## Boron-modified Chlorine-free $K^+$ -FeO<sub>x</sub>/SBA-15 as Highly Effective Catalyst for Propylene Epoxidation by Nitrous Oxide

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Modification of chlorine-free alkali metal ion (K<sup>+</sup>, Rb<sup>+</sup>, or Cs<sup>+</sup>)-containing FeO<sub>x</sub>/SBA-15 catalysts with boron enhanced their catalytic performances in propylene epoxidation by nitrous oxide. A B–K<sup>+</sup>–FeO<sub>x</sub>/SBA-15 catalyst (K/Fe = 2.5, B/Fe = 0.5) showed the best propylene oxide (PO) formation activity, providing PO selectivities of 79 and 55% at propylene conversions of 4.8 and 13% at 350 and 400 °C, respectively.

The epoxidation of propylene using a "green" oxidant has attracted much attention in recent years.<sup>1</sup> Although oxygen or air is the most ideal oxidant, the epoxidation of  $C_3H_6$  by  $O_2$  is still not successful, and PO selectivity can hardly exceed 60% even at a low  $C_3H_6$  conversion.<sup>2</sup> A few efficient catalysts have been reported for the epoxidation of  $C_3H_6$  by  $H_2O_2$  in liquid phase,<sup>3</sup> but the high cost of  $H_2O_2$  and the difficulty in its handling are problems. Many studies have contributed to the in situ production of  $H_2O_2$  from  $O_2$ – $H_2$  gas mixture for  $C_3H_6$  epoxidation.<sup>4</sup> Among the catalysts reported, the Au–Ti-based vapor-phase catalysts developed by Haruta and co-workers have attracted much attention.<sup>4b–4d</sup>

Recently, we studied an iron-based  $C_3H_6$  epoxidation catalytic system with N<sub>2</sub>O as the oxidant.<sup>5</sup> We reported that a KCl-modified 1 wt % FeO<sub>x</sub>/SBA-15 (K/Fe = 5) catalyst could provide PO selectivities of 72 and 50% at C<sub>3</sub>H<sub>6</sub> conversions of 4.5 and 10%, respectively.<sup>5a,5b</sup> However, the use of other potassium salt such as KAc as the modifier led to remarkably lower PO formation activities.<sup>5b</sup> Because chlorine may go to the gas phase to act as a radical promoter and may be lost during the reaction, it is useful to develop a highly efficient chlorinefree catalyst. Herein, we report our recent finding that the presence of boron can significantly enhance the catalytic properties of the no-chlorine K<sup>+</sup> (Rb<sup>+</sup> or Cs<sup>+</sup>)–FeO<sub>x</sub>/SBA-15 catalysts.

SBA-15 and FeO<sub>x</sub>/SBA-15 were prepared using the procedure reported previously.<sup>5b</sup> The modified FeO<sub>x</sub>/SBA-15 catalysts were prepared by impregnation of the FeO<sub>x</sub>/SBA-15 powder with an aqueous solution of alkali metal acetate or a mixed aqueous solution containing alkali metal acetate and H<sub>3</sub>BO<sub>3</sub> in a fixed ratio, followed by drying and calcination at 823 K for 6 h. The contents of iron and potassium in the catalysts were determined by ICP. The catalysts were characterized by XRD and N<sub>2</sub> sorption. Catalytic reactions were carried out using a fixedbed flow reactor (quartz tube) operated at atmospheric pressure. The products were analyzed by two on-line gas chromatographs.

Table 1 shows the catalytic performances of the 1 wt %  $FeO_x/SBA-15$  catalysts modified by various alkali metal ions with and without boron for the epoxidation of  $C_3H_6$  by  $N_2O$ . It should be noted that no reaction occurred without iron irrespective of the presence or absence of boron or alkali metal ions on SBA-15. In the absence of an alkali metal ion, no formation of

Table	1.	Effect	of	boron	on	catalytic	results	of	alkali	metal
ion-mo	odif	fied Fe	$D_x/$	SBA-1	5 fo	r C <sub>3</sub> H <sub>6</sub> e	poxidati	on	by $N_2$	Зa

