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1 **Physicochemical implications of cyanobacteria oxidation with Fe(VI)**

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Preproof

## 13 **Abstract**

14 Increases in harmful algal blooms has negatively impacted many surface-sourced drinking water utilities.  
15 To control these blooms, many water utilities implement pre-oxidation with ozone, chlorine, or  
16 permanganate; however, pre-oxidation of algae has both positive and negative water quality outcomes.  
17 This study investigated ferrate (Fe(VI)) as an alternative oxidant by measuring its effect on cell lysing,  
18 surface characteristics, and coagulation in waters containing the cyanobacteria *Microcystis aeruginosa*.  
19 Bench scale studies were conducted to examine the complex combination of processes in a Fe(VI)-algae  
20 system. These processes were characterized by fluorescence index, surface charge, collision frequency  
21 modeling, particle counts and sphericity, total nitrogen, and ferrate decomposition measurements. Results  
22 showed that Fe(VI) lysed algal cells, but further oxidation of released organic matter is possible. The  
23 presence of algae did not significantly impact the rate of Fe(VI) decomposition. Fe(VI) pre-oxidation may  
24 also be capable of decreasing the formation of nitrogenated disinfection byproducts through subsequent  
25 oxidation of released nitrogen rich organic matter. Streaming current and zeta potential results indicate  
26 destabilization of the resulting algae and iron suspension was incomplete under most conditions. Particle  
27 collision frequency modeling indicates fluid shear to be an important aggregation mechanism of the  
28 resulting suspension. Overall, Fe(VI) is a viable alternative to other strong oxidants for water utilities  
29 struggling with harmful algal blooms, but the final fate of the resulting organic matter must be further  
30 studied.

31 *Keywords:* Harmful Algae Bloom; *Microcystis aeruginosa*; Ferrate; Fe(VI); Oxidation; Coagulation

## 32 **1. Introduction**

33 Algal blooms in surface waters are a major threat to water quality and public health, especially when  
34 the surface waters are sources of drinking water (Brooks et al., 2016). The occurrence of harmful algal  
35 blooms (HABs) are expected to increase as global water temperatures increase (Paerl and Huisman,  
36 2008), and occur in areas that historically have not had HAB problems. In some situations, an increase in

37 algae may also be an unintended consequence of successful acid rain mitigation that has increased pH to  
38 levels more conducive to the autochthonous production of organic carbon (Anderson et al., 2017).

39 *Microcystis aeruginosa* is a common type of cyanobacteria (e.g. blue-green algae) that occurs in fresh  
40 and brackish waters (Codd et al., 1989). In general, individual *M. aeruginosa* cells are polydisperse,  
41 ranging in diameters from 3 to 10  $\mu\text{m}$  (Dang et al., 2012; Fang et al., 2010; Li et al., 2016; Vlaski, 1998).  
42 This cyanobacteria species is also toxin-producing, and can cause serious liver, digestive, neurological,  
43 and skin issues in humans (Kenefick et al., 1993). Therefore, it is imperative to find the best practices to  
44 mitigate the impact of *M. aeruginosa* on drinking water supplies.

45 To control HABs, water utilities can employ several different technologies, including powdered  
46 activated carbon adsorption, and oxidation with strong oxidants, like ozone. Ozone is generally effective  
47 at addressing algal blooms and associated toxins (Loganathan, 2016). However, ozone generation,  
48 contact, and off-gas destruction equipment requires capital investment for permanent infrastructure  
49 needed to address algae concerns that are likely episodic and difficult to predict. A similar dilemma  
50 confronts other on-site strong oxidant generation approaches (e.g. chlorine dioxide and UV/H<sub>2</sub>O<sub>2</sub>)  
51 Oxidation of HABs with free chlorine is generally effective, but may increase the formation of  
52 disinfection byproducts (DBPs) (Xie et al., 2013). Permanganate (MnO<sub>4</sub>) is another option (Chen and  
53 Yeh, 2005; Ma et al., 2012a); however, health concerns related to the exposure of manganese (Mn), an  
54 unavoidable byproduct of permanganate oxidation, exist (Tobiason et al., 2016). These health concerns  
55 have resulted in Mn being placed on the Contaminant Candidate List in the United States with a  
56 recommended secondary maximum contaminant limit of 50  $\mu\text{g/L}$  (Bouchard et al., 2018) while Canada  
57 has established a regulated maximum acceptable concentration of 120  $\mu\text{g/L}$ . Ultimately, the use and  
58 selection of the best strong oxidant for HAB treatment is still unclear (Drikas et al., 2001).

