

## Accepted Manuscript

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PII: S1385-8947(14)00806-7  
DOI: <http://dx.doi.org/10.1016/j.cej.2014.06.075>  
Reference: CEJ 12314

To appear in: *Chemical Engineering Journal*

Received Date: 6 March 2014  
Revised Date: 15 June 2014  
Accepted Date: 16 June 2014



Please cite this article as: J. Guo, Y. Peng, S. Wang, X. Yang, Z. Yuan, Filamentous and non-filamentous bulking of activated sludge encountered under nutrients limitation or deficiency conditions, *Chemical Engineering Journal* (2014), doi: <http://dx.doi.org/10.1016/j.cej.2014.06.075>

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1 **Filamentous and non-filamentous bulking of activated sludge encountered under**  
2 **nutrients limitation or deficiency conditions**

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16

17 **Abstract:** Although the limitation or deficiency of nutrients, such as nitrogen (N) and  
18 phosphorus (P), has been one of the frequently reported factors causing filamentous or  
19 non-filamentous bulking of activated sludge, the mechanisms are still unclear. In this  
20 work, the long-term effects of N and P limitation or deficiency on sludge settleability  
21 and bioflocculation characteristics were investigated in six sequencing batch reactors  
22 (SBRs) fed with wastewater with different nutrient availability. The sludge volume  
23 index (SVI), microbial community structures, intracellular poly- $\beta$ -hydroxyalkanoates  
24 (PHAs) and extracellular polymeric substances (EPS) were characterised over time.  
25 Bulking was not observed in SBRs with N limitation or deficiency, in which SVI  
26 remained below 150 mL/g. In contrast, bulking was encountered in those reactors  
27 with P deficiency. The occurrence of non-filamentous bulking was associated with a  
28 higher carbohydrates fraction and a lower proteins fraction in EPS. In the case of  
29 filamentous bulking, SVI correlated negatively with the amount of PHAs. Our  
30 experimental data support the hypothesis that the occurrence and/or the type of  
31 bulking in activated sludge could be affected by the combination of kinetic selection,  
32 microbial storage, as well as the EPS composition.

33 **Keywords:** sludge settleability; filamentous bulking; non-filamentous bulking;  
34 substrate storage; extracellular polymeric substances (EPS); filamentous bacteria

35

## 36 1. Introduction

37 The performance of an activated sludge system for biological wastewater treatment is  
38 often deteriorated due to sludge separation problems caused by sludge bulking.

39 Bulking consists of filamentous bulking due to excess proliferation of filamentous  
40 bacteria [1] and non-filamentous bulking (also known as *Zoogloea* bulking or viscous  
41 bulking) [2], resulting from certain microbes that produce large amounts of  
42 biopolymers on their surface [3].

43 The causes for inducing filamentous bulking are complicated [4] and include  
44 factors such as low dissolved oxygen (DO) concentrations [5-7], low organic loading  
45 rates [8], low substrate concentration gradients [9], low pH [10], and low  
46 temperatures [11]. Nutrient limitation [12] has also been identified as a factor for the  
47 proliferation of filamentous bacteria in activated sludge. In order to obtain well-  
48 settling sludge, the ratio of biological oxygen demand (BOD) to nitrogen (N) to  
49 phosphorus (P) in influent should generally satisfy 100:5:1 [1]. Peng et al. [13]  
50 showed that filamentous bulking was stimulated by the lack of either N or P in the  
51 feed. However, the simultaneous absence of both N and P did not induce filamentous  
52 bulking [13]. Low nutrient supplies have also been suggested to cause non-  
53 filamentous bulking. It was reported that activated sludge treatment of nutrient-  
54 deficient wastewater such as some types of industrial wastewaters led to severe slime  
55 formation and consequently biomass separation difficulties due to non-filamentous  
56 bulking [2, 14, 15]. Non-filamentous bulking at a full-scale wastewater treatment  
57 plant (WWTP), which was hypothetically due to low concentrations of soluble  
58 phosphate (0.2 mg/L), was solved by supplying additional soluble phosphate [16].

59 However, the mechanisms involved in both filamentous and non-filamentous  
60 bulking induced by nutrient limitation/deficiency are not fully understood at present.

61 There is still controversy about which bulking type would be caused under nutrient  
62 limitation. On one hand, it is hypothesised that nutrient deficiency has an effect on the  
63 competition between floc-forming and filamentous bacteria, causing filamentous  
64 bulking when filamentous bacteria proliferate due to their enhanced ability to uptake  
65 substrates under stress conditions [13, 17]. On the other hand, nutrient limitation has  
66 also been hypothesised to induce the production of extracellular polymeric substances  
67 (EPS) on the surface of microorganisms [18]. The EPS are important for the  
68 physicochemical properties of activated sludge flocs and have been implicated to  
69 affect sludge settling properties [19], inducing non-filamentous bulking. In addition,  
70 when sludge is subject to nutrients limitation or deficiency, more carbon substrate can  
71 be used for accumulation of poly-hydroxyalkanoates (PHA) and glycogen [20], which  
72 would affect the competition between filaments and floc-formers, as well as sludge  
73 settleability.

74 The objective of this study was to shed light on the mechanism of filamentous and  
75 non-filamentous bulking of activated sludge induced by nutrients limitation or  
76 deficiency, through a comprehensive experimental study. Six lab-scale sequencing  
77 batch reactors (SBR) were operated for 130-230 days with various nutrients-supplying  
78 conditions. The sludge volume index (SVI), PHA storage and EPS composition, Gram  
79 and Neisser staining, fluorescent *in situ* hybridization (FISH) and microscopic  
80 observations were used to monitor sludge properties and to track the changes of  
81 microbial morphology and community structure. These experimental data led to the  
82 connections between bulking type and the associated sludge properties, including

83 sludge settleability, microbial structure, intracellular storage and extracellular  
84 polymeric substrates under the stress condition of nutrients limitation or deficiency.

85

## 86 **2. Materials and Methods**

### 87 **2.1 Lab-scale SBR reactors**

88 The experiments were performed in six identical SBRs each with a 12-L working  
89 volume. Each reactor was equipped with an air compressor for aeration and a stirrer  
90 for mixing. Operation of the SBRs was based on 6 h cycles consisting of a feed phase  
91 (10 min) in which 6 L fresh medium was supplied giving rise to a hydraulic retention  
92 time of 12 h, an anoxic phase (110 min), an aerobic phase (180 min), a settling phase  
93 (50 min) and an effluent withdrawal phase (10 min) in which 5.85 L of reactor  
94 supernatant were withdrawn. The bulk liquid DO concentration in aerobic periods was  
95 controlled at  $2.0 \pm 0.2$  mg/L under aerobic periods. Temperatures in all reactors were  
96 controlled at  $25 \pm 2$  °C. pH was recorded but not controlled, and fluctuated between 7.0  
97 and 7.5. The biomass concentrations in all reactors were kept in the range of  
98 1800~2400 mg/L with sludge wasting that ensured an operation at a sludge age of 20  
99 days of each reactor. The surfaces of tube, pumps and reactors were cleaned manually  
100 weekly in order to prevent biomass attachment.

101 The feed conditions for the SBRs are summarised in Table 1. SBRs 1-4 were  
102 operated for 233 days, to investigate the effects of nutrient deficiency on sludge  
103 settleability and microbial community structure. With COD/N/P ratios being  
104 300:30:10 in the feed, SBR1 was operated as a control. SBR2 (COD/N/P set at

105 300:0:10), SBR3 (COD/N/P set at 300:30:0) and SBR4 (COD/N/P set at 300:0:0)  
106 were operated to investigate the effects of N, P and simultaneous N&P deficiency  
107 respectively. In order to investigate the combined effects of sludge cultivation history  
108 and influent nutrient ratios, which may affect the types of bulking and the dominant  
109 filaments, two additional reactors (SBRs 5-6) were operated for 130 days in three  
110 phases. Phase I (days 1-24) was used to collect base line data with normal feed  
111 (COD/N/P set at 300:30:15). The effects of N limitation (COD/N/P set at 300:5:15)  
112 and P limitation (COD/N/P set at 300:30:1) on sludge proprieties were investigated  
113 during Phase II (days 25-66) in SBR5 and SBR6, respectively. The effects of N  
114 deficiency and P deficiency on sludge proprieties were further investigated during  
115 Phase III (days 67-130).

