
415 [40, 41, 48], which is considered as the key parameter for 3D printing [49, 50], formwork pressure
416 [51], and distinct layer casting [52] of cement-based materials. The evolution of static yield stress
417 with the elapsed time of blends is shown in Fig. 7. The parameters are further summarized in Table
418 4, where the growth rate is denoted as the slope in 20-120 min. With the increase of SRA from 0 to
419 2%, the growth rate increases by 1.15 times as well as the peak value by 1.04 times of the static yield
420 stress of the LHC paste. As mentioned above, the addition of 10% MEA decreases the flowability and
421 increases the dynamic yield stress of pastes, as a result, the initial static yield stress (at 10 min) also
422 increases. With regard to the static yield stress development as shown in Table 4, the peak value and
423 growth rate of the LHC paste are increased by 1.68 times and 1.56 times respectively with 10% MEA.
424 Moreover, a positive correlation between the growth rate of static yield stress and MEA content is
425 observed. As shown in Table 1, the main component of MEA, MgO, reacts with water in an alkaline
426 solution to form brucite, i.e. $\text{Mg}(\text{OH})_2$. The brucite crystals grow on the surface of MgO particles and
427 increase the surface roughness. With the hydration going on, the particle interactions as well as the
428 bridging effect of brucite crystals and other hydrates contribute to the more rapid development of
429 static yield stress.

430 Interestingly, a comparison of M10S0P2 and M10S2P2 reveals that SRA is more effective in
431 accelerating the static yield stress growth in blends of LHC and MEA than that of LHC paste, of
432 which the nominal values are 2.33/1.68 vs. 1.15/1.00 respectively. As mentioned above, with the
433 increasing dosage of SRA, the dynamic yield stress increases first and then decreases in LHC-MEA
434 blends. However, an opposite trend with the increasing SRA dosage was observed in neat LHC paste.
435 By contrast, adding 2% SRA significantly increases the growth rate of the static yield stress of pure
436 LHC paste and blends of LHC and MEA. The physical definitions of the dynamic yield stress and
437 static yield stress are similar, which correspond to the stress that the paste starts to flow, but the test
438 procedures are quite different [39]. As shown in Figs. 3 and 4, the effect of SRA on the dynamic yield
439 stress is mainly involved in the physical interaction of SRA molecules and the cement suspension, it
440 cannot account for the increasing growth rate of the static yield stress which is a complex
441 physicochemical process. The reason may be those hydration products in LHC and blends of LHC
442 and MEA are all affected by SRA [6, 30, 31], while the reaction of MEA is also affected at the early

443 age, the mechanisms will be discussed later.

