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25 studies. The application of SEM, XRPD and DSC evidenced drug physical transformation  
26 from crystalline to amorphous state and therefore, the achievement of an amorphous solid  
27 dispersion. The introduction of a novel technique,  $\mu$ -CT, to characterise the internal structure  
28 of these materials revealed key information regarding materials distribution and void content.  
29 Dissolution profile studies evidenced a high increase in drug release profile compared to pure  
30 ABZ. These promising results can lead to a great enhancement of the oral bioavailability of  
31 ABZ dosage forms. Therefore, HME is a potential continuous manufacturing technique to  
32 overcome ABZ poor solubility properties and lead to a significant increase in the therapeutic  
33 effect.

34 **Keywords:** Hot-melt extrusion; Amorphous solid dispersions; Albendazole; Continuous  
35 manufacturing;  $\mu$ -CT.

## 36 **1. Introduction**

37 A major focus of current pharmaceutical industry research is directed at the need to  
38 manufacture and deliver better quality medicines in a cost efficient manner (Madan and  
39 Madan, 2012). However, the physicochemical properties of Active Pharmaceutical  
40 Ingredients (APIs) are not always ideal and properties such as poor aqueous solubility, which  
41 influences dissolution and oral bioavailability, can be detrimental during pharmaceutical  
42 development (Munos, 2009; Kawakami, 2012). APIs that exhibit low solubility properties but  
43 high permeability through biological membranes are considered Class II compounds within  
44 the Biopharmaceutics Classification System (BCS) (Lindenberg et al., 2004) and in order to  
45 overcome poor solubility properties several formulation techniques can be considered. Some  
46 of the most common approaches are the introduction of chemical transformations such as the  
47 production of salt or co-crystal forms and other process modifications for example drug

48 micronisation or the production of amorphous solid dispersions (Stegemann et al., 2007;  
49 Kawabata et al., 2011; Jones et al., 2014).

50 It has been recognised that a change in the API's molecular physical state from a crystalline  
51 ordered structure to an amorphous state dramatically enhances its solubility and dissolution  
52 properties (Zhang et al., 2004). This physical transformation of the drug can be achieved by  
53 Hot-Melt Extrusion (HME) in order to deliver an amorphous solid dispersion with increased  
54 dissolution properties, which is controlled by the polymeric carrier excipient combination  
55 employed.

56 HME is a widely known manufacturing process that has been used in the plastic (Michaeli et  
57 al., 1993) and food industries (Cheng and Friis, 2010) and more recently, in the  
58 pharmaceutical industry (Crowley et al., 2007). In HME, a hydrophilic polymeric carrier and  
59 a poor water soluble drug are homogeneously mixed to form a molecular solid dispersion  
60 (Repka et al., 2007). HME can be achieved using a single or twin-screw extruder, both types  
61 have been widely studied and the advantages and disadvantages regarding the material  
62 mixing achieved reviewed (Van zuilichem et al., 1999). Selection of the components must be  
63 carefully performed taking into account the melt temperature ( $T_m$ ) of both the polymer and  
64 the API as well as the glass transition temperature ( $T_g$ ) of the polymer. These parameters  
65 play a key role in obtaining an amorphous solid dispersion as well as being key determinants  
66 of product stability (Newman et al., 2012). Initial assessment of the solubility properties can  
67 be performed by evaluating drug-polymer miscibility properties or also by using a  
68 mathematical approach such as the Hoy and Hoftzyer/Van Krevelen method (Forster et al.,  
69 2001). After production, characterisation techniques such as X-Ray Powder Diffraction  
70 (XRPD) and thermal analysis by Differential Scanning Calorimetry (DSC) constitute  
71 important techniques for the assessment of drug solid state (Maniruzzaman et al., 2013).  
72 Previous HME applications have focused on the development of new drug delivery systems

73 such as sustained released or taste-masking formulations (Maniruzzaman et al., 2012; Gue et  
74 al., 2013; Schilling and McGinity, 2010; Verhoeven et al., 2009b). By applying modelling  
75 techniques such as Computational Fluid Dynamics (CFD), Eitzlmayr et al., (2014),  
76 demonstrated that HME processes can be fully designed and noted the importance of  
77 selecting adequate screw elements configuration as this has an impact on the screws filling  
78 degree and therefore the heat transfer mechanisms within the extruder. Moreover, processing  
79 parameters such as melt temperature can be calculated taking into account the polymer's and  
80 API's viscosity values. Finally Quality by Design (QbD) has emerged as a potent tool to  
81 investigate the working space limits of HME processes based on the desired product  
82 specifications (Thiry et al., 2015; Maughan and Rhamzan, 2012).

83 The main aim of this research comprised the development and characterisation of novel  
84 albendazole (ABZ) formulations manufactured by continuous HME processing to improve  
85 ABZ dissolution properties and determine the influence of different drug contents in relation  
86 to material properties such as drug content uniformity, materials homogeneity and internal  
87 porosity by the application of a novel technique such as micro computed tomography ( $\mu$ -CT).  
88 ABZ is an anthelmintic drug used in the treatment of hydatid disease, among other parasitic  
89 worm infestations. Reported physicochemical properties of ABZ such as a low aqueous  
90 solubility of 0.0228 mg/mL and a melting temperature ( $T_m$ ) of 208°C were crucial to  
91 determine the suitability of this drug molecule for HME processing. APIs with a high melting  
92 point are preferred to avoid any degradation product as it has been previously observed using  
93 temperature sensitive drugs. It is also widely known that the low solubility and dissolution  
94 rate of ABZ lead to erratic absorption (below 5%) from the gastrointestinal tract mainly  
95 observed through pharmacokinetic studies (Marriner et al., 1986; Jung et al., 1998).  
96 Moreover, Newman et al., (2012), classified ABZ as one of the BCS II compounds where a

97 solid phase transformation using a hydrophilic polymer such as PVP could become a suitable  
98 approach towards the enhancement of its oral bioavailability.

