



## **UNIVERSITI PUTRA MALAYSIA**

## CONVECTION BOUNDARY LAYER FLOWS OVER NEEDLES AND CYLINDERS IN VISCOUS FLUIDS

## **SYAKILA BINTI AHMAD**

IPM 2009 4



### CONVECTION BOUNDARY LAYER FLOWS OVER NEEDLES AND CYLINDERS IN VISCOUS FLUIDS

By

### SYAKILA BINTI AHMAD

Thesis Submitted to the School of Graduate Studies, Universiti Putra Malaysia, in Fulfilment of the Requirements for the Degree of Doctor of Philosophy

May 2009



To My Beloved Family and Friends.



Abstract of thesis presented to the Senate of Universiti Putra Malaysia in fulfilment of the requirement for the degree of Doctor of Philosophy

#### CONVECTION BOUNDARY LAYER FLOWS OVER NEEDLES AND CYLINDERS IN VISCOUS FLUIDS

By

SYAKILA BINTI AHMAD

**May 2009** 

Chairman : Norihan Md. Arifin, PhD

Institute : Institute for Mathematical Research

Convection is the heat transfer process which is frequently encountered in environmental and engineering applications. In this study, the problems of steady laminar convection boundary layer flows over needles and cylinders immersed in an incompressible and viscous fluid are theoretically considered. The dimensional partial differential equations governing the boundary layer flows are first transformed into nondimensional equations. These equations are then transformed using non-similar transformation. Then, these transformed nonlinear systems of equations are solved using an implicit finite difference scheme known as the Keller-box method, which has been found to be very suitable in dealing with nonlinear and parabolic equations. The complete numerical method used in this study is programmed in Fortran. Numerical computations are carried out for various values of the dimensionless parameters of the problems, which include the Prandtl number Pr, the ratio of the major and minor axes of the cylinder  $b_c/a_c$ , the mixed convection parameter  $\lambda$ , the modified mixed convection parameter  $\hat{\lambda}$ , the transverse curvature parameter  $\Lambda$ , the parameter *a* representing the needle size and the viscosity/temperature parameter  $\theta_r$ . Numerical results



presented in this study are the skin friction coefficient, the heat transfer coefficient, the local Nusselt number, the cylinder temperature as well as the velocity and temperature profiles. The obtained results show that the flow and the thermal characteristics are significantly influenced by these parameters.



Abstrak tesis yang dikemukakan kepada Senat Universiti Putra Malaysia sebagai memenuhi keperluan untuk ijazah Doktor Falsafah

#### ALIRAN LAPISAN SEMPADAN OLAKAN PADA JARUM DAN SILINDER DALAM BENDALIR LIKAT

Oleh

#### SYAKILA BINTI AHMAD

Mei 2009

### Pengerusi : Norihan Md. Arifin, PhD

Institut : Institut Penyelidikan Matematik

Olakan adalah suatu proses pemindahan haba yang sering berlaku dalam persekitaran dan juga dalam kebanyakan aplikasi kejuruteraan. Dalam kajian ini, masalah aliran lapisan sempadan olakan mantap dan berlamina terhadap jarum dan silinder dalam bendalir likat dan tak termampatkan telah dipertimbangkan secara teori. Persamaan pembezaan separa berdimensi yang menakluk aliran lapisan sempadan terlebih dahulu dijelmakan kepada persamaan tak berdimensi. Seterusnya, persamaan tersebut akan dijelma menggunakan penjelmaan tak serupa. Sistem persamaan terjelma tak linear yang diperoleh diselesaikan secara berangka menggunakan skim beza terhingga tersirat iaitu kaedah kotak Keller yang merupakan satu kaedah yang sangat sesuai untuk menyelesaikan persamaan tak linear dan parabolik. Kaedah berangka yang digunakan dalam kajian ini telah dibangunkan dalam bentuk pengaturcaraan komputer dengan menggunakan Fortran. Pengiraan berangka dilakukan untuk pelbagai nilai parameter tak berdimensi seperti nombor Prandtl Pr, nisbah paksi major dan minor silinder  $b_c/a_c$ , parameter olakan campuran  $\lambda$ , parameter a yang mewakili saiz jarum dan parameter