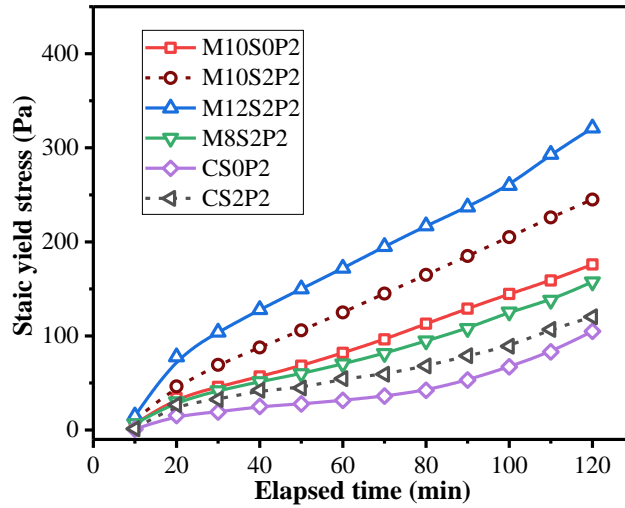


Fig. 7 Evolution of static yield stress of blends

Table 4 Parameters of blended pastes by static shearing tests

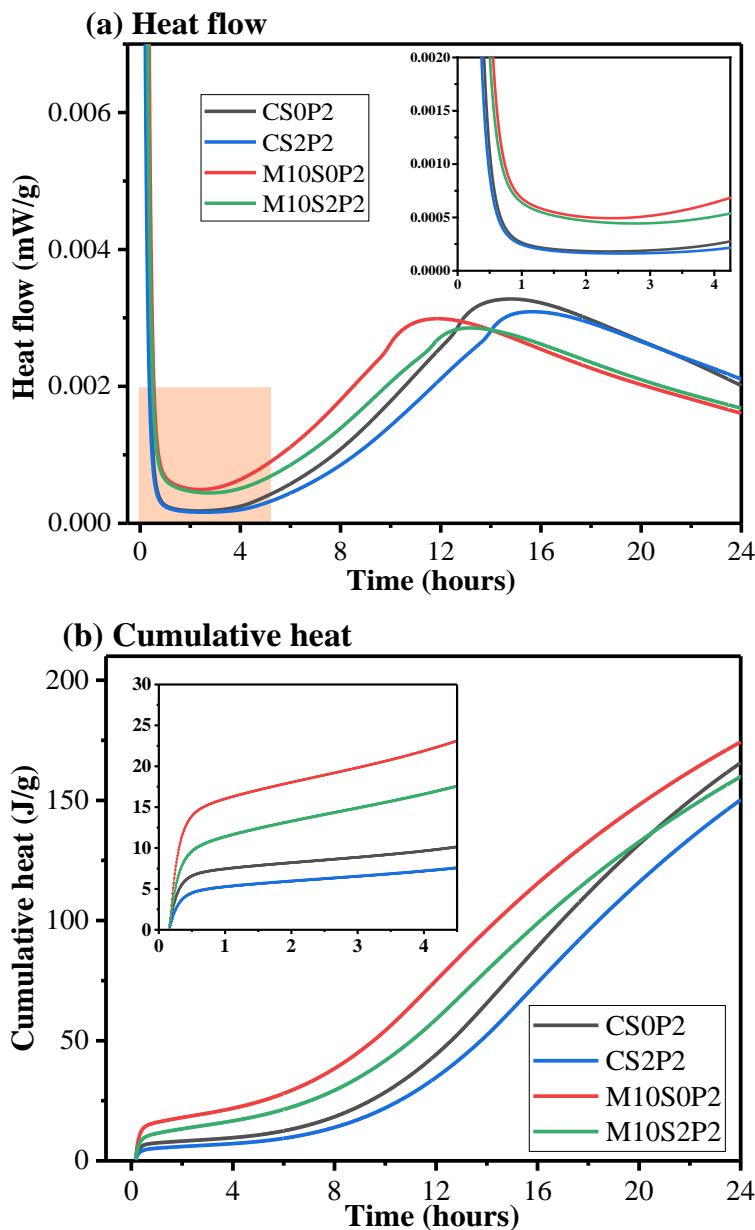
Mix	Peak value (Pa)		Growth rate (Pa/min)	
	Measured value	Nominal value	Measured value	Nominal value
CS0P2	105.0	1.00	0.90	1.00
CS2P2	120.3	1.15	0.93	1.04
M10S0P2	176.0	1.68	1.42	1.58
M10S2P2	245.0	2.33	1.99	2.22
M8S2P2	157.5	1.50	1.27	1.42
M12S2P2	321.0	3.06	2.43	2.72

3.2.2 Hydration and solid phase assemblage

The calorimetric results are shown in Fig. 8, in which the dosage of SP is fixed at 0.2%, the single or combined effects of MEA and SRA are detected on the hydration of LHC with SP. With 10% MEA addition, the induction period is shortened and the initial cumulative heat increases, and time to reach the main peak and the peak value of the heat release rate are reduced. As a comparison, SRA retards the hydration process of LHC and leads to lower initial heat and more gradual acceleration, the main exothermic peak is delayed and the cumulative heat decreases. In comparison with CS2P2, the induction period of M10S2P2 is shortened, and the main exothermic peak appears earlier.

In summary, MEA accelerates the hydration of LHC but the accelerating effect is weakened at the later age on the cumulative heat, while SRA shows a notable retarding effect during the test period. When MEA and SRA are used simultaneously, their effects are time-dependent. In the first 4 h, the reaction of MgO promotes the heat release and shortens the induction period. During the period of 4-

