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Noble gas as a proxy to understand the evolutionary path of migrated  $\text{CO}_2$  in a shallow aquifer system

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#### 15 Abstract

16 To provide confidence in the safety of a carbon capture and storage (CCS) project, researchers 17 have focused on developing monitoring techniques to trace the unlikely, but potentially possible, migration of  $CO_2$  from a deep reservoir. Among the various techniques, noble gas tracing is a beneficial 18 approach, owing to the unique noble gas fingerprints present in injection fluids, the deep reservoir, and 19 the shallow aquifer above the storage area. However, the value of this approach has been limited to 20 demonstrations in a natural analogue CO<sub>2</sub>-rich reservoir and an artificial injection test site. Therefore, 21 22 further efforts are required to link those valuable observations to an actual CCS site. In this study, we outline how to use these tracers for actual monitoring work in a shallow aquifer system. First, two 23 artificial injection tests were performed using He, Ar, Kr, and SF<sub>6</sub> to understand the behavior of the 24 25 leaked plume in the shallow aquifer system. In both tests, the noble gas ratio remarkably changed with the 26 solubility-controlled process and the mixing process. To extend and link the valuable findings from the 27 artificial injection tests to an actual  $CO_2$  leakage event, we performed a leakage simulation using data from a real CO<sub>2</sub> injection site, i.e., the Weyburn–Midale site. This simulation suggested that combinations 28 29 of <sup>4</sup>He with other heavier noble gases can be used to monitor  $CO_2$  leakage, as they allow us to separate 30 and explain the major interactions governing the migration of the leaked plume in the shallow aquifer 31 system. Additionally, although the high  $CO_2$  density of a dissolved plume is known to add uncertainty in quantitative approaches, the influence of those effects was negligible when compared to the errors arising 32 33 from the wide variation in the noble gas fingerprints in the leaked CO<sub>2</sub>. This study, therefore, provides insight into the evolutionary path of the migrated  $CO_2$  plume in the shallow aquifer system and to the 34 results can be used to inform the tracing of a leakage source within a shallow aquifer despite various 35 36 mechanisms complicating the plume distribution.

37 Keywords: Carbon capture and storage; CO<sub>2</sub> leakage; noble gas tracing; degassing; inherent tracer;
38 monitoring

#### 39 1 Introduction

A carbon capture and storage (CCS) project uses an impermeable or low-permeability cap rock to 40 trap sequestered  $CO_2$  in a formation without leakage. The  $CO_2$  injected into the storage formation is 41 sequestrated by subsurface trapping mechanisms, namely structural/stratigraphic trapping, residual 42 trapping, solubility trapping, and mineral trapping mechanisms. Evidence shows that these are effective 43 on a geologic time scale (Alcalde and Flude et al., 2018; Altman et al., 2014; IPCC, 2005). However, a 44 recent event where artificial injection activity of water in an enhanced geothermal system (EGS) triggered 45 a 5.5 magnitude earthquake of in Pohang, South Korea (Lee et al., 2019) led to increased public 46 awareness of the potential issues of injecting fluids into the subsurface in Korea. This situation led to the 47 temporary closure of a CO<sub>2</sub> capture and storage demonstration project intended to be performed in the 48 Pohang Basin, South Korea (Chen et al., 2018). Furthermore, it was alleged that CO<sub>2</sub> that had leaked from 49 50 the storage formation at the Weyburn-Midale site had polluted a nearby shallow groundwater zone (Beaubien et al., 2013). These examples highlight the need for a robust monitoring regime of any future 51 geological storage site to provide reassurance that CO<sub>2</sub> is being safely stored and that any migration from 52 53 the site can be detected.

54 The monitoring of leaked  $CO_2$  is often complicated by naturally occurring  $CO_2$  in the subsurface system. The distribution of  $CO_2$  is very heterogeneous in a natural groundwater system as a result of 55 56 chemical, biological, and physical interactions (Risk et al., 2015). The use of stable C isotopes for leakage monitoring can also be challenging because their signals in leaked fluids can overlap with those of 57 58 common surface sources (e.g., landfills) (Györe et al., 2017), following bacterial activity that enriches the <sup>13</sup>C by an oxidation process (Whiticar et al., 1999). However, noble gases are chemically and biologically 59 60 inert, and are only affected by quantifiable physical processes in a shallow aquifer system. Therefore, 61 noble gases can provide a means to separate and explain the physical processes in a biochemically 62 complicated system (Kilgallon et al., 2018). The benefits of this tracer were first recognized in an

enhanced oil and recovery (EOR) site, where engineers used this particular characteristic of noble gases to explain the physical process of a solubility-controlled mechanism in a multi-phase system composed of gas, water, and oil phases (Bosch and Mazor, 1988; Ballentine et al., 2002; Prinzhofer, 2013). In this complex system, the noble gases were phase-partitioned at the materials' interfaces, and the noble gas compositions were mass-dependently fractionated according to their solubilities (Ballentine et al., 1991, 1994; Lollar et al., 1997; Pinti and Marty, 1995). These valuable techniques have now been extended to the study of CCS projects to monitor the migration of a multiphase CO<sub>2</sub> plume in the subsurface system.

Although noble gases have been actively applied in CCS research for various purposes (Myers et al., 2013), they have been largely used to identify  $CO_2$  migration from a deep reservoir into a shallow aquifer to define a preferential pathway of migrated  $CO_2$  and to resolve the physical interactions governing the fate of the  $CO_2$ -rich plume.

Noble gases have been used to trace CO<sub>2</sub> leakage in natural analogue sites and artificial injection 74 experiments. Lafortune et al. (2009) suggested the potential applicability of noble gas for tracing gas 75 76 leakage from a reservoir into a shallow groundwater system, as the reservoir has a signature of this tracer 77 that is distinguished from that of shallow-depth groundwater. This was clearly proven at a natural 78 analogue site of post-emplacement seepage. For example, Gilfillan et al. (2011) concluded that an 79 elevation of HCO<sub>3</sub><sup>-</sup> in shallow-subsurface and surface waters originated from deep reservoir leakage, 80 based on a fingerprint of high-crustal <sup>4</sup>He. Györe et al. (2018) also pointed out that high <sup>4</sup>He in a deep reservoir can be used as a potential fingerprint to trace the fugitive release of reservoir gas. The concept 81 of a noble gas fingerprint was extended to tracer-enhancement work for artificially injected CO<sub>2</sub> at the 82 83 Cooperative Research Centre for Greenhouse Gas Technologies (CO2CRC) Otway Project to produce a strong signal for CO<sub>2</sub> plume leakage by distinguishing artificial CO<sub>2</sub> from natural CO<sub>2</sub> (Stalker et al., 84 85 2015).

86 In order to better understand the pathway of migrating  $CO_2$  within a deep reservoir, several artificial injection experiments have been undertaken. For example, CO<sub>2</sub> gas was injected into a 87 heterogeneous hydrocarbon reservoir (~3,080 m deep) within the Tuscaloosa Formation reservoir, 88 89 Mississippi, United States, and was followed by continuous monitoring (Lu et al., 2012). This resulted in 90 a unique bumpy breakthrough of noble gas having multi-peaks suggesting the existence of preferential paths between a leakage point and monitoring wells (Lu et al., 2012). In a shallow depth vadose zone 91 92 injection test, preferential paths were found between the injection point and monitoring probes, as induced by the natural heterogeneity of the limestone at the DEMO-CO<sub>2</sub> project, France (Rillard et al., 2015). 93 Lighter noble gases (He and Ne) were more helpful in defining the preferential path in the vadose zone 94 95 than  $CO_2$  and other tracers as they have faster arrival times at the monitoring probes owing to their higher 96 diffusion coefficients and lower solubility within the soil water in the CO<sub>2</sub>-Vadose project, France (Cohen 97 et al., 2013).

Detailed and extensive research on the fate of CO<sub>2</sub> has been undertaken in natural CO<sub>2</sub>-rich 98 99 reservoirs, which serve as analogues for artificial  $CO_2$  storage. For example, Zhou et al. (2005) constrained the evolution of natural CH<sub>4</sub> and CO<sub>2</sub> based on the mass-dependent fractionation of noble 100 101 gases in a coalbed methane system. Studies on a natural analogue site of a deep  $CO_2$  storage reservoir 102 suggested that a multi-step solubility-controlled process was significantly involved in the fate of CO<sub>2</sub> gas 103 under the impermeable cap-rock, as explained by the deeply fractionated noble gas ratio (Gilfillan et al., 104 2008; Zhou et al., 2012). Then, Gilfillan et al. (2009) concluded that naturally injected  $CO_2$  has been 105 primarily sequestrated within deep reservoirs through a solubility-controlled mechanism. In an engineered 106  $CO_2$  injection site, Györe et al. (2015) and Györe et al. (2017) observed that the noble gas composition of 107 produced gas can be successfully used to constrain the fate of the sequestrated  $CO_2$  at the Cranfield enhanced oil recovery (EOR) field and identified a clear sink of free-phase  $CO_2$  in areas making contact 108 109 with the reservoir groundwater. A numerical model has also been applied to define the fate of a reservoir

of  $CO_2$  by identifying the budget of residual trapped and immobilized gas in a deep storage site at the CO2CRC Otway test injection site (LaForce et al., 2014). Moreover, Zhang et al. (2011) delineated that immobilized gaseous  $CO_2$  retards the arrival of noble gas tracers, owing to their preferential partitioning into  $CO_2$  bubbles at interfaces. In a recent artificial injection experiment, an attempt was made to understand the fate of artificial  $CO_2$  released into a shallow groundwater system (Ju et al., 2019), where the fate of the leaked  $CO_2$  was constrained using noble gases. This highlighted the importance of solubility control and mixing mechanisms in shallow-depth groundwater.