59 Ferrate (Fe(VI)) is emerging as an alternative oxidant in water treatment due to its strong oxidation  
60 potential and limited production of hazardous by-products (DeLuca et al., 1983; Gan et al., 2015; Jiang et  
61 al., 2019; Sharma et al., 2016). Fe(VI) may be generated onsite as a liquid sodium ferrate product, or  
62 generated off-site and shipped as a stable potassium ferrate (K<sub>2</sub>FeO<sub>4</sub>) salt (US Patent 8.449,756 B2:

63 Monzyk et al., 2013). The use of ferrate as  $K_2FeO_4$  has low capital expenses and can be utilized as needed  
64 to address urgent water quality concerns, making it more conducive to urgent episodic use (Cui et al.,  
65 2018).

66 Fe(VI) use does not directly generate a hazardous byproduct such as  $KMnO_4$  (i.e. Mn). Furthermore,  
67 Fe(VI) does not directly form halogenated DBPs, although formation of bromate has been noted (Huang  
68 et al., 2016; Jiang et al., 2016a), with yields lower than similar dosages of ozone (Jiang et al., 2019). In  
69 addition, the in-situ formation of Fe(III) particles a  $\gamma-Fe_2O_3$  core and a  $\gamma-FeOOH$  shell that may benefit  
70 downstream treatment processes (Deng et al., 2018; Goodwill et al., 2015; Lv et al., 2018; Pucek et al.,  
71 2013) by decreasing the amount of coagulant needed due to the formation of Fe(III) during ferrate  
72 decomposition (Jiang et al., 2016b). However, questions about coagulation efficacy and dominant  
73 mechanisms remain, with differential settling (e.g. “sweep flocculation”) being proposed (Lv et al., 2018).

74 Removal of the toxin microcystins-LR (MC-LR) from the cyanobacteria *Planktothrix* by Fe(VI)  
75 oxidation has been analyzed (Yuan et al., 2002). It was found that the toxin was easily decomposed by  
76 oxidation, but the removal efficiency depended on Fe(VI) dose, pH, and contact time. The degradation of  
77 MC-LR follows second-order kinetics that decreases with increasing pH (Jiang et al., 2014). Similarly,  
78 the effect of Fe(VI) pre-oxidation on cell viability of *M. aeruginosa* and the fate of microcystins (MC) in  
79 various waters investigated by Fan et al. (2018) found that while Fe(VI) induced cell lysis, there was no  
80 significant increases in extracellular MC. A possible mechanism for this may be that reactive oxygen  
81 species and  $H_2O_2$  formed during the decomposition of potassium ferrate enter the cells and oxidize  
82 intracellular MC (Sharma et al., 2015). Fan et al. (2018) also determined that the effectiveness of Fe(VI)  
83 oxidation was decreased by high concentrations of natural organic matter (NOM).

84 The effect of Fe(VI) oxidation and coagulation on *M. aeruginosa* cell integrity, intracellular organic  
85 matter (IOM) release, and DBP formation has been observed using flow cytometry (Zhou et al., 2014).  
86 IOM release was discovered to increase with ferrate dose, and IOM is known to produce DBPs during  
87 subsequent treatment processes. Conversely, Fe(VI)-induced coagulation can destabilize *M. aeruginosa*  
88 cells, decrease the amount of algal organic matter (AOM) released, and lower concentrations of THMs

89 and HAAs (Liu et al., 2017; Zhou et al., 2014). Liu and Liang (2008), and Ma and Liu (2002) found that  
90 Fe(VI) pre-oxidation improved removal of green algae species with prolonged pretreatment time while  
91 also decreasing the required alum dosage for effective coagulation. Lastly, Alshahri et al. (2019) found  
92 that ferrate was more effective in removing AOM than FeCl<sub>3</sub> in seawater.

93 Prior studies increase understanding of the Fe(VI)-algae system, but also have limitations. Most  
94 freshwater studies used waters not demonstrative of drinking water quality, pH values > 8, or cell  
95 concentrations in the millions of cells per mL, which is not representative of bloom concentrations that  
96 may impart low to moderate adverse health effects (20,000 and 100,000 cells/mL) per World Health  
97 Organization guidelines (WHO, 2003). Additionally, the dominant collision mechanism between Fe(VI)  
98 resulting particles and *M. aeruginosa* cells has not been examined. The overall goal of this study was to  
99 fill research gaps in the use of ferrate for HAB mitigation in realistic bloom algal cell concentrations and  
100 other relevant drinking water supply conditions. Specific objectives of the research included: (1)  
101 determine the effects and extent of Fe(VI) on algal cell lysing, including IOM and total nitrogen (TN), (2)  
102 quantify surface charges on resulting Fe(III)- *M. aeruginosa* suspensions, (3) elucidate dominant  
103 mechanisms of collisions between particles, and (4) to explicate corresponding resultant particle size  
104 distributions.