99 Previous work comprising solid dispersions of ABZ and PVP K12 manufactured by solvent  
100 evaporation method was carried out by Torrado et al., (1996) in order to improve ABZ  
101 dissolution rate. In our study we were able to successfully produce stable amorphous solid  
102 dispersions of ABZ by HME process with increased dissolution properties and provide novel  
103 characterisation studies by the application of  $\mu$ -CT.

## 104 **2. Materials and methods**

### 105 2.1. Materials

106 Albendazole (ABZ,  $\geq 98\%$ ) was purchased from Sigma-Aldrich Company Ltd. (Gillingham,  
107 Dorset, United Kingdom). Pharmaceutical grade polyvinylpyrrolidone K12 (PVP K12 PF),  
108 was kindly donated by BASF (Cheshire, United Kingdom). Other reagents such as methanol  
109 (HPLC grade,  $\geq 99.5\%$ ), potassium chloride AR grade, sodium dihydrogen phosphate ( $>99.0$   
110  $\%$ ) and glacial acetic acid (ACS reagent,  $\geq 99.7\%$ ) were obtained from Sigma-Aldrich.

### 111 2.2. Miscibility studies

112 Miscibility properties of ABZ and PVP K12 were theoretically assessed using the Hansen  
113 solubility parameter calculations and confirmed by hot-stage microscopy (HSM) using a  
114 Reichert-Jung polyvar optical microscope fitted with a hot-stage. Raw materials, physical  
115 mixtures (PM) at 1/99, 5/95 and 10/90 % w/w and extruded materials were studied using a  
116 heating rate of 10 °C/min.

### 117 2.3. Continuous manufacturing by Hot-Melt Extrusion (HME)

118 Formulations of ABZ and PVP K12 comprising 1/99, 5/95 and 10/90 (% w/w) (F1, F2 and  
119 F3, total sample weight of 50 g) were prepared (Jones et al., 2014; Kelly et al., 2015).  
120 Previous sieving of PVP K12 through a mesh of 250  $\mu\text{m}$  was carried out for particle size

121 homogenisation purposes. Physical mixtures of ABZ – PVP K12 were manually blended for  
122 2-5 minutes prior extrusion. All formulations were processed by HME using a Thermo  
123 Scientific® Process 11 co-rotating twin-screw extruder (40L/D) (Karlsruhe, Germany) with  
124 the following standard screw configuration: (FS 11/40) x 7 + (KE 10/90°) x 8 + (KE 10/60°)  
125 x 4(F) + (FS 11/40) x 8 + (KE 10/60°) x 6(F) + (FS 11/40) x 7 + (KE 10/90°) x 4 + (KE  
126 10/60°) x 3(F) + (KE 10/30°) x 5(F) + (FS 11/40) x 9; (FS 11/40: feed screw with a pitch of  
127 11 mm and length of 40 mm; KE 10/90°: kneading element with thickness of 10 mm and 90°  
128 offset angle; KE 10/60°: kneading element with thickness of 10 mm and 60° offset angle; KE  
129 10/30°: kneading element with thickness of 10 mm and 30° offset angle; F: forward). The 11  
130 mm screw diameter extruder was fitted with a single orifice die of 2.0 mm diameter and  
131 processing parameters are presented in Table 1. Cooling of the strands was performed at  
132 room temperature and then stored in a sealed glass container under temperature controlled  
133 conditions of 25 °C and 50 °C. Initial studies of all extruded materials were performed at zero  
134 time and stability studies performed after 1, 3 and 6 months storage under conditions  
135 indicated in the text.

#### 136 2.4. Scanning Electron Microscopy (SEM)

137 HME formulations containing ABZ – PVP K12 were analysed by SEM for the presence of  
138 crystalline ABZ. Gold-coated samples of the extruded materials were mounted on the sample  
139 holder using silver paint and uncoated samples of pure ABZ and physical mixtures ABZ –  
140 PVP K12 were mounted using double-sided conductive tape. Measurements were performed  
141 using a Hitachi SU 6600 high-resolution analytical FE-SEM (New York, United States) at  
142 5.00 and 20.00 kV and a Zeiss IS50 (Oberkochen, Germany) at 20.00 kV.

#### 143 2.5. Computed Tomography ( $\mu$ -CT)

144 Cross-sections of the extruded materials were analysed by CT x-rays scanning to assess the  
145 internal void content (porosity) at a microstructural level, as well as sample uniformity by the

146 characterisation of the average molecular densities. A Bruker high resolution X-ray Micro-  
147 CT SkyScan 1272 (Kontich, Belgium) with an X-ray source voltage of 50 kV was used. The  
148 system was equipped with an aluminium 0.25 mm filter and 11 Mp CCD detector. Sample  
149 preparation required the introduction of a piece of extruded material inside a drinking straw  
150 to avoid any interference due to sample movement during measurement. Extruded material of  
151 ABZ – PVP K12 at 1/99 (% w/w) was analysed using a rotation step of  $0.6^\circ$  and extruded  
152 materials at 5/95 and 10/90 (% w/w) a rotation step of  $0.10^\circ$  and exposure time of 300 ms.  
153 The scanned images were reconstructed using the NRecon software (version 1.6.9.18, Bruker  
154 Micro-CT, Kontich, Belgium). To visualise and analyse the data, CTAn software (version  
155 1.14.4.1, Bruker, Micro-CT, Kontich, Belgium) and CTVol software (version 2.2.3.0, Bruker  
156 Micro-CT, Kontich, Belgium) for surface rendering were used. A set of calculations within  
157 CTAn including image thresholding were applied to determine a region of interest (ROI)  
158 within the cross section of the extruded material and avoid any interference caused by the  
159 straw. Porosity calculations were performed considering the volume of internal closed pores  
160 which are completely surrounded by solid material.

## 161 2.6. X-Ray Powder Diffraction (XRPD)

162 All extruded materials were analysed by XRPD in order to determine the molecular  
163 transformation of the drug from crystalline to amorphous state. A Bruker AXS D8 advanced  
164 transmission diffractometer (Karlsruhe, Germany) with theta-theta geometry, primary  
165 monochromatic radiation ( $\text{Cu K}\alpha_1\lambda = 1.54056 \text{ \AA}$ ), a Braun 1D position sensitive detector  
166 (PSD) and an automated multi-position x-y sample stage were used. Raw materials and  
167 physical mixtures drug-polymer were also characterised, and their XRPD patterns compared  
168 with the extruded materials.

