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1 **Capacitive and non-capacitive faradaic charge storage**

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9 **ABSTRACT**

10 This article aims to offer a critical overview of selected literature on capacitive and non-
11 capacitive faradaic charge storage. It is particularly relevant to the concept of
12 pseudocapacitance that is generally described as a result of fast surface **faradaic** processes. In
13 general, faradaic processes represent electron transfer reactions at the interface between an
14 electrode and its contacting solid or liquid electrolyte phase that is able to accept or donate
15 electrons. Obviously, not all faradaic processes can be associated with pseudocapacitance.
16 The question is how to differentiate pseudocapacitance related faradaic charge storage from
17 the others. Therefore, attempts have been made to apply the band model for semiconductors
18 to account qualitatively for the origin of pseudocapacitance. **Capacitive** and **non-capacitive**
19 faradaic processes are then proposed to define and differentiate different charge storage
20 mechanisms in supercapacitor and battery. On the other hand, the unequal electrode
21 capacitance approach and the use of Ca²⁺ in aqueous electrolytes are discussed in relation
22 with enhanced energy capacity of supercapacitors. In addition, the principle of supercapattery
23 as a hybrid device is explained with recent literature examples.

24 **Key words:** Capacitive charge storage; Faradaic process; Supercapacitor; Supercapattery;
25 Unequal electrode capacitance.

1 **1. Introduction**

2 Since the beginning of human civilisation, the use of energy has been an important
3 means of survival. From burning wood to nuclear energy, the search for and the utilisation of
4 various energy forms form an important part of human history. In recent years, due to the fast
5 depletion of fossil fuel reserves and the increasing negative environmental impact of CO₂
6 emission, political and economic emphases have been placed on the rapid development of
7 alternative energy technologies, particularly through solar, wind and wave generation.
8 However, the energy derived from these renewable sources must be stored and supplied
9 efficiently in order to be considered a viable competitor to traditional non-renewable options
10 [1]. Energy storage devices including supercapacitor, battery and supercapattery are such
11 devices that are able to store charges in a fast and efficient way and hence help harvest and
12 convert renewable energy to a usable form.

13 Electrical energy can be electrochemically stored in two fundamental ways: (1) in
14 solid electrode materials relying on fast charge separation and/or chemical reactions of the
15 materials and (2) in liquid electrolytes flowing through a battery of electrochemical cells. The
16 latter is typically represented by redox flow battery. It is unique because energy storage is
17 achieved by reduction and oxidation of redox couples in different electrolytes separated by a
18 membrane and circulated in their own respective spaces [2]. However, due to the requirement
19 for storage and transport of a large volume of the electrolytes, the application for redox flow
20 batteries is limited to stationary needs at present. Great efforts have therefore been made to
21 deeply and comprehensively understand charge storage processes in solid electrode materials
22 in order to develop versatile energy storage devices (e.g. supercapacitors) and improve their
23 performance, which is also of interest of this study.

24 In general, electrical charge can be stored in the surface and/or solid phases of the
25 electrodes relying on the following storage mechanisms: double layer charging, faradaic

1 processes, or a combination of both. For instance, the charging-discharging process in an
2 activated carbon electrode is due to charge adsorption or accumulation at the interface
3 between the electrode and the electrolyte, giving rise to the electric double layer (EDL)
4 capacitance. This process is largely electrostatic and non-faradic in nature. It means that
5 ideally, no electron transfer takes place across the electrode/electrolyte interface and the
6 storage of electric charge and energy involves no chemical and physical changes inside the
7 solid phase of the electrode [3]. For the charge storage in a faradaic process, it is generally
8 accepted that large pseudocapacitance arises from electrosorption of ions accompanied by
9 surface redox reactions in which electrons transfer occurs crossing the interface of the current
10 collector and active material.

11 It is however necessary to point out both EDL and pseudocapacitive storage processes
12 are capacitive in nature. In experimental terms, they both offer rectangular cyclic
13 voltammograms (CVs) and linear (or triangular) galvanostatic charge and discharge plots
14 (GCDs) [4]. On the other hand, when the redox active material on electrodes undergoes a
15 reversible or quasi-reversible electron transfer reaction at well separated or isolated sites,
16 current peaks forms on the CV and non-linear potential (or voltage) variation occurs on the
17 respective GCDs. Such electrochemical features are the same or comparable to those of
18 recharge batteries, and should not be used for a capacitance measurement. Thus this type of
19 charge storage is recognised as a non-capacitive faradaic process here.

20 Consequently, one should not associate all these well-known faradaic processes with
21 pseudocapacitance. The question is how to differentiate pseudocapacitance related faradaic
22 charge storage from the others, namely, the non-faradaic charge accumulation in the EDL and
23 the non-capacitive battery-like behaviours of some electrode materials. Herein, the authors
24 propose to define and differentiate the aforementioned charge storage mechanisms according
25 to **Fig. 1**. Attempts have also been made to account for the origin of pseudocapacitance using

1 the band model for semiconductors. Further, the recent developments in gaining improved
 2 supercapacitor performance are introduced and discussed in terms of modifications of
 3 aqueous electrolytes and an unequal electrode capacitance approach in laboratory.

4

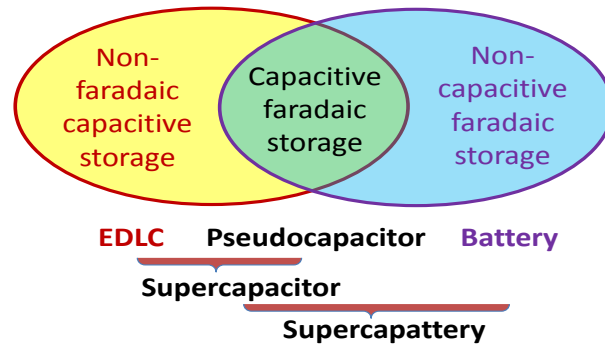
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10 **Fig. 1.** Schematic correlation between EDL capacitor, pseudocapacitor, battery and
 11 supercapattery (= hybrid of supercapacitor and battery) in terms of capacitive and faradaic
 12 charge storage processes.

13

14 In order to understand how supercapacitors store large amount of energy and discharge it
 15 for high power applications, it may be easier to start with a review on the fundamentals of the
 16 conventional capacitors that are widely used in electronic devices. In principle, the amount of
 17 charge (Q) stored is in proportion to the voltage (U) applied across the capacitor. The
 18 proportionality is called capacitance (C) which links Q and U according to Eq. (1):

$$19 \quad Q = CU \quad (1)$$

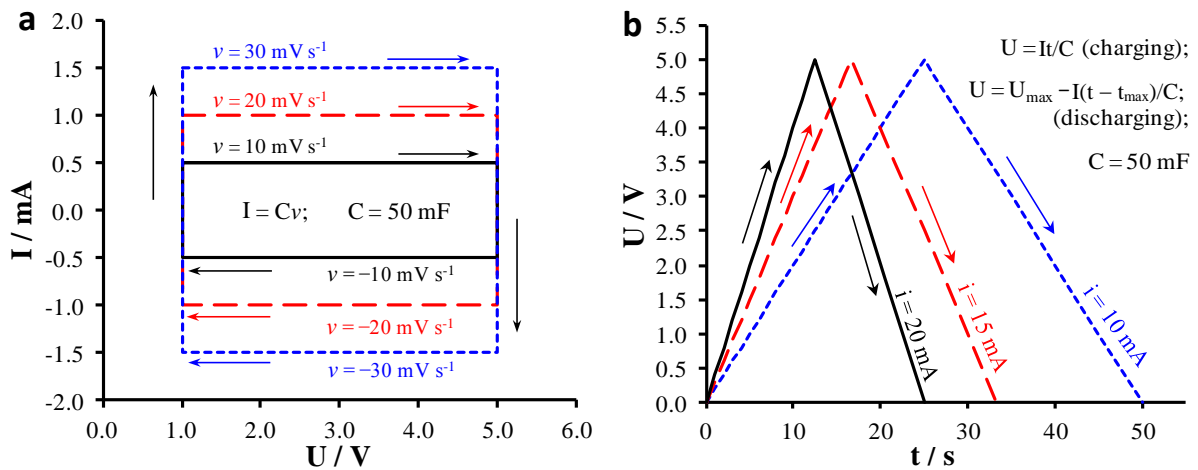
20 C is a constant determined by the dielectric constant of the dielectric medium and
 21 proportional to the ratio of the area of the electrode/dielectric interface and the separation
 22 distance between the two electrode plates of the capacitor. When the applied voltage varies
 23 linearly with time (t), i.e. $U = U^0 + vt$, where U^0 is the starting cell voltage which may be zero
 24 and v is the linear variation rate of voltage, Eq. (1) can be mathematically converted into Eq.
 25 (2), which can be further simplified to Eq. (3) by correlating the current, **I**, with v [4].

$$1 \quad \frac{dQ}{dt} = C \cdot \frac{dU}{dt} + U \cdot \frac{dC}{dt} = C \cdot \frac{dU}{dt} \quad (2)$$

$$2 \quad C = \frac{dQ}{dt} / \frac{dU}{dt} = \frac{I}{\nu} \quad (3)$$

3 Therefore, the current flowing through a capacitor is in a linear relationship with ν , but
 4 independent of U . For a constant C , Eq. (3) gives the rectangular $I - U$ plots as shown in **Fig.**
 5 2a, which is also called cyclic voltammograms or CVs. In **Fig.** 2a, the current, I , not only
 6 increases proportionally with the increase of ν , but also follows the direction of voltage
 7 variation, i.e. ν is positive when voltage increases and it is negative when voltage decreases.
 8 The CV is very useful for evaluation of capacitive behaviour of a device or electrode made
 9 from a synthetic pure or composite material.

10 In practice, galvanostatic charging-discharging (GCD) is also used to calculate the
 11 capacitance of a device or electrode material. Under a constant current, according to Eq. (3),
 12 the charging process of the capacitor reflects a constant rate of voltage increase and vice
 13 versa, the discharging relates to a voltage decrease in a constant rate. As a result, a triangular
 14 curve is observed as shown in **Fig.** 2b where the voltage of the capacitor is plotted against the



15 **Fig. 2.** (a) CVs at indicated linear variation rates of voltage and (b) GCD plots at indicated
 16 constant currents as derived from Eq. (3) for a 50 mF capacitor with $U_{\text{max}} = 5 \text{ V}$. In the GCD
 17 plots in (b), $t_{\text{max}} = U_{\text{max}} C / I$ [4].
 18

1 time during a cycle of constant current charging and discharging.

