

4<sup>th</sup> Biannual Post Graduate Conference  
18<sup>th</sup>-20<sup>th</sup> November 2015, Seri Iskandar, Perak

# Simulation and Development of Performance Correlations of 3-D Turning Diffuser via ACFD

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**Abstract**— This paper aims to intensively simulate the performances of 3-D turning diffuser by varying geometrical and operating parameters and to develop the performance correlation by means of Asymptotic Computational Fluid Dynamic (ACFD) technique. The performances of turning diffusers were measured primarily by outlet pressure recovery coefficient,  $C_p$  and flow uniformity index,  $\sigma_{out}$ . The geometrical and operating parameters namely inflow Reynolds number ( $Re_{in} = 5.786 \times 10^4 - 1.775 \times 10^5$ ), inlet throat width ratio ( $L_{in}/W_1 = 1.5 - 25.0$ ) and outlet-inlet configurations ( $W_2/W_1 = 1.067 - 2.667$  and  $X_2/X_1 = 1.118 - 2.778$ ) were varied. The performance correlations as a function of geometrical and operating parameters, i.e.  $C_p = f(L_{in}/W_1, W_2/W_1, X_2/X_1, Re_{in})$  and  $\sigma_{out} = f(L_{in}/W_1, W_2/W_1, X_2/X_1, Re_{in})$  are successfully developed via ACFD with deviation to the experiment approximately of 7%.

**Keywords**— ACFD; CFD; turning diffuser

## I. INTRODUCTION

Study of the geometry effect on diffuser performance has been of fundamental interest to researchers in the area of fluid mechanics since decades and it continues to grow [1-8]. The performance of diffuser is primarily evaluated by means of:

- (i) Outlet pressure recovery coefficient ( $C_p$ )

$$C_p = \frac{2(P_{out} - P_{in})}{\rho V_{in}^2} \quad (1)$$

where,

$P_{out}$  = outlet static pressure (Pa)

$P_{in}$  = inlet static pressure (Pa)

$\rho$  = flow density ( $\text{kg/m}^3$ )

$V_{in}$  = inlet air velocity (m/s)

- (ii) Flow uniformity index ( $\sigma_{out}$ )

$$\sigma_{out} = \sqrt{\frac{1}{N-1} \sum_{i=1}^N (V_i - V_{out})^2} \quad (2)$$

where,

$N$  = number of measurement points

$V_i$  = local outlet air velocity (m/s)

$V_{out}$  = mean outlet air velocity (m/s)

The value of  $C_p$  indicates how much kinetic energy is successfully converted to pressure energy. The main problem in achieving high pressure recovery is flow separation, which results in non-uniform flow distribution. The  $\sigma_{out}$  is used to measure the dispersion of local velocity from the mean velocity. It is strongly dependent on the distribution of core flow and the presences of secondary flow. The flow is considered uniform with the presences of secondary flow of less than 10%.

In the current work, the performance of 3-D turning diffuser with 90° angle of turn ( $\Delta\phi$ ) as shown in Fig. 1 is intensively simulated by varying geometrical and operating parameters namely inflow Reynolds number ( $Re_{in} = 5.786 \times 10^4 - 1.775 \times 10^5$ ), inlet throat width ratio ( $L_{in}/W_1 = 1.5 - 25.0$ ) and outlet-inlet configurations ( $W_2/W_1 = 1.067 - 2.667$  and  $X_2/X_1 = 1.118 - 2.778$ ).

Asymptotic Computational Fluid Dynamic (ACFD) is a relatively new analytical technique established by Herwig et al. that applies Taylor Series expansion to produce correlations between all the relevant non-dimensional variables of the problem analysed by CFD [9-12]. This technique requires less number of solutions  $n + 1$  than the usual-used linear regression and curve fitting techniques,  $4^n$

