

Technical University of Denmark



Control Structure Design for an EBP2R Process Operated as a Sequencing Batch Reactor

Valverde Pérez, Borja; Fuentes-Martínez, José Manuel ; Flores Alsina, Xavier; Wágner, Dorottya Sarolta; Gernaey, Krist V.; Huusom, Jakob Kjøbsted; Plósz, Benedek G.

Publication date:
2015

Document Version
Peer reviewed version

[Link back to DTU Orbit](#)

Citation (APA):

Valverde Perez, B., Fuentes-Martínez, J. M., Flores Alsina, X., Wágner, D. S., Gernaey, K., Huusom, J. K., & Plósz, B. G. (2015). Control Structure Design for an EBP2R Process Operated as a Sequencing Batch Reactor. Poster session presented at 9th IWA Symposium on Systems Analysis and Integrated Assessment (Watermatex 2015), Gold Coast, Queensland, Australia.

DTU Library

Technical Information Center of Denmark

General rights

Copyright and moral rights for the publications made accessible in the public portal are retained by the authors and/or other copyright owners and it is a condition of accessing publications that users recognise and abide by the legal requirements associated with these rights.

- Users may download and print one copy of any publication from the public portal for the purpose of private study or research.
- You may not further distribute the material or use it for any profit-making activity or commercial gain
- You may freely distribute the URL identifying the publication in the public portal

If you believe that this document breaches copyright please contact us providing details, and we will remove access to the work immediately and investigate your claim.

Control Structure Design for an EBP2R Process Operated as a Sequencing Batch Reactor

Borja Valverde-Pérez*, José Manuel Fuentes-Martínez*, Xavier Flores-Alsina**, Dorottya S. Wágner*, Krist V. Gernaey**, Jakob Kjøbsted Huusom** and Benedek Gy. Plósz*

*Department of Environmental Engineering, Technical University of Denmark, Miljøvej, Building 113, 2800 Kgs. Lyngby, DENMARK

**Department of Chemical and Biochemical Engineering, Technical university of Denmark, Søtofts Plads, Building 229, 2800 Kgs. Lyngby DENMARK

1. INTRODUCTION

Current resource recovery strategies [1]:

- Metal salt addition for phosphorus precipitation
- Ultrafiltration

Disadvantages:

- High energy demand
- Requires metal salts

Resource recovery through a two-stages bacterial-algal system [2]:

- Enhanced biological phosphorus removal and recovery system (EBP2R) to produce growth media with targeted N-to-P ratios
- Optimal algal cultivation, thereby intracellularly storing both N and P
- Direct application on land for fertigation

Advantages:

