



Water Activities and Osmotic Coefficients of Aqueous Solutions of Five Alkyl-Ammonium Sulfates and Their Mixtures with H₂SO₄ at 25 °C

Journal:	<i>Aerosol Science & Technology</i>
Manuscript ID:	AST-MS-2014-196
Manuscript Type:	Original Manuscript
Date Submitted by the Author:	23-Oct-2014
Complete List of Authors:	Sauerwein, Meike Clegg, Simon Chan, Chak
Keywords:	amine sulfate salts, ammonium sulfates, water activity, osmotic coefficient, extended ZSR

SCHOLARONE™
Manuscripts

1
2
3 **Water Activities and Osmotic Coefficients of Aqueous Solutions of Five**
4 **Alkyl-Aminium Sulfates and Their Mixtures with H₂SO₄ at 25 °C**
5
6

7 Running Title: "Water activities of aqueous alkylaminium sulfates"
8
9

10
11 Meike Sauerwein¹, Simon L. Clegg^{2,*}, and Chak K. Chan^{1,3,*}
12
13

14 ¹ *Division of Environment, Hong Kong University of Science and Technology, Clear Water Bay,*
15 *Kowloon, Hong Kong*
16
17

18 ² *School of Environmental Sciences, University of East Anglia, Norwich NR4 7TJ, U.K.*
19

20 ³ *Department of Chemical Engineering, Hong Kong University of Science and Technology, Clear*
21 *Water Bay, Kowloon, Hong Kong*
22

23 **Corresponding author: sclegg@uea.ac.uk; keckchan@ust.hk*
24
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

Abstract

Alkylammonium sulfates are frequently detected in ambient aerosols, and are believed to be important in the nucleation of new particles in the atmosphere, despite their comparatively low gas phase concentrations. In this study water activities and osmotic coefficients have been measured, using a chilled mirror dew point technique, of aqueous mixtures of sulfuric acid and the following alkylammonium sulfates: methylammonium, ethylammonium, dimethylammonium, diethylammonium and trimethylammonium sulfate. The solutions were prepared by mixing solutions of the five corresponding amines and aqueous sulfuric acid and determining the exact ammonium to sulfate molar ratios by ion chromatography. The results were correlated using an extended Zdanovskii-Stokes-Robinson equation to enable concentration/water activity relationships to be calculated over the entire composition range from pure aqueous sulfuric acid to pure aqueous ammonium sulfates. Comparisons with water activities of ammonium sulfate/sulfuric acid mixtures showed very similar behavior for cation:sulfate ratios of 1:1 (the bisulfate salts) and lower, but that osmotic coefficients for the 2:1 ratio (the ammonium sulfates) were much greater than for ammonium sulfate. These results differ from those obtained in another recent study (S. L. Clegg, C. Qiu, and R. Zhang [2013] *Atmos. Environ.* 73:145–158). The relative values of the osmotic coefficients, in concentrated solutions, suggest that the numbers of methyl or ethyl groups in the ammonium ion may have a stronger lowering effect on water activity than the alkyl chain length.

1. INTRODUCTION

Short chain aliphatic amines such as methyl- and ethyl-amines are alkaline, volatile, water soluble organic compounds. Despite their low average ambient concentrations of about 10 - 100 ppt in the gas phase (Ge et al. 2011a), and high pure liquid vapor pressures (Ge et al. 2011b), they are able to substantially enhance the formation of secondary aerosols (Murphy et al. 2007; Kurtén et al. 2008; Almeida et al. 2013). Maximum mass loadings of short chain alkyl-amine ions, accounting for up to several hundred pg m^{-3} , have been detected in the accumulation mode of atmospheric aerosols (Müller et al. 2009; VandenBoer et al. 2011), and showing a strong dependence on relative humidity (*RH*), pH and temperature (Pratt et al. 2009; Rehbein et al. 2011).

Major pathways of amine removal from the gas phase include photo-oxidation processes (Nielsen et al. 2012), gas-particle partitioning via acid-base reactions (Wang et al. 2010; Rehbein et al. 2011; Liu et al. 2012), and the displacement of ammonia from ammonium salts under elevated amine gas phase concentrations (Lloyd et al. 2009; Bzdek et al. 2010; Qiu et al. 2011; Chan and Chan, 2012). The resulting alkyl-ammonium (aminium) salts – including sulfates, nitrates (Pratt et al. 2009), and carboxylates (Smith et al. 2010) – can promote particle growth and cloud droplet formation. Re-volatilization of amines from the particle phase has been observed for aminium nitrates (Murphy et al. 2007), as well as for certain secondary and tertiary aminium sulfates (Chan and Chan, 2013).

Our current understanding of the chemical and physical properties of aminium sulfates is far less developed than for ammonium sulfate. Recent studies have explored characteristics of dry and aqueous methyl- and ethyl-aminium sulfates including their densities and thermostability (Qiu and Zhang, 2012; Lavi et al. 2013; Clegg et al. 2013), hygroscopic and crystallization behavior (Qiu and Zhang, 2012; Chan and Chan, 2013), as well as the ability to act as cloud condensation nuclei (CCN) (Lavi et al. 2013). Methyl- and ethyl-aminium sulfates appear to have hygroscopic growth factors (based upon particle radius) that differ significantly from those of ammonium sulfate over a wide range of *RH*, with decreasing growth factors as the number of alkyl-group carbons increase (Qiu and Zhang, 2012). When converted to water uptake on a molar basis these results are much closer to those for $(\text{NH}_4)_2\text{SO}_4$ (Clegg et al. 2013, Fig. 7c), but the scatter in the data make it difficult to draw firm conclusions or clearly differentiate the behavior of one salt from another. In drying experiments using an electrodynamic balance, supermicron droplets of primary methyl- and ethyl-aminium sulfates formed stable crystals, while the secondary and tertiary amines showed non-crystalline or liquid phase states even under dry conditions (Chan and Chan, 2013). Furthermore, secondary and tertiary alkyl-amines (re-)evaporated from aminium sulfate particles upon drying at room temperature under amine-free gas phase conditions. For instance, trimethylamine sulfate droplets with an initial molar aminium:sulfate ratio of 2:1 was found to have a stoichiometric ratio of 1:1 under dry amine-free conditions (Chan and Chan, 2013). This observation demonstrates the need to minimize or correct for amine evaporation in studying these salts, especially under low *RH* conditions.

1
2
3
4
5 Water and solute activities in aqueous aerosols are needed in order to calculate gas/liquid/solid
6 partitioning in the atmosphere and understand the role of aerosols in atmospheric processes. The
7 behavior of mixtures containing common inorganic salts, acids, and bases is relatively well understood
8 and a number of models of their equilibrium thermodynamic properties have been developed (e.g.,
9 Zhang et al. 2000; Wexler and Clegg, 2002; Fountoukis and Nenes, 2007; Zuend et al. 2011). However,
10 present knowledge of amines and aminium salts is limited. There have been a few studies of osmotic
11 coefficients of aminium chlorides (Macaskill and Bates, 1986) and nitrates (Bonner 1981), but there
12 are no direct measurements of water activities of aminium sulfates or their mixtures with other solutes.
13 In the Extended Aerosol Inorganics Model (*E-AIM*, Wexler and Clegg, 2002), it assumed that aminium
14 cations interact with anions in the same way as ammonium, NH_4^+ (Clegg et al. 2013). The accuracy of
15 this approximation is not known.
16
17
18
19
20
21

22 Besides the commonly used isopiestic method of measuring water activities (e.g. Rard and Platford,
23 1991), direct static and direct dynamic methods exist (Blandamer et al. 2005). In studies of aerosols in
24 the laboratory, electrodynamic balances and hygroscopic tandem differential mobility analyzers
25 (HTDMAs) have often been deployed to indirectly determine the relationship between concentration
26 and water activity. These aerosol techniques can cover a wide range of relative humidities and allow
27 measurements of solutions supersaturated with respect to the dissolved solutes. To account for the
28 possibility of evaporative losses of solute, Peng and Chan (2001) and Lightstone et al. (2000) have
29 described correction techniques for carboxylic acids and ammonium nitrate. However, amine
30 evaporation, which is to be expected for the salts of secondary and tertiary methyl- and ethylamines,
31 can lead to mass decreases of the total solute in the case of nitrate and chloride salts and changes in the
32 aminium:sulfate ratio in the case of sulfate salts. This poses a challenge to measuring water activities
33 of aqueous aminium sulfates while maintaining a constant aminium:sulfate ratio.
34
35
36
37
38
39
40

41 In this work water activities (a_w) have been measured for mixtures of sulfuric acid and five
42 alkylaminium sulfates of high atmospheric relevance: methylaminium sulfate (MAS), ethylaminium
43 sulfate (EAS), dimethylaminium sulfate (DMAS), diethylaminium sulfate (DEAS), and
44 trimethylaminium sulfate (TMAS), for various aminium:sulfate molar ratios at 25 °C. By using bulk
45 solutions in the experiments the potential evaporation of amines during the measurements was
46 minimized relative to other methods (Chan and Chan, 2013). (In contrast to aerosols, a bulk solution
47 has a low surface area to volume ratio resulting in much less evaporation, at the expense of the ability
48 to study supersaturated solutions.) Measurements were made at four different aminium:sulfate molar
49 ratios (approximately 0.5:1, 1:1, 1.5:1 and 2:1) for mixtures containing each amine. To facilitate
50 comparison of the results of this study and those of Clegg et al. (2013) at molar ratios of 2:1 (aminium
51 sulfate), and to enable water activities to be calculated for any ratio, we have interpolated the
52 experimental data to fixed water activities and fitted the values with an extended
53
54
55
56
57
58
59
60

Zdanovskii-Stokes-Robinson equation (Clegg et al. 2003). We have also used the ion-interaction model of Pitzer, Simonson, and Clegg (Clegg et al. 1992) to represent osmotic and activity coefficients of the five pure aqueous aminium sulfates over a wide range of concentrations.

2. THEORY

2.1 Osmotic coefficients

Osmotic coefficients (ϕ) are related to water activities (a_w) according to the equation:

$$\ln(a_w) = -(\sum_i m_i \cdot \phi \cdot M_w / 1000) \quad (1)$$

where m_i is the molality of ion or uncharged solute species 'i' (in mol kg⁻¹ water), and M_w (g) is the molar mass of water (Robinson and Stokes, 1970). Because the distribution of total sulfate ($\text{SO}_4^{2-}(\text{tot})$) between HSO_4^- and SO_4^{2-} forms in our experiments is not known, all osmotic coefficients presented in this work are stoichiometric or total values (ϕ_{st}). These are related to the measured water activity by:

$$\phi_{\text{st}} = -\ln(a_w) / (m_{\text{st}} \cdot M_w / 1000) \quad (2)$$

where m_{st} is the stoichiometric molality $m_{\text{st}} = m\text{H}^+(\text{tot}) + m\text{CH}_3\text{NH}_3^+ + m\text{SO}_4^{2-}(\text{tot})$ (where CH_3NH_3^+ is the aminium ion of interest), or simply $3m\text{SO}_4^{2-}(\text{tot})$.

2.2 Extended Zdanovskii-Stokes-Robinson (ZSR) model

This is a widely used method of estimating the solvent content of solution mixtures from those of solutions of the individual pure solutes at the same solvent activity as the mixture (Stokes and Robinson, 1966). In the present study we have applied a simplified version of the extended ZSR approach of Clegg et al. (2003), see their Eq. 7, to represent water activities and osmotic coefficients of ternary mixtures of aminium sulfate - H_2SO_4 - H_2O :

$$W_{\text{tot}} = w_a^0 + w_{\text{as}}^0 + (n_a + n_{\text{as}}) x_a x_{\text{as}} \cdot A^0 \quad (3)$$

where W_{tot} denotes the total mass of water in the solution mixture, and w^0 is the amount of water associated with the acid 'a' or aminium sulfate 'as' in a pure aqueous solution at the same water activity as the mixture. The molar amount of each solute present in the mixture is denoted by n , and the mole fractions of the two dry solutes are calculated as $x_a = n_a / (n_a + n_{\text{as}})$ and $x_{\text{as}} = n_{\text{as}} / (n_a + n_{\text{as}})$. We fitted Eq. 3 to the experimental results to determine the empirical parameter A^0 and calculate the

water amounts (in kg H₂O per mole of solute) associated with the pure aminium sulfate salt (w_{as}^0) over a wide range of water activity.

2.3 Ion interaction Model

The Pitzer, Simonson, and Clegg thermodynamic model (Clegg et al. 1992) is a mole fraction based ion interaction model which can represent solvent and solute activities in pure solutions and mixtures to very high solute concentrations. We have fitted this model to the osmotic coefficients of the pure aqueous aminium sulfates determined in this study. The equation, for the water activity a_w , is given below for a solution containing a single electrolyte solute ($M_{v+}X_{v-}$) and water:

$$\ln(a_w) = \ln(x_w) + 2A_x I_x^{3/2} / (1 + \rho I_x^{1/2}) - x_M x_X B_{MX} \exp(-\alpha I_x^{1/2}) + x_1^2 (W_{w,MX} + (x_1 - x_w) U_{w,MX}) + 4x_w x_M x_X (2 - 3x_w) V_{w,MX}, \quad (4)$$

where A_x is the mole fraction Debye-Hückel constant (2.917 at 298.15 K), I_x is the ionic strength (equal to $0.5 \sum_i x_i |z_i|^2$), ρ is a constant set equal to 13.0, x_w denotes the mole fraction of water, and x_1 denotes the total mole fraction of ions ($x_M + x_X$). The coefficient α is equal to 13.0. The Debye-Hückel term (the second one on the first line of Eq. 4) describes the behavior of very dilute solutions. The model equation includes four fitted interaction parameters B_{MX} , $W_{w,MX}$, $U_{w,MX}$ and $V_{w,MX}$, that describe mid- and short-range interactions between water, sulfate (X), and aminium cations (M).

3. METHODS

Samples containing both sulfuric acid and each of the individual amines were prepared at four aminium:sulfate ratios of approximately 0.5:1, 1:1, 1.5:1 and 2:1. Because of the approximate concentrations of the amine stock solutions (see below) and unknown degree of evaporation of the amines during sample preparation, aminium and sulfate concentrations in the primary samples were measured by ion chromatography to determine the exact mole ratios. Water activities of the solutions, and their dilutions with water, were determined using a water activity meter using the chilled mirror dew point technique.

3.1 Preparation of solutions and determination of mole ratios

The stock solutions were prepared from concentrated sulfuric acid (H₂SO₄, 95 – 98 wt%, Acros Organics), and concentrated amine solutions, to achieve the highest possible molar fractions of the solute (and lowest possible water contents) without requiring additional drying steps. The H₂SO₄ was titrated against standardized NaOH and found to have a concentration of 95.51 ± 0.16 wt%.