117 Recently, studies have begun applying a noble gas fingerprinting tool for an actual monitoring purpose, i.e., to trace leaked  $CO_2$  from a reservoir into a shallow aquifer system. The noble gas tracing in 118 the shallow system is based on the inherent compositional difference between the reservoir fluid and the 119 groundwater above, and the composition of injected CO<sub>2</sub> is dependent on various CO<sub>2</sub> capture 120 121 mechanisms (Flude et al., 2016). Gilfillan et al. (2017) recognized the usefulness of composition at a real CO<sub>2</sub> injection site. For example, the storage reservoir was two orders of magnitude richer in radiogenic 122 <sup>4</sup>He compared to normal soil gases, providing an opportunity to evaluate allegations that unplanned 123 migration of CO<sub>2</sub> into a shallow aquifer near the Weyburn Midale oil fields had taken place. 124

125 Although noble gases have proved useful for tracing a CO<sub>2</sub> plume in many sites as described above, to the best of our knowledge, it has not yet been extensively used for monitoring in a shallow 126 127 aquifer (Lee et al., 2016). Moreover, most works have been limited to artificial release experiments and natural analogue sites, implying that further efforts are still required to link the valuable previous 128 129 observations to an actual CCS site. Therefore, this study attempted to discuss the application of these tracers to the monitoring of actual unplanned CO2 migration from a CCS site. For this purpose, two 130 131 injection tests were completed in a shallow aquifer system using noble gas tracers. This was intended to 132 explain the major processes responsible for the fate of the migrated  $CO_2$  plume in a multi-phase state and 133 to verify the findings from previous research. Then, based on the observations, we simulated the  $CO_2$  134 leakage by using analytical solutions and discussed how to use noble gas to identify  $CO_2$  migration, and 135 to constrain the fate of the migrated  $CO_2$ .

136 2 Material and methods

#### 137 **2.1** Artificial injection test

Sequestrated  $CO_2$  can be mobile when the cap-rock is broken or damaged (Figure 1). Then, 138 139 portions of free-phase CO<sub>2</sub> move upward due to buoyancy forces. Accidental leakage can occur through various vertical conduits such as an injection well, abandoned wells, or natural faults over different 140 periods of time (e.g., continuous low level leakage or short duration blowouts) (Alcalde and Flude, 2018). 141 142 While the free-phase  $CO_2$  migrates through conduits, it can spread into the multiple layers splitting the 143 mass (Jung et al., 2014) (Figure 1). Among the multiple layers, the ones with lower-permeabilities act as a 144 barrier preventing the CO<sub>2</sub> from reaching a shallower aquifer. Following a series of stratigraphic trappings, some volumes of  $CO_2$  finally reach the lower pressure system of shallow groundwater, which is 145 the very portion discussed throughout this paper. 146

The two artificial injections were performed to demonstrate the accidental leakage of  $CO_2$  into the 147 shallow aquifer. In particular, the injection experiments focused on the early-stage fate of free-phase CO<sub>2</sub> 148 reaching the low-pressure system (i.e. shallow aquifer). The initial state of  $CO_2$  is characterized by a high 149 150 partial pressure that can naturally nucleate the bubbles (Figure 1). The degassing dominantly occurs around a leakage point until stabilization occurs in the low-pressure system. After the degassing, the CO<sub>2</sub> 151 152 bubbles are redistributed between the groundwater (dissolved and remaining budget) and the atmosphere 153 (degassed and lost budget), reducing the total migrated CO<sub>2</sub> budget. The initial degassing is very important because it controls the overall budget of CO<sub>2</sub> remaining in the subsurface after it migrates into a 154 155 shallower system (Ju et al., 2019). In this context, the two experiments, in which gas-charged groundwater was injected into a shallow aquifer, were performed to demonstrate the early-stagesolubility-controlled process (i.e. degassing).



Figure 1. Conceptual figure to demonstrate accidental CO<sub>2</sub> leakage from a deep reservoir into a shallow
groundwater system. Early-stage fate of CO<sub>2</sub> is primarily controlled by the solubility-controlled process
(i.e., degassing) due to a high gas pressure.

162 **2.2** Test site overview

163 The first injection test was conducted in Wonju, Korea (Figure 1). The aquifer at the study site 164 consists of weathered and highly fractured Jurassic biotite granite overlain by soil and alluvial deposits 165 (Yu et al., 2006; Baek and Lee, 2011). The single-well tracer test (SWTT) was performed in the alluvial 166 deposits, which are a uniform material without fractures and conduits. The aquifer thickness was 10–15 m.

The aquifer hydrology at the site had a wide range of seasonal and spatial variations. The observed water 167 table was 2-13 m below the ground surface, but remained below 11 m during the dry season, when the 168 pilot test was performed. The hydraulic gradient varied from 0.008 m to 0.023 m. A pumping and slug 169 test revealed that the hydraulic conductivity of the site ranged between  $2.0 \times 10^{-4}$  cm/s and  $4.2 \times 10^{-3}$ 170 cm/s. In addition, the flow velocity of the regional groundwater was estimated, using <sup>3</sup>H-<sup>3</sup>He analysis, to 171 vary from 1.9  $\times$  10<sup>-6</sup> to 1.2  $\times$  10<sup>-4</sup> m/s (Kaown et al., 2014). A detailed description of the geologic 172 features, seasonal variations in aquifer hydrology, and land-use history of the study site can be found in 173 Lee et al. (2015). 174

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Figure 2. (a) Site map of Wonju, Korea; (b) full-screened KDPW4 was used for the SWTT at the site.
Injection was completed 24–27 m below the ground surface and approximately 10 m below the water
table. The injection interval was isolated using packer during the SWTT. The water table inside the
interval changed from 14.07 m (i.e. red triangle) to 16.64 m (i.e. blue triangle) below the surface during
the pull-phase of SWTT.

181 The second injection and recovery test was completed at the Korea CO<sub>2</sub> Storage Environmental
182 Management (K-COSEM) experimental test site in Eumseong, Korea (Figure 3). A monitoring network

was established at the test site for the CO<sub>2</sub> release and monitoring experiments. Geological information 183 184 was collected from borehole data at the study site: an alluvial deposit was found occurring 0-2 m below ground level (b.g.l.), weathered soils were found 2-30 m b.g.l., weathered rocks were found 30-70 m 185 186 b.g.l., and bedrock was found > 70 m b.g.l. (Ju et al., 2018a). The host rock was dark gray or light gray 187 biotite granite. The inter-well tracer test (IWTT) was performed in the weathered soils zone regarded as a 188 uniform material without any fractures and conduits. The water table was 16-17 m b.g.l., and the hydraulic gradient ranged from 0.01 to 0.05. The regional flow direction was from northwest to southeast. 189 The hydraulic conductivity estimated from the pumping test ranged from  $4.0 \times 10^{-6}$  m/s to  $2.0 \times 10^{-5}$  m/s. 190 191 A push-and-pull test was performed to identify the groundwater linear velocity (0.06–0.44 m/d), effective porosity (0.02-0.23), and uppermost aquifer thickness (47 m) of the study site. Detailed discussions on 192 the sequential hydraulic tests for establishing the monitoring network at the K-COSEM experimental test 193 site are summarized in Lee et al. (2017) and Lee et al. (2018). 194



Figure 3. (a) Site map of Eumseong, Korea. (b) Injection well (IW) and saturated zone monitoring well (SMW) 2-3 were used for the IWTT. The injection was completed 21–24 m below the ground surface and 4.5–7.5 m below the water table. Injection fluid moved along an induced pressure gradient of 0.93 between the two wells.

200 2.3 Experimental design overview

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Tracer-mixed groundwater was prepared and artificially injected into the groundwater. First, each
 sample of tracer-infused groundwater was created by flowing inert gases into local groundwater using a

203 gas regulator, ball-flowmeter, flexible tube, silencer (for gas diffusion), and carboy bottle (Figure 4). The 204 volumes of gas-charged groundwater samples were gently mixed together in the order of their solubility 205 in groundwater (i.e.,  $Kr \rightarrow Ar \rightarrow He$ ). The injection was completed using a submersible and controllable 206 quantitative pump "MP1" (Grundfos, Bjerringbro, Denmark). The sample for the injection fluid (C<sub>0</sub>) was 207 collected during the injection period, and the salinity was measured at the sampling time using portable 208 equipment from Yellow Springs Instruments (YSI) (YSI Inc./Xylem Inc., USA). The salinity was 209 reported in units of ppt, with a precision of ±0.01 ppt.



Figure 4. Schematic figure of the injection system. Volumes of tracer-infused groundwater were first prepared by blowing a pure gas (He, Ar, Kr of 99%) into the local groundwater; then, the gas-charged water samples were gently mixed together in a closed tank with a circulation pump until they were injected into the groundwater system. The injection fluid ( $C_0$ ) was sampled at the sampling port attached to this tank during the injection period.