## 105 **2. Materials and Methods**

### 106 **2.1. Chemicals and Reagents**

107 High purity (> 92%) Potassium ferrate (K<sub>2</sub>FeO<sub>4</sub>) was acquired as a dry, crystalline powder from  
108 Element 26 Technology (Friendswood, TX, USA), utilizing an electrochemical production method (US  
109 Patent 8.499,756 B2) All other chemicals were purchased from Fisher Scientific (Fair Lawn, NJ, USA),  
110 and were reagent grade.

## 111 **2.2. Algal Culturing and Suspensions**

112 Initial cultures of *Microcystis aeruginosa* were acquired from the University of Texas at Austin  
113 Culture Collection of Algae. The cultures were grown in batch mode in autoclaved 250 mL Erlenmeyer  
114 flasks containing 5 mL of *M. aeruginosa*, and 145 mL of sterile Bold 3N media made following the  
115 method from Plummer & Edzwald (2002). Stock cultures of the *M. aeruginosa* cells in log growth phase  
116 (approximately 1,500,000 cells/mL) were collected and separated from the Bold 3N media via  
117 centrifugation (Sorvall Legend X1R, Thermo Scientific). Algal cell concentrations of either 20,000  
118 cells/mL or 100,000 cells/mL ( $\pm 10\%$ ) were used for the experiments, and verified using a laser light  
119 blockage particle counter (PC5000, Chemtrac). These algal cell concentrations were chosen based on the  
120 WHO guidelines for cell counts that generally indicate a cyanobacterial bloom (WHO, 2003). Additional  
121 information on the growth, harvesting, separation, and preparation of algal cultures and suspensions can  
122 be found in Text SI-1.

## 123 **2.3. Ferrate Pre-oxidation Reaction**

124 Ferrate pre-oxidation experiments were carried out in mixed, cubic batch reactors (PB-900  
125 Programmable Jar Tester, Phipps & Bird) at room temperature ( $20 \pm 1^\circ\text{C}$ ). The desired concentration of  
126 algae (20,000 cells/mL or 100,000 cells/mL) was added to each reactor, along with 1 mM of bicarbonate  
127 buffer ( $\text{HCO}_3^-$ ) and reagent grade water (RGW) to reach a total volume of 1 L. The pH of the solution was  
128 adjusted to either  $6.2 \pm 0.1$  or  $7.5 \pm 0.1$  by the drop-wise addition of 2%  $\text{H}_2\text{SO}_4$ . After the pH was  
129 adjusted, a predetermined dose of ferrate (0, 20, 50, or 100  $\mu\text{M}$ ) was added to the beaker and rapidly  
130 mixed ( $G \approx 150 \text{ s}^{-1}$ ) for 1 minute, followed by slow mixing ( $G \approx 55 \text{ s}^{-1}$ ) for 30 minutes when the pH was  
131 6.2, or 60 minutes when the pH was 7.5. The pH was adjusted as necessary during mixing by drop-wise  
132 addition of 2%  $\text{H}_2\text{SO}_4$  or 5% NaOH. Samples were collected for further analyses after slow mixing.  
133 Reaction completion (i.e. absence of oxidants) was confirmed by indirectly measuring the resultant  
134 Fe(VI) concentration using the ABTS spectrophotometric method (Lee et al., 2005) and no quenching  
135 agents were utilized.



## 136 **2.4. Analytical Methods**

### 137 **2.4.1. Particle Size**

138 Particle size measurements between 2  $\mu\text{m}$  and 125  $\mu\text{m}$  were measured on a laser light blockage  
139 (LLB) particle counter (PC5000, Chemtrac). A 1 mL sample taken from the reactor at 2 cm below the  
140 water surface was diluted to 1:100, and analyzed. The dilution was made to prevent coincidence errors on  
141 the particle counter. For particle size measurements between 10 nm and 10,000 nm, an additional 10 mL  
142 sample was taken from the reactors at 2 cm below the water surface and analyzed using a Dynamic Light  
143 Scattering (DLS) instrument (Zetasizer Nano ZA, Malvern Instruments). The DLS approach is more  
144 appropriate for monodispersed, homogenous solutions with particle sizes below 10  $\mu\text{m}$ , as it is based on  
145 particle diffusion. The algal solutions created for the experiments are not monodispersed, and thus the  
146 number output from the instrument is an estimate. DLS results are not reported for algae only conditions,  
147 as *M. aeruginosa* cells are exclusively  $> 1 \mu\text{m}$  (Hadjoudja et al., 2010; Li et al., 2016). The measurement  
148 method included 7 replicate measurements, each with 9 runs.