2 When the capacitor is charged, a voltage, U , will build up across the two electrodes. The
3 amount of energy (ϵ) stored and the power output (P) from the capacitor can be determined
4 through a series of calculations below. At first, the work, $d\epsilon$, done in a short time to move a
5 small quantity of charge, dQ , to be accumulated at the electrode/dielectric medium interface
6 can be calculated from Eq. (4) by considering $d\epsilon = UdQ$. If the heat loss during charging is
7 insignificant, the total energy stored in the capacitor is then determined after integration. It is
8 worth noting that a practical capacitor has always a maximum tolerable voltage, U_{\max} , beyond
9 which the dielectric or ionic medium will break down (or decompose). Thus there is a
10 maximum energy capacity, ϵ_{\max} , that can be correlated to U_{\max} and the capacitance, C , which
11 is the property of the capacitor (or electrode) material used.

$$12 \quad d\epsilon = U \cdot dQ = \frac{Q}{C} \cdot dQ \quad (4)$$

$$13 \quad \epsilon_{\max} = \int_0^Q \frac{Q}{C} dQ = \frac{1}{2} \cdot \frac{Q^2}{C} = \frac{Q \cdot U_{\max}}{2} = \frac{C \cdot U_{\max}^2}{2} \quad (5)$$

14 Secondly, it is to determine the power output, P , using the time needed to fully discharge
15 the capacitor as expressed in Eq. (6):

$$16 \quad P = \frac{\epsilon}{t} = \frac{C \cdot U^2}{2 \cdot t} \quad (6)$$

17 In fact, Eq. (6) can be further developed into Eq. (7) by taking the equivalent series
18 resistance (ESR) and the working load (R_L) into account since the ESR is the unavoidable
19 nature of an electric power source. The power transferred from the source to the load can also
20 be derived from $P = iU = i^2 R_L$.

$$21 \quad P_{\max} = \left(\frac{U_{\max}}{R_L + \text{ESR}} \right)^2 R_L = \frac{R_L \cdot U_{\max}^2}{(R_L + \text{ESR})^2} \quad (7)$$

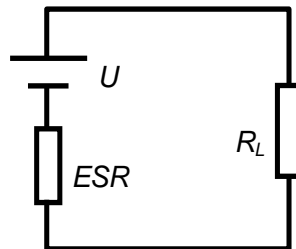
22 where $U = I \cdot (R_L + \text{ESR})$ with the current passing through the circuit shown in **Fig. 3**. It is

1 obvious that the maximum power, P_{\max} , can be reached at $R_L = \text{ESR}$, leading to Eq. (8) which
 2 shows P_{\max} is a function of U and ESR , but independent of C , although C determines the
 3 amount of energy stored in the capacitor. Furthermore, by bringing Eq. (8) into Eq. (6), the
 4 shortest discharging time, t_{\min} , can be obtained, which is practically useful and important for
 5 device design, such as supercapacitor supported systems. However, Eq. (9) has currently not
 6 gained enough recognition or attention in terms of reporting data and analyses. This is
 7 somehow unfortunate because highlighting the maximum power of supercapacitors against
 8 that of batteries without mentioning the lasting time the device can work at the high power
 9 may confuse or even mislead readers and customers who are not well informed.

$$10 \quad P_{\max} = \frac{\text{ESR} \cdot U^2}{(\text{ESR} + \text{ESR})^2} = \frac{U^2}{4 \cdot \text{ESR}} \quad (8)$$

$$11 \quad t_{\min} = \frac{C \cdot U^2}{2 \cdot P_{\max}} = \frac{C \cdot U^2}{2U^2/(4 \cdot \text{ESR})} = 2 \cdot C \cdot \text{ESR} \quad (9)$$

12



13

14

15 **Fig. 3.** The electric circuit for derivation of P_{\max} and t_{\min} (cf. Eq. (7) - (9)). R_L is the resistance
 16 of the working load, U and ESR are the voltage and the equivalent series resistance of the
 17 power source, respectively.

18

19 **2. Non-faradaic capacitive storage**

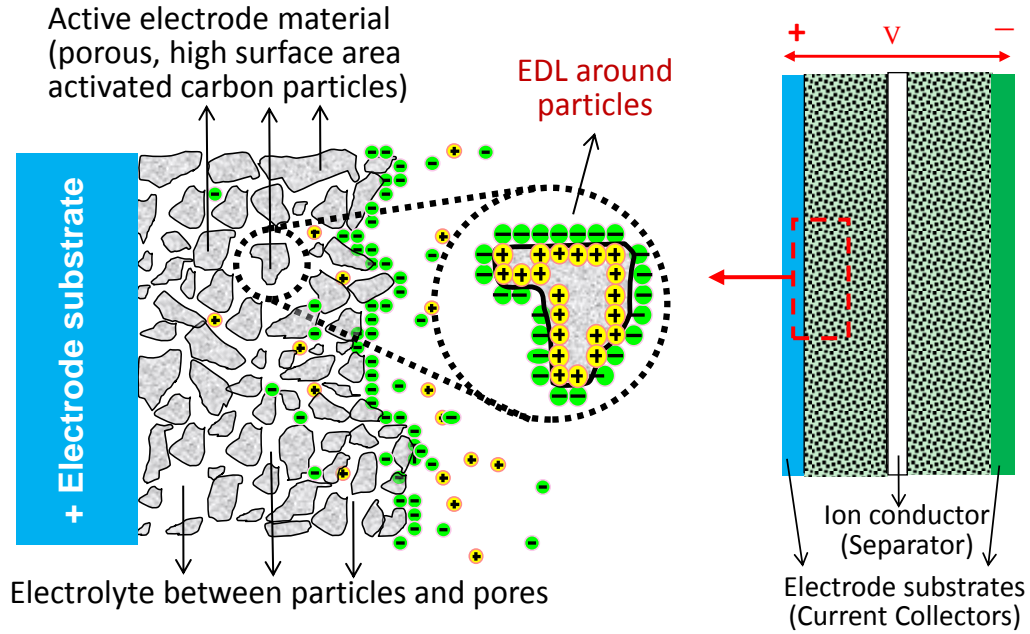
20 The capacitance of a conventional capacitor typically ranges between $10^{-6} - 10^{-2}$ F,
 21 therefore the energy stored in the capacitor is too small for meaningful practical uses. For

1 example, for a 50 mF capacitor with an applied voltage of 100 V, the energy stored is only
2 250 J. Hence, in recent years, supercapacitors, also known scientifically as electrochemical
3 capacitors, become an important development in the field of energy storage and conversion.
4 The capacitance of commercial supercapacitors can commonly reach to $10^2 - 10^4$ F. However,
5 this huge difference in capacitance does not change the fact that a supercapacitor is still a
6 capacitor. There is no doubt that the behaviour of a supercapacitor should also be governed
7 by all the equations discussed in the previous section and be the same as those in **Fig. 2**,
8 showing the rectangular CVs and triangular GCD plots.

9

10 2.1. Supercapacitors with double layer capacitance

11 EDL capacitors are the first generation supercapacitors in which charge storage occurs in
12 the electric double layer at the electrode/electrolyte interface and relies mainly on charge
13 separation. Although this storage mechanism is the same as that in the traditional electrolytic
14 capacitors, the specific capacitance ($C_s, \text{F g}^{-1}$) increases drastically by taking advantages of
15 the high porosity and large specific surface area ($\text{m}^2 \text{g}^{-1}$) of the active electrode materials, e.g.
16 activated carbon. **Fig. 4** illustrates the displaced ions in the electrolyte in the interconnected
17 pores of the electrode and the balancing charges (i.e. excess of electrons or holes) on the wall
18 surfaces of the pores that are formed between the packed activated carbon particles.
19 **Ass**uming that the electrode/electrolyte interface has true capacitance of $0.1 - 0.3 \text{ F m}^{-2}$ and
20 the specific surface area of activated carbons is $1000 \text{ m}^2 \text{g}^{-1}$, the specific capacitance, C_s , of
21 activated carbon can be calculated to range from 100 to 300 F g^{-1} . However, in many cases,
22 the specific capacitance of activated carbons is usually about 100 F g^{-1} [5]. The cause is
23 largely because the high porosity and specific surface area make activated carbons weaker
24 and less conducting. The other issue is that not all the internal surface area, such as those of
25 the wall of micro-pores, can be accessed by ions in the activated carbon for charge storage.



1

2 **Fig. 4.** Schematic illustration of charge storage mechanism in an EDL capacitor using porous
 3 and high surface area activated carbon particles as the electrode.

4

5 Therefore, nanomaterials, such as carbon nanotubes (CNTs) and graphenes, have been
 6 suggested as a good solution to solve the problems [6-8]. In addition to the extra high specific
 7 surface area and the construction of three dimensional structures, CNTs and graphene can
 8 also benefit the electron conduction through carbon structures and the ion conduction through
 9 the liquid electrolyte contained in the carbon structures [9].

10

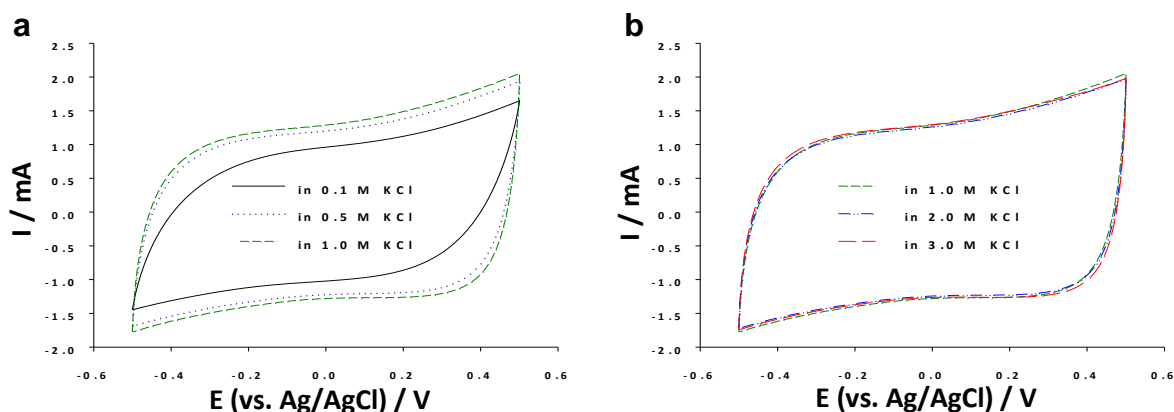
11 In particular, CNTs have been widely studied and recognised as suitable materials for
 12 applications in supercapacitors with the acknowledgement of the novel structure, narrow pore
 13 size distribution, low resistivity and high mechanical strengths [10-13]. Comparing with the
 14 porous activated carbon in the upper bound, CNTs have exhibited higher capacitance, e.g.
 15 102 F g⁻¹ for multi-walled CNTs [14], and 180 F g⁻¹ for single-walled CNTs [15]. It has also
 16 been reported that a single-walled CNT based supercapacitor showed a promising power
 17 capability of 20 kW kg⁻¹ with a maximum energy capacity of around 7 Wh kg⁻¹ at 0.9 V in a
 solution of 7.5 N KOH [15]. On the other hand, factors that affect the performance of CNT

1 based supercapacitors have been extensively researched from the aspects of structural
2 properties (e.g. diameter, length and pore size), graphitisation by heating and modification via
3 chemical activation, functionalization and surface treatment [6]. Among these, it was found
4 that boiling CNTs in a mixture of concentrated acids was one of the most effective methods
5 to modify CNT surfaces and introduce functional groups which play an important role on the
6 capacitance improvement [16, 17]. However, effects of the electrolytes on the capacitance of
7 supercapacitors have attracted relatively less attention [18-20]. It is acknowledged that
8 cations, anions and pH of the electrolyte may all affect the performance of a particular
9 electrode material. In this paper, CNTs and activated carbon electrodes are investigated in
10 correlation with the concentration and nature of ions, temperature, and the CNT surface
11 functional groups. The results are particularly interesting, confirming different affinities of
12 cations in the electrolyte (i.e. Ca^{2+} and K^+) towards the oxy-groups on CNT surfaces and
13 workability of this type of supercapacitors at temperatures below $-60\text{ }^\circ\text{C}$.

14

15 2.2. Effects of electrolyte

16 In the experiment, the effect of the electrolyte concentration on the electrochemical
17 behaviour was investigated by performing cyclic voltammetry in various KCl aqueous
18 solutions using a 5 mm dia. graphite disc electrode coated with a thin layer of activated
19 carbon (Haycarb, loading: 0.2 mg or 1.0 mg cm^{-2}) as the working electrode. A graphite rod
20 was used as the counter electrode and the Ag/AgCl couple used as the reference electrode.
21 The resulting CVs are shown in **Fig. 5**. These results agreed to certain extent with some
22 reported observations in literature that EDL capacitance increased with the increase of the
23 electrolyte concentration [21, 22], i.e. the CV current kept increasing until the concentration
24 of the KCl solution reached to 1.0 M (see **Fig. 5a**). Interestingly, the CVs observed with
25 further increasing the concentration to 3.0 M had shown insignificant changes in current as



1
2 **Fig. 5.** (a,b) CVs of the Haycarb carbon electrode (loading: 1 mg cm^{-2}) in KCl aqueous
3 solutions with different concentrations as indicated. Potential scan rate: 100 mV s^{-1} .

4
5 shown in **Fig. 5b**. It was likely that the active sites on the surface of Haycarb carbons were
6 saturated by the ions in the electrolyte while recording the previous CVs and became
7 inaccessible even though the ion concentration was significantly increased.