216 The first pilot test was carried out in Wonju, Korea, as a single-well tracer test (SWTT). The 217 SWTT is a three-step process consisting of push, drift, and pull periods. During the push period, gascharged groundwater (200 L) composed of salt, Ar, He, and  $SF_6$  was injected, and was followed by the 218 219 release of a chaser fluid (120 L) to flush the residual volume of injection water from the injection 220 wellbore. The injection speed was 9.30 L/min (September 22, 2016) using KDPW4 as the injection well. 221 This is a fully screened well with a depth of 27 m (Figure 1). The target injection zone was 24–27 m 222 below ground level, and 10 m below the water table. A packer was used to tightly seal the area 1 m above 223 the target injection zone. After the injection period, the tracer-infused water had a drift time of 1,522 min 224 in the groundwater system. Then, in the pull period, it was recollected for 319 min at a rate of 3.87 L/min through the injection well (September 23, 2016). At the same time, parts of the pulled groundwater were 225 226 sampled at the well surface. The samples of the inert gas tracers were collected at 2–10 min intervals that were gradually increased. The salinity was measured in situ using portable equipment from YSI (YSI 227 228 Inc./Xylem Inc, USA) every 2-10 min, and this interval was also gradually increased.

The second pilot test was performed at the K-COSEM experimental test site as an inter-well 229 230 tracer test (IWTT). Before the tracer injection, an induced hydraulic gradient of 0.93 was created between 231 the injection well (IW) and saturated zone monitoring well (SMW) 2-3 (Figure 3). Gas-charged 232 groundwater (1,000 L) composed of salt, Kr, Ar, and He was released into the IW at a rate of 4.74 L/min (October 13, 2016). The target injection zone was 21–24 m below the ground surface, and 4.5–7.5 m 233 234 below the water table at IW. The injection event was followed by 10 days of monitoring at the SMW 2-3 235 of down gradient (to October 22, 2016). Parts of the pulled groundwater were sampled at the well surface of SMW 2-3. The samples for the inert gas tracers were collected in 2-5 h intervals that were gradually 236 237 increased. The salinity was measured in situ using portable equipment from YSI (YSI Inc./Xylem Inc, USA) every 2–5 h, and this interval was also gradually increased. 238

239 **2.4** Data acquisition from water samples

240 The groundwater samples for sulfur hexafluoride (SF<sub>6</sub>) were collected in glass bottles and were 241 tightly sealed using caps with metal liners. The sample analysis was automatically completed at the Core Laboratory of Innovative Marine and Atmospheric Technology (CLIMATE) at the Pohang University of 242 243 Science and Technology (POSTECH). The automatic device included a gas chromatograph equipped with 244 an electron capture detector, a  $SF_6$ -extraction device, a global positioning system, and a data acquisition 245 system based on Visual Basic 6.0/C 6.0. The  $SF_6$  in the groundwater was quantified in comparison to gas standards of 6, 60, 103, 104, 200, 352, and 704 pptv. The precision of this method was better than 0.2% 246 (Koo et al., 2005). 247

For noble gas analysis, 28 cm<sup>3</sup> of groundwater was sampled using a copper tube and a stainless-248 steel clamp (to prevent air contamination). The samples were analyzed in the noble gas analysis 249 laboratory at the Korea Polar Research Institute (KOPRI). First, the dissolved gas was extracted from the 250 groundwater under a high vacuum ( $\sim 10^{-7}$  mbar) and stored in an aluminosilicate ampoule to remove the 251 majority of the water in a manner similar to the method of Lott and Jenkins (1998). The extracted gas was 252 further treated using a separated and automated processing line equipped with cryogenic traps and getter 253 254 pumps (hot and cold St 101, SAES) (Beyerle et al., 2000) as outlined in Stanley et al. (2009) to remove 255 residual water vapor, active gases, and other condensable gases. Then, each noble gas component was 256 cryogenically separated and drawn down into a mass spectrometer, i.e., a residual gas analyzer (RGA) 200 (Stanford Research Systems, California, USA), from low mass to high mass. <sup>4</sup>He, <sup>40</sup>Ar, and <sup>84</sup>Kr were 257 quantified and calibrated against air standards of 0.9–2.7 cm<sup>3</sup> in consideration of the wide concentration 258 range of artificially enhanced tracers. Then, the abundant isotopes were reported as the total amount of 259 each noble gas at standard temperature and pressure (STP), assuming they are isotopically air-like. The 260 261 analytical error for the post-injection data was less than 5% based on duplicate sample analyses (Ju et al., 2018b, 2019). 262

**Results** 263 3

264

#### 3.1 Tracing artificially leaked plume

The noble gas tracer method has shown the potential to explain the fate of high-pressure  $CO_2$  that 265 has migrated from a deep reservoir into a shallow aquifer system (Gilfillan et al., 2017; Ju et al., 2019). In 266 267 this section, the behavior of the noble gas was determined following the two separate controlled release experiments in the shallow-depth aquifer system. Specifically, during the two injection tests, the mass 268 269 recovery was observed after injecting the groundwater charged with the partitioning (i.e. inert gas tracers) 270 and non-partitioning tracers (i.e. salt) into the shallow aquifers. Here, the partitioning tracer is defined as a 271 substance having a partitioning behavior in a multi-phase system composed of gas and groundwater and, the non-partitioning tracer only exists as a dissolved phase in the multi-phase system. 272

273

## 3.1.1 Mass recovery curve of the leaked plume

A total of 200 L of groundwater (C<sub>0</sub>) containing 68.6 ppb of SF<sub>6</sub>,  $2.05 \times 10^{-6}$  cm<sup>3</sup> STP/g of He, 274  $3.06 \times 10^{-3}$  cm<sup>3</sup> STP/g of Ar, and 10.7 ppt of salt was injected into the shallow aquifer. The mass recovery 275 276 of the inert gas tracers was calculated in an identical manner as Kim et al. (2018), where the total recovery was a summation of the areas in a volume-concentration plot (i.e., recovery =  $\Sigma$  volume (L<sup>3</sup>) × 277 concentration  $(M/L^3)$ ). The results revealed that the recovery ratio of each tracer was clearly related to its 278 respective solubility. As shown in Figure 5a, the recovery ratios of SF<sub>6</sub>, He, Ar, and salt were 49.3%, 279 280 58.1%, 78.2%, and 73.1%, respectively. The solubility-controlled processes of phase-partitioning and 281 degassing influenced the fate of the injected gas tracers as expected (Ballentine et al., 2002). The tracer 282 recovery ratios from single-well push-pull tracer tests exhibited various ranges of distribution depending 283 on the nature of tracers, drift time, pump back rate, and density effect, and several controlled tests revealed that the recovery ratios do not reach 100% (Kim et al., 2018). Although salt is known to be 284 285 conservative in a groundwater system, the mass recovery of salt was slightly less than that of the Ar tracer.



As salt does not undergo phase-partitioning in a groundwater system, entrapment of salt mass into low

permeability zones was a possible reason for the mass loss in the SWTT (Kim et al., 2018, 2019).

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Figure 5. Mass recovery curves of the injected tracers (a) from the SWTT and (b) from the IWTT. Each Y-axis displays the recovery ratio of tracers recorded above the background level. The recovery rate of inert gas tracers was relative to their solubility for groundwater in an air-water system, indicating that solubility-controlled processes were involved in the fate of the leaked plume.

293	A total of 1,000 L of groundwater containing $4.02 \times 10^{-6}$ cm <sup>3</sup> STP/g of He, $2.29 \times 10^{-2}$ cm <sup>3</sup>
294	STP/g of Ar, $1.05 \times 10^{-5}$ cm <sup>3</sup> STP/g of Kr, and 5.87 ppt of salt was injected into the shallow aquifer. The
295	mass recovery rate of the IWTT was much lower than that of the SWTT. In particular, the difference
296	between the non-partitioning tracer (i.e., salt) and the partitioning tracers (i.e., noble gas tracers) in terms
297	of mass recovery was much greater than that of the SWTT, in which the mass recoveries of He, Ar, Kr,
298	and salt were 0.0135%, 0.0137%, 0.0602%, and 75.0%, respectively. The non-partitioning tracer flows
299	along the groundwater flow paths, and only a portion of the tracer mass is not captured in the recovery
300	well because of dispersion or density-effect (Kim et al., 2018). In contrast, the partitioning tracers can
301	easily escape from the flow paths, owing to their high diffusivity and partitioning behavior (Carrigan et al.,
302	1996; Heilweil et al., 2004), resulting in a significant decrease in the mass recovery (see next section).
303	Specifically, the extremely low level of recovery for the noble gas tracers, which was three orders of
304	magnitude lower than that of salt, seems to be attributable to several factors related to the design of the
305	experiment: 1) the brine had been charged with insoluble tracers for several hours; therefore, it is possible
306	that the total gas pressure of injected water increased beyond $P_{ATM} + P_{H2O}$ at the injection point, resulting
307	in active bubble growth; 2) the pumping action at the extraction well (i.e., SMW 2-3) possibly induced a
308	pressure drop, accelerating the bubble growth; 3) the upward movement of the injected plume toward the
309	water table through the permeable materials of the borehole resulted in a re-equilibrium of the high P
310	plume (i.e. gas-charged water) with the atmosphere. Istok et al. (2006) highlighted the degassing
311	mechanism of a high P plume through borehole materials in detail. The mass recovery ratios of the
312	partitioning tracers, however, were clearly in the order of their solubilities for groundwater (Table A.1 in
313	Appendix A). Therefore, solubility-controlled processes influenced the fate of the gas-charged plumes
314	during the IWTT (Ballentine et al., 2002).