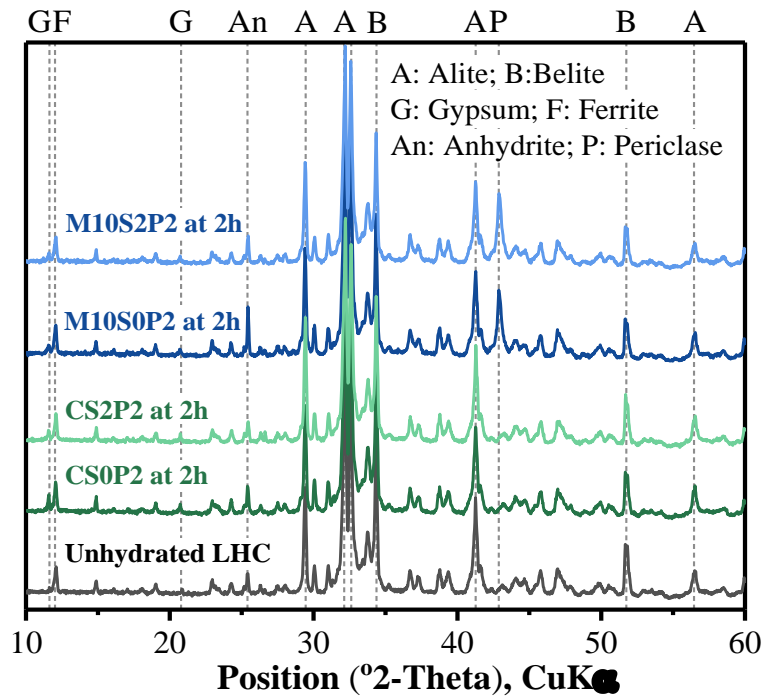
460 16 h, the retarding effect of SRA appears, thus affecting the exothermic peak and reducing the
 461 cumulative heat. During the period of 16-24 h, SRA shows the negligible effect on the exothermic
 2 rate, exothermic rates of LHC pastes are even higher than that of LHC and MEA blends, and their
 462 exothermic rates of LHC pastes are even higher than that of LHC and MEA blends, and their
 4 cumulative heat approaches gradually.
 463 cumulative heat approaches gradually.



465
 466 **Fig. 8** Hydration heat of blends composed of LHC, MEA, and SRA with SP

467 To assess the solid phase compositions of blends, XRD, and TGA were conducted on hydrated
 468 blends. To identify the hydration products, XRD tests were carried out first. Fig. 9 shows the XRD
 469 patterns of unhydrated LHC, hydrated blends with and without SRA. As shown in the figure, the main
 470 diffraction peaks are unhydrated clinkers and periclase, i.e. MgO. The reaction product of MEA, i.e.
 471 brucite, is not clearly observed. Moreover, the main hydrates of cement, as well as the effect of SRA
 472 are also not observed from the patterns. León-Reina [53] reported that the precision of the Rietveld

473 analysis varies from 0.6-1.2 wt.% for some crystalline phases of cement hydration products. In this
 474 study, only a small amount of clinkers is consumed in the first 2h, so the same for the formation of
 475 brucite and other hydrates of LHC. Therefore, it's difficult to directly determine the formation amount
 476 of cement hydrates and $Mg(OH)_2$ by Quantitative XRD at a very early age. As a complementary
 477 technique, TGA was used to quantitatively measure the contents of $Ca(OH)_2$ and $Mg(OH)_2$ at 0-2 h.



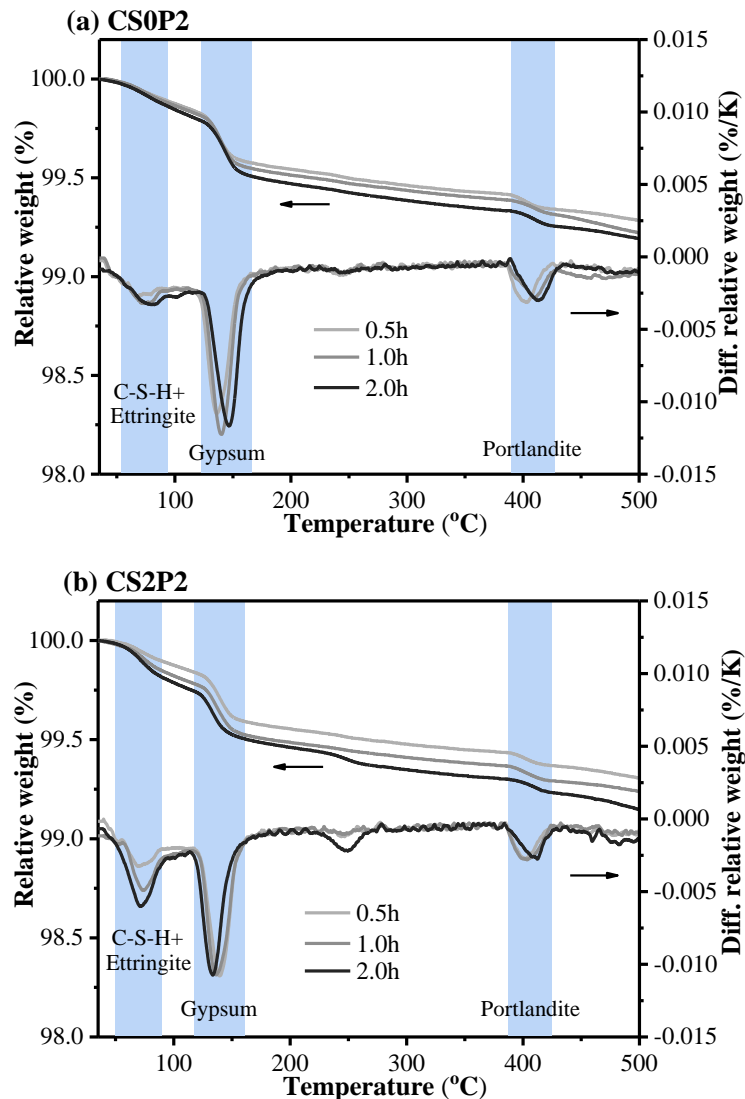
478 **Fig. 9** The XRD patterns of blends composed of LHC, MEA, and SRA with SP (A=Alite, B=Blite,
 479 F=Ferrite, P=Periclase, G=Gypsum, An=Anhydrite)

