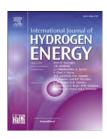
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Reducing cycling costs in coal fired power plants through power to hydrogen

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HIGHLIGHTS

- Hybrid operation of PtG and fossil fuel power plant is proposed to avoid shutdowns.
- The concept allows power plant continuous operation avoiding economic losses.
- The concept provides flexibility to power plants renewable energy for H2 production.
- Electricity producing cost is reduced between a 20% and 50% through the use of PtG.
- The reduction of shutdown economic penalties is larger than the incomes from H2.

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ABSTRACT

The increase of renewable share in the energy generation mix makes necessary to increase the flexibility of the electricity market. Thus, fossil fuel thermal power plants have to adapt their electricity production to compensate these fluctuations. Operation at partial load means a significant loss of efficiency and important reduction of incomes from electricity sales in the fossil power plant. Among the energy storage technologies proposed to overcome these problems, Power to Gas (PtG) allows for the massive storage of surplus electricity in form of hydrogen or synthetic natural gas. In this work, the integration of a Power to Gas system (50 MWe) with fossil fuel thermal power plants (500 MWe) is proposed to reduce the minimum complaint load and avoid shutdowns. This concept allows a continuous operation of power plants during periods with low demand, avoiding the penalty cost of shutdown. The operation of the hybrid system has been modelled to calculate efficiencies, hydrogen and electricity production as a function of the load of the fossil fuel power plant. Results show that the utilisation of PtG diminishes the specific cost of producing electricity between a 20% and 50%, depending on the framework considered (hot, warm and cold start-up). The main contribution is the reduction of the shutdown penalties rather than the incomes from the sale of the hydrogen. At the light of the obtained results, the hybrid system may be implemented to increase the cost-effectiveness of existing fossil fuel power plants while adapting the energy mix to high shares of variable renewable electricity sources.

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Introduction

The massive deployment of renewable energy technologies plays an essential role to tackle climate change, leading the transition towards a decarbonised society [1]. The European Union (EU), under the Paris Agreement (2015) on Climate Change [2], has established and updated specific objectives for the Member States to comply with the binding target to globally reduce greenhouse emissions at least 40% below 1990 levels by 2030. The European Directive 2018/2001 [3] on the promotion of the use of energy from renewable resources increases the previous objective of 27% of renewable share to reach a more ambitious target of 32% by 2030. Worldwide, the International Energy Agency (IEA) foresees a 43% increase in the global renewable power capacity between 2017 and 2022 [4].

Important challenges related to the grid and the electric sector in general must be tackled to achieve an efficient integration of renewable technologies in the generation mix, safeguarding security and economic balance [5,6]. Most power pools are designed to favour renewable electricity to the detriment of fossil-based electricity. The former role of fossil fuel power plants (FFPP) as base-load power has almost disappeared. Nowadays FFPP operate in cycling mode with frequent start-ups/shut-downs and continuous load variations to meet demand [7]. This kind of operation does not only deteriorate the equipment [8-10] but also causes drops in energy efficiency and increment in CO₂ emissions [11]. Although the additional emissions are negligible with regards to the CO2 reduction related to the savings in fossil fuel consumption (~45%), important economic penalties are derived from the increased number of start-ups under high variable renewable energy penetration (from around 0.6 to about 1 US\$/MWh) [12]. The cycling costs, together with the curtailment of incomes from electricity sale, could jeopardize the economic viability of fossil thermal plants.

The impacts of cycling coal power plants have been investigated during the last decade. In Europe, De Groot et al. [13] concluded that, under renewable penetration above 15%, the full load hours of coal-fired power plants decreased a 53% from 2005 to 2014, while the efficiency falls up to 10 points due to part-load operation. In Germany, a potential renewable increase from 14% to 34% in the period 2013–2030 would increase the number of start-ups and the respective costs by 81% and 119%, respectively [14]. In Central Western and Eastern Europe regions, the growth in the number of start-ups and load ramps was estimated in 4–23% and 63–181%, respectively [7], although the intensity of cycling operation depends strongly on the location of coal plant, being especially pronounced in Germany and the Czech Republic.

From real plant operation of two coal units of 300 MW and 600 MW in China, the increases in coal specific consumption and CO_2 emissions were estimated in 18% and 11%, respectively, at 35% load factor with respect to full load. NO_x emissions also grew 10% and 108%, respectively, while dust factor augmented 41% in both units. Regarding the impact of cold start-up, the NO_x emissions were equivalent to the amount of 8 and 12 h of regular full load operation, respectively, while dust emissions are roughly equal to those emitted during 7 h at full load in both units [11].

Regarding economic impacts, the selling price of electricity would not cover the generation costs in FFPP, even if enough flexibility is reached to integrate renewables [15]. Hentschel et al. [16] showed that faster ramp rates does not induce significant profits, but 50% reduction in minimum complaint load (MCL) decreases start-up costs by 71.43%, and increases profit by 7.11% in coal-fired power plants by avoiding the curtailment of incomes [16]. Also, lower MCL may reduce the start-up duration and subsequently its cost by 70% for hard coal plants and above 45% for lignite units [16,17].

In the North-eastern China, Yin et al. analysed and compared different scenarios of wind curtailment and regulation for coal-fired power plants [18]. The optimal scenario regarding economics requires wind curtailment of about 2% (meaning 17.5 TWh) to avoid excessive variability in the FFPP. They did not consider any energy storage for managing the demand variations.

Those facilities with lower MCL take huge advantage over their competitors to avoid stops in future scenarios with high variable renewable energy penetration. In general, this minimum load in coal-fired power plants is around 30–40% of the nominal power [15,19]. If a particular facility is able to reduce this load (e.g., down to 30%) when required by the grid operator, this power plant could remain working while other power plants will have to stop [20]. Moreover, the power initially assigned to those installations that finally have to stop will be distributed among the other power plants still working. Therefore, it will be highly probable that the latter will not have to operate at its MCL.

Under this framework, surplus electricity storage could be a transient solution to virtually reduce the minimum complaint load, thus favouring the cycling operation in power plants. Current share of renewables requires storage capacity ratios of 10% compared to the installed power capacity [14]. This figure could grow substantially for higher solar and wind penetration. In fact, passing from 80% to 100% renewable share in the energy mix implies to triple the capacity required for electricity storage [14]. Power to fuel will play an essential role in the future electricity market because of the versatility of fuels to be used in diverse sectors and the long-term storage character without significant losses [21–23].

Under the current transition of the energy network, this manuscript proposes the storage of electricity through Power to Gas (PtG) to reduce the minimum complaint load and avoid the shutdown of coal-fired power plants. Power to Gas consumes surplus electricity to produce hydrogen as energy vector through electrolysis (or methane through the methanation of the stored hydrogen and capture CO₂) [24–26]. A similar concept was studied by the authors, in which surplus electricity is stored from a nuclear power plant in order to allow a coal-fired power plant to sell electricity in its place [27]. In this case, the yearly-round efficiency of the coal-fired power plant increased two points, from 33.2% to 35.2%.

