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Biological phosphorus removal from abattoir wastewater at very short sludge ages mediated by novel PAO clade *Comamonadaceae* 

Huoqing Ge, Damien J. Batstone, Jürg Keller

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1	Biological phosphorus removal from abattoir wastewater at
2	very short sludge ages mediated by novel PAO clade
3	Comamonadaceae
4	Huoqing Ge, Damien J. Batstone, Jürg Keller*
5	AWMC, Advanced Water Management Centre, The University of Queensland, St Lucia,
6	4072, Queensland, Australia
7	
8	*Corresponding author:
9	Jürg Keller
10	
11	Advanced Water Management Centre (AWMC),
12	The University of Queensland, St Lucia,
13	QLD 4072, Australia
14	Phone: +61 7 3365 4727
15	Fax: +61 7 3365 4726
16	Email: j.keller@uq.edu.au
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25 Abstract:

26 Recent increases in global phosphorus costs, together with the need to remove phosphorus 27 from wastewater to comply with water discharge regulations, make phosphorus recovery 28 from wastewater economically and environmentally attractive. Biological phosphorus (Bio-P) 29 removal process can effectively capture the phosphorus from wastewater and concentrate it in 30 a form that is easily amendable for recovery in contrast to traditional (chemical) phosphorus 31 removal processes. However, Bio-P removal processes have historically been operated at 32 medium to long solids retention times (SRTs, 10-20 days typically), which inherently 33 increases the energy consumption while reducing the recoverable carbon fraction and hence 34 makes it incompatible with the drive towards energy self-sufficient wastewater treatment 35 plants. In this study, a novel high-rate Bio-P removal process has been developed as an 36 energy efficient alternative for phosphorus removal from wastewater through operation at an 37 SRT of less than 4 days. The process was most effective at an SRT of 2-2.5 days, 38 achieving >90% phosphate removal. Further reducing the SRT to 1.7 days resulted in a loss 39 of Bio-P activity. 16S pyrotag sequencing showed the community changed considerably with 40 changes in the SRT, but that *Comamonadaceae* was consistently abundant when the Bio-P 41 activity was evident. FISH analysis combined with DAPI staining confirmed that bacterial 42 cells of *Comamonadaceae* arranged in tetrads contained polyphosphate, identifying them as 43 the key polyphosphate accumulating organisms at these low SRT conditions. Overall, this 44 paper demonstrates a novel, high-rate phosphorus removal process that can be effectively 45 integrated with short SRT, energy-efficient carbon removal and recovery processes.

46

47 Keywords: Biological phosphorus removal; Short sludge retention time; Polyphosphate
48 accumulating organisms; *Comamonadaceae*; Tetrad-forming bacteria

49

#### 50 1. Introduction

51 Phosphorus is an important element to agricultural and industrial activity, and there are 52 concerns over its depletion as a non-renewable resource (Yuan et al., 2012). Thus there is growing interest in capturing and recycling phosphorus from other sources, such as 53 54 wastewater. Phosphorus removal is essential in advanced wastewater treatment to meet 55 reduced discharge limits on effluent phosphorus concentrations. Phosphorus removal results 56 in a solids stream rich in phosphorus that has the potential for recovery. Phosphorus removal 57 via biological processes is more economical and environmentally sustainable compared to 58 traditional (chemical) phosphorus removal processes for a number of reasons, including 59 chemical costs, the ability to subsequently release and recover phosphorus, and plant-60 availability of phosphorus where waste activated sludge (WAS) is used directly (Shu et al., 61 2006).

62

So far, Bio-P removal processes have been widely applied to treat domestic wastewater (<10 63 mg P  $L^{-1}$  in influent) (Pijuan et al., 2008), abattoir wastewater (20-40 mg P  $L^{-1}$ ) (Lemaire et 64 al., 2009), and high-strength industrial wastewater (60-100 mg P L<sup>-1</sup>) (Broughton et al., 2008). 65 66 Effective phosphorus removal (>90%) has been achieved in most cases, resulting in a final phosphorus concentration generally below 1 mg  $L^{-1}$  phosphate (PO<sub>4</sub><sup>3-</sup>)-P. The typical process 67 68 configuration for the Bio-P process is either alternating anaerobic/aerobic phase in one 69 reactor (e.g. sequencing batch reactor (SBR)) or recirculating sludge through anaerobic and 70 aerobic zones, often with anoxic reactor(s) in between for denitrification (e.g., Bardenpho, 71 modified University of Cape Town (UCT), etc.) (Oehmen et al., 2007). Generally, an overall 72 sludge retention time (SRT) in the range of 8-30 days is applied (Oehmen et al., 2007) to 73 retain key organisms, e.g. nitrifiers for nitrification. This relatively long SRT can introduce 74 challenges to maintain a stable Bio-P removal process, as some organisms (e.g. denitrifiers

