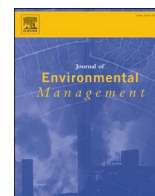


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Research article

Economic Model Predictive Control for optimal struvite recovery

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ABSTRACT

Resource recovery from municipal wastewater has been a prime focus for a decade. Although several recovery processes already exist in the market today, the high cost of material, inherent disturbance in the influent quality, lack of real time monitoring of critical parameters, and lack of a robust automation system may result in sub-optimal performance. This work attempts to construct a model based predictive control for optimal operation of a struvite recovery unit in a full scale WRRF. A multi-parameter based predictive control has been developed by implementing an Economic Model Predictive Controller (EMPC) for optimal dosing of magnesium hydroxide in a struvite recovery unit. The EMPC used customized objective function for real-time optimization of performance and economical parameters of the crystallization unit. The effectiveness of the proposed EMPC controller is verified through tests conducted on the Benchmark Simulation Model No. 2 (BSM2d.). The results obtained from the simulator-based evaluation of EMPC demonstrate a significant improvement in resource recovery at reduced operational costs. The economic advantages of implementing an EMPC compared to proportional and constant magnesium dosage has also been enumerated.

1. Introduction

The Wastewater Treatment Plants (WWTPs) are consistently upgrading their processes to include more recovery operations and conform to its new terminology as Water Resource Recovery Facilities (WRRFs) (Regmi et al., 2019). Innovative treatment technologies are being implemented to enable better processing and disposal of the wastewater sludge. Struvite precipitation is one such process that gained popularity over the past decade (Jensen et al., 2015). Struvite (magnesium ammonium phosphate hexahydrate) has been of special interest due to its potential applicability as a slow-release fertilizer. The use of slow-release fertilizers (such as struvite) can offset the environmental deterioration caused by the excessive use of mineral-based fertilizers and eventually play a vital role in the modern eco-friendly sustainable agricultural sector (Rahman et al., 2014). Moreover, depleting reserves of mineral phosphorus also encouraged to explore alternative renewable sources (Cordell and Bennett, 2011). Struvite can be precipitated by adding Magnesium Hydroxide ($Mg(OH)_2$) to a stream rich in ammonium (NH_4^+) and phosphate (PO_4^-) ions. In a typical WRRF, these nutrient-rich streams can be found in the supernatants of the anaerobic-digested sludge (Rahaman et al., 2008). Therefore, a struvite recovery unit is often installed after the dewatering unit to recover the Nitrogen (N) and

Phosphorus (P) before recycling the supernatant back to the biological reactors.

Although the struvite precipitation process was designed with an aim of generating a commercially marketable slow-release fertilizer, in most WRRFs it is often used as a strategy to prevent the scale formation along the sludge train and eventually reduce the maintenance cost (b). Several social, economic, and technological reasons can be attributed to their inability to produce a commercially marketable product. The prices of $Mg(OH)_2$ and the energy required to operate fluidized bed reactors result in higher production costs. The fluctuations in the nutrient concentrations of the influent supernatant and the resulting inability to maintain a stable product quality add to the problem. These disturbances can often result in suboptimal performance of the crystallizers designed for struvite production. Instrument Control and Automation (ICA) offers several control strategies for ensuring optimal operation of various treatment processes. Although several works have already presented the advantages of introducing a struvite crystallization unit in a WRRF (Mbamba et al., 2016), we could not find control strategies for optimal operation of struvite production process. Several experimental studies have been conducted for the purpose of identifying the optimal operating conditions for struvite precipitation (Forrest et al., 2008; Jia et al., 2017). However, a continuous full-scale struvite production

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the digestates entering the struvite recovery unit. The current work focuses specifically on the struvite recovery process alone. Therefore, improvements in the unit processes preceding the struvite recovery unit, as well as modeling inadequacies associated with the integration of the struvite recovery unit in the updated BSM2d, are not addressed. Within the aforementioned limits, the steady-state operating conditions of the struvite unit and the mass balances for N and P occurring in the struvite recovery unit are presented as Fig. 4S in the supplementary material.

2.2. Economic Model Predictive Control

The Model Predictive Control (MPC) is a commonly used strategy for optimal control. In a conventional MPC, the outputs y_{k+i} are predicted for the finite prediction-interval N_p using a mathematical model and the control moves ($u_k, u_{k+1}, \dots, u_{k+N_c-1}$) are calculated for a control horizon N_c to minimize an objective function J . The objective function for an error minimization control is calculated by a weighted square average of the control error and change in manipulated variable. In Equation (2) the term k and i are the time indices along the prediction horizon, r_{k+i} is the reference value (set-point), w_{SP} and $w_{\Delta u}$ are weights for the control error and change in manipulated variables respectively. Penalizing the control error by increasing the values of w_{SP} in the objective function keeps the output variable close to the reference value. Increasing the value of $w_{\Delta u}$ suppresses rapid changes in the manipulated variables and makes the controller more sluggish.

$$J(u_k) = \sum_{i=0}^{N_p-1} r_{k+i} - y_{k+i}^2 w_{SP} + \sum_{i=0}^{N_c} \Delta u_{k+i-1}^2 w_{\Delta u} \quad (2)$$