The objective and novelty of this paper is to demonstrate and quantify the economic benefits of reducing the minimum complaint load of coal-fired power plants through electricity storage via Power to Gas with hydrogen production. The continuous operation at MCL coupled with PtG is compared to scenarios in which shutdown takes place and conventional hot-, warm- and cold start-ups are needed.

Case study

The coal-fired power plant selected in this work is assumed to have a gross power output of 500 MW_e (of which 5% are consumed by the auxiliaries) with a minimum complaint load of 40%. The Power to Hydrogen system coupled to the power plant may consume up to the 10% of its nominal gross power (i.e., 50 MW_e). The efficiency of the electrolyser is assumed 75% (Alkaline type, HHV-basis), with neglecting variations at partial load [28]. The coupling of the power plant with this energy storage process provides flexibility allows virtually reducing its minimum complaint load to 30% of nominal full load (Fig. 1).

Operation framework

A reduction of the grid electricity demand or an extremely large production of renewable energy will force coal-fired power plants to reduce their operation load. If load falls below the minimum compliant load, the power plant will have to stop. The conceptual framework of the six most relevant cycling processes that describe the variation in speed and load of coal-fired power plants is given in this section (Fig. 2). These concepts and assumptions will be used while establishing the different scenarios under study which exhaustively cover the potential operation sequences of the power plants [29].

- Process 1. From 'no speed no load' (NSNL) to 'minimum complaint load' (MCL). First, the speed of the turbine increases from zero to 'full speed no load' (FSNL), which corresponds to the value at which the generator is synchronized to the grid frequency and the turbine may start generating power. Then, the load increases from FSNL to MCL. MCL is the minimum load at which the turbine is complaint with technical limitations and emissions. The total duration of Process 1 depends on the type of startup. It will take a total of 3 h for hot starts (i.e., for offline).
 - The total duration of Process 1 depends on the type of start-up. It will take a total of 3 h for hot starts (i.e., for offline periods between 6 h and 12 h prior the start), 9 h for warm starts (i.e., 24–48 h offline) and 21 h for cold starts (i.e., 72–96 h offline) [29]. It must be noted that no power output will be produced during part of Process 1; specifically, from NSNL to FSNL situations. In this study, it is assumed as simplification that the facility only produces power during the last one-third of the time, at a load equal to the MCL.
- Process 2. In this process, the load of the turbines can be varied between the minimum complaint load and the full load (FL). The ramp rate is assumed to be 2% of the full load per minute, for both increasing or reducing the load of the turbines. The time spent in Process 2 is much lower compared to the other cycling processes, and therefore neglected for the economic calculations in this study.
- Process 3. In this process, the coal-fired power plant performs a full load continuous operation.
- Process 4. In this process, the coal-fired power plant performs a continuous operation at minimum complaint load.
- Process 5. The Process 5 represents the shutdown of the power plant. The load is reduced and the speed of the turbine decreases from full load to zero, practically ceasing operation. The shutdown ramping rate is assumed to be 2%

- full load/min, which implies that half an hour is required to vary from full to minimum complaint load (40%) and a total of 50 min to reach NSNL. In this study, Process 5 will be simplified as a power production equal to MCL of 1-h duration, when computing costs and incomes.
- Process 6. This corresponds to the period in which the power plant is out of operation. It does not represent a hard-physical limit, but rather an economic limitation. Operators are interested in minimizing the number or start-ups and shut-downs to reduce thermal stress on the equipment and the subsequent O&M costs. Also, the time spent in Process 6 must be minimized to reduce the curtailment of economic incomes.

Methodology

The three most common shut-down sequences in fossil fuel power plant have been considered (hot, warm and cold shut-down) and six reference cases have been simulated: two reference cases for hot stops (6 and 12 h), two more cases for warm (24 and 48 h) and two others for cold shut-down (86 and 110 h). Conventional fossil fuel power plant operation is illustrated in Fig. 3 and the main difference between the reference cases is the duration of outage periods (X-axis).

The model considers the day divided in 24 h and calculates full and partial load performance of fossil fuel power plants according to an efficiency penalization and the state-of-theart operation behaviour. Hourly gross and net power, plant efficiency and chemical energy of the required fuel are the main technical outputs of the model. Economic parameters such as OPEX and CAPEX are calculated hourly and the fixed costs associated to the shut-downs are added. Other variables as CO₂ emissions and fuel costs are also calculated.

PtG hybridation with the fossil power plant allow for avoiding the shut-down of the power plant whenever the MCL has to be reduced from 40% (200MWe/500MWe) to 30% ((200-50)/500 MWe). Under hybridized operation, the fossil fuel power plant operates at 40% sending to the grid the demanded 30% and to the electrolyser the remaining 10% which corresponds to 50 MWe.

Therefore, the gross power, the efficiency and the input energy are calculated taking into account that the power plant operates at 40% load but only 30% of the power is sold to the electrical grid. The hourly economic parameters (OPEX, CAPEX and fixed cost of the stops) together with carbon emissions and fuel costs other OPEX are also calculated. Under this hybrid operation, the ramp-up of the power plant back to fulload operation (from MCL to FL) is faster since Process 1 is avoided. The hourly economic variables are also calculated for this period of time (Process 2).

Efficiency penalization and emissions

Partial load operation in coal-fired power plants worsens the radiative and convective exchanges inside the boiler, reducing thermal efficiency. Consequently, more fuel (per unit of power output) is needed and specific CO_2 emissions increase. Also, the variation of the temperature reached during combustion increases specific emissions [30].

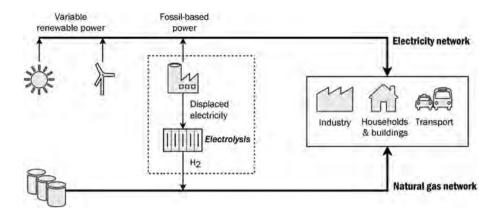


Fig. 1 – Integration of Power to Gas and fossil-based power plants in the energy system.

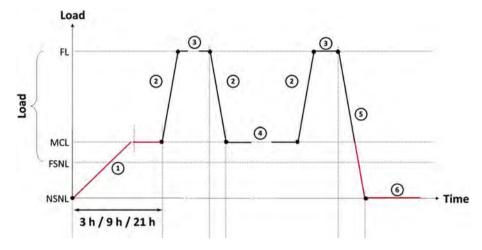


Fig. 2 - Type of cycling processes in coal-fired power plants.