1
2
3 Methylamine (MA, 37 – 43 wt% in H₂O, Aldrich), dimethylamine (DMA, 38 – 42 wt% in H₂O,
4 Aldrich), and trimethylamine (TMA, ~ 45 wt% in H₂O, Aldrich) were used without further treatment,
5 while ethylamine (EA, 69 – 72 wt% in H₂O, Aldrich) and diethylamine (DEA, > 99 wt%, Fluka)
6 were diluted with ultrapure water (18.2 mΩ) to approximately 50 wt% before mixing with the H₂SO₄.
7 Unique to the DEA system, we observed a mildly yellow color developing within a few hours upon
8 dilution of 99wt% DEA with ultrapure water. The color intensified when further mixed with H₂SO₄.
9 Using ion chromatography (IC), no significant change in the DEAH⁺ aminium ion concentration was
10 detected, suggesting that only trace amounts of DEA reacted to form the yellow by-product.
11
12
13
14
15

16 The stock solutions of all the mixtures were prepared in a similar way to the following example. For
17 the 2.0:1 dimethylaminium sulfate (DMAS) solution a mass of 4.0332 g of concentrated H₂SO₄
18 (containing 0.0393 mol of sulfate) was weighed into a glass container and immersed into an ice bath
19 to cool for several minutes. Next, 9.4775 g of 40.0 wt% DMA solution (containing approximately
20 0.0841 mol of amine) was added drop-wise under continuous shaking in ice water. The mass of
21 amine solution to be added was calculated from the stock solution concentrations, plus an additional
22 few percent to compensate for potential amine evaporation during mixing. Finally, the stock solution
23 was sealed and weighed again to determine the total amount of added amine solution. Further
24 samples were prepared by diluting known masses from each stock solution with ultrapure water.
25
26
27
28
29

30 Despite constant cooling, amine evaporation during preparation of stock solutions could not be fully
31 prevented. To determine the exact aminium:sulfate ratios, the aminium and sulfate contents of the
32 stock solutions for each of the four ratios, and for mixtures containing each amine, were measured by
33 ion chromatography (IC). We assumed that H₂SO₄ evaporation did not occur due to its extremely low
34 volatility. Molalities of aminium and H⁺ ion were calculated from the known mass of 95.51 wt%
35 H₂SO₄ stock solution present (yielding the concentration of sulfate ion), and the molar
36 aminium:sulfate ratio as determined by IC. Uncertainties in the ratio ranged between 1.2% and 5.8%.
37 In the case of the above mentioned DMAS example, the amount of dimethylaminium ion determined
38 in this way accounted for 0.0769 ± 0.0012 mol of DMA. Molar amounts (*n*) of total H⁺ in each
39 sample were calculated as $nH^+ = 2nSO_4^{2-} - nCH_3NH_3^+$, where CH₃NH₃⁺ represents any of the five
40 aminium cations. The mass of water in each sample was calculated from the following formula:
41 $(1.0 - 0.9551) \cdot massH_2SO_4(\sim 95 \text{ wt\% stock}) + (massCH_3NH_2(\sim 40 \text{ wt\% stock}) - massCH_3NH_2) + massH_2O_{added}$,
42 where *mass*CH₃NH₂ is the mass of amine present, calculated from the molalities of aminium, and
43 *mass*H₂O_{added} is the mass of water added to dilute the stock solution of the mixture to obtain the
44 sample to be measured.
45
46
47
48
49
50
51
52

53 For the IC measurements aliquots of all solutions were diluted with ultrapure water to 1 – 10 mg L⁻¹
54 (Metrohm, 881 compact IC Pro). The aminium cations were measured using a Metrosep C4 column
55 and an eluent of 3.0 mM HNO₃, 0.14 mM pyridine-2,6-dicarboxylic acid and 2% acetone; sulfate
56
57
58
59
60

1
2
3 concentrations were determined by a DIONEX IonPac® AS14A column eluted with a 1.0 mM
4 Na₂CO₃, 10.0 mM NaHCO₃ solution. Cation and anion standards for IC calibration were prepared
5 from amine hydrochlorides (NH₂CH₃HCl 99%, NH(CH₃)₂HCl 99%, N(CH₃)₃HCl 98%,
6 NH₂CH₂CH₃HCl 98%, NH(CH₂CH₃)₂HCl 99%, all from Sigma Aldrich, and dried under vacuum
7 over 18 h at 333 K), and ammonium sulfate ((NH₄)₂SO₄ > 99%, Sigma Aldrich), respectively. As
8 expected, the actual aminium:sulfate ratios measured by IC were lower than the nominal values
9 because of amine evaporation due to the heat of mixing and their volatile nature,. For example the
10 TMAH⁺:SO₄²⁻ ratio of the stock that was prepared as ~2:1 was found to be 1.78:1. Despite the
11 evaporation during sample preparation, the aminium:sulfate ratios of the samples prepared in this
12 study were still significantly higher (due to much lower losses of the amines) than those obtained by
13 drying mixed dilute solutions (Chan and Chan, 2013).
14
15
16
17
18
19
20
21

22 3.2 Water activity measurements

23 A water activity meter (Aqua lab Series 3TE, Decagon devices, Inc.) was used to determine the water
24 activities of bulk test solutions at 25.0 ± 0.2 °C, by measuring the equilibrium relative humidities
25 above the samples. The *RH*, expressed as a fraction, is related to the water activity (*a_w*) by:
26
27

$$28 \quad a_w = p(\text{H}_2\text{O}) / p^0(\text{H}_2\text{O}) = RH. \quad (5)$$

29
30
31
32 where *p*(H₂O) is the equilibrium partial pressure of water above the solution, and *p*⁰(H₂O) the vapor
33 pressure of pure water at the same temperature. The experimental uncertainty of the water activity
34 measurements was estimated to be within ± 0.003. During the course of the experiments
35 aminium:sulfate ratios of some of the samples were measured again, both before and after *a_w*
36 determination, and found to be unchanged from those of the initial stock solutions (within
37 experimental uncertainty). This confirmed that amine evaporation from the bulk samples was
38 negligible. The measured water activities, and calculated osmotic coefficients, are listed in Table 1.
39
40
41
42
43
44
45

46 4. RESULTS AND DISCUSSION

47 In this section we present measured water activities and osmotic coefficients of aminium - H⁺ - SO₄²⁻
48 aqueous solutions, and describe trends from low to high aminium:sulfate ratios. We also compare
49 values fitted using Eq. 3 to the measurements in order to evaluate the model's performance and the
50 limits of its application to aminium sulfate systems. Osmotic coefficients of aminium sulfates and
51 bisulfates obtained from the fitted Eq. 3 are then compared with those of their ammonium
52 counterparts and literature data, and findings are discussed. Last, the results of parameterization of
53 the ion interaction model (Eq. 4) are presented.
54
55
56
57
58
59
60

4.1 Changes of osmotic coefficient with increasing solute molality and aminium:sulfate ratios

To illustrate the trends from aqueous H_2SO_4 solutions to the fully neutralised aqueous $(\text{CH}_3)_n\text{NH}_{4-n})_2\text{SO}_4$ and $(\text{CH}_3\text{CH}_2)_n\text{NH}_{4-n})_2\text{SO}_4$, osmotic coefficients of solutions with different aminium:sulfate ratios are plotted against the square root of the sulfate molality in Fig. 1. Results for three aminium:sulfate molar ratios are shown for mixtures containing each aminium salt, for example 0.45:1, 0.89:1 and 1.95:1 for MAS.

For sulfate molalities between 0 and 1 mol kg^{-1} , osmotic coefficients at all aminium:sulfate ratios fall steeply, as expected, although the larger uncertainties in the osmotic coefficient at these high water activities mask a clear differentiation of the behavior of the solutions at different ratios. At molalities above 1 mol kg^{-1} of sulfate the osmotic coefficients of the solutions for the three aminium:sulfate ratios are quite different, with values in most instances much higher than those of $(\text{NH}_4)_2\text{SO}_4$ solutions of the same molality. (This corresponds to *lower* water activities.) The trends are similar for the mixtures for all five aminium salts. Because the aminium:sulfate ratios of the test solutions varied between the different amines studied, more direct comparisons are made with osmotic coefficients determined using the fitted Eq. 3, and are described in the subsections below.

4.2 Parameterization of the extended ZSR model

Because all measurements were made at distinct molalities rather than fixed water activity, which is the primary variable in the ZSR model, osmotic coefficients were first calculated at a series of fixed a_w ranging from about 0.4 to 0.975 for each aminium:sulfate ratio. This was done by linearly interpolating the experimental osmotic coefficients (plotted against the square root of sulfate molality). These interpolated values are listed in Table 1 of the Supplementary Information. The results of the interpolations were then fitted to Eq. 3, at each fixed a_w and for the full experimental range of aminium:sulfate ratios, to establish the model parameters for all mixtures. The number of moles of water associated with 1 mole of H_2SO_4 at each water activity, which is accurately known, was calculated from the equations of Clegg and Brimblecombe (1995). The unknowns in Eq. 3 are then w_{as}^0 , which is the moles of water associated with one mole of the pure aminium salt at each fixed a_w , and the mixture parameter A^0 . Fitted parameters and their uncertainties are listed in Table 2.

Representative results of the fits of Eq. 3 to the interpolated data are shown in Fig. 2, for a series of water activities from 0.65 to 0.95. Moving from left to right, the lines on each plot show the transition from pure aqueous H_2SO_4 ($m_{\text{salt}} = 0\text{ mol kg}^{-1}$) to the pure aqueous aminium sulfate salts ($m_{\text{acid}} = 0\text{ mol kg}^{-1}$). The methylaminium sulfate (MAS, Fig. 2a) and dimethylaminium sulfate (DMAS, Fig. 2b) data are fitted well over the entire composition range, including the solutions with

compositions very close to pure aminium sulfate. In the case of trimethylaminium sulfate (TMAS, Fig. 2e) there is a suggestion that the model-calculated molalities for the pure aminium sulfate composition are too low (therefore yielding osmotic coefficients that are too high), because of the shape of the fitted curves very close to the x-axis. This may also be true for ethylaminium sulfate (EAS, Fig. 2b) at the lowest a_w fitted, although the results are less clear. In some of the DEAS solutions the amine was in excess, resulting in small negative values of m_{acid} for two of the solutions shown in Fig. 2d. Calculated water activities for the aqueous $(\text{NH}_4)_2\text{SO}_4$ - H_2SO_4 system are shown in Fig. 2f. For compositions between NH_4HSO_4 and $(\text{NH}_4)_2\text{SO}_4$ the results are clearly very different from those for the aminium-based systems, especially for the pure sulfate salt. This is discussed further below. The fit of Eq. 3 at a single water activity is shown in Fig. 3 for aqueous mixtures of each aminium salt with H_2SO_4 . The parameter A° in Eq. 3 accounts for the observed departure from linear behavior (which would yield a straight line between the $\text{kg H}_2\text{O mol}^{-1}$ values of the two pure solutes).

The results from the fitted Eq. 3 are compared in Fig. 4 with measured and interpolated osmotic coefficients in order to investigate the performance of the model in estimating osmotic coefficients at arbitrary aminium:sulfate ratios. Two aminium:sulfate ratios were initially selected: values close to 2:1 and close to 1:1. The results for MAS and DMAS are satisfactory for both ratios, with the fitted Eq. 3 yielding osmotic coefficients that agree with the measurements to within the uncertainty in the model. However, in the cases of EAS (ratio 0.95:1) and TMAS (ratio 1.78:1) there are consistent offsets, with the osmotic coefficients calculated from the measurements lying at the limit of the uncertainty of the model. The same deviations are visible for these ratios in Fig. 2b,e. However, for both salts the deviations of the measured solution molalities from the fitted values, for the nearest ratios to those noted above, lie in the opposite direction. The results for these ratios are shown as osmotic coefficients in Fig. 4f. As expected, the deviations shown in these plots are of opposite sign to those shown in Fig. 4b,e for the closely similar ratios. This confirms they are due to differences in the experimental results, rather than systematic deviations of the model from the data.

For DEAS there are similar consistent differences between measured and fitted osmotic coefficients for the 1.03:1 molar ratio, but there are no data for ratios close to this for comparison. For those DEAS solutions in which the amine was in excess, leading to m_{acid} values below zero in Fig. 2d, the water associated with this excess (hence its effect on the molalities m_{acid} and m_{salt}) was estimated by assuming the excess amine takes up water according to Raoult's law, thus

$$a_w = x_{\text{H}_2\text{O}} = n_{\text{H}_2\text{O}} / (n_{\text{H}_2\text{O}} + n_{\text{Amine}}). \quad (6)$$

The total amount of water, for these cases, is therefore assumed to be the sum of the water associated with the pure aminium salt (one of the fitted parameters in Eq. 3) and water associated

1
2
3 with excess amine for the experimental water activity and obtained using Eq. 6. As shown on
4 Fig. 4e, the treatment of the additional amine in this way yields good agreement with the
5 experimental results.
6
7

8
9 Overall, the extended ZSR approach embodied in Eq. 3 provides, within the margins of error, good
10 fits to measurements, despite the relatively few data. Nevertheless, there is no reason why the simple
11 model equation should exactly represent the underlying relationship between water activity and
12 composition, complicated as it is by the equilibrium between H^+ , SO_4^{2-} , and HSO_4^- ions. Such a
13 difference is apparent in Fig. 2 for aminium:sulfate ratios closest to pure aqueous H_2SO_4 : the fitted
14 molalities are greater than those of the test solutions, for all the salts, for water activities of 0.75 and
15 0.65. This will result in model-calculated osmotic coefficients that may be too low, which should be
16 borne in mind when using the equations.
17
18
19
20
21
22

23 **4.3 Comparison of aminium sulfates and bisulfates and their ammonium counterparts**

24 Osmotic coefficients of aqueous aminium bisulfates and sulfates are compared in Fig. 5 to those of
25 their ammonium counterparts (from the work of Clegg et al. [1998], and calculated using the online
26 *E-AIM* model). Within the experimental uncertainty, values for the aqueous aminium bisulfates are
27 in good agreement with ammonium bisulfate, suggesting that at an aminium:sulfate ratio of 1:1
28 (Fig. 5a) osmotic coefficients of NH_4HSO_4 serve as a reasonable proxy for the ϕ_{st} of aqueous
29 aminium bisulfate solutions.
30
31
32
33

34
35 However, as the aminium:sulfate ratio increases from 1:1 to 2:1 (see Fig. 5b), which corresponds to
36 pure aqueous aminium sulfate solutions, the osmotic coefficients increase significantly. There are
37 substantial differences from the osmotic coefficients of ammonium sulfate solutions. These
38 correspond to lower water activities for any given concentration or, conversely, higher water uptake
39 for a given water relative humidity (equilibrium water activity). In contrast, the osmotic coefficients
40 of NH_4HSO_4 and $(NH_4)_2SO_4$ solutions exhibit only small differences from each other over the entire
41 concentration range.
42
43
44

45
46 Solutions of the primary aminium sulfates (MAS, EAS) have osmotic coefficients closer to
47 ammonium sulfate than the secondary and tertiary aminium compounds (DMAS, DEAS, and
48 TMAS). The relative values of the osmotic coefficients at higher molalities, shown in Fig. 5b,
49 suggest that the numbers of methyl or ethyl groups in the aminium ion may have a stronger effect on
50 water activity than the alkyl chain length has. Similar trends have been observed by Bonner (1981)
51 for methylaminium chloride solutions, where $(CH_3)_3NHCl$ possesses the largest osmotic coefficients
52 followed by $(CH_3)_2NH_2Cl$ and CH_3NH_3Cl at molalities above 4 mol kg^{-1} .
53
54
55
56
57
58
59
60

1
2
3 To compare results of this study with those of Clegg et al. (2013) for the aqueous aminium sulfates
4 (their Table 6), we have plotted the moles of water per mole of solute for aqueous MAS, EAS,
5 DMAS, DEAS, and TMAS as a function of equilibrium relative humidity in Fig. 6. Significant
6 differences between all aminium sulfates can be seen (Fig. 6a). However, the results of Clegg et al.
7 (2013), shown in Fig. 6b, correspond quite closely to the properties of aqueous $(\text{NH}_4)_2\text{SO}_4$ at all
8 relative humidities and are similar to each other. The reason for the differences between the results of
9 the two studies are not known. Clegg et al. (2013) calculated water uptake as a function of relative
10 humidity from size-based hygroscopic growth factors measured by Qiu and Zhang (2012) using an
11 HTDMA, and measured densities of aqueous aminium sulfate solutions. Both the HTDMA
12 experiments and the preparation of the aminium sulfate salts included drying processes down to or
13 below 10% *RH*, which may have resulted in the evaporation of the amines and a change in the
14 aminium:sulfate ratios, as experienced by Chan and Chan (2013), but this cannot be confirmed. It
15 also seems unlikely that this alone could account for the large differences observed.