149 Particle size was also characterized on a mass basis by iron fractionation with several filters of  
150 progressively smaller effective size exclusions following the procedure outlined by Goodwill et al.  
151 (2015). Total iron was measured using the Hach FerroVer® colorimetric method (10249) with a  
152 spectrophotometer (DR1900, Hach), conforming to Standard Methods Section 3500-Fe B (Rice et al.,  
153 2012).

### 154 **2.4.2. Surface Charge**

155 Surface charge of resulting particles were assessed via zeta potential and streaming current  
156 measurements. Zeta potential values were measured using the DLS instrument, with an overall approach  
157 similar to the particle size measurement method. The DLS technique calculates ZP by optically measuring  
158 the electrophoretic mobility of particles smaller than 10  $\mu\text{m}$ . Streaming current measurements were made  
159 using a laboratory charge analyzer (LCA-01, Chemtrac) and included cationic polymer (Nalco Nacrolyte)  
160 titrations to determine the amount of additional coagulant needed to completely neutralize the surface

161 charge of the algae-ferrate suspension. The LCA measures the change in conductivity for a wide range of  
162 particle sizes by imparting motion to the fluid suspension in order to displace the electrical double layer  
163 next to the charged particles. The displacement of the electrical charges creates a current corresponding to  
164 the amount of charge on the particles. 500 mL samples were placed into a beaker on a stir plate. The  
165 solution was slowly mixed ( $G \approx 55 \text{ s}^{-1}$ ), and the initial pH was recorded. The polymer was diluted with  
166 RGW just prior to use to achieve a stock concentration of 11.6 mg/mL. Small doses of the coagulant were  
167 added over time while the streaming current value (SCV) of the solution was monitored. The final pH of  
168 the solution, and the total amount of coagulant added to achieve a SCV of 0 were recorded.

### 169 **2.4.3. Cell Lysing**

170 Excitation-emission scans were collected on a fluorescence spectrophotometer (LS 55 Fluorescence  
171 Spectrophotometer, PerkinElmer) to identify cell lysing (Wert et al., 2014). Samples were first filtered  
172 through a 0.2  $\mu\text{m}$  MF and then excited at 370 nm. The fluorescence intensity was measured at emission  
173 wavelengths from 300 nm to 800 nm in 2 nm increments, and the excitation and emission monochromator  
174 bandpasses were set at 5 nm. Fluorescence index (FI) was calculated as the ratio of emission intensities  
175 (470 nm divided by 520 nm) at an excitation wavelength of 370 nm (Cory et al., 2010; McKnight et al.,  
176 2001). As a ratio, FI is a concentration-independent metric when applied over a narrow range of  
177 concentrations (Wert et al., 2014). Each fluorescent sample was measured in triplicate.

178 Cell lysing was also quantified via total nitrogen measurements. A full description of the methods  
179 and reagents used for the total nitrogen tests can be found in Text SI-2. Cell sphericity and 3-dimensional  
180 fluorescence images of algal cells before and after ferrate pre-oxidation as a direct indication for lysing  
181 were captured using high-content phenotypic-screening confocal fluorescence microscopy (Opera Phenix  
182 High Content Screening System, PerkinElmer). Detailed methods regarding the confocal fluorescence  
183 microscope and sphericity calculations can be found in Text SI-3.

## 184 **2.5. Collision Frequency Modeling**

185 Rectilinear Brownian motion ( $\beta_{\mu}$ ), fluid shear ( $\beta_M$ ), differential sedimentation ( $\beta_{DS}$ ), and total ( $\beta_{ij}$ )  
186 collision frequencies as a function of particle size were calculated using particle size distributions (PSDs)  
187 collected from the laser light blockage particle counter after ferrate pre-oxidation tests. The volume-  
188 average particle diameter ( $d_i$ ) used as the constant diameter of one of the two particles is defined in Eq.  
189 (1):

$$d_i = \left[ \left( \sum n_n d_n \right) / \left( \sum n_n \right) \right]^{1/3} \quad (1)$$

190 where  $n_n$  is the number of particles in the  $n$ th channel of the particle counter, and  $d_n$  is the average  
191 diameter of the  $n$ th channel of the particle counter (Chandrasekhar and Amy, 1996).