8 The capacitance improvement from the surface modification with functional groups is well
9 demonstrated by the significant current increase in the CVs recorded in 1.0 M KCl using a
10 6.5 mm dia. graphite disc electrode coated with acid-treated CNTs (**Fig. 6b**), in comparison
11 with those of as-received CNTs (**Fig. 6a**). It is acknowledged that using concentrated acids (a
12 mixture of H_2SO_4 and HNO_3 with 3:1 v:v in current case) to treat raw CNTs can introduce
13 oxygen-containing groups to the CNT surfaces, such as carbonyl, carboxyl and hydroxyl
14 groups or simply oxy-groups [23]. These functional groups not only improve the
15 hydrophilicity of the CNTs, but also enhance the overall charge storage performance [24].
16 The pair of broad peaks on the CV of **Fig. 6b** indicates the oxy-groups on the surfaces of the
17 acid-treated CNTs had undergone a reversible redox or faradaic reaction. Since the CV with
18 the broad peaks still remains fairly rectangular, it can still be regarded as being capacitive.
19 Thus, the acid-treated CNTs exhibited a much higher specific capacitance of 60 F g^{-1} than
20 that of the as-received CNTs (9.1 F g^{-1}), because the charge storage process of the former

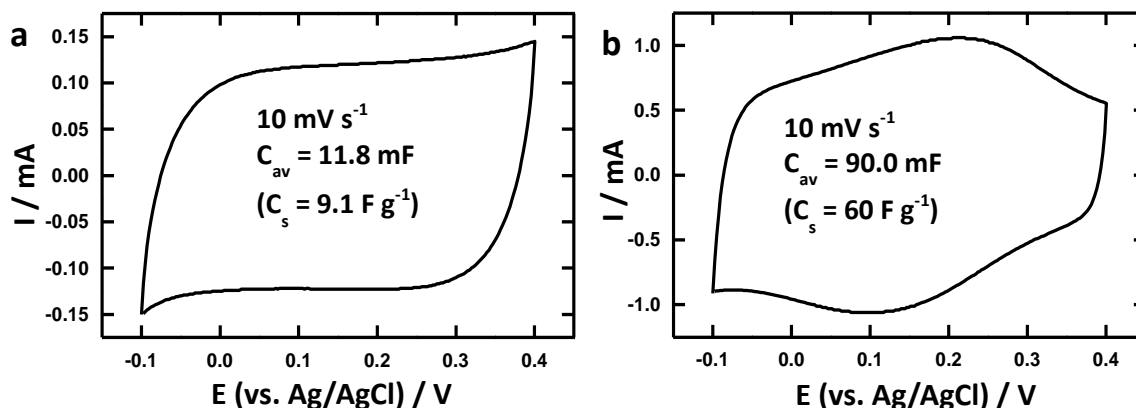
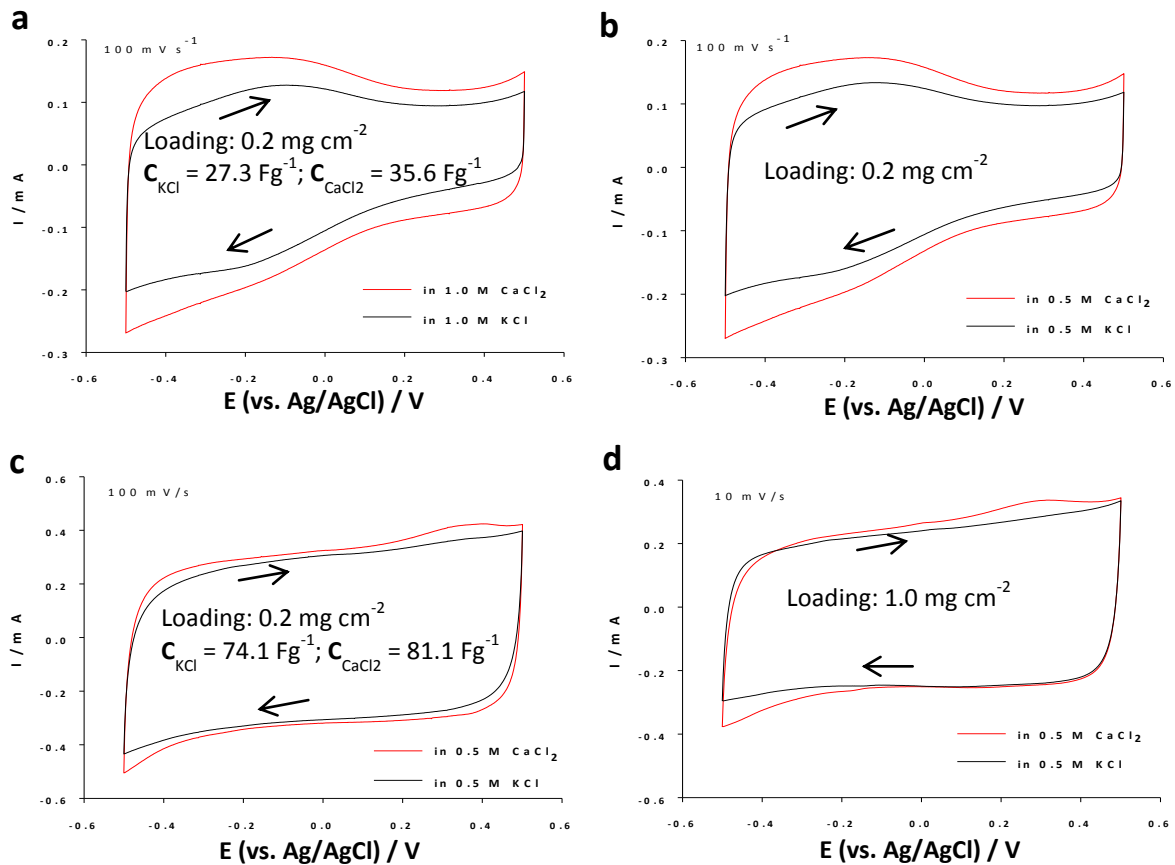


Fig. 6. CVs of (a) as-received CNT (1.3 mg) and (b) acid-treated CNT (1.5 mg) in 1.0 M KCl aqueous solution with indicated electrode capacitance averaged over the potential range (C_{av}) and specific capacitance (C_s). Potential scan rate: 10 mV s^{-1} .

involved both EDL capacitance and pseudocapacitance. It is worth mentioning that **Fig. 6b** shows that the increased charge storage occurs mostly in the middle of the potential window. This means that in a symmetrical capacitor, the increased charge capacity would be utilised at low voltages and hence contribute little to the energy capacity. It would be more meaningful to use such acid-treated CNTs or activated carbon in an asymmetrical supercapacitor so that the charge storage can increase at higher cell voltages to give rise to larger energy capacity. In such cases, the increased charge storage capacity can be further exploited together with the unequal electrode capacitance strategy as will be discussed in the later section.

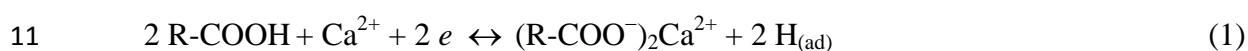
The influence of cations in the electrolyte on capacitance was also investigated by recording CVs in CaCl_2 and KCl solutions, respectively. It was particularly interesting to observe that the CVs of acid-treated CNTs recorded in the CaCl_2 solutions generally exhibit greater currents than those in the KCl solutions (see **Fig. 7a** and **b**). These differences could be attributed to the greater affinity of the Ca^{2+} ions than K^+ towards the oxy-groups on the CNT surfaces [25]. In fact, it has been mentioned in some early studies [26, 27] that the so-called Calcium Ionophore A23187 or Antibiotic A23187 has high selectivity for binding and



1
 2 **Fig. 7.** CVs of (a,b) acid-treated CNT recorded in (a) 1.0 and (b) 0.5 M solutions of CaCl_2
 3 (red curves) and KCl (black curves) [25], and of (c,d) Haycarb carbon both recorded in 0.5 M
 4 solutions of CaCl_2 (red curves) and KCl (black curves). Note that the electrode loading and
 5 scan rate are different and respectively indicated along with some of the capacitance values.
 6 Arrows indicate the direction of the potential scan. The CNTs were treated using the same
 7 method as those in **Fig. 6**, but in a recent batch [25].

8
 9 transporting the Ca^{2+} ion over other cations, such as Na^+ , K^+ and Mg^{2+} ions in biological
 10 systems. Therefore, if we could interpret this high Ca^{2+} ion selectivity of A23187 as the
 11 various oxygen containing groups in the ionophore molecule formed a Ca^{2+} ion binding
 12 site/cavity as illustrated in **Fig. 8a**, the unique interaction between Ca^{2+} and the CNT surface
 13 oxy-groups can be similarly explained in the current case. As schematically illustrated in **Fig.**
 14 **8b**, it can be assumed that the oxy-groups on CNT surfaces have high selectivity or affinity

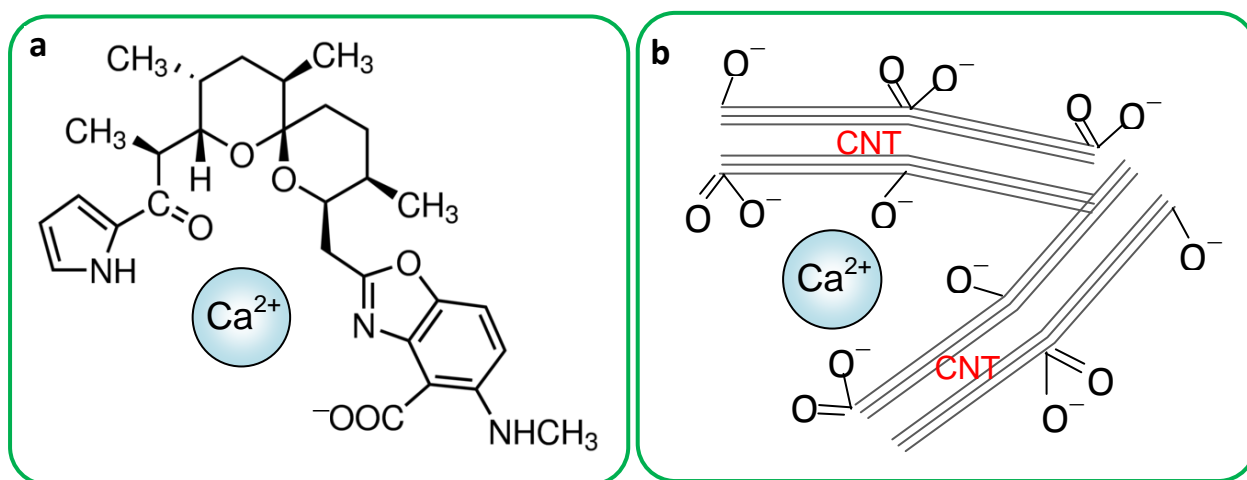
1 for Ca^{2+} ions. This assumption is in agreement with many previous studies involving
2 interactions between CNTs and Ca^{2+} ions [26-29]. It was also reported that according to
3 molecular dynamic simulation, the interaction between the carboxylate group on CNTs and
4 Ca^{2+} ions are more favourable over K^+ and Na^+ ions [28]. As a result of the greater affinity of
5 the surface oxy-groups with Ca^{2+} than with K^+ , about 30% capacitance increase was observed
6 as derived from the CVs (red curves) in **Fig. 7a** and **b**. Moreover, in an experimental study,
7 as-prepared CNTs (which must contain surface oxy-groups) were demonstrated to be
8 effective scaffold materials for osteoblast proliferation and bone formation, thanks to partly
9 the ability of the CNTs to conduct Ca^{2+} currents [29]. This means the structural arrangement
10 of the oxy-groups on the CNT surfaces are suitable for binding Ca^{2+} via Reaction (1) below.



