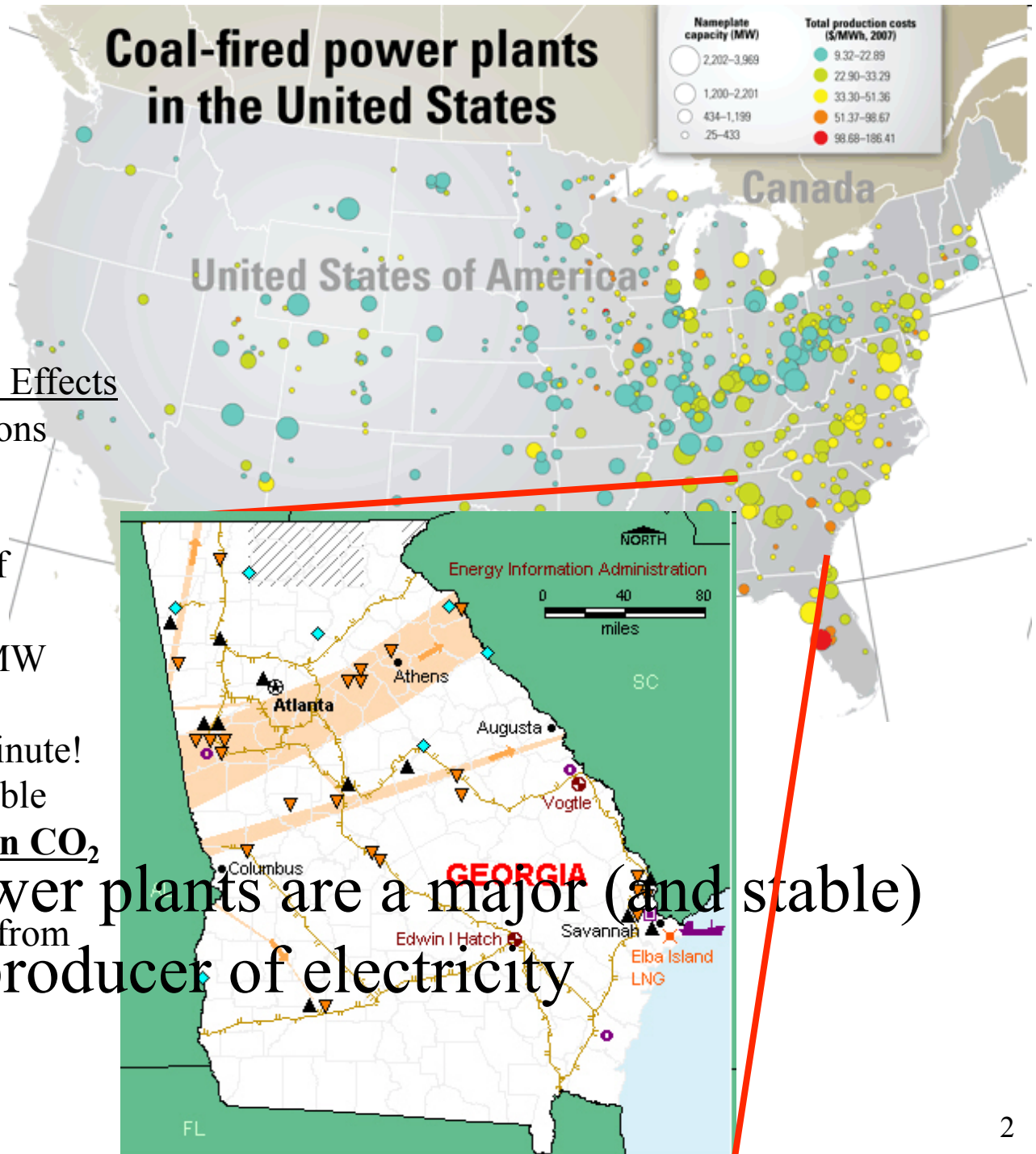


A New CO₂ Capture Platform: Hollow Fiber Adsorbents for Post- Combustion Recovery