75 and glycogen accumulating organisms (GAOs)) can outcompete polyphosphate accumulating 76 organisms (PAOs) for available carbon (Oehmen et al., 2007), resulting in a decreased Bio-P 77 activity and diminished phosphorus removal efficiency. Therefore, the focus of previous 78 work has been on the investigation of PAOs and their competitors, and process optimisation 79 to avoid competition. Novel processes, such as high-rate activated sludge (A-stage) processes 80 focus on carbon accumulation in an initial short-SRT process (Jimenez et al., 2005), and 81 achieving phosphorus removal in the same stage would be highly beneficial (Ge et al., 2013). 82 However, investigation of the minimal SRT required for Bio-P removal processes has been 83 limited so far. There are two papers most relevant in this regard. Mamais and Jenkins (1992) 84 evaluated the effect of SRT (2-4 days) on Bio-P removal, and reported that the Bio-P removal 85 functioned efficiently at the SRT above 2.9 days, and deteriorated once the SRT decreased to 86 2.6 days. Brdjanoyic et al. (1997) used a model-based approach to identify the minimum SRT 87 required for the stable Bio-P removal process, which was estimated as 8 days at 20°C, 88 extending to 16 days at 10°C and further to 32 days at 5°C. These SRTs are far beyond the 89 SRT range (0.5-2 days) normally applied in the A-stage processes.

90

91 The most well known group of PAOs is the Rhodocyclus-related "Candidatus 92 Accumulibacter phosphatis" (referred to as Accumulibacter hereafter), which has been 93 commonly found in many full-scale Bio-P removal plants, with a typical abundance of 5-20% 94 of the bacterial community (Yuan et al., 2012). The metabolism of Accumulibacter has been 95 studied extensively, and includes carbon (i.e., volatile fatty acids (VFAs)) uptake and 96 polyhydroxyalkanoates (PHA) formation under anaerobic conditions, followed by the 97 oxidation of PHA to provide energy for phosphate uptake and cell growth under subsequent 98 aerobic conditions (Oehmen et al., 2007). Several other bacteria have also been identified as 99 PAOs (referred to as non-Accumulibacter PAOs hereafter), including Tetrasphaera (Kong et

100 al., 2005; Nguyen et al., 2011), Pseudomonas (Günther et al., 2009), Microlunatus 101 phosphovorus (Nakamuka et al., 1995), Halomonas (Nguyen et al., 2012), and some 102 members of Actinobacteria (Beer et al., 2006). Some non-Accumulibacter PAOs (e.g. 103 Tetrasphaera) have been found to be more abundant in certain non-domestic full-scale Bio-P 104 removal plants than Accumulibacter (Nguyen et al., 2011). Metabolic processes of non-105 Accumulibacter PAOs are also reported to be different from Accumulibacter, where some can 106 take up carbon sources other than VFAs, such as glucose and amino acids, with unknown 107 storage compounds formed instead of PHA (Nakamura et al., 1995; Nguyen et al., 2011). The 108 diversity, metabolism, and function of non-Accumulibacter PAOs have not been investigated 109 to the same extent as Accumulibacter. In particular, phylogeny and function in non-domestic 110 and high-rate systems such as short SRT Bio-P systems (Ge et al., 2013) have not been 111 investigated, with most analysis having been done in domestic or synthetic feed systems.

112

113 This paper describes the development and characterisation of a high-rate Bio-P removal 114 process with an operating SRT of less than 4 days, focusing on the capability and 115 differentiation of the microbial agent compared to Bio-P processes in conventional, longer-116 SRT activated sludge systems.

117

118 2. Material and Methods

#### 119 2.1. Abattoir wastewater

Wastewater was collected from a local abattoir (following dissolved air flotation and solid paunch separation) in Queensland, Australia on a fortnightly basis and stored at 4°C. Wastewater was diluted with tap water to a total chemical oxygen demand (TCOD) of 2-3 g  $L^{-1}$  to dampen variations of the wastewater strength and composition due to the intermittent collection schedule. Characteristics of the wastewater feed (after the dilution) were analysed

regularly, and the results are summarised in Table 1. The average ratio of SCOD to total phosphorus in the wastewater feed was approximately 40.

127

#### 128 2.2. Sequencing batch reactor (SBR) setup and operation

129 A lab-scale SBR with a working volume of 5 L was used. The SBR was inoculated with 130 activated sludge from a non-enhanced biological phosphorus removal (non-EBPR) full-scale 131 wastewater treatment plant located in Brisbane, Australia. The SBR was operated with eight 132 cycles (3 h per cycle) per day in a temperature controlled room ( $20-22^{\circ}C$ ). Each cycle 133 consisted of a 10 min anaerobic period, a 105 min aerobic period, and a 65 min settle/decant 134 period. The wastewater was fed into the SBR in the first 5 min of the anaerobic period and 135 discharged in the decant period (5 min) to maintain the HRT. The SRT of the SBR was 136 maintained by wasting sludge during the last 5 min of the aerobic period. pH was measured 137 using a glass body pH probe (TPS, Australia), ranging between 7.0-7.8, but not controlled. 138 The dissolved oxygen (DO) concentration in the aerobic period was maintained between 1.5 and 2 mg  $O_2$  L<sup>-1</sup> by providing air intermittently with an on/off controller and using a DO 139 membrane probe (YSI, Australia). Both DO and pH probes were calibrated regularly and 140 141 connected to a process logic control system for data recording.