12 In addition, the fact that each Ca^{2+} ion has two positive charges could be another
13 important cause for the increase of the specific capacitance. To compare a 1:1 type electrolyte
14 with a 1:2 type, e.g. KCl vs. CaCl_2 , a simple way was adopted in this work to halve the
15 concentration of the latter, i.e. 1.0 M KCl vs. 0.5 M CaCl_2 . It is obvious that the CV current
16 observed in 0.5 M CaCl_2 (red curve in **Fig. 7b**) was greater than that observed in 1.0 M KCl
17 (black curve in **Fig. 7a**), leading to a higher specific capacitance. It is noticeable that the CNT
18 electrode was much more sensitive to replace KCl with CaCl_2 than to the doubled electrolyte
19 concentration as the concentration change (from 1.0 to 0.5 M) had a fairly small influence on
20 the CV current and shape. This is indicative of the charge (or ion) storage in the electrode
21 being determined mainly by the available sites on the CNT surface for ion sorption, instead of
22 the number of ions in the electrolyte [25].

23 However, when similar investigations were carried out using a Haycarb carbon electrode,
24 the greater current previously observed in CaCl_2 solutions became insignificant (see the
25 unpublished results shown in **Fig. 7c** and **d**). This is because there was much less oxy-groups

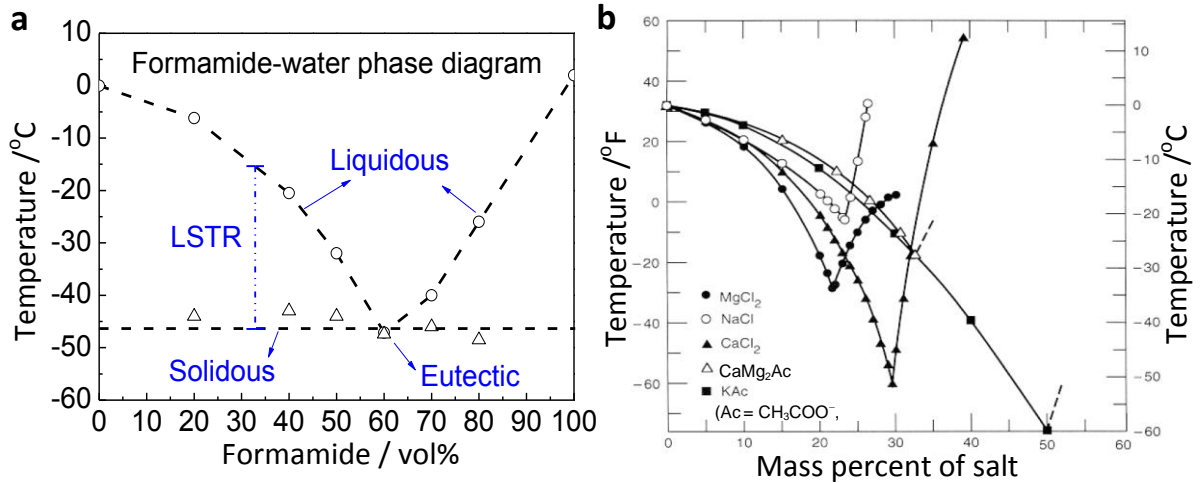
1 in the Haycarb carbons and the binding cavity formed between the carbon particles may not
2 be compatible with the Ca^{2+} ion in terms of size and shape.



3
4
5 **Fig. 8.** Schematic illustration of the binding of a Ca^{2+} ion by the oxy-groups in the cavity
6 formed (a) in the Calcium Ionophore A23187 molecule, and (b) in between the acid-treated
7 CNTs [25].

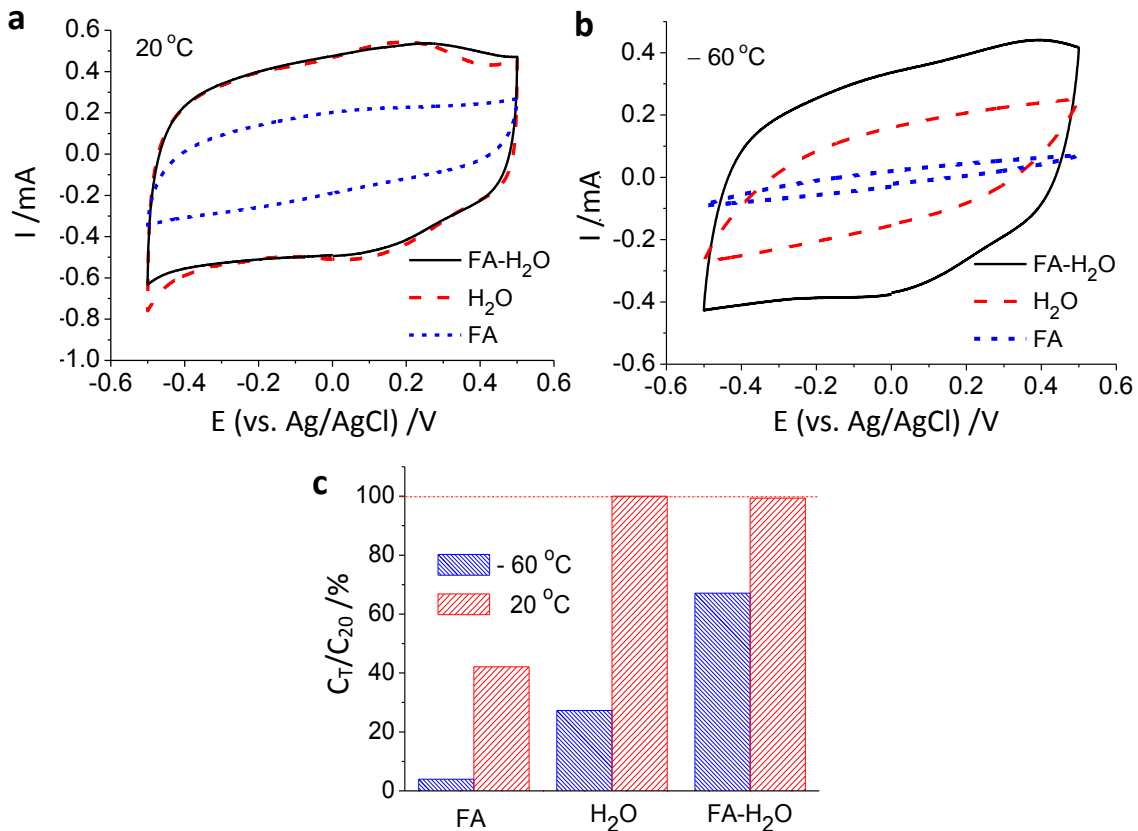
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9 On the other hand, for sub-zero temperature applications, organic electrolytes are
10 commonly used [30-32], but they have lower conductivity and are more expensive than
11 aqueous electrolytes. Mixing water with an additive may lead to low temperature benefits.
12 The binary phase diagram of water and formamide (FA) is shown in **Fig. 9a** with a eutectic
13 temperature of $-46\text{ }^{\circ}\text{C}$ [25]. The binary phase diagrams of water and some simple salts are
14 presented **Fig. 9b**, showing eutectic temperature below $-50\text{ }^{\circ}\text{C}$ on the $\text{CaCl}_2\text{-H}_2\text{O}$ curve. Thus,
15 by dissolving CaCl_2 into the $\text{FA-H}_2\text{O}$ mixture, a novel organoaqueous electrolyte was
16 prepared and proven to be able to work at temperatures below $-60\text{ }^{\circ}\text{C}$ [25].

17 **Fig. 10a** and **10b** compare the CVs of the CNT electrode measured in different
18 electrolytes at $20\text{ }^{\circ}\text{C}$ and $-60\text{ }^{\circ}\text{C}$, respectively. It can be seen that the solution of CaCl_2 in FA
19 is not a good electrolyte, but addition of FA into water does not affect very much the
20 electrochemical behaviour. Particularly, **Fig. 10b** confirms the $\text{CaCl}_2\text{-FA-H}_2\text{O}$ mixture to be



1

2 **Fig. 9.** (a) The formamide-water phase diagram. The dashed lines are presented as a vision
 3 guide [25]. (b) Phase diagrams of CaCl_2 , MgCl_2 , NaCl , CaMg_2Ac_6 (CMA), and KAc , $\text{Ac} =$
 4 CH_2COO^- [33].



5

6 **Fig. 10.** (a,b) CVs and (c) C_T/C_{20} ($= 100 \times \text{capacitance at designated temperature} / \text{capacitance}$
 7 at 20°C) of CNT electrode at (a) 20°C and (b) -60°C in the CaCl_2 solution of FA (1.0 M),
 8 H_2O (2.0 M) and mixed FA- H_2O (1:1, v:v, 2.0 M). Potential scan rate: 100 mV s^{-1} [25].

1 very good for low temperature uses. **Fig. 10c** presents the capacitance retention of the CNT
2 electrode as derived from the rectangular CVs in **Fig. 10a** and **10b**. At 20 °C, the measured
3 specific capacitance, C_s , was almost the same in $\text{CaCl}_2\text{-H}_2\text{O}$ (108.3 F g⁻¹) and $\text{CaCl}_2\text{-FA-H}_2\text{O}$
4 (107.6 F g⁻¹), whereas at -60 °C, C_s in $\text{CaCl}_2\text{-FA-H}_2\text{O}$ was still 72.7 F g⁻¹ (67% capacitance
5 retention), which is more than double of the value measured in $\text{CaCl}_2\text{-H}_2\text{O}$. Hence, it can be
6 concluded that the $\text{CaCl}_2\text{-FA-H}_2\text{O}$ mixture is an excellent electrolyte for capacitive charge
7 storage in partially oxidised CNTs at sub-zero-temperatures.

8

9 **3. Capacitive faradaic charge storage**

10 Charge storage in pseudocapacitive materials involves electron transfer reactions and
11 hence the reduction or oxidation changes in the electrode materials, which are also referred to
12 as faradaic reactions or processes. However, not all faradaic processes can contribute to
13 pseudocapacitive behaviours. Despite the electron transfer reactions in a rechargeable battery
14 or a fuel cell are also faradaic in nature, the respective current-voltage relations in these
15 electrochemical devices differ significantly from that in a capacitor [9]. Such energy storage
16 and discharge can be regarded as non-capacitive faradaic processes. The performance
17 difference between capacitive and non-capacitive faradaic processes could be the effect of
18 localised and delocalised valence electrons [4, 34].

19

20 **3.1. Reversible non-capacitive faradaic process in electrode coatings**

21 Non-capacitive faradaic process can result from localised reversible electron transfer
22 reactions in a redox active coating on an electrode. When this happens, the CV should be a
23 bell-shaped curve as displayed in **Fig. 11a** [3, 34]. The potential of the current peaks on the
24 CV is determined by the redox potential of the material. The current response towards the
25 potential change can be expressed as Eq. (10), which is derived from the Nernst and Randles-

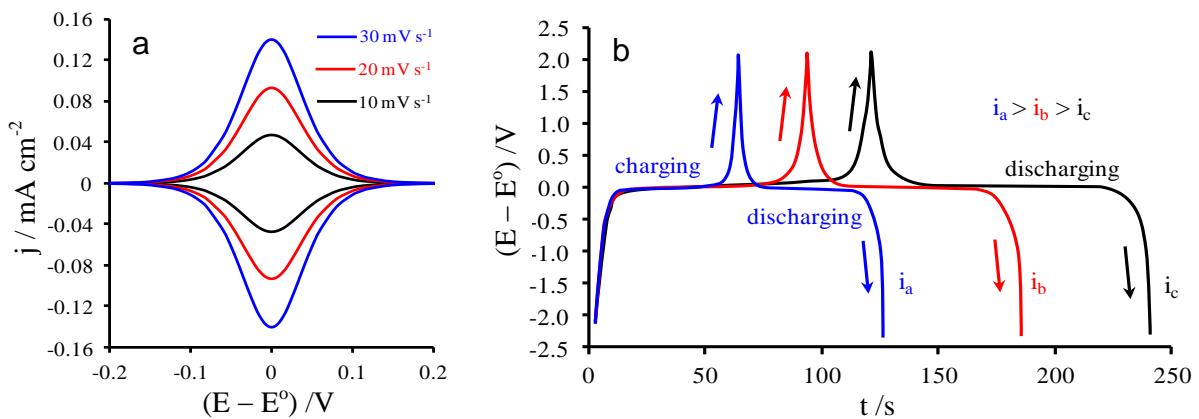
1 Sevcik equations [35].

$$2 \quad i = \frac{n^2 F^2 A \Gamma_i \nu \exp\left[\frac{(E - E^0) n F}{RT}\right]}{RT \left\{1 + \exp\left[\frac{(E - E^0) n F}{RT}\right]\right\}} \quad (10)$$

3 where n is the number of electrons transferred between the reduced and oxidised sites, F the
 4 Faraday constant, A the area of electrode, $\Gamma_i (= \Gamma_o + \Gamma_r)$ the total surface covered by the
 5 reduced and oxidised sites and ν is the potential scan rate, R the ideal gas constant and T the
 6 absolute temperature. Due to the strong dependence of the electrode reaction on potential, the
 7 GCD plots in **Fig. 11b** show potential plateaux over a narrow potential range. Nevertheless,
 8 the faradaic reaction took place in the electrode materials is reversible as the shapes of the
 9 CVs and GCDs are symmetrical in horizontal and vertical orientations, respectively [4].