Ryan Lively
The Impact of CO₂ on Global Climate Change
September 3rd, 2009

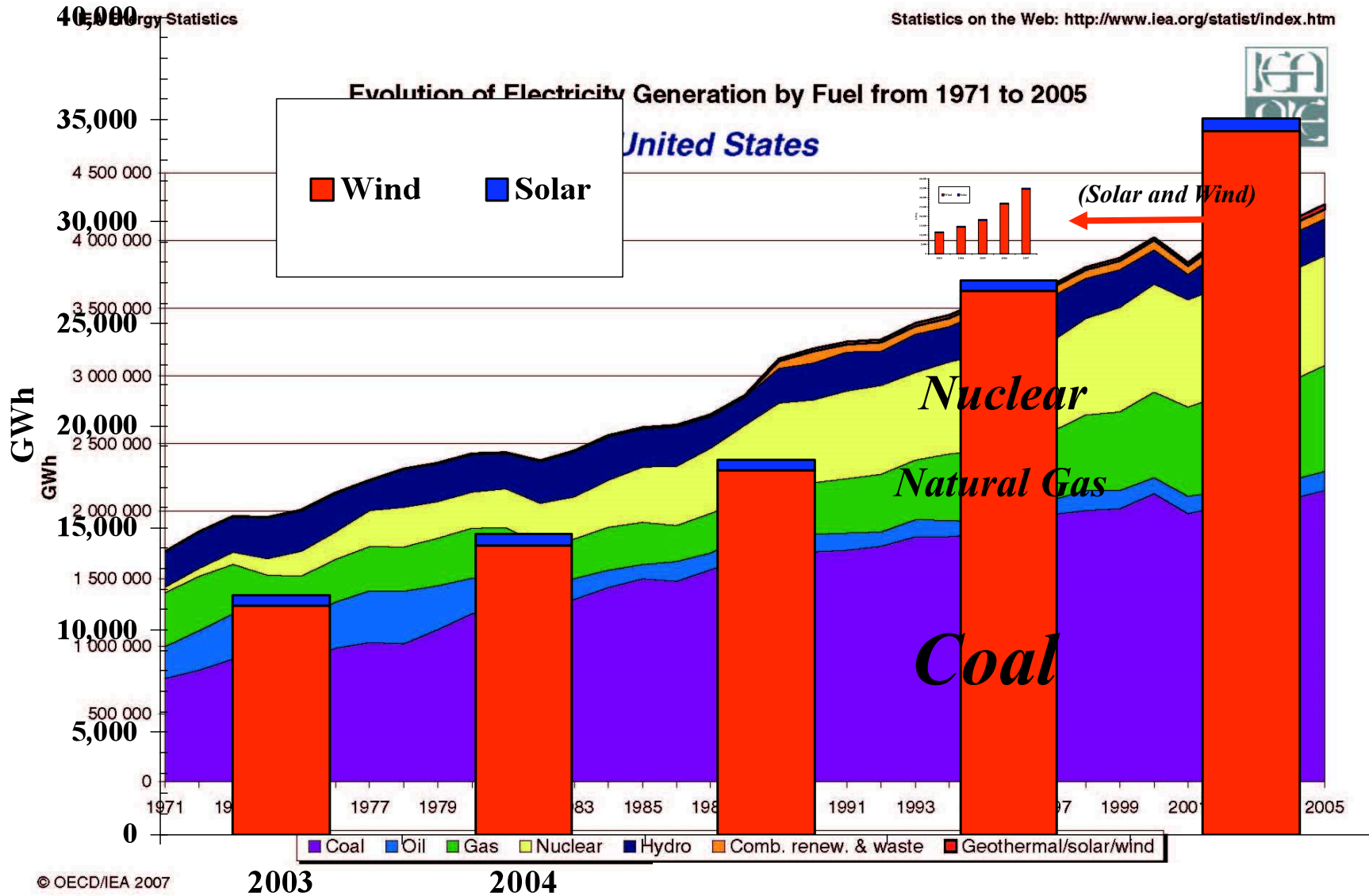


Coal Power Production Facts & Effects

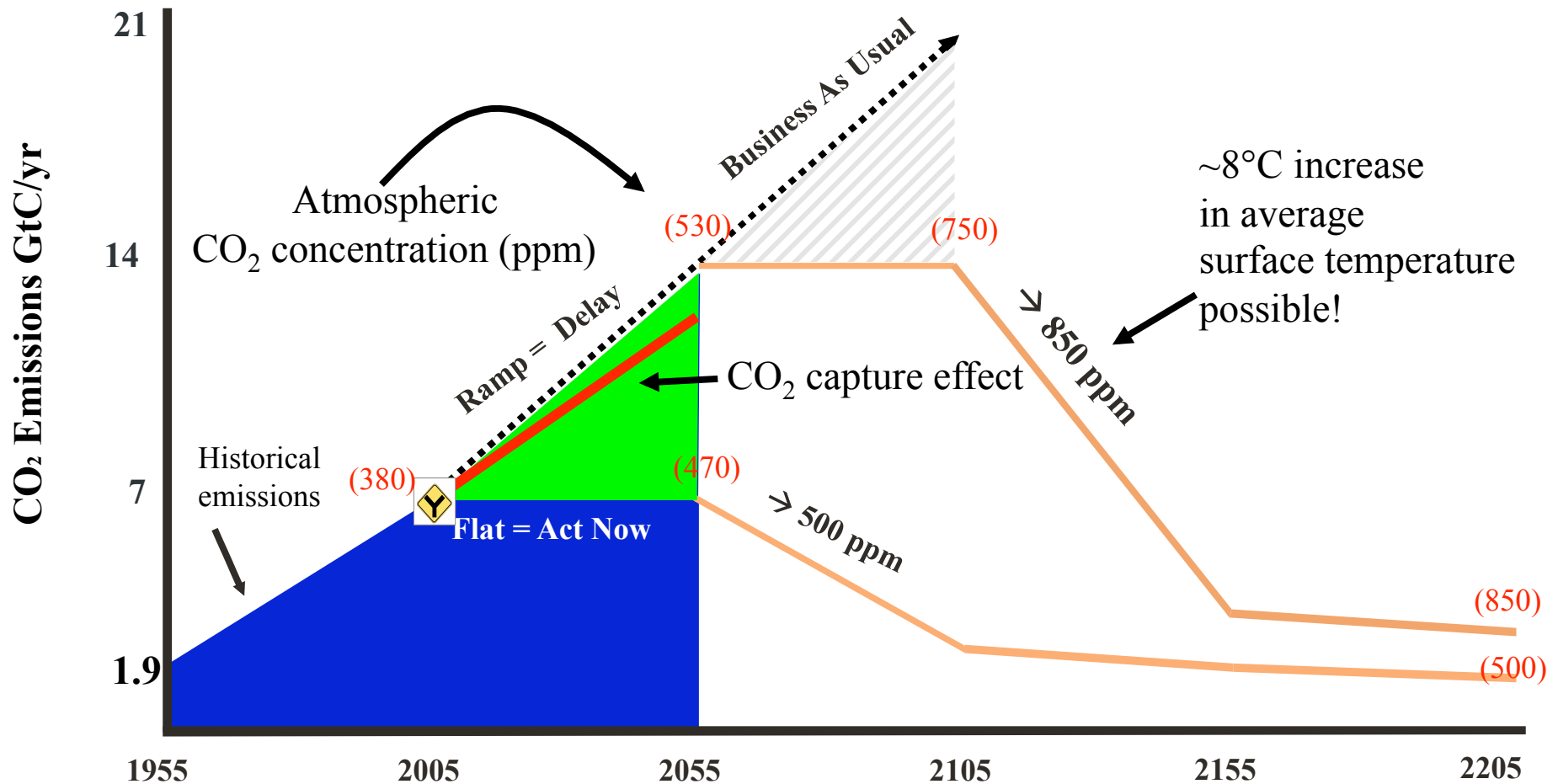
- ~600 coal fired power stations in the US
- 11 are in Georgia
- Releases 1 kg CO₂/kWhr of production
- That means a typical 500 MW unit releases ~9 tons of CO₂ per minute!
- US power stations responsible for ~0.3ppm/yr rise in CO₂

Coal-fired power plants are a major (and stable) producer of electricity

Why not simply switch to less polluting power production? –Scale.



CO₂ capture from coal fired power plants is one bridging strategy to lower CO₂ emissions



Source: Valerie Thomas

(Values) in parentheses are atmospheric ppm levels of CO₂

CO₂ Capture Strategies

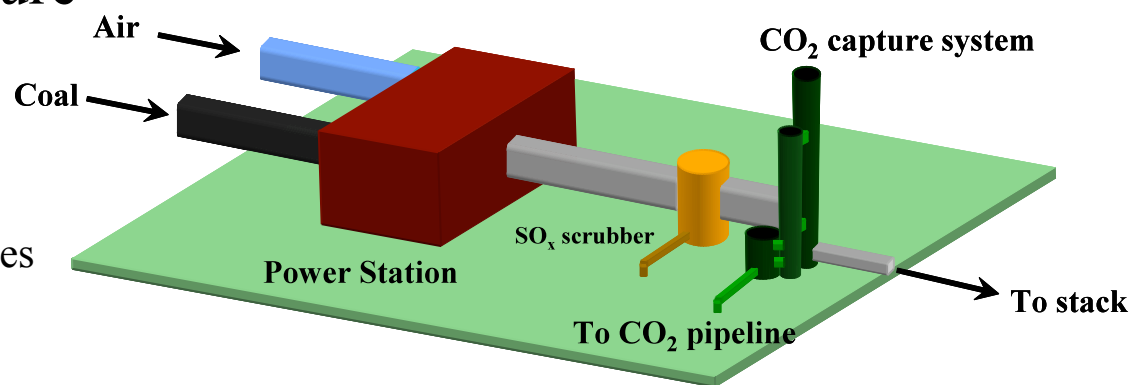
- Post-Combustion Capture

- Advantages

- Straightforward retrofit

- Disadvantages

- Low CO₂ partial pressures
 - Large quantities of gas

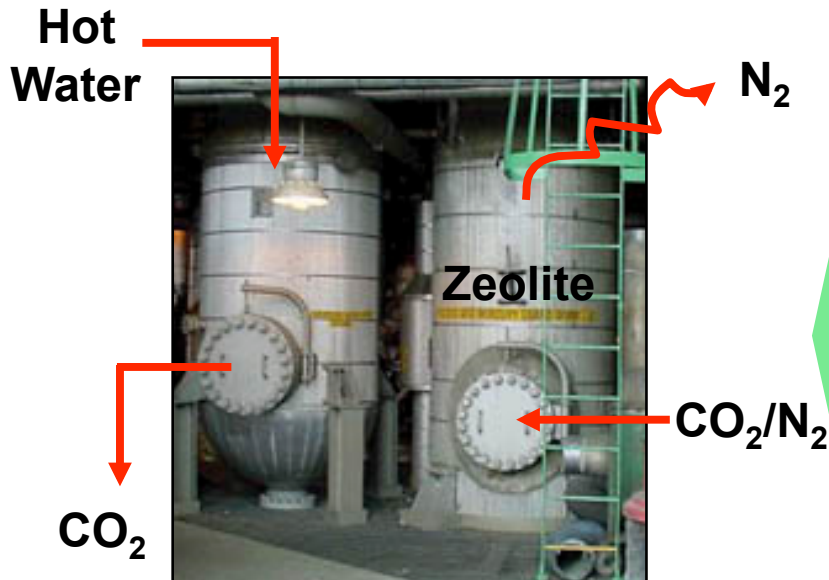
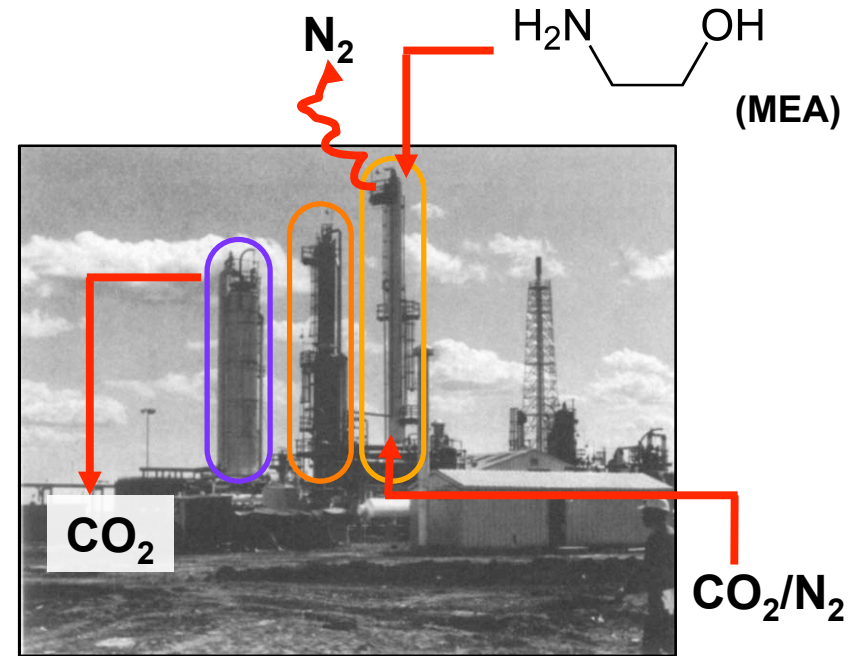