- Complete biological process
- Comparably lower environmental impact



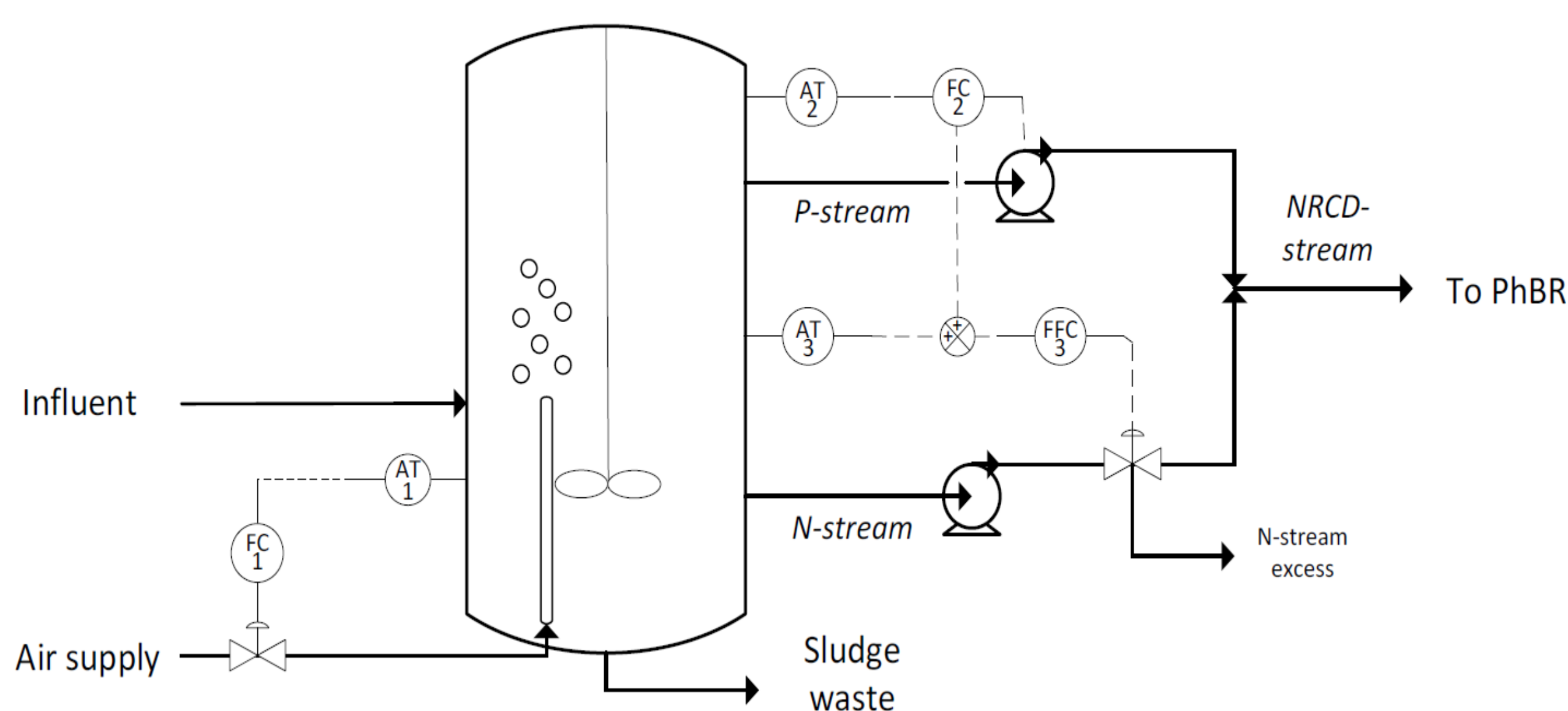
Optimal N-to-P ratio



Fertigation

Objective: How to keep a stable and optimal N-to-P ratio in the feed to the photobioreactor?