## 169 2.7. Differential Scanning Calorimetry (DSC)



170 Thermal analysis of the extruded materials, physical mixtures drug-polymer and raw  
171 materials was performed using a Mettler Toledo DSC 822° (Greifensee, Switzerland)  
172 differential scanning calorimeter. A standard In/Zn calibration was performed and an inert  
173 gas such as N<sub>2</sub> was used to purge throughout the equipment at 150 mL/min. Samples were  
174 ground using a mortar and pestle then introduced into 40 µl sealed aluminium crucibles with  
175 a pierced lid. All samples were heated from 25 to 250 °C, melting temperature (T<sub>m</sub>) of ABZ  
176 (208-210 °C), at a heating rate of 10 °C/min, data was evaluated using the Star<sup>®</sup> Evaluation  
177 Software and the T<sub>g</sub> events were characterised using the inflection method.

#### 178 2.8. Karl-Fischer studies for stability evaluation

179 A Mettler Toledo DL-39 Karl-Fischer instrument (Schwerzenbach, Switzerland) was used to  
180 assess the water content of the extruded materials after 1, 3 and 6 months storage. Previous  
181 sample preparation required grinding of the sample using a mortar and a pestle followed by  
182 dissolution of 10 mg of extruded material in 1 mL of methanol. Experiments were performed  
183 in chambers with controlled temperature and RH.

#### 184 2.9. Dissolution profile studies

185 Dissolution studies of the extruded materials and physical mixtures were carried out using a  
186 Sirius T3 measurement system (East Sussex, United Kingdom). Sample preparation required  
187 manual grinding using a mortar and a pestle to a fine powder. Particle size distributions of  
188 these materials were analysed (sample measurement time of 3 s) using a Malvern Mastersizer  
189 3000 (Worcestershire, United Kingdom) fitted with the Aero S dry dispersion unit, a micro  
190 tray and air pressure adjusted to 1 bar. Mean values (d<sub>10</sub>, d<sub>50</sub>, d<sub>90</sub>) obtained for PM of ABZ –  
191 PVP K12 at 1/99, 5/95 and 10/90 % w/w were 21.11, 61.09, 110.38 µm, 15.41, 50.48, 97.78  
192 µm and 10.55, 46.11, 90.46 µm, respectively. Moreover, mean values (d<sub>10</sub>, d<sub>50</sub>, d<sub>90</sub>) of  
193 extruded materials at 1/99, 5/95 and 10/90 % w/w were 33.93, 197.46, 463.48 µm, 18.01,  
194 123.54, 425.15 µm and 8.65, 88.90, 459.85 µm, respectively. Later sample preparation

195 included the formation of a 3 mm diameter single tablet by weighing between 7 to 12 mg of  
196 grinded material that was later considered for dosage adjustment of each formulation. Tablets  
197 were pressed using a custom made die and a Specac manual hydraulic press (Kent, United  
198 Kingdom) with a compaction pressure of 80 kN. A Sirius T3 measurement system was then  
199 used to obtain material dissolution profiles between pH values of 2 to 7. A stationary disk  
200 apparatus was used consisting of a tablet holder where die and tablet were inserted and  
201 analysed using 15 mL of acetate phosphate buffer dissolution media. The buffer media was  
202 used to simulate in-vitro gastrointestinal conditions by pH automatic adjustment from 2.0-3.7  
203 (time 0-30min), 3.7-5.2 (time 30-60min), 5.2-7.1 (time 60-90min), and 7.1 (time 90-130min)  
204 and tablet surface facing the media to facilitate tablet erosion. Physical mixtures as well as  
205 extruded materials produced were analysed under non-sink conditions by a titration method.  
206 Datapoints were collected every 30 seconds by an spectroscopic UV dip-probe at a  
207 wavelength of 250 nm and transformed using pKa values (4.08; 10.34) and Molar Extinction  
208 Coefficient (MEC) into dissolution profile curves representing drug release (%) over time.

### 209 **3. Results and discussion**

#### 210 3.1. Miscibility studies

211 The application of the Hoy and Hofzyer/Van Krevelen method through the Hansen solubility  
212 parameter calculation evidenced that ABZ and PVP K12 are highly miscible, with a solubility  
213 parameter difference ( $\Delta\delta$ ) of 5.70 MPa<sup>1/2</sup>. Individual solubility parameter values ( $\delta$ ) for ABZ  
214 and PVP K12 were previously calculated based on the contribution of dispersive forces ( $E_d$ ),  
215 polar interactions ( $E_p$ ) and hydrogen bonds ( $E_h$ ). Physical mixtures of ABZ and PVP K12  
216 were also characterised by Hot-Stage Microscopy (HSM) to assess the miscibility properties  
217 of the two components and also their suitability for HME processing. Figure 1, a-d illustrates  
218 pure ABZ sample and images e-g the results of the physical mixture of ABZ – PVP K12 at  
219 10/90 (% w/w) under different temperature conditions. Solid ABZ appears as dark crystals

220 using a 10x magnification lens, similar to the results observed by Moyano et al., (2014) using  
221 100x magnification. In their study, commercial ABZ melting event is characterised at an  
222 onset temperature of 186 °C and complete melting is observed at 216 °C. Similar results are  
223 shown in Figure 1, images a to d where commercial ABZ particles are stable at temperatures  
224 between 45 to 180 °C but complete melting event is shown at 210 °C. A physical mixture,  
225 ABZ – PVP K12 at 10/90 (% w/w), shows a characteristic birefringence property that allows  
226 the differentiation between amorphous polymer and ABZ crystals (Fig. 1, e to g). Initial  
227 stages of polymer melting can be observed at a temperature of 145 °C (Fig. 1f) similar to  
228 DSC thermal analysis behaviour observed by Baird and Taylor (2012) and at 180 °C, drug  
229 crystals dissolve within the polymer indicating the miscibility properties of the two materials  
230 (Fig. 1g). These results confirm the ability of ABZ and PVP K12 to form a miscible system  
231 when temperatures above the T<sub>g</sub> of the polymer are applied (T<sub>g</sub> of PVP K12 = 90 °C)  
232 (Reintjes, 2011).