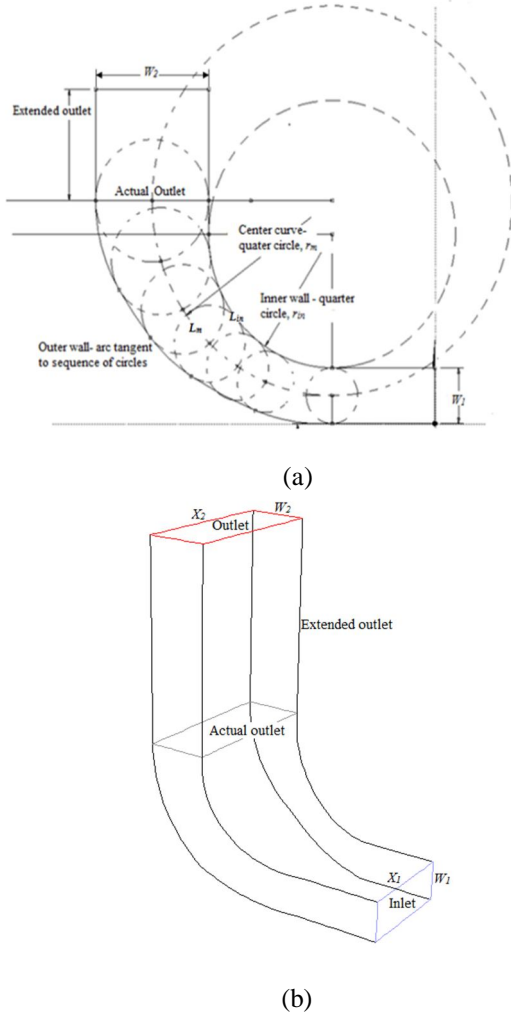


Fig. 1 A 90° 3-D turning diffuser (a) longitudinal section (b) isometric view

number of solutions to develop correlations from the CFD simulations, where  $n$  represents non-dimensional variables.

The performance correlations as a function of geometrical and operating parameters of 3-D turning diffuser are developed in the current work by means of ACFD, i.e.  $C_p = f(L_{in}/W_1, W_2/W_1, X_2/X_1, Re_{in})$  and  $\sigma_{out} = f(L_{in}/W_1, W_2/W_1, X_2/X_1, Re_{in})$ . These correlations minimise time and effort needed by other researchers to evaluate the performances of 3-D turning diffuser without necessarily of their own simulating the system.

## II. CFD METHODOLOGY

The  $C_p$  and  $\sigma_{out}$  were obtained from the CFD simulations by varying each geometrical and operating parameter within the specified range to five set of solutions. The reference case was prescribed at  $Re_{in,ref} = 6.382 \times 10^4$ ,  $W_2/W_{1ref} = 1.44$ ,

$X_2/X_{1ref} = 1.50$ ,  $L_{in}/W_{1ref} = 3.99$ . Other performance indicators such as loss coefficient ( $K$ ), dispersion of core flow ( $\sigma_y$ ), separation point ( $S$ ) and secondary flow index ( $S_{out}$ ) were considered to comprehensively discuss the results.

The following three-dimensional steady-state Reynolds Averaged Navier Stokes (RANS) equations were numerically solved:

Continuity equation:

$$\frac{\partial u}{\partial x} + \frac{\partial v}{\partial y} + \frac{\partial w}{\partial z} = 0 \quad (3)$$

x- momentum equation:

$$u \frac{\partial u}{\partial x} + v \frac{\partial u}{\partial y} + w \frac{\partial u}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial x} + \nu \left[ \frac{\partial^2 u}{\partial x^2} + \frac{\partial^2 u}{\partial y^2} + \frac{\partial^2 u}{\partial z^2} \right] + \frac{1}{\rho} \left[ \frac{\partial(-\rho \overline{u'u'^2})}{\partial x} + \frac{\partial(-\rho \overline{u'v'})}{\partial y} + \frac{\partial(-\rho \overline{u'w'})}{\partial z} \right] \quad (4)$$

y- momentum equation:

$$u \frac{\partial v}{\partial x} + v \frac{\partial v}{\partial y} + w \frac{\partial v}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial y} + \nu \left[ \frac{\partial^2 v}{\partial x^2} + \frac{\partial^2 v}{\partial y^2} + \frac{\partial^2 v}{\partial z^2} \right] + \frac{1}{\rho} \left[ \frac{\partial(-\rho \overline{u'v'})}{\partial x} + \frac{\partial(-\rho \overline{v'^2})}{\partial y} + \frac{\partial(-\rho \overline{v'w'})}{\partial z} \right] \quad (5)$$

z- momentum equation:

$$u \frac{\partial w}{\partial x} + v \frac{\partial w}{\partial y} + w \frac{\partial w}{\partial z} = -\frac{1}{\rho} \frac{\partial P}{\partial z} + \nu \left[ \frac{\partial^2 w}{\partial x^2} + \frac{\partial^2 w}{\partial y^2} + \frac{\partial^2 w}{\partial z^2} \right] + \frac{1}{\rho} \left[ \frac{\partial(-\rho \overline{u'w'})}{\partial x} + \frac{\partial(-\rho \overline{v'w'})}{\partial y} + \frac{\partial(-\rho \overline{w'^2})}{\partial z} \right] \quad (6)$$

The standard  $k-\varepsilon$  turbulence model adopted enhanced wall treatment,  $y^+ \approx 1.2 - 1.7$  as successfully validated in the previous progress was applied [13-15]. Each governing equation was independently solved using a double precision pressure-based solver. A robust pressure-velocity coupling algorithm, SIMPLE which uses a combination of momentum and continuity equations to derive an equation for pressure (or pressure correction) was applied. To reduce numerical diffusion, the QUICK scheme was employed for the discretization of the momentum equations, the turbulent kinetic energy equation and the turbulent dissipation rate equation. A PRESTO discretization scheme was applied for the continuity equation and a default scheme, i.e. Green-

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 Gauss Cell-based, was employed for the solution of the gradient. The solutions were considered converged when the scaled residual of all simulated variables dropped to  $10^{-6}$  and the conservation of overall mass balance through the domain boundary exceeded 99%.