## 116 **2.2 Synthetic wastewater and seeding sludge**

117 The medium for the SBRs consisted of a carbon source, a nutrient solution and a trace  
118 element solution. The normal synthetic wastewater contained  $\text{CH}_3\text{COONa}$  of 4.69  
119 mM (300 mg COD/L),  $\text{NH}_4\text{Cl}$  of 2.14 mM (30 mg N/L),  $\text{KH}_2\text{PO}_4$  of 0.32 mM (10 mg  
120 P/L in SBRs 1-4) or 0.48 mM (15 mg P/L in SBRs 5-6),  $\text{MgSO}_4 \cdot 7\text{H}_2\text{O}$  of 0.37 mM,  
121  $\text{KCl}$  of 0.48 mM,  $\text{CaCl}_2 \cdot 2\text{H}_2\text{O}$  of 0.10 mM and 1 mL/L of the following trace element  
122 solution: EDTA 10 g/L,  $\text{ZnSO}_4 \cdot 7\text{H}_2\text{O}$  0.12 g/L,  $\text{Na}_2\text{MoO}_4 \cdot 2\text{H}_2\text{O}$  0.06 g/L,  
123  $\text{MnCl}_2 \cdot 4\text{H}_2\text{O}$  0.12 g/L, KI 0.18 g/L,  $\text{CuSO}_4 \cdot 5\text{H}_2\text{O}$  0.03 g/L,  $\text{H}_3\text{BO}_3$  0.15 g/L,  
124  $\text{FeCl}_3 \cdot 6\text{H}_2\text{O}$  1.5 g/L. Under the conditions of nutrients limitation and deficiency, N  
125 and/or P concentrations in the synthetic wastewater were modified according to the  
126 specific values describe in Table 1.

127 Each SBR was inoculated with 2 L seed sludge from the secondary clarifier of the  
128 GaoBeiDian WWTP (Beijing, China). The seed sludge had a good settling property  
129 (SVI < 100 mL/g), in which only limited filamentous bacteria (Type 0092 as the  
130 dominant filament) were present as a floc backbone.

### 131 **2.3 Analytical methods**

132 The temperature, pH and DO were monitored on line using WTW pH/DO meters  
133 (WTW Multi 340i, Germany). Supernatant samples in all reactors were collected 2-3  
134 times every week to monitor effluent quality. Cycle studies were performed every 3  
135 weeks for all SBRs. Samples were analyzed after filtration through 0.45  $\mu\text{m}$  filter.  
136 COD,  $\text{NH}_4^+\text{-N}$ ,  $\text{NO}_2^-\text{-N}$ ,  $\text{NO}_3^-\text{-N}$ ,  $\text{PO}_4^{3-}\text{-P}$ , mixed liquor suspended solids (MLSS) and  
137 mixed liquor volatile suspended solids (MLVSS) were measured according to  
138 Standard Methods [21]. When conducting cycle studies, PHA and acetate analysis  
139 was carried out as described by Oehmen et al. [22].

### 140 **2.4 Microscopic observation and fluorescence in situ hybridization (FISH)**

141 Microscopic observation of mixed liquor samples was performed every week using an  
142 OLYMPUS-BX61 (Japan). Filamentous index (FI), a method of subjective scoring of  
143 filamentous bacteria abundance suggested by Eikelboom [1], was used to evaluate the  
144 abundance of filamentous bacteria present in the samples. The dominant filamentous  
145 bacteria were identified based on morphology observation, Gram and Neisser staining,  
146 and a sulfur deposit test according to Eikelboom [1] and Jenkins [2]. FISH was also  
147 conducted for further identifying the dominant filamentous bacteria as previously  
148 described [23-25]. Table S1 (Supporting Information) shows a list of oligonucleotide



149 probes used in this study. The images of FISH samples were captured using an  
150 OLYMPUS-BX61 fluorescence microscope.

## 151 **2.5 EPS extraction**

152 Sludge samples were collected from all reactors every 1-2 weeks for characterisation  
153 of the EPS composition over time. The EPS extraction methods were previously  
154 described in Guo et al. [26]. Total extractable EPS was defined as the sum of proteins,  
155 carbohydrates and DNA. Carbohydrates were determined using the anthrone method  
156 with the glucose standard (Aldrich). Proteins were measured with the Lowry  
157 procedure using BSA (bovine serum albumin) as standard. DNA was measured in the  
158 extracted EPS samples according to the method described in Frolund et al. [27].

159

## 160 **3. Results**

### 161 **3.1 Reactor performance**

162 The COD removal efficiency of SBRs 1, 2 and 5 were consistently above 85%, with  
163 the average COD concentration in effluent lower than 50 mg/L. In comparison, COD  
164 removal efficiencies were consistently lower for SBRs 3, 4 and 6 (50~65%). The  
165 effluent COD concentration was frequently higher than 100 mg/L, particularly when  
166 bulking occurred. For the control reactor (SBR1), the average  $\text{NH}_4^+\text{-N}$ ,  $\text{NO}_2^-\text{-N}$ ,  $\text{NO}_3^-\text{-N}$   
167 and  $\text{PO}_4^{3-}\text{-P}$  concentrations were 0.2, 0.8, 10.3 and 4.3 mg/L, respectively. SBRs 5  
168 and 6 in Phase I (with normal feed) showed good nitrification, phosphorus release and  
169 uptake performance. However, the deterioration of the P removal was caused by N  
170 limitation or deficiency, and deterioration of the N removal was caused by P

171 limitation or deficiency in Phases II and III. Similar phenomenon was observed in  
172 other reactors (SBRs 2, 3 and 4) with limited nutrient influent. No nitrification and  
173 denitrification were observed in SBRs 2 and 4. No clear phenotype of enhanced  
174 biological phosphorus removal was found in SBRs 3 and 4. The phenomenon of  
175 phosphorous release and uptake was observed in SBRs 1, 2 and 5, despite with poor P  
176 removal efficiency. Phosphorous concentrations in effluent of SBRs 1 and 5 were  
177 lower than 5 mg P/L, while the average effluent phosphorous concentration in SBR 2  
178 was higher than 9.1 mg P/L. The detailed effluent concentrations can be found in  
179 Table S2 (Supporting Information).

### 180 **3.2 Sludge settling properties**

181 Various influent nutrient ratios led to different sludge settleability, as evidenced by  
182 different SVI profiles (Fig. 1). SVIs in SBRs 1-4 slightly increased in the initial 30  
183 days but gradually decreased to below 150 mL/g in the following 60 days, which  
184 might be associated with the adaptation of microorganisms to laboratory conditions  
185 including the synthetic feed. From day 90, sludge settleability expressed in SVI  
186 showed different trends. The settling property of the SBR1 sludge with a normal  
187 influent nutrient ratio was generally very good with a SVI in the range of 40–130  
188 mL/g. Good sludge settleability with SVI of 40–125 mL/g was also obtained in SBR2,  
189 to which an influent without N was fed (C: N: P as to be 300/0/10). In SBR3 fed with  
190 influent without P, SVI was significantly higher than that in SBR1 and was in the  
191 range of 90–150 mL/g. However, the simultaneous N and P deficiency applied to  
192 SBR4 resulted in poor sludge settleability with SVI of 122-355 mL/g from day 90 to

193 day 230, which was higher than that in SBR3 during the corresponding period. The  
194 deficiency of P seemed to lead to poorer settleability while the deficiency of N did not.