### 233 3.2. Scanning Electron Microscopy (SEM)

234 All formulations processed by HME were characterised by SEM microscopy in order to  
235 assess the physical state of the drug within the polymeric matrix, and extruded materials  
236 appear to be homogeneous when compared to the physical mixtures (Figure 2, b to d). It was  
237 also observed that as the amount of drug increased the porosity within the samples also  
238 increased which suggests that there is a correlation between the PVP K12 polymer and the  
239 proportion of drug in the system with the relaxation properties exhibited by the extruded  
240 materials (Sarode and Kumbharkhane, 2012). Moreover, polymer surface analysis of  
241 extruded materials (Figure 2, e to g) suggests the presence of a laminated surface  
242 characteristic of all samples.

### 243 3.3. Computed Tomography (μ-CT)

244 Extruded materials were scanned using a  $\mu$ -CT instrument in order to show at a micro-  
245 molecular level the homogeneity properties and suitability of HME technique to obtain a high  
246 mixing degree product. Previous studies to assess drug content uniformity within HME  
247 systems incorporated a fluorescent dye (Park et al., 2013) however characterisation of  
248 materials internal structure by computed tomography (CT) has gained popularity as a useful  
249 tool to examine solid dosage forms such as tablets (Sinka et al., 2004) or granule  
250 intermediates (Crean et al., 2010) and more recently co-extruded materials (Vynckier et al.,  
251 2015). This technique offers the possibility to analyse the material's internal structure  
252 through X-rays scans and visualise density and porosity characteristics. Extruded materials  
253 comprising ABZ – PVP K12 at 1/99, 5/95 and 10/90 (% w/w) were analysed by  $\mu$ -CT (Fig. 3,  
254 a-c) and the cross-section visualised by density characterisation shows an increase in porosity  
255 as well as different density levels from low (red) to medium (green) and high (blue) density  
256 values that correspond to the densities of air, polymeric material such as PVP K12 and ABZ.  
257 The porosity as shown in Figure 3 could be explained by entrapped air or by electrostatic  
258 interactions that occurred between ABZ and PVP K12. Moreover, 3D analysis and  
259 differences in the morphometric parameters obtained for all extruded materials can be  
260 observed in Table 2. It is then evidenced that the degree of porosity is influenced by the drug  
261 content within the extruded material and this is the first report of non-homogeneity in  
262 extruded materials at a micro-structural level. This is similar to reported micro-structure  
263 variations for tablets (Sinka et al., 2004), granules (Crean et al., 2010) and calendered tablets  
264 (Vynckier et al., 2015) where it was observed the influence of pores formed during co-  
265 extrusion into tablet adhesion degree between core and coat. Such studies indicate that  
266 despite the known mixing ability of twin-screw processing (Crowley et al., 2007) standard  
267 techniques for assessing homogeneity may not be adequate.

268 3.4. X-Ray Powder Diffraction (XRPD)

269 The XRPD patterns of ABZ – PVP K12 extruded formulations, drug-polymer physical  
270 mixtures (PM) and pure drug was analysed in order to investigate if any re-crystallisation  
271 events registered over time (Figure 4). The XRPD pattern of ABZ shows intensity peaks at  $2\theta$   
272 angles of 6.91, 11.32, 13.83, 17.97, 19.51, 19.99, 20.75, 22.19, 23.85, 24.47, 24.72, 25.05,  
273 26.08, 26.23, 27.21, 28.73, 29.06, 30.00, 30.52 and  $31.05^\circ$  that correspond to ABZ crystalline  
274 form I (Pranzo et al., 2010). However, the intensity of the peak observed at  $25^\circ 2\theta$  is lower  
275 compared to the one observed by Pranzo et al., (2010). This may be due to specimen  
276 preparation errors in the commercial ABZ pattern reported by Pranzo et al., such as crystals  
277 non-random preferred orientation (Jenkins and Snyder, 1996).

278 The XRPD patterns of the physical drug-polymer mixtures (PM) and the extruded materials  
279 suggest the absence of a crystalline ordered structure of ABZ and the formation of an  
280 amorphous solid dispersion of the drug within the extruded polymer matrix. It can also be  
281 observed that by increasing ABZ content in the physical mixture (PM) samples, the height of  
282 the intensity peaks registered also increased (Fig. 4a). In contrast, the extruded materials do  
283 not show any intensity peaks relative to crystalline structures but a halo pattern characteristic  
284 of amorphous materials. By looking to the XRPD patterns obtained after 6 months storage of  
285 the extruded materials containing ABZ – PVP K12 at 10/90 (% w/w) (Fig. 4b), we can  
286 conclude that the materials are stable and there are no re-crystallisation events registered over  
287 time. Therefore, these results suggest that stable amorphous solid dispersions of ABZ in PVP  
288 K12 for all formulations were achieved.

### 289 3.5. Differential Scanning Calorimetry (DSC)

290 DSC analysis of the extruded materials, physical mixtures (PM) and raw materials was  
291 carried out to determine the formation of amorphous solid dispersions and also evaluate the  
292 presence of glass transition ( $T_g$ ) events (Fig. 5). Differences between the  $T_g$  values of the  
293 extruded ABZ formulations and physical mixtures (PM) drug-polymer (differences in scale to

294 be considered) indicated that a solid form transformation of the ABZ crystals occurred during  
295 HME and the extruded material thermograms do not show evidence of any endothermic event  
296 due to melting of crystalline material. Also, differences regarding T<sub>g</sub> appearance is observed  
297 and is normally considered a middle value comprised by the T<sub>g</sub> values of the raw materials  
298 involved (Maru et al., 2011; Baird and Taylor, 2012). Figure 6 shows the DSC thermograms  
299 of all extruded materials after 6 months storage. The presence of two T<sub>g</sub> events for the 1/99%  
300 (w/w) at 25 °C, 5/95% (w/w) at 25 °C, 10/90% (w/w) at 50 °C curves suggests that the  
301 material could have evolved to a solid glassy suspension. However, there is no evidence of  
302 recrystallisation events, conclude that extruded materials are stable over time. Moreover, the  
303 1/99% (w/w) at 50 °C and 5/95% (w/w) at 50 °C appear to have one T<sub>g</sub> event (solid  
304 dispersion), and the 10/90% (w/w) at 25 °C shows an amorphous curve without any T<sub>g</sub>  
305 events due to the heating rate.