16
17
18
19
20
21
22
23
24 Figure 6c,d shows plots of the water uptake by aminium nitrate and aminium chloride salts (Bonner
25 1981; Macaskill and Bates 1986), compared with that of the corresponding ammonium compounds.
26 In both cases the aminium compounds are more hygroscopic than the ammonium salts, thus showing
27 the same qualitative behavior as observed in this study for the sulfates, but to a much smaller degree.
28
29
30
31
32

33 **4.4 Osmotic coefficients of the aminium sulfate salts represented using an ion interaction** 34 **model**

35
36
37 We have fitted Eq. 4 to stoichiometric osmotic coefficients of the pure aqueous aminium sulfates,
38 from the results listed Table 2, to enable the compounds to be included in models and to extrapolate
39 their properties to higher concentrations than those measured. The value of parameter $V_{w, \text{MX}}$ for each
40 salt was constrained so that calculated values of ϕ_{st} values remain above zero to extreme
41 concentration (very low water activity). The model parameters for the five salts are listed in Table 3.
42
43
44

45
46 Fitted osmotic coefficients, and the values obtained from the measurements in this study, are shown
47 in Fig. 7. Broadly, the salts with the larger cations (TMAS, DEAS) have the highest osmotic
48 coefficients for any given concentration while aqueous solutions of the salt with the smallest cation
49 (MAS) have osmotic coefficients closest to those of aqueous $(\text{NH}_4)_2\text{SO}_4$. It should be noted that the
50 parameterization is based on limited data from 1 to 9 mol kg^{-1} , hence uncertainties in the parameter
51 values – and especially in the calculated properties beyond the limits of the data – are large. However,
52 the fitted model enables both the easy calculation of osmotic and activity coefficients of aqueous
53 alkylaminium sulfates solutions, and allows them to be included in mixtures (using the same ion
54 interaction model).
55
56
57
58
59
60

5. SUMMARY

In this study water activities of aqueous solutions of five aqueous methyl- and ethyl-aminium sulfates were measured for a range of aminium:sulfate ratios including (close to) bisulfate and sulfate compositions. Volatilization of amine occurred during preparation of bulk solutions but not during the water activity measurements. We demonstrated that measurements on bulk samples, where neither sample preparation nor measurements involve any drying step, is effective in minimizing evaporation and ensuring stable solution compositions during water activity measurements. The use of ion chromatography to determine the cation and anion content of the sample solutions allowed the stoichiometric ratio of aminium to sulfate ions to be verified in the samples.

We used an extended ZSR model to fit the water activity data as a function of composition from pure aqueous H_2SO_4 (for which water activities are accurately known) to the pure aqueous aminium sulfates. From the results we obtained estimates of the osmotic coefficients of aqueous solutions of these five salts. At moderate to high concentration the osmotic coefficients are all higher than those of aqueous $(\text{NH}_4)_2\text{SO}_4$, implying a higher equilibrium water uptake by the aminium sulfates for a given relative humidity. They are thus more hygroscopic than ammonium sulfate, in the order $\text{TMS} > \text{DEAS} \approx \text{DMAS} > \text{EAS} \approx \text{MAS} > (\text{NH}_4)_2\text{SO}_4$. These results differ from those in an earlier study in which water uptake was measured using an HTDMA (Clegg et al. 2013). These differences remain to be resolved.

For mixture compositions of 1:1 aminium:sulfate ratio (i.e., aminium bisulfate) the results of our water activity measurements for all the salts agree, essentially to within experimental uncertainty, with values for NH_4HSO_4 at the same solute molality. Hence the use of osmotic coefficients of ammonium bisulfate as estimates of those of methyl- and ethyl-aminium bisulfates is a satisfactory approximation.

ACKNOWLEDGEMENT

This work was supported by the Research Grants Council of the Hong Kong Special Administrative Region, China (GRF 600112); and by an International Exchange grant from the Royal Society (IE1111149).

REFERENCES

Almeida, J., Schobesberger, S., Kürten, A., Ortega, I. K., Kupiainen-Maatta, O., Praplan, A. P.,

- 1
2
3 Adamov, A., Amorim, A., Bianchi, F., Breitenlechner, M., David, A., Dommen, J., Donahue, N.
4 M., Downard, A., Dunne, E., Duplissy, J., Ehrhart, S., Flagan, R. C., Franchin, A., Guida, R.,
5 Hakala, J., Hansel, A., Heinritzi, M., Henschel, H., Jokinen, T., Junninen, H., Kajos, M.,
6 Kangasluoma, J., Keskinen, H., Kupc, A., Kurten, T., Kvashin, A. N., Laaksonen, A., Lehtipalo,
7 K., Leiminger, M., Leppa, J., Loukonen, V., Makhmutov, V., Mathot, S., McGrath, M. J.,
8 Nieminen, T., Olenius, T., Onnela, A., Petaja, T., Riccobono, F., Riipinen, I., Rissanen, M.,
9 Rondo, L., Ruuskanen, T., Santos, F. D., Sarnela, N., Schallhart, S., Schnitzhofer, R., Seinfeld,
10 J. H., Simon, M., Sipila, M., Stozhkov, Y., Stratmann, F., Tome, A., Trostl, J., Tsagkogeorgas,
11 G., Vaattovaara, P., Viisanen, Y., Virtanen, A., Vrtala, A., Wagner, P. E., Weingartner, E., Wex,
12 H., Williamson, C., Wimmer, D., Ye, P., Yli-Juuti, T., Carslaw, K. S., Kulmala, M., Curtius, J.,
13 Baltensperger, U., Worsnop, D. R., Vehkamäki, H., and Kirkby, J. (2013). Molecular
14 Understanding of Sulphuric Acid-Amine Particle Nucleation in the Atmosphere. *Nature*
15 502(7471):359–363.
16
17 Blandamer, M. J., Engberts, Jan B. F. N., Gleeson, P. T., and Reis, Joao Carlos R. (2005). Activity
18 of Water in Aqueous Systems; A Frequently Neglected Property. *Chem. Soc. Rev.* 34(5):440–
19 458.
20
21 Bonner, O. D. (1981). Osmotic and Activity Coefficients of Methyl-substituted Ammonium
22 Nitrates at 298.15 K. *J. Chem. Eng. Data* 26(2):148–149.
23
24 Bzdek, B. R., Ridge, D. P., and Johnston, M. V. (2010). Amine Exchange into Ammonium
25 Bisulphate and Ammonium Nitrate Nuclei. *Atmos. Chem. Phys.* 10(8):3495–3503.
26
27 Chan, L. P. and Chan, C. K. (2012). Displacement of Ammonium from Aerosol Particles by Uptake
28 of Triethylamine. *Aerosol Sci. Technol.* 46:236–247.
29
30 Chan, L. P. and Chan, C. K. (2013). Role of the Aerosol Phase State in Ammonia/Amines
31 Exchange Reactions. *Environ. Sci. Technol.* 47(11):5755–5762.
32
33 Chang, I.-H., Lee, C.-G., and Lee, D. S. (2003). Development of an Automated Method for
34 Simultaneous Determination of Low Molecular Weight Aliphatic Amines and Ammonia in
35 Ambient Air by Diffusion Scrubber Coupled to Ion Chromatography. *Anal. Chem.*
36 75(22):6141–6146.
37
38 Clegg, S. L. and Brimblecombe, P. (1995). Application of a Multicomponent Thermodynamic
39 Model to Activities and Thermal Properties of 0 - 40 mol kg⁻¹ Aqueous Sulfuric Acid 328 K to
40 <200 K. *J. Chem. Eng. Data* 40:43-64.
41
42 Clegg, S. L., Brimblecombe, P., and Wexler, A. S. (1998). A Thermodynamic Model of the System
43 H⁺ - NH₄⁺ - SO₄²⁻ - NO₃⁻ - H₂O at Tropospheric Temperatures. *J. Phys. Chem. A*
44 102-2137-2154.
45
46 Clegg, S. L., Ho, S. S., Chan, C. K., and Brimblecombe, P. (1995). The Thermodynamic Properties
47 of Aqueous (NH₄)₂SO₄ to High Supersaturation, as a Function of Temperature. *J. Chem. Eng.*
48
49
50
51
52
53
54
55
56
57
58
59
60

- 1
2
3 *Data* 40: 1079-1090.
- 4
5 Clegg, S. L., Pitzer, K. S., and Brimblecombe, P. (1992). Thermodynamics of Multicomponent,
6 Miscible, Ionic Solutions. II. Mixtures Including Unsymmetrical Electrolytes. *J. Phys. Chem.*
7 96:9470-9479
- 8
9
10 Clegg, S. L., Qiu, C., and Zhang, R. (2013). The Deliquescence Behaviour, Solubilities, and
11 Densities of Aqueous Solutions of Five Methyl- and Ethyl-aminium Sulphate Salts. *Atmos.*
12 *Environ.* 73:145–158.
- 13
14
15 Clegg, S. L., Seinfeld, J. H., and Edney, E. O. (2003). Thermodynamic Modelling of Aqueous
16 Aerosols Containing Electrolytes and Dissolved Organic Compounds. II. An Extended Zdanovskii–
17 Stokes–Robinson Approach. *J. Aerosol Sci.* 34(6):667–690.
- 18
19
20 Fountoukis, C., and Nenes, A. (2007). ISORROPIA II: a Computationally Efficient
21 Thermodynamic Equilibrium Model for $K^+ - Ca^{2+} - Mg^{2+} - NH_4^+ - Na^+ - SO_4^{2-} - NO_3^- - Cl^- - H_2O$
22 aerosols. *Atmos. Chem. Phys.*, 7:4639-4659.
- 23
24
25 Ge, X., Wexler, A. S., and Clegg, S. L. (2011a). Atmospheric Amines – Part I. A Review. *Atmos.*
26 *Environ.* 45(3):524–546.
- 27
28 Ge, X., Wexler, A. S., and Clegg, S. L. (2011b). Atmospheric Amines – Part II. Thermodynamic
29 Properties and Gas/Particle Partitioning. *Atmos. Environ.* 45(3):561–577.
- 30
31
32 Kurtén, T., Loukonen, V., Vehkamäki, H., and Kulmala, M. (2008). Amines are Likely to Enhance
33 Neutral and Ion-induced Sulfuric Acid-Water Nucleation in the Atmosphere More Effectively
34 than Ammonia. *Atmos. Chem. Phys.* 8(14):4095–4103.
- 35
36
37 Lavi, A., Bluvshstein, N., Segre, E., Segev, L., Flores, M., and Rudich, Y. (2013). Thermochemical,
38 Cloud Condensation Nucleation Ability, and Optical Properties of Alkyl Aminium Sulphate
39 Aerosols. *J. Phys. Chem. C* 117(43):22412–22421.
- 40
41
42 Liang, Z., and Chan, C. (1997). A Fast Technique for Measuring Water Activity of Atmospheric
43 Aerosols. *Aerosol Sci. Technol.* 26:255-268.
- 44
45
46 Lightstone, J. M., Onasch, T. B., Imre, D., and Oatis, S. (2000). Deliquescence, Efflorescence, and
47 Water Activity in Ammonium Nitrate and Mixed Ammonium Nitrate/Succinic Acid
48 Microparticles. *J. Phys. Chem. A* 104(41):9337–9346.
- 49
50
51 Liu, Y., Ma, Q., and He, H. (2012). Heterogeneous Uptake of Amines by Citric Acid and Humic
52 Acid. *Environ. Sci. Technol.* 46(20):11112–11118.
- 53
54
55 Lloyd, J. A., Heaton, K. J., and Johnston, M. V. (2009). Reactive Uptake of Trimethylamine into
56 Ammonium Nitrate Particles. *J. Phys. Chem. A* 113(17):4840–4843.
- 57
58
59 Macaskill, J. B. and Bates, R. G. (1986). Osmotic and Activity Coefficients of Monomethyl-,
60 Dimethyl-, and Trimethylammonium Chlorides at 25°C. *J. Solution Chem.* 15(4):323–330.

- 1
2
3 Müller, C., Iinuma, Y., Karstensen, J., van Pinxteren, D., Lehmann, S., Gnauk, T., and Herrmann, H.
4 (2009). Seasonal Variation of Aliphatic Amines in Marine Sub-Micrometer Particles at the
5 Cape Verde Islands. *Atmos. Chem. Phys.* 9(24):9587–9597.
6
7
8 Murphy, S. M., Sorooshian, A., Kroll, J. H., Ng, N. L., Chhabra, P., Tong, C., Surratt, J. D.,
9 Knipping, E., Flagan, R. C., and Seinfeld, J. H. (2007). Secondary Aerosol Formation From
10 Atmospheric Reactions of Aliphatic Amines. *Atmos. Chem. Phys.* 7(9):2313–2337.
11
12 Myerson, A.S., Izmailov, A.F., and Na, H.-S. (1996). Thermodynamic Studies of Levitated
13 Microdroplets of Highly Supersaturated Electrolyte Solutions. *J. Crystal Growth.* 166:981-988.
14
15 Nielsen, C. J., Herrmann, H., and Weller, C. (2012). Atmospheric Chemistry and Environmental
16 Impact of The Use of Amines in Carbon Capture and Storage (CCS). *Chem. Soc. Rev.*
17 41(19):6684.
18
19
20 Peng, C. and Chan, C. K. (2001). The Water Cycles of Water-Soluble Organic Salts of Atmospheric
21 Importance. *Atmos. Environ.* 35(7):1183–1192.
22
23 Pratt, K. A., Hatch, L. E., and Prather, K. A. (2009). Seasonal Volatility Dependence of Ambient
24 Particle Phase Amines. *Environ. Sci. Technol.* 43(14):5276–5281.
25
26
27 Qiu, C., Wang, L., Lal, V., Khalizov, A. F., and Zhang, R. (2011). Heterogeneous Reactions of
28 Alkylamines with Ammonium Sulphate and Ammonium Bisulphate. *Environ. Sci. Technol.*
29 45(11):4748–4755.
30
31
32 Qiu, C. and Zhang, R. (2012). Physicochemical Properties of Alkylaminium Sulphates:
33 Hygroscopicity, Thermostability, and Density. *Environ. Sci. Technol.* 46(8):4474–4480.
34
35
36 Rard, J. A., and Platford, R. F. (1991). Experimental Methods: Isopiestic. In *Activity Coefficients in*
37 *Electrolyte Solutions*, 2nd Ed., ed. K. S. Pitzer, CRC Press, Boca Raton, p.209-278.
38
39 Rehbein, Peter J. G., Jeong, C.-H., McGuire, M. L., Yao, X., Corbin, J. C., and Evans, G. J. (2011).
40 Cloud and Fog Processing Enhanced Gas-to-Particle Partitioning of Trimethylamine. *Environ.*
41 *Sci. Technol.* 45(10):4346–4352.
42
43
44 Robinson, R. A. and Stokes, R. H. (1970). *Electrolyte Solutions*. Butterworth & Co., 571pp.
45 (Reprinted by Dover Publications, Mineola, New York, in 2002.)
46
47 Smith, J. N., Barsanti, K. C., Friedli, H. R., Ehn, M., Kulmala, M., Collins, D. R., Scheckman, J.
48 H., Williams, B. J., and McMurry, P. H. (2010). Observations of Aminium Salts in Atmospheric
49 Nanoparticles and Possible Climatic Implications. *Proc. Natl. Acad. Sci. U.S.A.* 107(15):6634–
50 6639.
51
52
53 Stokes, R. H., and Robinson, R. A. (1966). Interactions in Aqueous Nonelectrolyte Solutions. I.
54 Solute-solvent Equilibria. *J. Phys. Chem.* 70:2126-2130.
55
56
57 VandenBoer, T. C., Petroff, A., Markovic, M. Z., and Murphy, J. G. (2011). Size Distribution of
58
59
60

1
2
3 Alkyl Amines in Continental Particulate Matter and Their Online Detection in The Gas and
4 Particle Phase. *Atmos. Chem. Phys.* 11(9):4319–4332.