- The majority of the USA's power infrastructure cannot support other capture methods
- *Post-combustion capture is the single biggest target for effective carbon capture and storage*

Broad Routes for Post-Combustion CO₂ Capture

Absorption: Diffusion and/or reaction into a liquid (typically) to form a solution

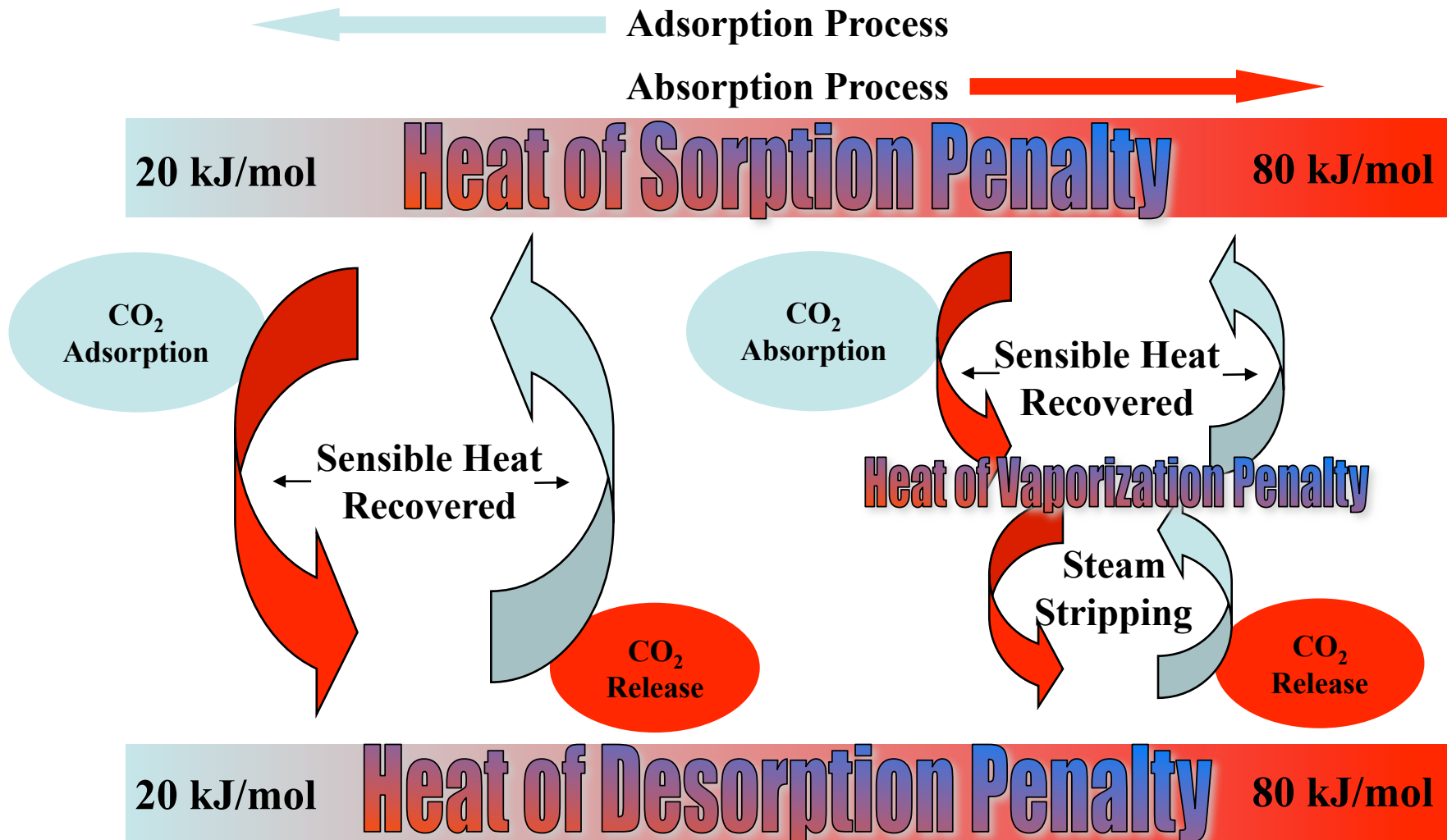
- Examples: Liquid amines (monoethanolamine), chilled ammonia, ionic liquids



Adsorption: Accumulation of molecules on the surface of a material

- Examples: Zeolites, activated carbon, silicas, solid supported amines

Basic Energetic Comparison between Adsorption and Absorption

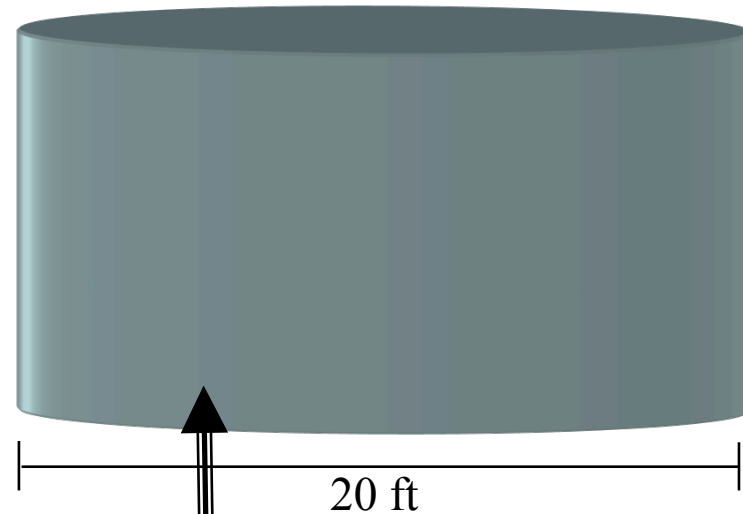


Fundamentally, adsorption processes have lower energetic needs than absorption processes

Issues with Packed Bed Adsorption Processes

Bed Pressure Drop:

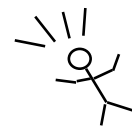
Need *very* large beds to minimize flue gas pressure drop



1×10^6 SCF per minute!