kelikatan/suhu  $\theta_r$ . Keputusan berangka yang dipersembahkan dalam kajian ini adalah pekali geseran kulit, pekali pemindahan haba, nombor Nusselt setempat, suhu silinder beserta profil halaju dan suhu. Keputusan yang diperoleh menunjukkan bahawa ciri-ciri aliran dan terma adalah sangat dipengaruhi oleh parameter-parameter yang dipertimbangkan di atas.



#### ACKNOWLEDGEMENTS

Bismillahirrahmanirrahim. Alhamdulillah. In the Name of Allah, the most Beneficient and the most Merciful, I would like to express my great appreciation for the guidance and assistance received throughout the journey of this thesis writing.

My deepest thanks to my respected supervisor and co-supervisors; Assoc. Prof. Dr. Norihan Md. Arifin, Assoc. Prof. Dr. Roslinda Mohd Nazar and Dr. Abdul Aziz Jaafar for their valuable guidance, knowledge, times and support, and also for making this thesis possible. I would also like to extend my appreciation to Prof. Ioan Pop from University of Cluj, Romania, for his motivation and support.

Many thanks to the Institute for Mathematical Research, Universiti Putra Malaysia (UPM) for giving me the opportunity to do my research here and also for providing me with a very good research environment and equipments. My special thanks to the staffs from the institute who have been very supportive and very helpful during my course of study here. Also thanks to all the staffs in UPM who have involved directly or indirectly during my studies and also during the preparation of this thesis. I would also like to express my sincere thanks to Universiti Sains Malaysia (USM) and Ministry of Higher Education Malaysia for the financial support throughout the course of my study.

I would like to thank all my friends and research colleagues who kindly provided valuable and helpful comments in the preparation of this thesis. Finally, thank you very much to the most important person in my life, my parent and members of the family for their unconditional love and support especially during the hard times. May Allah bless you all.



I certify that a Thesis Examination Committee has met on 27 May 2009 to conduct the final examination of Syakila binti Ahmad on her thesis entitled "Convection Boundary Layer Flows Over Needles and Cylinders in Viscous Fluids" in accordance with the Universities and University Colleges Act 1971 and the Constitution of the Universiti Putra Malaysia [P.U.(A) 106] 15 March 1998. The Committee recommends that the student be awarded the Doctor of Philosophy.

Members of the Thesis Examination Committee were as follows:

#### Noor Akma Ibrahim, PhD

Associate Professor Institute for Mathematical Research Universiti Putra Malaysia (Chairman)

#### Malik Abu Hassan, PhD

Professor Institute for Mathematical Research Universiti Putra Malaysia (Internal Examiner)

#### Mohd Noor Saad, PhD

Lecturer Institute for Mathematical Research Universiti Putra Malaysia (Internal Examiner)

#### **Bachok Taib, PhD**

Professor Center for Graduate Studies Universiti Sains Islam Malaysia Malaysia (External Examiner)

**BUJANG KIM HUAT, PhD** Professor and Deputy Dean School of Graduate Studies Universiti Putra Malaysia

Date: 13 July 2009



This thesis was submitted to the Senate of Universiti Putra Malaysia and has been accepted as fulfilment of the requirement for the degree of Doctor of Philosophy. The members of the Supervisory Committee were as follows:

### Norihan Md. Arifin, PhD

Associate Professor Institute for Mathematical Research Universiti Putra Malaysia (Chairman)

### Abdul Aziz Jaafar, PhD

Lecturer Institute for Mathematical Research Universiti Putra Malaysia (Member)

### Roslinda Mohd Nazar, PhD

Associate Professor Institute for Mathematical Research Universiti Putra Malaysia (Member)

### HASANAH MOHD. GHAZALI, PhD

Professor and Dean School of Graduate Studies Universiti Putra Malaysia

Date: 17 July 2009



#### DECLARATION

I hereby declare that the thesis is based on my original work except for quotations and citations, which have been duly acknowledged. I also declare that it has not been previously or concurrently submitted for any other degree at UPM or other institutions.