142

143 The SBR was operated for over 10 months where the HRT and SRT were varied to evaluate 144 the phosphorus removal performance. Table 2 summarized the HRT and SRT applied in each 145 operating period. It should be noted that the real SRT in some periods differed slightly from 146 the target SRT due to varying solids concentrations in the effluent.

147

148 **2.3. Chemical analysis** 

149	Mixed liquor samples were taken regularly and analysed for TCOD, soluble COD (SCOD),
150	total suspended solids (TSS), volatile suspended solids (VSS), total Kjeldahl phosphorus
151	(TKP) and $PO_4^{3-}$ . Before measuring $PO_4^{3-}$ and SCOD concentrations, the mixed liquor
152	samples were filtered through Millipore filter units (0.45 $\mu m$ pore size). TSS, VSS, and COD
153	were analysed based on Standard Methods (APHA, 1998). PO <sub>4</sub> <sup>3-</sup> and TKP were measured
154	using a Lachat Quik-Chem 8000 Flow Injection Analyser (Lachat Instrument, Milwaukee).
155	
156	2.4. Calculation methods
157	Specific Removal Efficiency $(mgP \ gVSS^{-1} \ d^{-1}) =$
158	$\frac{(PO_{4\ in}^{3-} - PO_{4\ out}^{3-}) \times SBR \ loading}{Biomass \ concentration \times Re \ actor \ volume}$
159	Where $PO_{4_{in}}^{3-} = PO_{4_{in}}^{3-} - P$ concentration in the influent (mg L <sup>-1</sup> );
160	$PO_4^{3-}$ out = $PO_4^{3-}$ -P concentration in the effluent (mg L <sup>-1</sup> );
161	SBR loading = 9 $L_{wastewater} d^{-1}$ ;
162	Biomass concentration = Biomass concentration in the SBR (g VSS $L^{-1}$ );
163	Reactor volume = 5 L.
164	
165	2.5. Characterisation of microbial communities
166	2.5.1. 16S rRNA gene amplicon pyrosequencing
167	Genomic DNA was extracted from the biomass samples collected in the SBR by using a
168	FastDNA Spin Kit for soil (MP Biomedicals, USA) according to the manufacturer's protocol.
169	The quantity and quality of the extracted DNA was measured using a NanoDrop
170	spectrophotometer (Thermo Fisher Scientific, USA) and agarose gel (1%, weight/volume)
171	electrophoresis. The extracted DNA was submitted to the Australian Centre for Ecogenomics
172	(ACE) for 16s rRNA gene pyrotag sequencing on the Genome Sequencer FLX Titanium

platform (Roche, USA). The primers used for pyrotag sequencing were modifications of the
926F (5'-AAACTYAAAKGAATTGACGG-3') and 1392wR (5'-ACGGGCGGTGWGTRC3').

176

Pyrotag sequence analysis was performed as described previously (Ge et al., 2013) using
ACE Pyrosequencing Pipeline (Imelfort and Dennis, 2011a) developed based on QIIME
(Caporaso et al., 2010) and ACACIA (Bragg et al., 2012). The generated operational
taxonomic units (OTUs) table was then normalised by using Nomaliser (Imelfort and Dennis,
2011b).

182

183 2.5.2. Fluorescence *in situ* hybridization (FISH) and polyphosphate (polyP) staining

184 FISH and polyP staining by DAPI (4', 6'- diamidino-2-phenylindole) is incompatible in a 185 single preparation, and these two must be done sequentially. FISH was performed according 186 to Amann (1995). Table 3 summarizes the oligonucleotide probes used in this study, along 187 with the hybridization conditions and related references. Slides were viewed using a Zeiss 188 LSM 510 Meta Confocal laser scanning microscope (Zeiss, Germany) and the location of 189 important fields noted after the image was acquired. Subsequent polyP staining was conducted by incubation with  $1 \mu g m L^{-1}$  DAPI in dark for 60 min (Serafim et al., 2002). The 190 191 fields from which FISH images had been collected were located, and images of DAPI stains 192 were also recorded by the confocal microscope with filter sets that allow the emission 193 wavelength of 450-520 nm to pass through.

194

195 2.5.3. Scanning electron microscopy (SEM) analysis

196 Biomass samples were collected from the SBR, freeze-dried and analysed using a SEM with

197 a back-scattered electron detector (excitation voltage of 12 kV) to investigate the morphology

of bacteria cells. Energy dispersive X-ray spectroscopy (EDX) together with a SEM was usedfor elemental (phosphorus) analysis.