### 306 3.6. Karl-Fischer studies for stability evaluation

307 All the raw materials and extruded samples were analysed by Karl-Fischer titration to  
308 determine the water content, since the well-known hygroscopicity of some pharmaceutical  
309 grade polymers such as polyvinylpyrrolidone (PVP) can be a limitation due to its influence  
310 on the stability of amorphous solid dispersions (Bianco et al., 2013). Low water content  
311 values of dosage forms containing hygroscopic polymeric materials such as PVP constitute a  
312 crucial parameter to be evaluated as there is evidence indicating that intramolecular bonds of  
313 polymeric materials and therefore the polymer free volume and other properties like plasticity  
314 or elasticity can be affected by increases in water content (Szakonyi and Zelko, 2012). The  
315 water content within the samples is a quality attribute to ensure product stability and to  
316 preserve the product from degradation phenomena, often known as drug-polymer phase  
317 separation events (Rumondor and Taylor, 2009). Table 3 presents the water content (%) of  
318 the raw materials and the ABZ – PVP K12 formulation at 10/90 (% w/w) observed at zero

319 and 6 months after storage. As depicted in Table 3, stored samples did not show water  
320 content increase higher than 0.2 % despite the high hygroscopicity properties of PVP. Non-  
321 parametric ANOVA (Kruskal-Wallis) test was also performed indicating that temperature  
322 changes do not have a significant influence in samples water content ( $P=0.288$  therefore  
323  $P>0.05$ ). Low water content values of 0.2 % are considered optimum for oral dosage forms in  
324 order to be stable and preserve their physicochemical properties. Solid dosage forms with  
325 water content values below 2 % are considered acceptable for a commercial pharmaceutical  
326 product although these values may differ depending on the type of product and specifications  
327 required.

### 328 3.7. Dissolution profile studies

329 Drug release of the extruded materials was characterised using a Sirius T3 measurement  
330 system under non-sink conditions and simulating gastrointestinal (GI) pH conditions. As can  
331 be observed in Figure 7, extruded materials (ABZ – PVP K12 ratios of 1/99 and 10/90 (%  
332 w/w)) increased release compared to the pure drug with values of 70 % drug release and  
333 extrapolated dissolution rates of  $45.09 \mu\text{g min}^{-1}$  and  $148.80 \mu\text{g min}^{-1}$ , respectively. Slightly  
334 lower values of 50 % drug release and extrapolated dissolution rate value of  $171 \mu\text{g min}^{-1}$   
335 were achieved by the extruded material containing 5/95 (% w/w). Similar results related to  
336 solid dispersions of a BCS Class II drug such as ABZ into a PVP matrix that showed such an  
337 increase in drug dissolution rate and a similar dissolution profile were observed by Frizon et  
338 al., (2013). Dissolution profiles of the extruded materials of ABZ – PVP K12 at 1/99 and  
339 5/95 % (w/w) did not achieve supersaturation (ABZ solubility below  $22.8 \mu\text{g/ml}$ ). However,  
340 supersaturation of the system was achieved by ABZ – PVP K12 formulation at 10/90 %  
341 (w/w) with a solubility value of  $30.33 \mu\text{g/ml}$ . It is of note in Figures 7 and 8 the increased and  
342 fast drug release profile (or also called “spring”) of the extruded materials that does not  
343 exhibit under the test conditions the characteristic “parachute” effect observed by Brouwers

344 et al., (2009). In our studies, an optimum drug release profile close to 100 % was not  
345 achieved and possible influence of the polymeric material PVP K12 needs to be further  
346 studied. Tablets did completely dissolved in the buffer media which suggests there is an  
347 effect of PVP that prevents the complete dissolution of ABZ leading to different proportions  
348 (%) of drug released over time, although this needs to be further studied. Moreover,  
349 dissolution studies of the extruded materials stored for 6 months at 25 °C and 50 °C revealed  
350 that the formulations were stable over time (Fig. 8). Extruded materials comprising 1/99 %  
351 (w/w) show a similar dissolution profile after 6 months storage in comparison to 5/95 % and  
352 10/90% w/w which show variations of approximately 10% drug release. Similar  
353 improvements towards ABZ dissolution rate were achieved by Torrado et al., (1996) that  
354 manufactured successful amorphous solid dispersions of ABZ in PVP K12 by the classic  
355 solvent evaporation method and also carried out bioavailability studies in animals. We  
356 demonstrate the suitability of a lab scale HME process to obtain stable amorphous solid  
357 dispersions of ABZ with enhanced dissolution properties that could lead to novel  
358 formulations with enhanced oral bioavailability.

#### 359 **4. Conclusions**

360 Amorphous solid dispersions of ABZ, an anthelmintic drug with poor water solubility  
361 properties, in PVP K12 matrix were produced by HME method. Evidence of solid form  
362 transformation of ABZ is proved by characterisation of the extruded materials using SEM,  
363 XRPD and DSC all of which indicate the formation of an amorphous drug polymer system.  
364 We also introduced a novel tool for the characterisation of HME materials, computed  
365 tomography ( $\mu$ -CT), which provided an insight into internal material properties such as  
366 porosity and materials distribution indicating that despite the previous physicochemical  
367 results the strands are not homogeneous. The potential impact on pharmaceutical properties  
368 will have to be further investigated and maybe mitigated if the strands were pelletised or



369 milled before further processing. Analysis of the samples after 6 months storage did not  
370 indicate any drug re-crystallisation events, which suggest that the samples were stable over  
371 time. Main factors involved are the use of a polymeric material with high Tg such as PVP  
372 K12 as well as the possibility of a complex formation between the drug and the polymer that  
373 will be further studied. High dissolution rate increase of ABZ in gastrointestinal simulated  
374 media was achieved with values of 70 % drug release for the extruded materials containing  
375 ABZ – PVP K12 at 1/99 and 10/90 (% w/w). Six months storage under temperature  
376 controlled conditions did not affect the dissolution profiles and Karl-Fischer results showed  
377 that samples were not affected by water intake. To conclude, HME can be applied as a  
378 continuous manufacturing technique of novel oral dosage forms comprising ABZ without the  
379 need of further processing techniques in order to improve its dissolution behaviour and  
380 possible enhancement of oral bioavailability.