315

## 3.1.2 Fate of the leaked plume

316 In the mass recovery curves, the recovery ratios of the noble gas tracers followed the order of the 317 tracers' solubilities in groundwater, suggesting that solubility-controlled processes influenced the 318 migration of the leaked plume. The Rayleigh distillation equation was used to explain the influence of the 319 solubility-controlled processes on the fate of the leaked plume (Ballentine et al., 2002). The equations for 320 estimating the degassing process are listed in Appendix A, where the partitioning coefficients in pure 321 water system were adopted for the calculation (Table A.1). A continuous degassing of the He and Ar tracers is apparent, as shown in Figure 6 (i.e., the gray arrow). Without the degassing loss, the tracers 322 323 were expected to follow the mixing line between the injection and background concentration (i.e., the 324 dashed line for Figure 6a and dash-dot line for Figure 6b). However, once the degassing process starts, the noble gas composition of the dissolved plume fractionates, because less soluble and lighter elements are 325 326 preferentially lost into the gas phase at the gas/water interfaces than those that are heavier (Ballentine et al., 2002). As shown in Figure 6, the He/Ar changed relative to the tracer's solubility, following the 327 328 degassing line (i.e., gray arrow). During the SWTT, the noble gas distribution was defined by the two 329 physical processes such as the degassing and mixing processes. The two processes could not be explained 330 separately, as the concentration change arose from both mechanisms occurring at the same time (Figure 6a). This seemed to be attributable to the experimental procedure of the SWTT, in which the three-step 331 332 process (push-drift-pull) caused multiple stress periods (e.g. pressure instability/vertical movement) that 333 caused the dissolved plume to irregularly degas as the local groundwater diluted the multi-phase plume.



![](_page_21_Figure_2.jpeg)

**Figure 6.** (a) Noble gas concentration anomaly of the SWTT. The injected tracer changed with both the degassing and mixing processes. The two processes occurred concurrently and could not be explained separately. The heavily degassed sample spent the longest time in the groundwater system, showing the bottom upward recovery toward background levels. (b) Noble gas concentration anomaly of the IWTT. The degassing process first occurred and was followed by a mixing process. The mass retention and loss of the tracer gases can be evaluated in either an open system (orange colored) or a closed system (green colored) at the intercept (see the text for details).

342 Two distinctive models were employed to explain the mass retention and the loss of injected tracers during the IWTT (Ballentine et al., 2002; Gilfillan et al., 2008; Ma et al., 2009). The first is the 343 344 degassing of tracers in a closed system, in which air bubbles are retained and trapped in a groundwater system following the degassing process. In a closed system, equilibrium is achieved between the gas 345 346 phase and the dissolved phase in the groundwater at the end of the degassing process. The second is phase-partitioning in an open system, in which the degassing process results in a mass reduction in the 347 total mass. Consequently, air bubbles, having mobility, are lost into the atmosphere following the phase-348 349 partitioning. In an open system, the air mass is lost into the atmosphere stepwise until the end of the 350 degassing process. Both of these extreme cases were modeled and elucidated for the fate of injected fluid 351 during the IWTT (Appendix A). In Figure 6b, phase-partitioning in the closed system is denoted by a gray 352 line and that in the open system is depicted by a gray dotted line.

The two processes (i.e., degassing and mixing) were separated in the time domain during the IWTT, in which the degassing process occurred first and was followed by the mixing process, unlike in the SWTT. The separation of the two processes gave us an opportunity to quantify the degassed amount (Zhou et al., 2005). At the intercept, the gas/water ratio was 2.44 for the closed system and 0.162 for the open system. As the shallow groundwater cannot hold such a large amount of gas (gas/water = 2.44) in the system, the environment behaved like an open system during the degassing process. Then, the gas volume liberated from water was constrained at the intercept of the open system and reached  $0.162 \times 10^6$ cm<sup>3</sup> (Figure 6b) (Appendix A). This amount corresponds to the residual Ar of  $3.61 \times 10^{-4}$  cm<sup>3</sup> STP/g in groundwater that is already close to the ASW level ( $3.60 \times 10^{-4}$  cm<sup>3</sup> STP/g) in an aquifer system, suggesting the injected plume depressurized and stabilized in the local system even before interacting with local groundwater.

#### 364 4 Discussion

Noble gas tracers were employed for two injection tests to explain the physical processes 365 involved in the migration of a leaked plume, i.e., gas-charged water, in a shallow aquifer system. During 366 367 the tests, the fate of the leaked plume was first defined by a solubility-controlled process (i.e., degassing), 368 which was followed by a volumetric mixing process. This result is consistent with observations from 369 another artificial injection test (Ju et al., 2019), which revealed that the noble gas anomaly in a  $CO_2$ -rich plume is a function of the degassing and physical mixing processes in a shallow aquifer system (see 370 Figure 11 in Ju et al., 2019). Furthermore, these are similar to the conclusions reached at a natural CO<sub>2</sub> 371 372 production site (Zhou et al., 2005) that stripping loss of insoluble gases was followed by dilution by 373 diffusive mixing with the un-degassed local groundwater. These observations suggest that the solubility-374 controlled process and the mixing process are primarily responsible for the fate of the leaked plume in the shallow aquifer system. 375

# 3764.1Application of a noble gas tracer to the detection of CO2 leakage: Case study at the377Weyburn and Midale oil fields

378 Noble gas tracers have been applied to study the fate of leaked  $CO_2$  in a shallow aquifer system 379 (Gilfillan et al., 2011; Ju et al., 2019; Zhou et al., 2005). However, previous studies have been sparingly 380 applied to artificial injection tests and natural analogue sites. Although these works provide an insight on 381 the behavior of a leaked plume, further efforts are required to link those valuable observations to an actual

382 CCS site. Specifically, we need to know what we would observe if the free-phase  $CO_2$  accidently reached 383 the shallow aquifer. This can be demonstrated by simulating the hypothetical leakage on an actual CCS 384 site based on our observations from the two distinct artificial injection tests and other valuable previous 385 studies. To understand the fate of  $CO_2$  under hypothetical leakage conditions, the monitoring data from 386 the Weyburn storage site was incorporated in the leakage simulation.

The Weyburn Midale oil field is a CO<sub>2</sub>-EOR and CO<sub>2</sub> storage site, where a large amount of CO<sub>2</sub> 387 has been introduced into a deep reservoir (Gilfillan et al., 2017). Recently, this site received public 388 attention as CO<sub>2</sub> leakage allegations implying that anthropogenic CO<sub>2</sub> leaked from the deep reservoir into 389 a nearby shallow aquifer on private land were made. At this site, Gilfillan et al. (2017) used the inherent 390 noble gas tracers in the different fluids associated with the site to judge whether upward migration had 391 occurred from the deep reservoir into the shallow aquifer. Based on the results, the leakage allegation (i.e., 392 393 upward migration of CO<sub>2</sub>) were proved false, as the observed concentration of noble gas tracers simply did not follow the composition of the reservoir CO<sub>2</sub> carrying the high amount of radiogenic <sup>4</sup>He (see 394 Table 1 for the composition of two reservoirs). 395

Though this case study proved the usefulness of a noble gas tracer, we have expanded this study in a more quantitative way to discuss what we would actually observe if free-phase  $CO_2$  leaked into a shallow aquifer. Repeated simulations were made based on various analytical models to understand how we can use a noble gas tracer as a proxy to understand the fate of free-phase  $CO_2$  that has leaked from a deep reservoir into a shallow aquifer system.

401 **Table 1** Noble gas composition in shallow groundwater and in a  $CO_2$  plume. The noble gas distribution of 402 dissolved  $CO_2$  was calculated based on the composition of gas produced from the Weyburn storage 403 reservoir. Note that the composition of the shallow aquifer is close to that of the air saturated water 404 (ASW).

	$^{4}$ He (×10 <sup>-8</sup> )	Ne ( $\times 10^{-7}$ )	$^{20}$ Ne (×10 <sup>-7</sup> )	$^{40}$ Ar (×10 <sup>-4</sup> )	$^{36}$ Ar (×10 <sup>-6</sup> )	$^{84}$ Kr (×10 <sup>-8</sup> )
Dissolved	763	0.084	0.076	0.724	0.138	1.440
$\operatorname{CO}_2, \operatorname{C}_0^{\dagger}$	1831	0.135	0.123	0.986	0.186	0.344
$(std dev.)^{+}$	58.2	32.9	33.1	21.7	21.0	86.9
Shallow Aquifer <sup>§</sup>	5.84	1.90	1.73	3.04	1.03	4.92
$(\text{std dev.})^{\ddagger}$	29.1	18.5	18.3	9.24	8.96	11.2
ASW <sup>¶</sup>	4.25	1.81	1.64	3.25	1.10	4.29

405 All the measured data were from Gilfillan et al. (2017) in  $\text{cm}^3/\text{g}$ .

<sup>†</sup>noble gas contents in dissolved  $CO_2$  prior to stripping loss calculated assuming 100% dissolution of the free-phase  $CO_2$  at the P and T conditions of shallow groundwater; temperature of 14.3°C, salinity of 0.02 g/kg, and pressure of 0.101 MPa. The high level of <sup>4</sup>He in the dissolved  $CO_2$  is attributed to an interaction between the reservoir gas and crustal sources. The depletion of the other noble gases is due to an interaction between the reservoir gas and artificially injected  $CO_2$ .

- 411 <sup>‡</sup>1 sigma value relative to the average (%).
- 412 <sup>§</sup>average concentration of noble gases in the shallow groundwater samples.
- 413 <sup>¶</sup>Air saturated water (ASW) concentration was calculated assuming a temperature of 14.3°C, salinity of
- 414 0.02 g/kg, and altitude of 580 m.
- 415 **4.1.1** Fate of free-phase CO<sub>2</sub> in the shallow aquifer

416 Previous studies have revealed that diverse factors control the noble gas composition of captured CO<sub>2</sub> once it is injected into the subsurface, such as the initial capture process, degassing, dissolution, 417 diffusion, adsorption, CO<sub>2</sub> density, and reservoir interactions (e.g., with atmospheric, crustal, and mantle 418 419 sources) (Flude et al., 2016; Gilfillan et al., 2011; Holland and Gilfillan, 2013; Kilgallon et al., 2018; 420 Warr et al., 2015; Wilkinson et al., 2010; Zhou et al., 2005). Furthermore, a recent artificial release test 421 demonstrated the behavior of leaked CO<sub>2</sub> in a shallow aquifer, which was defined by degassing and mixing processes based on noble gas tracers (Ju et al., 2019). From the insights of previous works, we 422 will discuss how these processes are involved in the fate of free-phase  $CO_2$  in a shallow aquifer system 423 424 based on the behavior of noble gas tracer.