2. CONTROL STRUCTURE DESIGN

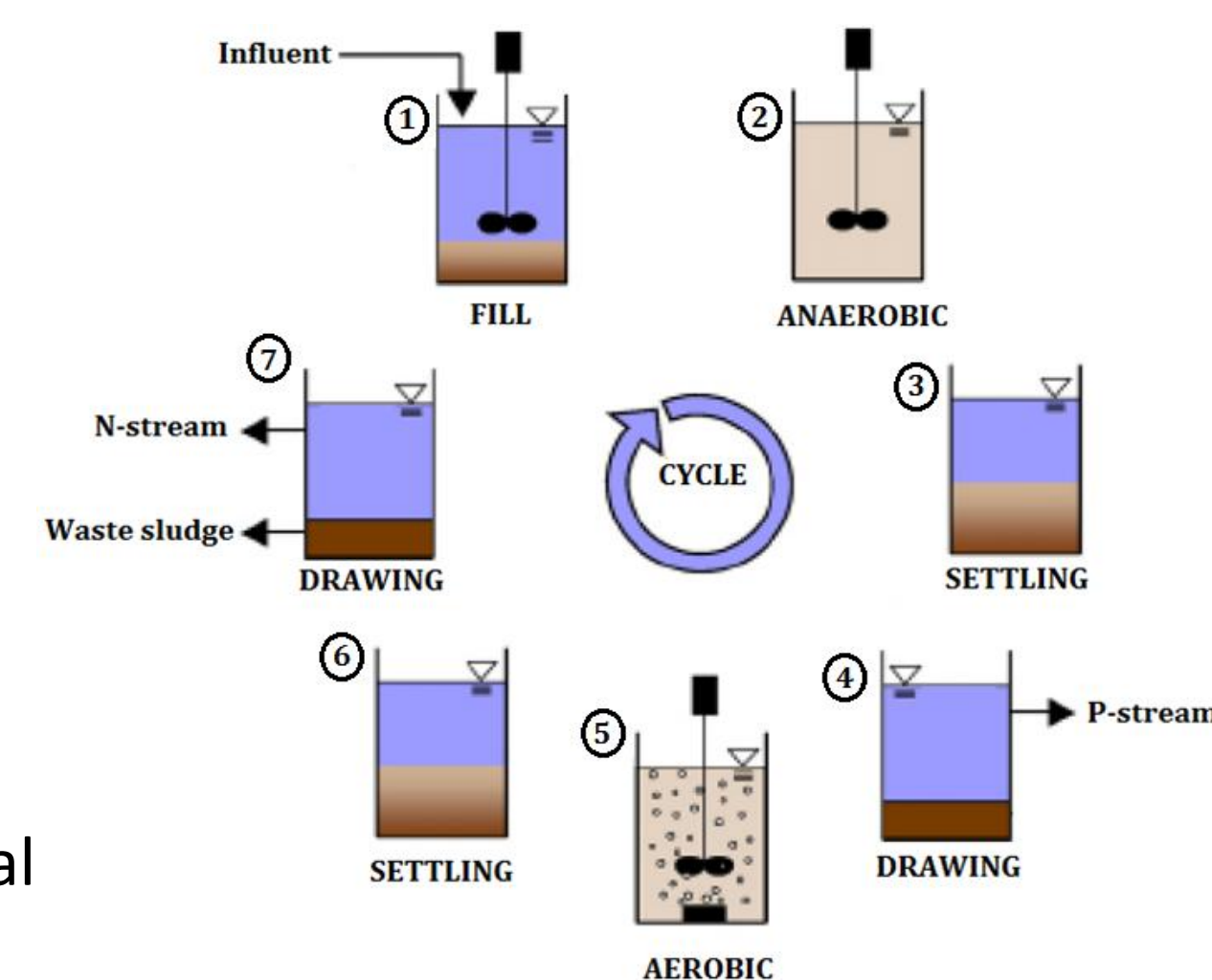


System description:

- 8-L volume sequencing batch reactor (SBR) operated at hydraulic retention time 18 h.
- Model calibrated at solid retention time (SRT) 8 days.

Process optimization:

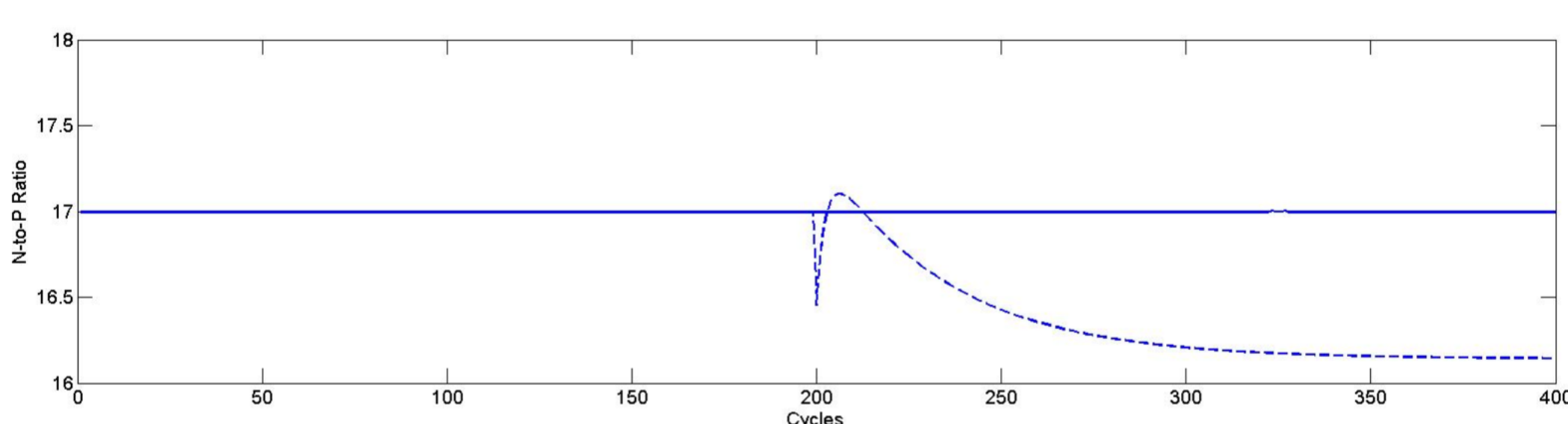
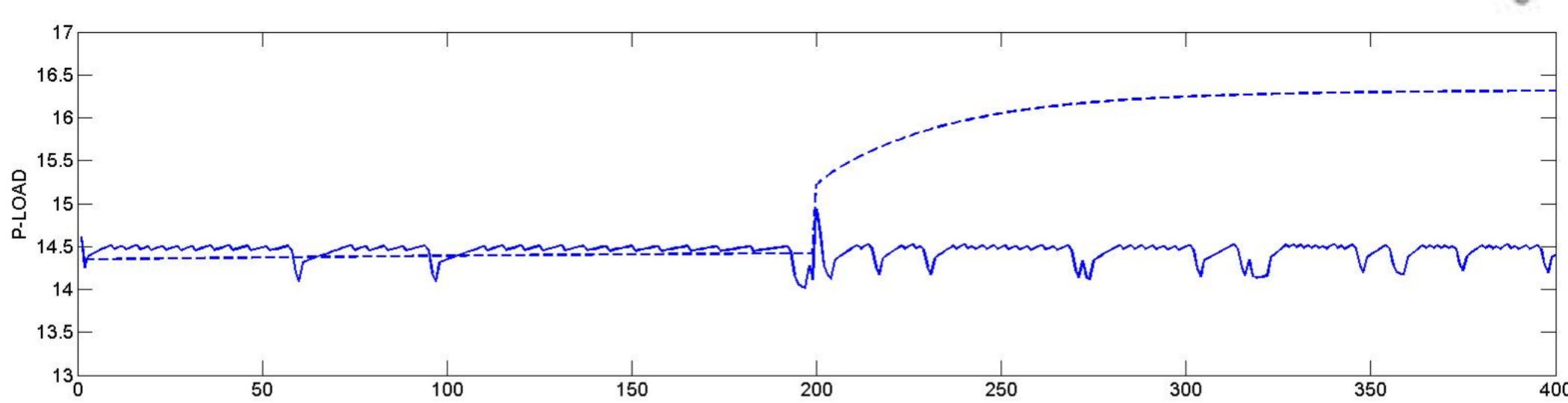
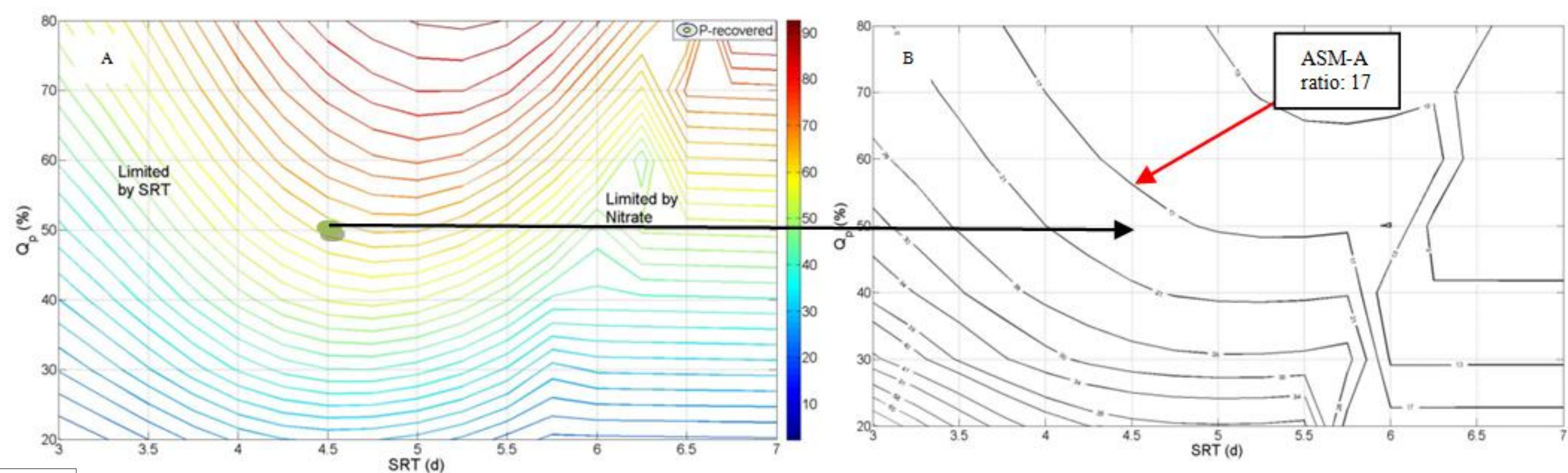
- Optimal P-recovery at SRT of 4.5 days and $Q_p=0.5 \cdot Q_{in}$. At other conditions PAO activity is limited by:
 - SRT
 - Nitrate recirculation to the anaerobic reactors
- The EBP2R is able to yield to N-to-P ratios optimal for cultivation of different green-microalgae:
 - Mixed algal culture used for ASM-A model calibration has an optimal N-to-P=17 [3]
- To accomplish with the nutrient requirement the N-stream has to be partially diverted to a completely autotrophic nitrogen removal (CANR) process.