200

201 3. Results

**3.1. Phosphorus removal performance** 

Fig. 1 shows  $PO_4^{3-}P$  present in the influent and effluent of the SBR during all operating 203 204 periods. Bio-P removal was present in the SBR at the end of the start-up period, and the 205 removal efficiency was consistently near or above 90% in the subsequent operating periods 206 (1-4), where the SRT was varied from 2 days to 4 days (HRT maintained at 0.5 day). The 207 specific removal efficiency was highest at 2 days SRT (Table 4), and slightly decreased with increasing the SRT to 2.5 days and further to 3 and 4 days. Typical Bio-P removal profiles 208 obtained in the cycle studies performed during these periods are shown in Fig. 2. Based on 209 the  $PO_4^{3-}$ -P concentrations of the raw wastewater fed into the SBR and the dilution within the 210 SBR, the calculated  $PO_4^{3}$ -P concentrations in the SBR bulk liquid after the feeding were 211 much lower than the  $PO_4^{3}$ -P concentrations measured at the end of the feeding period (Fig. 212 2). This clearly indicates that  $PO_4^{3-}$  was released to the bulk liquid during the anaerobic phase 213 and taken up from the liquid in the subsequent aerobic phase, with  $< 3 \text{ mg PO}_4^{3-}\text{P L}^{-1}$ 214 215 remaining in the effluent. Phosphate release was strongly linked to the uptake of the available 216 carbon (represented by SCOD) in the SBR, and an example of the SCOD uptake profile in a 217 SBR cycle during Period 2 (2 days SRT, 0.5 day HRT) is shown in Fig. 3. The majority of 218 SCOD was consumed during the anaerobic phase (including the feeding period), with a small 219 fraction of SCOD uptake during the subsequent aerobic phase, indicating the residual SCOD 220 was non-biodegradable. Moreover, the removal efficiency was not influenced by extending 221 the HRT to 1 day (Period 5), but dropped during Period 6 and Period 7, likely due to 222 variations in the feed composition. At the end of Period 7, the Bio-P removal efficiency

223 returned to the previous level (Fig. 1), and was maintained when the HRT was extended to 1 day again in Period 8 with doubling the COD feeding (to 4000 mg COD  $L^{-1}$ ) to maintain a 224 225 similar COD load as previously. Again, this indicated the HRT did not have a substantial 226 impact on the Bio-P removal efficiency, but instead that the Bio-P removal capability was 227 mainly driven by SRT. Additionally, the SRT was reduced to 1.7 day to determine the 228 minimum SRT for achieving Bio-P removal. As shown in Fig. 2, the Bio-P removal was lost, as reflected by the lack of  $PO_4^{3-}$  release during the anaerobic phase, ultimately resulting in a 229 230 decreased removal efficiency.

231

#### 232 3.2. Changes in microbial community composition for different SRTs

233 Fig. 4 shows average abundances of the major bacterial groups in the SBR under operations 234 with 2-4 days SRTs (0.5 day HRT), with additional information provided in Supplementary 235 Information Fig. S1. The phylogenetic relationship of these bacterial groups is also shown in 236 Fig. 4 (bottom). Generally, the SBR microbial communities changed considerably with 237 changes in SRT, except Comamonadaceae and Xanthomonadaceae, which were present 238 consistently. The family *Comamonadaceae* in this case was primarily represented by two 239 genera, one predominant in all the tested periods (approximately 30%), and the other 240 emerging at 2.5 and 4 days SRTs (approximately 8%), possibly induced by variations in the 241 feed composition. Members affiliated with *Moraxellaceae* were also consistently present at 2, 242 2.5 and 3 days SRTs, but disappeared at 4 days SRT, where increased abundances of 243 Sphingomonadaceae, Flexibacteraceae and Accumulibacter were observed. Among these 244 bacterial groups, Comamonadaceae was most closely related to Accumulibacter compared to 245 other abundant groups, nominating it as an organism of interest for further investigation.