### III. EFFECT OF VARYING GEOMETRICAL AND OPERATING PARAMETERS

Effects of varying geometrical and operating parameters ( $Re_{in}$ ,  $W_2/W_1$ ,  $L_{in}/W_1$  and  $X_2/X_1$ ) on the pressure recovery and flow uniformity of the 3-D turning diffusers are examined.

As depicted in Table 1, varying  $Re_{in}$  from  $5.786 \times 10^4$  to  $1.775 \times 10^5$  provides significant influence on the  $C_p$  and  $\sigma_{out}$ . The  $C_p$  is affected by the existences of flow separation and vortices, whereas the  $\sigma_{out}$  is resulted by the dispersion of core,  $\sigma_y$  and secondary flows,  $S_{out}$ . Applying high  $Re_{in}$  considerably influences the formation of vortices and onset flow separation of the 3-D turning diffuser as respectively shown in Fig. 2 and 3.

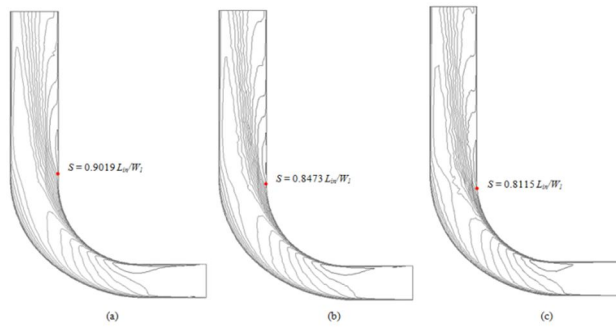


Fig. 2 Onset flow separation,  $S$  at (a)  $Re_{in} = 5.786 \times 10^4$ , (b)  $Re_{in} = 1.027 \times 10^5$  and (c)  $Re_{in} = 1.775 \times 10^5$

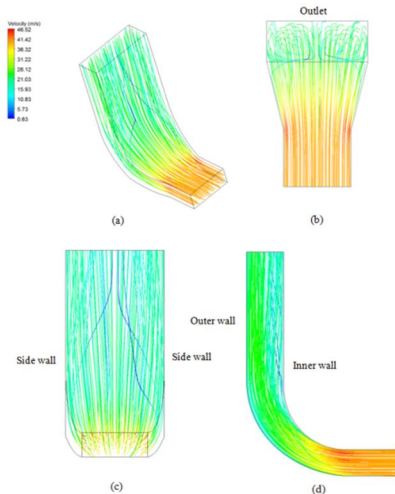


Fig. 3 Velocity streamlines at  $Re_{in} = 1.775 \times 10^5$  (a) isometric, (b) top, (c), front and (d) longitudinal views

Table 1 Effect of  $Re_{in}$

$Re_{in}$	Recovery performance		Flow performance		
	$C_p$	$K$	$\sigma_{out}$ (m/s)	$\sigma_y$ (m/s)	$S_{out}$
$5.786 \times 10^4$	0.216	0.784	2.71	2.91	0.133
$6.382 \times 10^4$	0.221	0.779	2.96	3.19	0.134
$1.027 \times 10^5$	0.205	0.795	4.56	4.94	0.141
$1.397 \times 10^5$	0.224	0.776	5.91	6.49	0.142
$1.775 \times 10^5$	0.192	0.808	7.23	7.88	0.152

Table 2 Effect of  $W_2/W_1$

$W_2/W_1$	Recovery performance		Flow performance		
	$C_p$	$K$	$\sigma_{out}$ (m/s)	$\sigma_y$ (m/s)	$S_{out}$
1.067	0.089	0.911	3.21	3.23	0.119
1.333	0.306	0.694	2.52	2.55	0.138
1.440	0.221	0.779	2.96	3.19	0.134
2.000	0.472	0.528	2.04	2.05	0.215
2.667	0.513	0.487	1.70	1.78	0.255