Partial load curves provide the range of decrease in energy efficiency under partial load operation. According to the literature [13], a decrease of 3–8% points could be achieved in the energy efficiency of the coal-fired power plants. Eq. (1), taken from [11] (similar to Ref. [15]), presents a linear regression model derived from an extensive set of experimental data which related gross efficiency and load operation of the plant expressed as a decimal.

$$\eta_{qross} = -0.0703 \cdot load^3 + 0.0507 \cdot load^2 + 0.1266 \cdot load + 0.313$$
 (1)

Typical performance parameters of a 500 MW $_{\rm e}$ subcritical coal-fired power plant are calculated using Eq. (1) presented in Table 1 [11].

The specific CO_2 emissions at full load amount to 785.7 kg/MWh (i.e., 330 kg/MWh_{th}). The decrease in thermal efficiency makes these emissions to increase up to 898.6 kg/MWh (an increment of 14%) when operating at 40% load.

Economics

The economic assessment compares the cost of conventional shutdowns (hot-, warm- and cold start-ups) with the cost of continuous operation at MCL coupled with PtG. The following variables are quantified: (i) total cost (Eq. (2)), (ii) specific cost of electricity, (iii) incomes (Eq. (3)), and (iv) differential profit.

$$Total cost \left\lceil \frac{\epsilon}{h} \right\rceil = OPEX \left\lceil \frac{\epsilon}{h} \right\rceil + CAPEX \left\lceil \frac{\epsilon}{h} \right\rceil$$
 (2)

$$\begin{aligned} &\mathsf{OPEX}\Big[\frac{\mathfrak{S}}{h}\Big] = \mathsf{Fuel}\; \mathsf{costs}\Big[\frac{\mathfrak{S}}{h}\Big] + \mathsf{FixedO}\; \mathsf{PEX}\Big[\frac{\mathfrak{S}}{h}\Big] + \mathsf{Other}\; \mathsf{OPEX}\; \Big[\frac{\mathfrak{S}}{h}\Big] \\ &\mathsf{Incomes}[\mathfrak{S}] = \mathsf{Net}\; \mathsf{Electricity}\; \mathsf{Production}\; [kWh] * \mathsf{Electricity}\; \mathsf{Price}\Big[\frac{\mathfrak{S}}{kWh}\Big] \end{aligned}$$

The CAPEX is assumed 2400 €/kWe for the conventional coal-fired power plant [31], and 1800 € per kWe of installed capacity of electrolysis for the Power to Hydrogen facility [32] plus and an additional 10% due to connections to the coal power plant. This cost is distributed along the installation lifetime of 25 years. The power plant will present fixed OPEX of 35,000 €/MWe/y [33] and variable OPEX of 3.2 € per MWh_e of electricity [31,34], Table 2. The total OPEX will vary between 32.3 €/MWh_e at full load (i.e., 25.1 €/MWh_e fixed plus 7.2 €/MWh_e variable) and 41.9 €/MWh_e at minimum complaint load (i.e., 28.7 €/MWh_e fixed plus 13.2 €/MWh_e variable). Additional shutdown costs are included and assumed to be 75,000 € for hot start-up, 92,500 € for warm start-up and 140,000 € for cold start-up [34,35].

Other economic values presented in Table 2 are the price of coal, and the selling prices of hydrogen and electricity. It

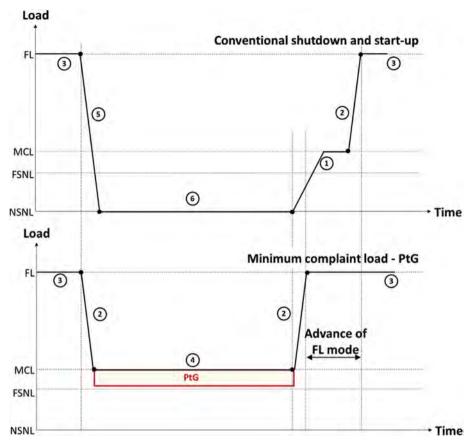


Fig. 3 — Cycling process for conventional shutdown and start-up (top), and for operation at minimum complaint load with PtG facility coupled (bottom).

has been considered a pessimistic PEM electrolyser cost by 2030 (1700 €/kWe) [36] plus an additional quantity for a hydrogen tank and an additional 10% for balance of plant (BOP). The coal fuel price considered is the average of the period 2015-2018 in the Northwest European market price according the data in [37]. It has been assumed 60 €/MWh_e as the lowest Electricity prices for non-household consumers [38], however this variable has high uncertainty as it is 60 pounds/MWh_e in the UK [39], a range between 70 and 125 €/ MWh for several European countries [40] or up to 130\$/MWh_e in Singapore [41]. The price of hydrogen considered is based in the most cost effective hydrogen generated by steam reforming 34 €/MWh [42]. Under these assumptions, the cost of producing electricity is calculated by adding the OPEX costs (fixed cost plus coal costs) and CAPEX costs distributed in 25 years. This cost ranges from 44.3 €/MWh_e, when operating at full load, to 53.9 €/MWh_e for minimum complaint load situations.

Start-up scenarios

For comparison purposes, all data related to production, emissions and economics are calculated for specific time frames: 24 h for the hot start-ups, 72 h for the warm start-ups and 120 h for the cold start-ups.

Table 1 — Performance of a 500 MW _e subcritical coal-fired	
power plant at partial load.	

Load factor [%]	Thermal efficiency gross [%]	Coal input power [MW _{th}]	Specific CO ₂ emissions [kgCO ₂ /MWh]
100	42.00	1190.5	785.7
90	41.68	1079.8	791.8
80	41.07	973.9	803.4
70	40.24	869.9	820.2
60	39.20	765.3	841.8
50	38.02	657.6	868.0
40	36.73	544.6	898.6

Scenario 1 — Hot start-up

Fig. 3 illustrates the two different operating modes compared in Scenario 1. These two modes correspond to (i) conventional and (ii) PtG concept operation when the load of the power plant required by the grid operator is below MCL. In conventional shutdowns the power plant follows the sequence 5, 6, 1 and 2 of the processes described in Section Case study, while in the proposed concept using Power to Gas follows the sequence 2, 4 and 2 of these processes. As Scenario 1 considers hot start-up, the duration of Process 1 (i.e., from NSNL to MCL) will be 3 h, during which power is produced only for 1 h and at a load equal to MCL (see section Case study).

The results section presents the analysis of single shutdowns of 6 and 12 h duration, within a time framework of 24 h.

Scenario 2 — Warm start-up

Under longer shutdown periods, the situation described in Fig. 3 is a very conservative assumption, since the grid operator will probably require a load increment during the shutdown. This requirement is associated to the instantaneous coverage of the load coming from other less flexible power plants that are forced to stop. Hence, besides the situations described in Fig. 3, an additional case is studied in Scenario 2. This additional case considers a temporary load increase from MCL to full load during the shutdown period (Fig. 4). It is only considered for the operation with PtG, as conventional operation would present a very limited time at full load due to the time spent in Process 1 (illustrated in the bottom graph of Fig. 4).