10 The cause for CVs or GCD plots in **Fig. 11** are not rectangular or triangular like those
 11 shown in **Fig. 2** may be explained from a view point of electron energy states. As electron
 12 energy states are separated in isolated molecules or insulators, the energy levels of the filled
 13 and vacant states are singular and the process that electron inject to (or remove from) an

14



15

16 **Fig. 11.** (a) CVs at indicated potential scan rates and (b) GCD plots at indicated constant
 17 currents of $i_a > i_b > i_c$ for a reversible faradaic reaction with localised electron transfer to and
 18 from isolated redox sites on the electrode [4].

1 electrode may take place in very well separated redox active sites. In other words, because
2 these redox centres are non-interactive or electronically isolated from each other but have
3 equal or fairly close energy states, electron acceptance or donation occurs at potentials very
4 close to each other, resulting in the peak shaped CV in a narrow potential range as shown in
5 **Fig. 11a**. However, if these redox active sites can interact with each other due to either short
6 separations or good electronic conductivity or both, their energy states can merge into a broad
7 band with negligibly small differences between the neighbouring states. Such a situation
8 corresponds to the conduction band in semiconductors, including most transition metal oxides,
9 and is also comparable with the electron delocalisation in conjugated chemical bonds, as in
10 electronically conducting polymers (ECPs), resulting from overlapping electron orbits
11 between neighbouring atoms. As a result, electron transfer into (or from) each energy state in
12 this broad band becomes continuous over a wide range of potentials, which is responsible for
13 the constant current flow and hence the rectangular CV.

14

15 3.2. Pseudocapacitance from delocalised electrons

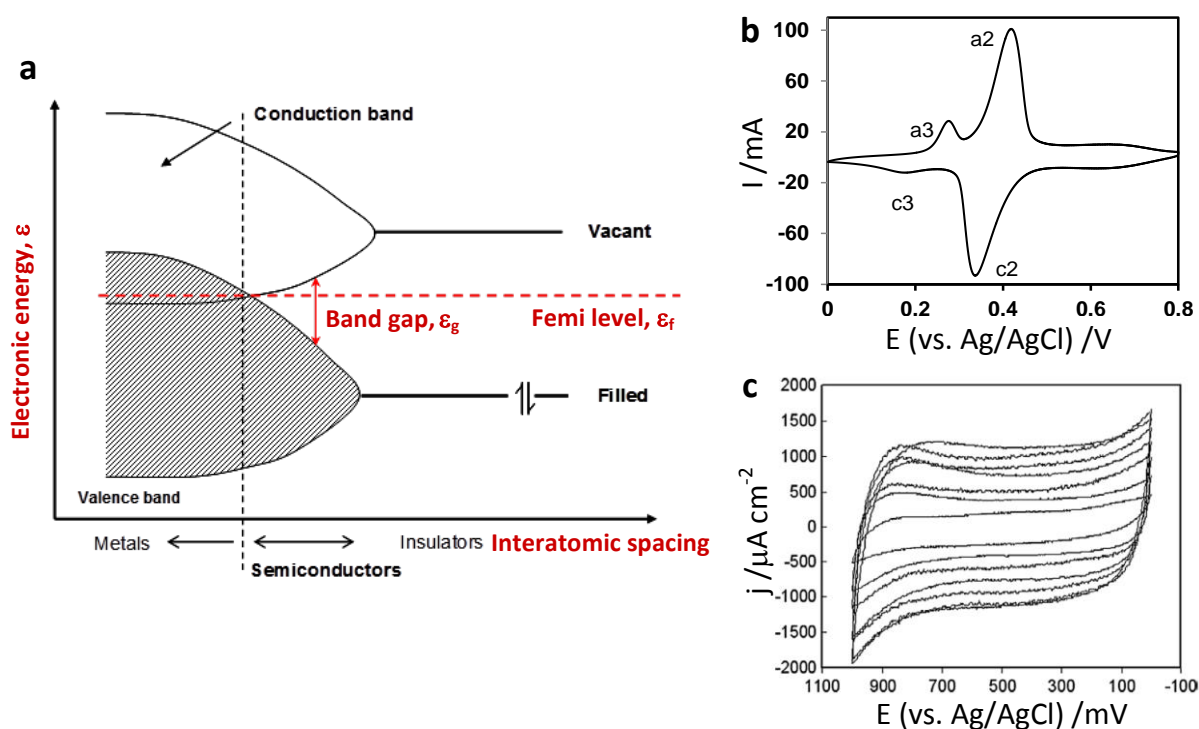
16 The above analysis is derived from the band theory for semiconductor [35], which can
17 also be applied for qualitative description of the capacitive faradaic process for charge
18 storage in pseudocapacitive materials. **Fig. 12a** illustrates the distribution energy states in
19 three different materials, namely, metals, semiconductors, and insulators. Electron energy
20 states of metals are completely overlapped, enabling free electron mobility in response to an
21 electrical field. Unfortunately, no capacitance can be achieved since charges cannot be stored
22 in a geometric location. Within an insulator, redox active sites are unable to interact with each
23 other electrically and hence behave like individual molecules. This means localised electron
24 transfer from the electrode substrate to each of the redox active sites in a narrow potential
25 range and hence a current peak on the CV. Such processes are shown in **Fig. 12b** on the CV

1 of an electro-deposited ferrocenyl polymer coating on a Pt disc electrode in an organic
2 electrolyte [36]. The large peak couple, a₂/c₂, results from the ferrocenyl groups, and the
3 smaller couple, a₃/c₃, from the polymer. As previously mentioned, a narrow peak would
4 form on the CV if the non-capacitive faradaic electrode reaction takes place in which electron
5 transfer reaction occurs at separated sites (e.g. the ferrocenyl groups) with energy states very
6 comparable to each other.

7 As shown in **Fig. 12a**, semiconductors are featured by their slightly separated filled
8 valence band and the vacant conduction band. When the applied potential is suitable for
9 electron excitation, electrons in the valence band can jump over to the conduction band and
10 become delocalised. At the same time, mobile holes are left in the valence band. Thus,
11 although the energy gap between the broad valence and conduction bands is small, the
12 continuous electron dislocation and hole production over the relatively wider potential range
13 give rise to the constant capacitive current flow as shown in **Fig. 12c**. These CVs were
14 recorded in 0.5 M LiCl using an electrode coated with thin films of MnO₂ with different
15 thicknesses.[37] Due to electron dislocation in semiconductor MnO₂ coatings conducted
16 amongst redox sites which interacted actively and continuously with each other between
17 neighbouring states, rectangular CVs were observed. This type of charge storage process is
18 the so called capacitive faradaic process.

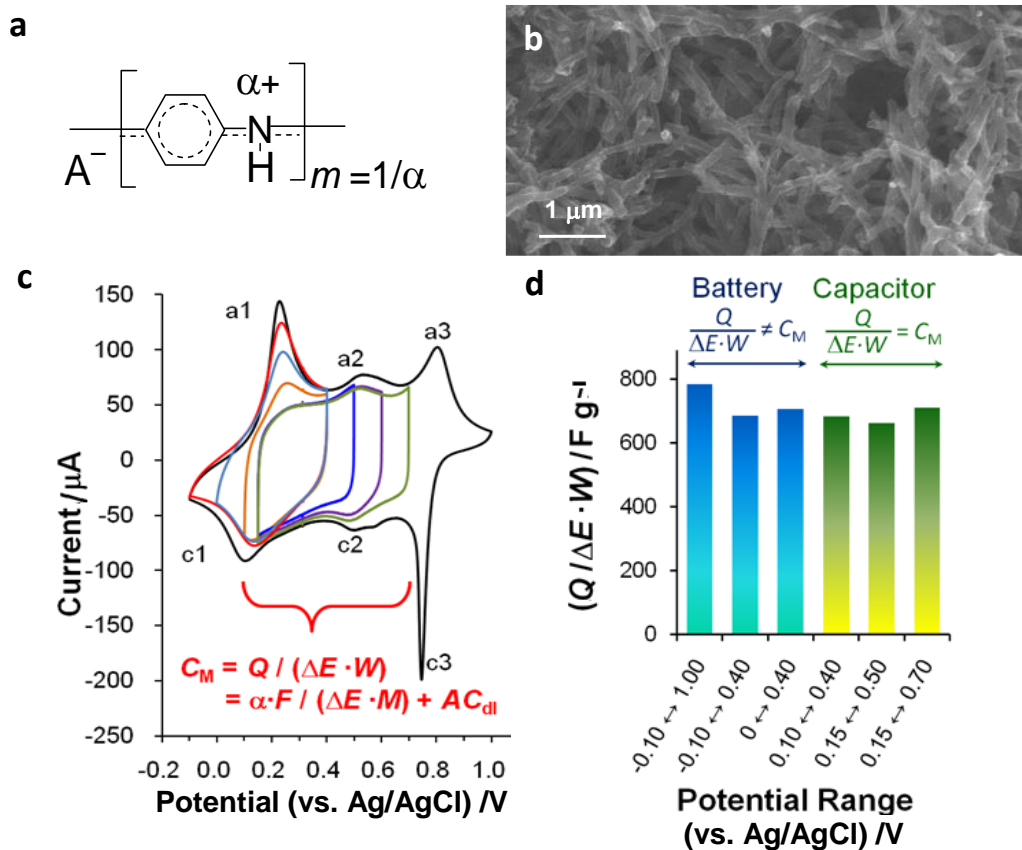
19 It is noteworthy that mixed forms of the above two types of charge storage mechanisms
20 are also observed in many cases with the development of advanced nanomaterials for
21 supercapacitor applications. For instance, it has been reported that the electro-deposited
22 polyaniline (PAN) nanofibrils were able to store charges relying on both pseudocapacitance
23 and EDL capacitance, giving rise to a maximum specific capacitance for PAN.[38] It was
24 also suggested that both charging processes were carried out in parallel. In other words, non-
25 faradaic capacitive, capacitive faradaic and non-capacitive faradaic reactions have all

1 proceeded in PAN and made contributions to the overall charge storage.



2
3 **Fig. 12.** (a) Schematic illustration of the band theory [34]. (b,c) CVs of (b) an
4 electrodeposited ferrocenyl bithiophenic polymer coating on Pt disc electrode in an
5 acetonitrile electrolyte at 20 mV s^{-1} [36] and (c) MnO₂ thin films of increasing thickness
6 formed by redox deposition on graphite electrode in 0.5 M LiCl at 25 mV s^{-1} [37].

7
8 In the work, the PAN nanofibrils were potentiostatically deposited at 1.0 V vs. Ag/AgCl
9 on a platinum disc electrode (1.6 mm in diameter) from a solution containing 0.25 M aniline
10 monomer and 1.0 M HCl. The polymerised PAN can be presented by the chemical formula in
11 **Fig. 13a**, showing the faradaic charge storage stoichiometry of PAN. The α number is used to
12 express the fraction of the charge of an electron that each aniline monomer unit shares, e.g.
13 0.5 electron per monomer ($\alpha = 0.5$) is needed to oxidise the polymer from its fully reduced
14 state (leucoemeraldine) to the partially oxidised state (emeraldine). Upon oxidation, the
15 polymer is doped by counter anions, A^- , to balance the positive charges in the polymer chains



1
 2 **Fig. 13.** (a) Faradaic charge storage stoichiometry of PAN, (b) SEM image and (c) CVs of
 3 PAN nanofibrils in 1.0 M HCl at 20 mV s^{-1} in different potential ranges [38]. (d) C_s or the
 4 $Q/(\Delta E \cdot W)$ ratio derived from the CVs in (c) with indicated potential ranges.