The Economic model predictive control (EMPC) is a variant of the MPC where the cost function includes process performances, energy savings or overall economic profit rather than the quadratic error between the reference and measured variable. The successful implementation of EMPC for optimal operation of various wastewater treatment processes can be found in literature (Zeng and Liu, 2015; Zhang and Liu, 2019). The cost function used for EMPC control in the struvite recovery process is defined in Equation (3) – (5).

$$J = \sum_{i=0}^{N_p-1} -P_{\text{Recovery}} \cdot \Phi_{\text{STR}} + M_{\text{Mg}} \cdot \Phi_{\text{Mg}} \quad (3)$$

where

$$P_{\text{Recovery}} = (PO_{4,\text{IN}} - PO_{4,\text{EFF}}) \cdot Q_{\text{IN}} \quad (4)$$

$$M_{\text{Mg}} = Q_{\text{Mg}} \cdot MW_{\text{Mg}} \cdot \rho_{\text{Mg}} \quad MW_{\text{Mg}} = 24.3 \text{ kg/kmol} \quad \rho_{\text{Mg}} = 25 \text{ kmol/m}^3 \quad (5)$$

Where $PO_{4,\text{EFF}}$ is the phosphate concentration in the overflow from the crystallizer, $PO_{4,\text{IN}}$ is the phosphate concentration in the influent, Q_{IN} is the flowrate of supernatant to the crystallizer and P_{Recovery} is the real-time estimate for the mass of phosphate recovered as struvite. Q_{Mg} is the volumetric flowrate of magnesium hydroxide, MW_{Mg} is the molecular weight of Mg and ρ_{Mg} is the molar density of the magnesium hydroxide solution. φ_{STR} is the market price of recovered phosphorus in the form of struvite and φ_{Mg} the market price of magnesium hydroxide used in struvite production.

2.3. Prediction model

The control action of the MPC is taken based on the prediction made by the model. Therefore, adequate model describing the relation between input and output variables are imperative (Revollar et al., 2018). Struvite production in the crystallizer depends on several variables which introduce non-linear interdependencies in process chemistry. Physio-chemical models such as PHREEQC can adequately explain the process of struvite precipitation (Daneshgar et al., 2019). However, the

lack of suitable sensors for measuring the concentration of every ionic species during the precipitation process poses a significant challenge in the use of mechanistic models for the purpose of automation and control. With the advent of data-driven models, various system identification techniques exist that can be used to establish a statistically significant correlation between the input and output variables of the process.

2.3.1. State-space representation

The discrete form of the linear state-space model is presented in Equations (6) and (7).

$$x_{k+1} = Ax_k + B \begin{bmatrix} u_k \\ d_k \end{bmatrix} \quad (6)$$

$$y_k = Cx_k + D \begin{bmatrix} u_k \\ d_k \end{bmatrix} \quad (7)$$

In Equations (6) and (7), x_k is the state variable at time instance k , u_k is the manipulated variable, d_k is the measured disturbance and y_k is the measured output. The list of input ($u_k = Q_{\text{Mg}}$ and $d_k = [Q_{\text{IN}} \quad PO_{4,\text{IN}}]$) and output variables $y_k = PO_{4,\text{EFF}}$ are provided in Table 1.

2.3.2. Generation of subspace identification model

Several algorithms are mentioned in literature for the purpose of identifying a linear, time-invariant, state-space model from input-output data (Verhaegen, 1994; Van Overschee and De Moor, 2012). In our work, the canonical variate analysis (CVA) approach for system identification algorithm, mentioned in (Larimore, 1990; Ljung, 1999) was used for estimating the state-space matrices of the multiple input-single output (MISO) model. The data for system identification is obtained from simulations performed in the BSM2d simulator using the dynamic influent. The n4sid function, provided as a part of the System Identification Toolbox in MATLAB is used to train the model and obtain the A, B, C and D matrices.

2.4. Control strategy

Four different scenarios, each with a different Magnesium dosing control strategy were evaluated. The base control strategy (C0) uses constant dosage of Magnesium ($Q_{\text{Mg}} = 0.13 \text{ m}^3/\text{day}$) and Sodium ($Q_{\text{Na}} = 0.10 \text{ m}^3/\text{day}$). C0 is the default dosing strategy in the BSM2d simulator, which provides a reference point against which the basic and advanced control strategies are assessed. The second control strategy (C1) is a feed-forward controller, where the Q_{Mg} is proportional to the flow of supernatant entering the crystallizer Q_{IN} (Fig. 2a). A feed-forward proportionality constant $K_P = 0.000675$ was provided for the controller C1. Feed-forward flow-proportional control (C1) is a commonly used basic dosing control strategy adopted in most WRRFs (Ratnaweera H and Fettig, 2015). Assessing the performance of a basic control strategy helps provide an intermediate reference point to highlight the benefits of implementing an advanced optimal control. The controllers C2 and C3 are EMPC controllers described in Equations (3)–(5). In C2 the market price of struvite (φ_{STR}) and magnesium hydroxide (φ_{Mg}) are held constant during the evaluation period. In C3 the cost (φ_{STR}) and (φ_{Mg}) are chosen as time varying inputs to the EMPC

Table 1
MPC settings.