5
6 Wang, L., Lal, V., Khalizov, A. F., and Zhang, R. (2010). Heterogeneous Chemistry of Alkylamines
7 with Sulfuric Acid: Implications for Atmospheric Formation of Alkylammonium Sulphates.
8 *Atmos. Environ.* 44(7):2461–2465.

9
10 Wexler, A. S., and Clegg, S. L. (2002). Atmospheric Aerosol Models for Systems Including The
11 Ions H^+ , NH_4^+ , Na^+ , SO_4^{2-} , NO_3^- , Cl^- , Br^- , and H_2O . *J. Geophys. Res.-Atmos.* 107: D14, Art. No.
12 4207. (*E-AIM*: <http://www.aim.env.uea.ac.uk/aim/aim.php>)
13
14

15
16 Zhang, Y., Seigneur, C., Seinfeld, J. H., Clegg, S. L., Jacobson, M., and Binkowski, F. S. (2000). A
17 Comparative Review of Inorganic Aerosol Thermodynamic Equilibrium Modules: Similarities,
18 Differences, and Their Likely Causes. *Atmos. Environ.* 34:117-137.

19
20 Zuend, A., Marcolli, C., Booth, A. M., Lienhard, D. M., Soonsin, V., Krieger, U. K., Topping, D.
21 O., McFiggans, G., Peter, T., and Seinfeld, J. H. (2011). New and Extended Parameterization
22 of The Thermodynamic Model AIOMFAC: Calculation of Activity Coefficients for
23 Organic-Inorganic Mixtures Containing Carboxyl, Hydroxyl, Carbonyl, Ether, Ester, Alkenyl,
24 Alkyl, and Aromatic Functional Groups, *Atmos. Chem. Phys.*, 11: 9155–9206.
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

FIGURES

Figure Captions

FIGURE 1. Experimentally determined stoichiometric osmotic coefficients (ϕ_{st}) plotted against the square root of the total sulfate molality ($m_{SO_4^{2-}}$), for aqueous mixtures of all five aminium sulfates with H_2SO_4 , at three different aminium:sulfate molar ratios (noted on the plots). Different symbols are used for each ratio. The solid line shows values for aqueous $(NH_4)_2SO_4$ (Clegg et al. 1995), and the dashed line for aqueous H_2SO_4 (Clegg and Brimblecombe 1995). (a) MAS (methylaminium sulfate). (b) EAS (ethylaminium sulfate). (c) DMAS (dimethylaminium sulfate). (d) DEAS (diethylaminium sulfate). (e) TMAS (trimethylaminium sulfate).

FIGURE 2: Aminium sulfate (m_{salt}) and H_2SO_4 molalities (m_{acid}) in the mixtures, interpolated for fixed water activities from 0.65 to 0.95 (indicated on the plots). Symbols: values from Table 1 of the Supplementary Information. Lines: calculated using the fitted extended ZSR model (Eq. 3) using coefficients from Table 2. (a) MAS. (b) EAS. (c) DMAS. (d) DEAS. (e) TMAS. (f) Molalities of aqueous $(NH_4)_2SO_4$ - H_2SO_4 mixtures, calculated using the model of Clegg et al. (1998).

FIGURE 3: The mass (kg) of water per mole of total solutes, at a water activity of 0.70, plotted against the dry mole fraction of aminium sulfate salt present (x_{salt}), from pure aqueous H_2SO_4 ($x_{salt} = 0.0$) to pure aqueous aminium sulfate ($x_{salt} = 1.0$). Symbols: open circle – interpolated values from Table 1 of the Supplementary Information; filled circle – pure aqueous H_2SO_4 from the work of Clegg and Brimblecombe (1995). Lines – calculated using the fitted extended ZSR model (Eq. 3) using coefficients from Table 2. (a) MAS. (b) EAS. (c) DMAS. (d) DEAS. (e) TMAS.

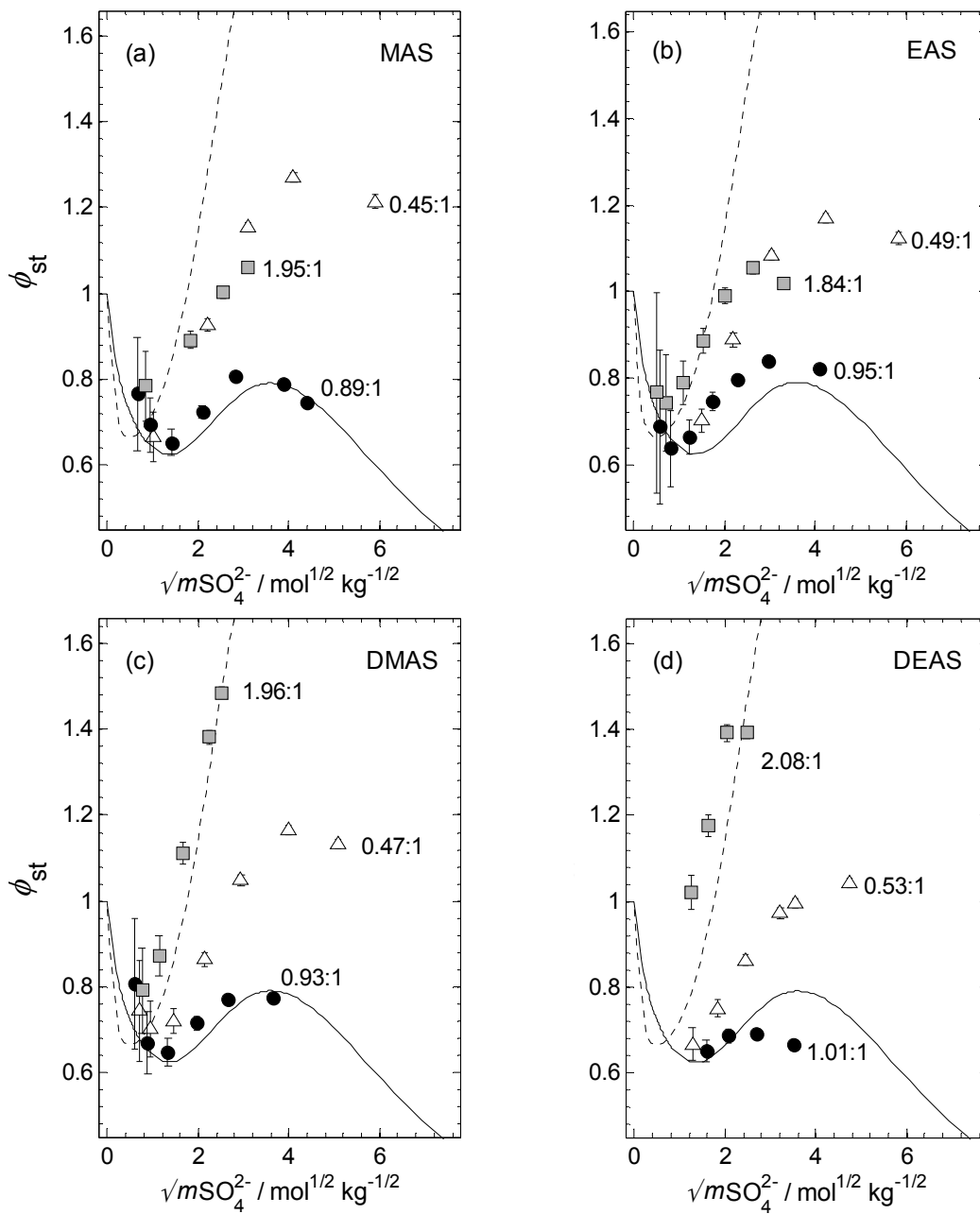
FIGURE 4. Stoichiometric osmotic coefficients (ϕ_{st}) plotted against the square root of the total sulfate molality ($m_{SO_4^{2-}}$), for aqueous mixtures of all five aminium sulfates with H_2SO_4 , at two different aminium:sulfate molar ratios (noted on the plots). Symbols: solid and shaded – experimental values (Table 1); open symbols – interpolated (Table 1 of the Supplementary Information). Lines: solid – from the fit of the extended ZSR model (Eq. 3), with coefficients listed in Table 2; dashed – these indicate the effects of the uncertainties in the fit of Eq. 3. (a) MAS. (b) EAS. (c) DMAS. (d) DEAS. (e) TMAS. (f) Additional results for EAS and TMAS (as indicated) for ratios close to those shown in plots (b) and (e).

1
2
3 FIGURE 5. Stoichiometric osmotic coefficients (ϕ_{st}) of aminium bisulfates
4 (aminium:sulfate ratio 1:1) and aminium sulfates (ratio 2:1) plotted against the square root
5 of total sulfate molality (mSO_4^{2-}). Symbols: values calculated using the extended ZSR
6 model (Eq. 3), with parameters listed in Table 2. Lines: values for aqueous NH_4HSO_4 (plot
7 a) and $(NH_4)_2SO_4$ (plot b) calculated from the results of Clegg et al. (1998), and Clegg et al.
8 (1995), respectively. The identities of the aminium salts in the mixtures are indicated on the
9 plots. (a) Aqueous aminium bisulfates, and NH_4HSO_4 . For clarity, the results for sulfates
10 EAS to TMAS are offset vertically by the amounts indicated in parentheses on the plot. (b)
11 Aqueous aminium sulfates, and $(NH_4)_2SO_4$.
12
13
14
15
16

17
18 FIGURE 6. Comparison of water uptake by different aminium salts plotted as moles of
19 water (nH_2O) per mole of salt against equilibrium relative humidity (RH , as a fraction).
20 Symbols: circle – methylaminium; solid circle - ethylaminium; square – dimethylaminium;
21 solid square – diethylaminium; triangle – trimethylaminium. (a) Sulfates (this study).
22 Values for the points were calculated using the extended ZSR model (Eq. 3), with
23 coefficients in Table 2. The lowest line on the plot is for aqueous $(NH_4)_2SO_4$ and was
24 calculated using the results of Clegg et al. (1995). Other lines, for each aminium sulfate,
25 were calculated using Eq. 4 and the parameters in Table 3. (b) Sulfates (Clegg et al. 2013).
26 The values for the points were taken from their Table 6. The line is for aqueous $(NH_4)_2SO_4$,
27 the same as in (a). (c) Nitrates (Bonner 1981). The line is for aqueous NH_4NO_3 , calculated
28 using the results of Clegg et al. (1998). (d) Chlorides (Macaskill and Bates 1986). The line
29 is for aqueous NH_4Cl , calculated using the equation of Liang and Chan (1997) and results of
30 Myerson et al. (1996).
31
32
33
34
35
36
37

38 FIGURE 7. Stoichiometric osmotic coefficients (ϕ_{st}) of the aminium sulfates, plotted against
39 the square root of sulfate molality (mSO_4^{2-}). Symbols: osmotic coefficients of each salt (as
40 indicated on the plot) calculated using Eq. 3 with the coefficients in Table 2. Lines: osmotic
41 coefficients fitted using the ion interaction model (Eq. 4), and calculated using the
42 parameters in Table 3.
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

FIGURE 1:



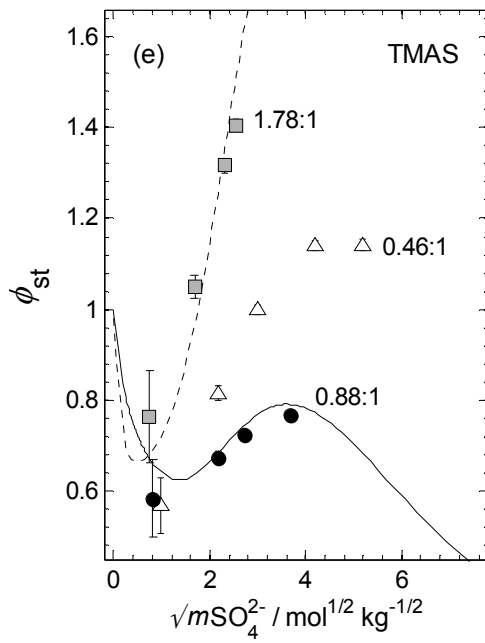


FIGURE 2:

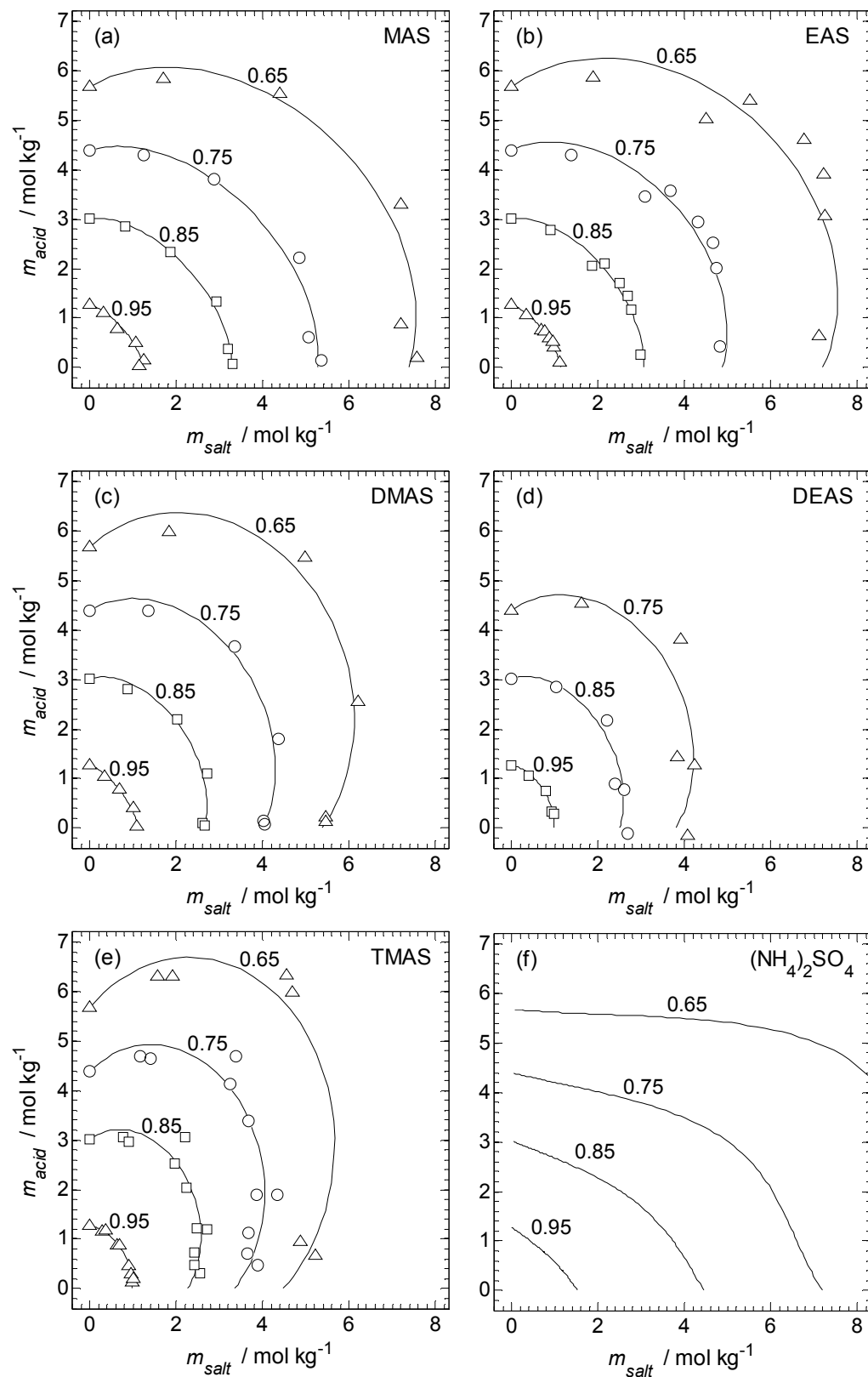


FIGURE 3:

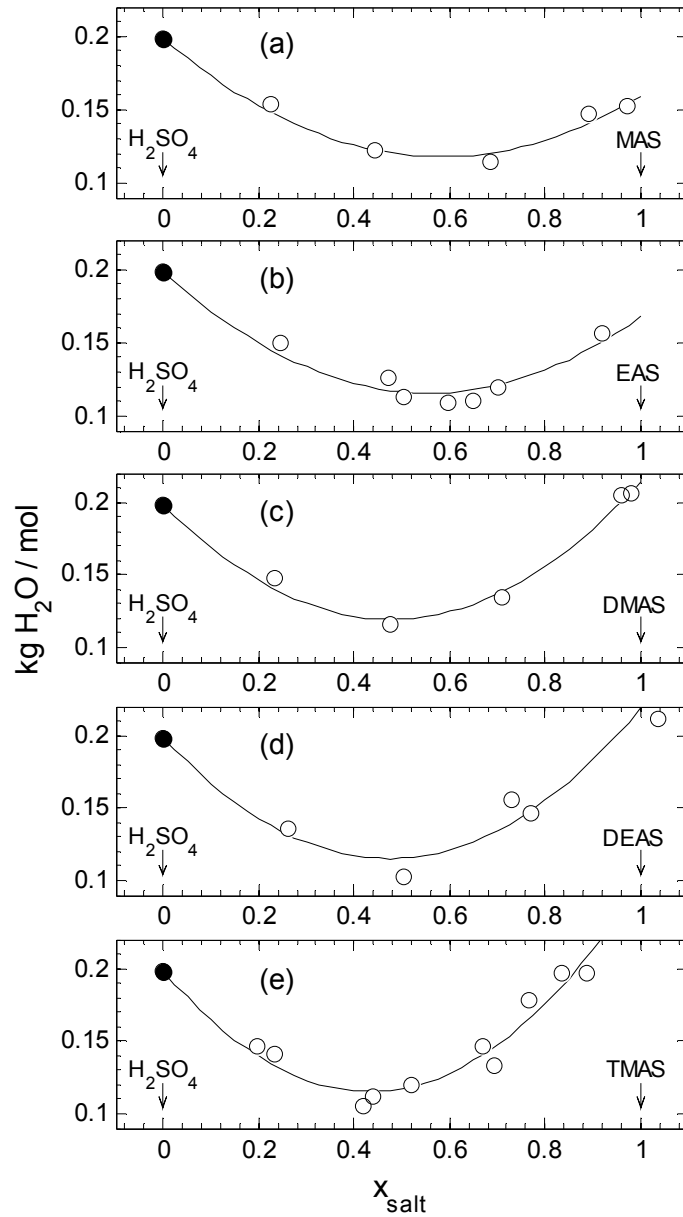
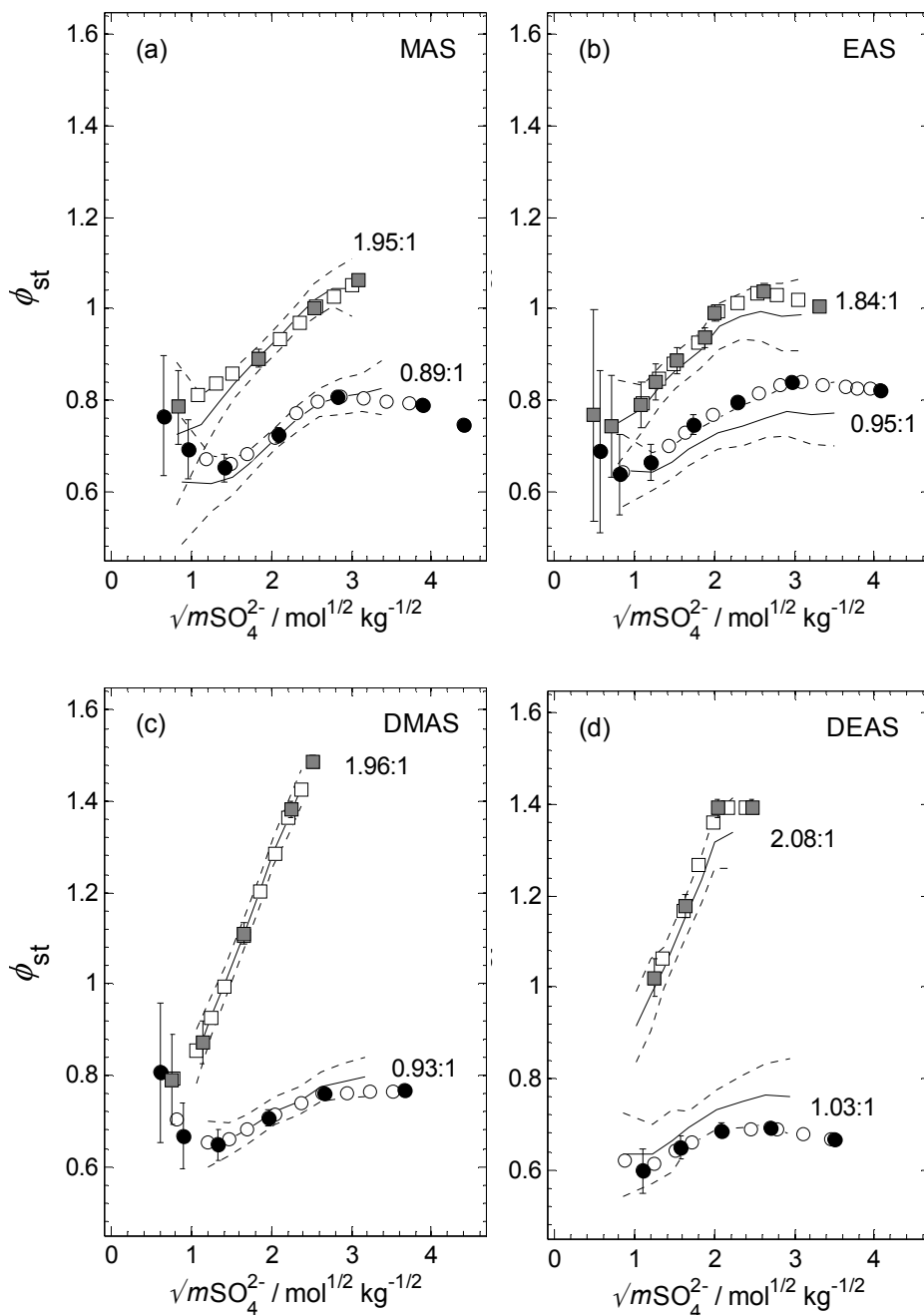


FIGURE 4:



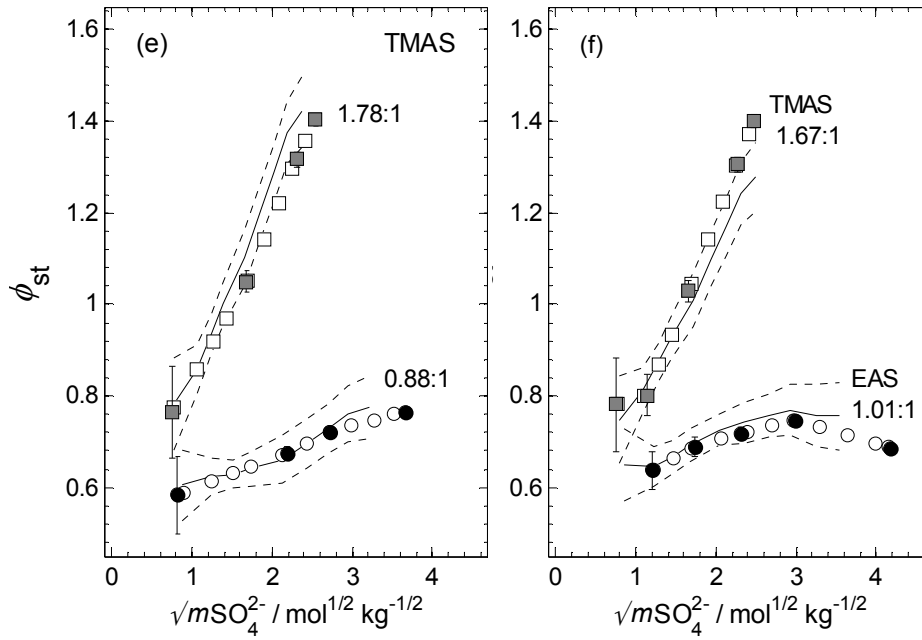


FIGURE 5:

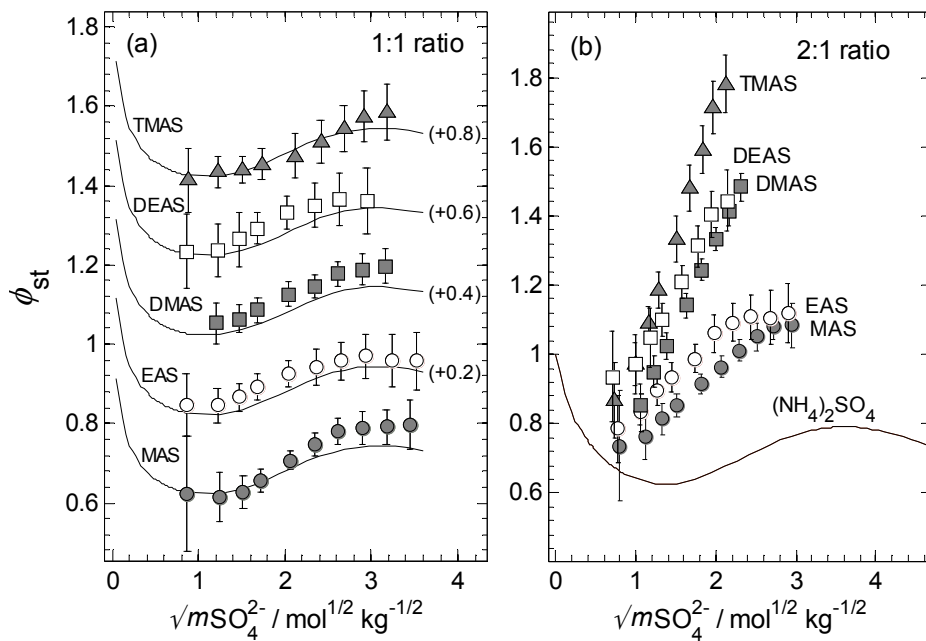


FIGURE 6:

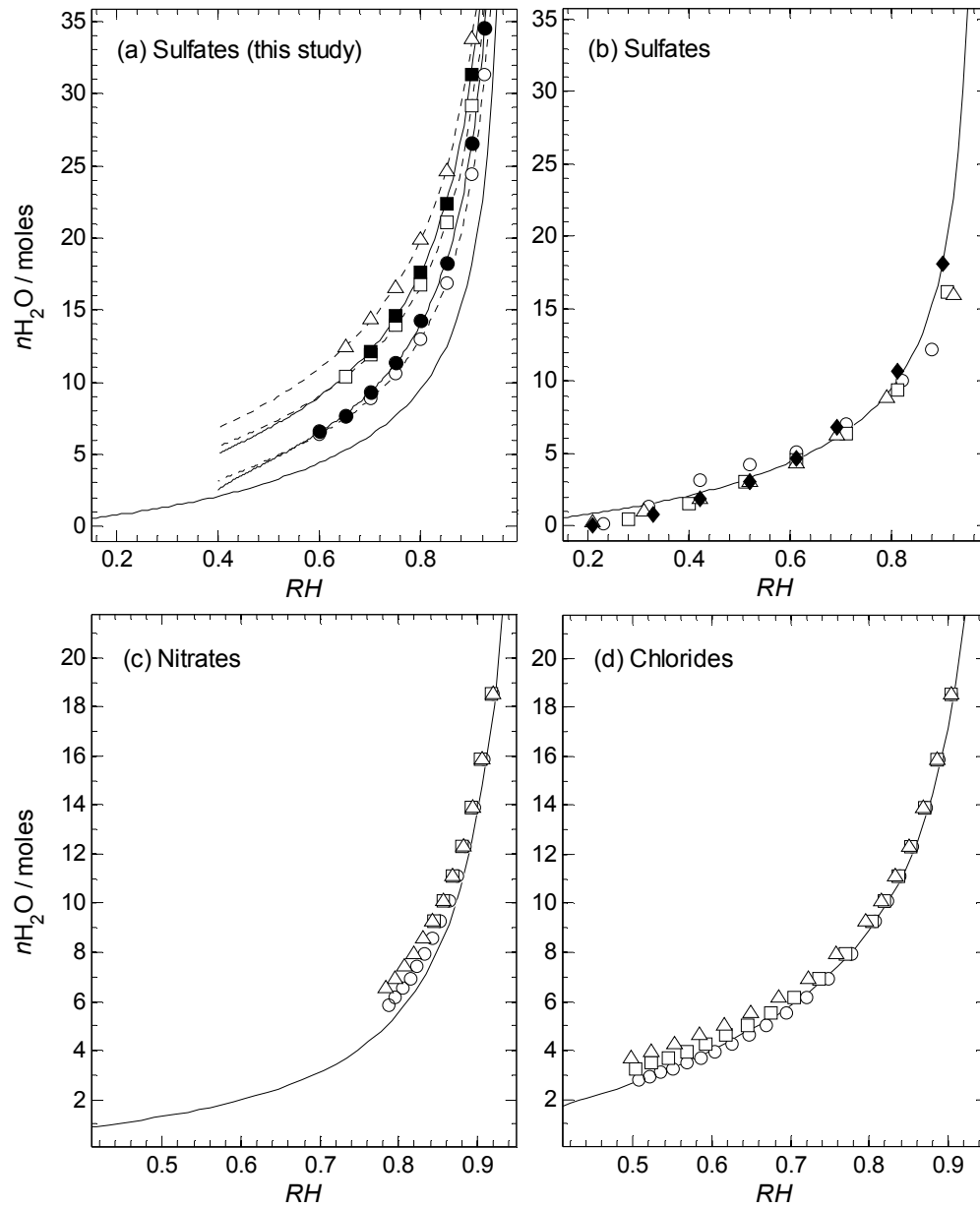
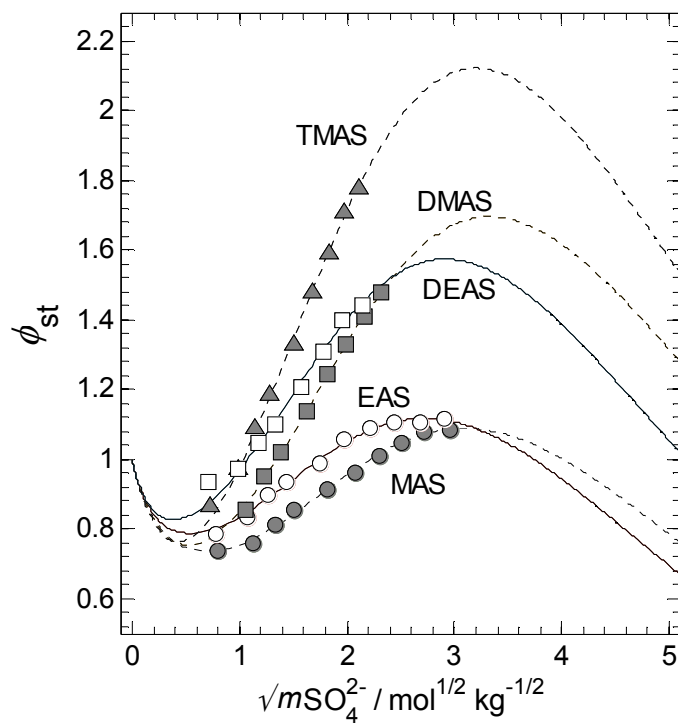


FIGURE 7:



TABLES

TABLE 1. Experimental Values of Water Activities (a_w) and Calculated Stoichiometric Osmotic Coefficients (ϕ_{st}) of Aminium Sulfate – H₂SO₄ Solutions at 25.0 ± 0.2°C.^a

	aminium:sulfate ratio ^b	a_w	$m\text{SO}_4^{2-}$ (mol kg ⁻¹) ^c	ϕ_{st}
MAS	0.4461 ± 0.0150	0.996	0.0513 ± 0.0013	(1.5664 ± 1.0878)
	0.4461 ± 0.0150	0.987	0.4873 ± 0.0119	0.4968 ± 0.1157
	0.4461 ± 0.0150	0.968	1.0204 ± 0.0249	0.5898 ± 0.0566
	0.4518 ± 0.0120	0.964	1.0191 ± 0.0206	0.6657 ± 0.0568
	0.4461 ± 0.0150	0.919	2.2869 ± 0.0558	0.6864 ± 0.0269
	0.4461 ± 0.0150	0.783	4.9235 ± 0.1202	0.9209 ± 0.0150
	0.4518 ± 0.0120	0.781	4.9268 ± 0.0997	0.9267 ± 0.0148
	0.4461 ± 0.0150	0.555	9.5249 ± 0.2325	1.1438 ± 0.0113
	0.4518 ± 0.0120	0.551	9.5332 ± 0.1929	1.1556 ± 0.0110
	0.4461 ± 0.0150	0.325	16.828 ± 0.4107	1.2358 ± 0.0110
	0.4518 ± 0.0120	0.314	16.872 ± 0.3413	1.2692 ± 0.0110
	0.4461 ± 0.0150	0.106	34.737 ± 0.5789	1.1954 ± 0.0153
	0.4518 ± 0.0120	0.101	34.931 ± 0.4493	1.2144 ± 0.0159
	0.8851 ± 0.0200	0.993	0.0435 ± 0.0010	(2.9913 ± 1.2875)
	0.8851 ± 0.0200	0.982	0.4307 ± 0.0101	0.7658 ± 0.1315
	0.8610 ± 0.0110	0.968	0.8832 ± 0.0142	0.6886 ± 0.0651
	0.8851 ± 0.0200	0.967	0.8961 ± 0.0210	0.6929 ± 0.0643
	0.8851 ± 0.0200	0.933	1.9796 ± 0.0464	0.6516 ± 0.0303
	0.8851 ± 0.0200	0.843	4.3775 ± 0.1025	0.7236 ± 0.0153
	0.8610 ± 0.0110	0.840	4.3006 ± 0.0692	0.7501 ± 0.0155
	0.8610 ± 0.0110	0.708	7.8069 ± 0.1256	0.8184 ± 0.0102
	0.8851 ± 0.0200	0.705	8.0047 ± 0.1875	0.8080 ± 0.0101
	0.8851 ± 0.0200	0.524	15.143 ± 0.3546	0.7897 ± 0.0073
	0.8610 ± 0.0110	0.522	14.542 ± 0.2339	0.8264 ± 0.0074
	0.8851 ± 0.0200	0.457	19.419 ± 0.2413	0.7454 ± 0.0064
	0.8610 ± 0.0110	0.448	18.539 ± 0.1247	0.8014 ± 0.0067
	1.3528 ± 0.0410	0.995	0.0359 ± 0.0010	(2.7555 ± 1.5556)
	1.3528 ± 0.0410	0.993	0.1813 ± 0.0052	0.7169 ± 0.3087
	1.3528 ± 0.0410	0.988	0.3765 ± 0.0108	0.5767 ± 0.1495
	1.3708 ± 0.0410	0.973	0.7800 ± 0.0224	0.6534 ± 0.0735
	1.3528 ± 0.0410	0.946	1.7189 ± 0.0494	0.6014 ± 0.0345
	1.3708 ± 0.0410	0.872	3.6827 ± 0.1056	0.6910 ± 0.0177
	1.3708 ± 0.0410	0.758	6.8136 ± 0.1950	0.7512 ± 0.0112

1					
2					
3		1.3708 ± 0.0410	0.613	11.893 ± 0.1768	0.7627 ± 0.0080
4		1.7819 ± 0.0510	0.999	0.0314 ± 0.0009	(0.3924 ± 1.7667)
5		1.7819 ± 0.0510	0.994	0.1235 ± 0.0036	0.9015 ± 0.4527
6		1.7819 ± 0.0510	0.989	0.3452 ± 0.0101	0.6110 ± 0.1631
7		1.7819 ± 0.0510	0.974	0.7029 ± 0.0206	0.6844 ± 0.0815
8		1.7819 ± 0.0510	0.944	1.5640 ± 0.0459	0.6818 ± 0.0381
9		1.7819 ± 0.0510	0.862	3.3066 ± 0.0971	0.8288 ± 0.0200
10		1.7819 ± 0.0510	0.723	6.2423 ± 0.1833	0.9600 ± 0.0130
11		1.7819 ± 0.0510	0.612	9.0849 ± 0.1316	0.9989 ± 0.0107
12		1.9486 ± 0.0160	0.971	0.7021 ± 0.0106	0.7846 ± 0.0816
13		1.9486 ± 0.0160	0.850	3.3675 ± 0.0510	0.8908 ± 0.0195
14		1.9486 ± 0.0160	0.705	6.4547 ± 0.0978	1.0007 ± 0.0123
15		1.9486 ± 0.0160	0.579	9.5286 ± 0.0496	1.0611 ± 0.0101

	aminium:sulfate ratio ^b	a_w	$m\text{SO}_4^{2-}$ (mol kg ⁻¹) ^c	ϕ_{st}	
22					
23					
24					
25					
26					
27	EAS	0.4825 ± 0.0200	0.993	0.0524 ± 0.0020	(2.3623 ± 1.0694)
28		0.4825 ± 0.0200	0.983	0.4729 ± 0.0183	0.6576 ± 0.1201
29		0.4825 ± 0.0200	0.967	0.9528 ± 0.0368	0.6517 ± 0.0610
30		0.4870 ± 0.0230	0.919	2.2161 ± 0.1004	0.7052 ± 0.0282
31		0.4914 ± 0.0230	0.794	4.7903 ± 0.2161	0.8894 ± 0.0160
32		0.4825 ± 0.0200	0.794	4.7872 ± 0.1851	0.8932 ± 0.0157
33		0.4914 ± 0.0230	0.586	9.1326 ± 0.4120	1.0839 ± 0.0121
34		0.4825 ± 0.0200	0.488	9.1332 ± 0.3532	(1.4535 ± 0.0142)
35		0.4870 ± 0.0230	0.321	17.749 ± 0.8044	1.1863 ± 0.0115
36		0.4870 ± 0.0230	0.124	33.931 ± 1.2267	1.1393 ± 0.0144
37		0.9454 ± 0.0360	0.998	0.0303 ± 0.0012	(1.4288 ± 1.8405)
38		0.9454 ± 0.0360	0.988	0.3158 ± 0.0123	0.6875 ± 0.1785
39		0.9454 ± 0.0360	0.978	0.6555 ± 0.0255	0.6375 ± 0.0872
40		0.9454 ± 0.0360	0.949	1.4590 ± 0.0569	0.6638 ± 0.0407
41		0.9454 ± 0.0360	0.886	2.9979 ± 0.1168	0.7447 ± 0.0216
42		0.9454 ± 0.0360	0.798	5.2503 ± 0.2046	0.7952 ± 0.0140
43		0.9454 ± 0.0360	0.671	8.7775 ± 0.3420	0.8411 ± 0.0102
44		0.9454 ± 0.0360	0.478	16.607 ± 0.4429	0.8224 ± 0.0074
45		1.0099 ± 0.0500	0.951	1.4569 ± 0.0760	0.6381 ± 0.0411
46		1.0099 ± 0.0500	0.893	3.0307 ± 0.1582	0.6886 ± 0.0216
47		1.0099 ± 0.0500	0.813	5.3265 ± 0.2780	0.7192 ± 0.0139
48		1.0099 ± 0.0500	0.697	8.9513 ± 0.4672	0.7471 ± 0.0101
49					
50					
51					
52					
53					
54					
55					
56					
57					
58					
59					
60					

1
2
3
4
5
6
7
8
9
10
11
12
13
14
15
16
17
18
19
20
21
22
23
24
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

1.0099 ± 0.0500	0.524	17.406 ± 0.6802	0.6870 ± 0.0068
1.1905 ± 0.0200	0.971	0.7913 ± 0.0218	0.6881 ± 0.0725
1.1905 ± 0.0200	0.939	1.8068 ± 0.0498	0.6446 ± 0.0330
1.1905 ± 0.0200	0.856	4.0262 ± 0.1111	0.7128 ± 0.0164
1.1905 ± 0.0200	0.736	7.7104 ± 0.2127	0.7356 ± 0.0100
1.1905 ± 0.0200	0.568	15.745 ± 0.2299	0.6654 ± 0.0063
1.2978 ± 0.0370	0.956	1.2983 ± 0.0548	0.6413 ± 0.0453
1.2978 ± 0.0370	0.903	2.6853 ± 0.1133	0.7056 ± 0.0235
1.2978 ± 0.0370	0.831	4.6696 ± 0.1970	0.7351 ± 0.0150
1.2978 ± 0.0370	0.732	7.7931 ± 0.3287	0.7418 ± 0.0104
1.2978 ± 0.0370	0.601	13.389 ± 0.2982	0.7029 ± 0.0072
1.4046 ± 0.0390	0.995	0.0304 ± 0.0011	(2.8436 ± 1.8344)
1.4046 ± 0.0390	0.987	0.2846 ± 0.0105	0.8287 ± 0.1981
1.4046 ± 0.0390	0.979	0.5875 ± 0.0216	0.6792 ± 0.0970
1.4046 ± 0.0390	0.954	1.2774 ± 0.0469	0.6770 ± 0.0460
1.4046 ± 0.0390	0.901	2.6358 ± 0.0968	0.7292 ± 0.0239
1.4046 ± 0.0390	0.824	4.6022 ± 0.1690	0.7799 ± 0.0152
1.4046 ± 0.0390	0.722	7.6359 ± 0.2805	0.7904 ± 0.0106
1.4046 ± 0.0390	0.581	13.253 ± 0.3098	0.7573 ± 0.0075
1.8372 ± 0.0610	0.997	0.0284 ± 0.0013	(1.7369 ± 1.9591)
1.8372 ± 0.0610	0.990	0.2425 ± 0.0112	0.7667 ± 0.2323
1.8379 ± 0.0760	0.985	0.3304 ± 0.0183	(0.8465 ± 0.1724)
1.8372 ± 0.0610	0.980	0.5109 ± 0.0235	0.7439 ± 0.1120
1.8372 ± 0.0610	0.951	1.1781 ± 0.0542	0.7891 ± 0.0507
1.8379 ± 0.0760	0.931	1.5822 ± 0.0875	0.8403 ± 0.0395
1.8372 ± 0.0610	0.894	2.3370 ± 0.1076	0.8872 ± 0.0279
1.8379 ± 0.0760	0.837	3.5098 ± 0.1940	0.9359 ± 0.0209
1.8372 ± 0.0610	0.805	4.0464 ± 0.1863	0.9919 ± 0.0185
1.8376 ± 0.0760	0.680	6.8598 ± 0.3818	1.0391 ± 0.0140
1.8376 ± 0.0760	0.551	10.962 ± 0.4204	1.0057 ± 0.0104

	aminium:sulfate ratio ^b	a_w	$m\text{SO}_4^{2-}$ (mol kg ⁻¹) ^c	ϕ_{st}
DMAS	0.4729 ± 0.0180	0.991	0.0489 ± 0.0016	(3.5509 ± 1.1500)
	0.4729 ± 0.0180	0.981	0.4851 ± 0.0154	(0.7447 ± 0.1174)
	0.4692 ± 0.0180	0.968	0.8855 ± 0.0281	0.6761 ± 0.0655
	0.4729 ± 0.0180	0.920	2.1384 ± 0.0679	0.7183 ± 0.0289
	0.4692 ± 0.0180	0.805	4.6242 ± 0.1466	0.8671 ± 0.0157

1					
2					
3	0.4692 ± 0.0180	0.611	8.6305 ± 0.2743	1.0562 ± 0.0115	
4	0.4692 ± 0.0180	0.363	15.875 ± 0.5061	1.1812 ± 0.0107	
5					
6	0.4692 ± 0.0180	0.198	25.817 ± 0.5320	1.1599 ± 0.0118	
7					
8	0.9341 ± 0.0250	0.992	0.0427 ± 0.0013	(3.4774 ± 1.3112)	
9	0.9341 ± 0.0250	0.984	0.3699 ± 0.0112	0.8067 ± 0.1529	
10					
11	0.9541 ± 0.0250	0.972	0.7873 ± 0.0238	0.6674 ± 0.0730	
12	0.9341 ± 0.0250	0.940	1.7776 ± 0.0537	0.6477 ± 0.0336	
13					
14	0.9541 ± 0.0250	0.863	3.8492 ± 0.1158	0.7065 ± 0.0172	
15	0.9541 ± 0.0250	0.747	7.0988 ± 0.2132	0.7604 ± 0.0110	
16					
17	0.9541 ± 0.0250	0.572	13.475 ± 0.2024	0.7671 ± 0.0075	
18	1.4150 ± 0.0470	0.996	0.0357 ± 0.0013	(2.2529 ± 1.5649)	
19	1.4150 ± 0.0470	0.992	0.1580 ± 0.0057	(0.9408 ± 0.3550)	
20					
21	1.4150 ± 0.0470	0.985	0.3256 ± 0.0118	(0.8588 ± 0.1738)	
22	1.4150 ± 0.0470	0.976	0.6847 ± 0.0249	0.6565 ± 0.0836	
23					
24	1.4176 ± 0.0450	0.974	0.6857 ± 0.0241	(0.7016 ± 0.0836)	
25	1.4150 ± 0.0470	0.946	1.5354 ± 0.0558	0.6732 ± 0.0388	
26					
27	1.4163 ± 0.0470	0.872	3.2931 ± 0.1198	0.7707 ± 0.0200	
28	1.4163 ± 0.0470	0.752	6.1320 ± 0.2226	0.8621 ± 0.0128	
29	1.4163 ± 0.0470	0.634	9.1957 ± 0.1801	0.9155 ± 0.0101	
30					
31	1.9247 ± 0.0550	0.989	0.1369 ± 0.0046	(1.4946 ± 0.4113)	
32	1.9247 ± 0.0550	0.987	0.2744 ± 0.0092	(0.9052 ± 0.2059)	
33					
34	1.9247 ± 0.0550	0.971	0.5796 ± 0.0195	(0.9394 ± 0.0995)	
35	1.9247 ± 0.0550	0.940	1.2923 ± 0.0434	0.8859 ± 0.0465	
36					
37	1.9247 ± 0.0550	0.846	2.7676 ± 0.0930	1.1154 ± 0.0247	
38	1.9247 ± 0.0550	0.690	5.0326 ± 0.1690	1.3625 ± 0.0172	
39	1.9247 ± 0.0550	0.610	6.3280 ± 0.0998	1.4437 ± 0.0150	
40					
41	1.9579 ± 0.0310	0.976	0.5762 ± 0.0133	0.7910 ± 0.0990	
42	1.9579 ± 0.0310	0.941	1.2891 ± 0.0298	0.8728 ± 0.0461	
43					
44	1.9579 ± 0.0310	0.848	2.7407 ± 0.0634	1.1105 ± 0.0243	
45	1.9579 ± 0.0310	0.687	5.0320 ± 0.1163	1.3822 ± 0.0166	
46					
47	1.9579 ± 0.0310	0.601	6.3431 ± 0.0566	1.4852 ± 0.0148	
48	2.0515 ± 0.0760	0.973	0.5809 ± 0.0245	(0.8718 ± 0.0997)	
49	2.0515 ± 0.0760	0.857	2.8200 ± 0.1188	(1.0125 ± 0.0247)	
50					
51	2.0515 ± 0.0760	0.723	5.2094 ± 0.2195	(1.1520 ± 0.0167)	
52	2.0515 ± 0.0760	0.652	6.5885 ± 0.1485	(1.2012 ± 0.0140)	
53					
54					
55					
56					
57					
58					
59					
60					