Control structure:

Pairing of manipulated and controlled variables :

- **Phosphorus control loop:** pump in the P-stream controls the phosphorus load to the photobioreactor (PBR). *Run-to-run control strategy*
- **N-to-P ratio control loop:** valve splits the N-stream flow between the PBR and the CANR system. *Ratio controller operating during the batch*
- **Dissolved oxygen control loop:** air supply (modeled as kLa) controls the oxygen level in the aerobic tank. *Control during the batch*
- **SRT:** ideally controlled by wasting a constant fraction of the total biomass.



Dashed line: open loop simulation; solid line: closed loop simulation

Performance:

System response to step disturbances in the influent:

- **Total phosphorus ($\pm 20\%$):** in open loop the disturbance affects both P recovered and N-to-P ratio; the control system rejects the influent disturbance.
- **Total nitrogen ($\pm 30\%$):** in open loop the disturbance affects only the N-to-P ratio; the control system rejects the influent disturbance.
- **Total COD ($\pm 20\%$):** in open loop the disturbance impact is comparably low; the control system rejects the influent disturbance.

Comparison with continuous layout [4]:

- The SBR leads to higher maximum phosphorus recovery: 80-90% vs 60% recovery in the continuous system
- The SBR is more flexible rejecting disturbances associated to the phosphorus load into the reactor

3. CONCLUSION

- **Control structure** for the EBP2R has been **developed and tested** under step influent disturbances
- **Higher phosphorus recovery** allows **better rejection of disturbances** in the influent phosphorus load compared to the continuous system
- **Future research** should address the **controllability of the PBR** and the **upstream online optimization** according to the PBR performance

ACKNOWLEDGEMENT



The research was financially supported by the Danish Council for Strategic Research, as part of the **Integrated Water Technology** (InWaTech) project, a collaboration between the Technical University of Denmark (DTU) and the Korea Advanced Institute of Science and Technology (KAIST).

References:

[1] Verstraete, W., Van de Caveye, P. and Diamantis, V., 2009. Bioresource Technology, 100, 5537-5545

[2] Valverde-Pérez, B., Ramin, E., Smets, B.F., and Plósz, B. Gy., 2015. Water Research, 68, 821-830

[3] Wágner, D.S., Valverde-Pérez, B., Sæbø, M., Bregua de la Sotilla, M., Van Wageningen, J., Smets, B.F., and Plósz, B.Gy., 2015. In preparation.

[4] Valverde-Pérez, B., Fuentes-Martínez, J.M., Flores-Alsina, X., Gernaey, K.V., Huusom, J.K., and Plósz, B.Gy., 2015. Computer Aided Chemical Engineering, 37, 2555 – 2560