195 SVI levels of the SBRs 5 and 6 sludges slightly increased to 150 mL/g in the initial  
196 10 days and then became below 100 mL/g at the end of Phase I (Fig. 1b). In Phase II,  
197 good sludge settleability was maintained in both reactors, with the average SVI being  
198 62 and 80 mL/g, respectively, despite of the imposition of N and P limitation,  
199 respectively. Subsequently, SBR5 and SBR6 were operated with wastewater without  
200 N or P, respectively (Phase III). Distinctly, the SVI of SBR6 (no P in the feed) rose  
201 rapidly after Day 100 (up to 500-600 mL/g) due to serious sludge bulking. In  
202 comparison, the settleability SBR5 (no N in the feed) remained stable.

### 203 **3.3 Growth of filamentous bacteria**

204 Microscopic observation was conducted to monitor the change of sludge morphology  
205 (as shown in Fig. 2) and the growth of filamentous bacteria. The growth of  
206 filamentous bacteria (FI of 2-3 in a scale of 0-5, as shown in Table 2) was observed in  
207 SBR3 with the deficiency of P. Many filamentous bacteria were present in the sludge  
208 (FI of 3-4 in a scale of 0-5) in SBR4 (Fig. 2d), in contrast to other reactors SBRs 1, 2  
209 and 5, where much fewer filamentous bacteria were present (FI lower than level 2).  
210 Interestingly, the microorganisms in the SBR6 sludge were primarily floc-forming  
211 bacteria, and few filamentous bacteria (FI below 1) extended from the flocs, although  
212 high SVI was observed in this reactor (Fig. 2f). Thus, filamentous bacteria were not  
213 responsible for the increased SVI and non-filamentous bulking (viscous bulking)  
214 occurred in SBR6. In fact, microscopic observation showed a change from normal

215 compact flocs (average diameter ca. 100  $\mu\text{m}$ ) to much more open, loose and  
216 irregularly shaped flocs, and with many free-swimming bacteria. In comparison, the  
217 well-settling sludge (average SVI of 50 mL/g) in SBR5 contained dense and compact  
218 flocs (Fig. 2e), in spite of some limited filaments growing out of flocs.

219 Gram and Neisser staining and FISH analysis were employed for identification of  
220 the dominant filamentous bacteria in systems with filamentous bulking. Various  
221 influent nutrient ratios resulted in different dominant filamentous bacteria (Table 2,  
222 Fig. 3). In SBR1 with normal influent nutrient ratios, no distinct filaments extended  
223 from the flocs, despite that some Type 0092 and Type 0041 filamentous were found  
224 inside the flocs. Although no filamentous bulking occurred in SBR2 fed with influent  
225 without N, short and slightly bowed Type 0092 (filament length usually smaller than  
226 200  $\mu\text{m}$ ) extended out from the flocs. Compared to SBR2 with lower filament  
227 diversity, more types of filaments, including Type 021N, Type 0092 and *M. parvicella*  
228 with very small numbers were detected in SBR5. The dominate filamentous bacteria  
229 in SBR3 have a morphology similar to that of the *Nostocoida limicola*-like filaments  
230 as described in [1, 2], but did not bind to the probes of NLIMI91 or NLIMIII301 [28].  
231 Moreover, FISH analysis indicated that *T. nivea* were present in very small numbers  
232 in SBR3. There seemed to be two types of *N. limicola* possibly occurred in SBR3.  
233 One type produced relatively long filaments ( $> 200 \mu\text{m}$ ). Cells were oval shaped with  
234 cell septa clearly observable. This type of filament was not only found with the floc  
235 structure but also in the bulk solution. The filament staining is Gram positive and  
236 Neisser negative (yellow). On the other hand, another type of *N. limicola*-like was

237 mostly observed in the bulk solution, and sheathed filaments composed of rectangular,  
238 also with distinct septa. Gram staining is positive. Specially, Neisser staining is  
239 positive (purple). In SBR4, the most dominant filaments, in an excessive abundance  
240 level (FI of 3-4), were *N. limicola*-like. A relatively smaller number of Type 0092 (FI  
241 of 1-2) was also found. However, the characteristics of *N. limicola*-like in SBR4  
242 showed some differences from those in SBR3. They are Gram positive and Neisser  
243 positive (purple). As reported, *N. limicola*-like are often found in industrial  
244 wastewater with low nutrients [2]. With decreased the influent N concentration in  
245 SBR5, a limited number of Type 021N and Type 0092 extended out from the flocs.

#### 246 **3.4 PHA storage**

247 Although it is widely reported that nutrient limitation is favourable for PHA synthesis  
248 in microbial cells (Third et al., 2003), the effect of storage phenomena on sludge  
249 settleability has not been thoroughly studied [29], in particular under the nutrients  
250 limitation or deficiency condition. In this study, sludge samples were collected every  
251 3 weeks for the measurement of PHA, including poly- $\beta$ -hydroxybutyrate (PHB), poly-  
252  $\beta$ -hydroxyvalerate (PHV) and poly- $\beta$ -hydroxy-2-methylvalerate (PH2MV). Table 2  
253 compares the average PHA concentration in all reactors and Fig. 4 plots SVI against  
254 the stored intracellular PHA, measured in all reactors during the course of the study.  
255 PHA storage amounts in N limitation or deficiency systems (SBRs 2 and 5) were  
256 clearly higher than in all other reactors including those with P limitation or deficiency  
257 (SBRs 3 and 6). Our results are consistent with the previous observation that PHA  
258 accumulation is favoured under low ammonium concentrations [20]. Surprisingly,

259 however, the limitation or deficiency of P, which is also key element for cell growth,  
260 did not stimulate PHA accumulation. SBR4 with simultaneous N and P deficiency had  
261 the lowest PHA concentration. SBRs 3 and 6 (Phase III) fed with P-deficient influent,  
262 also had low PHA contents. The higher accumulation of PHA in SBR2 and SBR5  
263 coincided with the excellent sludge settleability. In comparison, poorer settleability  
264 was obtained in SBRs 3, 4 and 6, where lower PHA contents were accumulated in  
265 sludge samples. Storage phenomenon in the form of PHA has previously been found  
266 to have an important role on sludge settleability [29, 30]. Compared to floc-formers,  
267 most of filaments are supposed to have no or lower ability to store substrates [30, 31].  
268 In this case, most of substrates were used for storage under the feast phase and the  
269 growth of filaments would be restricted.

### 270 **3.5 Formation of EPS**

271 Sludge settleability of activated sludge is greatly related to its EPS properties [32, 33].  
272 Therefore, the main components of EPS including carbohydrates, proteins and DNA  
273 were quantified in order to identify any correlation between SVI and the amount and  
274 composition of EPS (Figure 5 and Table S3). There is no significant correlation  
275 between the total amount of EPS and sludge settleability (Fig. 5a), which is consistent  
276 with the results reported by Liao et al. [34]. However, the carbohydrates fraction of  
277 EPS is positively correlated with SVI ( $R^2=0.5990$ ), while the proteins fraction is  
278 negatively correlated with SVI ( $R^2=0.5073$ ) (Fig. 5b and 5c, respectively). For SBRs  
279 2 and 5, both with N limitation/deficiency and good sludge settleability, the  
280 composition of EPS is very similar, despite. In both reactors, 17-19% of the  
281 extracellular substances is attributed to carbohydrates and 75-80% to proteins.  
282 Increases in the carbohydrates contents were observed in all SBRs (3, 4 and 6) with P

283 deficiency. For SBRs 3 and 4 with filamentous bulking sludge, low proteins (62-76%)  
284 and high carbohydrates content (20-30%) were observed in EPS. In contrast, a higher  
285 carbohydrates content ( $27\pm 10\%$ ) and a lower proteins content ( $69\pm 9\%$ ), compared to  
286 other reactors, were observed in Phase III in SBR6, where viscous bulking occurred.  
287 When serious non-filamentous bulking was encountered at the end of Phase III, the  
288 carbohydrates fraction reached 42% and the proteins fraction dropped to a level of  
289 55%.