481 **Fig. 10** shows the TGA results of blends with and without SRA cured for different ages. As seen
 482 in **Fig. 10a** to **d**, there are 3 main decomposition peaks in LHC blends, and 4 peaks in blends of LHC
 483 and MEA. CSH and/or ettringite decompose at around 90 °C, the weight loss between 120-170 °C is
 484 attributed to the decomposition of gypsum. The peaks around 340 °C and around 420 °C stems from
 485 the decomposition of brucite and portlandite, respectively.

486 Generally, structural build-up, i.e. evolution of static yield stress in this paper, is considered as
 487 closely relating to the hydrate amount of cement, mainly C-S-H [35, 54] and ettringite [42]. However,
 488 it is difficult to quantitatively analyse the solid phase change of Portland cement at a very early age.
 489 The contents of $Ca(OH)_2$ and $Mg(OH)_2$ in this paper were used to reflect the reaction degree of LHC
 490 and MEA, respectively. As shown in **Fig. 10a** and **b**, adding 2% SRA retards the hydration process of
 491 LHC. The portlandite content in the first 2 hours is reduced due to the retarding effect of SRA, but
 492 the static yield stress notably increases during this period. Similarly, the results presented in **Fig. 10c**
 493 and **d** show that the contents of $Mg(OH)_2$ are also affected by SRA at 0.5-2h. The contents of $Ca(OH)_2$

494 and $\text{Mg}(\text{OH})_2$ are further summarized in Fig. 10e. As seen in Fig. 10e, adding MEA leads to more
 495 $\text{Ca}(\text{OH})_2$ formation, which confirms the acceleration effect of MEA on LHC hydration. In the
 496 previous section, the acceleration effect on the static yield stress growth by MEA is attributed to the
 497 hydration product, $\text{Mg}(\text{OH})_2$. It's worth noting that the content of $\text{Mg}(\text{OH})_2$ from Fig. 10e is around
 498 three times of $\text{Ca}(\text{OH})_2$ in M10S0P2 and M10S2P2. The formation of $\text{Mg}(\text{OH})_2$ seems to play an
 499 important role in promoting the growth of static yield stress in fresh blended pastes.

500 Fig. 10e also presents that 2% SRA significantly reduces the amount of $\text{Mg}(\text{OH})_2$ as detected by
 501 TGA. Moreover, $\text{Ca}(\text{OH})_2$ contents in the neat LHC paste and blends of LHC and MEA are all reduced
 502 by SRA. With less amount of reaction products, why do M10S2P2 exert an even much higher growth
 503 rate of the static yield stress? To answer this question, the zeta potential of re-dispersed suspensions,
 504 BET analysis, and SEM observations were further conducted.