Parameter	Description	Value	Unit
T_s	Time step	15	minutes
N_p	Prediction Horizon	3	
N_c	Control Horizon	2	
u_{min}	Minimum value of Q_{Mg}	0.05	m^3/day
u_{max}	Maximum value of Q_{Mg}	0.30	m^3/day

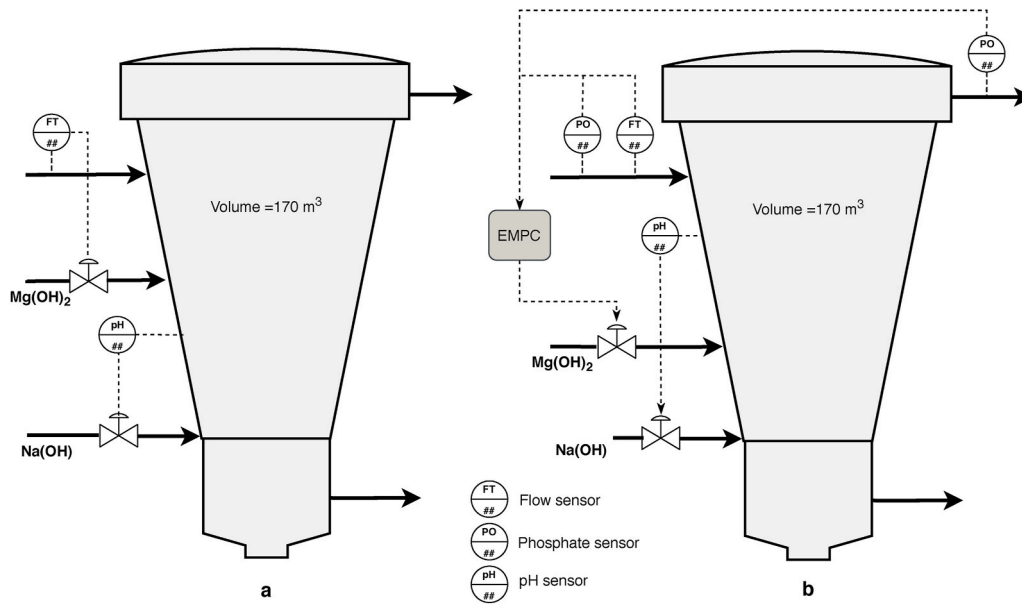


Fig. 2. Control Schematic of Struvite Crystallization Unit (a.) feed forward flow proportional control (C1) and (b.) EMPC (C2 and C3).

controller. The control strategies for C1, C2 and C3 are shown in Fig. 2 and details regarding the measured and manipulated variables are presented as Table 1S in the supplementary material. In addition to control strategies for magnesium dose prediction, an on-off pH controller was provided in C1, C2 and C3 to ensure the pH values stay above 8.1.

To study the difference between C2 and C3 control strategy (Fig. 2b.), a hypothetical scenario is considered where the cost of struvite (φ_{STR}) is changed once every 30 days. The new values of φ_{STR} are randomly selected between the range $\varphi_{STR,MIN} = 7.5$ and $\varphi_{STR,MAX} = 9.5$ in the first day of every month. The Φ_{Mg} values were held constant during the evaluation of control strategies to better understand the effects of monthly price variations on the control action of EMPC. It should be noted that the prices φ_{STR} and φ_{Mg} are mere representative values taken from literature (Solon et al., 2017) and do not reflect the exact price of struvite or magnesium hydroxide in the market.

2.5. Performance evaluation

Several standardized criteria for evaluating the performance of control strategies are reported in literature (Vanrolleghem et al., 1996). However, in this work we limit our evaluation to the parameters that are directly influenced by the struvite crystallization unit. The performance criteria used in our evaluations are explained in Equations (8)–(11).

M_{STR} (kg/day) is the average per day value for the mass of struvite produced by the crystallizer unit during the evaluation period. Equation (8) describes the calculation of M_{STR} .

$$M_{STR} (kg / day) = \frac{1}{T} \int_{245}^{609} Q_{STR}(t) \cdot X_{STR}(t) \cdot MW_{STR} \quad (8)$$

M_{Mg} is the average (kg/day) mass for Magnesium hydroxide consumed by the struvite crystallization unit.

$$M_{Mg} (kg / day) = \frac{1}{T} \int_{245}^{609} Q_{Mg}(t) \cdot MW_{Mg} \cdot \rho_M \quad (9)$$

Operational Cost Index (OCI) is a standard economic measure used to calculate the total cost (material and energy) incurred during the daily operation of a WRRF. Since this work focuses on optimizing struvite crystallization, a simpler version of the operational parameters

$Profit_{CRYST}$ was also calculated using factors that has a direct influence on the cost of the struvite crystallization unit.

$$Profit_{CRYST} = M_{STR} \cdot \varphi_{STR} - M_{Mg} \cdot \varphi_{Mg} \quad (10)$$

For the scenario with time-varying market price of struvite ($\varphi_{STR}(t)$), the method for calculating $Profit_{CRYST}$ is presented in Equation (11).

$$Profit_{CRYST} = \frac{1}{T} \int_{245}^{609} Q_{STR}(t) \cdot X_{STR}(t) \cdot MW_{STR} \cdot \varphi_{STR}(t) - Q_{Mg}(t) \cdot MW_{Mg} \cdot \rho_M \cdot \varphi_{Mg}(t) \quad (11)$$

EV_{TP} is the number of times effluent total phosphorus limits (TP = 2 gp m⁻³) are violated during the evaluation period.