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388 **References**

389 Baird, J.A., Taylor, L.S., 2012. Evaluation of amorphous solid dispersion properties using  
390 thermal analysis techniques. *Advanced drug delivery reviews* 64, 396-421.

391 Bianco, S., Tewes, F., Tajber, L., Caron, V., Corrigan, O.I., Healy, A.M., 2013. Bulk, surface  
392 properties and water uptake mechanisms of salt/acid amorphous composite systems.  
393 *International journal of pharmaceutics* 456, 143-152.

394 Brouwers, J., Brewster, M.E., Augustijns, P., 2009. Supersaturating drug delivery systems:  
395 the answer to solubility-limited oral bioavailability?. *Journal of pharmaceutical sciences* 98,  
396 2549-2572.

397 Cheng, H., Friis, A., 2010. Modelling extrudate expansion in a twin-screw food extrusion  
398 cooking process through dimensional analysis methodology. *Food and Bioproducts*  
399 *Processing* 88, 188-194.

400 Crean, B., Parker, A., Roux, D.L., Perkins, M., Luk, S.Y., Banks, S.R., Melia, C.D., Roberts,  
401 C.J., 2010. Elucidation of the internal physical and chemical microstructure of  
402 pharmaceutical granules using X-ray micro-computed tomography, Raman microscopy and  
403 infrared spectroscopy. *European journal of pharmaceutics and biopharmaceutics: official*  
404 *journal of Arbeitsgemeinschaft fur Pharmazeutische Verfahrenstechnik e.V* 76, 498-506.

405 Crowley, M.M., Zhang, F., Repka, M.A., Thumma, S., Upadhye, S.B., Battu, S.K., McGinity,  
406 J.W., Martin, C., 2007. Pharmaceutical applications of hot-melt extrusion: part I. *Drug*  
407 *development and industrial pharmacy* 33, 909-926.

408 Eitzlmayr, A., Koscher, G., Reynolds, G., Huang, Z., Booth, J., Shering, P., Khinast, J., 2014.  
409 Mechanistic modeling of modular co-rotating twin-screw extruders. *International journal of*  
410 *pharmaceutics* 474, 157-176.

- 411 Forster, A., Hempenstall, J., Tucker, I., Rades, T., 2001. Selection of excipients for melt  
412 extrusion with two poorly water-soluble drugs by solubility parameter calculation and  
413 thermal analysis. *International journal of pharmaceutics* 226, 147-161.
- 414 Frizon, F., Eloy, J.d.O., Donaduzzi, C.M., Mitsui, M.L., Marchetti, J.M., 2013. Dissolution  
415 rate enhancement of loratadine in polyvinylpyrrolidone K-30 solid dispersions by solvent  
416 methods. *Powder Technology* 235, 532-539.
- 417 Gue, E., Willart, J.F., Muschert, S., Danede, F., Delcourt, E., Descamps, M., Siepmann, J.,  
418 2013. Accelerated ketoprofen release from polymeric matrices: importance of the  
419 homogeneity/heterogeneity of excipient distribution. *International journal of pharmaceutics*  
420 457, 298-307.
- 421 Jenkins, R., Snyder, R.L., 1996. *Introduction to X-ray powder diffractometry*. New York  
422 Wiley.
- 423 Jones, D.S., Margetson, D.N., McAllister, M.S., Yu, T., Shu, L., McCoy, C.P., Andrews,  
424 G.P., 2014. Thermodynamically stable amorphous drug dispersions in amorphous hydrophilic  
425 polymers engineered by hot melt extrusion. *Chemical Engineering Research and Design* 92,  
426 3046-3054.
- 427 Jung, H., Medina, L., García, L., Fuentes, I., Moreno-Esparza, R., 1998. Biopharmaceutics:  
428 absorption studies of albendazole and some physicochemical properties of the drug and its  
429 metabolite albendazole sulphoxide. *Journal of pharmacy and pharmacology* 50, 43-48.
- 430 Kawabata, Y., Wada, K., Nakatani, M., Yamada, S., Onoue, S., 2011. Formulation design for  
431 poorly water-soluble drugs based on biopharmaceutics classification system: basic  
432 approaches and practical applications. *International journal of pharmaceutics* 420, 1-10.