Slow Response Times:

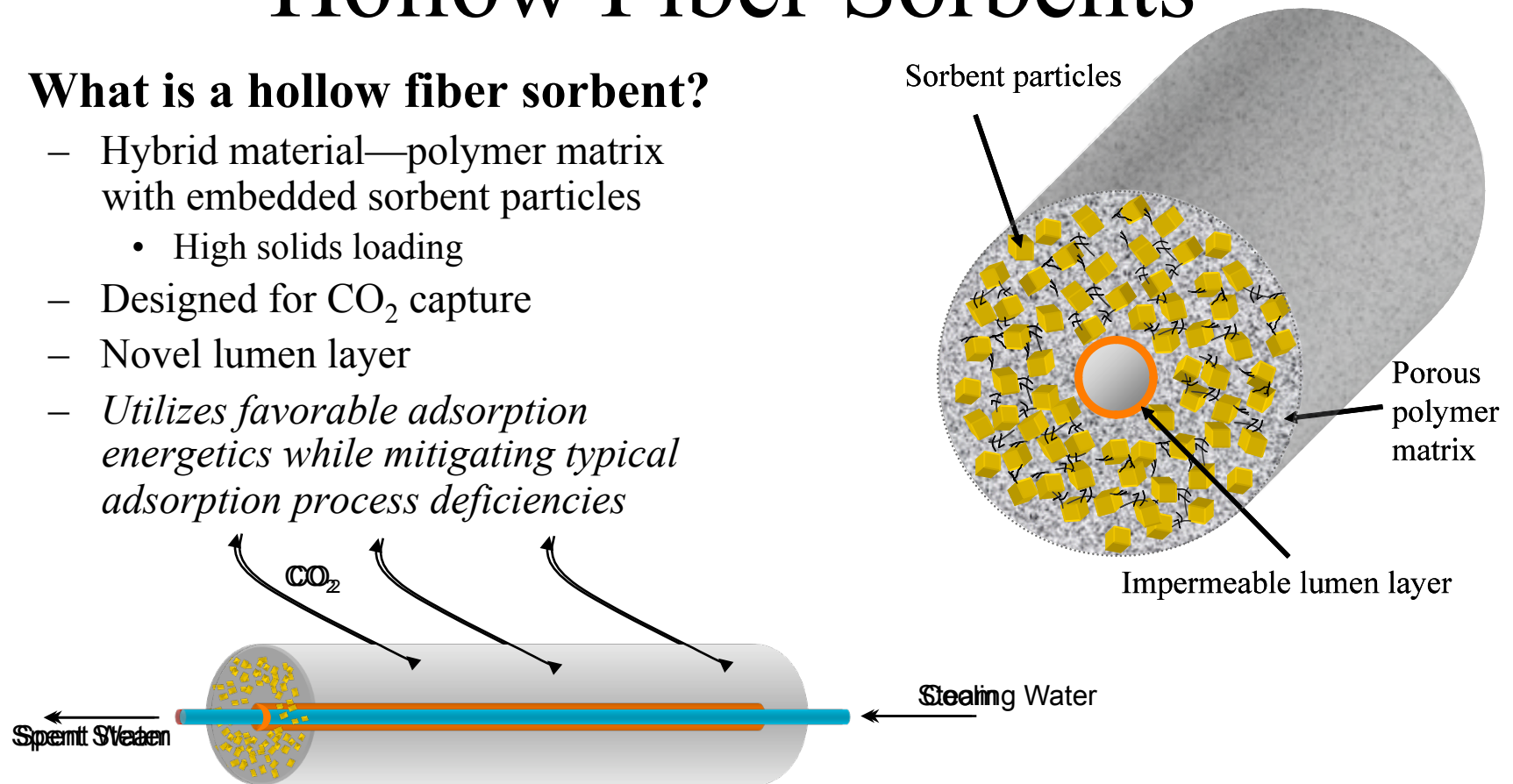
Need a high number (~50) of beds to ensure steady state operation



Hollow Fiber Sorbents

- **What is a hollow fiber sorbent?**

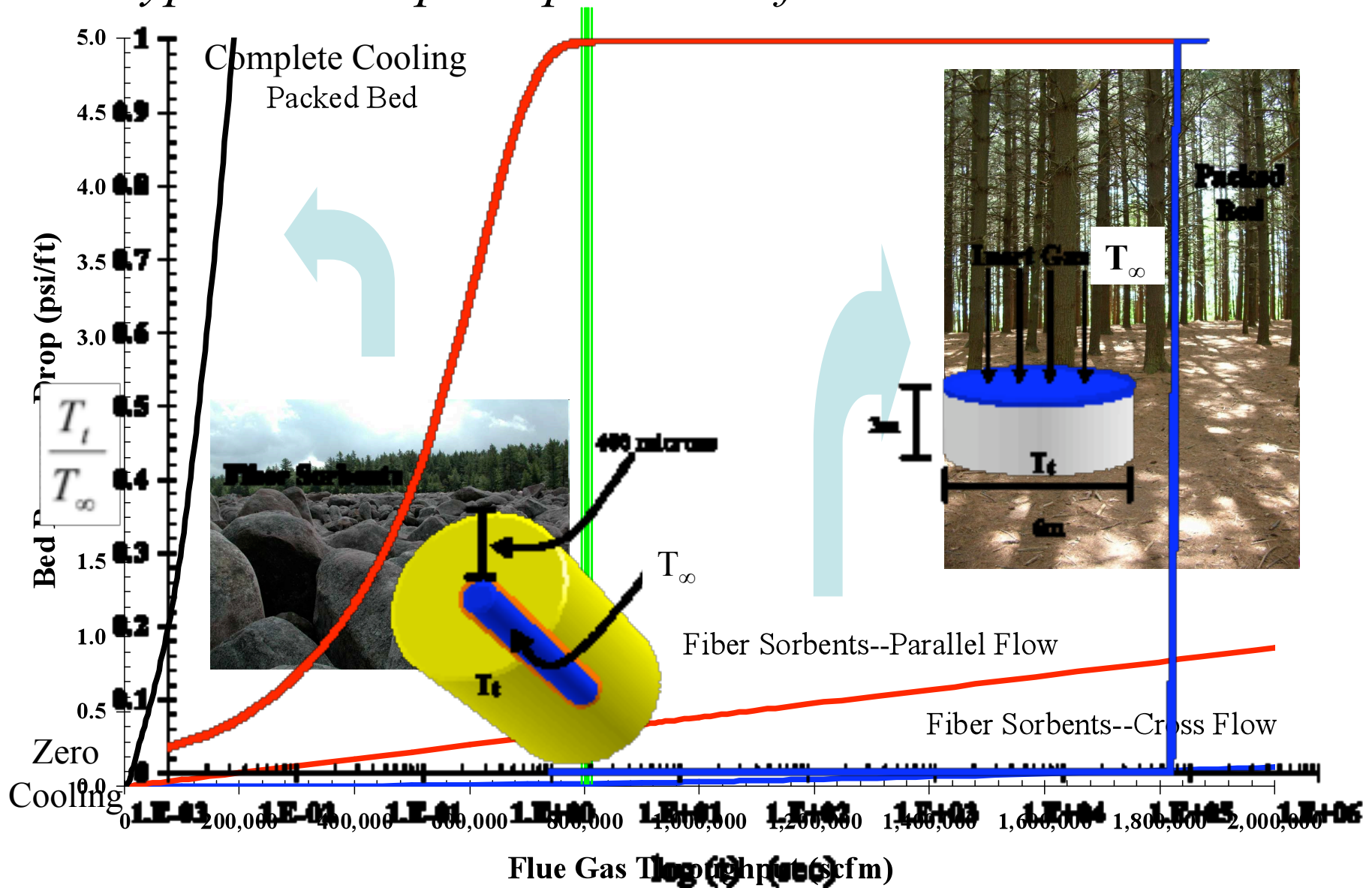
- Hybrid material—polymer matrix with embedded sorbent particles
 - High solids loading
- Designed for CO₂ capture
- Novel lumen layer
- *Utilizes favorable adsorption energetics while mitigating typical adsorption process deficiencies*