2.6. Implementation in simulink platform

The simulink implementation files for the modified BSM2d simulator is available in literature (Solon et al., 2017). The basic (C1) as well as advanced (C2, C3) control strategies are constructed in the base open-loop BSM2d SIMULINK file (C0) with constant dose of magnesium. The nonlinear MPC block provided in simulink was used to construct the EMPC and configure the controller parameters for C2 and C3. Four separate files were created each with a different control strategy described as C0, C1, C2, and C3. The SIMULINK files for implementation of the EMPC control strategy in a BSM2d can be provided on request. The standard procedure executing the simulator are provided in the BSM2d simulator manual (Jeppsson et al., 2007). The following steps were applied for simulation and subsequent evaluation of the control strategies.

1. Initialize the BSM2d with the default values provided in the simulator.
2. Simulate from t = 0 to t = 300 days using the constant influent data.
3. Initialize the simulink model with the final values of the steady state simulation (using constant influent data). This allows the next simulation (with dynamic influent data) to begin at the exact position as where the steady state simulation had ended.
4. Simulate the model with the dynamic influent file for a period of 609 days (from t = 0 to t = 609 days).
5. The data from the simulations with dynamic influent file is stored in the MATLAB workspace.

6. Utilize the data recorded from $t = 245$ to $t = 609$ days to assess the performance parameters mentioned in Equations 8–11.

3. Results and discussion

3.1. System identification results

The data received from the dynamic simulation of C1 is used to develop the state-space model. The timeseries data used in the subspace identification method contains Q_{Mg} , Q_{IN} , and $PO_{4,IN}$ as model inputs and $PO_{4,EFF}$ as model output, with a time span of 609 days ($t = 0$ to $t = 609$ days) sampled at an interval of 15 min. The data is split to training data 75% ($t = 0$ to $t = 455$), which provides adequate number of data points necessary to construct a reliable model. The remaining 25% of the data is chosen as validation data ($t = 455$ to $t = 609$) which was used to confirm the ability of model to predict $PO_{4,EFF}$ in the overhead stream of struvite recovery unit. The training data is used to calibrate the model and obtain the A, B, C, and D matrices (Eqs (6) and (7)) defined in the state-space matrix.

$$A = \begin{bmatrix} 0.9914 & -0.0086 & -0.0003 \\ -0.0114 & 0.9753 & 0.1115 \\ 0.0076 & -0.0200 & 0.7998 \end{bmatrix}, B = \begin{bmatrix} -8.6 & 6.8 & 12.8 \\ 1.9 & 156.7 & -2.9 \\ 1.1 & -232.8 & -1.7 \end{bmatrix}$$

$$C = [10.141 \quad -0.044 \quad -0.002], D = [0 \quad 0 \quad 0]$$

The model is then used to predict the output for the validation data. The validation plot, showing a comparison between the validation dataset and the value predicted by the state-space model is presented in Fig. 3.

A close match is observed between the measured data and the data predicted by the model. The adequate match between the model predicted and plant data as well as the R^2 value of 0.91 demonstrate the ability of the state-space model to predict the effluent PO_{4-P} concentrations in the overhead streams from the crystallizer.

3.2. MPC settings

The choice of prediction and control horizon, limits of manipulated variables determine the performance of an MPC. Systematic procedures are explained to determine the optimal values of these tuning parameters (Lee and Yu 1994). In our case, the parameters were tuned based on experience gained from running the BSM2d simulator with steady-state as well as the dynamic weather data. The MPC parameters used in the simulations are presented in Table 1.

The time-step in the influent disturbance file, the sampling interval of data used in prediction model generation, and the logging rate of simulations results in the MATLAB workspace were set at 15 min. In order to maintain uniformity, the same value was also used as EMPC's time-step. The Q_{Mg} values in dynamic simulation using C1 strategy varies within the range $0.10 \text{ m}^3/\text{day}$ to $0.20 \text{ m}^3/\text{day}$. In the EMPC strategy, range of variations in Q_{Mg} was increased by reducing the lower

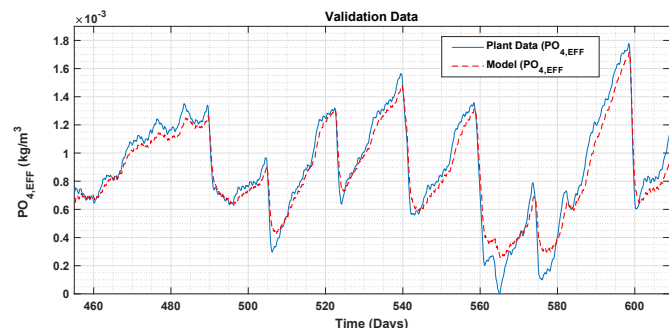


Fig. 3. System Identification, validation plots model versus simulated values.