425 The free-phase  $CO_2$  that leaks from a deep reservoir into a shallow aquifer is rich in <sup>4</sup>He from previous interactions with a deep crustal source but is low in other elements from the initial industrial 426 capture process (Table 1). Following leakage, free-phase CO2 forms a dissolved plume in a shallow 427 aquifer, and the contents of the plume naturally follow those of the free-phase CO<sub>2</sub>. The concentration of 428 the CO<sub>2</sub> plume (i.e., the blue cross symbol) will change in the groundwater system depending on various 429 physical interactions, which are depicted using the <sup>4</sup>He and <sup>40</sup>Ar tracers in Figure 7. A detailed description 430 of the theoretical calculations can be found in Appendix A. One of most noticeable processes controlling 431 432 the fate of this plume is a volumetric mixing process (Gilfillan et al., 2011; Ju et al., 2019) (see also Figure 6) occurring as the CO<sub>2</sub> plume moves through porous media with the local groundwater. While 433 being gradually mixed with the local groundwater, the initial plume becomes depleted in <sup>4</sup>He and 434 enriched in <sup>40</sup>Ar (i.e., the black line). The noble gas anomaly in this process is dependent on the 435 compositional difference between the initial plume and local groundwater, and their mixing fractions, 436 whereby <sup>4</sup>He could vary by up to -99.6% and <sup>40</sup>Ar could vary by up to 256% (i.e., the light gray zone). 437

![](_page_27_Figure_1.jpeg)

#### 438

Figure 7. Percent change in the noble gas concentration (i.e.,  $[NG - NG_i] / NG_i \times 100$ ) from the initial 439 440 composition (NG<sub>i</sub>) under various physical processes. The composition of the initial plume was calculated 441 assuming 100% dissolution of free-phase CO<sub>2</sub> in the shallow aquifer (see Table 1). BGs (i.e., pink cross 442 symbols) present the concentrations of shallow aquifer samples, and ASW is the air saturated water 443 concentration under local groundwater conditions (i.e., green diamond; see Table 1). In the light gray zone, the mass distribution is controlled predominantly by mixing processes. Volumetric mixing occurs as 444 445 the CO<sub>2</sub> plume moves through a porous medium with the local groundwater (i.e., the black line) 446 (Appendix A). The diffusion process occurs along a concentration gradient, for example, at a plume boundary or water table (i.e. the red line) and is depicted with diffusion coefficients from Jähne et al. 447 448 (1987) and Wise and Houghton (1966) (Eq. A.4 in Appendix A). It only occurs at  $t > 4\pi D$ , theoretically (i.e., the dotted line before threshold) (Fetter, 1999). The dark gray zone indicates a large contribution of a 449 450 solubility-controlled process to the fate of the CO<sub>2</sub> plume. The degassing process occurs during the initial

451 period of a leakage and continues until the plume is stabilized in the relatively low pressure condition of 452 the shallow aquifer (i.e., the blue and light blue lines) modeled using partitioning coefficients from the 453 NIST chemistry webbook of Sander (2017) (Appendix A). Explanations for each degassing system (i.e., 454 closed and open) can be found in the text. The air intrusion line depicts the data contamination due to the 455 addition of atmospheric air into groundwater during the sampling procedure (i.e., the black dotted line). 456 All the measured data were from Gilfillan et al. (2017).

457 Diffusive movement occurs along the concentration gradient under Fick's second law and would be observable at the plume boundary where the CO<sub>2</sub> plume meets the local groundwater. This also occurs 458 at the water table, when the plume makes contact with the atmosphere. Therefore, in these places (i.e., 459 plume boundary and water table), the composition of the noble gas will be differentiated from that of the 460 plume center (i.e., the red line in Figure 7). The maximum change (%) is, however, consistent with the 461 462 volumetric mixing process, as this process is also based on the concentration difference between the CO<sub>2</sub> plume and local groundwater. The diffusion process affects the fate of dissolved gas plume at a natural 463 gas production site (Zhou et al., 2005). With the gas production, there was an intensive stripping loss of 464 insoluble noble gases, which resulted in a steep concentration gradient at a contact boundary where noble 465 gas tracers diffusively spread along a concentration gradient. In a fractured aquifer, this process can result 466 467 in significant loss of insoluble noble gases into immobile zones because of a concentration gradient 468 between the mobile (i.e. fractures) and immobile zones, and therefore, a delay of lighter elements 469 observable at monitoring points (Carrigan et al., 1996; Sanford et al., 1996). Moreover, this behavior was 470 minutely demonstrated in a numerical simulation following a detailed laboratory experiment (Kilgallon et al., 2018), in which the arrival time of the noble gas was determined predominantly by the diffusion 471 472 process while migrating in a gas phase CO<sub>2</sub>.

473 In contrast, a solubility-controlled process leads to a depletion of all tracers (i.e., the dark gray
474 zone in Figure 7). This process is possibly observable at the initial stage of leakage when the CO<sub>2</sub> plume

475 is unstable owing to the high partial pressure of inherent gases (Figure 1). The initial plume would degas 476 the CO<sub>2</sub> rapidly until it stabilized in the lower pressure of the shallow groundwater, as shown in the IWTT (Figure 6b). During this process, the free CO<sub>2</sub> carries the insoluble gases from the dissolved phase and 477 478 stays in the surrounding environment, resulting in a gas-water equilibrium (closed) or CO<sub>2</sub> bubbles of 479 infinitesimally small size escaping from the groundwater continuously until the end of degassing process 480 (open) (Ballentine et al., 2002; Gilfillan et al., 2008; Ma et al., 2009). This process results in the noble gases fractionate continuously until the plume is stabilized at local conditions of P, T, and CO<sub>2</sub>-density in 481 shallow groundwater. It is evident that the lighter <sup>4</sup>He tends to be more depleted compared to the heavier 482 <sup>40</sup>Ar, and this trend appears more significant in the open system than in the closed system (dark gray 483 zone). The solubility-controlled process is a major mechanism controlling the fate of a CO<sub>2</sub>-rich plume, 484 and has been observed in a natural analogue site of  $CO_2$  leakage (Zhou et al., 2005) and an artificial  $CO_2$ 485 injection experiment (Ju et al., 2019), in addition to the current experiments. 486

The adsorption process is known to result in a relative enrichment of heavy noble gases (i.e. Kr 487 and Xe) in terrigenous sediments (Fanale and Cannon, 1971), and this phenomenon is particularly 488 489 noticeable in a system that includes organic rich units such as shale formation (Podosek et al., 1981). 490 Should groundwater or free-phase  $CO_2$  makes contact with such an organic rich formation, it will become 491 enriched in heavier species (i.e., Kr and Xe) from the ASW composition, reflecting the release of sedimentary noble gases (i.e., heavier species) from the organic source kerogens (Torgersen et al., 2004). 492 493 The action of this process has been demonstrated in organic rich sediments, where the distribution of the heavier species can be distinguished from those of a normal oil-water system (Torgersen and Kennedly, 494 1999) and gas-water system (Ma et al., 2009). Unfortunately, proper coefficients had not been provided 495 for this mechanism (Holland and Gilfillan, 2013; Myers et al., 2013; Flude et al., 2016), and inevitably, 496 an analytical calculation was not made for this process. However, groundwater that makes contact with 497 organic matter evidently becomes enriched in heavier noble gases (i.e. Kr and Xe); therefore, samples 498

affected by this process should be carefully treated, and lighter species (i.e. He, Ne and Ar) should beadopted for the other quantitative evaluations.

The air intrusion line depicts data contamination due to the addition of atmospheric air into groundwater during the sampling process. The effects of air contamination are very different from the other processes, as air contamination results in positive changes for both elements (i.e., the right-side of the white zone in Figure 7). This suggests that we can possibly distinguish and separate this erroneous behavior for quantitative evaluations.

506 4.1.2 Monitoring efficiency of noble gas tracers

As noble gas analysis is time-intensive, people who want to use these tracers for monitoring  $CO_2$ 507 leakage will naturally wonder which tracer is most efficient. It seems evident that the tracer showing the 508 509 largest compositional difference between the free-phase  $CO_2$  and shallow system would be the most 510 efficient for tracing  $CO_2$  leakage in a shallow aquifer (Flude et al., 2016). In that regard, the tracer with 511 the largest difference in concentration between the C<sub>0</sub> (i.e., dissolved CO<sub>2</sub> from Table 1) and BG (i.e., shallow aquifer from Table 1) can easily detect  $CO_2$  in the monitoring system. In addition to the 512 513 compositional difference, the natural variation is another factor controlling the monitoring efficiency. In terms of leakage monitoring, the natural variation of monitoring parameters can dilute the leakage signal 514 and deteriorate the monitoring efficiency. For this complicated issue, Risk et al. (2015) defined a 515 516 minimum threshold value for each monitoring parameter to confirm CO<sub>2</sub> leakage safely. According to previous research, a "leakage" could be detected safely when signals of a monitoring parameter increase 517 518 over the three sigma value of the natural variation of the parameter. In Table 2, the threshold values  $(3\sigma)$ 519 are listed for each tracer.