290 When SVI was plotted against the carbohydrates or proteins fractions for each  
291 reactor (Fig. S1, SI), no significant correlation between SVI and carbohydrates or  
292 proteins fractions is observed for SBRs 1, 2 and 5 with sludge of good settleability.  
293 However, for reactors with bulking (SBRs 3, 4 and 6), the carbohydrates fraction of  
294 EPS has a more positively correlation with SVI ( $R^2=0.7850$ ,  $0.7821$  and  $0.9486$  for  
295 SBR3, 4 and 6, respectively), while the proteins fraction is negatively correlated with  
296 SVI ( $R^2=0.7418$ ,  $0.7446$  and  $0.9277$  for SBR3, 4 and 6, respectively).. The  
297 correlations are much stronger for SBR6 with viscous bulking than for other reactors.  
298 This suggests that the observed non-filamentous bulking was possibly caused by the  
299 overproduction of extracellular carbohydrates in the biomass. A similar phenomenon  
300 was found by Jobbagy et al. [15] in which an exponential correlation between the  
301 extracellular carbohydrates contents and SVI values was observed.

302

#### 303 **4. Discussion**

304 Many hypotheses explaining filamentous bulking such as kinetics selection, diffusion  
305 selection and storage selection have been put forward to date [17, 29, 35]. Kinetic  
306 selection theory, formulated by Chudoba et al. [36], assumed that floc-formers and  
307 filaments have different kinetic parameters  $K_S$  (half-saturation constant) and  $\mu_{max}$

308 (maximum growth rate) for the substrate. The floc-formers usually dominate over  
309 filaments at high substrate concentrations, since they have high  $\mu_{\max}$  and  $K_S$  for  
310 soluble substrates. In contrast, the filamentous bacteria would be more favoured at  
311 low substrate concentrations, since filaments are thought to have lower  $K_S$  values.  
312 However, Martins et al. [37] proposed that substrate diffusion limitation inside the  
313 flocs might be a critical cause for filamentous bulking than kinetics selection. They  
314 assumed that floc-formers grow in three dimensions and form the floc matrix, while  
315 filaments grow in only one or two dimensions [38]. Thus, the floc-formers would be  
316 more affected by diffusion resistance of substrates at low substrate concentrations.  
317 The storage selection theory is based on the assumption that floc-formers have higher  
318 substrate uptake rates and capacities to store substrates, while most of the filamentous  
319 microorganisms are supposed to have no or lower ability to store substrates [29].  
320 Therefore, floc-formers are favoured at high substrate concentrations, compared to  
321 filamentous bacteria.

322 Two types of bulking, i.e. filamentous bulking and non-filamentous bulking were  
323 encountered in this study. In SBRs 2 and 5 with N limitation or deficiency,  
324 filamentous bulking did not occur. In comparison, filamentous bulking occurred in  
325 SBR3 and SBR4 with P deficiency. The correlation between SVI and PHA supports  
326 the storage selection hypothesis. In SBRs 2 and 5, part of the substrates were stored as  
327 intracellular PHA in the feast phase. In the famine phase, growth would have occurred  
328 based on the storage product. Such a growth mechanism is known to favour floc-  
329 formers over filaments as most of filamentous bacteria are known to have a lower



330 ability to produce carbon storage products [30, 31], while several types of filaments  
331 (like *Microthrix parvicella* and *Thiothrix nivea*)  
332 have a similar capacity to store substrates [37, 39-41]. In this case, well-settling  
333 sludge was obtained due to the limited proliferation of filaments. Compared to SBRs  
334 1, 2 and 5, PHA formation was not stimulated but attenuated in SBRs 3 and 4.  
335 Without PHA formation giving advantage to floc-formers, filamentous bacteria  
336 probably gained advantage through their competitiveness for nutrients at low  
337 concentrations due to their kinetics advantages. Consequently, filamentous bulking  
338 was caused in these reactors (i.e. SBRs 3 and 4).

339 In comparison to SBRs 2 and 5 with N limitation/deficiency, SBRs 3, 4 and 6  
340 produced more carbohydrates (and less proteins) in EPS as compounds without N or P.  
341 It is unclear, why PHA formation was stimulated by N limitation/deficiency while  
342 carbohydrates formation was stimulated by P limitation/deficiency. The strong  
343 positive correlation between SVI and the carbohydrates fraction in EPS suggests the  
344 excessive production of carbohydrates in EPS is detrimental to sludge settleability.  
345 This supports the observation in [18] that a higher carbohydrates fraction and a lower  
346 proteins fraction in EPS would deteriorate sludge settleability. Different from SBR3  
347 and SBR4, non-filamentous bulking rather than filamentous bulking occurred in  
348 SBR6. With P limitation/deficiency, all these reactors had similar levels of PHA,  
349 carbohydrates and proteins. It is not clear why filamentous bacteria did not develop in  
350 SBR6. This could be related to the relatively short operational time of SBR6 after  
351 bulking occurred (Day 110 – Day 130). Indeed, the SBR6 sludge, prior to bulking,

352 contained filaments at very low levels (FI was lower than 1). Given the high SVI  
353 observed in SBR6 in the absence of filaments, a possible contribution of viscous  
354 bulking to the high SVIs in SBR3 and SBR4 should not be ruled out.

355 The dominant filamentous bacteria under nutrient deficiency were seldom  
356 documented in the previous studies [17]. Through microscopic observation, staining  
357 reactions and FISH analysis, the dominant filaments grew in reactors with filamentous  
358 bulking were identified in this study. In SBRs 3 and 4, the proliferation of two typical  
359 bacteria, *N. limicola*-like and *T. nivea* were identified. These filaments' affinities for  
360 nutrient are critical parameters in the competition for the limited nutrients. It is  
361 assumed that *N. limicola*-like and *T. nivea* have high affinities for nutrients, including  
362 N and P. *N. limicola*-like are usually found in systems where there is low DO or  
363 septicity, and often found in industrial WWTPs with low nutrients [2]. Similarly, *T.*  
364 *nivea* are also often detected in industrial WWTPs [33]. The filaments have a high  
365 affinity for substrate (e.g. acetate) and nutrients, but a relatively low substrate uptake  
366 rate [42].

367 N and P are the basic elements for the growth of microorganisms. The activated  
368 sludge still kept a stable growth phenomenon in the systems fed without N (SBRs 2  
369 and 5 in Phase III). The MLSS concentrations in these reactors were kept around 2000  
370 mg/L, although the growth rate of activated sludge in SBR5 became slower during  
371 Phase III, compared to that during Phases I and II. It is assumed that some unknown  
372 fixation microorganisms might be capable of supplying the entire N requirements of  
373 the system. It is reported that genomic analysis of some polyphosphate accumulating  
374 organisms (PAOs) and glycogen accumulating organisms (GAOs) indicates an ability

375 to fix nitrogen [43, 44], which might be relevant in these nitrogen-limiting systems,  
376 given the FISH analysis suggested the presence of PAOs and GAOs (data not shown).  
377 Although P was not supplied in SBR6 during Phase III, microorganisms in the  
378 reactors might still gain them for their growth, which might be from the sludge decay  
379 products. In addition, it is assumed that P was taken up in excess and stored to be re-  
380 utilized during P limitation or deficiency. It is still not clear what is the mechanism of  
381 the microorganism growth in SBRs 3 and 4 without any phosphorus. It is necessary to  
382 detect N and P levels in the internal of sludge to clarify why the cells still keep  
383 growing under no nutrients feeding.