246

#### 247 **3.3. Identification of putative PAOs in the high-rate Bio-P removal process**

248 The ability to form and store polyP (a key feature of PAOs) by *Comamonadaceae* was further 249 investigated using FISH analysis and DAPI staining. There is no FISH probe available to 250 target the entire family of *Comamonadaceae*, but a previously published Cte probe is 251 targeting several prevalent genera in this family, including *Comamonas spp.*, Acidovorax spp., 252 Hydrogenophaga spp., and Aquaspirillum spp. (Schleifer et al., 1992). Bacterial cells 253 hybridized with the Cte probe were present in all biomass samples of 2-4 days SRTs. They 254 existed in three different morphotypes, including small rods, often present as single cells that 255 were either within or attached to the flocs, small cocci formed in tetrads occurring singly or 256 in clusters, and filaments often arranged in chains (an example is shown in Supplementary 257 Information Fig. S2). However, polyP was found only in tetrads according to the DAPI stain, 258 which showed intracellular yellowish granules suggesting polyP storage. Fig. 5 shows an 259 example of FISH images collected from a biomass sample of 2 days SRT, with the tetrads 260 hybridized with Cte and Eubmix probes displaying DAPI-positive polyP in the tetrads. This 261 strongly indicates that the Cte probe-defined *Comamonadaceae* with a tetrad morphology 262 (here called tetrad-Comamonadaceae) were putative PAOs. FISH hybridisation 263 simultaneously with DAPI (including the EUBmix probe) generally indicated no probe 264 binding in contrast with literature methods (Serafim et al., 2002), which may be due to the 265 high polyP content in the cells interfering with binding. Thus the microscopic examination of 266 FISH and DAPI staining were conducted separately in this study to obtain the photos shown 267 in Fig. 5.

268

In general, a small portion of short-rod shaped cells were also observed to be DAPI positive
in the samples at 4 days SRT, and identified as *Accumulibacter* by FISH analysis using
PAOmix probes (photos not shown).

273 As the tetrad-forming bacteria containing polyP at short SRTs (e.g. 2 days) were of particular 274 interest, they were further investigated by SEM combined with EDX elemental analysis. Fig. 275 6 shows SEM images and spot EDX analysis of tetrad-forming bacteria at 2 days SRT. 276 Strong phosphorus peaks were observed in all the cocci of the tetrads (one example shown in 277 Fig. 6A), along with some other peaks (the carbon and oxygen peaks originated from the 278 organic biomass matrix), while much lower levels of phosphorus were detected from the 279 biomass background (one example shown in Fig. 6B). The cellular phosphorus observed with 280 EDX was most likely polyP, which is a major component of intracellular phosphorus pools 281 stored in bacterial cells (Ohtake et al., 1994).

282

283 4. Discussion

#### **4.1. Impact of SRT on the high-rate Bio-P removal performance**

285 Complete phosphorus removal was achieved in the high-rate SBR with 2-4 days SRT, and the 286 specific removal rate appeared to increase with a decrease in SRT from 4 to 2 days. However, 287 further decreasing the SRT to 1.7 days resulted in the cessation of Bio-P removal, probably 288 due to wash out of functional PAOs from the SBR. This indicates an optimum of 2-2.5 days 289 SRT. In practise, a high-rate Bio-P removal process with such short SRTs can strongly 290 enhance the competitiveness of Bio-P removal process and expand applications over other 291 phosphorus removal methods, as this process allows substantial process intensification 292 through reducing reactor and clarifier volumes (correspondingly lower construction costs). It 293 should also be noted that in this high-rate Bio-P removal process, there was no 294 nitrification/denitrification for nitrogen removal due to the inability of nitrifiers to grow at 295 such short SRTs. If the practical treatment target is the combined nitrogen and phosphorus 296 removals, this high-rate Bio-P removal process can achieve only partial nitrogen removal due 297 to absorption and assimilation, rather than nitrification (Ge et al., 2013). It means the SBR

effluent may be required to be post-treated for residual nitrogen removal e.g. via an anammox process (a low energy-demand nitrogen removal process with no carbon requirement). This combined treatment process could still offer a number of benefits in terms of costs, energy demand and space requirements compared to conventional nutrient removal processes (see the detailed evaluation in Ge et al. (2013)), particularly where a high-nitrogen, low carbon effluent can be utilised for irrigation, and where sludge can be digested and phosphorus recovered from centrate.

305

306 There are extensive studies that evaluate Bio-P removal efficiencies at different SRTs, with 307 the majority focusing on SRTs between 8-12 days, which also enable nitrogen removal. A 308 shorter SRT of 5 days was tested in the studies of Choi et al. (1996) and Chang et al. (1996). 309 Bio-P removal was achieved in both cases but the phosphorus removal efficiency of 310 approximately 85% was slightly lower than the efficiency (>90%) obtained at 10 days SRT. 311 The SRT was further reduced to 3.2 days in the study of Mamais and Jenkins (1992), which 312 achieved a removal efficiency of approximately 90% at 3.2 days and 2.9 days SRTs. 313 However, the removal efficiency decreased to approximately 80% with further reducing the 314 SRT to 2.6 days, and to 40% at 2.3 days SRT, which is not consistent with the observations 315 in this study. This difference was likely due to the relatively low COD loading rate of the 316 SBR in their studies, which may not have provided sufficient carbon for PAOs. This need for 317 organic carbon is a challenge in applying short SRT Bio-P removal in domestic wastewater, 318 which has lower COD (300-500 mg COD  $L^{-1}$ ). However, the results here indicate the 319 essential metabolic capability existing for successful phosphorus removal exists at SRTs 320 down to 2 days, and can likely be applied to emerging low-energy, assimilative-adsorptive-321 accumulative high-rate aerobic wastewater treatment processes (Batstone et al., 2014), if 322 organic carbon can be suitably retained or supplied (e.g., from primary sludge hydrolysis).

