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Article title:	Evaluation of biodegradable polyester-co-lactone microparticles for protein delivery
Article no:	LDDI_A_814060
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http://informahealthcare.com/ddi ISSN: 0363-9045 (print), 1520-5762 (electronic)

Drug Dev Ind Pharm, Early Online: 1-10 © 2013 Informa Healthcare USA, Inc. DOI: 10.3109/03639045.2013.814060



# Evaluation of biodegradable polyester-co-lactone microparticles for protein delivery

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#### 21 Abstract

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22 Poly(glycerol adipate-co-m-pentadecalactone) (PGA-co-PDL) was previously evaluated for the 23 colloidal delivery of  $\alpha$ -chymotrypsin. In this article, the effect of varying polymer molecular 24 weight (M<sub>w</sub>) and chemistry on particle size and morphology; encapsulation efficiency; in vitro 25 release; and the biological activity of  $\alpha$ -chymotrypsin ( $\alpha$ -CH) and lysozyme (LS) were 26 investigated. Microparticles were prepared using emulsion solvent evaporation and evaluated by various methods. Altering the M<sub>w</sub> or monomer ratio of PGA-co-PDL did not significantly 27 affect the encapsulation efficiency and overall poly(1,3-propanediol adipate-co- $\omega$ -pentadeca-28 lactone) (PPA-co-PDL) demonstrated the highest encapsulation efficiency. In vitro release varied 29 between polymers, and the burst release for  $\alpha$ -CH-loaded microparticles was lower when a 30 higher M<sub>W</sub> PGA-co-PDL or more hydrophobic PPA-co-PDL was used. The results suggest that, 31 although these co-polyesters could be useful for protein delivery, little difference observed 32 between the different PGA-co-PDL polymers and PPA-co-PDL generally provided a higher 33 encapsulation and slower release of enzyme than the other polymers tested. 34

# **Keywords**

α-chymotrypsin, biodegradable polyesters, lysozyme, microparticles, PGA-co-PDL, protein delivery

## History

Received 16 October 2012 Revised 18 April 2013 Accepted 4 June 2013 Published online

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#### Introduction 37

38 Numerous protein and peptide pharmaceuticals such as recom-39 binant human growth hormone, gaserelin acetate, leuprolide 40 acetate and recombinant bovine somatropin have already received 41 approval from regulating authorities worldwide<sup>1</sup>. However, there 42 are many difficulties associated with delivering biopharmaceut-43 ical drugs. The oral route of administration of proteins results in 44 substantial degradation and poor bioavailability<sup>2</sup>, therefore, 45 parenteral delivery is usually preferred. However, proteins often 46 exhibit short half-lives in serum, thus requiring frequent admin-47 istration to maintain their plasma level<sup>3</sup>. To prolong the 48 therapeutic level of proteins, controlled release is required and 49 this can be achieved using biodegradable polymers<sup>4</sup>. A range of 50 formulation methods have been utilized to encapsulate proteins in 51 polymeric micro- and nanoparticles, but water-in-oil-in-water 52 (w/o/w) emulsion solvent evaporation is the most frequently used 53 method. Difficulties in the encapsulation of proteins are related to 54 their high molecular weight (M<sub>W</sub>), high water solubility and 55 instability upon exposure to formulation conditions<sup>5</sup>. An initial 56 burst release followed by slow, incomplete release of the native 57 protein as a result of protein instability and aggregation has also 58 been recognized as a major problem<sup>6</sup>. Interactions between the 59 protein and the polymer also influence the release profile. These 60 interactions are dependent on protein M<sub>W</sub>; isoelectric point; 61

102 amino acid composition; and hydrophobicity, as well as polymer 103  $M_w$  and chemistry<sup>1</sup>. Polymer properties such as  $M_w$ , copolymer 104 composition and crystallinity can also be tailored to alter polymer 105 degradation and subsequent drug release profiles<sup>7,8</sup>. For example, 106 an increase in the  $M_W$  of Poly(lactic-co-glycolic acid) (PLGA) 107 resulted in longer degradation times and slower release of bovine 108 serum albumin and tetanus toxid<sup>9,10</sup>. Bovine serum albumin 109 (BSA) and lysozyme (LS) were encapsulated using two different 110 M<sub>w</sub>s of PLGA by (w/o/w) solvent extraction and oil-in-oil (o/o) 111 solvent evaporation systems<sup>11</sup>. BSA was efficiently encapsulated 112 independently of PLGA M<sub>W</sub>, whereas the encapsulation of LS was 113 favored with low M<sub>W</sub> PLGA. 114

Although the choice of polymer is critical, few new polymers 115 have been developed for specific drug delivery applications, and 116 mono- and copolymers of poly(lactic acid) (PLA) and poly(gly-117 colic acid) (PGA) are commonly adopted due to their widespread 118 availability and approval for human use. One alternative is to 119 develop new polymeric delivery systems to release the protein and 120 retain bioactivity over the required target period<sup>12</sup>. 121

A family of biodegradable polyesters with backbone function-122 ality, synthesized via the enzyme catalyzed transesterification of a 123 combination of activated diacids, glycerol and lactone monomers 124 has been designed to overcome the lack of chemical functionality of the commonly used polyesters<sup>13,14</sup>. The free hydroxyl group 125 126 from the glycerol monomer allows for the attachment of chemical 127 moieties such as pharmaceutically active drugs, hence introducing 128 the potential for the controlled incorporation and release of 129 desired molecules (drugs, proteins and peptides). In addition, the 130 physical characteristics (hydrophilicity and hydrophobicity) of 131 these polymers can easily be manipulated by varying the 132