SYAKILA BINTI AHMAD Date: 10 July 2009



## TABLE OF CONTENTS

DEDICATION	ii
ABSTRACT	111
ABSTRAK	V
ACKNOWLEDGEMENTS	vii
APPROVAL	viii
DECLARATION	Х
LIST OF TABLES	xiv
LIST OF FIGURES	XV
LIST OF ABBREVIATIONS	xxii

### CHAPTER

1	INTE	RODUCT	ION	1
	1.1	Forced	, Free and Mixed Convection	1
	1.2	Viscou	s Fluid	2
	1.3	Bound	ary Layer Theory	3
	1.4	The Ef	fects of Prandtl Number on Boundary Layer	5
	1.5	Object	ives and Scope	7
	1.6	Literat	ure Review	8
		1.6.1	Free Convection over Cylinders of Elliptic Cross	
			Section	9
		1.6.2	Forced and Mixed Convection over Thin Needles	10
		1.6.3	Mixed Convection over Slender Cylinder	11
		1.6.4	Mixed Convection over Horizontal Circular Cylinder	12
		1.6.5	The Keller-box Method	13
	1.7	Goverr	ning Equations	14
		1.7.1	The Dimensional Equations, Boundary Layer and	
			Boussinesq Approximations	15
		1.7.2	The Non-dimensional Equations	23
		1.7.3	Non-similar Transformation	24
	1.8	Thesis	Outline	25
2	THE	KELLE	R-BOX METHOD	27
	2.1	Introdu	iction	27
	2.2	The Fir	nite Difference Method	28



	2.3	Newto	on Method	33
	2.4	Block	Elimination Method	37
	2.5	Initial	Conditions	46
3	FREI	E CONVE	ECTION BOUNDARY LAYER FLOW	
	OVE	R CYLIN	DERS OF ELLIPTIC CROSS SECTION	51
	3.1	Introdu	uction	51
	3.2	Consta	ant Surface Heat Flux	52
		3.2	Mathematical Formulation	52
		3.3	Solution Procedure	53
		3.4	Results and Discussion	55
	3.2	Tempe	erature-dependent Viscosity	67
		3.2	Mathematical Formulation	67
		3.3	Solution Procedure	70
		3.4	Results and Discussion	71
	3.5	Conclu	usions	83
4	FOR	CED CON	NVECTION BOUNDARY LAYER FLOW	
	OVE	R A MOV	ING THIN NEEDLE	85
	4.1	Introdu	uction	85
	4.2	Mathe	matical Formulation	87
	4.3	Solutio	on Procedure	89
	4.4	Result	s and Discussion	91
	4.5	Conclu	usions	98
5	MIXI	ED CONV	VECTION BOUNDARY LAYER FLOW	
	ALO	NG VERT	FICAL THIN NEEDLES	100
	5.1	Introdu	uction	100
	5.2	Mathe	matical Formulation	101
	5.3	Solutio	on Procedure	103
	5.4	Result	s and Discussion	105
	5.5	Conclu	usions	111
6	MIXI	ED CONV	VECTION BOUNDARY LAYER FLOW	
-	ALO	NG VER	FICAL MOVING THIN NEEDLES	112
	6.1	Introdu	uction	112
	6.2	Variab	le Wall Temperature	114
		6.2.1	Mathematical Formulation	114
		6.2.2	Solution Procedure	116
		6.2.3	Results and Discussion	117
		0.2.0	<b></b>	± ± /