323

# 4.2. Dynamic nature of microbial communities and correlations with the high-rate Bio-P removal process

326 This is the first molecular study to determine bacterial community diversities and dynamics 327 of Bio-P removal processes at short SRTs (<4 days). Generally, the bacterial communities are 328 very dynamic under different SRTs in the SBR, but the population of Comamonadaceae was 329 consistently present in the functionally stable SBR. Comamonadaceae has been commonly 330 detected in activated sludge wastewater treatment processes at both full and lab scales, and is 331 capable of consuming a wide variety of organic acids, including amino acids (Willems, et al., 332 1991). The versatile nature of *Comamonadaceae* may have given them a competitive 333 advantage to become abundant in the high-rate SBR, as proteins that are among the main 334 components in the abattoir wastewater used in this study and could be broken down to amino 335 acids, could allow Comamonadaceae to outcompete organisms that are only capable of 336 utilising VFAs. Moreover, altering SRT in the SBR resulted in changes of the reactor 337 performance, which may have also influenced the SBR communities. For example, the 338 population of Moraxellaceae was nearly eliminated at 4 days SRT compared with 2-3 days 339 SRTs, possibly because *Moraxellaceae* were inhibited by high-ammonia present at a 4 day 340 SRT (resulting from an increase in protein hydrolysis).

341

Variations in the feed composition (organics in abattoir wastewater) were also observed to affect the bacterial community structure in the SBR. For example, *Saprospiraceae* (Fig. S1) emerged in an operating period with an SRT of 2.5 days, but was not present in other periods at SRTs of 2 and 3 days. This indicates that the selection pressure due to changes in the feed composition may have had further influence on the bacterial community compositions in addition to the SRT. Variations in the compositions of abattoir wastewater across different

collections (e.g. containing more proteins) may have given *Saprospiraceae* a transient
advantage over the rest of the mixed microbial community, as *Saprospiraceae* has been
reported to be capable of hydrolysing proteins (Xia et al., 2008). Similarly, *Chitionphagaceae*became more abundant during the two subsequent operating Periods 2-3 (2 and 4 days SRTs),
which could also be for the same reason.

353

354 Although SRT was a dominant driver for microbial community, the Bio-P removal was 355 functionally very stable in the SBR during Periods 1-4 for over 100 days. It suggests that 356 population shifts or community fluctuations under different stress conditions caused by 357 environmental/operational changes (e.g. variations of wastewater compositions, HRT, etc.) 358 still allowed functional stability for Bio-P removal. This indicates that different PAO 359 populations appeared in the community (see e.g. the different Comamonadaceae genera 360 present at 4 days SRT) with similar capability, thereby ensuring the stability of the Bio-P 361 removal process.

362

#### 363 4.3. Putative PAOs responsible for the high-rate Bio-P removal process

364 This study has shown that the Cte probe-defined tetrad-Comamonadaceae is likely to be an 365 important group of PAOs present in the high-rate Bio-P removal process, as they were 366 present in large amounts and accumulated polyP as indicated by DAPI staining. Although the 367 family of *Comamonadaceae* contains numerous genera, they have diverse ecophysiological 368 behaviours. For example, genus *Curvibacter* is likely to be involved in protein hydrolysis and 369 denitrification (Nielsen et al., 2010) and genus Malikia has been identified as a PHA and 370 polyP accumulating bacterium (Spring et al., 2005). This may indicate that different genera of 371 Comamonadaceae as identified here may play different roles in the high-rate Bio-P removal 372 process, such as proteolysis to supply soluble carbon and/or polyP accumulation. We

- attempted to utilise more specific FISH probes, including the ACI208 probe for Acidovorax
- 374 *spp.* (Amann et al., 1996). However, this did not bind to tetrad-*Comamonadaceae*.
- 375

376 Bacterial cells of *Comamonadaceae* with a tetrad morphology were observed for the first 377 time in this study. Tetrad-forming organisms have been observed in Bio-P removal systems before, which have been shown, phylogenetically, to be members of the Alphaproteobcteria 378 379 (e.g. Amaricoccus spp., and 'Defluvicoccus vanus'), Betaproteobacteria (Quadracoccus sp.), 380 Gammaproteobacteria and Actinobacteria (Tetrasphaera spp., Micropruina glycogenica and 381 Kineosphaera limosa) (Maszenan et al., 2005; Oehmen et al., 2007; Nguyen et al., 2011). 382 Understanding of the relevance of this morphology to Bio-P is limited, although preliminary 383 investigations have been made, such as 'Defluvioccus'-related tetrad-forming organisms 384 showing phenotypic traits similar to GAOs (Wong et al., 2004), and Tetrasphaera forming 385 clusters of tetrads identified as a putative PAO (Nguyenn et al., 2011). Moreover, it is still 386 unknown what factors (e.g. process operation, wastewater composition, etc.) induce bacterial 387 cells to arrange themselves in tetrads, and what benefits can be obtained from this 388 arrangement. The need for future studies may therefore mainly be related to the 389 understanding of key factors that affect the morphotypes of Comamonadaceae and the 390 relations to their phenotypes.