	aminium:sulfate ratio ^b	a_w	$m\text{SO}_4^{2-}$ (mol kg ⁻¹) ^c	ϕ_{st}	
1					
2					
3					
4					
5	DEAS	0.5205 ± 0.0280	0.996	0.0389 ± 0.0021	(1.9064 ± 1.4367)
6		0.5205 ± 0.0280	0.989	0.3463 ± 0.0190	0.6091 ± 0.1634
7		0.5205 ± 0.0280	0.973	0.7256 ± 0.0399	(0.6979 ± 0.0801)
8		0.5258 ± 0.0280	0.944	1.6153 ± 0.0887	0.6662 ± 0.0378
9		0.5258 ± 0.0280	0.873	3.3483 ± 0.1841	0.7495 ± 0.0205
10		0.5258 ± 0.0280	0.757	5.9851 ± 0.3290	0.8627 ± 0.0141
11		0.5258 ± 0.0280	0.581	10.356 ± 0.5682	0.9717 ± 0.0113
12		0.5258 ± 0.0280	0.511	12.501 ± 0.6861	0.9951 ± 0.0108
13		0.5258 ± 0.0280	0.284	22.366 ± 0.9986	1.0429 ± 0.0104
14		0.9942 ± 0.0370	0.989	0.2780 ± 0.0135	(0.7361 ± 0.2028)
15		0.9942 ± 0.0370	0.983	0.0255 ± 0.0012	(3.6394 ± 2.1935)
16		0.9942 ± 0.0370	0.982	0.5379 ± 0.0262	0.6365 ± 0.1059
17		1.0268 ± 0.0250	0.962	1.2102 ± 0.0444	0.5976 ± 0.0481
18		0.9942 ± 0.0370	0.956	1.2030 ± 0.0585	(0.6867 ± 0.0491)
19		1.0105 ± 0.0370	0.916	2.4981 ± 0.1212	0.6499 ± 0.0251
20		1.0105 ± 0.0370	0.852	4.3347 ± 0.2100	0.6862 ± 0.0160
21		1.0105 ± 0.0370	0.762	7.2647 ± 0.3503	0.6923 ± 0.0110
22		1.0105 ± 0.0370	0.642	12.284 ± 0.4004	0.6672 ± 0.0076
23		1.4600 ± 0.0840	0.999	0.0201 ± 0.0014	(0.9210 ± 2.7669)
24		1.4600 ± 0.0840	0.993	0.2048 ± 0.0143	0.6042 ± 0.2745
25		1.4600 ± 0.0840	0.983	0.4276 ± 0.0299	0.7566 ± 0.1342
26		1.4600 ± 0.0840	0.965	0.9412 ± 0.0658	0.7072 ± 0.0631
27		1.4600 ± 0.0840	0.919	1.9251 ± 0.1346	0.8153 ± 0.0337
28		1.4600 ± 0.0840	0.850	3.2805 ± 0.2294	0.9144 ± 0.0225
29		1.4600 ± 0.0840	0.746	5.3432 ± 0.3736	1.0147 ± 0.0168
30		1.4600 ± 0.0840	0.640	7.9577 ± 0.3893	1.0377 ± 0.0128
31		1.5406 ± 0.0210	0.963	0.9499 ± 0.0245	0.7411 ± 0.0609
32		1.5406 ± 0.0210	0.920	1.9401 ± 0.0499	0.7952 ± 0.0314
33		1.5406 ± 0.0210	0.851	3.3414 ± 0.0860	0.8934 ± 0.0198
34		1.5406 ± 0.0210	0.750	5.5010 ± 0.1416	0.9691 ± 0.0138
35		1.5406 ± 0.0210	0.647	8.3302 ± 0.1076	0.9683 ± 0.0104
36		2.0979 ± 0.0330	0.968	0.7645 ± 0.0223	(0.7788 ± 0.0755)
37		2.0567 ± 0.0330	0.958	0.7650 ± 0.0225	(1.0377 ± 0.0764)
38		2.0773 ± 0.0330	0.918	1.5571 ± 0.0459	1.0211 ± 0.0397
39		2.0773 ± 0.0330	0.844	2.6643 ± 0.0783	1.1768 ± 0.0257
40		2.0773 ± 0.0330	0.731	4.1566 ± 0.1221	1.3923 ± 0.0197
41		2.0773 ± 0.0330	0.631	6.1016 ± 0.0912	1.3947 ± 0.0151
42					
43					
44					
45					
46					
47					
48					
49					
50					
51					
52					
53					
54					
55					
56					
57					
58					
59					
60					

	aminium:sulfate ratio ^b	a_w	$m\text{SO}_4^{2-}$ (mol kg ⁻¹) ^c	ϕ_{st}	
1					
2					
3					
4					
5	TMAS	0.3977 ± 0.0220	0.994	0.0464 ± 0.0022	(2.4004 ± 1.2089)
6		0.3977 ± 0.0220	0.985	0.4559 ± 0.0217	0.6134 ± 0.1249
7		0.3977 ± 0.0220	0.966	0.9725 ± 0.0462	0.6516 ± 0.0604
8		0.3976 ± 0.0220	0.924	2.1967 ± 0.1047	0.6703 ± 0.0287
9		0.3976 ± 0.0220	0.802	4.8113 ± 0.2289	0.8501 ± 0.0162
10		0.3976 ± 0.0220	0.588	9.1489 ± 0.4357	1.0740 ± 0.0126
11		0.3976 ± 0.0220	0.299	17.866 ± 0.8513	1.2494 ± 0.0132
12		0.3976 ± 0.0220	0.161	27.154 ± 0.9694	1.2426 ± 0.0148
13		0.4646 ± 0.0060	0.971	0.9474 ± 0.0169	0.5681 ± 0.0605
14		0.4646 ± 0.0060	0.813	4.6963 ± 0.0837	0.8157 ± 0.0147
15		0.4646 ± 0.0060	0.615	8.9953 ± 0.1603	1.0000 ± 0.0103
16		0.4646 ± 0.0060	0.337	17.628 ± 0.3142	1.1406 ± 0.0096
17		0.4646 ± 0.0060	0.190	26.937 ± 0.2515	1.1419 ± 0.0110
18		0.8377 ± 0.0400	0.993	0.0371 ± 0.0018	(3.4993 ± 1.5104)
19		0.8377 ± 0.0400	0.986	0.3653 ± 0.0181	(0.7140 ± 0.1552)
20		0.8377 ± 0.0400	0.971	0.7932 ± 0.0394	0.6865 ± 0.0731
21		0.8377 ± 0.0400	0.943	1.7830 ± 0.0885	0.6090 ± 0.0340
22		0.8377 ± 0.0400	0.869	4.7048 ± 0.2335	0.5507 ± 0.0144
23		0.8377 ± 0.0400	0.577	13.008 ± 0.3975	0.7822 ± 0.0080
24		0.8786 ± 0.0140	0.979	0.6725 ± 0.0171	0.5840 ± 0.0845
25		0.8786 ± 0.0140	0.841	4.7657 ± 0.1211	0.6739 ± 0.0141
26		0.8786 ± 0.0140	0.747	7.4545 ± 0.1894	0.7229 ± 0.0102
27		0.8786 ± 0.0140	0.572	13.494 ± 0.1567	0.7660 ± 0.0073
28		1.0405 ± 0.0360	0.994	0.0356 ± 0.0014	(3.1275 ± 1.5711)
29		1.0405 ± 0.0360	0.991	0.1674 ± 0.0064	(0.9991 ± 0.3354)
30		1.0405 ± 0.0360	0.986	0.3351 ± 0.0127	(0.7599 ± 0.1686)
31		1.0405 ± 0.0360	0.970	0.6815 ± 0.0259	(0.8176 ± 0.0846)
32		1.0405 ± 0.0360	0.947	1.5904 ± 0.0603	0.6295 ± 0.0374
33		1.0405 ± 0.0360	0.879	3.4397 ± 0.1305	0.6938 ± 0.0189
34		1.0405 ± 0.0360	0.777	6.4035 ± 0.2429	0.7303 ± 0.0118
35		1.0405 ± 0.0360	0.670	9.0493 ± 0.1758	0.8188 ± 0.0095
36		1.3393 ± 0.0360	0.979	0.6024 ± 0.0199	0.6623 ± 0.0945
37		1.3393 ± 0.0360	0.909	2.3787 ± 0.0785	0.7421 ± 0.0261
38		1.3393 ± 0.0360	0.882	3.0104 ± 0.0994	0.7741 ± 0.0214
39		1.3393 ± 0.0360	0.759	5.5501 ± 0.1832	0.9208 ± 0.0137
40		1.3393 ± 0.0360	0.657	7.8126 ± 0.1292	0.9937 ± 0.0111
41		1.3916 ± 0.0350	0.977	0.6036 ± 0.0198	(0.7237 ± 0.0946)
42					
43					
44					
45					
46					
47					
48					
49					
50					
51					
52					
53					
54					
55					
56					
57					
58					
59					
60					

1
2
3
4
5
6
7
8
9
10
11
12
13
14
15
16
17
18
19
20
21
22
23
24
25
26
27
28
29
30
31
32
33
34
35
36
37
38
39
40
41
42
43
44
45
46
47
48
49
50
51
52
53
54
55
56
57
58
59
60

1.3916 ± 0.0350	0.887	3.0433 ± 0.0997	0.7313 ± 0.0210
1.3916 ± 0.0350	0.774	5.6505 ± 0.1851	0.8375 ± 0.0132
1.3916 ± 0.0350	0.679	8.0241 ± 0.1332	0.8916 ± 0.0104
1.5313 ± 0.0390	0.998	0.0280 ± 0.0009	(1.1021 ± 1.986)
1.5313 ± 0.0390	0.992	0.1370 ± 0.0044	(1.0396 ± 0.4090)
1.5313 ± 0.0390	0.988	0.2803 ± 0.0089	(0.7969 ± 0.2009)
1.5313 ± 0.0390	0.980	0.5569 ± 0.0177	0.6599 ± 0.1021
1.5313 ± 0.0390	0.948	1.2766 ± 0.0406	0.7740 ± 0.0463
1.5313 ± 0.0390	0.875	2.7080 ± 0.0862	0.9098 ± 0.0240
1.5313 ± 0.0390	0.740	4.9449 ± 0.1575	1.1267 ± 0.0158
1.5313 ± 0.0390	0.682	5.8864 ± 0.0800	1.2030 ± 0.0141
1.6736 ± 0.0330	0.977	0.5587 ± 0.0162	0.7819 ± 0.1021
1.6736 ± 0.0330	0.946	1.2893 ± 0.0374	0.8017 ± 0.0459
1.6736 ± 0.0330	0.858	2.7610 ± 0.0801	1.0289 ± 0.0240
1.6736 ± 0.0330	0.697	5.1187 ± 0.1485	1.3066 ± 0.0162
1.6736 ± 0.0330	0.627	6.1684 ± 0.0750	1.4018 ± 0.0146
1.7776 ± 0.0420	0.977	0.5628 ± 0.0192	0.7649 ± 0.1015
1.7776 ± 0.0420	0.852	2.8240 ± 0.0965	1.0494 ± 0.0239
1.7776 ± 0.0420	0.685	5.3263 ± 0.1819	1.3160 ± 0.0162
1.7776 ± 0.0420	0.613	6.4545 ± 0.1040	1.4029 ± 0.0145

^a Numbers given in brackets were omitted from the fits of the extended ZSR model.

^b Molar ratio. ^c The total sulfate molality in the solution.

TABLE 2. Parameters of the Extended ZSR Model (Eq. 3), at Fixed Water Activities (a_w), for Mixtures of Amminium Sulfate Salts and H_2SO_4 .

	a_w	w_a^0	w_{as}^0	A^0
MAS	0.975	1.4725	1.5727 ± 0.2800	-0.769 ± 0.880
	0.95	0.7904	0.8026 ± 0.0480	-0.593 ± 0.180
	0.925	0.5641	0.5647 ± 0.0200	-0.516 ± 0.076
	0.9	0.4496	0.4389 ± 0.0099	-0.430 ± 0.037
	0.85	0.3312	0.3043 ± 0.0057	-0.330 ± 0.021
	0.8	0.2682	0.2335 ± 0.0060	-0.278 ± 0.023
	0.75	0.2276	0.1901 ± 0.0052	-0.250 ± 0.021
	0.7	0.1984	0.1592 ± 0.0056	-0.238 ± 0.022
	0.65	0.1759	0.1357 ± 0.0047	-0.226 ± 0.019
	0.6	0.1578	0.1148 ± 0.0066	-0.208 ± 0.022
EAS	0.975	1.4725	1.6755 ± 0.0200	-0.765 ± 0.063
	0.95	0.7904	0.8775 ± 0.0190	-0.615 ± 0.055
	0.925	0.5641	0.6224 ± 0.0190	-0.526 ± 0.054
	0.9	0.4496	0.4795 ± 0.0160	-0.438 ± 0.044
	0.85	0.3312	0.3283 ± 0.0116	-0.353 ± 0.033
	0.8	0.2682	0.2569 ± 0.0125	-0.331 ± 0.034
	0.75	0.2276	0.2051 ± 0.0099	-0.296 ± 0.028
	0.7	0.1984	0.1678 ± 0.0098	-0.266 ± 0.027
	0.65	0.1759	0.1388 ± 0.0097	-0.249 ± 0.027
	0.6	0.1578	0.1185 ± 0.0089	-0.232 ± 0.025
DMAS	0.95	0.7904	0.9017 ± 0.0330	-0.635 ± 0.120
	0.925	0.5641	0.6586 ± 0.0130	-0.606 ± 0.055
	0.9	0.4496	0.5250 ± 0.0100	-0.543 ± 0.042
	0.85	0.3312	0.3796 ± 0.0083	-0.456 ± 0.032
	0.8	0.2682	0.3014 ± 0.0059	-0.416 ± 0.023
	0.75	0.2276	0.2505 ± 0.0048	-0.372 ± 0.020
	0.7	0.1984	0.2139 ± 0.0054	-0.347 ± 0.021
	0.65	0.1759	0.1861 ± 0.0046	-0.325 ± 0.019
DEAS	0.975	1.4725	1.9987 ± 0.1340	-1.528 ± 0.335
	0.95	0.7904	1.0246 ± 0.0630	-0.948 ± 0.180
	0.925	0.5641	0.7269 ± 0.0510	-0.740 ± 0.140
	0.9	0.4496	0.5644 ± 0.0160	-0.607 ± 0.056
	0.85	0.3312	0.4023 ± 0.0130	-0.493 ± 0.046
	0.8	0.2682	0.3178 ± 0.0130	-0.445 ± 0.046

1					
2					
3		0.75	0.2276	0.2634 ± 0.0120	-0.406 ± 0.043
4		0.7	0.1984	0.2188 ± 0.0130	-0.373 ± 0.043
5					
6	TMAS	0.975	1.4725	1.8522 ± 0.0620	-1.416 ± 0.220
7		0.95	0.7904	1.0241 ± 0.0140	-0.958 ± 0.044
8		0.925	0.5641	0.7553 ± 0.0140	-0.862 ± 0.041
9		0.9	0.4496	0.6082 ± 0.0190	-0.773 ± 0.056
10		0.85	0.3312	0.4432 ± 0.0200	-0.651 ± 0.058
11		0.8	0.2682	0.3582 ± 0.0150	-0.565 ± 0.043
12		0.75	0.2276	0.2988 ± 0.0120	-0.495 ± 0.035
13		0.7	0.1984	0.2592 ± 0.0110	-0.446 ± 0.032
14		0.65	0.1759	0.2234 ± 0.0100	-0.404 ± 0.029
15					
16					
17					
18					
19					
20					
21					
22					
23					
24					
25					
26					
27					
28					
29					
30					
31					
32					
33					
34					
35					
36					
37					
38					
39					
40					
41					
42					
43					
44					
45					
46					
47					
48					
49					
50					
51					
52					
53					
54					
55					
56					
57					
58					
59					
60					

TABLE 3. Fitted Parameters of the Ion Interaction Model (Eq. 4) for the Aminium Sulfate Salts.^a

	$B_{M,X}$	$W_{w,MX}$	$U_{w,MX}$	$V_{w,MX}^c$
MAS	-7.5248 ± 62.6909	-0.9172 ± 0.1226	4.5909 ± 0.3043	-4.0524
EAS	25.3847 ± 99.5183	-1.0045 ± 0.2158	4.5156 ± 0.5236	-2.3439
DMAS	-43.3109 ± 37.9502	-2.8277 ± 0.2547	6.8415 ± 0.4641	-6.2113
DEAS	44.6350 ± 140.0407	-2.5182 ± 1.5148	6.2800 ± 2.5315	-3.1156
TMAS	-94.4591 ± 124.0575	-4.2897 ± 1.4157	8.3745 ± 2.3377	-5.6426

^a Values of other coefficients and constants in the equation are: $A^\phi = 2.917$, $\alpha = 13.0$, and $\rho = 13.0$. ^b Parameter uncertainty at 90% confidence level. ^c This parameter was constrained artificially and not fitted.