384 Moreover, from the PHA and EPS data it can be inferred, N limitation or deficiency  
385 increased the intracellular PHA and extracellular proteins levels and was associated  
386 with good settling in SBRs 2 and 5. However, P limitation or deficiency distinctly did  
387 not stimulate the PHA storage, while increased the carbohydrates content of EPS in  
388 SBRs 3, 4 and 6, which was associated with poor settleability. Non-filamentous  
389 bulking occurred when the carbohydrates fraction was distinctly high in the EPS  
390 matrix. It is assumed that the intracellular PHA and the extracellular EPS matrix  
391 would change if encountering nutrient unavailability. The occurrence and/or the type  
392 of bulking in activated sludge could be affected by the combination of kinetic  
393 selection, microbial storage, as well as the EPS composition.

394 This study shows that P limitation seems to stimulate the production of extracellular  
395 carbohydrates rather than intracellular carbohydrates (PHA), which deteriorates  
396 sludge settleability through filamentous or non-filamentous bulking. P limitation  
397 should be avoided in activated sludge systems, especially when treating wastewater  
398 with low levels of P. Considering that the requirement of P for the growth of  
399 microorganisms is relatively lower compared to N, adding P in influent would not

400 distinctly increase operation cost, which can be used in practice. But the dosage  
401 warrants further batch tests.

402

### 403 **Conclusions**

404 This study investigated the long-term effects of nutrients (N and P) limitation or  
405 deficiency on sludge settleability, EPS, substrate storage and microbial community  
406 structure. N limitation or deficiency does not necessarily lead to sludge bulking, likely  
407 attributed to its stimulating effect on the formation of intracellular storage products,  
408 which gives competitive advantages to floc-formers over filamentous bacteria. In  
409 comparison, P deficiency caused sludge bulking. Both filamentous bulking and non-  
410 filamentous bulking could be induced by P limitation/deficiency, with reasons to be  
411 further identified. Filamentous bulking was strongly correlated with the excessive  
412 growth of *N. limicola*-like and *T. nivea*, while non-filamentous bulking is  
413 accompanied by a higher carbohydrates fraction and a lower than proteins fraction of  
414 EPS.

### 415 **Acknowledgement**

416 This work was financially supported by Natural Science Foundation of China  
417 (51208009) and National High Technology Research and Development Program (863  
418 Program) of China (2011AA060903-02). We also acknowledge support from Natural  
419 Science Foundation of Beijing (8132008). Zhiguo Yuan acknowledges the support  
420 from the Beijing City Government through the 'HaiJu' Program.

421

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- 531
- 532

533 **Figure Captions**

534 **Table 1.** Summary of feed conditions in six reactors with different influent nutrient  
535 ratios

536 **Table 2.** The properties of sludge under different nutrient-supplying conditions

537 **Figure 1.** SVI profiles in six SBRs (a: SVIs of the sludge in SBRs 1-4; b: SVIs of the  
538 sludge in SBRs 5-6)

539 **Figure 2.** Microscopic observations of activated sludge in all SBRs at the end of the  
540 study

541 **Figure 3.** Typical FISH, Gram and Neisser staining images of dominant filaments  
542 from various reactors (Bar=20  $\mu\text{m}$ .)

543 **Figure 4.** SVI vs. PHA in all reactors. Higher amounts of PHA accumulated in SBRs  
544 1, 2 and 5 with good settleability, as shown in the right oval; Lower amounts of PHA  
545 accumulated in SBRs 3 and 4 with filamentous bulking, as shown in the left oval;  
546 SBR6 with non-filamentous bulking has a moderate amount of PHA, as shown in the  
547 middle oval.

548 **Figure 5.** Correlation between SVI and EPS, extracellular carbohydrates and proteins  
549 contents of total EPS in the biomass

550



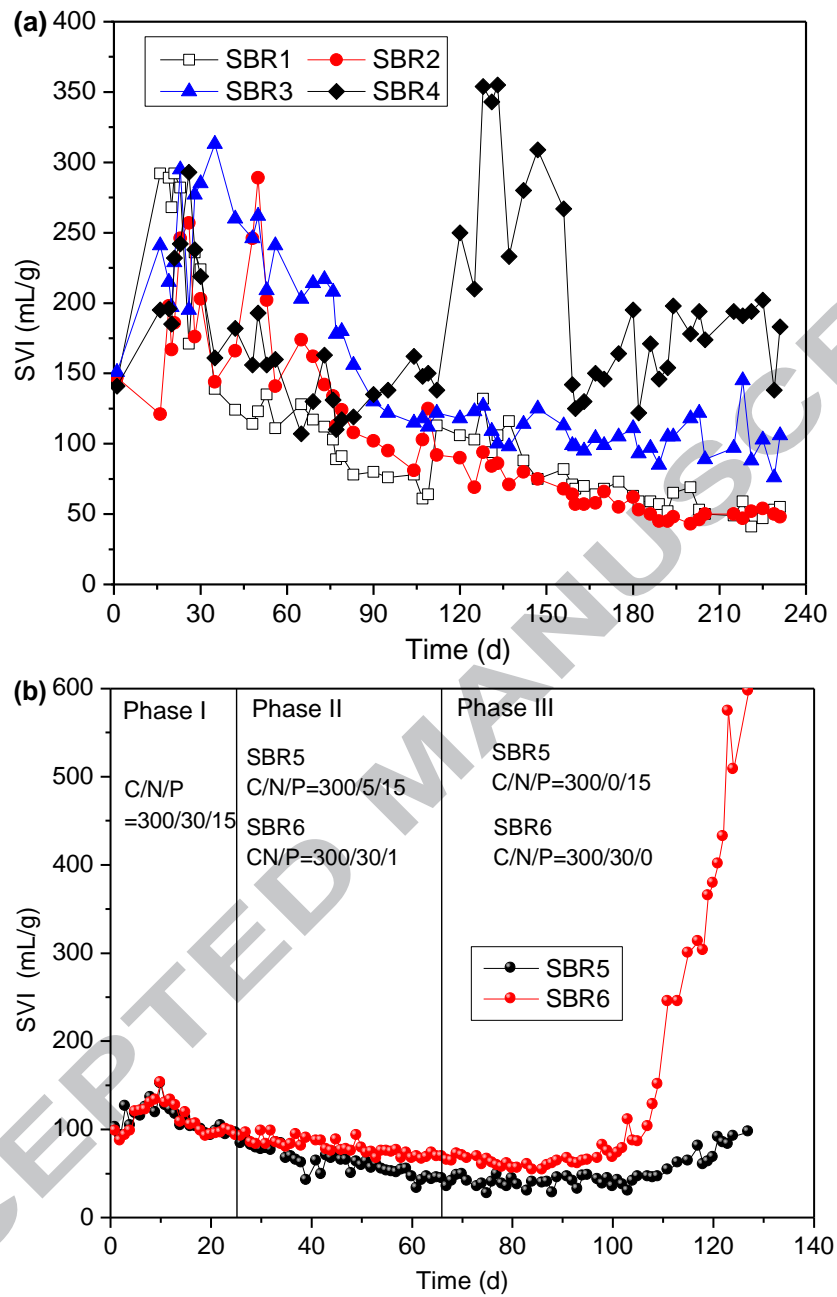
**Table 1.** Summary of feed conditions in six reactors with different influent nutrient ratios

Reactor	Phase	Time (days)	C/N/P (mgCOD:mgN:mgP)	Remarks
1	—	1-233	300/30/10	Control
2	—	1-233	300/0/10	N deficiency
3	—	1-233	300/30/0	P deficiency
4	—	1-233	300/0/0	N&P deficiency
5	I	1-24	300/30/15	Control
	II	25-66	300/5/15	N limitation
	III	67-130	300/0/15	N deficiency
6	I	1-24	300/30/15	Control
	II	25-66	300/30/1	P limitation
	III	67-130	300/30/0	P deficiency