Table 3 Effect of  $L_{in}/W_1$

$L_{in}/W_1$	Recovery performance		Flow performance		
	$C_p$	$K$	$\sigma_{out}$ (m/s)	$\sigma_y$ (m/s)	$S_{out}$
1.52	-0.007	1.007	3.86	4.30	0.290
3.99	0.221	0.779	2.96	3.19	0.134
8.99	0.027	0.973	2.25	2.28	0.240
13.00	-0.243	124.3	2.51	2.51	0.075
25.00	-1.666	2.666	2.22	2.30	0.270

Table 4 Effect of  $X_2/X_1$

$X_2/X_1$ ( $\theta$ )	Recovery performance		Flow performance		
	$C_p$	$K$	$\sigma_{out}$ (m/s)	$\sigma_y$ (m/s)	$S_{out}$
1.118 (3.7°)	0.080	0.920	3.38	3.43	0.111
1.389 (11.9°)	0.192	0.808	3.02	3.18	0.125
1.500 (15.2°)	0.221	0.779	2.96	3.19	0.134
2.090 (30.6°)	-0.049	1.049	3.30	3.65	0.369
2.778 (43.9°)	0.373	0.627	1.49	1.40	0.308

Table 2 shows that the  $C_p$  and  $\sigma_{out}$  of the diffuser improve with the increase of  $W_2/W_1$  to maximum due to high turbulence intensity blending up uniformly the flow and nominal existences of flow separation within the inner wall as respectively shown in Fig. 4 and 5.

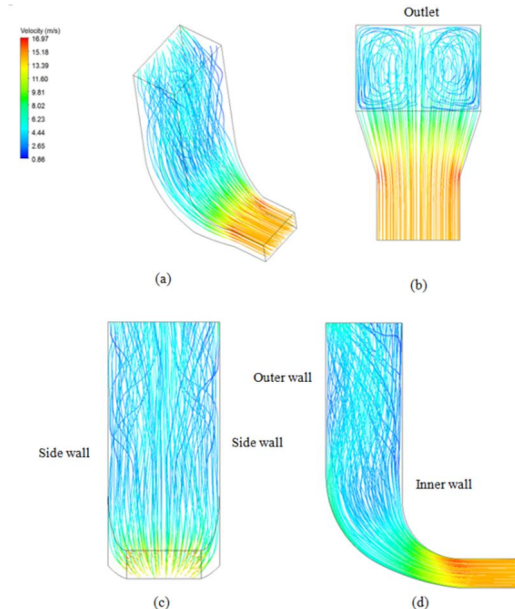


Fig. 4 Velocity streamlines at  $W_2/W_1 = 2.667$  (a) isometric, (b) top, (c), front and (d) longitudinal views

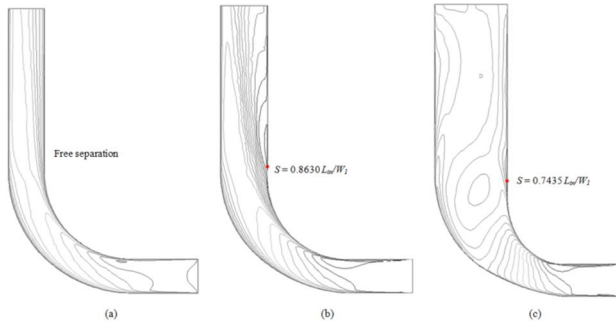


Fig. 5 Onset flow separation,  $S$  at (a)  $W_2/W_1 = 1.067$  (b)  $W_2/W_1 = 1.440$  and (c)  $W_2/W_1 = 2.667$

As depicted in Table 3, the best recovery of the 3-D turning diffuser,  $C_p = 0.221$  is attained by applying  $L_{in}/W_1 = 3.99$ . Nevertheless, elongating the diffuser  $L_{in}/W_1 \geq 8.99$  may associate with skin friction loss that is found to affect severely the recovery regardless of zero separation (Fig. 6, 7 (b) and (c)). Elongating the 3-D turning diffuser to maximum,  $L_{in}/W_1 = 25.0$  basically remedies the flow uniformity approximately of 43% from the worst,  $\sigma_{out} = 3.86$ . This is attributed by less dispersion of core flow at relatively long  $L_{in}/W_1$ .