Supplementary Information

Water Activities and Osmotic Coefficients of Aqueous Solutions of Five Alkyl-Aminium Sulfates and Their Mixtures with H₂SO₄ at 25 °C

Meike Sauerwein¹, Simon L. Clegg^{2,*}, and Chak K. Chan^{1,3,*}

¹ *Division of Environment, Hong Kong University of Science and Technology, Clear Water Bay, Kowloon, Hong Kong*

² *School of Environmental Sciences, University of East Anglia, Norwich NR4 7TJ, U.K.*

³ *Department of Chemical Engineering, Hong Kong University of Science and Technology, Clear Water Bay, Kowloon, Hong Kong*

*Corresponding author: sclegg@uea.ac.uk; keckchan@ust.hk

The information in this document is supplementary to the following publication: *****

Notes

The aminium salts studied in this work are: MAS – methylaminium sulfate; EAS – ethylaminium sulfate; DMAS - dimethylaminium sulfate; DEAS – diethylaminium sulfate and TMAS - trimethylaminium sulfate.

Throughout this document, the molar aminium:sulfate ratio in the solutions is abbreviated as "A:S". A ratio of 2:1 corresponds to pure aqueous aminium sulfate, and a ratio of 0:1 to pure aqueous H₂SO₄.

Contents

Table1: Solute molalities at fixed values of the water activity, obtained by interpolation of the experimental results.

SI TABLE 1. Total sulfate molalities ($m\text{SO}_4^{2-}$ in mol kg^{-1}) at fixed water activities ($a_{w,\text{fix}}$) obtained by linear interpolation of the experimental results (as osmotic coefficients vs $\sqrt{m\text{SO}_4^{2-}}$). The molar aminium:sulfate ratio ($A:S$) is listed for each mixture (a value of 0.0 corresponds to pure aqueous H_2SO_4 , and a value of 2.0 to the pure aqueous aminium sulfate).

	$A:S$	$a_{w,\text{fix}}$	$m\text{SO}_4^{2-}$	$A:S$	$a_{w,\text{fix}}$	$m\text{SO}_4^{2-}$
MAS	0.4461	0.975	0.8349	0.8731	0.500	16.020
	0.4490	0.950	1.4102	0.8731	0.475	17.904
	0.4490	0.925	2.1092	0.8731	0.450	18.744
	0.4461	0.900	2.6789	1.3618	0.975	0.7267
	0.4461	0.850	3.6670	1.3618	0.950	1.5584
	0.4461	0.800	4.6047	1.3618	0.925	2.2861
	0.4490	0.750	5.5424	1.3618	0.900	2.9483
	0.4490	0.700	6.5292	1.3708	0.850	4.2721
	0.4490	0.650	7.5324	1.3708	0.800	5.6492
	0.4490	0.600	8.5634	1.3708	0.750	7.0794
	0.4490	0.550	9.5685	1.3708	0.700	8.7304
	0.4490	0.525	10.239	1.3708	0.650	10.490
	0.4490	0.500	10.934	1.7819	0.975	0.6872
	0.4490	0.475	11.659	1.7819	0.950	1.3911
	0.4490	0.450	12.415	1.7819	0.925	1.9936
	0.4490	0.425	13.207	1.7819	0.900	2.5319
	0.4490	0.400	14.038	1.7819	0.850	3.5693
	0.8731	0.975	0.6455	1.7819	0.800	4.6243
	0.8851	0.950	1.4141	1.7819	0.750	5.6769
	0.8851	0.925	2.1883	1.7819	0.700	6.8145
	0.8851	0.900	2.8607	1.7819	0.650	8.0839
	0.8851	0.850	4.1841	1.9486	0.950	1.1708
	0.8610	0.800	5.3437	1.9486	0.925	1.7269
	0.8610	0.750	6.6678	1.9486	0.900	2.2772
	0.8851	0.700	8.1729	1.9486	0.850	3.3746
	0.8851	0.650	9.9331	1.9486	0.800	4.4268
	0.8851	0.600	11.853	1.9486	0.750	5.4883
	0.8851	0.550	13.960	1.9486	0.700	6.5774
	0.8851	0.525	15.095	1.9486	0.650	7.7558
				1.9486	0.600	8.9904

	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}
EAS	0.4825	0.975	0.7159	0.9454	0.600	11.329	1.4046	0.925	2.0363
	0.4847	0.950	1.4087	0.9454	0.550	13.335	1.4046	0.900	2.6697
	0.4847	0.925	2.0617	0.9454	0.525	14.415	1.4046	0.850	3.9349
	0.4892	0.900	2.6329	0.9454	0.500	15.553	1.4046	0.800	5.2766
	0.4892	0.850	3.6761	1.0099	0.950	1.4848	1.4046	0.750	6.7583
	0.4892	0.800	4.6780	1.0099	0.925	2.1744	1.4046	0.700	8.4040
	0.4870	0.750	5.6766	1.0099	0.900	2.8515	1.4046	0.650	10.304
	0.4870	0.700	6.7013	1.0099	0.850	4.2592	1.4046	0.600	12.408
	0.4870	0.650	7.7444	1.0099	0.800	5.7141	1.2978	0.950	1.4598
	0.4870	0.600	8.8179	1.0099	0.750	7.2437	1.2978	0.925	2.1155
	0.4892	0.550	10.083	1.0099	0.700	8.8423	1.2978	0.900	2.7580
	0.4892	0.525	10.777	1.0099	0.650	10.899	1.2978	0.850	4.1314
	0.4892	0.500	11.496	1.0099	0.600	13.234	1.2978	0.800	5.6000
	0.4892	0.475	12.245	1.0099	0.550	15.881	1.2978	0.750	7.1871
	0.4892	0.450	13.025	1.0099	0.525	17.345	1.2978	0.700	9.0112
	0.4892	0.425	13.840	1.1905	0.950	1.4416	1.2978	0.650	11.109
	0.4892	0.400	14.696	1.1905	0.925	2.1903	1.8372	0.975	0.6222
	0.9454	0.975	0.7314	1.1905	0.900	2.8649	1.8376	0.950	1.1985
	0.9454	0.950	1.4314	1.1905	0.850	4.2107	1.8376	0.925	1.7005
	0.9454	0.925	2.0633	1.1905	0.800	5.7021	1.8376	0.900	2.2148
	0.9454	0.900	2.6716	1.1905	0.750	7.2602	1.8376	0.850	3.2480
	0.9454	0.850	3.9200	1.1905	0.700	9.1541	1.8374	0.800	4.1539
	0.9454	0.800	5.1988	1.1905	0.650	11.380	1.8374	0.750	5.2513
	0.9454	0.750	6.5438	1.1905	0.600	13.911	1.8374	0.700	6.3944
	0.9454	0.700	7.9398	1.4046	0.975	0.6901	1.8376	0.650	7.7286
	0.9454	0.650	9.4992	1.4046	0.950	1.3912	1.8376	0.600	9.2803

	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}
DMAS	0.4711	0.950	1.3665	1.4150	0.975	0.7128
	0.4711	0.925	2.0178	1.4150	0.950	1.4141
	0.4711	0.900	2.5973	1.4157	0.925	2.0446
	0.4711	0.850	3.6808	1.4157	0.900	2.6397
	0.4692	0.800	4.7297	1.4163	0.850	3.8084
	0.4692	0.750	5.7461	1.4163	0.800	4.9840
	0.4692	0.700	6.7662	1.4163	0.750	6.1692
	0.4692	0.650	7.8028	1.4163	0.700	7.4458

1						
2						
3	0.4692	0.600	8.9026	1.4163	0.650	8.7715
4	0.4692	0.550	10.182	1.9247	0.925	1.5469
5						
6	0.4692	0.525	10.851	1.9247	0.900	1.9511
7						
8	0.4692	0.500	11.543	1.9247	0.850	2.7133
9						
10	0.4692	0.475	12.260	1.9247	0.800	3.4473
11						
12	0.4692	0.450	13.005	1.9247	0.750	4.1695
13						
14	0.4692	0.425	13.783	1.9247	0.700	4.8920
15						
16	0.4692	0.400	14.595	1.9247	0.650	5.6770
17						
18	0.9441	0.975	0.6666	1.9579	0.975	0.5907
19						
20	0.9441	0.950	1.4526	1.9579	0.950	1.1100
21						
22	0.9441	0.925	2.1818	1.9579	0.925	1.5600
23						
24	0.9441	0.900	2.8617	1.9579	0.900	1.9613
25						
26	0.9541	0.850	4.2146	1.9579	0.850	2.7162
27						
28	0.9541	0.800	5.5983	1.9579	0.800	3.4350
29						
30	0.9541	0.750	7.0118	1.9579	0.750	4.1398
31						
32	0.9541	0.700	8.6579	1.9579	0.700	4.8434
33						
34	0.9541	0.650	10.431	1.9579	0.650	5.5852
35						
36	0.9541	0.600	12.338			
37						

	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	
38	DEAS	0.5231	0.975	0.7413	1.0105	0.650	11.917
39		0.5231	0.950	1.4376	1.4600	0.975	0.6383
40		0.5258	0.925	2.0847	1.4600	0.950	1.2693
41		0.5258	0.900	2.7011	1.4600	0.925	1.7963
42		0.5258	0.850	3.8793	1.4600	0.900	2.3047
43		0.5258	0.800	5.0082	1.4600	0.850	3.2872
44		0.5258	0.750	6.1388	1.4600	0.800	4.2750
45		0.5258	0.700	7.3353	1.4600	0.750	5.2638
46		0.5258	0.650	8.5657	1.4600	0.700	6.4392
47		0.5258	0.600	9.8427	1.4600	0.650	7.6968
48		0.5258	0.550	11.266	1.5406	0.950	1.2494
49		0.5258	0.525	12.040	1.5406	0.925	1.8263
50		0.5258	0.500	12.862	1.5406	0.900	2.3564
51		0.5258	0.475	13.747	1.5406	0.850	3.3627
52		0.5258	0.450	14.673	1.5406	0.800	4.4223
53		0.5258	0.425	15.646	1.5406	0.750	5.4939
54		0.5258	0.400	16.670	1.5406	0.700	6.8127

1						
2						
3	1.0105	0.975	0.7528	1.5406	0.650	8.2315
4	1.0187	0.950	1.5476	2.0773	0.900	1.8323
5						
6	1.0187	0.925	2.2500	2.0773	0.850	2.5787
7						
8	1.0105	0.900	2.9542	2.0773	0.800	3.2560
9	1.0105	0.850	4.3815	2.0773	0.750	3.9134
10	1.0105	0.800	5.9853	2.0773	0.700	4.7374
11	1.0105	0.750	7.7174	2.0773	0.650	5.7168
12						
13	1.0105	0.700	9.7163			

	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	<i>A:S</i>	$a_{w,fix}$	mSO_4^{2-}	
14										
15										
16										
17										
18										
19	TMAS	0.3977	0.975	0.73668	0.4646	0.400	15.3133	1.3393	0.750	5.73954
20		0.3976	0.950	1.43877	0.8377	0.950	1.51281	1.3393	0.700	6.84566
21		0.3976	0.925	2.15380	0.8377	0.925	2.43117	1.3916	0.850	3.90447
22		0.3976	0.900	2.73233	0.8377	0.900	3.39960	1.3916	0.800	5.05948
23		0.3976	0.850	3.81077	0.8377	0.850	5.26663	1.3916	0.750	6.24735
24		0.3976	0.800	4.84504	0.8377	0.800	6.68383	1.3916	0.700	7.49645
25		0.3976	0.750	5.84594	0.8377	0.750	8.07663	1.5313	0.975	0.68480
26		0.3976	0.700	6.84575	0.8377	0.700	9.46925	1.5313	0.950	1.23500
27		0.3976	0.650	7.85804	0.8377	0.650	10.8803	1.5313	0.925	1.74907
28		0.3976	0.600	8.89485	0.8377	0.600	12.3265	1.5313	0.900	2.23941
29		0.3976	0.550	10.0912	0.8786	0.975	0.79568	1.5313	0.850	3.14107
30		0.3976	0.525	10.7341	0.8786	0.950	1.55066	1.5313	0.800	3.97015
31		0.3976	0.500	11.3976	0.8786	0.925	2.29066	1.5313	0.750	4.78288
32		0.3976	0.475	12.0840	0.8786	0.900	3.02425	1.5313	0.700	5.59313
33		0.3976	0.450	12.7963	0.8786	0.850	4.49032	1.6736	0.975	0.59811
34		0.3976	0.425	13.5375	0.8786	0.800	5.92840	1.6736	0.950	1.18729
35		0.3976	0.400	14.3114	0.8786	0.750	7.37643	1.6736	0.925	1.66180
36		0.4646	0.950	1.52498	0.8786	0.700	8.97821	1.6736	0.900	2.08516
37		0.4646	0.925	2.15155	0.8786	0.650	10.6651	1.6736	0.850	2.87769
38		0.4646	0.900	2.74603	0.8786	0.600	12.4471	1.6736	0.800	3.62060
39		0.4646	0.850	3.88097	1.0405	0.925	2.20637	1.6736	0.750	4.34688
40		0.4646	0.800	4.97580	1.0405	0.900	2.88065	1.6736	0.700	5.07019
41		0.4646	0.750	6.04646	1.0405	0.850	4.26437	1.6736	0.650	5.81498
42		0.4646	0.700	7.12107	1.0405	0.800	5.71286	1.7776	0.975	0.60565
43		0.4646	0.650	8.21328	1.0405	0.750	7.06151	1.7776	0.950	1.10711
44		0.4646	0.600	9.38166	1.0405	0.700	8.29918	1.7776	0.925	1.57019
45		0.4646	0.550	10.7169	1.3393	0.975	0.70060	1.7776	0.900	2.01142

1									
2									
3	0.4646	0.525	11.4148	1.3393	0.950	1.35096	1.7776	0.850	2.85491
4	0.4646	0.500	12.1360	1.3393	0.925	1.98129	1.7776	0.800	3.61241
5									
6	0.4646	0.475	12.8831	1.3393	0.900	2.58843	1.7776	0.750	4.35546
7									
8	0.4646	0.450	13.6592	1.3393	0.850	3.67904	1.7776	0.700	5.09736
9	0.4646	0.425	14.4679	1.3393	0.800	4.70860	1.7776	0.650	5.86661
10									
11									
12									
13									
14									
15									
16									
17									
18									
19									
20									
21									
22									
23									
24									
25									
26									
27									
28									
29									
30									
31									
32									
33									
34									
35									
36									
37									
38									
39									
40									
41									
42									
43									
44									
45									
46									
47									
48									
49									
50									
51									
52									
53									
54									
55									
56									
57									
58									
59									
60									