192 Two particle densities were used in the collision modeling: 978 kg/m<sup>3</sup> (*M. aeruginosa* at 20°C (Li et  
193 al., 2016)) and 1500 kg/m<sup>3</sup> (a relatively high iron-based floc density (Bache and Gregory, 2010)).

194 The rectilinear collision frequency functions are expressed by Equations SI-1 through SI-4, from Han and  
195 Lawler (1992).

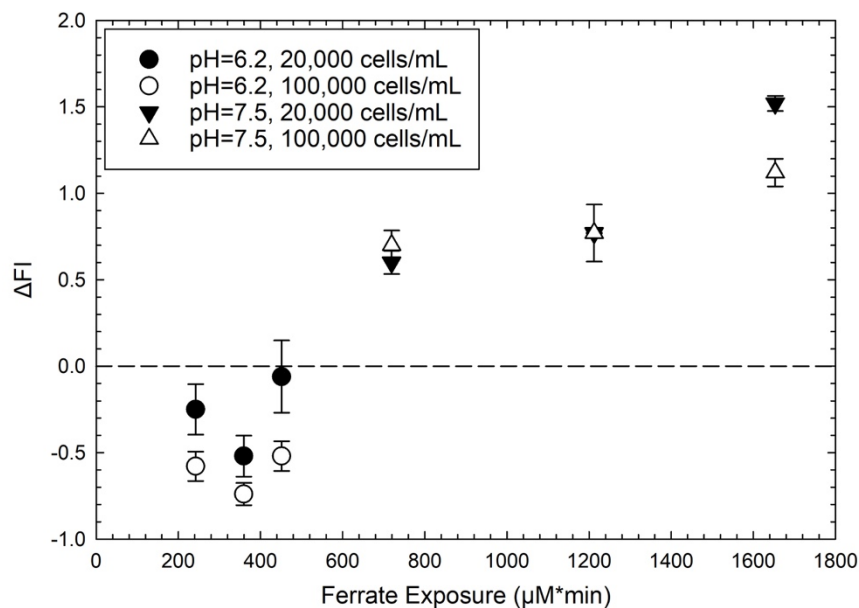
196 A curvilinear model was also presented as a set of corrections to the rectilinear collision frequency  
197 functions, following Han and Lawler (1992). These corrections account for hydrodynamic retardation and  
198 other short-range effects of particle collisions due to fluid motion. The correction factors applied to the  
199 rectilinear collision frequency functions, and the curvilinear total collision frequency are defined by  
200 Equations SI-5 through SI-8.

## 201 **3. Results and Discussion**

### 202 **3.1. Effect on *M. aeruginosa* Cell Damage**

203 Changes in FI were used to determine if IOM was released after the oxidation of *M. aeruginosa* cells  
204 with ferrate (Figure 1). The change in FI is represented by the difference between FI when Fe(VI) = 0 μM  
205 at some algal concentration and pH, and when Fe(VI) is added at the same conditions. Increases in FI  
206 indicate IOM release into the dissolved phase during oxidation, while decreases in FI correspond to IOM

207 release during oxidation, as well as further oxidation and compositional changes by Fe(VI) (Wert et al.,  
208 2014). FI detects released IOM by indicating the aromaticity of the organic matter (McKnight et al.,  
209 2001). Patterns in FI results were confirmed by results of UV<sub>254</sub> absorbance (Figure SI-1) (Wert et al.,  
210 2014).



211  
212 **Figure 1.** Changes in FI after oxidation of algal cells by ferrate in laboratory water matrix; 1 mM HCO<sub>3</sub><sup>-</sup>,  
213 initial algal concentration ≈ 20,000 cells/mL or 100,000 cells/mL, pH = 6.2 or 7.5, Fe(VI) = 20, 50, or  
214 100 μM. Each point represents the average change in FI of 3 measurements from when Fe(VI) = 0 μM.  
215 Error bars represent the positive and negative of one standard deviation.