	6.3	Variab	le Surface Heat Flux	124
		6.3.1	Mathematical Formulation	124
		6.3.2	Solution Procedure	126
		6.3.3	Results and Discussion	127
	6.4	Conclu	isions	134
7	MIXI	ED CONV	<b>VECTION BOUNDARY LAYER FLOW</b>	
	ALO	NG A VE	RTICAL MOVING SLENDER CYLINDER	136
	7.1	Introdu	action	136
	7.2	Mathe	matical Formulation	137
	7.3	Solutio	on Procedure	140
	7.4	Result	s and Discussion	143
	7.5	Conclu	isions	149
8	MIXI	ED CONV	ECTION BOUNDARY LAYER FLOW	
	PAST	' AN ISO'	THERMAL HORIZONTAL CIRCULAR	
	CYLI	NDER W	ITH TEMPERATURE-DEPENDENT	
	VISC	OSITY		151
	8.1	Introdu	action	151
	8.2	Mathe	matical Formulation	153
	8.3	Solutio	on Procedure	157
	8.4	Result	s and Discussion	159
	8.5	Conclu	isions	166
9	CON	CLUSION	NS	168
	9.1	Summ	ary of Research	168
	9.2	Furthe	r Research	171
REI	FERENC	ES		173

REFERENCES	173
APPENDICES	187
BIODATA OF STUDENT	208



## LIST OF TABLES

Table		Page
3.1	Values of the cylinder temperature $\theta_w$ for $Pr = 1$ with blunt orientation ( $b_c/a_c = 0.1$ and 0.25) compared to Merkin (1977a)	57
3.2	Values of the cylinder temperature $\theta_w$ for $Pr = 1$ with blunt orientation ( $b_c/a_c = 0.5$ and 0.75) compared to Merkin (1977a)	58
3.3	Values of the cylinder temperature $\theta_w$ for $Pr = 1$ with slender orientation ( $b_c/a_c = 1$ and 0.75) compared to Merkin (1977a)	59
3.4	Values of the cylinder temperature $\theta_w$ for $Pr = 1$ with slender orientation ( $b_c/a_c = 0.5$ and 0.25) compared to Merkin (1977a)	60
3.5	Values of the heat transfer $q_w$ for $\Pr = 1$ with blunt orientation ( $b_c/a_c = 0.1$ and 0.25) when $\theta_r \to -\infty$	73
3.6	Values of the heat transfer $q_w$ for $\Pr = 1$ with blunt orientation ( $b_c/a_c = 0.5$ and 0.75) when $\theta_r \to -\infty$	74
3.7	Values of the heat transfer $q_w$ for $\Pr = 1$ with slender orientation ( $b_c/a_c = 1$ and 0.75) when $\theta_r \to -\infty$	75
3.8	Values of the heat transfer $q_w$ for $\Pr = 1$ with slender orientation ( $b_c/a_c = 0.5$ and 0.25) when $\theta_r \to -\infty$	76
4.1	Skin friction coefficient $C_f \operatorname{Re}^{1/2}$ over thin needles for $m = 0$	93
4.2	Values of $\theta'(a)$ over thin needles for $m = 0$ and $a = 0.1$	93



## LIST OF FIGURES

Figure		Page
1.1	The velocity and thermal boundary layers	4
1.2	The effect of Prandtl number Pr on velocity and thermal boundary layers thicknesses	6
1.3	The types of fluid for various values of Prandtl number $\Pr$	7
1.4	Physical model and coordinate system for free convection over a cylinder of elliptic cross section	18
2.1	Net rectangle for difference approximations	29
2.2	Flow diagram for the Keller-box method	50
3.1	Physical model and coordinate system for free convection over a cylinder of elliptic cross section with constant surface heat flux	53
3.2	The local skin friction coefficient $C_f$ for various Pr with blunt orientation ( $b_c/a_c = 0.1$ )	61
3.3	The cylinder temperature $\theta_w$ for various Pr with blunt orientation ( $b_c/a_c = 0.1$ )	61
3.4	The local skin friction $C_f$ coefficient for various Pr with slender orientation ( $b_c/a_c = 0.75$ )	62
3.5	The cylinder temperature $\theta_w$ for various Pr with slender orientation ( $b_c/a_c = 0.75$ )	62
3.6	The local skin friction coefficient $C_f$ for $Pr = 0.7$ and 6.8 with blunt orientation (various $b_c/a_c$ )	64