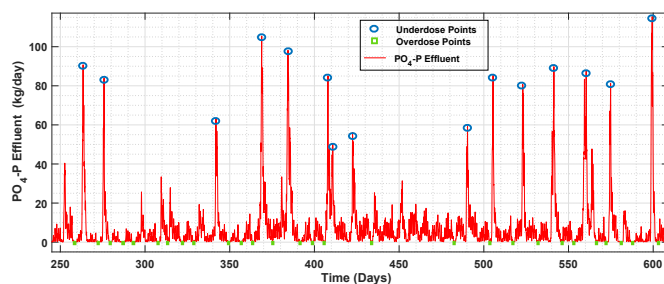


Fig. 4. Effluent PO_{4-P} from the crystallizer for constant dosing condition.

limit value of $0.1 \text{ m}^3/\text{day}$ by 50% ($-0.05 \text{ m}^3/\text{day}$) and increasing upper limit value of $0.20 \text{ m}^3/\text{day}$ by 50% ($+0.10 \text{ m}^3/\text{day}$). Therefore, the parameters u_{min} and u_{max} (Table 1) were set as $0.05 \text{ m}^3/\text{day}$ and $0.3 \text{ m}^3/\text{day}$ respectively. The steady state-simulations were used to determine the appropriate values of N_p and N_c . Step changes were provided in the values of Φ_{STR} and the performance of the EMPC was assessed by recording its ability to reach a new minimum point. At each simulation run the values of prediction and control horizon were gradually increased from a lower value $N_p = 2$ and $N_c = 1$, and the controller performance was evaluated at every step. The controller performance showed no significant change when the values were increased above, $N_p = 3$ and $N_p = 2$. Therefore, the values of prediction and control horizon were maintained at 3 and 2 respectively.

3.3. Controller performance evaluation

A quantitative assessment is necessary to compare the of the performance of various control strategies presented in Fig. 2. The waste-quality parameters of the influent and effluent streams of the struvite crystallization unit for all four strategies are utilized to generate comparison plots and calculate the performance evaluation indicators mentioned in Eqs. 8–11. The dynamic values of the soluble PO_{4-P} in the overhead flow of the struvite crystallization unit for the constant dosing scenario (C0) is presented in Fig. 4.

The benefits of introducing a struvite recovery unit in terms of improving effluent water-quality and reducing maintenance costs in WRRF is already reported in literature (Mbamba et al., 2016). However, Fig. 4 indicates that maintaining a constant magnesium hydroxide flowrate (C0) in the crystallizer would not be the most optimal dosing strategy. Several underdosing points (marked in circles) are indicated where increasing the dosage could have resulted in higher phosphorus recovery in the form of struvite. Fig. 4 also indicates overdosing points (marked in squares) where Magnesium was dosed beyond what was required.

The suboptimal performance of C0 can be attributed to two factors a. fluctuations in flowrate (Q_{IN}) b. fluctuations in influent phosphate concentrations ($PO_{4,IN}$). The flow proportional dosing control strategy (C1) partially offsets the problem of suboptimal dosing because of its ability to detect fluctuations in the flowrate of supernatant to the crys-

Table 2
Performance criteria for the three evaluated control strategies.

Performance Criteria	C0 Constant	C1 Flow Proportional	C2 EMPC
Struvite Production (kgP/day)	91.1	98.4 (8.01%)	102.49 (12.50%)
Mg Consumed (kg/day)	78.9	72.1 (-8.62%)	72.2 (-8.49%)
OCI	9105.1	9073.4 (-0.348%)	9002.1 (-1.131%)
Profit (€/day)	314.73	418.56 (33.0%)	453.33 (44.0%)
EV _{TP}	21	18 (14.2%)	9 (57.1%)

tallizer. The improvement in dosing strategy can be reaffirmed in Table 2., which indicates an increase (8.01%) in average phosphorus recovery while reducing (8.62%) the Magnesium consumption. However, the dose prediction is entirely based on the flowrate, and flow-proportional control strategy (C1) does not consider the fluctuations in the $\text{PO}_4\text{-P}$ concentrations in the influent. Therefore, suboptimal dosing is observed in situations with higher influent $\text{PO}_4\text{-P}$ fluctuations.

The EMPC predicts the dose based on the optimal value of cost function (Equation (3)). Since the dose prediction considers both flowrate as well as influent $\text{PO}_4\text{-P}$ concentrations, a better control over the recovery of phosphorus can be expected. Fig. 5 shows a more stable effluent $\text{PO}_4\text{-P}$ concentration in C2 compared to C0 and C1. The dynamic plots for Magnesium consumed, recovery percentage and mass of struvite production are presented in supplementary material. A comparison between the performance indices presented in Table 2 indicates a 12.5% increase in the average daily struvite production and an 8.5% drop in total magnesium consumption compared to the base dosing control strategy (C0).

A comparison between the control strategies in terms of overall profits for struvite production indicate a 33.01% increase for C1 and 44.03% increase for C2 when compared to the base control strategy C0. The increase in overall profits are primarily due to improvements in phosphorus recovery and a reduction in magnesium used in the crystallizer by avoiding overdosing. Apart from the increase in profits for struvite production, implementing EMPC also demonstrates fewer effluent violations in the treated effluent from WRRF (Table 2). Fewer effluent violation would imply fewer effluent penalties, which could further add to the savings.