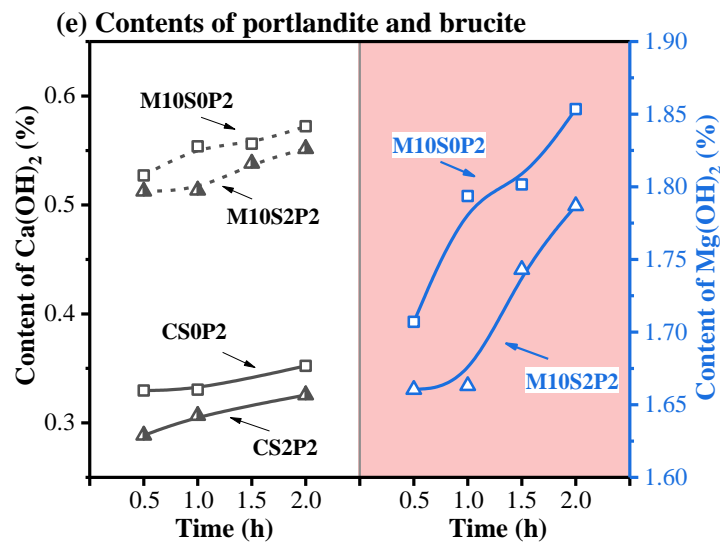
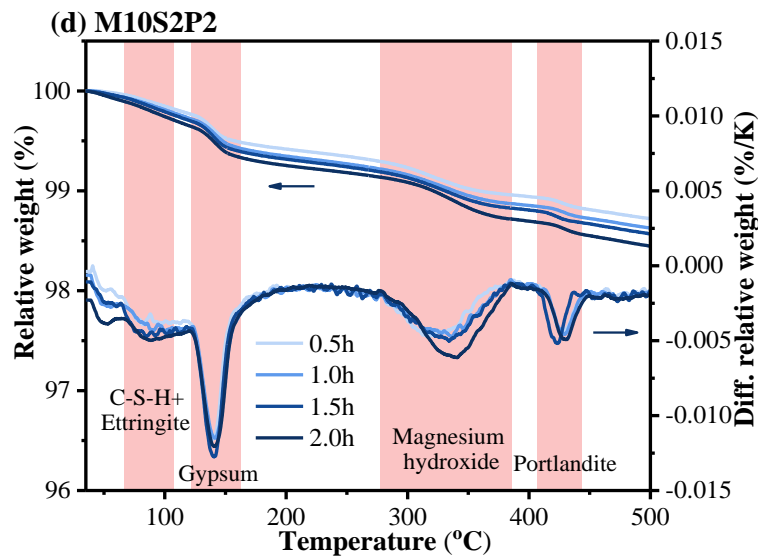
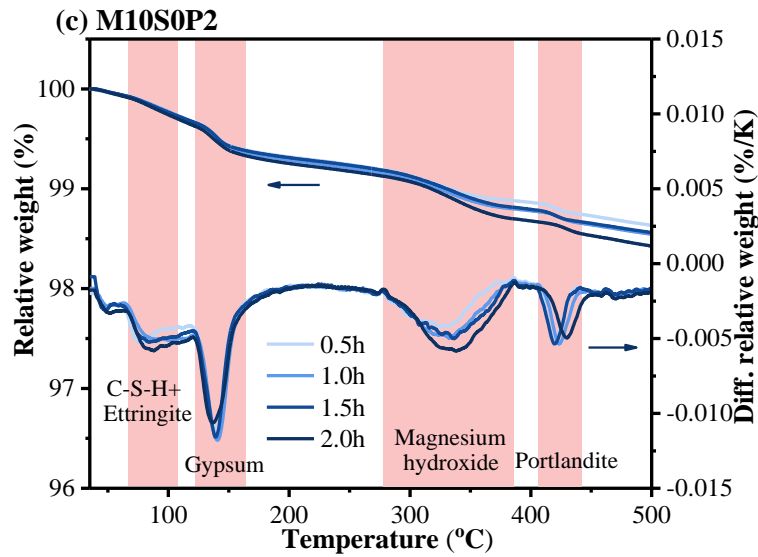


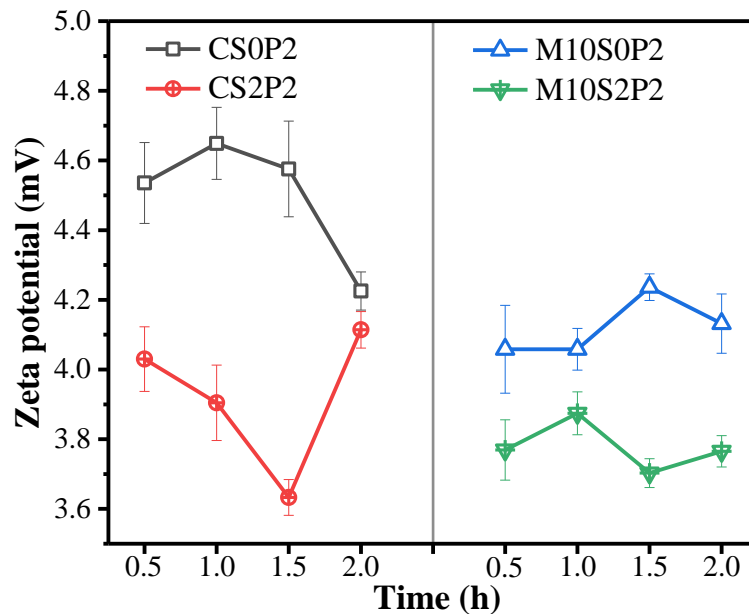
Fig. 10 TGA results of the hydrated blends of LHC and MEA with/without SRA