The analysis of the Scenario 2 is performed in a time frame of 72 h. For each of the three cases (i.e., conventional, PtG, and PtG with temporary full load), two single shutdowns of 24 and 48 h are studied. The duration of the temporary load increment is fixed at 12 h in both cases (PtG keeps working until 100% load is reached). Also, as Scenario 2 considers warm start-up, the duration of Process 1 will be 9 h, during which power is produced only for 3 h at MCL.

Scenario 3 — Cold start-up

Scenario 3 analyses the same cases that Scenario 2, assuming a longer time frame and a cold start-up. Hence, it is compared the conventional shutdown (Fig. 3, top), the continuous operation at MCL thanks to Power to Gas (Fig. 3, bottom), and the operation at MCL through PtG with a temporary load increment up to full load (Fig. 4, middle).

The analysis is performed in a time frame of 120 h. For each of the three cases, two single shutdowns of 72 and 96 h are studied. The duration of the temporary load increment is fixed at 24 h. Also, as cold start-up is assessed, the duration of

Table 2 – Main assumptions of	the model.	
Variable	Value	Reference
Technical		
Gross power plant output [MW _e]	500	
Ancillaries' consumption [%]	5	
Net power plant output [MW _e]	475	
Power to Hydrogen capacity [MW _e]	50	
Electrolyser efficiency [%]	75	[28]
Economic		
CAPEX power plant [€/kW _e]	2400	[31]
CAPEX Power to Hydrogen [€/kW _e]	1800 + 10%	[36]
Fixed OPEX [€/MW _e /y]	35,000	[33]
Variable OPEX [€/MWh _{th}]	3.2	[31,34]
Shutdown cost [€]		
Hot start-up	75,000	[34,35]
Warm start-up	92,500	[34,35]
Cold start-up	140,000	[34,35]
Coal fuel price [€/MWh _{th}]	10	[37]
Pool electricity price [€/MWh _e]	60	[38]
Hydrogen price [€/MWh _{th}]	30	[42]

Process 1 will be 21 h, during which power is produced only for 7 h at MCL.

Results

Scenario 1 - Hot start-up

In this section, the conventional shutdown is compared with the continuous operation at MCL through Power to Gas. The technical and economic results are gathered in Table 3 for shutdowns of 6 and 12 h duration in a time frame of 24 h.

It can be seen that despite the duration of the shutdown is limited, conventional operation leads to economic losses in both cases. For 6 h shutdowns, the costs associated to the start-up process makes profits to be negative. While for 12 h shutdowns, the curtailment of incomes from selling the electricity is equally critical. Considering the 24 h time frame, the specific cost of produced electricity increases up to 67.0 $\[\in \]$ MWh_e and 93.6 $\[\in \]$ /MWh_e.

When the plant is continuously operated at minimum complaint load, the sale of electricity increases 30%−72% (6 h−12 h shutdowns respectively) and start-up costs are avoided. Thus, specific production costs are kept in the range 52−61 €/MWh_e, which is below or close above the selling price. This decrease of production costs transforms the conventional shutdown situation with economic losses into a profitable operation.

In order to make comparisons, the differential profit is preferred. This economic parameter is the difference between the profits of the two alternative proposals, i.e., the potential savings. Thus, the continuous operation at MCL through PtG allows saving $124,740-145,375 \in$ when the shutdown lasts for 6-12 h.

As expected, the application of Power to Gas provides higher savings at longer shutdown periods. Nevertheless, most part of the incomes comes from the electricity sale. The potential incomes related to hydrogen sale represent only between 5.4% and 9.3% of the differential profit. Therefore, the economic improvement of the alternative mode of operation (continuous MCL via PtG) is not related to the energy storage technology that is used but to the avoidance of the shutdown itself.

It should be mentioned that avoiding shutdowns makes CO_2 emissions to grow 36% and 92% (for 6 h and 12 h shutdowns, respectively) as the coal consumption increases in the same proportion.

Scenario 2 - Warm start-up

In Scenario 2, medium outages periods (24–48 h) are assessed under a reference time frame of 72 h, Table 4. The conventional shutdown with warm start-up is compared to the continuous operation at MCL, and to the operation at MCL with a temporary power production at full load.

As in Scenario 1, the absolute profit of conventional shutdowns is negative. It may be noticed that in this case there is a remarkable difference in profit values when comparing the 24 h and 48 h shutdowns, Fig. 5. This divergence is mainly associated to the ratio between the offline period and the time

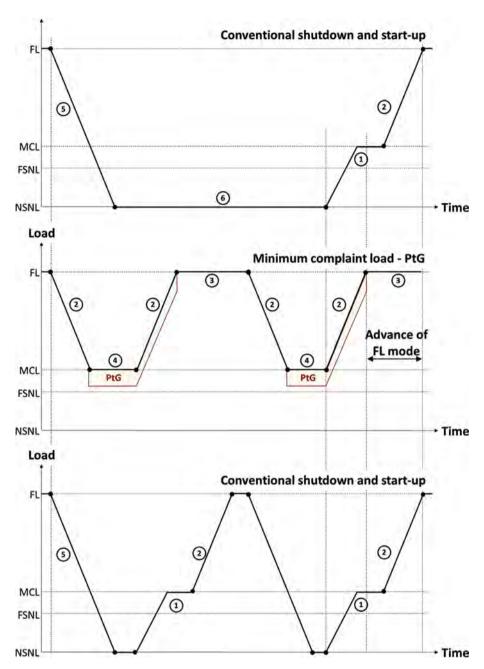


Fig. 4 — Cycling process for conventional shutdown and start-up (top), for operation at minimum complaint load with PtG and intermediate full load period (middle), and for conventional shutdown and start-up with intermediate full load period (bottom).

frame. In the 48 h shutdown, the offline period consumes twothirds of the reference time frame, while the warm start-up spends 9 additional hours. This gives a total of 57 h, representing the 80% of the total time frame of 72 h. Thus, the electricity production is very limited and the economic results are conditioned by this fact. In any case, as conclusions are drawn by the differential profit between the Power to Gas concept and the conventional operation, the influence of the time frame is palliated.

Regarding the specific cost of generating electricity, it increases up to 64.3 \in /MWh_e and 119.9 \in /MWh_e for

conventional shutdowns of 24 and 48 h, respectively. When the outage is avoided by continuously operating at MCL via PtG, the specific cost diminishes to $54.2 \in /MWh_e$ and $68.7 \in /MWh_e$. Under this concept, the former value becomes competitive, presenting costs below the selling price. Additionally, both values are lowered to $49.9 \in /MWh_e$ and $60.1 \in /MWh_e$ in the case that the grid operator requires temporarily to rise load to 100% (12 h) during the offline period.