3.4. Economic assessment of time varying cost function

The influence of introducing a time varying cost function on the effluent $\text{PO}_4\text{-P}$ concentration and the magnesium dose prediction is presented in Fig. 6.

It is observed that in situations with lower φ_{STR} , the C3 strategy predicts a lower magnesium dosage and a subsequent reduction in phosphorus recovery. The reduction in struvite prices (reflected in φ_{STR}) moved the optimal dosing point to a lower value (resulting in lower phosphorus recovery percentage) in order to generate savings on the magnesium cost. When the costs are increased, higher recovery of phosphorus (in the form of struvite) is restored. A comparison between the average (kg/day) values of struvite produced, magnesium consumed and the profits for all three control strategies in the presence of a monthly variations in struvite costs are presented in Table 3. It is observed that using costs as inputs to the EMPC controller as opposed to a constant cost function results in an additional 8.1% increment in the overall profits incurred in struvite production.

A complete list of evaluation parameters for all the three control

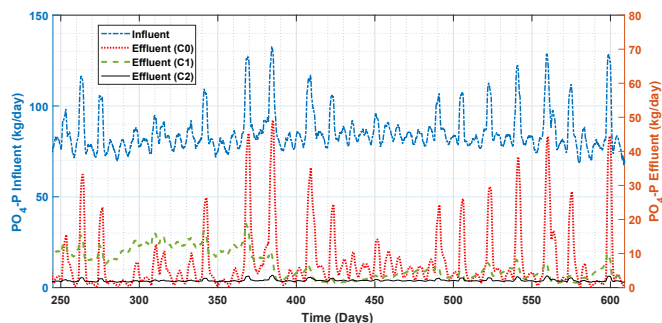


Fig. 5. A comparison between Mass flowrate of Phosphorus at the influent and effluent of struvite crystallization unit with dynamic influent data for various control strategies. A 3-day moving-average-filter is used to improve visualization.

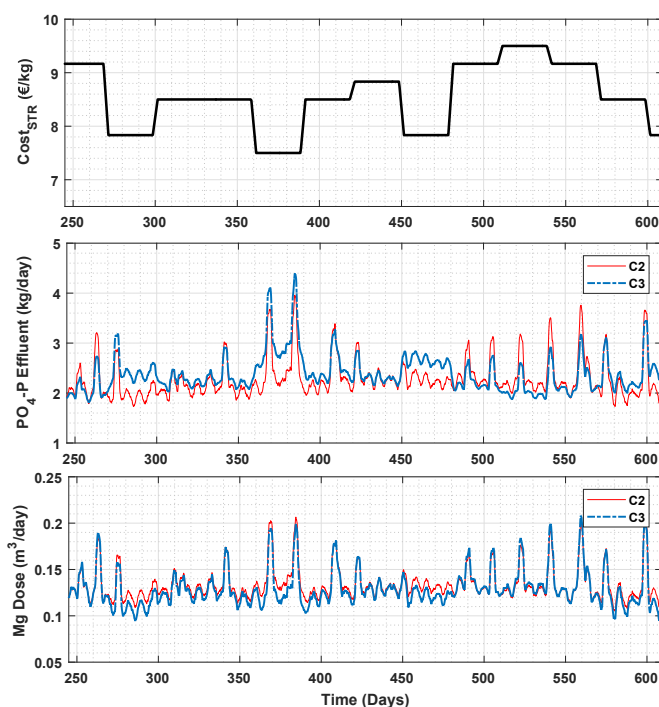


Fig. 6. A comparison between C2 and C3 control strategy a. Market price for struvite during the evaluation period. b. Mass flowrate of phosphorus in the crystallizer effluent c. Volumetric flowrate of magnesium. A 3-day moving-average-filter is implemented in b. and c. to improve visualization.

Table 3

Economic Assessment for time varying struvite costs.

Economic Parameters	C0	C1	C2	C3
Struvite Production (kgP/day)	91.1	98.4	102.5	102.1
Mg Consumed (kg/day)	78.9	72.1	72.2	70.9
Profit (€/day)	291	388	413	447

strategies are presented in the supplementary material. The EMPC strategy also provides a convenient alternative to adjust the controller parameters based on the price factors without the need for retuning the controller parameters. Although the work primarily defines the optimization problem based on two parameters a.) Cost of Struvite b.) Cost of Magnesium, EMPC also provides the possibility of including more optimization parameters (Shaddel et al., 2019a) as long as a reliable correlation between the manipulated variables and the measured parameters exist.

4. Conclusion

The work demonstrates the advantages of a multi-parameter-based control strategy for optimal dosing of magnesium in a struvite crystallization unit. A systematic procedure for developing a data-driven model for establishing a correlation between the input and output parameters of the struvite crystallization process has also been presented. Performance evaluation of the EMPC indicates a significant improvement in the overall profits when compared to both constant as well as flow proportional dosing strategy. The operational flexibility of the EMPC controller was demonstrated by its ability to conveniently switch between multiple operating conditions by using the market price of struvite and magnesium as their input variables. Although the work demonstrated the optimization strategy based merely on two economic parameters (magnesium dose flowrate and phosphorus recovery); the flexible nature of the EMPC allows the possibility of introducing

multiple evaluation criteria in the objective function. The multi-parameter based optimal control approach using a data-driven model presents an opportunity to further improve the process operation and achieve better product quality by deploying the optimal dose strategy based on criteria such as struvite crystal dimensions, settling properties etc.