3.2.3 Zeta potential of re-dispersed suspensions

Fig. 11 shows zeta potential values of re-dispersed suspensions of powder samples hydrating for

513 different ages with the W/P ratio of 50. Generally, the measurement of Zeta potential is conducted on
514 the diluted suspensions to ensure the test precision. However, the hydration process of cement in the
2 diluted suspensions is far different from the actual condition
515

516 Zeta potential values of the four samples are all positive. For CS0P2, the zeta potential value
517 increases first and then decreases with the elapsed time. As reported by Huang et al. [42], the zeta
518 potential of particles from alite paste shows a similar trend with results in this paper, the authors found
10 that the CSH fraction in the solid phase is linearly related with the reduction of zeta potential values
519 because of the deprotonation of surface silanol groups [55]. In M10S0P2, the zeta potential also
12 increases first then decreases with time. However, adding SRA changes it into a basically inverse
13 trend. Doubtlessly, the results confirm that SRA notably changes the surface characteristic of particles
14 in hydrated blends, this seems to be the reason for the dramatical variation of the static yield stress.
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524
525 **Fig. 11** Zeta potential values of re-dispersed suspensions at W/P ratio of 50

526 3.2.4 Microstructure morphology of hydrated blends

527 As seen in previous sections, one of the main hydration products, $Mg(OH)_2$, in LHC-MEA blends
528 makes it more evident to find the correlation between the evolution of static yield stress and the
49 hydrates amount. Results as shown in Fig. 10e confirm that SRA retards the reaction of MgO , however,
50 promotes the static yield stress development of blends even though the hydrate amount is lower. To
51 better understand the effect of SRA on the hydration of blends, especially for the formation of
52 hydrates on the particle surface, SEM observation and BET analysis on hydrated blends were
53 conducted.
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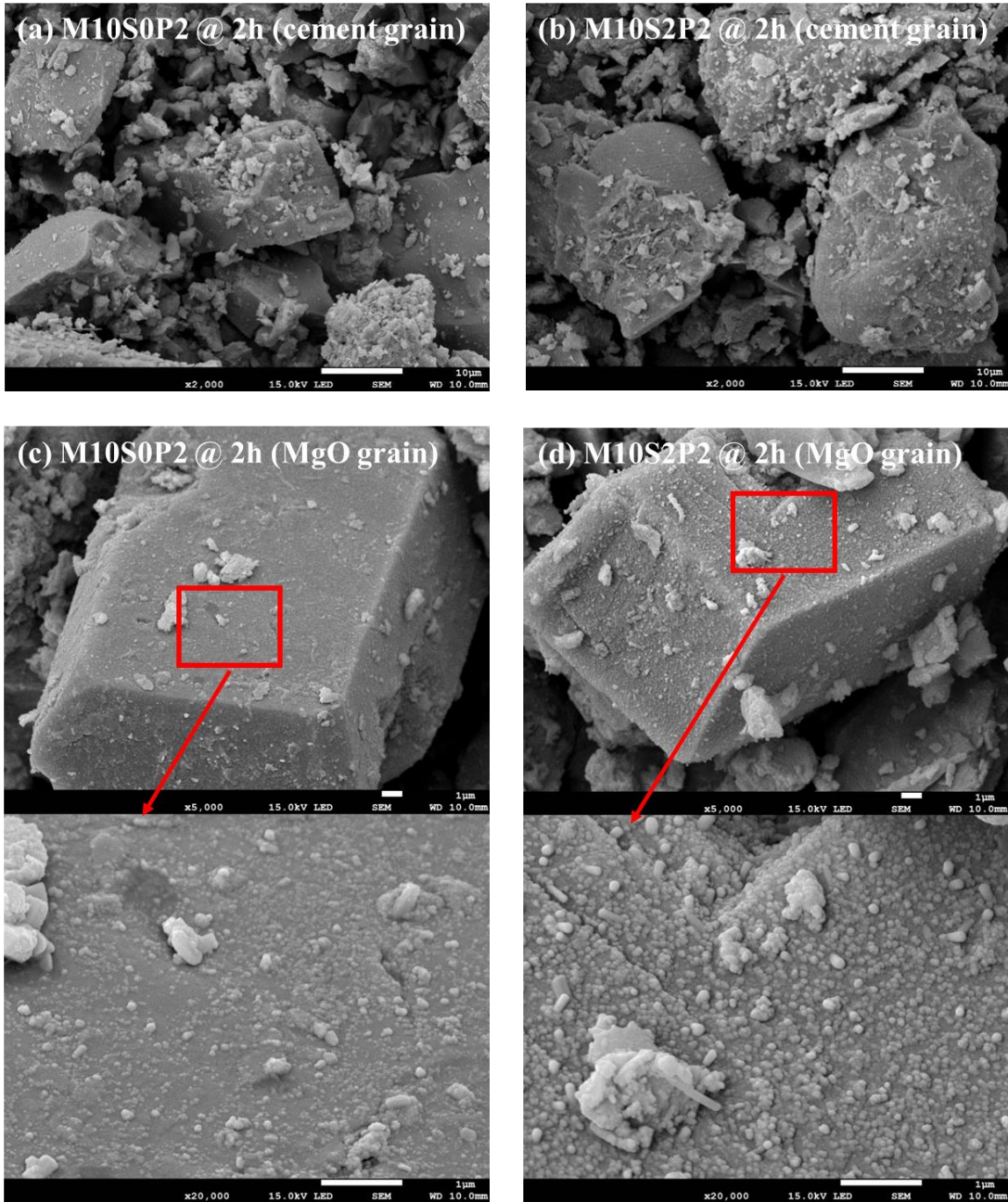