216 At pH 6.2, all FI values are negative, indicating IOM release and further oxidation. The most  
217 significant decreases in FI at pH 6.2 occurred when the Fe(VI) dose was 50 μM (ferrate exposure = 359  
218 μM•min) for both algal concentrations. When the pH was 7.5, a majority of the FI values were positive,  
219 which suggests that IOM was released during oxidation, but there was no further oxidation by Fe(VI).  
220 The largest increase in FI when pH = 7.5 occurred when Fe(VI) = 50 μM (ferrate exposure = 1212  
221 μM•min) for the low algae concentration, but at Fe(VI) = 100 μM (ferrate exposure = 1653 μM•min) for

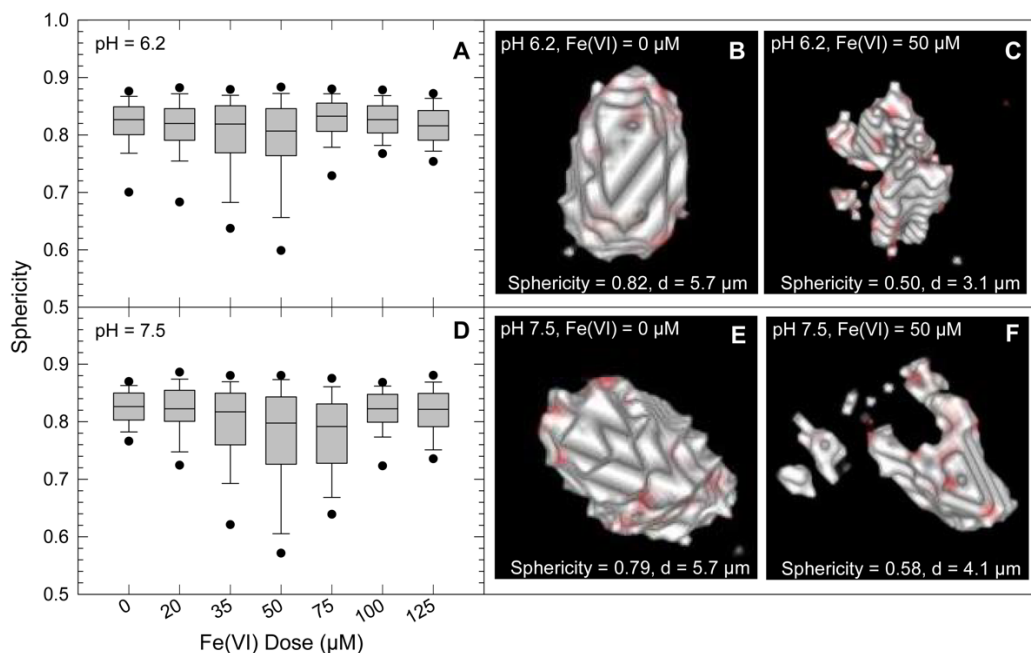
222 the high algae concentration. A comparison of the same *M. aeruginosa* concentrations and ferrate doses at  
223 differing pH values shows that IOM release and further oxidation occurs more frequently at pH 6.2.

224 It is noteworthy that IOM release and further oxidation was more prominent at a lower pH. At higher  
225 pH values, ferrate exposure is greater due to a slower Fe(VI) decay rate. However, Figure 1 shows more  
226 oxidation when the total exposure is less. This can be explained by the lower oxidation potential of ferrate  
227 at pH 7.5 versus 6.2 resulting from the dominance of  $\text{HFeO}_4^-$  with larger oxo-ligand spin density than  
228  $\text{FeO}_4^{2-}$  ( $\text{pK}_{\text{a}3} = 7.3$ ) (Sharma, 2011). Figure 1 supports the conclusion that oxidation potential is more  
229 important than total oxidant exposure with respect to algal cell lysing. A similar pH dependence has been  
230 noted with respect to Fe(VI) transformation of DBP precursors (Jiang et al., 2016b). Utilities  
231 implementing Fe(VI) for HABs must focus on pH in addition to Fe(VI) dose.

232 Total nitrogen measurements (Figure SI-2) showed a decrease in TN concentrations with Fe(VI)  
233 dose after oxidation for all conditions, especially at pH 6.2, agreeing with FI results which may further  
234 support cell lysis. This signifies that nitrogen rich IOM is released and oxidized. In addition, many TN  
235 concentrations were below the detection limit (e.g. ~100% decrease), which suggests the limited  
236 formation of nitrogenated DBPs (N-DBPs) precursor material. However, even at low concentrations (i.e.  
237  $\leq 1 \mu\text{M}$ ) certain N-DBPs (e.g. bromonitromethane) may still pose a chronic toxicity risk (Plewa et al.,  
238 2004). However, it is important to note that the relatively low TN values determined in this study it is  
239 difficult to see changes in TN values, meaning TN may not serve as an appropriate indirect method for  
240 quantifying cell lysis. A more in-depth discussion about the TN results can be found in Text SI-4.