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backbone chemistry<sup>15</sup>. Previously, poly(glycerol adipate) (PGA) 133 and poly(glycerol adipate-co- $\omega$ -pentadecalactone) (PGA-co-PDL) 134 have been investigated for the delivery of dexamethasone 135 phosphate<sup>16</sup> and ibuprofen<sup>17</sup>. More recently, PGA-co-PDL has 136 shown promise as a sustained release carrier for pulmonary 137 delivery using the model drug, sodium flourescein<sup>18</sup>. PGA-138 co-PDL (1:1:1, M<sub>W</sub> 30.0 KDa) has also previously been used to 139 140 prepare  $\alpha$ -chymotrypsin ( $\alpha$ -CH)-loaded microparticles via the double (w/o/w) emulsion solvent evaporation method<sup>19,20</sup>. 141 In the initial w/o emulsification step, a lipophilic surfactant is 142 incorporated to aid the emulsification of the aqueous drug 143 solution and the organic phase containing the polymer. Gaskell 144 et al. found that on average 22.1  $\mu$ g  $\alpha$ -CH per 1 mg PGA-co-PDL 145 146 was encapsulated, and there was a loss of enzyme bioactivity during encapsulation followed by a further gradual loss upon 147 release<sup>19</sup>. The low amount of  $\alpha$ -CH encapsulated is typical of 148 these systems due to the diffusion of the protein from the inner to 149 outer aqueous phases during particle formation and upon solvent 150 evaporation. These different previous studies have all utilized a 151 1;1;1 ratio of monomers, and the  $M_W$  of the particular polymers 152 used varied depending upon the M<sub>w</sub> achieved during synthesis 153 Which, given the nature of these reactions, can be difficult to 154 precisely control. It is therefore not known whether the copolymer 155 156 composition or M<sub>W</sub> may influence the characteristics of the 157 particles formed.

Polymer properties such as molecular weight Mw, copolymer composition and crystallinity can be tailored to alter polymer degradation and the consequent drug release profiles as well as the microparticles characteristics. The nature of the protein encapsulated can also affect the particle formation, loading, release and bioactivity profiles<sup>21</sup>.

Therefore this study is an extension of the work presented by 164 Gaskell et al., examining the effect of small changes in polymer 165 Mw and copolymer composition on the encapsulation efficiency, 166 loading, particle size, morphology, in vitro release and bioactivity 167 of two different proteins, α-CH (25 kDa) and LS (14 kDa). These 168 enzymes differ in size (LS, 14 KDa, α-CH, 25 KDa), isoelectric 169 point (LS, 11.2,  $\alpha$ -CH, 9.1) and stability (LS is more stable than 170 171 α-CH).

#### 172 173 Materia

# 173 Materials and methods

# 175 Materials

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176 Novozyme 435 (a lipase from Candida antarctica immobilized on 177 a microporous acrylic resin) was purchased from Bio Catalytics 178 (USA) and stored over P2O5 at 5°C prior to use. Glycerol, 1.3-179 propandiol, ω-pentadecalactone, α-chymotrypsin (type II from 180 bovine pancreas), lysozyme (from chicken egg white), aerosol OT 181 (dioctyl sodium sulphosuccinate), poly(vinyl alcohol) (PVA, M<sub>w</sub> 182 9-10 KDa, 80% hydrolyzed), azocasein, 4-methylumbelliferyl 183 β-D-N,N',N"-triacetylchitotrioside, citric acid, trichloroacetic 184 acid (TCA) and sodium citrate were all obtained from Sigma-185 Aldrich Chemicals (UK). Dichloromethane and N-[2-hydro-186 xyethyl]piperazine-N'-[2-ethanesulphonic acid] (HEPES) were 187 purchased from BDH (UK). Tetrahydrofuran (THF) was 188

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purchased from Fisher Scientific. Phosphate buffered saline 199 tablets at pH 7.4 were obtained from Oxoid (UK). Divinyl 200 adipate (DVA) was obtained from Fluorochem (UK). A polystyr- 201 ene standards kit was purchased from Supelco (USA). 202

## **Polymer synthesis**

205 The copolymers PGA-co-PDL and PPA-co-PDL were synthe-206 sized, processed and characterized using methods adapted from 207 Thompson et al.<sup>22</sup> and further described by Gaskell et al.<sup>15</sup> 208 Polymer M<sub>W</sub> was varied by controlling the reaction time. 209 Reaction times of 6, 18 and 24 h were used to prepare PGA-210co-PDL (1:1:1) with a M<sub>W</sub> of 11.4, 26.0 and 39.2 KDa, 211 respectively. The ratio of divinyl adipate (DVA) and glycerol 212 (1:1) to  $\omega$ -pentadecalactone was varied to produce polymers 213 theoretically containing 1:1:0.5 and 1:1:1.5 of DVA, glycerol and 214  $\omega$ -pentadecalactone, respectively. Using the same reaction condi-215 tions, PPA-co-PDL with a Mw of 22.0 KDa was synthesized from 216 a 1:1:1 molar ratio of DVA: 1.3-propanediol: ω-pentadecalactone 217 over 24 h. 218

The polymers were characterized by gel permeation chroma-219 tography, GPC (Viscotek TDA Model 300 ran by OmniSEC3 220 operating software precalibrated with polystyrene standards) and 221 <sup>1</sup>H-NMR spectroscopy (Bruker AVANCE 300 operated via 222 XWIN-NMR v3.5). <sup>1</sup>H-NMR ( $\delta_{\rm H}$  CDCl<sub>3</sub>, 300 MHz) PGA-223 co-PDL (1:1:0.5): 1.34 (s, 11H, H-g), 1.65 (m, 8H, H-e, e', h), 224 2.32 (m, 6H, H-d, d', i), 4.05 (q)-4.18 (m) (6H, H-a, b, c, f), 5.2 225 (s, H, H-j), PGA-co-PDL (1:1:1): 1.34 (s, 22H, H-g), 1.65 (m, 8H, 226 H-e, e', h), 2.32 (m, 6H, H-d, d', i), 4.05 (q)-4.18 (m) (6H, H-a, b, 227 c, f), 5.2 (s, H, H-j) and PGA-co-PDL (1:1:1.45) 1.30 (s, 32H, 228 H-g), 1.68 (m, 9H, H-e, e', h), 2.32 (m, 6H, H-d, d', i), 4.05 229 (q)-4.18 (m) (6H, H-a, b, c, f), 5.2 (s, H, H-j). Protons a to j are 230 illustrated in Figure 1. 231