3.7	The cylinder temperature $\theta_w$ for $Pr = 0.7$ and 6.8 with blunt orientation (various $b_c/a_c$ )	64
3.8	The local skin friction coefficient $C_f$ for $Pr = 0.7$ and 6.8 with slender orientation (various $b_c/a_c$ )	65
3.9	The cylinder temperature $\theta_w$ for $Pr = 0.7$ and 6.8 with slender orientation (various $b_c/a_c$ )	65
3.10	Velocity profiles $f'$ at lower stagnation point of the cylinder, $x = 0$ for various Pr with $b_c/a_c = 0.1$ (blunt orientation)	66
3.11	Temperature profiles $\theta$ at lower stagnation point of the cylinder, $x = 0$ for various Pr with $b_c/a_c = 0.1$ (blunt orientation)	67
3.12	Physical model and coordinate system for free convection over a cylinder of elliptic cross section with temperature- dependent viscosity	68
3.13	Heat transfer $q_w$ for $\Pr = 1$ (blunt: $b_c/a_c = 0.1$ )	77
3.14	Heat transfer $q_w$ for $Pr = 1$ (blunt: $b_c/a_c = 0.25$ )	78
3.15	Heat transfer $q_w$ for $Pr = 1$ (blunt: $b_c/a_c = 0.5$ )	78
3.16	Heat transfer $q_w$ for $Pr = 1$ (blunt: $b_c/a_c = 0.75$ )	79
3.17	Heat transfer $q_w$ for $Pr = 6.8$ (slender: $b_c/a_c = 1.0$ )	79
3.18	Heat transfer $q_w$ for $Pr = 6.8$ (slender: $b_c/a_c = 0.75$ )	80
3.19	Heat transfer $q_w$ for $Pr = 6.8$ (slender: $b_c/a_c = 0.5$ )	80
3.20	Heat transfer $q_w$ for $Pr = 6.8$ (slender: $b_c/a_c = 0.25$ )	81
3.21	Temperature profiles $\theta$ at $\zeta \approx 0$ for blunt orientation with $b_c/a_c = 0.1$ for $Pr = 1$ and 6.8	82



3.22	Temperature profiles $\theta$ at $\zeta \approx 0$ for slender orientation with $b_c/a_c = 0.25$ for Pr = 1 and 6.8	82
4.1	Physical model and coordinate system for forced convection over a moving thin needle	88
4.2	Variation of the skin friction coefficient $C_f \operatorname{Re}^{1/2}$ with $a$ when $m = 0$	94
4.3	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $a$ for various values of $\Pr$ when $m = 0$	95
4.4	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\Pr$ for various values of $a$ when $m = 0$	96
4.5	Velocity profiles $f'$ for various values of $a$ when $m = 0$	97
4.6	Temperature profiles $\theta$ for various values of $a$ when $Pr = 0.7$ (air) and $m = 0$	97
4.7	Temperature profiles $\theta$ for various values of $\Pr$ when $m = 0$ and $a = 0.01$	98
5.1	Physical model and coordinate system for mixed convection along a vertical thin needle	102
5.2	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 0$ (paraboloid)	106
5.3	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 0$ (paraboloid)	107
5.4	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 1$ (cylinder)	108
5.5	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\lambda$ for various values of a when $\Pr = 0.7$ and $m = 1$ (cylinder)	108