The revenues from the sale of hydrogen may represent a higher percentage of the differential profit than in Scenario 1, but still the avoidance of the shutdown is the main

Case	Conventional shutdown	MCL with PtG	Conventional shutdown	MCL with PtG
Start-up	Hot	n/a	Hot	n/a
Shutdown duration [h]	6	6	12	12
Time frame [h]	24	24	24	24
Technical data				
Input coal [MWh _{th}]	17,645.34	24,075.83	10,502.48	20,200.48
Electricity produced (total) [MWh _e]	6982.50	9105.00	4132.50	7095.00
Electricity production increment with respect to conventional	n/a	2122.50	n/a	2962.50
shutdown [MWh _e]				
Electricity directed to PtG [MWh _e]	n/a	300.00	n/a	600.00
Stored energy (H ₂) [MWh]	n/a	225.00	n/a	450.00
CO ₂ emissions [t]	5823	7945	3466	6666
Economic data				
Costs [€]	392,736	476,975	311,708	432,642
Start-up cost [€]	75,000	n/a	75,000	n/a
Total costs [€]	467,736	476,975	386,708	432,642
Cost increment with respect to conventional shutdown [€]	n/a	9239	n/a	45,934
Incomes electricity [€]	418,950	546,300	247,950	425,700
Incomes H ₂ [€]	n/a	6750	n/a	13,500
Total Incomes [€]	418,950	553,050	247,950	439,200
Profit [€]	-48,786	-138,758	76,075	6738
Differential profit [€/24h]	n/a	124,861	n/a	145,496
Differential hourly profit [€/h]	n/a	5203	n/a	6062

contribution. The income from hydrogen ranges between 10.4% and 15.8% of the differential profit when operating continuously at MCL, and it decreases to 3.4%—8.4% if a temporary load increment is demanded.

The hourly differential profits are lower than for hot start-ups in Scenario 1 if continuous operation at MCL is performed (from 3600 \in /h to 4750 \in /h), but higher if the temporary load increase is required (5525 \in /h to 6670 \in /h). This clearly shows that the lower contribution of H₂ incomes to the differential profit, the higher the hourly differential profit.

Scenario 3 — Cold start-up

Specific cost of electricity [€/MWh_e]

Specific cost of additional electricity [€/MWh]

In Scenario 3, long outages of 72 and 96 h are considered, within a total time frame of 120 h. Besides, the operation under conventional shutdown uses cold start-up to resume power production, spending 21 additional hours in this process. Thus, according to the assumptions in Section Case study, the longer shutdown in conventional operation will present 110 h without power production, 7 h at MCL, and 3 h at full load. This limited electricity production leads to a specific cost of 950 €/MWh_e in the time frame of 120 h. In Scenario 3, the specific cost of electricity is below the selling price (i.e., below 60 €/MWh_e) only in the case of 72 h shutdown, operating at MCL through PtG, and attending the operator's requirement of a load increment to 100% for 24 h (Table 5, third column). Hence, positive economic profit is only found under this particular case. Nevertheless, the differential profit is remarkable in all cases, and may be as high as 588,800 € for the best case.

As in the previous scenarios, when the profit generated from the hydrogen sale is relevant (e.g., up to 46.3% of the differential profit in the case of 72 h shutdown), the differential hourly profit decreases (down to 1457 €/h in this case).

93 58

60.95

15.44

52.39

4.35

Sensitivity analysis

66 99

The most significant and uncertain economic parameters used in the calculations of the model are the CAPEX cost of the PtG system and the costs of shut-down and start-ups. A sensitivity analysis was performed to determine the effect of the assumed parameters in the obtained results. CAPEX cost of the PtG system is varied a 20%, while coal and shut-down and start-up costs are varied a 10%.

Table 6 summarizes the economic results for the Scenario 1 (Hot start-up with stops of 6 and 12 h) and Scenario 3 (Cold start-up with 72 h stop). As previously analysed, the base case shows losses in the reference case, i.e. current power plants, and profits when PtG is used to virtually reduce MLC and to store energy. In the case of a hot stops of 6 h, the difference between both cases totalized 124,861 € (76,075 - (-48,786)). The influence of a 20% change in PtG CAPEX is not relevant with a variation of 3% in the profit of the PtG cases. The influence in the coal cost is the most relevant variable in this sensitivity analysis. In this case, a variation of 10% in the coal cost changes the economic results of reference and PtG cases. The net profit in the case of an increment of 10% adds up 118,430 € similar to the base case but with different addends (51,999 - (-66,431)). If coal cost decreases the profit is 131,292 €. Finally, a 10% variation of the shut-down and start-

Table 4 $-$ Conventional shutdown operation vs. continuous operation at MCL (PtG) vs. continuous operation at MCL (P	tG)
with temporary Full Load, under Scenario 2 assumptions, Bold represents the key variables of the system.	

Case	Conventional shutdown	MCL with PtG	MCL with PtG and temporary FL	Conventional shutdown	MCL with PtG	MCL with PtG and temporary FL
Start-up	Warm	n/a	n/a	Warm	n/a	n/a
Shutdown duration [h]	24	24	24	48	48	48
Temporary Full Load duration [h]	n/a	n/a	12	n/a	n/a	12
Time frame [h]	72	72	72	72	72	72
Technical data						
Input coal [MWh _{th}]	47,305.93	69,592.63	77,368.98	18,734.50	54,091.22	61,867.57
Electricity produced (total) [MWh _e]	18,762.50	25,875.00	29,895.00	7362.50	17,835.00	21,855.00
Electricity production increment with	n/a	7112.50	11,132.50	n/a	10,472.50	14,492.50
respect to conventional shutdown [MWh _e]	,			,		
Electricity directed to PtG [MWh _e]	n/a	1200	600	n/a	2400	1800
Stored energy (H ₂) [MWh]	n/a	900	450	n/a	1800	1350
CO ₂ emissions [t]	15,611	22,966	25,532	6182	17,850	20,416
Economic data						
Costs [€]	1,114,228	1,400,737	1,490,021	790,113	1,222,683	1,311,967
Start-up cost [€]	92,500	n/a	n/a	92,500	n/a	n/a
Total costs [€]	1,206,728	1,400,737	1,490,021	882,613	1,222,683	1,311,967
Cost increment with respect to conventional shutdown [€]	n/a	194,009	283,293	n/a	340,070	429,354
Incomes electricity [€]	1,125,750	1,552,500	1,793,700	441,750	1,070,100	1,311,300
Incomes H ₂ [€]	n/a	27,000	13,500	n/a	54,000	40,500
Total Incomes [€]	1,125,750	1,579,500	1,807,200	441,750	1,124,100	1,351,800
Profit [€]	-80,978	178,763	317,179	-440,863	-98,583	39,833
Differential profit [€/24h]	n/a	259,740	398,157	n/a	342,280	480,697
Differential hourly profit [€/h]	n/a	3602	5530	n/a	4754	6676
Specific cost of electricity [€/MWh _e]	64.32	54.13	49.84	119.88	68.56	60.03
Specific cost of additional electricity [€/MWh]	n/a	27.28	25.45	n/a	32.47	29.63