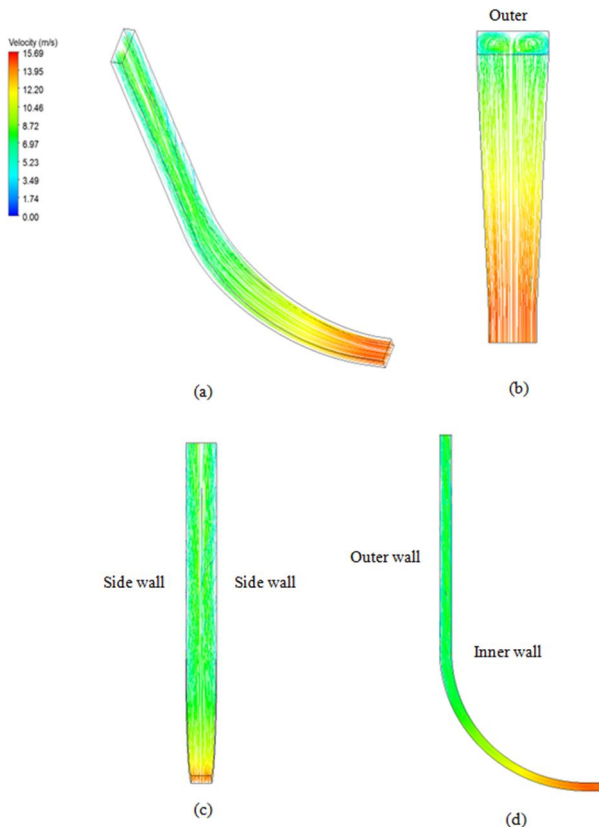


Fig. 6 Velocity streamlines at  $L_{in}/W_1 = 25.0$  (a) isometric, (b) top, (c), front and (d) longitudinal views

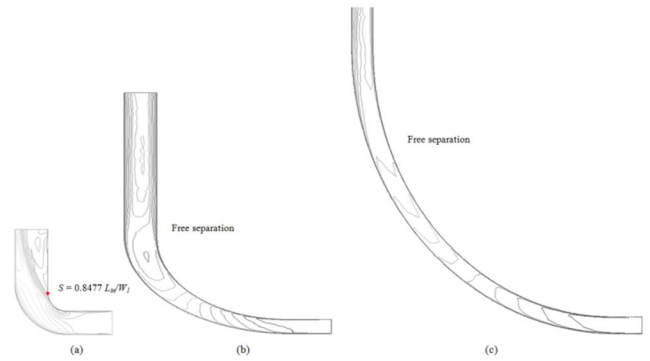


Fig. 7 Onset flow separation,  $S$  at (a)  $L_{in}/W_1 = 1.52$  (b)  $L_{in}/W_1 = 8.99$  and (c)  $L_{in}/W_1 = 25.0$

Table 4 shows that varying  $X_2/X_1$  influences significantly the recovery and flow performances of the 3-D turning diffuser. Increasing the turbulent intensity could really impede the flow separation and lessen the growth of inner wall boundary layer hence provides promising pressure recovery and flow uniformity (see Figures 8 and 9).

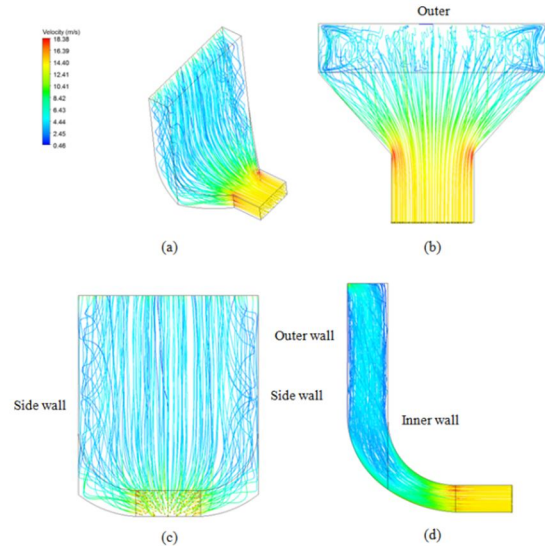


Fig. 8 Velocity streamlines at  $X_2/X_1 = 2.778$  (a) isometric, (b) top, (c), front and (d) longitudinal views

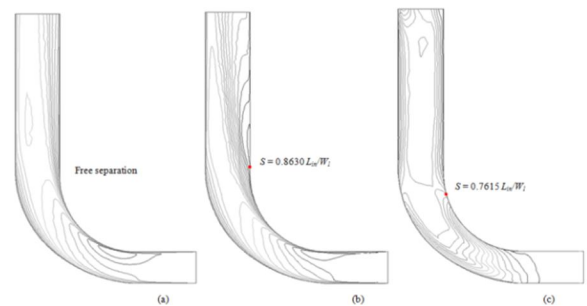


Fig. 9 Onset flow separation,  $S$  at (a)  $X_2/X_1 = 1.118$  (b)  $X_2/X_1 = 1.500$  and (c)  $X_2/X_1 = 2.778$