Fig. 12 SEM images of blends of LHC and MEA

Fig. 12 displays the SEM images of hydrated blends, where Fig. 12a and b correspond to cement grains of M10S0P2 and M10S2P2 hydrating for 2h, while Fig. 12c and d are referred to MgO grains of M10S0P2 and M10S2P2 hydrating for 2h. The cement grain surfaces are rough and covered with small-size hydrates. However, it is very hard to distinguish the effect of SRA on hydrate morphology. As seen in Fig. 12c and d, small brucite crystals grow on the surface of MgO grains. As to M10S2P2, the morphologies of the MgO surface at 2h are significantly changed with the addition of 2% SRA. More nucleation sites can be observed in Fig. 12d, where the MgO grain surface is covered with many small-size brucite crystals. A similar phenomenon with the hydrate morphology change has also been reported in [56], with the addition of SRA, finer crystals of hydration products are observed in

546 ordinary Portland cement system. As seen in the figure, MgO particles in M10S2P2 are covered with
 547 more and denser fine brucite crystals, and the particle interactions among solid particles are
 2 strengthened, thus increasing the growth rate of static yield stress.
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549 **Table 5** presents the specific surface area of hydrated blends and the corresponding static
 6 rheological parameters. With the addition of 10% MEA, the specific surface area of LHC paste is
 550 increased from 0.856 m²/g to 1.5707 m²/g., while the addition of SRA increases the specific surface
 551 area of both LHC paste and LHC-MEA blends. There is a clear positive relationship between the
 11 surface area and peak value, growth rate of static yield stress. Lou et al. [44] pointed out that cement
 12 with a higher hydration rate dissolves more quickly, which reduces the mean particle size and
 13 produces pores, thereby increasing the specific surface area. In this paper, the difference between
 14 CS0P2 and M10S0P2 in the surface area well correspond to their difference in hydration rate. MEA
 15 promotes the hydration of LHC-MEA blends and leads to a higher specific surface area. SRA retards
 16 the hydration process, however, contributes to more nucleation sites and amount of brucite crystals
 17 on the MgO surface, thereby producing a rougher surface and increasing the specific surface areas of
 18 CS2P2 and M10S2P2. The rougher surface contributes to stronger particle interactions and leads to
 19 faster static yield stress development.
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33 **Table 5** Effect of admixture on the specific surface area of hydrated cement pastes
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Sample at 2h	Surface area of cement paste (m ² /g)	Evolution of static yield stress	
		Peak value (Pa)	Growth rate (Pa/min)
CS0P2	0.8560	105.0	0.90
CS2P2	0.9671	120.3	0.93
M10S0P2	1.5707	176.0	1.42
M10S2P2	1.5935	245.0	1.99

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Based on the results above, the effects of MEA and SRA on the time-dependent behaviour of LHC pastes can be summarised. The hydration of MgO is a typical process of dissolution and crystallization. MgO first dissolves and diffuses into the pore solution and forms the oversaturated solution. Then the formation of Mg(OH)₂ takes place at nucleation sites near the MgO grains, such as the MgO grain surface, boundary, and inner pores. The whole hydration process is seen as the self-expansion of MEA particles [3]. Due to the effect of alkali, the size of Mg(OH)₂ hydrating in cement pore solution is smaller and more irregular than in pure water [57]. Also, the oversaturation, the sites of nucleation and growth, and the morphology of Mg(OH)₂ are reported to be affected by alkali [58].