5
 6 along which the electrons are delocalised amongst several neighbouring monomers. The
 7 prepared PAN nanofibrils had a thickness in the range of 50 – 150 nm and were
 8 interconnected to form a porous structure as shown in **Fig. 13b**.

9 CVs were also recorded in 1.0 M HCl in different potential ranges to characterise
 10 capacitive behaviours of the PAN nanofibrils. It can be seen in **Fig. 13c** that the CV shape
 11 changes significantly with positively shifting the negative potential scan limit and becomes
 12 rectangular with diminishing or disappearance of peak a1. This indicates the PAN behaved
 13 like a capacitor within a narrow potential range in which reversible conversion between
 14 leucoemeraldine and emeraldine was the major electrode reaction [38]. With further

1 extension of the potential window, PAN however behaved like a battery since the polymers
2 started experiencing irreversible changes caused by the oxidation to the fully oxidised state,
3 pernigraniline. Again, due to the non-capacitive or battery-like behaviour of PAN, the peak
4 shaped CVs should not be used for the capacitance measurement as the large peak current
5 will lead to a misleading ultra-high capacitance value [39].

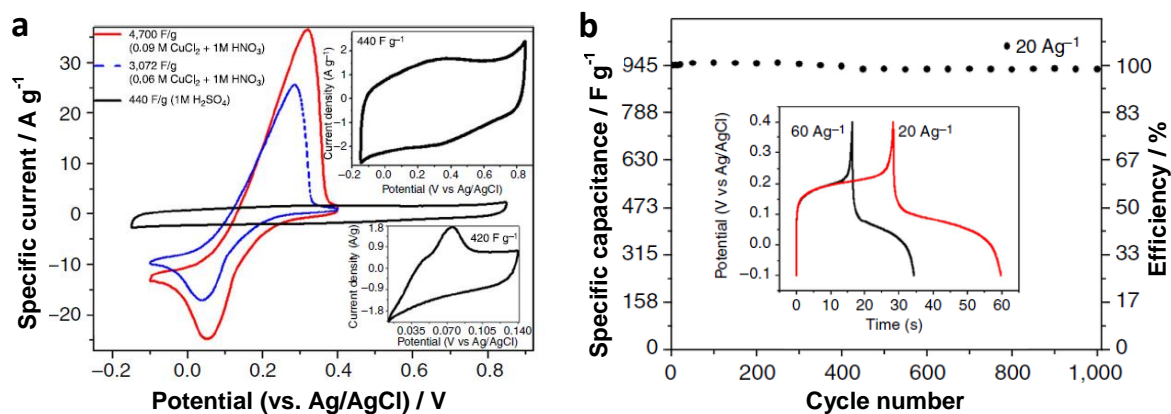
6 In contrast, the specific capacitance of PAN can be calculated as below based on the
7 rectangular CVs in **Fig. 13c** after combining faradaic and double layer contributions,

$$8 \quad C_s = \frac{Q}{\Delta E \cdot W} = \frac{\alpha \cdot F}{\Delta E \cdot M} + AC_{dl} \quad (11)$$

9 where F is the Faraday constant, ΔE the potential range, M the molecular mass of the
10 monomer unit in the polymer, A the specific area ($\text{m}^2 \text{g}^{-1}$) and C_{dl} the double layer
11 capacitance per unit true area of the material (F m^{-2}). In accordance with the redox
12 mechanism of PAN, α varies with ΔE , but the relation may not be linear. Thus the maximum
13 value of C_s can appear at smaller values of α and ΔE [38, 40], where the reversible redox
14 reactions (capacitive faradaic reactions) of PAN predominate. In this situation, electron
15 delocalisation occurs along the polymer chains to enable high conductivity and
16 pseudocapacitance. However, it is worth pointing out that the C_s values derived from the
17 rectangular CVs of PAN are generally smaller than those $Q/(\Delta E \cdot W)$ ratios measured over the
18 wide potential range in which battery-like behaviour dominated as shown in **Fig. 13d**. This is
19 due to the insulating-to-conducting phase transition in the polymer leading to the large
20 current of peak a1 [41].

21 Interestingly, measuring capacitance based on a non-capacitive faradaic charge
22 storage process does not come singly but in pairs, giving misleading results. It was reported
23 that combination of an activated carbon electrode with a redox electrolyte containing CuCl_2
24 could increase significantly the charge storage capacity of activated carbon, compared with a

1 conventional inert electrolyte as shown in **Fig. 14a** [42]. As expected, a huge current peak
 2 was observed because in the acidic media (1 M HNO₃), CuCl₂ reacted with the oxy-groups on
 3 the surface of the activated carbon electrode by self-reduction to form an additional redox

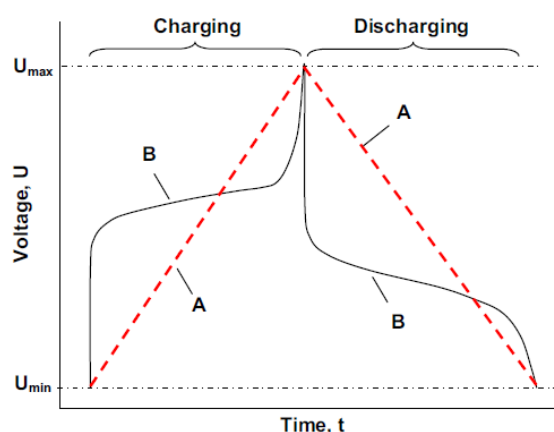


4
 5 **Fig. 14.** (a) CVs of activated carbon in an acidic aqueous solution with and without CuCl₂ at
 6 5 mV s⁻¹. The top inset is the magnification of the CV in a 1 M H₂SO₄ solution and the
 7 bottom inset shows the curve in 1 M HNO₃ and 0.12 M CuSO₄. (b) The GCD cycling
 8 performance of the as-prepared electrode in 1 M HNO₃ and 0.06 M CuCl₂ aqueous
 9 electrolyte solution at 20 A g⁻¹. The inset shows charge-discharge curves at different current
 10 densities. (Reprinted by permission from Macmillan Publishers Ltd, [42]).

11
 12 layer of CuCl. Unfortunately, the CVs in **Fig. 14a** were misused to derive an ultrahigh but
 13 misleading specific capacitance of 4700 F g⁻¹. The related GCD plots (**Fig. 14b**) are akin to
 14 those of rechargeable batteries other than the triangular plot of a capacitor as shown in **Fig.**
 15 **2b**. Similar to the aforementioned cases, although this electrode-electrolyte reaction was
 16 faradaic in nature, it took place at fixed or localised redox activated sites (C=O bond on the
 17 carbon surface) which are not interactive with each other to generate pseudocapacitance.

18 However, in the paper, the performance characteristics were still calculated based on the
 19 peak shaped CVs regardless the origin of the charge storage, giving rise to ultrahigh values of
 20 4700 F g⁻¹ for specific capacitance of the electrode and 163 Wh kg⁻¹ for average energy

1 capacity. These results particularly need to be considered since the charging energy had been
2 underestimated and discharging energy been overestimated in comparison with the symmetric
3 triangular GCD plot of an ideal capacitor (the red dashed plot in **Fig. 15**). This is because the
4 calculated energy is the area under the dashed straight lines, whereas, the actual energy is the
5 area under the curved solid lines. The charging energy is larger than the discharging one,
6 reflecting the electrode reaction being not fully reversible and hence only a portion of the



7
8 **Fig. 15.** Schematic comparison of the GCD plot of a quasi-reversible faradaic reaction such
9 as the case in **Fig. 14** (black solid lines) with that of an ideal capacitive faradaic reaction (red
10 dashed lines). The area under the potential curve of the GCD is proportional to the energy
11 consumed (or released) during charging (or discharging) [43].

12
13 energy used during the charging period was released during the discharging period. In this
14 case, the energy efficiency considered as the ratio of discharging energy to charging energy is
15 far smaller than 1, which is not ideal for energy storage.

16 Different charge storage mechanisms have been briefly introduced, including non-
17 faradaic EDL storage or capacitive faradaic pseudocapacitance and non-capacitive faradaic
18 battery-like behaviours. However, classification of individual charge storage mechanisms has
19 become rather ambiguous since the emergence of advanced composite electrode materials
20 (e.g. the composites of carbon materials with ECPs [16] or transition metal oxides [44]) or

1 the application of a novel redox active electrolyte [42]). Confusions therefore appeared in the
2 literature [39, 45-47] in terms of understanding of the origin of pseudocapacitance and
3 determination of capacitance. Although Conway had stated an average pseudocapacitance of
4 a battery could be determined by dividing the withdrawable charge (ΔQ) with the voltage
5 difference (ΔE) in 1991, he simultaneously emphasised that the discharge characteristics of Q
6 vs. time would not be similar as those of a capacitor, which is not very useful and informative
7 and could be misleading [48]. Hence, it is essential and crucial to carefully define and
8 differentiate the charge storage process according to the electrochemistry of the electrode
9 materials and from the viewpoint of the semiconductor or delocalisation band theory. This is
10 certainly significant and helpful to precisely evaluate the performance of supercapacitors and
11 beneficial for designing practical devices for energy storage, such as supercapattery.

12

13 **4. Energy capacity enhanced by unequal capacitance**

14 4.1. Unequal capacitance theory

15 It is well known that supercapacitors are high power energy storage devices, but
16 relatively low in energy capacity compared to batteries. There is a strong desire for
17 improving the energy capacity of supercapacitors. In theory, this improvement can be
18 achieved by either increasing the capacitance or expanding the working voltage of a
19 supercapacitor based on Eq. (5), where ε represents the energy stored in a supercapacitor, C
20 capacitance and U voltage.

21 For symmetrical supercapacitors, capacitance equalisation of the two electrodes is
22 necessary to maximise material utilisation and specific energy storage capacity, because the
23 positive and negative electrodes have the same working potential range. Practically, one
24 should also consider if the open circuit potential (OCP) of the material is at the centre of the
25 potential range [49], because the OCP does not always match the potential of zero charge

1 (PZC) with reference to **Fig. 16**. However, it may not be the same case in asymmetrical
 2 supercapacitors. The amount of charge, Q , stored in the positive and negative electrodes in an
 3 asymmetrical supercapacitor must be the same and is governed by Eq. (12) to (14),

$$4 \quad Q = C_P U_P = C_N U_N \text{ or } U_N = U_P C_P / C_N \quad (12)$$

$$5 \quad C = \frac{C_P C_N}{C_P + C_N} = \frac{C_P}{1 + C_P / C_N} \quad (13)$$

$$6 \quad U = U_P + U_N = U_P (1 + C_P / C_N) \quad (14)$$

7 where C_P and C_N are the capacitance, and U_P and U_N are the “working potential range” of the
 8 positive and negative electrodes in the cell. Note that U_P or U_N is defined as the difference
 9 between the more positive (or less negative) and less positive (or more negative) potential
 10 limits of the working potential range. It means that U_P or U_N is always positive, disregarding
 11 the electrode’s polarity.

12 Another upper and lower limit, “exploitable potential range” for positive or negative
 13 electrode, U_P^o or U_N^o , is set by any irreversible electrode reactions in a supercapacitor cell,
 14 such as solvent decomposition and over-oxidation or over-reduction of the electrode
 15 materials. Thus, $U_P \leq U_P^o$ and $U_N \leq U_N^o$. Eq. (15) describes the relationship among U , U_P , U_N ,
 16 U_P^o and U_N^o . (Note: $U_P^o = \text{CPR}(+)$ and $U_N^o = \text{CPR}(-)$ in **Fig. 16**.)