IV. PERFORMANCE CORRELATIONS VIA  
ACFD

Applying Taylor Series expansion to find outlet pressure recovery ( $C_p$ ) correlation:

$$C_{p\ 3DTD\ acfd} = C_{p\ ref} + (\phi_1 - \phi_{1\ ref}) \frac{\partial C_{p\ ref}}{\partial \phi_1} + (\phi_2 - \phi_{2\ ref}) \frac{\partial C_{p\ ref}}{\partial \phi_2} + (\phi_3 - \phi_{3\ ref}) \frac{\partial C_{p\ ref}}{\partial \phi_3} + (\phi_4 - \phi_{4\ ref}) \frac{\partial C_{p\ ref}}{\partial \phi_4} \quad (2)$$

where,

$$\phi_1 = \left[ \frac{Re_{in}}{Re_{in\ ref}} \right]^a, \phi_2 = \left[ \frac{L_{in}/W_1}{L_{in}/W_{1\ ref}} \right]^b, \phi_3 = \left[ \frac{W_2/W_1}{W_2/W_{1\ ref}} \right]^c, \phi_4 = \left[ \frac{X_2/X_1}{X_2/X_{1\ ref}} \right]^d$$

$a = 2, b = 1, c = 3, d = 3$  are chosen so that all lines could fit in a graph as shown in Fig. 10 and intersect at a point that represents as  $C_{p\ ref} = 0.230$

$$\phi_{1\ ref} = \left[ \frac{Re_{in\ ref}}{Re_{in\ ref}} \right]^a = 1.0, \text{ thus } \phi_{2\ ref} = \phi_{3\ ref} = \phi_{4\ ref} = 1.0$$

$$\frac{\partial C_{p\ ref}}{\partial \phi_1} = -0.0028, \frac{\partial C_{p\ ref}}{\partial \phi_2} = -0.03056, \frac{\partial C_{p\ ref}}{\partial \phi_3} = 0.0592,$$

$$\frac{\partial C_{p\ ref}}{\partial \phi_4} = 0.0306 \text{ are slopes of the corresponding lines}$$

Substituting all the constants in equation 2:

$$C_{p\ 3DTD\ acfd} = 0.230 - \left( \left[ \frac{Re_{in}}{Re_{in\ ref}} \right]^2 - 1 \right) 0.0028 - \left( \left[ \frac{L_{in}/W_1}{L_{in}/W_{1\ ref}} \right]^1 - 1 \right) 0.03056 + \left( \left[ \frac{W_2/W_1}{W_2/W_{1\ ref}} \right]^3 - 1 \right) 0.0592 + \left( \left[ \frac{X_2/X_1}{X_2/X_{1\ ref}} \right]^3 - 1 \right) 0.0306 \quad (3)$$

Applying Taylor Series expansion to find flow uniformity ( $\sigma_{out}$ ) correlation:

$$\sigma_{out\ 3DTD\ acfd} = \sigma_{out\ ref} + (\phi_1 - \phi_{1\ ref}) \frac{\partial \sigma_{out\ ref}}{\partial \phi_1} + (\phi_2 - \phi_{2\ ref}) \frac{\partial \sigma_{out\ ref}}{\partial \phi_2} + (\phi_3 - \phi_{3\ ref}) \frac{\partial \sigma_{out\ ref}}{\partial \phi_3} + (\phi_4 - \phi_{4\ ref}) \frac{\partial \sigma_{out\ ref}}{\partial \phi_4} \quad (4)$$

where,

$$\phi_1 = \left[ \frac{Re_{in}}{Re_{in\ ref}} \right]^a, \phi_2 = \left[ \frac{L_{in}/W_1}{L_{in}/W_{1\ ref}} \right]^b, \phi_3 = \left[ \frac{W_2/W_1}{W_2/W_{1\ ref}} \right]^c, \phi_4 = \left[ \frac{X_2/X_1}{X_2/X_{1\ ref}} \right]^d$$

$a = 2, b = 1, c = 3, d = 3$  are chosen so that all lines could fit in a graph as shown in Fig. 11 and intersect at a point that represents as  $\sigma_{out\ ref} = 3.2$