391

#### 392 5. Conclusions

Bio-P removal can be achieved in the high-rate SBR with short SRTs (<4 days) treating abattoir wastewater, with the specific removal efficiency being highest at 2-2.5 days SRTs. Reducing the SRT further to 1.7 days resulted in a drastic decrease of Bio-P removal performance in the SBR. Varying SRTs in the SBR also influenced the bacterial community compositions, but the population of *Comamonadaceae* was consistently dominant in the

functionally stable SBR with 2-4 days SRTs. Bacterial cells of *Comamonadaceae* (Cte probedefined) arranged in tetrads contained positive DAPI stained polyP, indicating *Comamonadaceae* was a strong candidate as the responsible PAO in this high-rate Bio-P
removal process.

402

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Characteristic	Wastewater
TCOD ( $g L^{-1}$ )	$2.9 (0.2)^a$
$\text{SCOD}^{b}$ (g L <sup>-1</sup> )	1.0 (0.1)
pH	7-7.5
$TKP^b \ (mg \ L^{-1})$	28.2 (1.1)
$PO_4^{3-}-P (mg L^{-1})$	23.4 (0.6)

Table 1 – Characteristics of the wastewater used in this study.

<sup>a</sup>: Standard deviations shown in parenthesis are based on 17 different wastewater samples

collected over a 10 months period.

<sup>*b*</sup>: SCOD: Soluble COD; TKP: Total Kjeldahl phosphorus.

Operating period	HRT (day)	Target SRT (day)	Actual SRT (day)
Start-up (55 days)	0.5	2	2.1
Period 1 (33 days)	0.5	3	2.8
Period 2 (21 days)	0.5	2	1.9
Period 3 (28 days)	0.5	4	3.8
Period 4 (27 days)	0.5	2.5	2.3
Period 5 (25 days)	1	2.5	2.4
Period 6 (27 days)	1	2	2
Period 7 (39 days)	0.5	2	2
Period 8 (15 days)	1	2	2
Period 9 (9 days)	1	1.7	1.7

Table 2 – Summary of the SBR operating conditions in this study.

Table 3 – Oligonucleotide probes used for FISH.

Probe	Specificity	Sequence (5'-3')	Formamide%	References
ACI208	Acidovorax spp.	CGCGCAAGGCCTTGC	20	Amann et al. (1996)
	Commonae en Acidovorar en			
	Comamonas spp., Actaovorax spp.,		20	
Cte		TICCATCCCCTCTGCCG	20	Schleifer et al. (1992)
	Hydrogenophaga spp., Aquaspirillum spp.			
EUB338		GCTGCCTCCCGTAGGAGT	0-50	Amann et al. (1990)
		$\sim$		
EUB338 II	Most hacteria	GCAGCCACCCGTAGGTGT	0-50	Daims et al. $(1999)$
LOD550 II	most bacteria	GEAGEEACCEGIAGOIGI	0-50	
			0.50	
EUB338 III		GCTGCCACCCGTAGGTGT	0-50	Daims et al. (1999)
PAO462		CCGTCATCTACWCAGGGTATTAAC	C 35	Crocetti et al. (2000)
PAO651	Most Accumulibacter	CCCTCTGCCAAACTCCAG	35	Crocetti et al. (2000)
1110051	most neeununouen		55	elocota et ul. (2000)
			25	
PAU846		GTIAGCIACGGCACTAAAAGG	55	Crocetti et al. (2000)

EUB338, EUB338II and EUB338III were applied simultaneously as EUBmix. PAO264, PAO651, PAO846 were used together in a mixture called PAOmix.

	UDT	(D)T	$PO_4^{3-}$ -P removal	Specific PO <sub>4</sub> <sup>3-</sup> -P removal
Operating period	HRT	SRT	(%)	$(mg gVSS^{-1}d^{-1})$
Start-up	0.5d	2.1d	58.7±6.3	4.8±0.6
Period 1	0.5d	2.8d	95.8±2.3	8.9±0.2
Period 2	0.5d	1.9d	90.7±3.1	11.4±0.2
Period 3	0.5d	3.8d	88.8±2.1	7.2±0.1
Period 4	0.5d	2.3d	91.3±3.6	9.4±0.3
Period 5	1d	2.4d	89.4±1.5	5.8±0.1
Period 6	1d	2.0d	77.6±4.1	7.8±0.2
Period 7	0.5d	2.0d	65.2±4.9	9.4±0.3
Period 8	1d	2.0d	96.1±1.6	8.0±0.1
Period 9	1d	1.7d	51.3±3.5	7.0±0.3

Table 4 – A Summary of the phosphate ( $PO_4^{3-}P$ ) removal performance in the high-rate SBR.