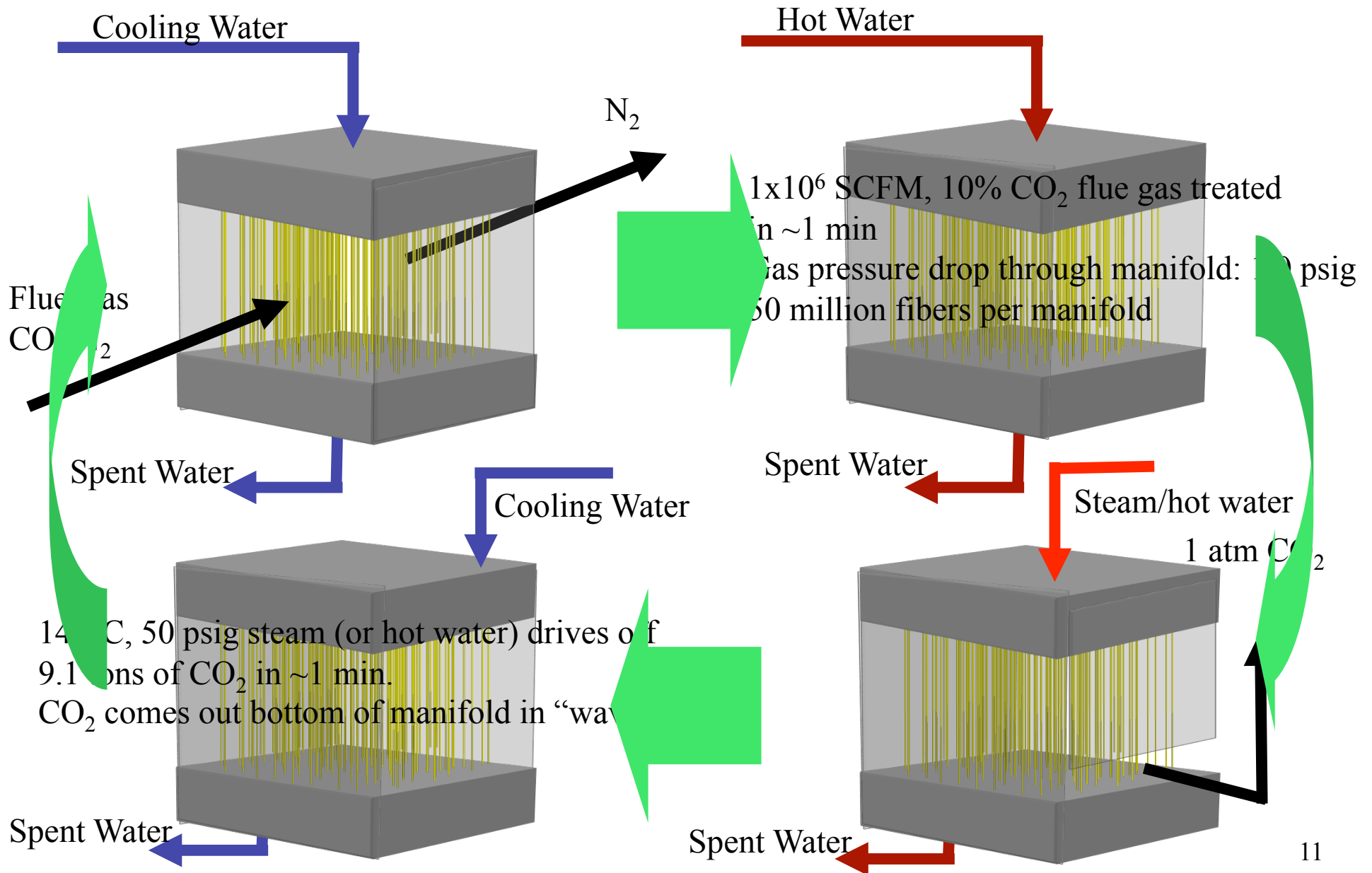
Cooling water used to aid in sorption process. Plant steam used for desorption step.

Thin fiber wall allows for rapid heat transfer. Barrier layer prevents mass exchange between heat transfer agent and CO₂

“Utilizes favorable adsorption energetics while mitigating typical adsorption process deficiencies” ...but how?



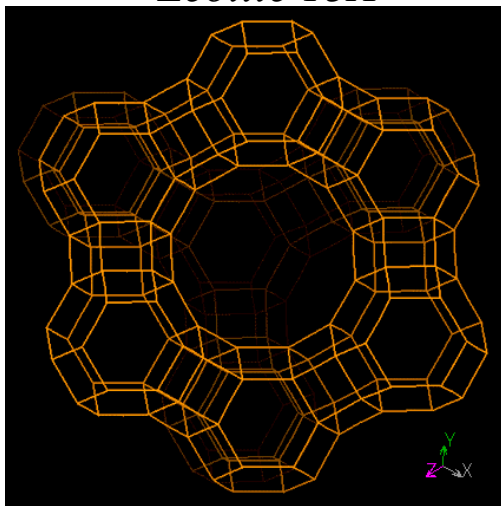
Using Fiber Sorbents in Thermal Swing Adsorption Mode



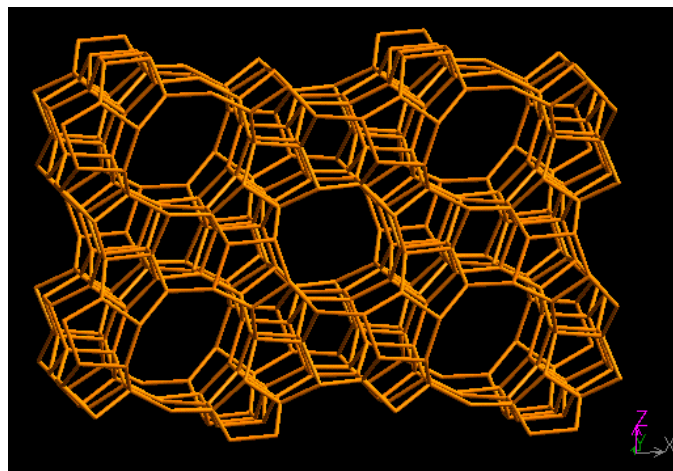
Adsorbent Selection

| <u>Sorbent</u> | Zeolite 13X | High Silica MFI | Anchored Amines |
|--|--------------------|------------------------|------------------------|
| CO ₂ Dry Sorption Capacity | High | Medium | Low |
| CO ₂ Wet Sorption Capacity | Very Low | -- | Medium |
| Heat of Sorption | Medium | Low | High |
| Diffusion Coefficient [cm ² /s] | 10 ⁻⁵ | 10 ⁻⁷ | -- |

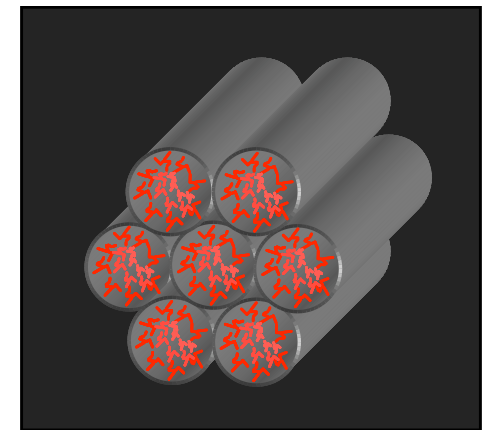
Zeolite 13X



High Silica MFI

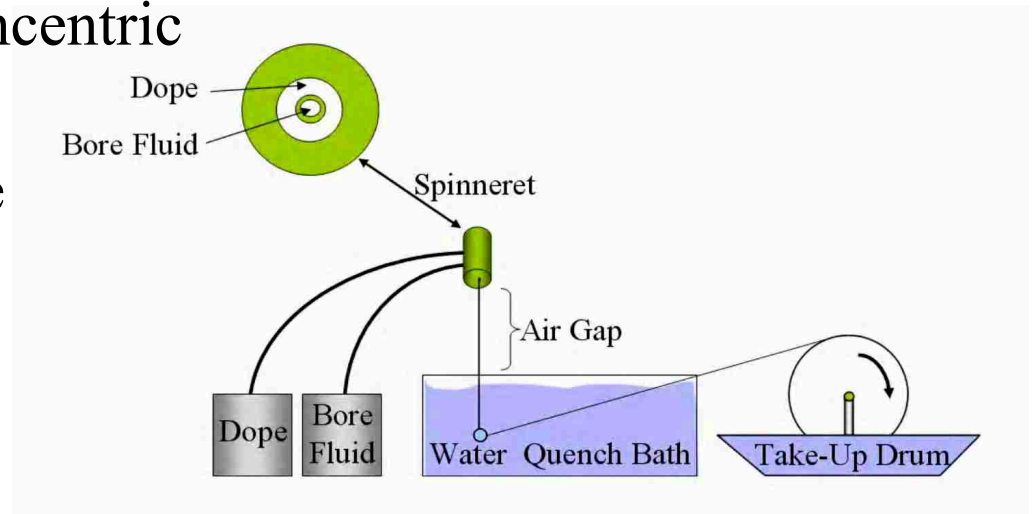


Anchored Amines

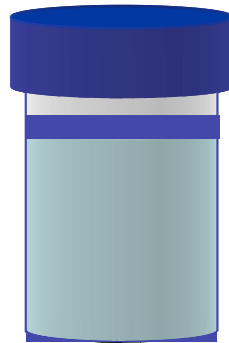


Hollow Fiber Sorbents: Fabrication

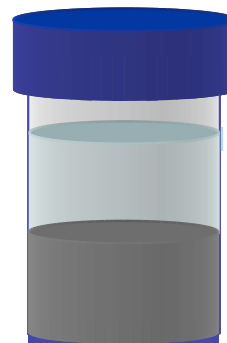
- Extrusion through a concentric annulus
- Fiber characteristics are controlled by:
 - Extrusion rate
 - Fiber take up rate
 - Air gap height
 - Operating temperature