**Table 2** Conditions for detecting the  $CO_2$  leakage in a monitoring system. A large difference in noble gas composition between the  $C_0$  (i.e., dissolved  $CO_2$  from Table 1) and the BG (i.e., shallow aquifer from

522 Table 1) indicates a high monitoring efficiency. The CO<sub>2</sub> leakage will be recorded in a monitoring system for the first time when the concentration starts to increase/decrease over the  $3\sigma$  value, which was 523 524 calculated for each element (upper section). Each cell in bottom section indicates the minimum proportion of  $CO_2$  plume arriving at a monitoring system needed to overcome the detection threshold (i.e., the value 525 corresponding to the  $3\sigma$  value in Figure 8) calculated for various cases of degassing loss. Note that the 526 large difference in <sup>4</sup>He content between the C<sub>0</sub> and BG will generate a huge signal that will be larger than 527 528 the  $3\sigma$  value with a small portion of CO<sub>2</sub> arriving at a monitoring point. Therefore, a high monitoring efficiency will be achieved. 529

	<sup>4</sup> He	<sup>20</sup> Ne	<sup>40</sup> Ar	<sup>36</sup> Ar	<sup>84</sup> Kr	<sup>4</sup> He/ <sup>40</sup> Ar	<sup>84</sup> Kr/ <sup>20</sup> Ne
	$(\times 10^{-8} \text{ cm}^3/\text{g})$	$(\times 10^{-7} \text{ cm}^3/\text{g})$	$(\times 10^{-4} \text{ cm}^{3}/\text{g})$	$(\times 10^{-6} \text{ cm}^3/\text{g})$ (	$\times 10^{-8} \text{ cm}^{3}/\text{g}$	) $(\times 10^{-3})$	-
$ C_0 - BG ^{\dagger}$	1292	1.63	2.19	0.865	4.03	152	0.601
$3\sigma$ of BG <sup>‡</sup>	5.09	0.95	0.84	0.276	1.65	0.123	0.210
Degassing Amount <sup>¶</sup>			mixing	g % with CO <sub>2</sub> plu	ume <sup>§</sup>		
0	0.394	58.4	38.6	31.9	41.0	0.00288	5.64
1.8	1.14	56.4	35.6	30.7	40.0	0.00823	5.18
4.5	5.78	55.4	32.8	29.4	38.7	0.04	5.57
7.2	37.4	55.1	31.1	28.6	37.7	0.198	6.44

<sup>530</sup> All the measured data were from Gilfillan et al. (2017).

<sup>1</sup>degassed amount from a CO<sub>2</sub> plume in an open system in units of  $\times 10^{-7}$  cm<sup>3</sup> STP/g.

<sup>&</sup>lt;sup>†</sup>difference in noble gas concentration between the initial  $CO_2$  plume ( $C_0$ ) and the shallow groundwater

<sup>532 (</sup>BG). Note that a large difference indicates a high monitoring efficiency.

<sup>&</sup>lt;sup>‡</sup>3 standard deviation of shallow groundwater samples, presenting the natural variability.

<sup>§</sup>At least n% of the CO<sub>2</sub> plume should arrive at the monitoring system to override the detection threshold (i.e., the  $3\sigma$  value) and so that CO<sub>2</sub> leakage can be reported. This concept was introduced by Risk et al. (2015).

538

#### 4.1.2.1 Physical processes affecting the monitoring efficiency

539 As noble gas distribution is related to physical interactions in the CO<sub>2</sub> leakage condition (see 540 section 4.1.1. Fate of free-phase  $CO_2$  in shallow aquifer), the monitoring efficiency of noble gas tracers is 541 also dependent on physical processes. When  $CO_2$  leakage occurs in a shallow aquifer, one can first observe the front of the  $CO_2$  plume at a monitoring well as it gradually approaches the monitoring areas. 542 In this case, the "first signal" of the noble gas parameters will be variable, depending on the nature and 543 magnitude of the physical processes controlling the evolution of the CO<sub>2</sub>-rich plume. The evolutionary 544 path of the CO<sub>2</sub> plume was depicted using noble gas tracers under physical processes (Figure 8), and was 545 546 based on observations made from two iterations of artificial injection tests and previous studies (Gilfillan 547 et al., 2011; Ju et al., 2019; Sanford et al., 1996; Zhou et al., 2005). In this scenario, the initial  $CO_2$  plume is unstable, owing to the high partial pressure of CO<sub>2</sub> in the shallow aquifer (Figure 1). Therefore, it 548 549 undergoes a degassing process rapidly until it stabilizes at the shallow aquifer conditions of P, T, and 550 CO<sub>2</sub>-density. Then, the remaining mass (i.e. dissolved phases) undergoes a mixing process as the plume moves through the porous medium with the local groundwater toward the observation wells (Figure 1) (Ju 551 552 et al., 2019).

From a monitoring point of view, the concentrations of the noble gases will start to deviate gradually from the composition of the air saturated water (ASW) (i.e. green diamond) as the plume approaches an observation point and, at some point, they will vary over the threshold (i.e., the.  $3\sigma$  line), confirming CO<sub>2</sub> leakage occurrence (Figure 8). Information about the first detection points (i.e., the minimum mixing proportion of the CO<sub>2</sub> plume needed to override the detection limit and the composition of the noble gas tracer at this point) is listed in Table 2. For example, we can see the first arrival of <sup>4</sup>He when the CO<sub>2</sub> plume (1.14%) approaches a monitoring well, which initially loses a CO<sub>2</sub> mass of  $1.8 \times 10^{-5}$ CO<sub>2</sub> cm<sup>3</sup> STP/g H<sub>2</sub>O during the degassing event.

![](_page_33_Figure_2.jpeg)

Figure 8. Evolution of a CO<sub>2</sub> plume under physical processes in terms of noble gas concentration. All the 562 563 measured data and hypothetical values (i.e. leaked fluid) were from Gilfillan et al. (2017). In this scenario, 564 the initial plume is unstable and, therefore, undergoes the degassing process rapidly until stabilization is achieved in the shallow groundwater system (i.e., gray lines). Then, the degassed plume undergoes a 565 566 dilution process by mixing with local groundwater (i.e., blue or pink lines). Due to the diffusion process, the points can deviate from the degassing-mixing trend and converge toward a natural background level 567 as diluted (i.e., brown arrow), and action of this process can be prominent at the plume boundary or water 568 569 table as facing a concentration gradient. From a monitoring point of view, the observed concentration will 570 gradually evolve from the Air Saturated Water level (ASW; i.e. green diamond; see Table 1) as the CO<sub>2</sub>

plume approaches a monitoring point, and one can eventually notice the  $CO_2$  leakage occurrence when signals override the detection threshold,  $3\sigma$  value. Note that the degassing process was depicted in both the air-H<sub>2</sub>O system and CO<sub>2</sub>-H<sub>2</sub>O system (see the text for the definition of both systems). The theoretical air-H<sub>2</sub>O system is gradually getting apart from the real CO<sub>2</sub>-H<sub>2</sub>O system, as degassed mass increases (see the gray lines).

In most cases, the <sup>4</sup>He species and their various combinations with other species showed high 576 monitoring efficiencies than the other heavier species, which was attributed to the large amount of <sup>4</sup>He in 577 the CO<sub>2</sub> plume. However, it should be noted that the efficiency of one tracer is fairly dependent on the 578 action of the physical processes in plume migration. For example, if the CO<sub>2</sub> plume lost more than  $7.2 \times$ 579  $10^{-5}$  CO<sub>2</sub> cm<sup>3</sup> STP/g H<sub>2</sub>O during the degassing process, then <sup>36</sup>Ar and <sup>40</sup>Ar will be ahead of <sup>4</sup>He in the 580 monitoring well (Figure 8). Furthermore, if the diffusion process is dominant at the plume front, <sup>4</sup>He can 581 be delayed behind other heavier species in the monitoring system because of its fast dilution along the 582 583 concentration gradient, which has been demonstrated in other artificial injection tests (Carrigan et al., 1996; Sanford et al., 1996). Therefore, the detection efficiency in terms of its role as an early warning for 584  $CO_2$  leakage is dependent only on the leakage conditions, and it cannot be said that any single tracer is 585 superior to others. 586

587

#### 4.1.2.2 Influence of density of CO<sub>2</sub> on the monitoring efficiency

Free-phase  $CO_2$  forms a  $CO_2$ -rich plume in a shallow aquifer after a leakage event. The partitioning behavior of noble gas is different in pure water and in  $CO_2$ -rich plume owing to an increase in the molecular interactions inside a plume with a high  $CO_2$  density (Warr et al., 2015). Until now, the air– H<sub>2</sub>O partitioning coefficient has been adopted for describing the distribution of noble gas tracers in a COrich system instead of the  $CO_2$ -H<sub>2</sub>O partitioning coefficient, owing to an absence of previous studies (Gilfillan et al., 2008; LaForce et al. 2014; Zhang et al. 2011). This situation caused uncertainty and errors

in quantitative calculations. For example, Zhou et al. (2012) could not determine a clear reason for mismatches of heavier noble gases to the analytical model, i.e., whether it was caused by the absence of a proper coefficient (i.e., the  $CO_2$ –H<sub>2</sub>O partitioning coefficient) or by the influence of another physical process (i.e., sedimentary excess Kr; see Figure 12 in that paper). Then, Warr et al. (2015) pointed out the problem; specifically, the partitioning behavior of a noble gas tracer in a  $CO_2$ -rich system differs remarkably from that in an air-H<sub>2</sub>O water system.