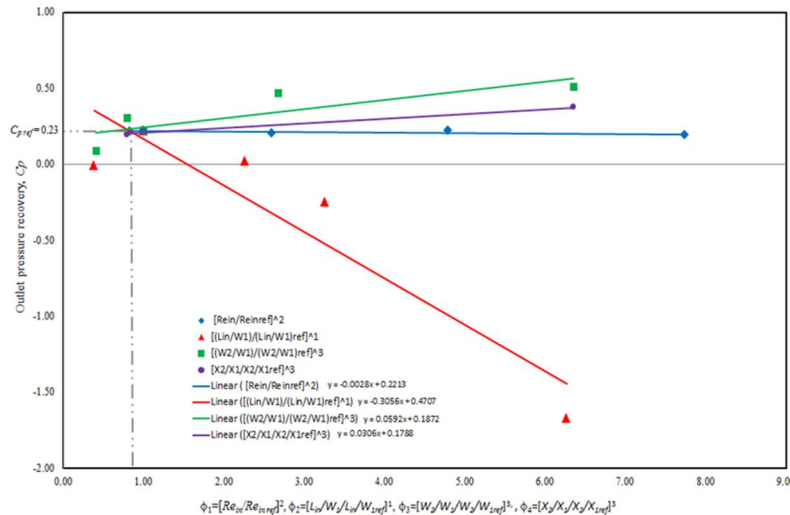


Fig. 10 Outlet pressure recovery,  $C_p$  of 3-D turning diffuser with respect to  $\phi_1 = [Re_{in}/Re_{in\ ref}]^2$ ,  $\phi_2 = [L_{in}/W_1/L_{in}/W_{1\ ref}]^1$ ,  $\phi_3 = [W_2/W_1/W_2/W_{1\ ref}]^3$  and  $\phi_4 = [X_2/X_1/X_2/X_{1\ ref}]^3$

$$\phi_{1\text{ ref}} = \left[ \frac{Re_{in\text{ ref}}}{Re_{in\text{ ref}}} \right]^a = 1.0, \text{ thus } \phi_{2\text{ ref}} = \phi_{3\text{ ref}} = \phi_{4\text{ ref}} = 1.0$$

$$\frac{\partial \sigma_{out\text{ ref}}}{\partial \phi_1} = 0.6531, \frac{\partial \sigma_{out\text{ ref}}}{\partial \phi_2} = -0.2202, \frac{\partial \sigma_{out\text{ ref}}}{\partial \phi_3} =$$

$$-0.2725, \frac{\partial \sigma_{out\text{ ref}}}{\partial \phi_4} = -0.2545 \text{ are slopes of the}$$

corresponding lines

Substituting all the constants in equation 4:

$$\begin{aligned} \sigma_{out\ 3DTD\ acfd} = & 3.2 + \left( \left[ \frac{Re_{in}}{Re_{in\text{ ref}}} \right]^2 - 1 \right) 0.6531 - \\ & \left( \left[ \frac{L_{in}/W_1}{L_{in}/W_{1ref}} \right]^1 - 1 \right) 0.2202 - \left( \left[ \frac{W_2/W_1}{W_2/W_{1ref}} \right]^3 - 1 \right) 0.2725 - \\ & \left( \left[ \frac{X_2/X_1}{X_2/X_{1ref}} \right]^3 - 1 \right) 0.2545 \end{aligned} \quad (5)$$

$C_{p\ 3DTD\ acfd}$  and  $\sigma_{out\ 3DTD\ acfd}$  obtained using developed correlations (3) and (5) are compared with the experimental results as respectively tabulated in Tables 5 and 6. Satisfied agreement between ACFD and experiment results with average deviation of 6.7 and 7.1% is respectively obtained. Hence, the developed correlations can be used as a guideline to preliminarily evaluate the performance of 3-D turning diffuser.

Table 5 Comparison of outlet pressure recovery coefficient ( $C_p$ ) of 3-D turning diffuser obtained from ACFD correlation and experiment

$\phi_{1,2,3}$	No.	$C_{p\ 3DTD\ cfd}$	$C_{p\ 3DTD\ acfd}$	$C_{p\ 3DTD\ exp}$	Deviation (%)	
$\phi_1$	0.822	1	0.216	0.230	0.210	9.8
	1.000	2	0.221	0.230	0.217	6.0
	2.590	3	0.205	0.226	0.203	11.1
	4.792	4	0.224	0.219	0.219	0.2
	7.735	5	0.192	0.211	0.194	8.8
$\phi_2$	0.381	6	-0.007	0.252	-	-
	1.000	7	0.221	0.230	0.217	6.0
	2.253	8	0.027	0.185	-	-
	3.258	9	-0.243	0.150	-	-
	6.266	10	-1.666	0.043	-	-
$\phi_3$	0.407	11	0.089	0.195	-	-
	0.793	12	0.306	0.218	-	-
	1.000	13	0.221	0.230	0.217	6.0
	2.679	14	0.472	0.329	-	-
	6.353	15	0.513	0.547	-	-
$\phi_4$	0.414	16	0.08	0.229	-	-
	0.794	17	0.192	0.230	0.217	6.0
	1.000	18	0.221	0.230	-	-
	2.705	19	-0.049	0.232	-	-
	6.352	20	0.373	0.236	-	-
Average deviation (%)					6.7	

Table 6 Comparison of flow uniformity index ( $\sigma_{out}$ ) of 3-D turning diffuser obtained from ACFD correlation and experiment