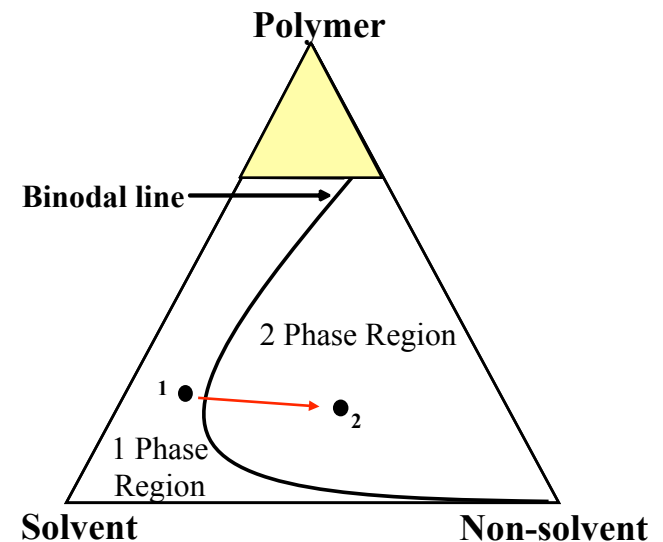
*1 phase
polymer solution*



"Cloud Point"



*2 phase
polymer solution*



Ternary Diagram

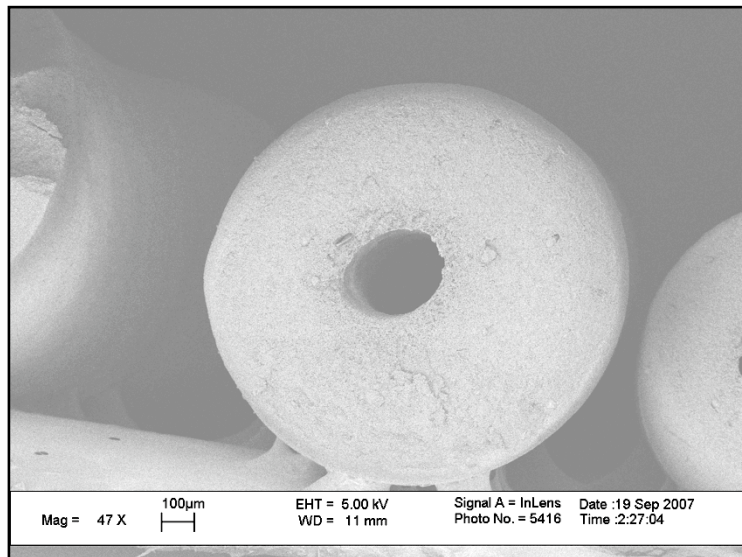
Fiber Sorbent Spinning: 75wt% Solids

Spinning Conditions

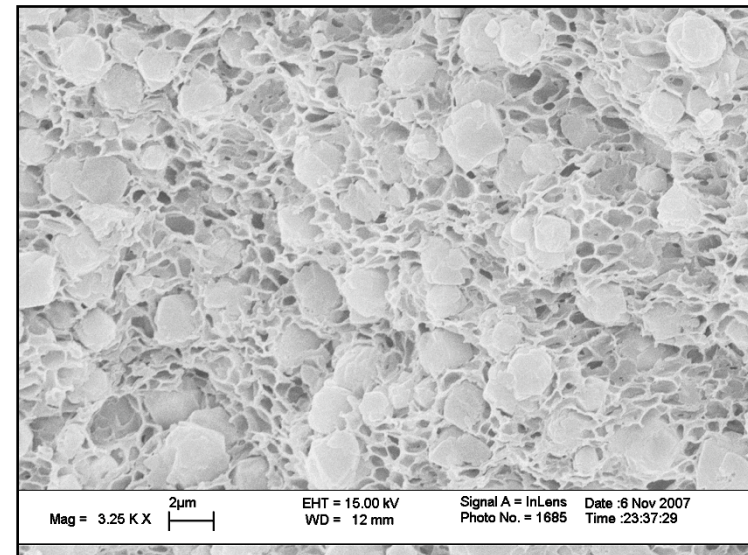
| | |
|-------------------------|----------------------------|
| Core flow rate | 1000 mL/hr |
| Bore flow rate | 250 mL/hr |
| Bore Composition | 80/20 NMP/H ₂ O |
| Operating Temp. | 25°C |
| Take-up Rate | 11.7 m/min |
| Air Gap | 3.0 cm |

Materials Used

| | |
|--------------------|-----------------------|
| Sorbent | Zeolite 13X |
| Polymer | Cellulose Acetate |
| Solvent | N-methylpyrrolidone |
| Non-Solvent | Water |
| Pore Former | Polyvinyl pyrrolidone |