Under CO<sub>2</sub> saturation conditions, i.e., 3.97 kg/m<sup>3</sup> (see Table A.1), the partitioning ratio of <sup>4</sup>He 600 species to CO<sub>2</sub> water increased by 2.26%, but those of others decreased, e.g., by up to -7.32% for <sup>40</sup>Ar and 601 -23.05% for <sup>84</sup>Kr (Table 3). Figure 9 shows the percent change in noble gas concentration with a 602 solubility-controlled process both in an air-H<sub>2</sub>O system (pink-colored) and in a CO<sub>2</sub>-H<sub>2</sub>O system (blue-603 colored). The CO<sub>2</sub>-rich plume will have a lower amount of heavier isotopes compared with that in the air-604 605 H<sub>2</sub>O system, owing to the difference in water/gas partitioning coefficients between an air-H<sub>2</sub>O system and  $CO_2$ - H<sub>2</sub>O system (see the definition of  $\delta$  partitioning in Table 3). This trend may affect the quantitative 606 607 evaluation of the fate of CO<sub>2</sub> (Table 3). However, this effect looks relatively minor in this specific case, 608 owing to the wide distribution of initial values (i.e., blue stars), which cancels out this trend (Figure 8).

**Table 3** Percent differences between water/gas partitioning coefficients of noble gases (top) and percent differences between noble gas concentrations in a  $CO_2$ -H<sub>2</sub>O system and an air-H<sub>2</sub>O system (below). The latter was calculated for various degassing events.

	<sup>4</sup> He	<sup>40</sup> Ar	<sup>84</sup> Kr
a		····· % <sup>†</sup> -····	
Spartitioning	2.26	-7.32	-23.05
Degassing		0⁄~ ¶	
amount		70	
0	0	0	0
1.8	2.83	-2.09	-3.94

4.5	7.21	-5.15	-9.57
7.2	11.79	-8.12	-14.86

- 612 <sup>†</sup>percent difference of water/gas partitioning coefficient of noble gases (unit: mM/atm) between the two
- 613 systems,  $(k_{i,CO_2 H_2O} k_{i,air H_2O})/k_{i,air H_2O} \times 100$ . Partitioning coefficients can be found in Table
- 614 A.1 of Appendix A.
- 615 <sup>‡</sup>total degassed mass in an open system (unit:  $\times 10^{-7}$  cm<sup>3</sup> STP/g).
- 616 percent difference of concentration (unit: cm<sup>3</sup> STP/g) between the two systems, ( $C_{i,CO_2 H_2O}$  –

617 
$$C_{i,air-H_2O})/C_{i,air-H_2O} \times 100.$$

618

![](_page_36_Figure_9.jpeg)

619

**Figure 9.** Percent change in noble gas concentration from its initial composition in a  $CO_2$  plume undergoing a degassing process for both air–H<sub>2</sub>O and  $CO_2$ –H<sub>2</sub>O systems. The air–H<sub>2</sub>O system was depicted using partitioning coefficients from the NIST chemistry webbook of Sander (2017) (pinkcolored), and the  $CO_2$ –H<sub>2</sub>O system was based on coefficients from Warr et al. (2015) (blue) assuming a  $CO_2$ -saturated state (i.e., 3.97  $CO_2$  kg/m3) at a temperature of 14.3°C, altitude of 580 m, and water column of 10 m (Table A.1). The theoretical air–H<sub>2</sub>O system will deviate from the real  $CO_2$ –H<sub>2</sub>O system

because molecular interactions increase with  $CO_2$  concentration. Note that the difference between the air-H<sub>2</sub>O (pink) and  $CO_2$ -H<sub>2</sub>O (blue-colored) systems is smaller than the difference between the closed (dotted) and open (line) systems (see the text for definition of each system). The noble gas composition of the initial plume was from Gilfillan et al. (2017).

630

#### 4.1.2.3 Optimal tracers for detecting CO<sub>2</sub> leakage

Although the <sup>4</sup>He tracer appears efficient in tracing the CO<sub>2</sub> leakage owing to its large 631 compositional difference between the two reservoirs (Table 2), the wide variation in ascending  $CO_2$ 632 possibly hinders the accurate quantitative estimation. At the Weyburn site, the variation in <sup>4</sup>He 633 distribution was 58.2% (1 $\sigma$ ) for CO<sub>2</sub> (Table 1), and this was attributed to the interaction between CO<sub>2</sub> and 634 crustal fluids that reside in the deep reservoir (Gilfillan et al., 2017). The scattered distribution of initial 635 values can add errors and uncertainty to the evaluation and tracing of the fate of CO<sub>2</sub> (Wilkinson et al., 636 2010). This issue can be resolved by using atmospheric noble gases such as <sup>20</sup>Ne, <sup>36</sup>Ar, and <sup>84</sup>Kr, which 637 have been adopted as they ignore wide variations due to interactions with reservoir fluids (Ma et al., 638 2009). 639

640 In Figure 10, an anomaly of atmospheric noble gas is depicted with the various physical processes, 641 where clear separation between the mixing (i.e., the light gray zone) and degassing processes (i.e., the 642 dark gray zone) implies the applicability of the tracers to constraining the physical processes. However, 643 when they are plotted together in Figure 11 to explain the evolution of the  $CO_2$  plume, the anomalies driven by the two processes (i.e., mixing and degassing) overlap each other within analytical error ranges 644 645 and therefore one cannot differentiate one from the other. Moreover, the wide scatters of the initial values (i.e. blue stars) significantly overrode the post-anomaly of the tracers, which was contrary to the results 646 647 obtained in the case where <sup>4</sup>He is combined with other components (see Figure 8, relative to Figure 11). Other combinations of atmospheric elements also exhibited similar problems, as illustrated in 648

Supplementary Figure 1. Though atmospheric components have been demonstrated to distinguish 649 physical processes in many studies and have proved useful (Ballentine et al., 1991; Battani et al., 2000; 650 Ma et al., 2009; Zhou et al., 2012), in this particular case, they cannot be used to determine the physical 651 anomalies (Figure 11 and Supplementary Figure 1). This simulation indicated that <sup>4</sup>He and its 652 combinations with heavier species are the most powerful proxies for understanding the fate of a CO<sub>2</sub> 653 654 plume, as they have more distinguishable compositional changes under physical interactions than other combinations. The overall result suggests that it is mandatory to check whether the post-anomaly of a 655 656 selected tracer (i.e. degassing-mixing trend) cancels out the heterogeneous distribution of reservoir gases.

![](_page_38_Figure_2.jpeg)

657

Figure 10. Percent change in noble gas composition in the initial CO<sub>2</sub> plume under various physical
processes. BGs (i.e., pink cross symbols) present the concentrations of shallow aquifer samples, and ASW
is the air saturated water in a local groundwater condition (i.e., green diamond; see Table 1). Note that the

![](_page_39_Figure_1.jpeg)

distinction between mixing processes (i.e. the light gray zone) and solubility-controlled processes (i.e. the

dark gray zone) is apparent. All the measured data were from Gilfillan et al. (2017).

662

663

665

666 concentration. All the measured data were from Gilfillan et al. (2017). In this scenario, the initial plume is 667 unstable and, therefore, undergoes a degassing process rapidly until stabilization in a shallow 668 groundwater system is achieved (i.e., the gray line) (see Figure 1). Then, the degassed plume undergoes a 669 dilution process when it mixes with local groundwater (i.e., the blue lines). Note that the degassing and 670 mixing process overlap each other and cannot be separated from the other. Furthermore, see that the wide 671 distribution of the initial values (i.e., blue stars) cancels out the post anomaly.

Figure 11. Evolution of a CO<sub>2</sub> plume under physical processes in terms of atmospheric noble gas

#### 4.2 Identifying leakage hot spots using noble gas fingerprint in an actual CO<sub>2</sub> leakage site

Accidental leakage from a deep reservoir into a shallow system can happen through various pathways, such as an injection well, an abandoned well, or natural conduits (e.g., faults or poor caprock integrity), possibly exposing  $CO_2$  at various points in shallower groundwater. This suggests that the actual  $CO_2$  leakage we would observe in a shallow aquifer is complicated and cannot be easily discussed with a noble gas fingerprint.

![](_page_40_Figure_2.jpeg)

678

Figure 12. He–Kr plot after CO<sub>2</sub> leakage into a shallow groundwater is allowed to occur; the plot was
modified form Ju et al. (2019). The samples were lying on the new dilution line of the mixing trajectory
between a partially degassed CO<sub>2</sub> plume and a background concentration (i.e. the pink/purple diamond).
In other words, the samples were a mixture of the degassed CO<sub>2</sub> plume and the local groundwater. Note

that the leakage spot (0 m; i.e., red circles) exhibited the largest variation in the mixing trajectory as the CO<sub>2</sub> plume interacted with the degassed CO<sub>2</sub> plume. The other samples were collected at a certain distance from the leakage point, and they exhibited a smaller variation.

