

# Effect of boron promotion on coke formation during propane dehydrogenation over Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts

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## Introduction:

Coke formation continues to be an important challenge for Pt-based catalysts during propane dehydrogenation (PDH)<sup>1</sup>. Boron promotion drastically reduces coke formation on nickel<sup>2</sup> during steam reforming and on cobalt<sup>3</sup> during Fischer-Tropsch synthesis. DFT calculations and catalyst characterization indicate that reduced boron atoms selectively block step and/or subsurface sites, thus preventing nucleation and growth of deactivating carbon<sup>2,3</sup>.

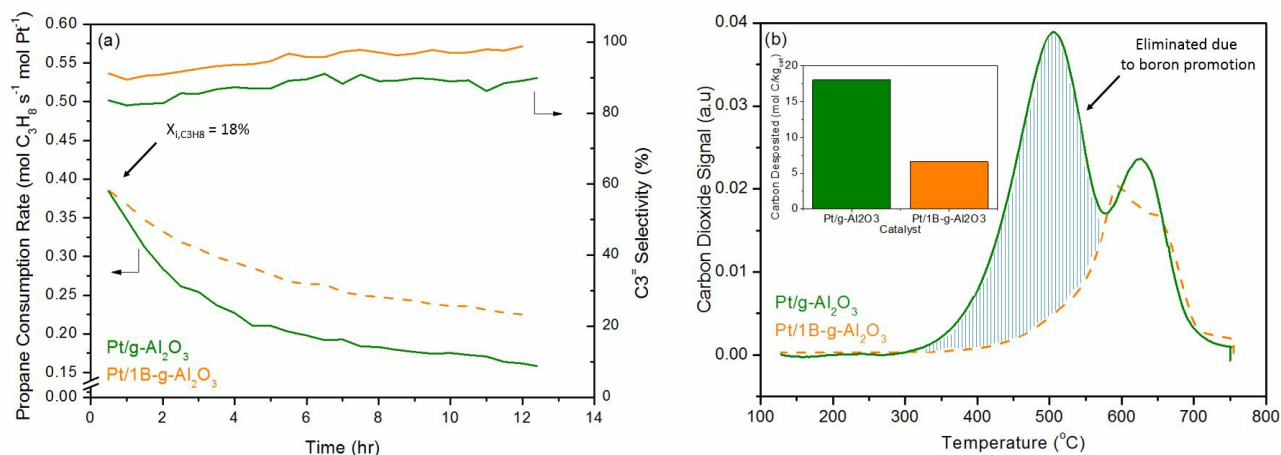
In this work, boron is introduced to enhance the catalytic performance of Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts during PDH. A series of catalysts with different boron loadings was prepared following various impregnation sequences. Detailed characterization and DFT calculations help identify boron's location and state (alloy/amorphous oxide).

## Results:

XB- $\gamma$ -Al<sub>2</sub>O<sub>3</sub> support materials (X=wt.%B) were prepared via wet impregnation of H<sub>3</sub>BO<sub>3</sub> onto commercial  $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. Three different synthesis routes were followed: (a) Pt/XB- $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalysts were prepared via wet impregnation of H<sub>2</sub>PtCl<sub>6</sub> onto XB- $\gamma$ -Al<sub>2</sub>O<sub>3</sub>. (b) 1B/Pt- $\gamma$ -Al<sub>2</sub>O<sub>3</sub> was prepared via wet impregnation of H<sub>3</sub>BO<sub>3</sub> onto Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> i.e., an inverse sequential impregnation. (c) Pt-1B- $\gamma$ -Al<sub>2</sub>O<sub>3</sub> was prepared by co-impregnation. Pt/ $\gamma$ -Al<sub>2</sub>O<sub>3</sub> was prepared as a reference. The platinum loading was fixed at 3wt.% to facilitate characterization and obtain B/Pt (mol) ratios from 1-10.

Effects of boron loading and impregnation sequence were investigated during short-term (20 min) PDH tests at 600°C and a C<sub>3</sub>H<sub>8</sub>/H<sub>2</sub> ratio of one. Unlike with nickel and cobalt,<sup>2,3</sup> the promoting effect of boron was only observed when boron was introduced *before* the active metal. The Pt/1B- $\gamma$ -Al<sub>2</sub>O<sub>3</sub> catalyst showed only a minor reduction in activity during the short-term experiment but achieved a 2.6-fold reduction in the amount of deposited carbon for an optimal loading of 1wt.% B. Long-term experiments (12 hr) confirmed the improved stability and selectivity of Pt/1B- $\gamma$ -Al<sub>2</sub>O<sub>3</sub>, (Fig.1a) with a 3.2-fold reduction in deposited carbon and an increase in propylene selectivity from 92 to 98%. TPO-profiles (Fig.1b) of spent catalysts show that boron promotion eliminates and reduces the low- and high-temperature carbon oxidation peaks, respectively. Propylene decomposition experiments on pure and boron-modified  $\gamma$ -Al<sub>2</sub>O<sub>3</sub> relate the low-temperature peak to carbon formed on the support.

NH<sub>3</sub>-TPD experiments indicate that boron modifies the number and strength of the support acid sites. In-situ XRD experiments under H<sub>2</sub> at 600°C exclude the formation of a Pt-B alloy. TEM-EDS shows a uniform distribution of boron over the material. DFT calculations support the formation of boron oxide rather than a Pt-B alloy. Testing and characterization thus indicate that boron modifies both the active-metal *and* the support. Clearly, the promoting effect of boron is more complex than often assumed<sup>4</sup>.



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