# Particle preparation

234 The multiple emulsion-solvent evaporation (w/o/w) technique was 235 employed for the encapsulation of  $\alpha$ -CH and LS as reported previously<sup>19</sup>. Briefly, a 1% (v/v) solution of protein (100 mg mL<sup>-</sup> 236 237 ) in phosphate buffered saline (PBS) pH 7.4 was added dropwise to a homogenizing solution of polymer (30 mgmL<sup>-1</sup>) and aerosol 238 AOT (2 mM) in dichloromethane (15 ml) and emulsified using a 239 IKA yellowline DI 25 basic at 8000 rpm for 30-40 s. This first 240 emulsion was then gradually added to a mixing 1% (w/v) PVA 241 242 solution (135 ml). This w/o/w emulsion was left to mix with a 243 Silverson L4 RT mixer at 1000 rpm for 3 h to allow for 244 dichloromethane evaporation at 25 °C. The particles obtained 245 were collected by centrifugation (EBA 20, Hettich) at 6000 g for 246 6 min at room temperature. The supernatant was labeled "wash 247 1" and retained for further analysis. The microparticles were 248 re-suspended in 120 ml PBS buffer to remove the residual PVA 249 present on the surface of the particles and centrifuged as before. 250 The collected supernatants were labeled "wash 2". The 251 microparticles were then filtered, vacuum-dried overnight and 252 stored in the fridge. Three batches of each type of particle were 253 prepared. 254



Figure 1. Chemical structure of PGA-co-PDL (1:1:1).

#### 265 Particle characterization

266 The particles were visualized by scanning electron microscopy 267 (FEI - Inspect S Low VAC Scanning Electron Microscope). A 268 suspension of particles in water was deposited on 13 mm 269 aluminum stubs layered with a sticky conductive carbon tab and 270 air dried. An atomic layer of gold was deposited onto the particle 271 containing stubs using an EmiTech K 550X Gold Sputter Coater, 272 25 mA for 3 min. 273

Particle size and size distribution were determined by a laser 274 scattering device (Beckman Coulter LS 13 320, with aqueous 275 liquid module) according to the method described by Pamujula 276 et al.<sup>23</sup> The Frauenhofer method was used to calculate the size 277 distribution of particles in water. The results obtained from 278 measurements of at least three batches of microparticles were 279 described by the volumetric mean diameter of the microparticles 280 (VMD) in micrometers. Equation (1) gives the formula for the 281 span of the volume distribution, which measures the width of the 282 size distribution relative to the median diameter (d[v,50]). A more 283 heterogeneous size distribution gives a large span value<sup>24</sup>. 284

$$Span = \frac{d[v, 90] - d[v, 10]}{d[v, 50]}$$
(1)

288 Powder X-ray diffraction (PXRD) patterns were collected by 289 using a Rigaku Miniflex X-ray diffractometer. Samples were 290 finely ground and packed into an aluminum sample holder. 291 Patterns were collected between 5° and 50°  $2\theta$ , at increments of 292  $0.02^{\circ} 2\theta$ , scanning speed 2°min-1, voltage 30 KV, current 15 mA 293 using CuK $\alpha$  (1.54 Å) radiation. 294

#### 295 Drug loading and encapsulation efficiency 296

297 The theoretical encapsulation efficiencies and enzyme loading 298 from three different batches of microparticles were calculated from the measurement of the non-encapsulated protein fraction 299 present in the wash samples (Equation 2) and with the assumption 300 301 that no protein was lost during the preparation and processing of the particles<sup>19</sup>. The enzyme loading ( $\mu$ g/mg) was determined 302 303 using (Equation 3).

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#### In vitro release of enzyme from microparticles 316

Sacrificial sampling was used to observe the release of the 317 enzyme from the particles. In a clean dry 1.5 ml microtube, 10 mg 318 of vacuum-dried particles and 1 ml of phosphate buffer saline pH 319 7.4 at 37 °C were placed under sink conditions. The microtubes 320 were then incubated at 37 °C in an orbital shaker (IKA KS 130) at 321 250 rpm. Samples were removed at increasing time points over 322 24 h and centrifuged (5 min at 13500 rpm (17000 g), accuSpin 323 Micro 17) to collect the particles. The supernatants were retained 324 for analysis by the protein assays described below. 325

326 The bioactivity of both enzymes was presented as the bioactive 327 fraction of the released enzyme. This was calculated from the 328 ratio of enzyme concentration determined from enzyme activity 329 and the total enzyme concentration as determined by UV spectroscopy using the methods described below $^{25}$ . 330

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# Methods for assessing protein content and activity

332 The encapsulation washes (wash 1 and 2) and supernatants from 333 the release studies were analyzed for protein content<sup>19</sup> and 334 activity using the following methods. 335

### UV spectrophotometry

To determine the total protein content in a sample, the absorbance 338 was measured at 282 nm for both  $\alpha$ -CH and LS, (UV/VIS 339 spectrophotometer Lambda 40, Perkin Elmer, run via the UV 340 WinLab version 2.80.03 software). 341

## Azocasein assay

344 The proteolytic activity of  $\alpha$ -CH following release from particles 345 was determined using a chromogenic-based technique as modified 346 by Gaskell et al.<sup>19</sup> Briefly, 50 µL sample, standard or blank and 347 200 µL of azocasein (10 mg/ml), prepared in 25 mM HEPES 348 buffer were incubated for 3h at 37°C. The reaction was 349 terminated by addition of 750 µL of 0.3 M trichloroacetic acid 350 to precipitate the undigested protein-chromogenic conjugate and 351 the samples were centrifuged for 5 min at 13 500 rpm (17 000 g) 352 (accuSpin Micro 17) to remove the precipitate. Blank samples 353 were prepared using deionized water to determine the amount 354 of azo-dye released nonenzymatically from the substrate. 355 Absorbance of the samples was recorded at 415 nm compared to 356 blank reagent samples using UV/VIS spectrophotometer Lambda 357 40, Perkin Elmer, using the UV WinLab version 2.80.03 software. 358 Three replicates of each sample were obtained and processed. 359