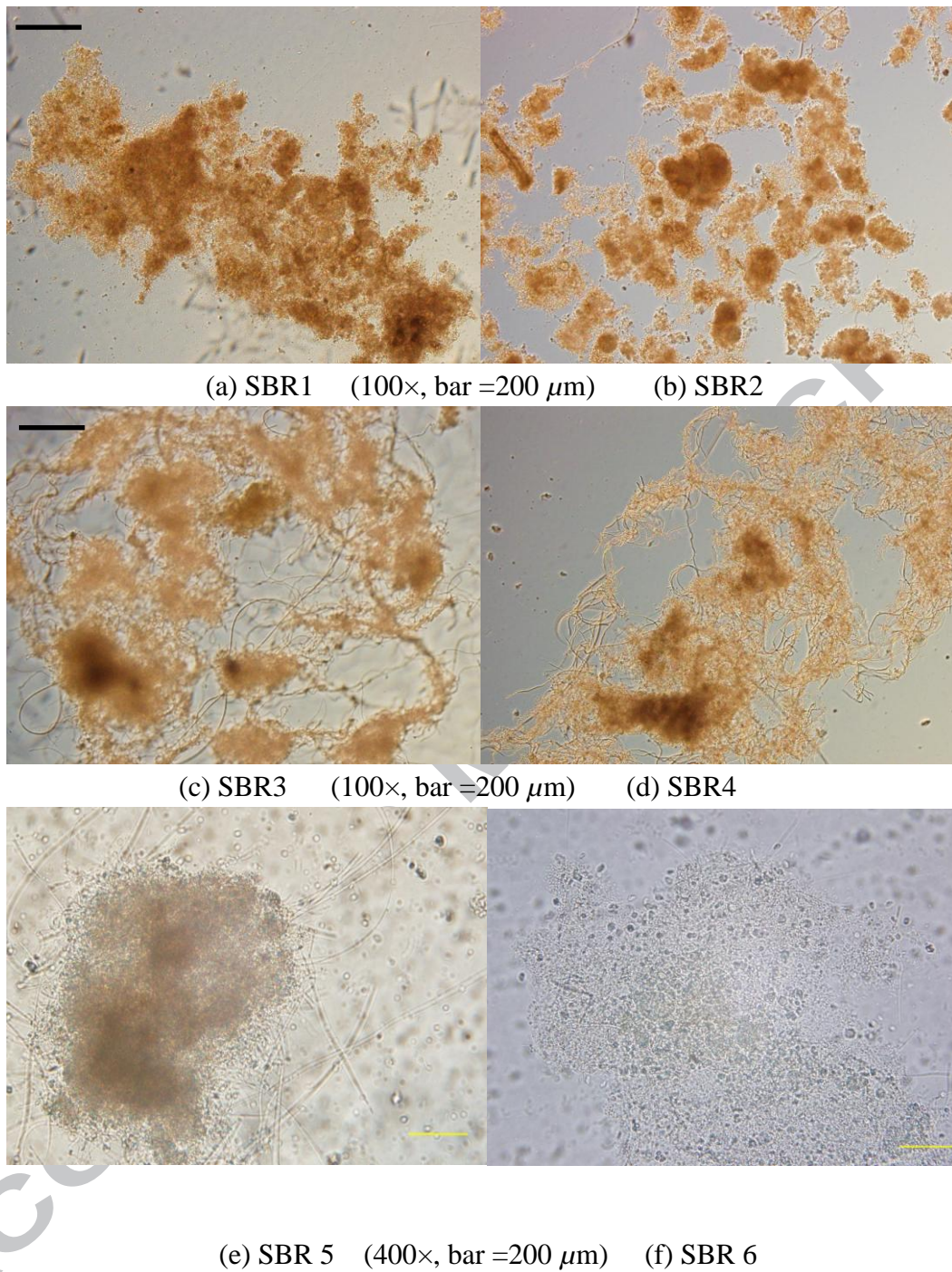
**Table 2.** The properties of sludge under different nutrient-supplying conditions

Reactor	Phase	C/N/P ratio	SVI* (mL/g)	PHA* (mmol C/L)	FI (0-5)	Detected filaments
SBR1	—	300/30/15	108±67	7.2±0.7	0-1	Type 0092, Type 0041
SBR2	—	300/0/10	108±63	13.5±0.1	0-1	Type 0092, Type 0041,
SBR3	—	300/30/0	153±65	4.6±0.5	2-3	<i>N. limicola</i> -like, <i>T. nivea</i>
SBR4	—	300/0/0	186±60	2.5±0.5	3-4	<i>N. limicola</i> -like, <i>T. nivea</i> , Type 0092
SBR5	I	300/30/15	111±15	7.0±0.9	0	No filaments extended from flocs
	II	300/5/15	62±15	14.6±1.3	0-1	Type 021N, Type 0092
	III	300/0/15	49±17	8.9±0.6	1-2	Type 021N, Type 0092
SBR6	I	300/30/15	111±17	6.8±0.5	0	No filaments extended from flocs
	II	300/30/1	80±9	4.6±0.4	0	No filaments extended from flocs
	III	300/30/0	150±150	5.6±0.4	0	No filaments extended from flocs

\*: values showed as mean ± standard deviation (n=58 for SVI calculation; n=8 for PHA calculation)

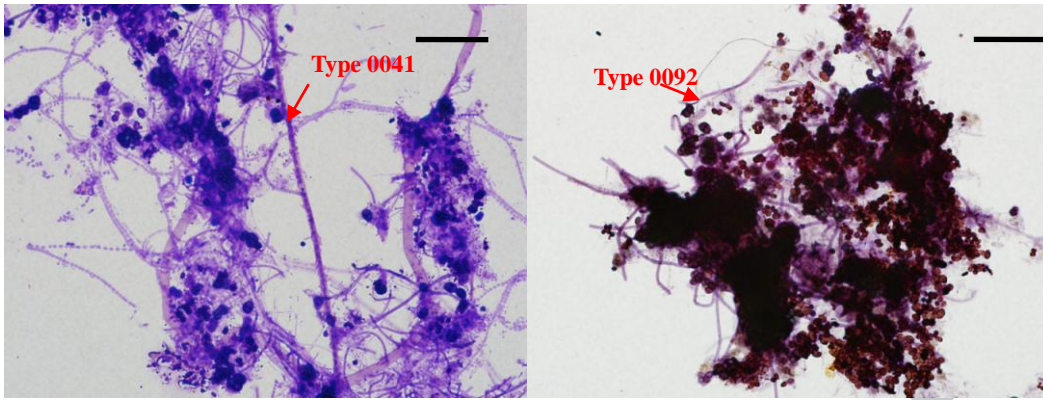


**Figure 1.** SVI profiles in six SBRs (a: SVIs of the sludge in SBRs 1-4; b: SVIs of the sludge in SBRs 5-6)



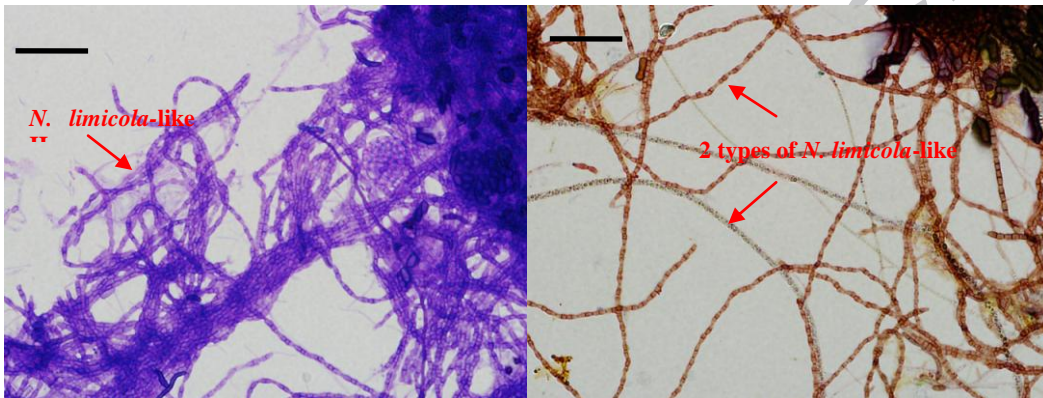
**Figure 2.** Microscopic observations of activated sludge in all SBRs at the end of the study