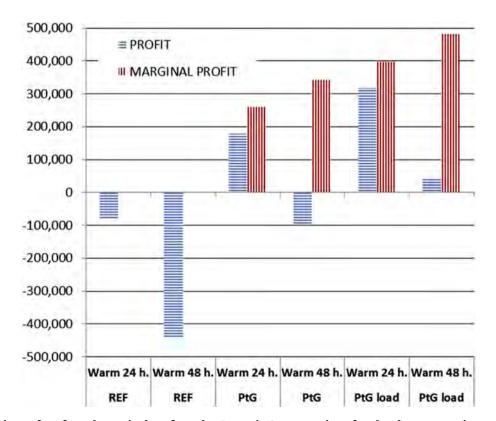


Fig. 5 — Comparison of profit and marginal profit under Scenario 2 assumptions for shutdown operation vs. continuous operation at MCL (PtG) vs. continuous operation at MCL (PtG) with temporary Full Load.

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Table 5 — Conventional shutdown operation vs. continuous operation at MCL (PtG) vs. continuous operation at MCL (PtG) with temporary Full Load, under Scenario 3 assumptions. Bold represents the key variables of the system.

Case	Conventional shutdown	MCL with PtG	MCL with PtG and temporary FL	Conventional shutdown	MCL with PtG	MCL with PtG and temporary FL
Start-up	Cold	n/a	n/a	Cold	n/a	n/a
Shutdown duration [h]	72	72	72	96	96	96
Temporary Full Load duration [h]	n/a	n/a	24	n/a	n/a	24
Time frame [h]	120	120	120	120	120	210
Technical data						
Input coal [MWh _{th}]	35,198.55	95,732.66	111,259.72	1939.28	80,231.25	95,758.31
Electricity produced (total) [MWh _e]	13,822.50	32,595.00	40,685.00	736.25	24,555.00	32,595.00
Electricity production increment with respect to conventional shutdown [MWh _e]	n/a	18,772.50	26,862.50	n/a	23,818.75	31,858.75
Electricity directed to PtG [MWh _e]	n/a	3600	2400	n/a	4800	3600
Stored energy (H ₂) [MWh]	n/a	2700	1800	n/a	3600	2700
CO ₂ emissions [t]	11,616	31,592	36,716	640	26,476	31,600
Economic data						
Costs [€]	944,059	2,101,932	2,280,242	573,066	1,923,877	2,102,188
Start-up cost [€]	140,000	n/a	n/a	140,000	n/a	n/a
Total costs [€]	1,084,059	2,101,932	2,280,242	713,066	1,923,877	2,102,188
Cost increment with respect to conventional shutdown [€]	n/a	1,017,873	1,196,183	n/a	1,210,811	1,389,122
Incomes electricity [€]	829,350	1,955,700	2,441,100	44,175	1,473,300	1,955,700
Incomes H ₂ [€]	n/a	81,000	54,000	n/a	108,000	81,000
Total Incomes [€]	829,350	2,036,700	2,495,100	44,175	1,581,300	2,036,700
Profit [€]	- 254,709	- 65,232	214,858	- 668,891	- 342,577	- 65,488
Differential profit [€/24h]	n/a	189,477	469,567	n/a	326,314	603,403
Differential hourly profit [€/h]	n/a	1579	3913	n/a	2719	5028
Specific cost of electricity [€/MWh _e]	68.30	64.49	56.05	778.36	78.35	64.49
Specific cost of additional electricity [€/MWh]	n/a	54.22	44.53	n/a	50.83	43.60

up cost only influence in the reference case. The influence in the total cost is larger than this 10% and increases up to 15%. In any case, the net profit remains in similar values to the base case. In the rest of the cases, similar trends are observed.

The final economic profit depends more on each specific case shorter or larger stops and/or days to consider in calculations (24 h or 120 h) than in variation of the main economic assumptions. The most attractive scenario would be a case with low coal costs as the profit, in the cases which make use of PtG, is larger than in reference case. Since the coal PP does not stop, continue in operation and coal is used in these hours.

For sake of clarity, data from the sensitivity analysis are illustrated in Fig. 6 for those cases with a reference frame time of 24 h (hot start-ups) and those cases with a reference frame time of 120 h (cold start-ups). The three variables that have been modified are the investment cost of the PtG facility, the cost of the fuel and the cost of shutting down the power plant. Their variation is represented in X-axis while the variation of profit under the different studied scenarios is represented in the Y-axis. The slope of the represented lines indicates the significance of each economic parameter. At the light of Fig. 5, the cost of fuel appears to be the most relevant economic parameter under all of the studied scenarios.

Table 6 — Sensitivity analysis under the Scenario 1 and 3 assumptions. Economical results with variations of the PtG CAPEX, coal cost and shut-down and start-up costs. Bold represents the key variables of the system.

		REFERENCE 24 h				REFERENCE 120 l	1
	REF	REF	PtG	PtG	REF	PtG	PtG load
	Hot 6 h.	Hot 12 h.	Hot 6 h.	Hot 12 h.	Cold 72 h.	Cold 72 h.	Cold 72 h.
PROFIT. Base case	-48,786	-138,758	76,075	6738	-254,709	-65,232	214,858
+20% cost PtG	-48,786	-138,758	73,688	4351	-254,709	− 77,166	202,924
-20% cost PtG	-48,786	-138,758	78,462	9125	-254,709	-53,297	226,792
+10% cost coal	-66,431	-149,260	51,999	-13,462	-289,908	-160,964	103,598
-10% cost coal	-31,141	-128,255	100,151	26,939	-219,510	30,501	326,118
+10% cost stops	-56,286	-146,258	76,075	6738	-256,109	-65,232	214,858
-10% cost stops	-41,286	-131,258	76,075	6738	-253,309	-65,232	214,858

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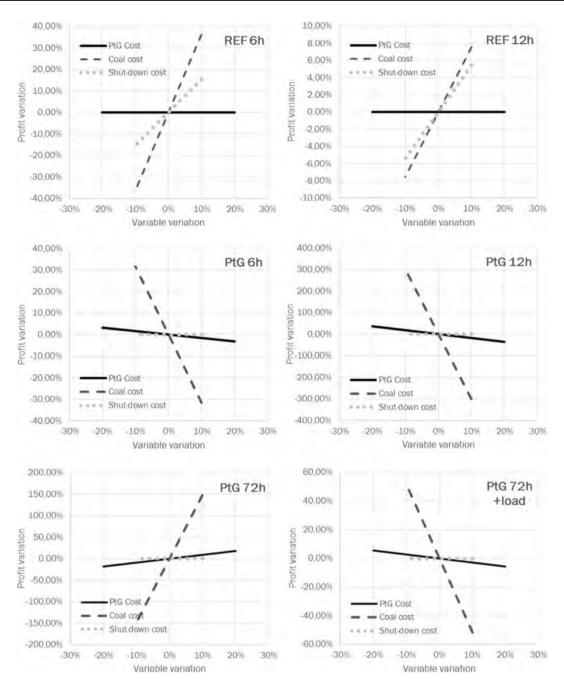


Fig. 6 - Sensitivity analysis of most significant economic variables.