- 433 Kawakami, K., 2012. Modification of physicochemical characteristics of active  
434 pharmaceutical ingredients and application of supersaturatable dosage forms for improving  
435 bioavailability of poorly absorbed drugs. *Advanced drug delivery reviews* 64, 480-495.
- 436 Kelly, A.L., Halsey, S.A., Bottom, R.A., Korde, S., Gough, T., Paradkar, A., 2015. A novel  
437 transfectance near infrared spectroscopy technique for monitoring hot melt extrusion.  
438 *International journal of pharmaceutics*.
- 439 Lindenberg, M., Kopp, S., Dressman, J.B., 2004. Classification of orally administered drugs  
440 on the World Health Organisation model list of essential medicines according to the  
441 Biopharmaceutics Classification System. *European journal of pharmaceutics and*  
442 *biopharmaceutics* 58, 265-278.
- 443 Madan, S., Madan, S., 2012. Hot melt extrusion and its pharmaceutical applications. *Asian*  
444 *Journal of Pharmaceutical Sciences* 7(2), 123-133.
- 445 Maniruzzaman, M., Boateng, J.S., Bonnefille, M., Aranyos, A., Mitchell, J.C., Douroumis,  
446 D., 2012. Taste masking of paracetamol by hot-melt extrusion: an in vitro and in vivo  
447 evaluation. *European journal of pharmaceutics and biopharmaceutics: official journal of*  
448 *Arbeitsgemeinschaft fur Pharmazeutische Verfahrenstechnik e.V* 80, 433-442.
- 449 Maniruzzaman, M., Morgan, D.J., Mendham, A.P., Pang, J., Snowden, M.J., Douroumis, D.,  
450 2013. Drug-polymer intermolecular interactions in hot-melt extruded solid dispersions.  
451 *International journal of pharmaceutics* 443, 199-208.
- 452 Marriner, S.E., Morris, D.L., Dickson, B., Bogan, J.A., 1986. Pharmacokinetics of  
453 Albendazole in man. *European Journal of Clinical Pharmacology* 30, 705-708.
- 454 Maru, S.M., de Matas, M., Kelly, A., Paradkar, A., 2011. Characterization of thermal and  
455 rheological properties of zidovudine, lamivudine and plasticizer blends with ethyl cellulose to  
456 assess their suitability for hot melt extrusion. *European journal of pharmaceutical sciences:*  
457 *official journal of the European Federation for Pharmaceutical Sciences* 44, 471-478.

- 458 Maughan, L., Rhamzan, A., 2012. The evolution of QbD – From inception to maturity in  
459 2012. Reg Rapporteur e.V 9, 9.
- 460 Michaeli, W., Frings, W., Höcker, H., Berghaus, U., 1993. Reactive Extrusion of Styrene  
461 Polymers. International Polymer Processing 8, 308-318.
- 462 Moyano, J.R., Liró, J., Pérez, J.I., Arias, M.J., Sánchez-Soto, P.J., 2014. Thermal analysis of  
463 Albendazole investigated by HSM, DSC and FTIR. Microscopy: advances in scientific  
464 research and education (A. Méndez-Vilas, Ed.), 1043-1050.
- 465 Munos, B., 2009. Lessons from 60 years of pharmaceutical innovation. Nature reviews. Drug  
466 discovery 8, 959-968.
- 467 Newman, A., Knipp, G., Zografí, G., 2012. Assessing the performance of amorphous solid  
468 dispersions. Journal of pharmaceutical sciences 101, 1355-1377.
- 469 Park, J.B., Kang, C.Y., Kang, W.S., Choi, H.G., Han, H.K., Lee, B.J., 2013. New  
470 investigation of distribution imaging and content uniformity of very low dose drugs using  
471 hot-melt extrusion method. International journal of pharmaceutics 458, 245-253.
- 472 Pranzo, M.B., Cruickshank, D., Coruzzi, M., Cairra, M.R., Bettini, R., 2010. Enantiotropically  
473 related albendazole polymorphs. Journal of pharmaceutical sciences 99, 3731-3742.
- 474 Reintjes, T., 2011. Solubility enhancement with BASF pharma polymers. Solubilizer  
475 Compendium.
- 476 Repka, M.A., Battu, S.K., Upadhye, S.B., Thumma, S., Crowley, M.M., Zhang, F., Martin,  
477 C., McGinity, J.W., 2007. Pharmaceutical applications of hot-melt extrusion: Part II. Drug  
478 development and industrial pharmacy 33, 1043-1057.
- 479 Rumondor, A.C.F., Taylor, L.S., 2009. Effect of Polymer Hygroscopicity on the Phase  
480 Behavior of Amorphous Solid Dispersions in the Presence of Moisture. Molecular  
481 Pharmaceutics 7, 477-490.

482 Sarode, A.V., Kumbharkhane, A.C., 2012. Dielectric relaxation and thermodynamic  
483 properties of polyvinylpyrrolidone using time domain reflectometry. *Polymer International*  
484 61, 609-615.

485 Schilling, S.U., McGinity, J.W., 2010. Novel application of hot-melt extrusion for the  
486 preparation of monolithic matrices containing enteric-coated particles. *International journal*  
487 *of pharmaceutics* 400, 24-31.

488 Sinka, I.C., Burch, S.F., Tweed, J.H., Cunningham, J.C., 2004. Measurement of density  
489 variations in tablets using X-ray computed tomography. *International journal of*  
490 *pharmaceutics* 271, 215-224.

491 Stegemann, S., Leveiller, F., Franchi, D., De Jong, H., Lindén, H., 2007. When poor  
492 solubility becomes an issue: From early stage to proof of concept. *European journal of*  
493 *pharmaceutical sciences* 31, 249-261.

494 Szakonyi, G., Zelko, R., 2012. The effect of water on the solid state characteristics of  
495 pharmaceutical excipients: Molecular mechanisms, measurement techniques, and quality  
496 aspects of final dosage form. *International journal of pharmaceutical investigation* 2, 18-25.

497 Thiry, J., Krier, F., Evrard, B., 2015. A review of pharmaceutical extrusion: Critical process  
498 parameters and scaling-up. *International journal of pharmaceutics* 479, 227-240.

499 Torrado, S., Torrado S., Torrado, J.J., Cadorniga, R., 1996. Preparation, dissolution and  
500 characterization of albendazole solid dispersions. *International journal of pharmaceutics* 140,  
501 247-250.

502 Van Zuilichem, D.J., Kuiper, E., Stolp, W., Jager, T., 1999. Mixing effects of constituting  
503 elements of mixing screws in single and twin screw extruders. *Powder Technology* 106, 147-  
504 159.

505 Verhoeven, E., Siepmann, F., De Beer, T.R., Van Loo, D., Van den Mooter, G., Remon, J.P.,  
506 Siepmann, J., Vervaet, C., 2009b. Modeling drug release from hot-melt extruded mini-  
507 matrices with constant and non-constant diffusivities. European journal of pharmaceutics and  
508 biopharmaceutics: official journal of Arbeitsgemeinschaft fur Pharmazeutische  
509 Verfahrenstechnik e.V 73, 292-301.