5.6	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = -1$ (cone)	109
5.7	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = -1$ (cone)	109
5.8	Velocity profiles $f'$ for various values of $a$ with $Pr = 0.7$ , $m = 1$ and $\lambda = -3$	110
5.9	Temperature profiles $\theta$ for various values of $a$ with $Pr = 0.7$ , $m = 1$ and $\lambda = -3$	110
6.1	Physical model and coordinate system for mixed convection along a vertical moving thin needle with variable wall temperature	115
6.2	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 0$	118
6.3	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 0$	119
6.4	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = 2.5$ (assisting flow)	120
6.5	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = 2.5$ (assisting flow)	120
6.6	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = -2.5$ (opposing flow)	121
6.7	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = -2.5$ (opposing flow)	122
6.8	Velocity profiles $f'$ for various values of $a$ with $Pr = 0.7$ , $m = 0$ and $\lambda = 5$ (assisting flow)	123
6.9	Temperature profiles $\theta$ for various values of $a$ with $Pr = 0.7$ , $m = 0$ and $\lambda = 5$ (assisting flow)	123



6.10	Physical model and coordinate system for mixed convection along a vertical moving thin needle with variable surface heat flux	125
6.11	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 0$	128
6.12	Variation of the reduced surface temperature $\theta(a)$ with $\lambda$ for various values of $a$ when $\Pr = 0.7$ and $m = 0$	129
6.13	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = 3$ (assisting flow)	130
6.14	Variation of the reduced surface temperature $\theta(a)$ with Pr for various values of $a$ when $m = 0$ and $\lambda = 3$ (assisting flow)	130
6.15	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = -3$ (opposing flow)	132
6.16	Variation of the reduced surface temperature $\theta(a)$ with $\Pr$ for various values of $a$ when $m = 0$ and $\lambda = -3$ (opposing flow)	132
6.17	Velocity profiles $f'$ for various values of $a$ with $Pr = 0.7$ , $m = 0$ and $\lambda = 5$ (assisting flow)	133
6.18	Temperature profiles $\theta$ for various values of $a$ with $Pr = 0.7$ , $m = 0$ and $\lambda = 5$ (assisting flow)	134
7.1	Physical model and coordinate system for mixed convection along a moving vertical slender cylinder	138
7.2	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\Lambda$ for the case of assisting flow with various values of $\operatorname{Pr}$ and $\hat{\lambda}$	144
7.3	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\Lambda$ for the case of assisting flow with various values of $\Pr$ and $\hat{\lambda}$	144
7.4	Variation of the skin friction coefficient $C_f \operatorname{Re}_x^{1/2}$ with $\Lambda$ for the case of opposing flow with various values of $\Pr$ and $\hat{\lambda}$	145



7.5	Variation of the local Nusselt number $Nu_x \operatorname{Re}_x^{-1/2}$ with $\Lambda$ for the case of opposing flow with various values of $\operatorname{Pr}$ and $\hat{\lambda}$	146
7.6	The effect of transverse curvature $\Lambda$ on velocity profiles $f'$ for the case of assisting flow with $\hat{\lambda} = 1$ and $\Pr = 0.7$	147
7.7	The effect of transverse curvature $\Lambda$ on temperature profiles $\theta$ for the case of assisting flow with $\hat{\lambda} = 1$ and $\Pr = 0.7$	147
7.8	The effect of modified mixed convection parameter $\hat{\lambda}$ on velocity profiles $f'$ for the case of assisting flow with $\Lambda = 3.21$ and $Pr = 0.7, 6.8, 10$	148
7.9	The effect of modified mixed convection parameter $\hat{\lambda}$ on temperature profiles $\theta$ for the case of assisting flow with $\Lambda = 3.21$ and $Pr = 0.7, 6.8, 10$	149
8.1	Physical model and coordinate system for mixed convection past a horizontal circular cylinder	155
8.2	The skin friction coefficient $C_f$ for various values of $\lambda$ when $Pr = 1$ (case of constant viscosity)	160
8.3	The Nusselt number $Nu$ for various values of $\lambda$ when $Pr = 1$ (case of constant viscosity)	161
8.4	The skin friction coefficient $C_f$ for various values of $\theta_r$ when $Pr = 0.7$ and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	162
8.5	The Nusselt number $Nu$ for various values of $\theta_r$ when Pr = 0.7 and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	163
8.6	The skin friction coefficient $C_f$ for various values of $\theta_r$ when $\Pr = 7$ and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	163
8.7	The Nusselt number $Nu$ for various values of $\theta_r$ when $\Pr = 7$ and $\lambda = 0.5$ (assisting flow), $\lambda = -1.0$ (opposing flow)	164