573 SRA changes the physicochemical properties of the pore solution in the cement paste and may
574 alter the dissolution and crystallization process of periclase. As shown in Figs. 8-12, SRA retards the
2 hydration of LHC and MEA blends, changes the surface charge of hydrated particles, and reduces the
575 formation contents of $\text{Ca}(\text{OH})_2$ as well as $\text{Mg}(\text{OH})_2$. Some researchers have summarized the retarding
4 mechanisms of SRA as follows: (i) an organic molecule film is formed by SRA molecules and reduces
576 the interfacial energy, thus hindering the hydration process [59]; (ii) based on the theory of “similarity
6 and intermiscibility”, SRA reduces the polarity, as well as alkali contents and pH value, of the pore
577 solution and increases the oversaturation level [60, 61]. After mixing with the solution of water and
8 SRA, LHC and MEA grains, due to the polarity, are wetting and wrapped with a water film. Then the
578 SRA molecules adsorb on the surface. The oversaturation level in the pore solution is first reached
10 near the grain surface, however, affected by SRA. Taking MgO as an example, because of the SRA
11 concentration in the pore solution, $\text{Mg}(\text{OH})_2$ is prone to nucleating on the MgO surface rather than in
579 the boundary and inner pores. More nucleation sites appear on the surface compared with blends with
12 no SRA, but the total amount of $\text{Mg}(\text{OH})_2$ is lower. The amount and morphology of hydrates on grains
13 surface also play an important role in the time-dependent rheological behaviours.
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30 4 Conclusions

31 Based on the experimental data, the main conclusions can be drawn as follows:

32 (1) The complex interactions among MEA, SRA, and SP on the dynamic yield stress and plastic
33 viscosity are presented by the response surface methodology. The effect of SRA is dependent on the
34 dosage, while the addition of MEA changes the role of SRA on the dynamic yield stress. The zeta
35 potential tests with designed premixing procedures show no evident competitive adsorption between
36 SRA and SP. With the increasing dosage of SRA, the roles of SP and SRA are explained by “adsorbing
37 polymer” and “nonadsorbing polymer”.
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46 (2) The quantitative analysis of hydrate amount is related to the static rheological parameters.
47 MEA increases the growth rate and peak value of the static yield stress in LHC paste for accelerating
48 the early-age hydration of LHC. The content of $\text{Mg}(\text{OH})_2$ is higher than other hydrates of LHC. The
49 acceleration effect of MEA on hydration and the formation of $\text{Mg}(\text{OH})_2$ both contribute to the static
50 yield stress development.
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56 (3) SRA increases the growth rate and peak value of the static yield stress in both LHC paste and
57 blend of LHC and MEA. At the early-age stage, SRA retards the hydration process of LHC and MEA,
58 leading to lower contents of $\text{Mg}(\text{OH})_2$ and $\text{Ca}(\text{OH})_2$. The effect of SRA on time-dependent rheological
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604 behaviours stems from changes in the surface charge of hydrated particles and the hydrate
605 morphology on the particle surface.

606 (4) Taking the content and morphology of $Mg(OH)_2$ as a probe, it is confirmed that hydrates
607 amount is not the only factor affecting the static yield stress development. SRA alters the morphology
608 of brucite and changes the surface charge in hydrated blends of MEA and LHC. More and finer brucite
609 crystals forming on the MgO surface increase the specific surface area and strengthen the particles'
610 interactions, thereby promoting the static yield stress development.

611 (5) The combined use of MEA and SRA in LHC paste equilibrates the early-age hydration rate,
612 however, makes against the initial flowability. The rheological approach shows the potential for
613 designing the anti-crack concrete with multiple admixtures by taking the workability and the strength
614 gain at rest into consideration.

615 Nevertheless, only the dosage of SRA is taken into consideration in this paper. It is worth noting
616 that various SRAs with different functional groups and molecule structures may lead to different
617 results on the rheological behaviours and early-age hydration of cement pastes. Therefore, more in-
618 depth investigations are needed on this topic.

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