Conclusions

The increase of the renewable share in the energy generation mix affects the operational predictability and flexibility of the grid operator. This situation compels coal-fired power plants to improve their operational flexibility and face frequent shutdowns, increasing the generation cost.

An option to deal with this problem is to integrate energy storage systems in power plants to instantaneously respond to load changes, virtually reduce their minimum complaint load and avoid shutdowns caused by an increase of renewable share in the electrical grid. In this work, we have studied their coupling with Power to Hydrogen energy

storage for this purpose. Instead of shutting down the power plant, part of the power produced is diverted to an electrolyser that virtually allows to the power below the minimum complaint load and maintain the power plant in operation.

The paper presents the comparison of (i) conventional shutdowns, (ii) continuous operation at minimum complaint load thanks to the utilisation of Power to Gas, and (iii) operation at MCL through PtG with a temporary increment to full load during the outage, required by the grid operator. Three scenarios are established for the analysis, corresponding to hot-, warm- and cold start-ups. The assessments are performed within the time frames of 24 h, 72 h and 120 h duration, respectively.

In Scenario 1, the utilisation of PtG to virtually reduce the MCL allows diminishing the specific cost of producing electricity a 21.8%—34.7%, compared to the cost related to shutdowns of 6—12 h duration. Thus, positive profit is obtained instead of economic losses. The main contribution to this profitable situation is saving the costs of the shutdown rather than the incomes from the sale of the hydrogen.

In Scenario 2, the utilisation of Power to Gas reduces the specific cost of producing electricity to 54.2-68.7 €/MWh_e, for shutdowns of 24-48 h that are framed in a total period of 72 h duration. Hence, PtG utilisation is not enough to reduce the cost of generating electricity below the selling price (60 €/MWh_e) at long shutdowns. To convert the situation into a profitable scenario, it must be assumed that the grid operator requires a temporary load increment to 100% while the power plant is dispatching electricity at MCL. If the duration of this requirement is 12 h (out of the 72 h of the time frame), the specific cost of electricity does fall below the selling price, to the range of 49.9-60.1 €/MWh_e.

In Scenario 3, profitable scenarios are even more restricted. Costs of electricity generation below the selling price are only achieve for relatively short periods of outage and mandatory load increments from the grid operator. Therefore, avoiding losses as much as possible is the main objective in this Scenario.

Sensitivity analysis shows that the most relevant variables in economy do not essentially change the conclusions drawn. Coal price is the most important variable in the economic calculations. A reduction in coal price increases the profit of the proposed concept as maintain in operation the coal PP at low load and avoid the shut-down costs.

In summary, it has been shown that Power to Gas may convert scenarios with economic losses into profitable situations through the avoidance of shutdown costs. Besides, even when scenarios cannot be reverted to profitable situations, the economic losses are highly reduced. Also, it is worth to mention that in some cases, even if the cost of producing electricity is not reduced below the selling price, the incomes from the sale of the hydrogen may cover the difference and help achieving profitable scenarios.

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Nomenclature

FFPP Fossil fuel power plants FSNL Full speed no load

FL Full load

MCL Minimum complaint load

NSNL No speed no load

O&M Operation and Maintenance

PtG Power to Gas REF Reference case

REFERENCES

- [1] Mikulčić H, Ridjan Skov I, Dominković DF, Wan Alwi SR, Manan ZA, Tan R, Duić N, Hidayah Mohamad SN, Wang X. Flexible Carbon Capture and Utilization technologies in future energy systems and the utilization pathways of captured CO₂. Renew Sustain Energy Rev 2019;114. https:// doi.org/10.1016/j.rser.2019.109338.
- [2] United nations framework convention on climate change. Paris Agreement; 2015.
- [3] European Commission. Directive (EU) 2018/2001 of the European Parliament and of the Council of 11 December 2018 on the promotion of the use of energy from renewable sources. 2018.
- [4] IEA. Renewables 2017. Paris. 2017.
- [5] Nadeem F, Hussain SMS, Tiwari PK, Goswami AK, Ustun TS. Comparative review of energy storage systems, their roles, and impacts on future power systems. IEEE Access 2019;7:4555–85. https://doi.org/10.1109/ ACCESS.2018.2888497.
- [6] Martín M, Grossmann IE. Optimal integration of renewable based processes for fuels and power production: Spain case study. Appl Energy 2018;213:595–610. https://doi.org/10.1016/ j.apenergy.2017.10.121.
- [7] Eser P, Singh A, Chokani N, Abhari RS. Effect of increased renewables generation on operation of thermal power plants. Appl Energy 2016;164:723–32. https://doi.org/10.1016/ j.apenergy.2015.12.017.
- [8] Benato A, Bracco S, Stoppato A, Mirandola A. LTE: a procedure to predict power plants dynamic behaviour and components lifetime reduction during transient operation. Appl Energy 2016;162:880–91. https://doi.org/10.1016/ j.apenergy.2015.10.162.
- [9] Mertens N, Alobaid F, Starkloff R, Epple B, Kim HG. Comparative investigation of drum-type and once-through heat recovery steam generator during start-up. Appl Energy 2015;144:250–60. https://doi.org/10.1016/j.apenergy.2015.01.065.
- [10] Zhao Y, Fan P, Wang C, Liu M, Chong D, Yan J. Fatigue lifetime assessment on a high-pressure heater in supercritical coal-fired power plants during transient processes of operational flexibility regulation. Appl Therm Eng 2019;156:196–208. https://doi.org/10.1016/ j.applthermaleng.2019.04.066.
- [11] Dong Y, Jiang X, Liang Z, Yuan J. Coal power flexibility, energy efficiency and pollutant emissions implications in China: a plant-level analysis based on case units. Resour Conserv Recycl 2018;134:184–95. https://doi.org/10.1016/ J.RESCONREC.2018.03.012.
- [12] Lew D, Brinkman G, Kumar N, Lefton S, Jordan G, Venkataraman S. Finding flexibility. Cycling the conventional fleet. IEEE Power Energy Mag 2013:20—32. https://doi.org/10.1109/MPE.2013.2277988.
- [13] de Groot M, Crijns-Graus W, Harmsen R. The effects of variable renewable electricity on energy efficiency and full load hours of fossil-fired power plants in the European Union. Energy 2017;138:575–89. https://doi.org/10.1016/ J.ENERGY.2017.07.085.
- [14] Schill W-P, Zerrahn A. Long-run power storage requirements for high shares of renewables: results and sensitivities.