- 8.8 Variation of the separation point  $x_s$  with  $\lambda$  for Pr = 0.7 when 165  $|\theta_r| = 2, 4$  and  $|\theta_r| \to \infty$  (constant viscosity)
- 8.9 Variation of the separation point  $x_s$  with  $\lambda$  for Pr = 7 when 165  $|\theta_r| = 2, 4$  and  $|\theta_r| \to \infty$  (constant viscosity)
- 8.10 Variation of the separation point  $x_s$  with  $\lambda$  for  $\Pr = 1$  when 166  $|\theta_r| \to \infty$  (constant viscosity)



## LIST OF ABBREVIATIONS

a	dimensionless needle size
$a_c$	length of semi-major axis for a cylinder of elliptic cross section
$a_{cc}$	radius of the circular cylinder
$b_c$	length of semi-minor axis for a cylinder of elliptic cross section
$C_f$	skin friction coefficient
f	non-dimensional stream function
g	acceleration due to gravity
$\operatorname{Gr}$	Grashof number
k	thermal conductivity of the fluid
m	power index
Nu	Nusselt number
$Nu_x$	local Nusselt number
Pr	Prandtl number
$q_w$	heat flux from the cylinder
R(x)	non-dimensional needle radius
Re	Reynolds number
$\operatorname{Re}_x$	local Reynolds number
T	non-dimensional fluid temperature
$T_r$	reference temperature
$T_w$	needle or cylinder temperature
$T_{\infty}$	ambient temperature
u, v	non-dimensional velocity components along the $x-$ and
	y- directions, respectively, for a cylinder of elliptic cross
	section and a circular cylinder



non-dimensional velocity components along the $x-$ and		
r- directions, respectively, for a thin needle and		
a slender cylinder		
non-dimensional velocity outside boundary layer		
free stream velocity		
non-dimensional Cartesian coordinates along the surface		
of the cylinder and normal to it, respectively, for a cylinder		
of elliptic cross section and a circular cylinder		
non-dimensional axial and radial coordinates, respectively,		
for a thin needle and a slender cylinder		
boundary layer separation point		

## Greek symbols

$\alpha$	thermal diffusivity
$\beta$	thermal expansion coefficient
$\delta_h$	velocity boundary layer thickness
$\delta_T$	thermal boundary layer thickness
$\Delta T$	characteristic temperature
$\eta$	similarity variable
$\gamma$	thermal property of the fluid
$\theta$	non-dimensional temperature
$\theta_r$	viscosity/temperature parameter
$\lambda$	mixed convection parameter
$\hat{\lambda}$	modified mixed convection parameter
Λ	transverse curvature parameter
ν	kinematic viscosity
$ u_{\infty}$	constant kinematic viscosity of the ambient fluid



$\mu$	dynamic viscosity
$\mu_{\infty}$	constant dynamic viscosity of the ambient fluid
ξ	non-dimensional coordinate
ρ	fluid density
$ au_w$	wall shear stress
$\psi$	stream function
$\zeta$	eccentric angle of a cylinder of elliptic cross section

### Subscripts

С	refers to a cylinder of elliptic cross section
CC	refers to a circular cylinder
w	condition at the surface of the cylinder
$\infty$	ambient/free stream condition

# Superscripts

' differentiation	with	respect to	<b>)</b>
-------------------	------	------------	----------

- dimensional variables