686 The actual  $CO_2$  leakage can complicate the noble gas distribution as ascending  $CO_2$  takes various paths into a shallow aquifer. However, we can still trace the CO<sub>2</sub> leakage by systematic and scientific 687 688 investigation. In the environmental forensic world, when attempting to trace a source spot in close 689 proximity, one can make use of an evolutionary pattern of a source compound (Morrison, 1999). 690 Similarly, from the artificial injection tests, we also observed an evolutionary path of a leaked plume where the noble gas composition undergoes a series of modification steps owing to physical processes (i.e. 691 degassing-mixing trend in Figure 8). This specific trend also has been shown in the artificial CO<sub>2</sub> 692 injection test in a shallow aquifer (Ju et al., 2019) and natural CO<sub>2</sub> production site (Zhou et al., 2005). 693

In terms of the evolutionary path, another representative result was demonstrated in Figure 12 694 695 following an artificial injection of CO<sub>2</sub> into shallow aquifer (Ju et al., 2019) In Figure 12, the monitoring 696 data is plotted on the gradual trend between the degassing-end (i.e. the intercept between black line and 697 dotted line) and the local groundwater (i.e. diamond symbols) (Ju et al., 2019). The trend indicated that 698 the degassed plume was gradually mixed with local groundwater after the solubility-controlled process 699 was swiftly finished. Here, the samples from a leakage spot (i.e., the red circles) exhibit the widest 700 variation on the mixing line, which stretches from the degassing-end. This was attributed to the 701 monitoring well, which was located at the closest point to a leakage spot and therefore efficiently captured the CO<sub>2</sub> plume shortly after the degassing-end. There is a clear distinction between the source 702 703 spot (i.e. wide variation) and the other monitoring wells besides the leakage spot (i.e. narrow variation 704 around the local BG), suggesting that, with this trend, a leaking point with an actual CO<sub>2</sub> leakage event can potentially be identified. Therefore, the evolutionary path of the leaked plume elucidated in this study 705 706 can be an important fingerprint when monitoring CO<sub>2</sub> leakage using a noble gas tracer.

#### 707 5 Conclusions

Although noble gas tracers have been proven useful in characterizing the fate of  $CO_2$  in many aspects of  $CO_2$  storage research, they have not been extensively used for monitoring  $CO_2$ , i.e., to trace leaked  $CO_2$  in shallow groundwater. Furthermore, noble gas application has been limited to the monitoring of natural analogue sites and CCS pilot test sites, suggesting we still need to link previous findings to an actual  $CO_2$  leakage event. Therefore, this study evaluated the applicability of noble gas tracers to monitoring actual  $CO_2$  leakage from a deep reservoir into a shallow groundwater system.

First, an artificial injection test was performed in a shallow-depth aquifer system to observe and verify observations from previous researches. Here, we used inert gas tracers (i.e.,  $SF_6$  and noble gases) to separate and explain the physical interactions that determine the fate of the leaked plume. During the tests, the fate of the leaked plume was a function of a solubility-controlled process (i.e., degassing) and a mixing process. This result was consistent with those of Ju et al. (2019) and Zhou et al. (2005), suggesting that the two processes are primarily responsible for the fate of the leaked plume in a shallow system.

While the artificial injection tests identified the major interactions responsible for the fate of the 721 722 leaked plume, the applicability of tracers to actual leakage monitoring work at a CCS site has not been 723 explored. Therefore, repeated simulations were conducted based on data from a real CO<sub>2</sub> injection site (the Weyburn and Midale oil fields) to predict the fate and evolutionary path of a leaked plume that we 724 would observe with actual  $CO_2$  leakage. This simulation indicated that <sup>4</sup>He and its combinations with 725 726 heavier species are useful monitoring parameters for evaluating the fate of a leaked plume. In contrast, in 727 terms of early warning of a leakage, none of the tracers were superior to the others, as their detection 728 efficiencies appear to be dependent on the leakage conditions and therefore under the control of physical 729 processes. Furthermore, the high density of the  $CO_2$  of a leaked plume possibly adds uncertainty and

errors to the quantitative evaluations. However, the wide scatter of the initial values (i.e., noble gas 730 variation in produced CO<sub>2</sub>) significantly overrides the effect of the other uncertainties in monitoring CO<sub>2</sub> 731 leakage at this specific site. This suggests the homogeneity of the initial plume is significantly important 732 733 in terms of the monitoring efficiency using noble gas tracers. Overall, the results of this study revealed 734 that a noble gas can be applied not only for qualitative purposes (i.e., leaking detection), but also for 735 identifying mass allocations and the evolutionary path of a leaked plume in a shallow aquifer system. Most importantly, the leaked plume has a unique evolutionary path in terms of noble gas tracers, which 736 are expected to act as important fingerprints for tracing a leakage spot as complex mechanisms affect the 737 738 CO<sub>2</sub> plume distribution.

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#### 748 Appendix A. Analytical solutions for the fate of CO<sub>2</sub> plume

When degassing happens in a closed system, the exsolved gas will still remain in the aquifer system, and an equilibrium will be achieved at the interfaces between the bubbles and remaining plume. In this situation, one-step partitioning determines the noble gas distribution, which is defined by Henry's constant, such as in Eq.(A.1) and Eq. (A.2) (Ballentine et al., 2002):

753 
$$\left(\frac{A}{B}\right)_{(g)} = \left(\frac{A}{B}\right)_{(l)} \times \alpha$$
 Eq. (A. 1)  
754  $\alpha = \frac{\frac{r_A}{\phi_A}K_A}{\frac{r_B}{\phi_B}K_B}$  Eq. (A. 2)

755 Here:

756  $\left(\frac{A}{R}\right)_{(g)} = A$  and B ratio in exsolved bubbles, where A and B are different noble gases;

757  $\left(\frac{A}{R}\right)_{(l)}$  = the composition of A and B remaining in the dissolved phase;

758  $\alpha$  = partitioning coefficient for gas/liquid system;

759  $K_A, K_B$  = Henry's constant for A and B (Table A.1);

760 **Table A.1** Partitioning coefficients of noble gas tracers in pure water and CO<sub>2</sub> saturated water.

	He	Ne	Ar	Kr
		mM	/atm	
Pure water <sup>†</sup>	0.389	0.482	1.711	3.211
$\text{CO}_2$ saturated water <sup>‡</sup>	0.398	-	1.586	2.471

761 <sup>†</sup>NIST chemistry webbook of Sander (2017) at temperature of  $14.3^{\circ}$ C.

<sup>†</sup>calculated according to Warr et al. (2015) where  $CO_2$  saturated water (3.97 kg/m<sup>3</sup>) was assumed in

temperature of  $14.3^{\circ}$ C, altitude of 580 m and water column of 10 m.

764  $r_A$ ,  $r_B$  = dissolved phase activity coefficients for A and B; and

- 765  $\phi_A$ ,  $\phi_B$  = gas phase fugacity coefficients for A and B.
- A Rayleigh equation was used to explain the degassing procedure in the open system, where gas bubbles continuously strip off the dissolved noble gas from the aquifer system at the gas/liquid interfaces of the exsolved bubbles until the end of the process (Ballentine et al., 2002; Zhou et al., 2005; Holland and Gilfillan, 2013).

770 
$$(\frac{A}{B})_{(l)} = (\frac{A}{B})_0 \times f^{\alpha - 1}$$
 Eq. (A.3)

- 771  $\left(\frac{A}{B}\right)_{(l)}$  = The composition of A and B remaining in the aquifer
- 772  $\left(\frac{A}{B}\right)_{(0)}$  = The composition of A and B in initial CO<sub>2</sub> plume

### 773 f = Fraction of element B remaining in dissolved plume

The plume is diluted by the diffusion process in the aquifer system, along the concentration gradient between the plume and local groundwater. In dominance of this process, the distribution of noble gas element is defined by the diffusion coefficient and the elapsed time since the leakage event happened, such as in Eq. (A. 4) (Fetter, 1999):

778 
$$C = \frac{(C_0 - C_i)V}{(4\pi t)^{3/2} \sqrt{D_x D_y D_z}}$$
Eq. (A. 4)

779 Here:

780 C = maximum concentration of element in leaked plume at a specific time, t (cm<sup>3</sup> STP/g);

- 781  $C_0 = initial$  concentration of element in the leaked plume (cm<sup>3</sup> STP/g);
- 782  $C_i$  = concentration of element in aquifer before leakage (cm<sup>3</sup> STP/g);

- V = volume of the initial leaked plume (cm<sup>3</sup>); 783
- t = elapsed time since leakage (s); and784
- $D_x$ ,  $D_y$ ,  $D_z$  = diffusion coefficients of element for x, y, z direction, respectively (cm<sup>2</sup>/s) (Table A.2). 785

Table A.2 Diffusion coefficients of noble gas tracers in water 786

	He	Ne	Ar <sup>‡</sup>	Kr	
		cm	2/s		
Pure Water <sup>†</sup>	6.12×10 <sup>-5</sup>	3.23×10 <sup>-5</sup>	1.94×10 <sup>-5</sup>	1.36×10 <sup>-5</sup>	
Jähne et a	al. (1987) at te	mperature c	of 14.3°C.		
Wise and	Houghton (19	966) at temp	perature of 1	4.3°C.	

- <sup> $\dagger$ </sup>Jähne et al. (1987) at temperature of 14.3°C. 787
- <sup> $\ddagger$ </sup>Wise and Houghton (1966) at temperature of 14.3°C. 788

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## **Highlights**

- Gas-charged water was injected into an aquifer to demonstrate CO<sub>2</sub> leakage
- Noble gases identified physical processes involved in the fate of gas-charged water
- Based on the injection tests, the fate of leaked CO<sub>2</sub> was studied using noble gases
- The evolutionary path of leaked CO<sub>2</sub> was depicted using noble gases for Weyburn site
- The evolutionary path can act as a fingerprint for identifying a leakage hot spot

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#### **Declaration of interests**

 $\boxtimes$  The authors declare that they have no known competing financial interests or personal relationships that could have appeared to influence the work reported in this paper.

The authors declare the following financial interests/personal relationships which may be considered as potential competing interests:

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