# Muramidase assay

The muramidase activity of LS was determined using the method 362 described by Telkov et al.<sup>26</sup> Supernatant (760 µL) was incubated 363 with 8 μM 4-Methylumbelliferyl-β-D-N,N',N"-triacetylchitotrio-364 side in 50 mM citrate buffer, pH 6.0, in the presence of 5 mM 365 MgSO<sub>4</sub> for 3 h at 37 °C. The fluorescence intensity was measured 366 using a fluorescence spectrophotometer (Varian Cary Eclipse, 367 operated via the Cary Eclipse Advanced Reads Application 368 version 1.1 (132) software) at an excitation wavelength of 350 nm 369 and an emission wavelength of 450 nm. 370

### Statistical analysis

Statistical analysis was performed using student t-paired test. The F-test was used to test the significance of variance. The statistical significance level was set at  $p \leq 0.05$ .

# **Results and discussion**

379 The aim of this research was to investigate if changes to the M<sub>w</sub> 380 and chemistry of PGA-co-PDL would alter the encapsulation, 381 release and bioactivity of  $\alpha$ -CH and LS loaded into microparticles 382 fabricated by a w/o/w double emulsion solvent evaporation 383 technique. 384

### Polymer synthesis and characterization

The lipase catalyzed ring opening polymerization of an equimolar 387 quantity of DVA, glycerol and  $\omega$ -pentadecalactone produced 388 PGA-co-PDL (1:1:1) of different M<sub>W</sub>s (11.2, 26.0 and 39.2 KDa) 389 by altering the time in contact with the lipase (6, 18 and 24 h, 390 respectively) (Figure 1). A maximum M<sub>W</sub> for this type of polymer 391 is usually obtained around 24h synthesis followed by a subse-392 quent decrease in  $M_W$  as hydrolytic reactions dominate<sup>27</sup>. 393 This means that the range and difference in M<sub>w</sub>s achievable is 394 small and can be difficult to control. The incorporation of 1,3-395 propandiol in place of the glycerol produced PPA-co-PDL (1:1:1, 396

 $M_W$  22.0 KDa) which is more hydrophobic than PGA-co-PDL as it does not have pendant hydroxyl groups.

A different set of polymers with a constant 1:1 ratio of DVA 399 and glycerol, but with either 0.5 or 1.5 equivalents of 400 ω-pentadecalactone, was also prepared (1:1:0.5, M<sub>W</sub> 23.0 KDa 401402 and 1:1:1.45,  $M_W$  34.0 KDa). These polymers should be more 403 (1:1:1.45) and less (1:1:0.5) hydrophobic than PGA-co-PDL 404 (1:1:1) depending on the relative number of hydroxyl groups. It is difficult to control the M<sub>W</sub> of these polymers as an increase in the 405 amount of  $\omega$ -pentadecalactone increases the polymer M<sub>W</sub> 406 obtained. This means it can be difficult to directly compare the 407 effect of monomer ratio on polymer and particle properties as 408 there is also a difference in M<sub>w</sub>. <sup>1</sup>H-NMR integration patterns 409 410 were used to confirm that the monomeric content in the polymers were as expected and comparable to that reported in previous 411 work<sup>22</sup>. The difference in the number of protons at  $\delta 1.34$  is 412 indicative of the different proportions of pentadecalactone within 413 the polymer backbone (1:1:0.5 (11H), 1:1:1 (22H) and 1:1:1.45 414 415 (32H)).

### 417 Particle characterization

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<sup>418</sup> Protein-containing and blank particles containing no protein were prepared from each of the different polymers. The mean median of particle diameters ( $d_{50}$ ) of three separate batches of  $\alpha$ -CH- or LS-loaded microparticles and the span values are presented in Table 1.

The particle sizes obtained ranged between 9 and 18 µm. The 424 particles prepared from PGA-co-PDL (1:1:0.5) were aggregated 425 so no size data was obtained for this polymer. There was no 426 significant difference observed between the sizes of most of the 427 α-CH- or LS-loaded particles for the different polymers used 428 except with PGA-co-PDL (1:1:1, 39.2 KDa) where significantly 429 larger LS-loaded particles were obtained (p < 0.05). Previously, it 430 was reported that the higher the M<sub>W</sub> or concentration of polymer 431 in the emulsion, the larger the diameter of the produced 432 particles<sup>28</sup>. It was not anticipated that any great differences in 433 particle size would be observed because the polymer M<sub>w</sub> range 434 studied was small, and the stirring speed, solution concentrations 435 and the organic phase volume were fixed which are the main 436 contributing factors affecting particle size<sup>20</sup>. Additionally, ana-437 lysis of the span values (see Table 1) indicates that all 438 microparticles produced had a large size distribution which 439 made it difficult to draw any real trends from the data obtained. 440

The morphology of microparticles is very important as it influences particle degradation and hence can affect the protein release<sup>29</sup>. Moreover, particle morphology is dependent on the nature, composition and  $M_W$  of the polymer<sup>30,31</sup> as well as the particle formulation conditions<sup>20</sup>.