Error margins indicate 95% confidence intervals across different measurements over each period.



Fig. 1 – Phosphate  $(PO_4^{3-})$  concentrations in influent and effluent across the whole operating period.



Fig. 2 – Phosphate ( $PO_4^{3-}$ ) profiles during the SBR cycle studies performed in the different operating periods. Open symbols shown at 5 min represent the dilution-based, calculated  $PO_4^{3-}$  concentrations in the SBR after feeding, corresponding to the equivalent closed symbol operations (the calculation considers the  $PO_4^{3-}$  concentrations of the raw wastewater fed into the SBR and the dilution within the SBR).



Fig. 3 – SCOD profiles in a SBR cycle under the SBR operation of 0.5 day HRT and 1.9 days SRT. Open symbols shown at 5 min represent the dilution-based, calculated SCOD concentration in the SBR after feeding, corresponding to the equivalent closed symbol operation (the calculation considers the SCOD concentration of the raw wastewater fed into the SBR and the dilution within the SBR).



Fig. 4 – Average abundances of the major bacterial groups (family level, except the genus of *Accumulibacter*) in the SBR operated at 2-4 days SRTs and their maximum likelihood phylogenetic relationship according to Dereeper et al. (2008) (*Comamonadaceae\_1* and *Comamonadaceae\_2* mean different genera within the family *Comamonadaceae;* Standard deviations shown in parenthesis are based on three sequential samples analysed at each of the three SRTs).



Fig. 5 – FISH and DAPI staining images of tetrad-forming bacteria in the high-rate SBR with 2 days SRT. (A) FISH image shows tetrad-forming bacteria hybridizing with bacterial probe Cte (red). (B) FISH image shows tetrad-forming bacteria hybridizing with bacterial probes EUBmix (green) and Cte (red). The overlay of red and green is yellow. (C) Tetrad-forming bacteria containing polyphosphate stained by DAPI. Polyphosphate emits a bright yellow colour and bacterial cells emit blue colour. The overlay of yellow and blue is bright white.



Fig. 6 – Characterisation of tetrad-forming bacteria using scanning electron microscope (SEM). (A) SEM image of typical tetrad-forming bacteria. The energy dispersive X-ray (EDX) spectrum shown below was collected from the specific spot within tetrad-forming bacteria indicated in the above image. (B) shows the EDX spectrum collected from the specific spot outside of tetrads-forming bacteria.

Biological phosphorus removal from abattoir wastewater at very short sludge ages mediated by novel PAO clade *Comamonadaceae* 

## **Research Highlights:**

Bio-P removal was achieved in a SBR based activated sludge process with < 4 days SRTs.

► The process was most effective at 2-2.5 days SRTs, but inhibited at 1.7 days SRT.

► Ability of polyphosphate storage was found in a novel PAO clade *Comamonadaceae*.

► The process can be integrated with short SRT, energy-efficient carbon removal

processes.

# Supplementary Information

**Manuscript title:** Biological phosphorus removal from abattoir wastewater at very short sludge ages mediated by novel PAO clade *Comamonadaceae* **Authors:** Huoqing Ge, Damien J. Batstone, Jürg Keller\*



Fig. S1 – Microbial communities (family level, expect the order of *BD7-3*) identified by 16S rRNA gene Pyrotag sequencing in the SBR in the start-up period (Day 34, Day 40, Day 52) and Periods 1-4 (Day 62, Day 72, Day 80, Day 98, Day 105, Day 110, Day 116, Day 128, Day 145 and Day 158). (S represents SRT, *Comamonadaceae\_1* and *Comamaonadaceae\_2* mean different genera within the family *Comamonadaceae*)



Fig. S2 – The FISH image of probe Cte-defined bacteria in activated sludge from the highrate SBR at 2 days SRT. It shows bacteria hybridizing with the bacterial probes Eubmix (green) and probe Cte (red) with different morphologies: small rods and filaments. The overlay of red and green is yellow.

Characteristic	Wastewater
$TKN^{a} (mg L^{-1})$	$110(15)^{b}$
$NH_4^+-N (mg L^{-1})$	65 (9)
Particulate N (mg L <sup>-1</sup> )	43 (1.1)

Table S1 – Nitrogen concentrations in the abattoir wastewater used in this study.

<sup>*a*</sup>: TKP: Total Kjeldahl nitrogen;  $NO_3^-$  and  $NO_2^-$  were also detected at much lower levels (data now shown).

<sup>b</sup>: Standard deviations shown in parenthesis are based on 17 different wastewater samples collected over a 10 months period.