510 Vynckier, A.K., Lin, H., Zeitler, J.A., Willart, J.F., Bongaers, E., Voorspoels, J., Remon, J.P.,  
511 Vervaet, C., 2015. Calendring as a direct shaping tool for the continuous production of  
512 fixed-dose combination products via co-extrusion. European Journal of Pharmaceutics and  
513 Biopharmaceutics.

514 Zhang, G.G., Law, D., Schmitt, E.A., Qiu, Y., 2004. Phase transformation considerations  
515 during process development and manufacture of solid oral dosage forms. Advanced drug  
516 delivery reviews 56, 371-390.

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518

519 **Figure captions**

520 Figure 1: Hot-stage microscopy (HSM, 10x magnification) images a to d: pure ABZ at 80 °C,  
521 145 °C, 180 °C and 210 °C, images e to g: physical mixture (PM) ABZ – PVP K12 at 10/90  
522 (% w/w) at 80 °C, 145 °C and 180 °C.

523 Figure 2: SEM images of pure drug (a), physical mixtures ABZ – PVP K12 at 1/99, 5/95 and  
524 10/90 (% w/w) (b to d) and extruded materials of ABZ – PVP K12 formulation at 1/99, 5/95  
525 and 10/90 (% w/w) (e to g).

526 Figure 3: Micro-CT single scanned images of extruded materials of ABZ – PVP K12 at 1/99,  
527 5/95 and 10/90 % (w/w) (a, b and c).

528 Figure 4: Diffractograms of (a) ABZ – PVP K12 formulations at time zero and (b) ABZ –  
529 PVP K12 at a 10/90 (% w/w) ratio after 6 months storage.

530 Figure 5: DSC thermograms of a: pure ABZ, b to d: physical mixtures (PM) of ABZ – PVP  
531 K12 at 1/99 (% w/w), 5/95 (% w/w) and 10/90 (% w/w) and e to g: extruded materials of  
532 ABZ – PVP K12 at 1/99 (% w/w), 5/95 (% w/w) and 10/90 (% w/w).

533 Figure 6: DSC thermograms after 6 months storage where a: extruded material of ABZ –  
534 PVP K12 at 1/99 % (w/w) at 25 °C, b: extruded material of ABZ – PVP K12 at 1/99 % (w/w)  
535 at 50 °C, c: extruded material of ABZ – PVP K12 at 5/95 % (w/w) at 25 °C, d: extruded  
536 material of ABZ – PVP K12 at 5/95 % (w/w) at 50 °C, e: extruded material of ABZ – PVP  
537 K12 at 10/90 % (w/w) at 25 °C and f: extruded material of ABZ – PVP K12 at 10/90 %  
538 (w/w) at 50 °C.

539 Figure 7: Dissolution profiles simulating gastrointestinal conditions of a: pure ABZ, b to d:  
540 physical mixtures (PM) of ABZ – PVP K12 at 10/90 (% w/w), 5/95 (% w/w) and 1/99 (%



541 w/w) and e to g: extruded materials of ABZ – PVP K12 at 5/95 (% w/w), 1/99 (% w/w) and  
542 10/90 (% w/w). Standard error bars are based on 2 tests per sample.

543 Figure 8: Dissolution profiles simulating gastrointestinal conditions, upper left image  
544 (extruded material of ABZ – PVP K12 at 1/99% (w/w)): a: pure ABZ, b: extrudate at time  
545 zero, c: extrudate after 6 months storage at 50 °C, d: extrudate after 6 months storage at 25  
546 °C; Upper right image (extruded material of ABZ – PVP K12 at 5/95 % (w/w)): a: pure ABZ,  
547 b: extrudate after 6 months storage at 25 °C, c: extrudate after 6 months storage at 50 °C, d:  
548 extrudate at time zero; Lower image (extruded material of ABZ – PVP K12 at 10/90 %  
549 (w/w)): a: pure ABZ, b: extrudate after 6 months storage at 25 °C, c: extrudate at time zero,  
550 d: extrudate after 6 months storage at 50 °C.

551

Table 1. HME processing parameters of ABZ – PVP K12 formulations

HME formulation	Barrel Zones	Barrel temperatures (°C, zones 1, 2, 3 and 4-8)	Screw speed (rpm)	Torque (Nm)	Throughput (Kg/h)
F1	1 - 8	70, 120, 140, 145	100	1.2 - 3	0.1 - 0.15
F2	1 - 8	70, 120, 140, 145	100	1.2 - 3	0.15
F3	1 - 8	70, 120, 140, 145	100	1.2 - 2.7	0.1 - 0.15

**Description:**

Table 1 shows the HME processing parameters applied for the development of three formulations comprising Albendazole (ABZ) and PVP K12 such as barrel temperatures and screw speed. Further information such as the torque values registered and the total throughput are also given.

553 Table 2. Morphometric parameters of extruded materials obtained by  $\mu$ -CT 3D analysis

<b>HME formulation</b>	<b>Object volume (mm<sup>3</sup>)</b>	<b>Volume closed pores (mm<sup>3</sup>)</b>	<b>Closed porosity (%)</b>
F1	25.17	0.01	0.04
F2	26.17	0.65	2.43
F3	12.70	0.20	1.57

554

**Description:**

555 Table 2 above shows the  $\mu$ -CT 3D analysis of the extruded materials such as the object  
556 volume, defined as the total volume analysed based on the external dimensions of the strand  
557 (diameter approximately 2.0 mm) and the closed pores, defined as the space within the object  
558 volume, which is completely surrounded by solid material.

559

Table 3. Karl-Fischer results after storage

Materials	Storage conditions	Average water content (% w/w)
Extruded material ABZ – PVP K12 10/90 (% w/w) ratio	Time zero, room temperature	0.1591 ± 0.0084
	6 months at 25 °C, 20% RH	0.1445 ± 0.0387
	6 months at 50 °C, 3% RH	0.1796 ± 0.0037

**Description:**

Table 3 above shows the average water content values (% w/w) obtained by Karl-Fischer coulometric titration using methanol as dissolution media. Mean standard deviation (SD) values of 3 replicates calculated for each sample are depicted using ± symbol (Kruskal-Wallis test, P=0.288 therefore P>0.05).