241 Sphericity measurements (Figure 2 A & D) also show that cell lysing trends with Fe(VI) dose and  
242 pH. In general, the algal cells become less spherical when the Fe(VI) dose ranges from 20 to 50  $\mu\text{M}$ ,  
243 indicating that the integrity of the algal cells is compromised and lysing occurred. The decreased  
244 sphericity and deformed structure of lysed cells was confirmed visually using the 3-dimensional  
245 fluorescence images (Figure 2 C & F). Cells exposed to Fe(VI) have noticeable deformities and appear

246 less spherical compared to cells not exposed to Fe(VI) (Figure 2 B & E). Further discussion of the  
247 sphericity results are provided in Text SI-5.

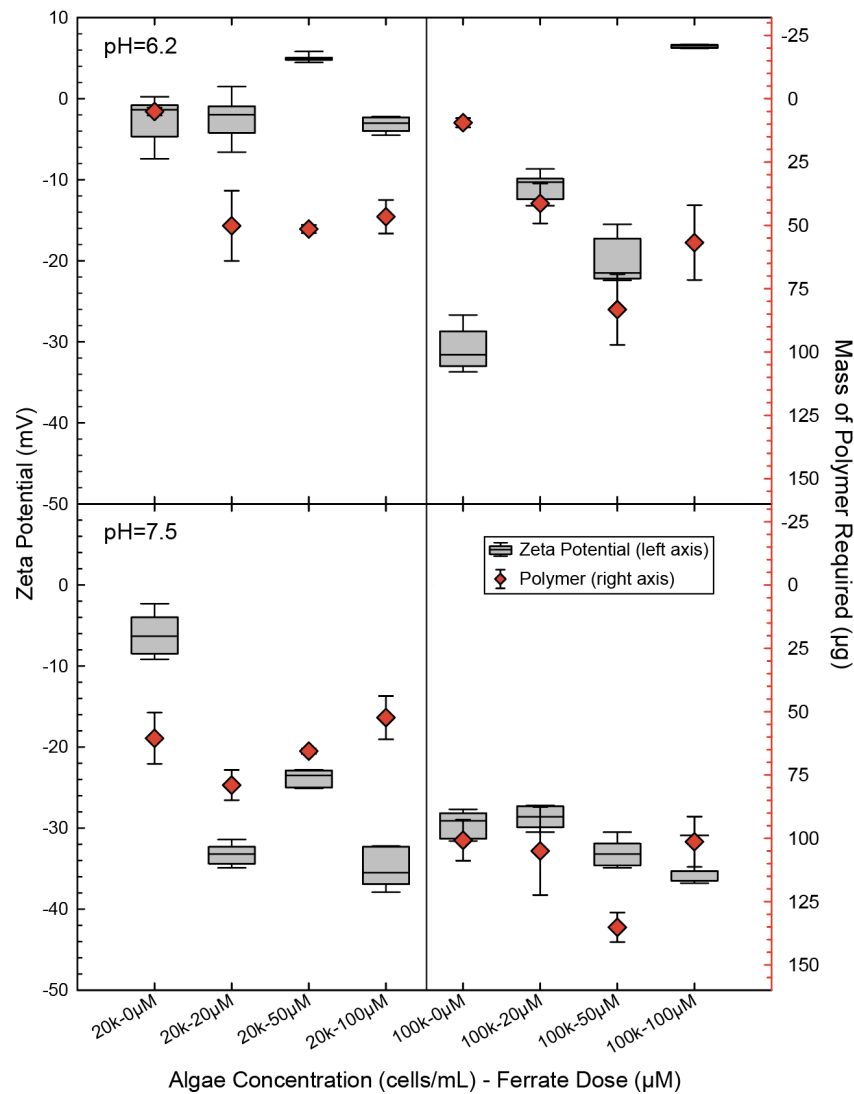


248  
249 **Figure 2:** Sphericity trends of algal cells after oxidation with varying Fe(VI) dose at pH 6.2 and 7.5 (A &  
250 D). 3-dimensional confocal fluorescence images of individual algae cells before (B & E) and after (C &  
251 F) exposure to 50 μM Fe(VI) at pH 6.2 and 7.5, respectively. The images after exposure represent the  
252 most extreme cases of lysis (i.e. cell with lowest sphericity). Experimental conditions: 1 mM HCO<sub>3</sub><sup>-</sup>,  
253 initial algal concentration ≈ 20,000 cells/mL. Each box and whisker plot represent the median, 10<sup>th</sup>, 25<sup>th</sup>,  
254 75<sup>th</sup>, and 90<sup>th</sup> percentile of 3 cells. Each point represents the 5<sup>th</sup> or 95<sup>th</sup> percentile outlier. Detailed high-  
255 content phenotypic-screening confocal fluorescence microscopy instrumental methods are located in Text  
256 SI-3.

### 257 3.2. Effect on *M. aeruginosa* Surface Charge

258 Zeta potential values were measured to assess the stability of the colloidal suspension resulting  
259 from Fe(VI) pre-oxidation (Figure 3). A negative zeta potential corresponds to negative surface charges,  
260 and denotes incomplete destabilization (e.g. insufficient coagulation). A near-zero zeta potential signifies

261 negligible surface charges, and complete coagulation. The ZP values shown are a function of algal  
262 concentration, Fe(VI) dose, and pH.



263  
264 **Figure 3.** Zeta potential and mass of polymer required to reach a SCV of 0 for algal cells and ferrate  
265 particles after ferrate pre-oxidation in lab water matrix; 1 mM  $\text{HCO}_3^-$ , initial algal concentration  $\approx$  20,000  
266 cells/mL or 100,000 cells/mL, pH = 6.2 or 7.5, Fe(VI) = 0, 20, 50, or 100  $\mu\text{M}$ . Each box and whisker plot  
267 represents the median, 10<sup>th</sup>, 25<sup>th</sup>, 75<sup>th</sup>, and 90<sup>th</sup> percentile of 7 measurements. Each point represents the  