The SEM images of the external structure of  $\alpha$ -CH loaded PGA-co-PDL microparticles prepared from PGA-co-PDL (1:1:1) of different M<sub>w</sub> are presented in Figure 2(A–C). Almost spherical microparticles with a slightly irregular shape and a rough ridged surface were observed. A high variability in microparticle size was noted during the SEM analysis which supports the span value 463 data shown in Table 1. A similar morphology was also observed 464 with LS-loaded microparticles fabricated from the same polymers 465 (Figure 2G–I). Hence, changing either the polymer  $M_W$  or the 466 type of protein encapsulated did not alter the particle morphology. 467

Altering the chemistry did, however, have an effect on particle 468 morphology. PGA-co-PDL (1:1:0.5) produced small, aggregated, 469 non-uniform particles (Figure 2D), and increasing the lactone 470 content within the polymer changed the particle morphology 471 slightly. With both  $\alpha$ -CH- and LS-loaded PGA-co-PDL (1:1:1.45) 472 particles, some of the particles appeared irregular in shape with 473 rough surfaces, while the others were spherical with a slightly 474 smoother surface than those prepared from PGA-co-PDL (1:1:1) 475 (Figure 2E and J). These smooth particles were more similar to 476 those obtained from PPA-co-PDL (Figure 2F and K). A similar 477 morphology to  $\alpha$ -CH-loaded microparticles was observed with 478 the LS-loaded microparticles (Figure 2H-K). Thompson et al. 479 reported similar morphological characteristics for particles 480 prepared from PGA-co-PDL and PPA-co-PDL<sup>22</sup>. Drug-free and 481 ibuprofen-loaded microspheres<sup>17</sup> produced using PGA-co-PDL 482 were rough with a ridged morphology, whereas the equivalent 483 PPA-co-PDL microspheres were smooth. 484

# Drug loading and encapsulation efficiency

487 Polymer M<sub>w</sub>, degree of hydrophilicity, polymer chemistry, 488 volume of organic phase and enzyme and polymer concentration 489 play an important role in determining the amount of enzyme 490 encapsulated. It was reported that increasing the M<sub>W</sub> of poly 491 (*e*-caprolactone), PLA and PLGA increased the encapsulation 492 efficiency and the mean particle size due to the increased 493 viscosity of the organic phase, which reduces protein diffusion 494 into the external aqueous phase before polymer hardening<sup>8,32</sup>. 495 Partitioning of the drug from the internal to the external aqueous 496 phase limits the encapsulation efficiency and drug loading in 497 particles prepared via the emulsion solvent evaporation technique. During particle formation, solvent removal and polymer precipitation can alter the amount of the protein that partitions into the external aqueous phase<sup>33</sup>. It was previously determined that 3 h was the optimum time for PGA-co-PDL protein-containing particle formation as this provided enough time for the solvent to evaporate yet minimized enzyme diffusion to the aqueous phase<sup>19</sup>.

The encapsulation efficiencies and enzyme loading from three different batches of microparticles prepared using different polymers are presented in Table 2.

Increasing the  $M_W$  of PGA-co-PDL had no significant effect on either the encapsulation efficiency or  $\alpha$ -CH loading (p > 0.05). However, a shift in PGA-co-PDL  $M_W$  from 11.4 to 39.2 KDa might not be large enough to induce a significant increase in the viscosity of the organic phase, leading to a change in enzyme loading. The degree of crystallinity of the polymer is another important factor affecting drug encapsulation as drugs will tend to be encapsulated in the amorphous region of the polymer<sup>34</sup>.

Table 1. The mean median of particle size and the span values for  $\alpha$ -CH- and LS-loaded microparticles prepared via the w/ o/w double emulsion solvent evaporation technique. The results are the mean of three different prepared batches  $\pm$  S.D.

	Mean median of particle size (µm)		Span values	
Polymer type	СН	LS	СН	LS
PGA-co-PDL (1:1:1, M <sub>W</sub> 11.4 KDa)	$13.6 \pm 1.4$	$9.3 \pm 1.4$	$2.2\pm0.2$	$2.1 \pm 0.2$
PGA-co-PDL (1:1:1, M <sub>w</sub> 26.0 KDa)	$14.4 \pm 2.9$	$12.2 \pm 0.9$	$1.9 \pm 0.2$	$2.3 \pm 0.3$
PGA-co-PDL (1:1:1, M <sub>w</sub> 39.2 KDa)	$13.8 \pm 2.9$	$17.5 \pm 0.6$	$2.8 \pm 1.2$	$3.3 \pm 0.6$
PGA-co-PDL (1:1:1.45, M <sub>w</sub> 34.0 KDa)	$9.6 \pm 0.81$	$15.1 \pm 1.0$	$1.6 \pm 0.3$	$2.1 \pm 0.2$
PPA-co-PDL (1:1:1, M <sub>w</sub> 22.0 KDa)	$10.0 \pm 1.2$	$14.4 \pm 1.5$	$2.2\pm0.5$	$2.6 \pm 0.4$

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\*\*Significant difference PGA-co-PDL (1:1:1.45, Mw 34.0 KDa) versus PGA-co-PDL (1:1:0.5, Mw 23.0 KDa), \*significant difference PPA-co-PDL (22.0 KDa) versus PGA-co-PDL (26.0 KDa) at p < 0.05.</li>

 Mw 34.0 KDa).

Figure 3. X-ray diffraction pattern of

co-PDL (11.4 KDa); C, PGA-co-PDL

α-Chymotrypsin-loaded particles formulated

from A, PPA-co-PDL (22.0 KDa); B, PGA-

(26.0 KDa); and D, PGA-co-PDL (1:1:1.5,

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The PXRD patterns illustrated in Figure 3 indicate that both PGA-682 co-PDL and PPA-co-PDL are semicrystalline copolymers. Both 683 684 PGA-co-PDL and PPA-co-PDL showed characteristic peaks at  $21.5^\circ$  and  $24^\circ$   $2\theta.$  PGA-co-PDL of different  $M_{Ws}$  have the same 685 686 XRD patterns, indicating they have the same level of crystallinity, 687 and this may explain the similar encapsulation efficiencies observed. However, the PXRD pattern for PPA-co-PDL has a 688 flatter baseline between  $0^{\circ}$  and  $20^{\circ} 2\theta$ , indicating that it is a more 689 crystalline material. This difference in degree of crystallinity 690 between PGA-co-PDL and PPA-co-PDL may have influenced 691 microparticle formation but does not explain the increased 692 encapsulation efficiency observed with PPA-co-PDL. 693