$\phi_{1,2,3}$	No.	$\sigma_{out\ 3DTD\ cfd}$	$\sigma_{out\ 3DTD\ acfd}$	$\sigma_{out\ 3DTD\ exp}$	Deviation (%)	
$\phi_1$	0.822	1	2.71	3.08	2.58	19.5
	1.000	2	2.96	3.20	3.20	0.0
	2.590	3	4.56	4.24	3.83	10.7
	4.792	4	5.91	5.68	6.59	13.9
	7.735	5	7.23	7.60	7.17	6.0
$\phi_2$	0.381	6	3.86	3.34	-	-
	1.000	7	2.96	3.20	-	-
	2.253	8	2.25	2.92	-	-
	3.258	9	2.51	2.70	-	-
	6.266	10	2.22	2.04	-	-
$\phi_3$	0.407	11	3.21	3.39	-	-
	0.793	12	2.52	3.27	-	-
	1.000	13	2.96	3.20	3.20	0.0
	2.679	14	2.04	2.67	-	-
	6.353	15	1.70	1.50	-	-
$\phi_4$	0.414	16	3.38	3.35	-	-
	0.794	17	3.02	3.25	-	-
	1.000	18	2.96	3.20	3.20	0.0
	2.705	19	3.3	2.77	-	-
	6.352	20	1.49	1.84	-	-
Average deviation (%)					7.1	

## V. CONCLUSION

In conclusion, the current work manages to intensively simulate the effects of geometrical and operating parameters on the performances of 3-D turning diffuser. The performance correlations as a function of geometrical and operating parameters are successfully developed via ACFD with deviation to the experiment approximately of 7%.

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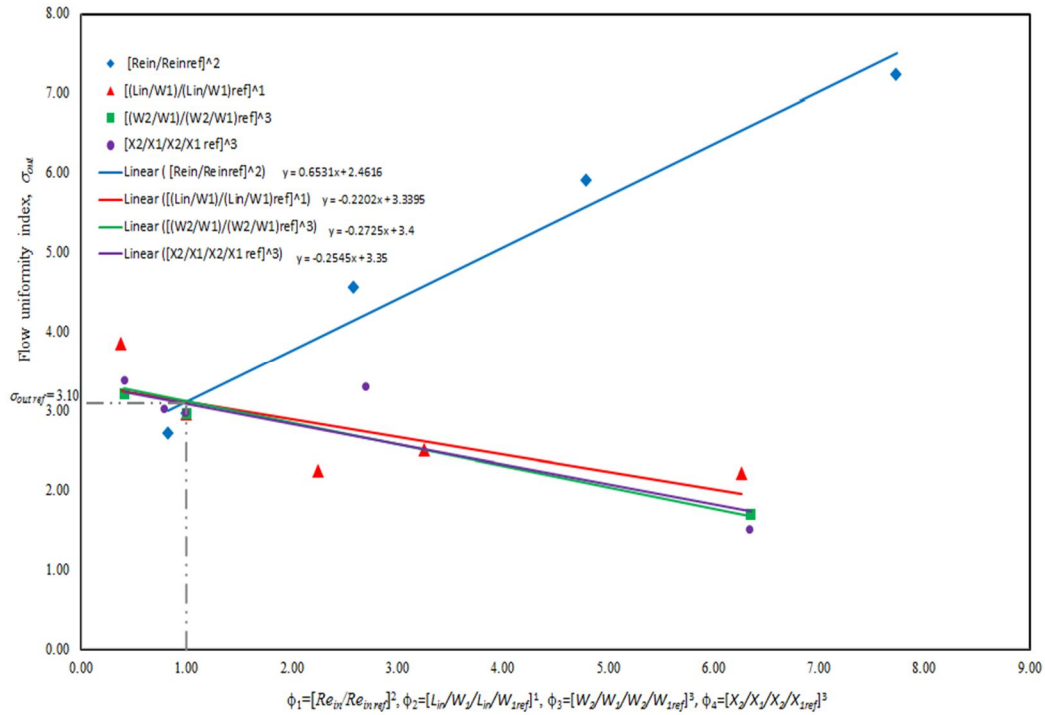


Fig. 11 Flow uniformity index,  $\sigma_{out}$  of 3-D turning diffuser with respect to  $\phi_1 = [Re_{in}/Re_{in\ ref}]^2$ ,  $\phi_2 = [L_{in}/W_1/L_{in}/W_{1\ ref}]^1$ ,  $\phi_3 = [W_2/W_1/W_2/W_{1\ ref}]^3$  and  $\phi_4 = [X_2/X_1/X_2/X_{1\ ref}]^3$