	$C_3H_6$	Selectivity/%			
Catalyst <sup>b</sup>	conv. /%	РО	Others <sup>c</sup>	CO <sub>x</sub>	
FeO <sub>x</sub> /SBA-15	1.3	0	50	50	
$B-FeO_x/SBA-15$	2.3	0	59	41	
Li <sup>+</sup> –FeO <sub>x</sub> /SBA-15	4.1	16	62	22	
B–Li <sup>+</sup> –FeO <sub>x</sub> /SBA-15	3.5	16	60	24	
Na <sup>+</sup> –FeO <sub>x</sub> /SBA-15	4.2	69	18	13	
B–Na <sup>+</sup> –FeO <sub>x</sub> /SBA-15	4.4	66	21	13	
$K^+$ –FeO <sub>x</sub> /SBA-15	3.8	64	14	22	
$B-K^+-FeO_x/SBA-15$	4.8	79	12	9.4	
$B-K^+-FeO_x/SBA-15^d$	1.6	80	11	8.9	
$B-K^+-FeO_x/SBA-15^e$	4.9	77	12	11	
$B-K^+-FeO_x/SBA-15^f$	8.9	68	14	18	
$B-K^+-FeO_x/SBA-15^g$	13	55	15	30	
$Rb^+$ – $FeO_x/SBA-15$	2.9	54	13	33	
$B-Rb^+-FeO_x/SBA-15$	4.2	74	13	13	
$Cs^+$ –FeO <sub>x</sub> /SBA-15	2.8	45	18	37	
$B-Cs^+-FeO_x/SBA-15$	4.4	76	14	10	

<sup>a</sup>Reaction conditions: W(catalyst) = 0.2 g,  $T = 350 \,^{\circ}\text{C}$ ,  $P(\text{C}_3\text{H}_6) = 2.5 \text{ kPa}$ ,  $P(\text{N}_2\text{O}) = 25.3 \text{ kPa}$ ,  $F(\text{total}) = 60 \text{ mL min}^{-1}$ , TOS = 30 min. <sup>b</sup>Fe content = 1 wt %; alkali metal ion/Fe (molar ratio) = 2.5, B/alkali metal ion (molar ratio) = 0.5. <sup>c</sup>Others include acrolein, allyl alcohol, acetone, and acetaldehyde. <sup>d</sup>TOS = 230 min. <sup>e</sup>Regenerating the catalyst after 230 min of reaction, followed by reaction for 30 min. <sup>f</sup>T = 375 °C. <sup>e</sup>T = 400 °C.

PO was observed over the  $FeO_x/SBA-15$  or the B-FeO<sub>x</sub>/SBA-15. The modification with a no-halogen alkali metal ion could also induce the PO formation and enhance C<sub>3</sub>H<sub>6</sub> conversion. Among the alkali metal ions, Na<sup>+</sup> and K<sup>+</sup> showed similar enhancing effects and were better than Li<sup>+</sup>, Rb<sup>+</sup>, and Cs<sup>+</sup> as modifiers. As compared with the KCl-FeO<sub>x</sub>/SBA-15 catalyst reported previously,<sup>5a</sup> the present chlorine-free  $K^+$ -FeO<sub>x</sub>/ SBA-15 catalyst exhibited a lower C3H6 conversion and a lower PO selectivity. However, the presence of boron remarkably increased the PO selectivities as well as C<sub>3</sub>H<sub>6</sub> conversions for the K<sup>+</sup>-, Rb<sup>+</sup>-, and Cs<sup>+</sup>-modified FeO<sub>x</sub>/SBA-15 catalysts although the catalytic performances of the  $Li^+$  and  $Na^+$ -FeO<sub>x</sub>/ SBA-15 catalysts were not obviously altered by boron. PO selectivities over the B- and K<sup>+</sup> (Rb<sup>+</sup> or Cs<sup>+</sup>)-doubly modified catalysts were higher than 70%. Similar to other catalysts,<sup>5,6</sup> the activity of the present catalyst also decreased with time on stream (TOS), but the activity can be recovered by regenerating the catalyst with a gas flow containing O<sub>2</sub> at 823 K (Table 1).

We have carried out further studies on the effect of boron on catalytic performances of the  $K^+$ -FeO<sub>x</sub>/SBA-15 catalysts with



**Figure 1.** Effect of boron on catalytic behavior of  $K^+-1$  wt % FeO<sub>x</sub>/SBA-15 catalysts with different K/Fe ratio (B/K = 0.5). ( $\bigcirc$ ) and ( $\bigcirc$ ), C<sub>3</sub>H<sub>6</sub> conversion; ( $\square$ ) and ( $\blacksquare$ ), PO selectivity. Solid and dashed lines are for the catalysts with and without boron modification, respectively. Reaction conditions are the same as those in Table 1.