694 Furthermore, changing the polymer composition by altering the pentadecalactone monomeric ratio from 0.5 to 1.5 molar ratio 695 significantly (p < 0.05) increased the encapsulation efficiency of 696 LS-loaded microparticles. An increase was also observed with 697  $\alpha$ -CH-loaded particles, but this was not significant (p > 0.05). 698 699 Compared to PGA-co-PDL, utilizing the more hydrophobic 700 polymer (PPA-co-PDL) a significant (p < 0.05) increase in 701 encapsulation efficiency and  $\alpha$ -CH loading (from 12.52 ± 4.42 to  $38.58 \pm 6.48\%$  and  $41.70 \pm 0.01$  to  $128.50 \pm 12.70$ , respect-702 703 ively) was observed. The highest  $\alpha$ -CH and LS encapsulation 704 efficiency and loading were obtained from the most hydrophobic 705 polymer, PPA-co-PDL. These results suggest that the more hydrophobic polymers demonstrate better encapsulation effi-706 ciency and drug loading of both enzymes compared to the less 707 hydrophobic variants. 708

Similarly, McGee et al. showed that ovalbumin-loaded microparticles prepared with PLGA with higher lactide to glycolide content (85:15) gave higher protein loading compared to the more hydrophilic one with 50:50 lactide to glycolide ratio<sup>35</sup>. Also, higher amounts of bovine albumin were encapsulated using PLGA (75:25) compared to the more hydrophilic PEGylated PLGA co-polymer<sup>36</sup>.

716 Comparing the encapsulation efficiencies and enzyme loading for both enzymes, it was found that LS showed a higher 717 encapsulation and loading compared to  $\alpha$ -CH with all the PGA-718 co-PDL variants assessed (Table 2). LS is a smaller, positively 719 charged enzyme that has the ability to be adsorbed onto the 720 surface of polymers and this adsorption will affect its encapsu-721 lation and release kinetics<sup>37</sup>. Furthermore, as previously 722 reported37,38, the temperature rises during the emulsification 723 724 steps and the adjustment of the pH to 7.4 can lead to favorable 725 conditions for LS adsorbing onto polymers. This could result in 726 increased amounts of LS being encapsulated within PGA-co-PDL.



Also, we cannot neglect that using 1% PVA as an emulsifier 748 imparts a negative charge to the surface of PGA-co-PDL and 749 PPA-co-PDL which would support enzyme binding. It was 750 reported that PVA, which is physically entrapped within the 751 surface layer of the polymer, imparts a negative surface charge on 752 the microparticles produced<sup>39,40</sup>. However, comparable amounts 753 of  $128.5 \pm 12.7$  and  $121.33 \pm 11.6 \,\mu\text{g/mg}$  particle of  $\alpha$ -CH and LS 754 were encapsulated, using PPA-co-PDL. This represents a signifi-755 cant increase over PGA-co-PDL for  $\alpha$ -CH- but not LS-loaded 756 particles. 757

## In vitro release

It was anticipated that polymer M<sub>W</sub> and polymer backbone 761 chemistry would be important factors affecting the drug release<sup>21</sup>. 762 Varying the M<sub>w</sub>, varies the degradation rate of the polymer and 763 release kinetics of the drug can be controlled accordingly<sup>41</sup>. 764 Additionally, the hydrophobicity of the polymer can affect the 765 drug release by reducing the rate of water penetration into the 766 microspheres and drug egress to some extent compared to the less 767 hydrophobic polymers<sup>42</sup>. Furthermore, different particle morphol-768 ogies may affect the protein release profile through its effect on 769 the microspheres porosity and the distribution of the drug within 770 the matrix  $^{29,43}$ . 771

The release profiles of either  $\alpha$ -CH or LS under sink conditions 772 from different batches are shown in Figures 4 and 5. Figure 4 773 shows the release of  $\alpha$ -CH from microparticles prepared using 774 different polymers over 24 h into PBS buffered saline. Most of the 775  $\alpha$ -CH-loaded microparticle formulations showed a biphasic 776 release pattern with an initial high burst release phase followed 777 by a continuous release phase for the first 5h which became 778 constant till the end of the release study. The extent of the burst 779 release varied between different microparticle formulations, 780 depending on the polymer used, and a notable difference was 781 observed between PGA-co-PDL (1:1:1 26.0 KDa or 11 KDa) and 782 the other polymers. 783

Other research groups<sup>11,33</sup> have observed that increasing 784 polymer M<sub>W</sub> led to a decrease in the total amount of enzyme 785 released. In this study, there was no general trend observed 786 between increasing M<sub>W</sub> and decreasing enzyme release, which 787 may be because the differences in M<sub>w</sub> were small, but there was 788 significantly less release after 24 h with PGA-co-PDL (39 KDa) 789 particles compared to PGA-co-PDL (26 KDa or 11 KDa) par-790 ticles. Varying the proportion of PDL within the polymer from 0.5 791 to 1.5 mole equivalents did not have any consistent effect on the 792

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Figure 5. Release profiles of lysozyme from polymeric microparticles prepared via the multiple emulsion solvent evaporation technique. The results are the mean of three different prepared batches at each time point  $\pm$  S.D.

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 $\alpha$ -CH release from microparticles. The biggest difference in 837 release was found when comparing PGA-co-PDL (26 KDa) with 838 the more hydrophobic polymer of a comparable M<sub>W</sub>, PPA-co-PDL 839 (22 KDa). Compared to PPA-co-PDL, PGA-co-PDL showed a 840 significantly (p < 0.05) higher burst release of  $\alpha$ -CH 841  $(20.13 \pm 3.0\%$  compared to  $8.54 \pm 2.7\%$ ) and a greater amount 842 843 of release after 24 h in PBS buffer ( $45.28 \pm 2.7\%$  compared to 844  $15.84 \pm 4.5\%$ ). Furthermore, PPA-co-PDL demonstrated the lowest burst and total release of  $\alpha$ -CH of all the prepared 845 846 microparticles.