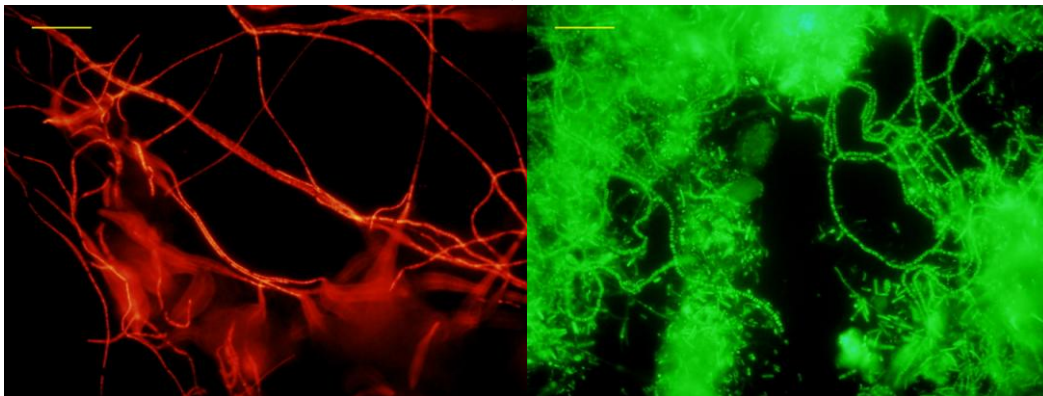
(a) SBR2, Gram staining image

(b) SBR2, Neisser staining image

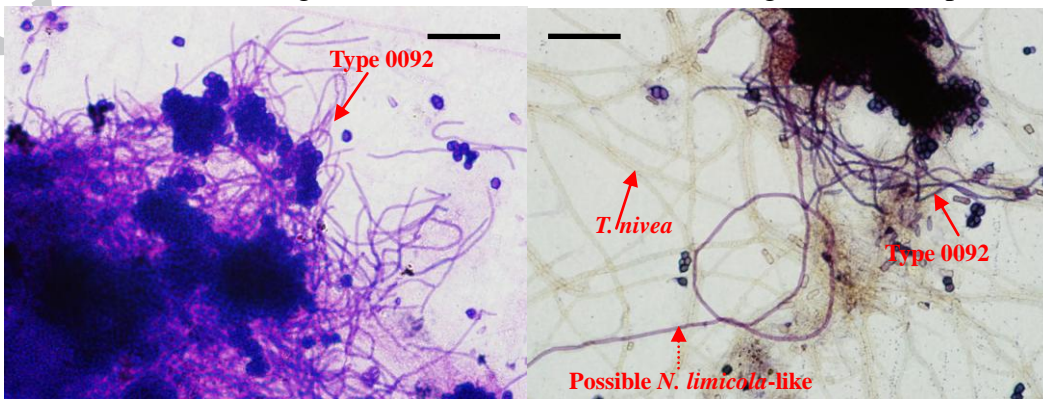


(c) SBR3, Gram staining image

(d) SBR3, Neisser staining image

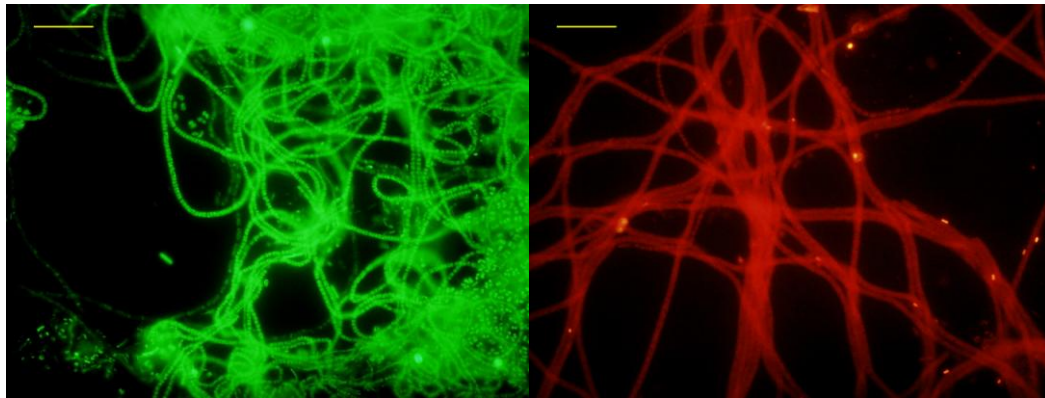
(e) SBR3, FISH image of *T. nivea*

(f) SBR3, FISH image of Eubmix probe



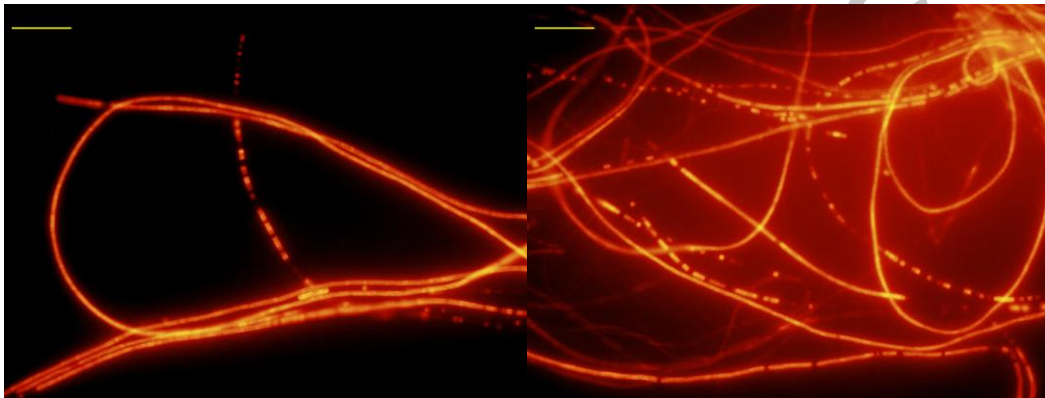
(g) SBR4, Gram staining image

(h) SBR4, Neisser staining image



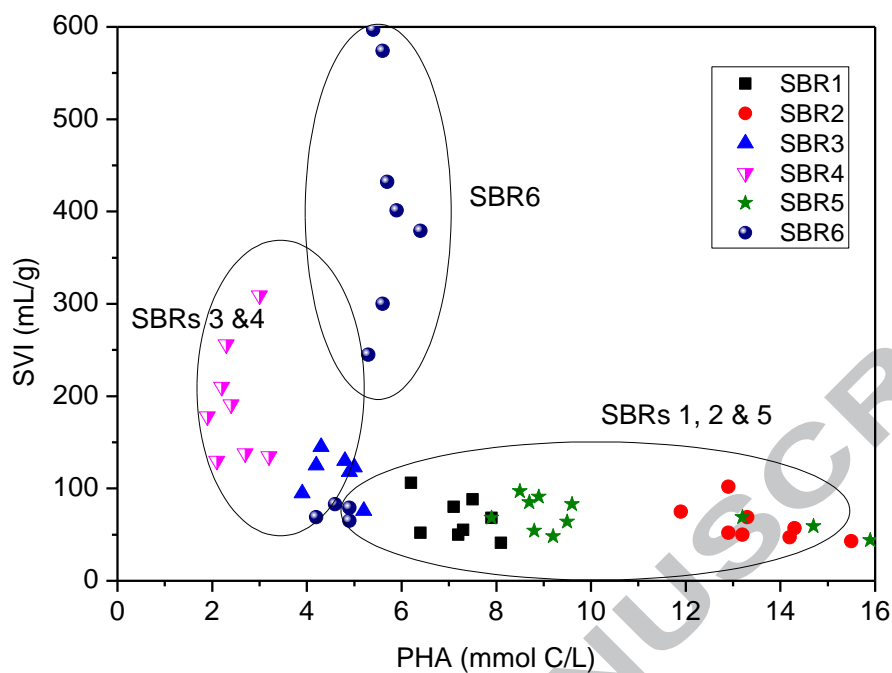
(i) SBR4, FISH image of Eubmix probe

(j) SBR4, FISH image of *T. nivea*

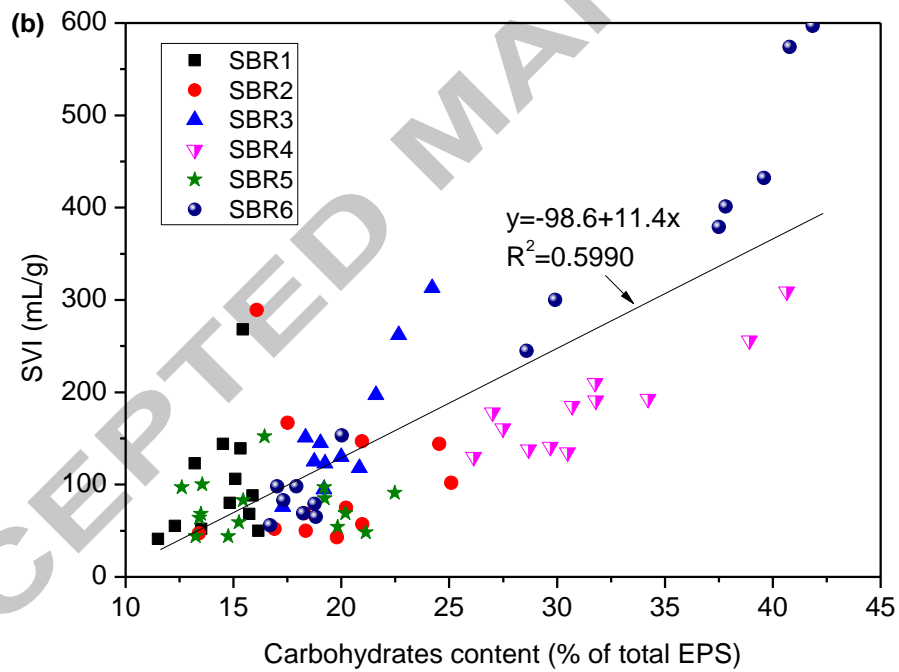
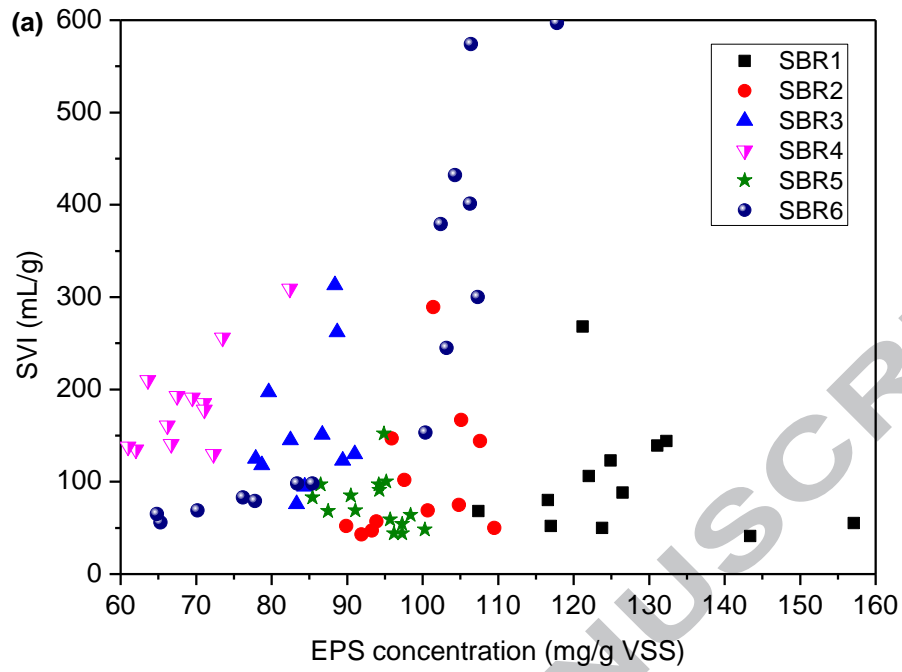


(k) SBR5, FISH image of Type 021N in Phase II (m) SBR5, FISH image of Type 021N in Phase III

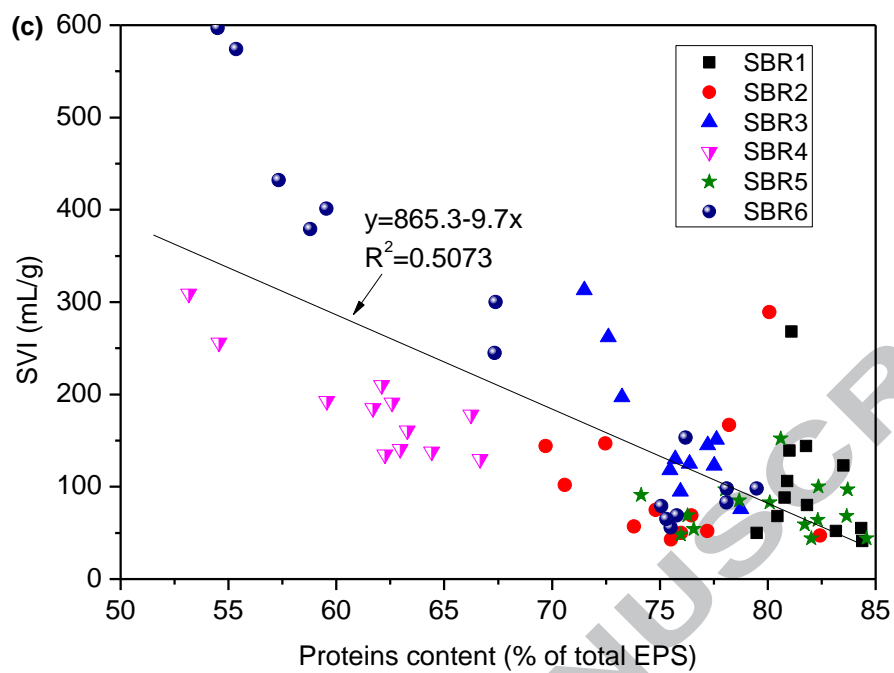
**Figure 3.** Typical FISH, Gram and Neisser staining images of dominant filaments from various reactors (Bar=20  $\mu\text{m}$ .)



**Figure 4.** SVI vs. PHA in all reactors. Higher amounts of PHA accumulated in SBRs 1, 2 and 5 with good settleability, as shown in the right oval; Lower amounts of PHA accumulated in SBRs 3 and 4 with filamentous bulking, as shown in the left oval; SBR6 with non-filamentous bulking has a moderate amount of PHA, as shown in the middle oval.







**Figure 5.** Correlation between SVI and EPS, extracellular carbohydrates and proteins contents of total EPS in the biomass

**Research Highlights**

- ▶ Effects of N/P deficiency on SVI, EPS, PHA and microbial community structure were examined.
- ▶ Bulking was not encountered in reactors with nitrogen limitation or deficiency.
- ▶ Bulking was encountered in those reactors fed with wastewater deficient in phosphorus.
- ▶ N limitation/deficiency stimulates formation of intracellular storage products (PHA).
- ▶ P limitation stimulates formation of carbohydrates.

## Graphical abstract