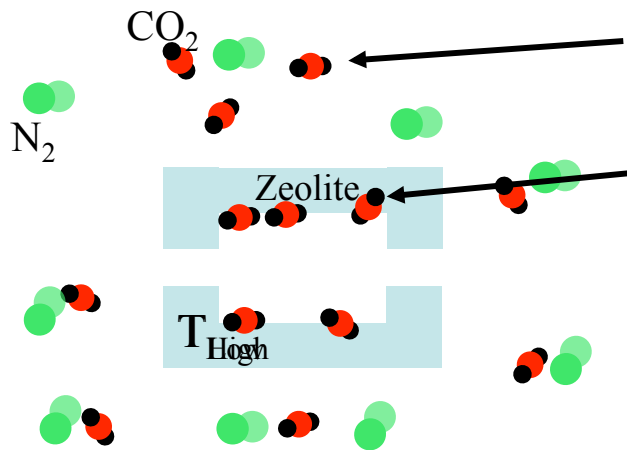
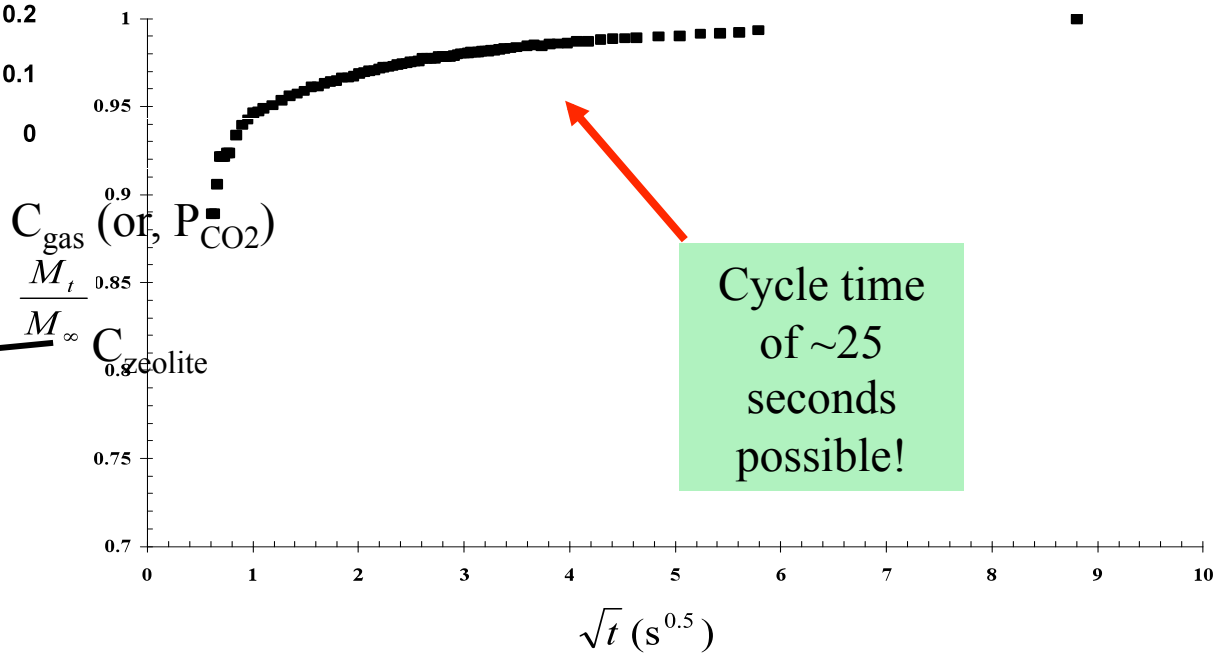
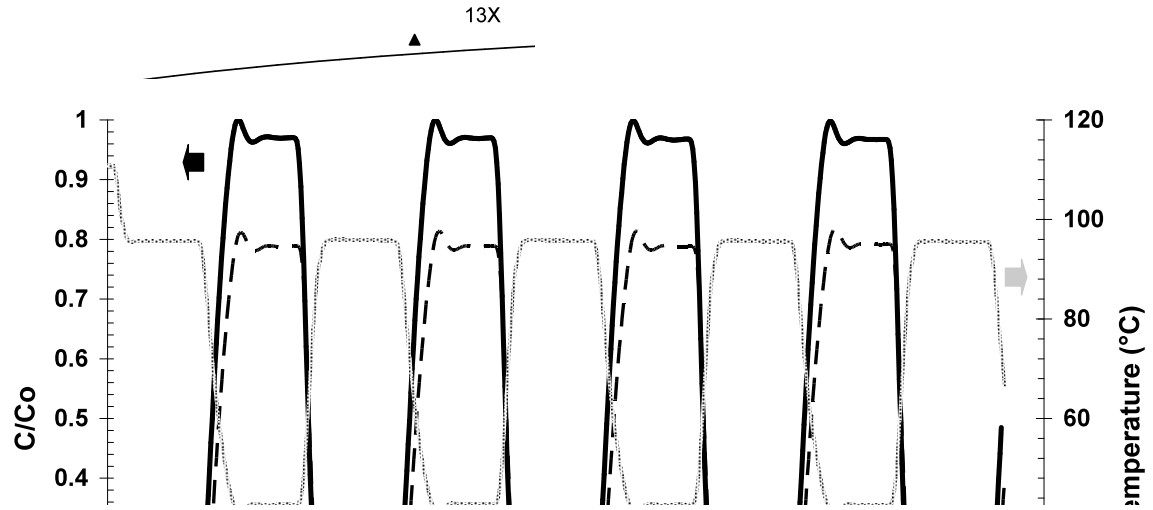
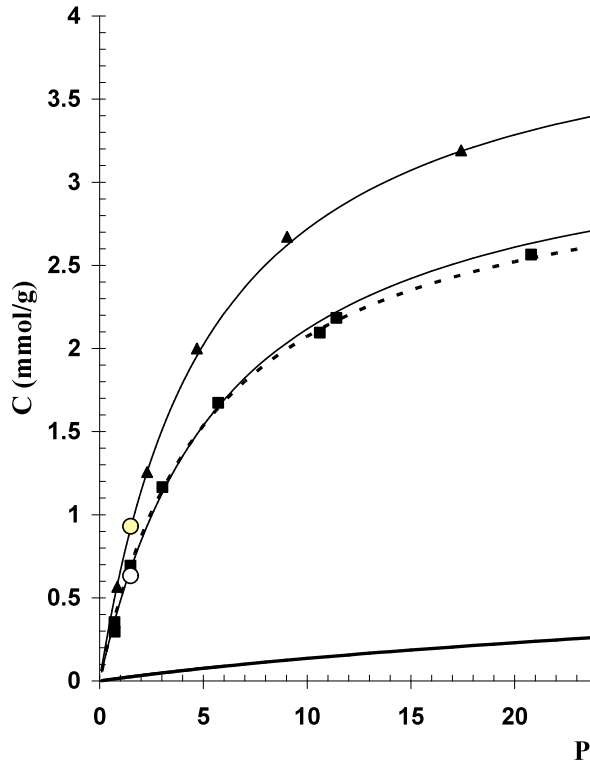


Fiber sorbent with correct dimensions



Zeolite 13X dispersed in cellulose acetate matrix

CO₂ Sorption Performance: Equilibrium, Cyclic, and Kinetic



$$\frac{C_{\text{gas}} \text{ (or, } P_{\text{CO}_2})}{M_t} \rightarrow \frac{C_{\text{zeolite}}}{M_{\infty}}$$

Barrier Layer Construction

N₂ Sweep

Neoprene/PVDC Latex Solution

Decreasing porosity
in r-direction

- ~30 microns
- Gradient serves as a backstop for latex

Permeation Results:

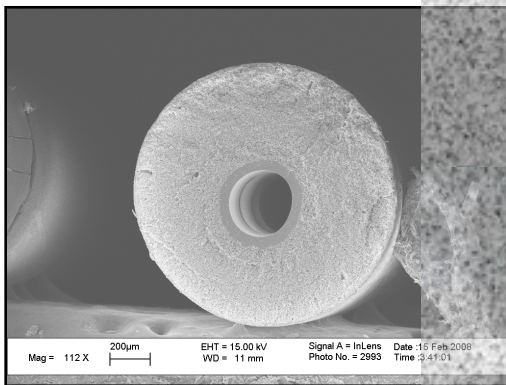
Uncoated: N₂~60,000 GPU

Coated: N₂~3.0 GPU

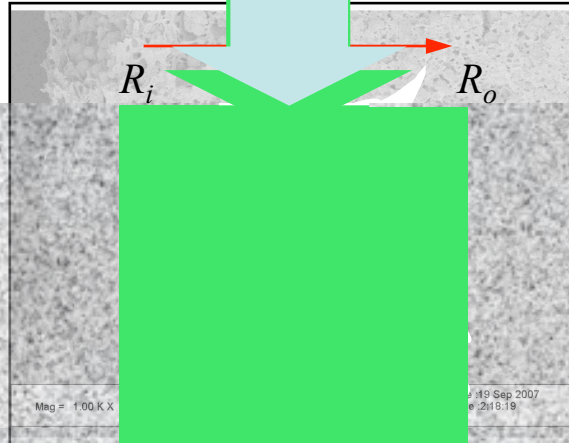
Expected: ~0.01 GPU

~5% steam/CO₂ losses

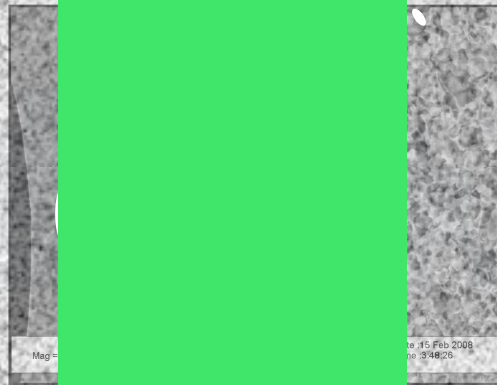
Fiber Sorbent
Core Structure



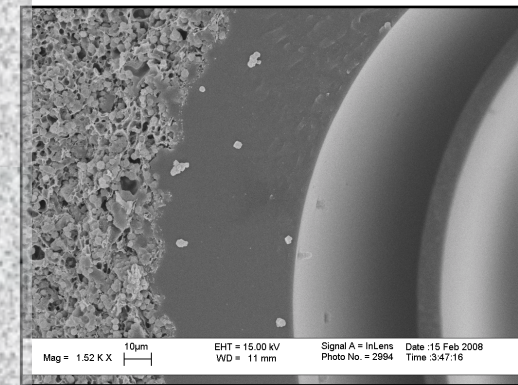
PVDC lumen layer on fiber sorbents



Porosity sorbents



Neoprene/PVDC Barrier Layer



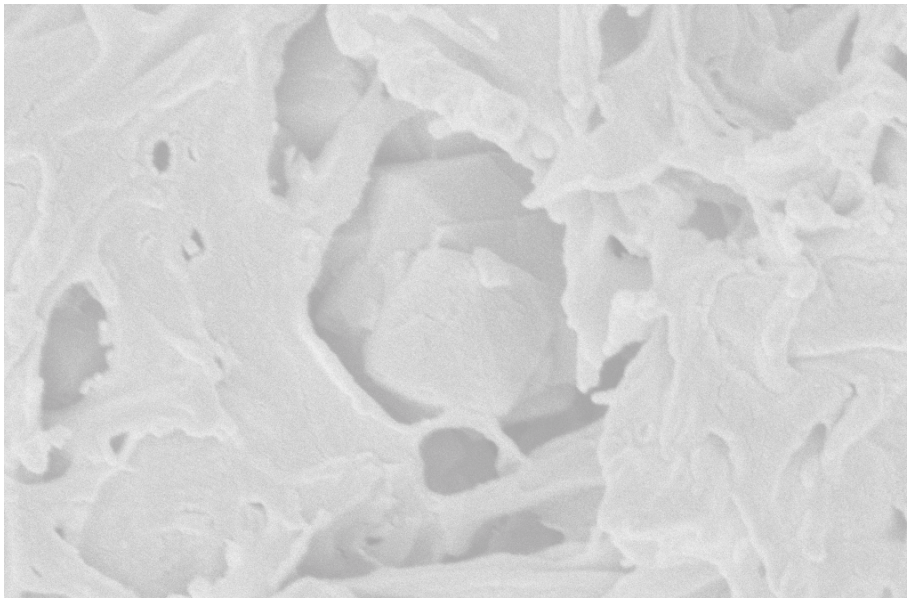
lumen layer surface

Future Work

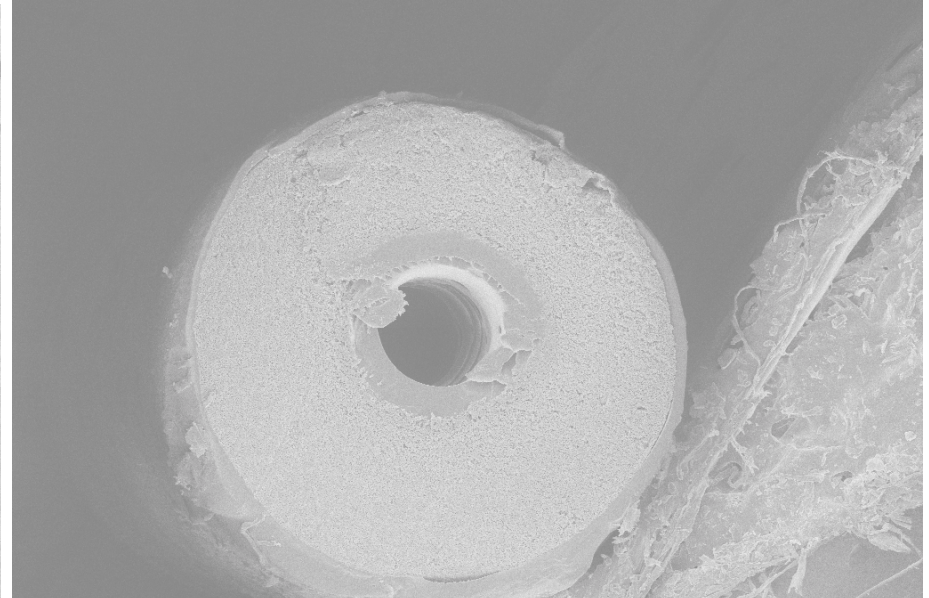
- Improving barrier layer performance
- Extending fiber sorbent platform to new sorbents and polymers
 - MFI (sorbent) and Torlon (polymer)
- Fiber stability in constant water/steam cycles
- CO₂ capture costs and economics

Acknowledgements

- Koros Research Group
 - Particularly: Jason Ward, Ryan Adams, Vinod Babu, JR Johnson
- Dr. Koros
- Dr. Chance
- ExxonMobil for funding the research
 - Particularly: Harry Deckman, Rusty Kelley

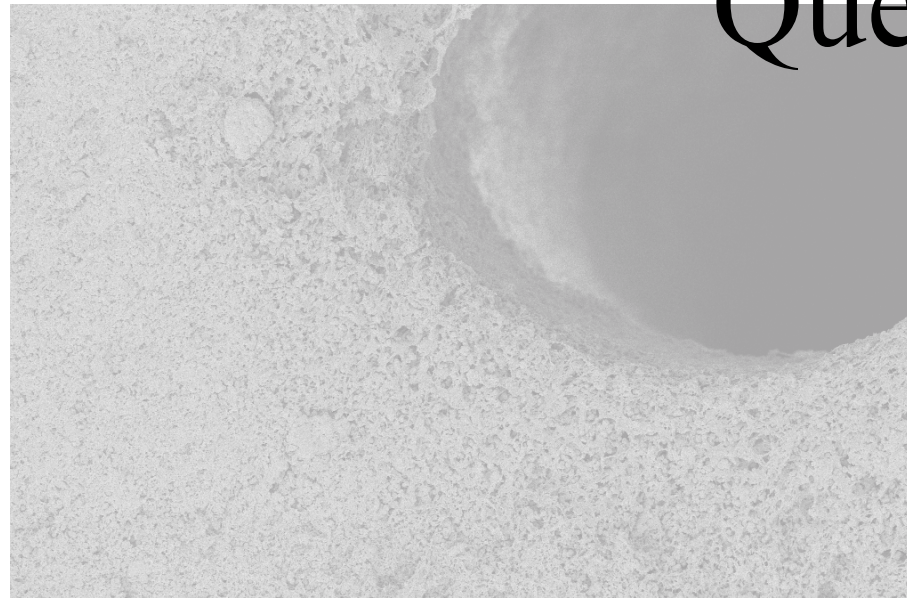


Mag = 20.00 K X 200nm
EHT = 5.00 kV Signal A = InLens Date :19 Sep 2007
WD = 11 mm Photo No. = 5414 Time :2:25:13

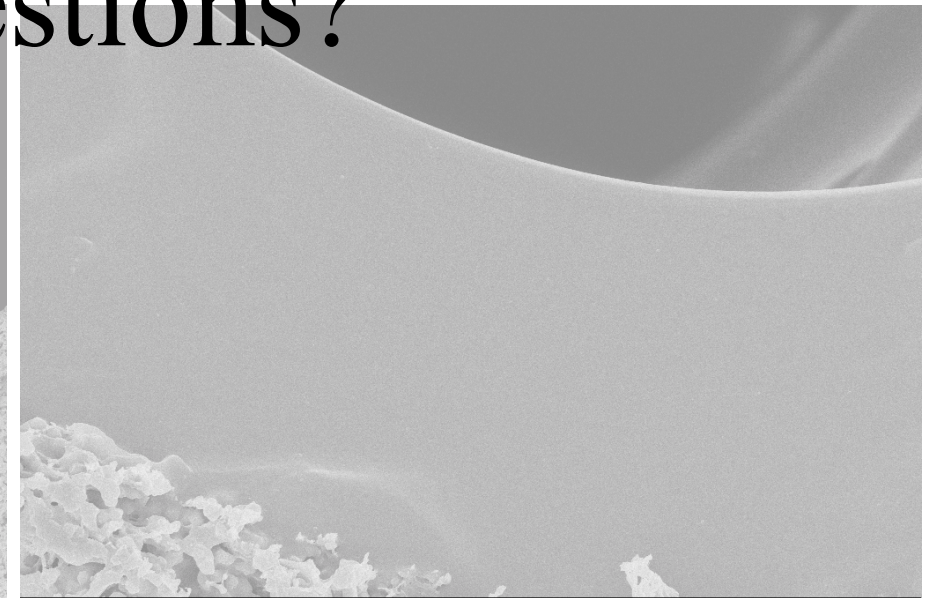


Mag = 51 X 100µm
EHT = 15.00 kV Signal A = InLens Date :27 Nov 2007
WD = 11 mm Photo No. = 3365 Time :2:40:43

Questions?



Mag = 250 X 20µm
EHT = 5.00 kV Signal A = InLens Date :19 Sep 2007
WD = 11 mm Photo No. = 5417 Time :2:27:33



Mag = 718 X 20µm
EHT = 15.00 kV Signal A = InLens Date :27 Nov 2007
WD = 11 mm Photo No. = 3368 Time :2:42:57