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- Renew Sustain Energy Rev 2018;83:156-71. https://doi.org/10.1016/j.rser.2017.05.205.
- [15] Brouwer AS, Van Den Broek M, Seebregts A, Faaij A. Operational flexibility and economics of power plants in future low-carbon power systems. Appl Energy 2015;156:107–28. https://doi.org/10.1016/ j.apenergy.2015.06.065.
- [16] Hentschel J, Babić U, Spliethoff H. A parametric approach for the valuation of power plant flexibility options. Energy Rep 2016;2:40–7. https://doi.org/10.1016/j.egyr.2016.03.002.
- [17] Romeo LM, Peña B, Bailera M, Lisbona P. Analysis of the influence of Power-to-Gas systems in cyclic performance of fossil fuel power plants. In: ECOS 2018 - proc. 31st int. Conf. Effic. Cost, optim. Simul. Environ. Impact energy syst.; 2018.
- [18] Yin S, Zhang S, Andrews-Speed P, Li W. Economic and environmental effects of peak regulation using coal-fired power for the priority dispatch of wind power in China. J Clean Product 2017;162:361–70. https://doi.org/10.1016/ j.jclepro.2017.06.046.
- [19] Garðarsdóttir S, Göransson L, Normann F, Johnsson F. Improving the flexibility of coal-fired power generators: impact on the composition of a cost-optimal electricity system. Appl Energy 2018;209:277–89. https://doi.org/ 10.1016/j.apenergy.2017.10.085.
- [20] Forman C, Gootz M, Wolfersdorf C, Meyer B. Coupling power generation with syngas-based chemical synthesis. Appl Energy 2017;198:180–91. https://doi.org/10.1016/ j.apenergy.2017.04.053.
- [21] Dincer I, Acar C. Smart energy solutions with hydrogen options. Int J Hydrogen Energy 2018;43:8579–99. https:// doi.org/10.1016/j.ijhydene.2018.03.120.
- [22] Maggio G, Nicita A, Squadrito G. How the hydrogen production from RES could change energy and fuel markets: a review of recent literature. Int J Hydrogen Energy 2019;44:11371-84. https://doi.org/10.1016/ j.ijhydene.2019.03.121.
- [23] Moriarty P, Honnery D. Prospects for hydrogen as a transport fuel. Int J Hydrogen Energy 2019;44:16029–37. https://doi.org/ 10.1016/i.jihydene.2019.04.278.
- [24] Vandewalle J, Bruninx K, D'haeseleer W. Effects of large-scale power to gas conversion on the power, gas and carbon sectors and their interactions. Energy Convers Manag 2015;94:28–39. https://doi.org/10.1016/j.enconman.2015.01.038.
- [25] Bailera M, Lisbona P, Romeo LM, Espatolero S. Power to Gas projects review: lab, pilot and demo plants for storing renewable energy and CO₂. Renew Sustain Energy Rev 2017;69. https://doi.org/10.1016/j.rser.2016.11.130.
- [26] Bailera M, Kezibri N, Romeo LM, Espatolero S, Lisbona P, Bouallou C. Future applications of hydrogen production and CO2 utilization for energy storage: hybrid Power to Gas-Oxycombustion power plants. Int J Hydrogen Energy 2017;42. https://doi.org/10.1016/j.ijhydene.2017.02.123.
- [27] Bailera M, Lisbona P, Romeo LM. Avoidance of partial load operation at coal-fired power plants by storing nuclear power through power to gas. Int J Hydrogen Energy

- 2019;44:26063-75. https://doi.org/10.1016/j.ijhydene.2019.08.033.
- [28] Matute G, Yusta JM, Correas LC. Techno-economic modelling of water electrolysers in the range of several MW to provide grid services while generating hydrogen for different applications: a case study in Spain applied to mobility with FCEVs. Int J Hydrogen Energy 2019;44:17431–42. https:// doi.org/10.1016/j.ijhydene.2019.05.092.
- [29] Gonzalez-Salazar MA, Kirsten T, Prchlik L. Review of the operational flexibility and emissions of gas- and coal-fired power plants in a future with growing renewables. Renew Sustain Energy Rev 2018;82:1497—513. https://doi.org/ 10.1016/j.rser.2017.05.278.
- [30] Belošević S, Tomanović I, Crnomarković N, Milićević A, Tucaković D. Numerical study of pulverized coal-fired utility boiler over a wide range of operating conditions for in-furnace SO2/NOxreduction. Appl Therm Eng 2016;94:657–69. https://doi.org/10.1016/ j.applthermaleng.2015.10.162.
- [31] Lenton R, Choudhuri G. Fuel and technology cost review final report. Australian Energy Market Operator; 2014.
- [32] Proost J. State-of-the art CAPEX data for water electrolysers, and their impact on renewable hydrogen price settings. Int J Hydrogen Energy 2019;44:4406–13. https://doi.org/10.1016/ j.ijhydene.2018.07.164.
- [33] ACIL Tasman. Fuel resource, new entry and generation costs in the NEM final Report. 2009.
- [34] Nalbandian-Sugden H. Operating ratio and cost of coal power generation. IEA Clean Coal Centre; 2016. https:// doi.org/978-92-9029-595-2.
- [35] Kumar N, Besuner P, Lefton S, Agan D, Hilleman D. Power plant cycling costs. National Renewable Energy Laboratory; 2012.
- [36] Parra D, Valverde L, Pino FJ, Patel MK. A review on the role, cost and value of hydrogen energy systems for deep decarbonisation. Renew Sustain Energy Rev 2019;101:279–94. https://doi.org/10.1016/j.rser.2018.11.010.
- [37] BP Statistical Review of World Energy. BP. 2019. https://www. bp.com/content/dam/bp/business-sites/en/global/corporate/ pdfs/energy-economics/statistical-review/bp-stats-review-2019-full-report.pdf.
- [38] Eurostat., EU. Eurostat. Statistics explained. 2019.
- [39] Strbac G, Shakoor A, Black M, Pudjianto D, Bopp T. Impact of wind generation on the operation and development of the UK electricity systems, Electr. Power Syst Res 2007;77:1214-27. https://doi.org/10.1016/j.epsr.2006.08.014.
- [40] Guilera J, Ramon Morante J, Andreu T. Economic viability of SNG production from power and CO₂. Energy Convers Manag 2018;162:218–24. https://doi.org/10.1016/ j.enconman.2018.02.037.
- [41] Miao B, Chan SH. The economic feasibility study of a 100-MW Power-to-Gas plant. Int J Hydrogen Energy 2019;44:20978–86. https://doi.org/10.1016/j.ijhydene.2019.02.044.
- [42] Parra D, Patel MK. Techno-economic implications of the electrolyser technology and size for power-to-gas systems. Int J Hydrogen Energy 2016;41:3748–61. https://doi.org/ 10.1016/j.ijhydene.2015.12.160.