Declaration of competing interest

The authors declare that they have no known competing financial

interests or personal relationships that could have appeared to influence the work reported in this paper.

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Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.jenvman.2020.111830>.

List of Variables

OCI	Operational Cost Index
EV _{TP}	Total Effluent Violations
N	Nitrogen
P	Phosphorus
Mg	referring to Magnesium Hydroxide
N _P	Prediction Horizon (time – step)
N _C	Control Horizon (time – step)
J	Objective Function
x _k	State variable at discrete time instance k
u _k	Manipulated variables at time instance k
y _k	Measured variables at time instance k
T _s	Time step (Days)
k	Time instance
r	Reference set-point
PO _{4, IN}	Concentration of soluble phosphates in the influent supernatant. (kg m ⁻³)
PO _{4, EFF}	Concentration of soluble phosphates in the overhead flow from crystallizer. (kg m ⁻³)
M _{STR}	Mass of struvite produced (kg /day)
M _{Mg}	Mass of Magnesium consumed in Crystallizer (kg /day)
Profit _{CRYST}	Profit generated by operating the crystallizer (€/day)
φ _{STR}	Market price of struvite (€/kg)
φ _{Mg}	Market price of Magnesium hydroxide (€/kg)
X _{STR}	= Concentration of struvite in the Struvite flow (kmol/m ³)
Q _{Mg}	Flowrate of Magnesium Hydroxide (m ³ /day)
Q _{Na}	Flowrate of Sodium hydroxide (m ³ /day)
Q _{IN}	Flowrate of supernatant to the crystallizer (m ³ /day)
P _{Recovery}	Mass of phosphorus recovered from crystallizer (kg/ day)
MW _{STR}	Molecular Weight (of Phosphorus) in Struvite (31 kg P/mole)
MW _{Mg}	Molecular Weight of Magnesium (23 kg/mole)
ρ _{Mg}	Molar density of Weight of Magnesium (25 kmol/m ³)

References

- Cordell, D., Bennett, E., 2011. A broken biogeochemical cycle. *Nature* 478, 29–31.
- Crutchik, D., Morales, N., Vázquez-Padín, J.R., Garrido, J.M., 2017. Enhancement of struvite pellets crystallization in a full-scale plant using an industrial grade magnesium product. *Water Sci. Technol.* 75 (3), 609–618.
- Daneshgar, S., Buttafava, A., Capsoni, D., Callegari, A., Capodaglio, A.G., 2018. Impact of pH and ionic molar ratios on phosphorous forms precipitation and recovery from different wastewater sludges. *Resources* 7 (4), 1–22.
- Daneshgar, S., Vanrolleghem, P.A., Vaneckhaute, C., Buttafava, A., Capodaglio, A.G., 2019. Optimization of P compounds recovery from aerobic sludge by chemical modeling and response surface methodology combination. *Sci. Total Environ.* 668, 668–677.
- Durand, H., Ellis, M., Christofides, P.D., 2016. Economic model predictive control designs for input rate-of-change constraint handling and guaranteed economic performance. *Comput. Chem. Eng.* 92, 18–36.
- Ellis, M., Liu, J., Christofides, P.D., 2017. Brief Overview of EMPC Methods and Some Preliminary Results in Economic Model Predictive Control: Theory, Formulations and Chemical Process Applications. Springer International Publishing, Switzerland.
- Forrest, A.L., Fattah, K.P., Mavinic, D.S., Koch, F.A., 2008. Optimizing struvite production for phosphate recovery in WWTP. *J. Environ. Eng.* 134 (5), 395–402.
- García, C.E., Prett, D.M., Morari, M., 1989. Model predictive control: theory and practice-A survey. *Automatica* 25 (3), 335–348.
- Gernaey, K.V., Jeppsson, U., Vanrolleghem, P.A., Copp, J.B., 2014. Scientific and Technical Report No. 23. In: Benchmarking of Control Strategies for Wastewater Treatment Plants. IWA Publishing, London, U.K report.
- Hasanlou, H., Torabian, A., Mehrdadi, N., Kosari, A.R., Aminzadeh, B., 2019. Performance comparison of predictive controllers in optimal and stable operation of wastewater treatment plants. *Pollution* 5 (4), 821–838.
- Jensen, P.D., Yap, S.D., Boyle-Gotla, A., Janoschka, J., Carney, C., Pidou, M., Batstone, D. J., 2015. Anaerobic membrane bioreactors enable high rate treatment of slaughterhouse wastewater. *Biochem. Eng. J.* 97, 132–141.
- Jeppsson, U., Pons, M.N., Nopens, I., Alex, J., Copp, J.B., Gernaey, K.V., Rosen, C., Steyer, J.P., Vanrolleghem, P.A., 2007. Benchmark simulation model no 2: general protocol and exploratory case studies. *Water Sci. Technol.* 56 (8), 67–78.
- Jia, G., Zhang, H., Krampe, J., Muster, T., Gao, B., Zhu, N., Jin, B., 2017. Applying a chemical equilibrium model for optimizing struvite precipitation for ammonium recovery from anaerobic digester effluent. *J. Clean. Prod.* 147, 297–305.