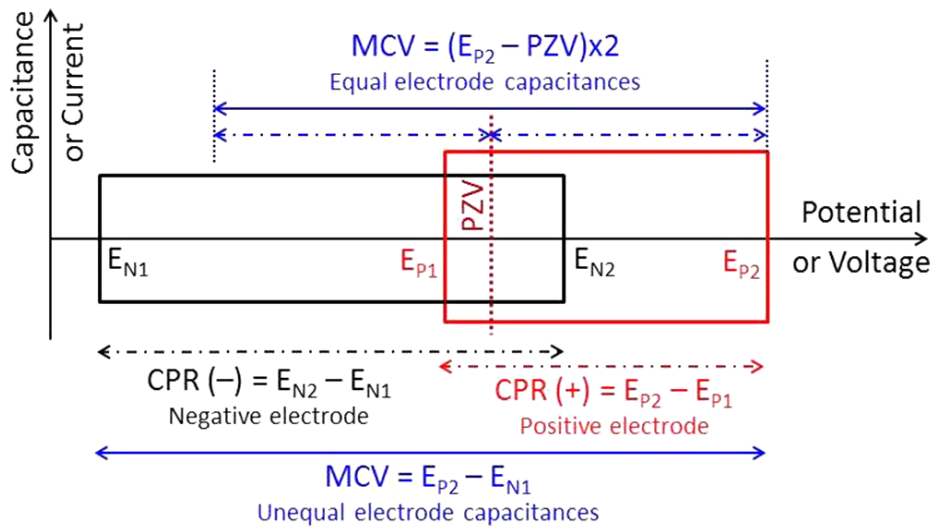
$$17 \quad U = U_N + U_P \leq U_P^o + U_N^o \quad (15)$$

18 Along the potential axis, U_P and U_N are next to each other, but U_P^o and U_N^o could be either
 19 connected or overlapping partially or completely. From Eq. (12), it can be found that if C_P
 20 increases, U_P will reduce and the same correlation applies to C_N and U_N . For a symmetrical
 21 supercapacitor, the above situation is avoided because of the equalised electrode capacitance
 22 (*i.e.* $C_N = C_P$). In the case of an asymmetrical supercapacitor, the two electrodes have likely
 23 different values for U_P^o and U_N^o . When the positive and negative electrodes are equalised in
 24 capacitance, the cell voltage will be limited either by the positive electrode if $U_P^o < U_N^o$, or

1 by the negative electrode if $U_P^o > U_N^o$. In cases where U_P^o and U_N^o overlap, they should be
 2 replaced by U_P and U_N respectively. However, the voltage of an asymmetrical supercapacitor
 3 can also be extended by increasing the capacitance of the “cell voltage limiting electrode”,
 4 leading to the increase of the energy stored by the supercapacitor as indicated in Eq. (16)
 5 which is derived from Eq. (5) and (12) to (14).

$$6 \quad E = \frac{1}{2}CU^2 = \frac{1}{2}C_P U_P^2 (1 + C_P/C_N) \quad (16)$$

7



8

9 **Fig. 16.** A model of supercapacitor voltage. Schematic illustration of supercapacitor
 10 maximum charging voltage (MCV), potential of zero voltage (PZV) and electrode capacitive
 11 potential range (CPR) [50]. $CPR(+)$ = U_P^o and $CPR(-)$ = U_N^o in Eq. (15).

12

13 It has been proven that the positive to negative electrode capacitance ratio (C_P/C_N) plays
 14 an important role in the improvement of a practical asymmetrical supercapacitors without
 15 changing the materials [51]. Along with C_P/C_N , the capacitive potential range (CPR) and
 16 potential of zero voltage (PZV) may affect the maximum charging voltage (MCV) and stored
 17 energy of the supercapacitor. **Fig. 16** shows a model of supercapacitor voltage [50]. The
 18 lower and upper potential limits of the negative and positive electrodes are denoted as E_{N1} ,

1 E_{N2} , E_{P1} and E_{P2} , respectively. The CPR of the negative or positive electrode is $E_{N2} - E_{N1}$ or
2 $E_{P2} - E_{P1}$, respectively. PZV is defined as the equal electrode potential when a supercapacitor
3 is fully discharged and its voltage is zero if $E_{N2} \geq E_{P1}$. PZV affects the coulombic efficiency
4 and the MCV of a supercapacitor, but is difficult to predict in practice. As shown in **Fig. 16**,
5 if the positive electrode is the “cell voltage limiting electrode” as the MCV of the
6 supercapacitor is determined by E_{P2} , then $PZV - E_{N1} > E_{P2} - PZV$, and the capacitance of the
7 two electrodes are equal, the MCV would be $(E_{P2} - PZV) \times 2$.

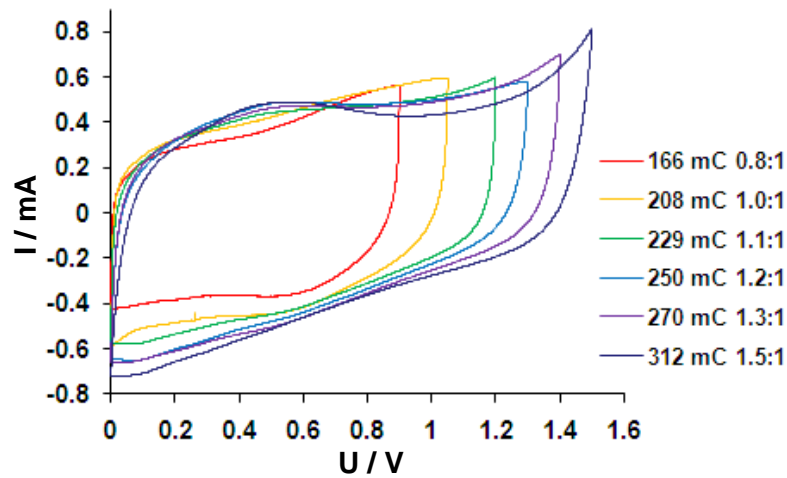
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9 4.2. Asymmetrical supercapacitor

10 A few asymmetrical supercapacitor examples have proved the practicality of the
11 unequal capacitance theory [50, 51]. An asymmetrical supercapacitor composing of a PAN-
12 CNT nanocomposites positive electrode and a CMPB (Cabot Monarch 1300pigment black)
13 negative electrode has been investigated [51]. PAN has very high theoretical specific
14 capacitance (750 F g^{-1}) [40] and excellent charging-discharging cycle stability [16], but it has
15 a small exploitable potential range of 0.7 - 0.8 V in acidic aqueous electrolytes [16]. If PAN
16 is used in a symmetrical supercapacitor, its energy capacity and power capability are
17 compromised, as indicated in Eq. (5), despite of the polymer’s ultrahigh specific capacitance.
18 In the previous research [51], several PAN-CNT positive electrodes were prepared at
19 deposition charges of 166 to 312 mC, corresponding to C_P/C_N ratios of 0.8 to 1.5. **Fig. 17**
20 shows the CVs of these PAN-CNT (+)|HCl (1.0 M)|CMPB (-) asymmetrical supercapacitors.
21 In this supercapacitor, the positive electrode PAN-CNT (+) is the “cell voltage limiting
22 electrode” [51]. In **Fig. 17**, the charging peaks can be identified on all these CVs near the
23 high voltage ends and the peak voltage shifted to higher values with increasing C_P/C_N ratio.
24 When the C_P/C_N ratio changes from 1.0 to 1.5, the cell capacitance only decreases by 7%,
25 while the specific energy of the cell increases over 80%. These improvements are remarkable,

1 as there was only a small increase of 12.9% in the total mass of the electrode materials.

2



3

4 **Fig. 17.** CVs of asymmetrical supercapacitors with a 0.3 mg CMPB negative electrode and a
5 PAN-CNT positive electrode at indicated C_P/C_N ratios without the charging current peak.
6 Scan rate: 20 mV s^{-1} [51].

7

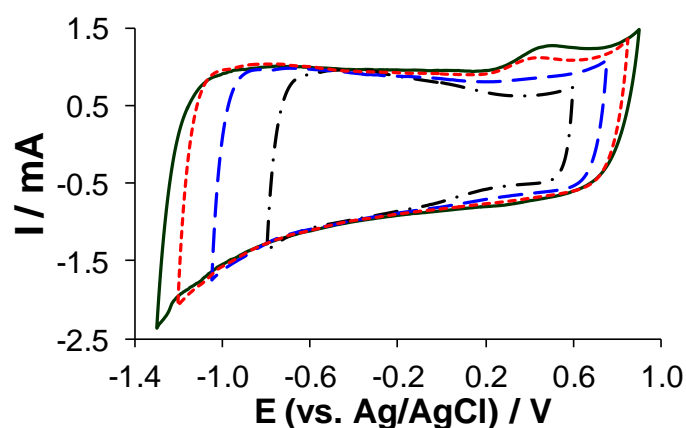
8 Similar asymmetrical supercapacitor composing of polypyrrole-CNT (PPy-CNT)
9 composites positive electrode and CMPB negative electrode have been fabricated and tested.
10 The relative research is still ongoing and unpublished. The preliminary data indicates that the
11 asymmetrical cell can improve the cell voltage from 1.0 to 1.4 V and cell specific energy
12 from 13.0 to 16.6 J g^{-1} comparing to the symmetrical cell. Recently, graphenes are popularly
13 used to form composite with conducting polymers that could increase supercapacitor cell
14 voltage when combined with suitable counter electrode and electrolyte [52].

15

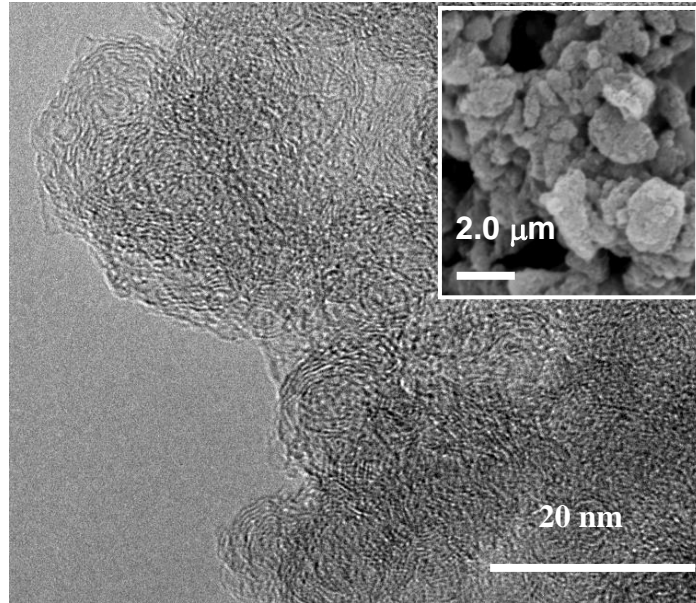
16 4.3. Unit cell supercapacitor

17 Conventionally, a symmetrical aqueous carbon-carbon supercapacitor is perceived to
18 show a narrower working voltage than an asymmetrical supercapacitor. However, recent
19 study suggested that a unit cell supercapacitor consisting of CMPB can reach beyond 1.9 V in

1 cell voltage, and retain over 85% of the initial capacitance through 10,000 cycles with the cell
2 becoming stable after the 1,000th cycles [53]. **Fig. 18** shows the CVs of CMPB in 0.3 M
3 K₂SO₄ solution at a scan rate of 5 mV s⁻¹ [53]. Basically, the negative current reflects the rate
4 of absorption/adsorption of hydrated cations, H₃O⁺ and K⁺, and desorption of anion, SO₄²⁻,
5 during the negative polarisation. The positive current corresponds to the rate of desorption of
6 the mentioned cations and absorption/adsorption anions in the course of positive polarisation.
7 It is also noticed that there is small positive current humps between 0.4 and 0.5 V on the CVs
8 when the negative potential limit reached beyond -1.0 V, where a fast increasing negative
9 current appeared due to the formation of hydrogen on the electrode. Actually, the current
10 humps locate in a very positive potential range. It suggests that the hydrogen is trapped in the
11 in the nanopores of CMPB at high negative polarisation.
12 The SEM and TEM images of the CMPB used in the research are shown in **Fig. 19** and
13 reveal micrometer sized aggregates of uniform onion-like spherical nanoparticles (10 nm)
14 [54]. This nanoporous structure could also make contribution to the extension of the negative
15 potential limit away from the theoretical value of water decomposition [55].