847 The initial burst release phase of  $\alpha$ -CH from these microparticles could be due to the rapid release of protein near to the 848 surface of microparticles which accumulates at the water/oil 849 interface during the solvent evaporation process. The release of 850 the protein entrapped within the polymeric matrix causes a 851 852 continuous release of  $\alpha$ -CH during the first 5 h. Furthermore, the 853 constant release phase could be attributed to the protein aggre-854 gation and degradation that occurs during the release process. 855 Despite the higher encapsulation efficiency gained from PPA-856 co-PDL, these particles demonstrated a slower burst and 857 continuous release rate compared with PGA-co-PDL with comparable Mw. This might be due to the higher hydrophobicity 858

and slower rate of degradation of this polymer (unpublished data). 903 The lower surface area available for contact with the dissol-904 ution medium and the large particle size could be other 905 contributing factors toward this slow release as denser micro-906 particles with smooth surfaces will usually produce a lower rate of 907 initial release compared with rough, porous microparticles. This is 908 in agreement with Thompson et al. who observed a similar effect 909 for ibuprofen release from PGA-co-PDL and PPA-co-PDL 910 microparticles<sup>17</sup>. 911

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The release profiles of LS from the different polymeric 912 microparticles are shown in Figure 5. In this case, the LS-loaded 913 microparticle formulations showed a very small initial burst phase 914 followed by continuous release until the end of the release study 915 at 24 h. With LS there was a general trend of increasing PGA-916 co-PDL (1:1:1) M<sub>W</sub> and decreasing enzyme release. The release 917 of LS from the 39 KDa polymer was significantly lower, and there 918 was less difference observed between the 26 KDa and 11 KDa 919 variants. Although, as with  $\alpha$ -CH, there was a difference in the 920 release of LS from PPA-co-PDL (22 KDa) and PGA-co-PDL 921 (26 KDa) of a comparable M<sub>W.</sub> with LS the release profile of the 922 PPA-co-PDL particles was virtually the same as that of PGA-923 co-PDL (39 KDa). 924 925 It was observed that the pattern of LS release was different 926 from that obtained with  $\alpha$ -CH.  $\alpha$ -CH release was characterized by an initial burst followed by a slow continuous release phase for the 927 first 5 h then a plateau was reached. On the other hand, LS showed 928 a lower burst release followed by a higher continuous release 929 930 phase. This was especially evident with the lower M<sub>W</sub> PGA-co-931 PDL. The lower burst release could be attributed to the more 932 efficient encapsulation of LS inside the microparticles with 933 minimum amounts remaining adsorbed on the surface. Stronger binding of LS to these polymers could be another reason for this 934 as LS is cationic and these particles have a slightly anionic surface 935 from incomplete removal of PVA. 936

937 With all the microparticles studied, an incomplete release of 938 enzyme from these was observed even after 3 weeks. This has been observed by many researchers, and it might be due to 939 940 degradation of the protein during the manufacturing of the microparticles<sup>44</sup>. Formation of intermolecular linkages, hydroly-941 sis of the protein molecule and the nonspecific adsorption 942 943 between polymer and protein either physically or chemically can lead to protein degradation<sup>45</sup>. 944

#### 946 947 Enzyme bioactivity

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Retaining biological activity is crucial for the delivery of enzymes 948 and peptides, and preservation of the tertiary structure is required 949 950 to maintain activity. Enzyme activity before and after encapsu-951 lation and upon release can be monitored to investigate the effect of these processes on biological activity. Many researchers have 952 953 estimated the bioactivity of LS by measuring the rate of degradation of *Micrococcus luteus* cells<sup>25,46</sup>. However, this 954 method is not always reproducible because of the dependence 955 on the ionic strength of the medium<sup>47,48</sup>. Different methods using 956 small synthetic substrates have been developed, investigated and 957 recommended for accurate determination of  $LS^{49-51}$ 958

Observation of the bioactive fraction of  $\alpha$ -CH released from 959 microparticles prepared using PGA-co-PDL and PPA-co-PDL 960 (Figure 6) indicates that the maximum bioactivity was observed at 961 zero hours and ranged between 27% and 60%. This was followed 962 963 by a sharp decrease in activity during release into PBS buffer (pH 7.4). It was noticed that  $\alpha$ -CH released from PGA-co-PDL 964 exhibited a maximum activity of between 40% and 60%, and PPA-965 co-PDL showed the lowest activity of  $\sim 27\%$  at zero hour. 966 Furthermore, a gradual loss in bioactivity was recorded for all the 967  $\alpha$ -CH-loaded microparticles investigated. The reduction in 968

activity of  $\alpha$ -CH could be attributed to conformational changes 991 in the  $\alpha$ -CH active site during emulsification. The homogeniza-992 tion and use of organic solvents are considered important steps in 993 causing protein deactivation and aggregation resulting in a low 994 bioactive fraction at zero hour<sup>52-54</sup>. The gradual loss in activity 995 during in vitro release was most likely due to autolysis and protein 996 fragmentation<sup>53</sup>. This finding is similar to what was already 997 reported by Gaskell et al. where they found that  $\alpha$ -CH released 998 from PGA-co-PDL-loaded microparticles lost its bioactivity 999 gradually with an onset of loss due to proteolysis upon 2 h 1000 release19 1001