different K/Fe ratio. Figure 1 shows that, in the absence of boron modification, both C<sub>3</sub>H<sub>6</sub> conversion and PO selectivity reach maximum values at a K/Fe ratio of 2.5, and further increases in the K/Fe ratio decrease the PO selectivity steeply. The conversion of  $C_3H_6$  also dropped at the same time. The addition of boron into the  $K^+$ -FeO<sub>x</sub>/SBA-15 catalysts with K/Fe ratios of 0.5 and 1.0 did not obviously change the catalytic performances. However, for the  $K^+$ -FeO<sub>x</sub>/SBA-15 catalysts with K/Fe ratios of >2.5, the presence of boron increased the catalytic performances significantly. Further studies with the B-K<sup>+</sup>- $1 \text{ wt \% FeO}_{x}/\text{SBA-15}$  (K/Fe = 2.5) by varying boron content confirmed that the catalyst with a B/K ratio of 0.5 exhibited the best performance for PO formation. PO selectivity was 79% at a C<sub>3</sub>H<sub>6</sub> conversion of 4.8% over this catalyst at 350 °C. By increasing the temperature to 375 and 400 °C,  $C_3H_6$ conversions rose to 8.9 and 13%, and PO selectivities could be maintained at 68 and 55%, respectively. These values are even better than those reported for the KCl-FeO<sub>x</sub>/SBA-15 catalyst and other iron-based catalysts.5a,6

To clarify why the presence of boron can exert such a positive role in raising the catalytic performances of the K<sup>+</sup> (Rb<sup>+</sup> or  $Cs^+$ )-FeO<sub>x</sub>/SBA-15 catalyst, we have investigated the influence of boron on catalyst structures. N2-sorption measurements showed that the addition of Li<sup>+</sup>, Na<sup>+</sup>, K<sup>+</sup>, Rb<sup>+</sup>, and Cs<sup>+</sup> to the 1 wt % FeO<sub>r</sub>/SBA-15 sample decreased BET surface areas from 684 to 444, 403, 269, 290, and 279 m<sup>2</sup> g<sup>-1</sup>, respectively. This change indicates that the alkali metal ions, especially those with strong basicity such as K<sup>+</sup>, Rb<sup>+</sup>, and Cs<sup>+</sup>, may partially destroy the mesoporous structure of SBA-15 via the reaction with the silica wall. The modification of boron raised the BET surface areas of the K<sup>+</sup>-, Rb<sup>+</sup>-, and Cs<sup>+</sup>-modified samples to 332, 372, and  $363 \text{ m}^2 \text{ g}^{-1}$ , respectively, but did not increase those of the Li<sup>+</sup>- and Na<sup>+</sup>-modified samples. Thus, boron may restore the ordered mesoporous structure to some extent through the interaction with K<sup>+</sup>, Rb<sup>+</sup>, or Cs<sup>+</sup>. Such effect of boron was also observed for the K<sup>+</sup>-FeO<sub>x</sub>/SBA-15 catalysts with different K/Fe ratios. As shown in Figure 2, the change in XRD patterns after the addition of boron to the sample with a K/Fe ratio of 5 clearly suggests that the partially destroyed ordered mesoporous structure is restored by boron modification.

However, the modification with other acidic groups such as phosphate and sulfate did not increase the catalytic performances of the K<sup>+</sup>–FeO<sub>x</sub>/SBA-15 catalyst significantly although they could also restore the ordered mesoporous structure. We specu-



**Figure 2.** XRD patterns of the  $K^+$ -1 wt % FeO<sub>x</sub>/SBA-15 samples with (B/K = 0.5) and without boron.

late that boron may have other functions such as improving the electrophilicity of the oxygen species derived from  $N_2O$ because of the electron-deficient nature of boron. Boron may also regulate the acid–base property of the catalyst, which may affect the consecutive conversion of PO. Our XPS studies suggest that boron is in +III state. As for the location of boron, we speculate that boron may be located inside the mesoporous channels and has strong interactions with both alkali metal ions and iron species.

In conclusion, we have found an interesting enhancing effect of boron on the catalytic performance of the FeO<sub>x</sub>/SBA-15 catalysts modified by K<sup>+</sup>, Rb<sup>+</sup>, or Cs<sup>+</sup> for PO formation. The chlorine-free  $B-K^+$ -FeO<sub>x</sub>/SBA-15 catalyst can provide better PO formation activity than the KCl–FeO<sub>x</sub>/SBA-15 catalyst.

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