16
17 **Fig. 18.** CVs of the conventional three-electrode cell using the CMPB-PTFE (2.5 mg) coated
18 graphite disc working electrode in 0.3 M K₂SO₄ solution over different working potential
19 windows. Scan rate: 5 mV s⁻¹ [53].



1

2 **Fig. 19.** TEM and SEM (insert) images of the CMPB [54].

3

4 **Fig. 20** shows the CVs of CMPB-PTFE (1.0 mg) in the conventional three-electrode
5 cell with the PZV of 50 mV and potential ranges with unequal electrode capacitance [53].

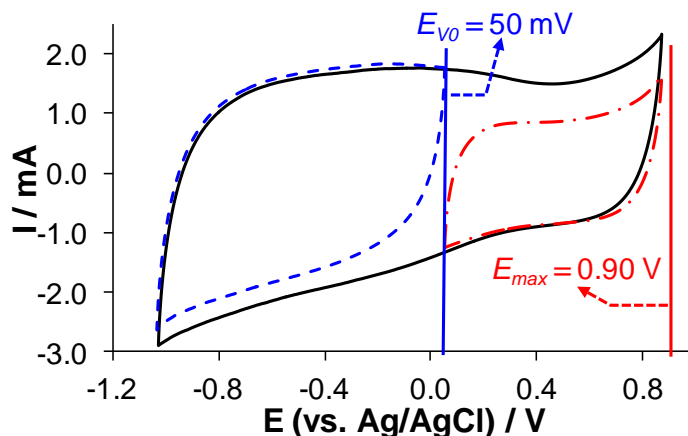
6 The C_P/C_N ratio comes to 4/3 and has successfully extended the negative electrode potential
7 windows towards a more negative range. Meanwhile, the positive electrode potential
8 windows kept the same, but the cell voltage increased from 1.6 V ($C_P/C_N = 1$) to 1.9 V
9 ($C_P/C_N = 4/3$). The energy capacity and capacitance have been compared between equal and

10 unequal electrode capacitance CMPB supercapacitors. **Fig. 21** shows the capacitance
11 retention of supercapacitor with different C_P/C_N ratios [53]. It can be found that the
12 supercapacitor with the C_P/C_N ratio of 4/3 performs better than the one with the ratio of 1.

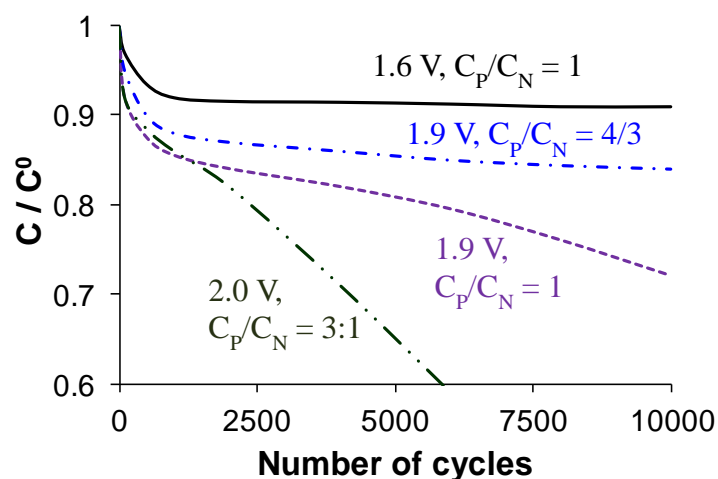
13 The calculation of the cell capacitance and specific energy capacity indicate that there will be
14 only 2% decrease of the cell capacitance but 38% increase of the cell specific energy capacity.

15 This is a typical zero cost engineering example.

16



1
2 **Fig. 20.** CVs of CMPB-PTFE (1.0 mg) in the conventional three-electrode cell with the PZV
3 of 50 mV and potential ranges with unequal electrode capacitance [53].



4
5 **Fig. 21.** Capacitance retention (C/C^0) as a function of the number of charge-discharge cycles
6 of sandwich-type supercapacitors with the cell voltage limit indicated [49].

7
8 **5. Supercapattery**

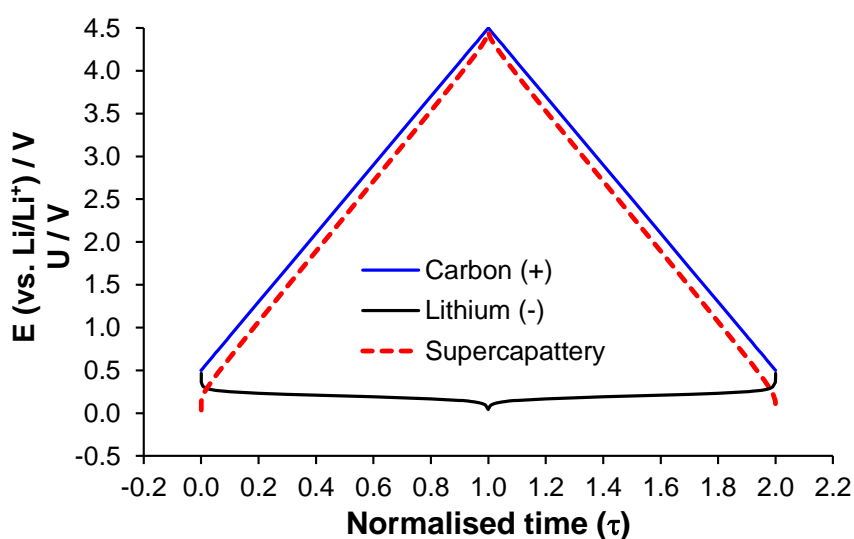
9 Another widely applied approach to increasing the energy capacity of supercapacitors
10 is using hybrid configurations that take the advantages of both the supercapacitor and battery.
11 The particular design involves combination of a supercapacitor electrode with a battery
12 electrode, such as the so called lithium ion capacitor [56] and the more general term
13 supercapattery (= **supercapacitor + battery**) [50, 57].

14 Theoretically, the hypothetical battery of lithium metal and fluorine gas (Li-F battery)

1 would output a cell voltage about 6.1 V and offer a specific energy content of 6304 Wh/kg at
2 room temperature. This value sets the upper limit of specific energy for all batteries. For Li-
3 ion batteries (e.g. $\text{Li}_x\text{C}_6 \mid \text{Li}_{1-x}\text{CoO}_2$), the theoretical specific energy is 552 Wh/kg at 3.5 V. If
4 one considers a supercapattery with a lithium metal negative electrode and a supercapacitor
5 positive electrode of 400 F/g, the specific energy value would be 625 Wh/kg for the cell
6 voltage to vary from 3.5 V to 1.0 V. In this calculation, the mass of the lithium metal is
7 negligible because the specific charge capacity of lithium is much larger than that of the
8 supercapacitor electrode. Thus, in theory, supercapattery can possess higher specific energy
9 than both battery and supercapacitor, and should be able to supply this specific energy at a
10 power output almost as high as supercapacitor with suitable electrode and cell designs.

11 Nanostructured carbons, such as activated carbon, CNT and graphene represent the
12 primary material choices for the polarisable capacitor-like electrode (i.e. capacitive non-
13 faradaic) owing to their large surface area, porosity, stability over a wide potential window,
14 as well as intrinsically low electrical resistance. Pseudo-capacitive materials including MnO_2 ,
15 RuO_2 and conducting polymers can also be used to gain higher electrode capacitance which
16 however also means narrower potential windows. As to the battery-like electrode, a much
17 wider choice of materials exists, from lead acid battery to metal/air systems, but metal
18 compounds such as SnO_2 , MnO_2 and LiFePO_4 are more practically and commercially
19 available. It should be mentioned that combining the supercapacitor and battery electrodes
20 into one device could result in performance very close to that of the supercapacitor [1, 50].
21 This is demonstrated by the calculated GCD plots shown in **Fig. 22** for a cell with a lithium
22 metal negative electrode and an activated carbon positive electrode. In the calculation, the
23 potential range of the activated carbon is set between 0.5 V and 4.5 V vs. Li/Li^+ to avoid
24 interaction of the carbon with lithium metal. With overall cell performance being comparable
25 to that of a supercapacitor, the analysis and comparison can follow those capacitor equations.

1 Examples of such capacitive cell behaviour are also reported in the literature [58, 59]. On the
 2 other hand, the combination of battery and supercapacitor electrodes may also present battery
 3 like features as that shown in **Figs. 14** and **15**. In such cases, data presentation and analysis
 4 should follow those for batteries. Particularly, specific charge capacity (e.g. mAh g⁻¹) should
 5 be reported, instead of specific capacitance (F g⁻¹). For hybrid devices showing rechargeable
 6 battery behaviour, the term supercabattery is recommended [50].



7
 8 **Fig. 22.** Calculated potentials of the positive activated carbon electrode (blue solid line) and
 9 the lithium metal negative electrode (solid black line) and the cell voltage (dashed red line)
 10 for a “Li | activated carbon” supercapattery.

11
 12 Recent studies reveal that an aqueous supercapattery consisting of a MnO₂ positive
 13 electrode and a Li/LISICON/PEO-LiTFSI/Li⁺ negative electrode had achieved a specific
 14 energy value of 114 Wh kg⁻¹ with a 4.3 V cell voltage [60]. The specific energy can come to
 15 520 Wh kg⁻¹ with a 3.8 V cell voltage, if the positive electrode is replaced by RuO₂ [60].
 16 However, the current density of the supercapattery discussed above is 0.255 mA cm⁻², which
 17 is still not ideal for high power application. Our recent supercapattery work based on an
 18 activated carbon (110 F g⁻¹) positive electrode and a Li/Li⁺ negative electrode using an ionic

1 liquid electrolyte can achieve a specific energy value of 200 Wh kg^{-1} at a 1.0 mA cm^{-2} current
2 density. The relative work is still ongoing and will be published elsewhere [61].

3

4 **6. Conclusions**

5 In this paper, we have proposed to define and differentiate **capacitive** and **non-**
6 **capacitive** faradaic processes for charge storage in supercapacitors according to the band
7 theory which the origin of pseudocapacitance has been correlated with electron transfer to or
8 from the conduction band of semiconductor type materials. The principle and performance
9 governing equations of conventional capacitors have been presented and applied to
10 differentiate between batteries and supercapacitors based on the shapes of CVs and GCDs. It
11 is confirmed that pseudocapacitance is featured by rectangular CVs and triangular GCDs and
12 peak-shaped CVs and non-linear GCDs are features of battery behaviour which should not be
13 used for measurement of capacitance values and energy estimation.

14 We have also found a unique affinity between Ca^{2+} ions and the oxy-groups on the
15 surfaces of CNTs, leading to a significant capacitance improvement. The specific capacitance
16 of the CNTs measured in CaCl_2 based electrolytes was generally higher than that in more
17 commonly used alkali salts based electrolytes. This understanding is new to supercapacitor
18 research and could have a significant impact on development of supercapacitors based on
19 CNTs, graphenes and/or activated carbons which are all enriched with various surface oxy-
20 groups. In particular, after mixing with FA and H_2O , the resultant organoaqueous CaCl_2
21 electrolyte enabled the CNTs to store charges at both room and sub-zero temperatures below
22 -60°C without a significant capacitance loss.

23 On the other hand, energy capacity enhancement by unequal capacitances has been
24 demonstrated in theory and examples. It clear shows that the phenomena of the potential of
25 zero voltage (PZV), capacitive potential range (CPR) and positive to negative electrode

1 capacitance ratio (C_P/C_N) affect the performance of supercapacitors. It also shows that for
2 energy enhancement, the capacitance unequalisation approach could be very low or almost
3 zero in engineering cost. The recent development in supercapattery that utilises both
4 capacitive and non-capacitive charge storage mechanisms (i.e. hybrid devices combining
5 supercapacitor and battery electrodes) reveals much increased energy capacity comparable or
6 higher than those existing rechargeable batteries, including the lithium ion battery. These
7 initial studies have demonstrated a very promising prospect of supercapattery.

8

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14

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