- Kazadi-Mbamba, C., Flores-Alsina, X., Batstone, J.D., Tait, S., 2016. Validation of a plant-wide phosphorus modelling approach with minerals precipitation in a full-scale WWTP. *Water Res.* 100, 169–183.
- Larimore, W.E., 1990. Canonical variate analysis in identification, filtering, and adaptive control. 29th IEEE Conference on Decision and Control 2, 596–604.
- Ljung, L., 1999. *System Identification: Theory for the User*. PTR Prentice Hall, New Jersey, USA, ISBN 978-0136566953.
- Lee, J.H., Yu, Z.H., 1994. Tuning of model predictive controllers for robust performance. *Comput. Chem. Eng.* 18 (1), 15–37.
- Nopens, I., Benedetti, L., Jeppsson, U., Pons, M., Alex, J., Copp, J.B., Gernaey, K.V., Rosen, C., Steyer, J., Vanrolleghem, P.A., 2010. Benchmark Simulation Model No 2: finalisation of plant layout and default control strategy. *Water Sci. Technol.* 62 (9), 1967–1974.
- O'Brien, M., Mack, J., Lennox, B., Lovett, D., Wall, A., 2011. Model predictive control of an activated sludge process: a case study. *Contr. Eng. Pract.* 19 (1), 54–61.
- Ostace, G.S., Cristea, V.M., Agachi, P.Ş., 2012. Cost reduction of the wastewater treatment plant operation by MPC based on modified ASM1 with two-step nitrification/denitrification model. *Comput. Chem. Eng.* 11, 2469–2479.
- Van Overschee, P., De Moor, B.L., 2012. *Subspace Identification for Linear Systems: Theory - Implementation - Applications*. Springer Science & Business Media, ISBN 978-1-4613-0465-4. <https://doi.org/10.1007/978-1-4613-0465-4>.
- Rahaman, M.S., Ellis, N., Mavinic, D.S., 2008. Effects of various process parameters on struvite precipitation kinetics and subsequent determination of rate constants. *Water Sci. Technol.* 57 (5), 647–654.
- Rahman, M.M., Salleh, M.A.M., Rashid, U., Ahsan, A., Hossain, M.M., Ra, C.S., 2014. Production of slow release crystal fertilizer from wastewaters through struvite crystallization - a review. *Arabian Journal of Chemistry* 7 (1), 139–155.
- Ratnaweera, H., Fettig, J., 2015. State of the art of online monitoring and control of the coagulation process. *Water* 7, 6574.
- Regmi, P., Miller, M., Jimenez, J., Stewart, H., Johnson, B., Amerlinck, Y., Volcke, E.I.P., Arnell, M., Garcia, P.J., Maere, T., Torfs, E., Vanrolleghem, P.A., Miletic, I., Rieger, L., Schraa, O., Samstag, R., Santoro, D., Snowling, S., Takács, I., 2019. The future of WRRF modelling - outlook and challenges. *Water Sci. Technol.* 79 (1), 3–14.
- Revollar, S., Álvarez, H., Lamanna, R., Vega, P., Goldar, A., 2018. Economic model predictive control of a wastewater treatment plant using neural and fuzzy models. *Computer Aided Chemical Engineering* 43, 1237–1242.
- Shaddel, S., Ucarb, S., Andreassen, J.P., Østerhus, S.W., 2019a. Engineering of struvite crystals by regulating supersaturation – correlation with phosphorus recovery, crystal morphology and process efficiency. *Journal of Environmental Chemical Engineering* 7 (1), 102918.
- Shaddel, S., Bakhtiyari-Davijany, H., Kabbe, C., Dadgar, F., Østerhus, S.W., 2019b. Sustainable sewage sludge management: from current practices to emerging nutrient recovery technologies. *Sustainability* 11 (12).
- Solon, K., Flores-Alsina, X., Kazadi Mbamba, C., Ikumi, D., Volcke, E.I.P., Vaneckhaute, C., Ekama, G., Vanrolleghem, P.A., Batstone, D.J., Gernaey, K.V., Jeppsson, U., 2017. Plant-wide modelling of phosphorus transformations in wastewater treatment systems: impacts of control and operational strategies. *Water Res.* 113, 97–110.
- Vanrolleghem, P.A., Vaneckhaute, C., 2014. Resource recovery from wastewater and sludge, modelling and control challenges. In: *IWA Specialist Conference on Global Challenges for Sustainable Wastewater Treatment and Resource Recovery*.
- Vanrolleghem, P.A., Jeppsson, U., Carstensen, J., Carlsson, B., Olsson, G., 1996. Integration of wastewater treatment plant design and operation - a systematic approach using cost functions. *Water Sci. Technol.* 34 (3–4), 159–171.
- Verhaegen, M., 1994. Identification of the deterministic part of MIMO state space models given in innovations form from input-output data. *Automatica* 30 (1), 61–74.
- Zeng, J., Liu, J., 2015. Economic model predictive control of wastewater treatment processes. *Ind. Eng. Chem. Res.* 54 (21), 5710–5721.
- Zhang, A., Liu, J., 2019. Economic MPC of wastewater treatment plants based on model reduction. *Water* 7 (10), 1–21.