At zero hour of release, LS retained almost 100% of its initial 1002 bioactivity within all the particles investigated. Then, with time it 1003 began to gradually lose its bioactivity (Figure 7). The higher  $M_W$ 1004 polymer, PGA-co-PDL (1:1:1, 39.0 KDa), and the more hydro-1005 phobic polymers, PGA-co-PDL (1:1:1.45) and PPA-co-PDL, 1006 showed a significantly (p < 0.05) higher bioactive fraction, after 1007 5 and 24 h release, compared to the other co-polymers. The 1008 maximum LS bioactive fraction was found using PGA-co-PDL 1009 (1:1:1.45, M<sub>w</sub> 34 KDa) and PGA-co-PDL (1:1:1, M<sub>w</sub> 39.2 KDa) 1010  $0.78 \pm 0.08$  and  $0.42 \pm 0.02$ , respectively, after incubation in 1011 PBS for 24 h. 1012

LS is a relatively stable enzyme<sup>55</sup> which can better withstand 1013 the harsh condition of the emulsification process and this was 1014 confirmed by the retention of its bioactivity at zero time of release 1015 (bioactive fraction ranged from 0.9 to 1.03 for all the investigated 1016 polymers, Figure 7). Similarly, it was reported by Giteau and 1017 coworkers that the LS released from PLGA microspheres was still 1018 biologically active compared to  $\alpha$ -CH, peroxidase and  $\beta$ -galacto-1019 sidase-loaded PLGA microspheres<sup>57</sup>. However, during in vitro 1020 release there was a gradual decrease in the bioactive fraction 1021 which could be attributed to the effect of PBS buffer on the 1022 released LS. So, the nature of the release medium on the enzyme 1023 activity is very important, as many proteins are not stable in buffer 1024 media at 37 °C. However, for most studies the choice of release 1025 medium is dictated by the in vivo target for delivery of the 1026 enzyme. Jiang et al. investigated protein stability and protein-1027 polymer interactions in different release media and their effect on 1028 protein release profiles from PLGA microspheres using LS as a 1029 model protein<sup>37</sup>. They found that LS showed a higher stability at 1030 pH 4.0 acetate buffer and pH 2.5 glycine buffer, whereas at pH 7.4 1031 PBS, the stability was low and significant protein adsorption was 1032 evident. Furthermore, the higher bioactive fraction of LS in PGA-1033 co-PDL (1:1:1, Mw, 39.2 KDa) and PGA-co-PDL (1:1:1.45) could 1034



Figure 6. Bioactive fraction of released  $\alpha$ -Chymotrypsin from (A) PGA-co-PDL (1:1:1, MW 11.4, 26.0 and 39.2 KDa) and (B) PGA-co-PDL (1:1:0.5, 1054 MW 23.0 KDa, 1:1:1.5, MW 34.0 KDa) and PPA-co-PDL (1:1:1, MW 22.0 KDa) in PBS buffer, pH 7.4. Triplicate samples were used from two different prepared batches at each time point  $\pm$  S.D.

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1077 1143 Figure 7. Bioactive fraction of released lysozyme from the different investigated polymers in PBS buffer, pH 7.4. Triplicate samples were used from 1078 1144 two different prepared batches at each time  $\pm$  S.D. 1079 1145

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1081 possibly be attributed to the higher solubility of these polymers in 1082 DCM compared with PPA-co-PDL and the lower M<sub>w</sub> PGA-co-1083 PDL polymers. Additionally, the longer the contact time of the 1084 enzyme in the organic phase, the more enzyme activity would be 1085 lost. Thus, a higher solidification rate would be beneficial in 1086 retaining the LS biological activity. Similar results were reported by Ghaderi and Carlfors regarding stability of LS during emulsification process within PLGA<sup>48</sup>. Future work will focus 1087 1088 1089 on enhancing macromolecule encapsulation efficiency as well as 1090 maintaining stability during the manufacturing process. For 1091 example, the use of additives to protect the protein structure or 1092 the application of alternative formulation methods such as spray 1093 drying or s/o/w emulsions may substantially reduce the loss in 1094 bioactivity during encapsulation.

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#### Conclusion 1097

This research has shown that altering the M<sub>W</sub> of PGA-co-PDL 1098 from 11.2 to 39.2 KDa had little impact on particle morphology, 1099 size, encapsulation efficiency or bioactivity of α-CH- and LS-1100 loaded microparticles. Altering the polymer chemistry had a 1101 greater effect, as a higher encapsulation efficiency and drug 1102 loading of both  $\alpha$ -CH and LS were obtained with PPA-co-PDL 1103 compared to PGA-co-PDL particles. A biphasic release pattern 1104 was obtained with all microparticles studied, and the release 1105 profiles varied according to the polymer used. A lower burst and 1106 1107 continuous release was obtained for both enzymes with the more hydrophobic polymers, PPA-co-PDL and PGA-co-PDL (1:1:1.45) 1108 and with the higher M<sub>W</sub> PGA-co-PDL (39.2 KDa). Furthermore, a 1109 very low burst release was recorded with LS compared to  $\alpha$ -CH 1110 with all the investigated polymers. 1111

One benefit of the low impact of small changes in M<sub>w</sub> or PDL 1112 content on encapsulation and release is that batch-to-batch 1113 variations in the polymers should not have a demonstrable 1114 effect on either the properties of particles formed or the 1115 encapsulation and release data obtained. These findings suggest 1116 that more substantial changes to polymer properties are required 1117 1118 to significantly influence the encapsulation and release of 1119 proteins. The nature of this type of polymerization reaction 1120 means that it is difficult to achieve higher M<sub>w</sub> materials and 1121 extend the range of M<sub>W</sub>s studied. Small changes to the polymer chemistry has been shown to have a greater effect, hence future 1122

studies will focus on further modifying the polymer chemistry 1147 either by incorporating different monomers into the backbone or 1148 via modification of the pendant hydroxyl groups. 1149

# **Declaration of interest**

1153 The authors report no conflicts of interest. 1154 Hesham Tawfeek thanks the Ministry of Higher Education, Egyptian government, for funding the research presented within this paper. 1155

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