268 average of 2 charge titrations, with error bars representing the positive and negative of two standard  
269 deviations.

270 From Figure 3, less negative ZP values were observed at pH 6.2 than for pH 7.5. For example, at  
271 20,000 cells/mL of algae and 50  $\mu\text{M}$  of Fe(VI), the median ZP values at pH 6.2 and 7.5 were +4.93 mV  
272 and -23.5 mV. This outcome is in agreement with prior Fe(VI)-HAB system ZP results (Deng et al.,  
273 2017) and further implies that particle destabilization is accomplished by charge neutralization (Bernhardt  
274 and Clasen, 1991; Van Benschoten and Edzwald, 1990). Charge neutralization occurred at a lower pH  
275 because of the low zero point charge of *M. aeruginosa* (Bernhardt and Clasen, 1991; Pieterse and Cloot,  
276 1997). There is also an increase in  $\text{H}^+$  ions at the lower pH, which serves to neutralize some sources of  
277 negative surface charge. When no Fe(VI) was added, near zero zeta potentials were recorded in the low  
278 algae condition. In general, increasing Fe(VI) doses lead to a less negative ZP at pH 6.2, and more  
279 negative ZP values when pH was 7.5 indicating incomplete coagulation occurred when the pH is greater  
280 than 7, and more complete coagulation occurred when the pH is 6.2. Therefore, pH plays an important  
281 role in the treatment process because it impacts Fe(VI) oxidation and surface charge.

282 Resulting colloidal suspensions were titrated with a cationic polymer to illustrate the extent of  
283 coagulation required after ferrate pre-oxidation (Figure 3). Titration curves indicating the amount of  
284 cationic polymer added over time versus the SCV are shown in Figure SI-4. The total amount of cationic  
285 polymer required to achieve a neutral charge during these titrations are presented in Figure 3. A larger  
286 amount of polymer required suggests incomplete coagulation after ferrate pre-oxidation. Fe(VI) alone  
287 may not be an adequate to fully destabilize an algal and Fe(III) particle suspension. A smaller mass of  
288 polymer required indicates a more neutral surface charge, and improved coagulation performance. In  
289 general, the titration results trend with zeta potentials (Barron et al., 1994). In the cases where this is not  
290 true, the discrepancies can be attributed to differences between the analytical approaches. The DLS  
291 technique optically measures the electrophoretic mobility of particles only  $< 10 \mu\text{m}$  in order to calculate  
292 ZP. On the other hand, the LCA imparts motion to the suspension in order shear layer surface charges.  
293 The displaced ions then create a current with a magnitude corresponding to the amount of charge on the  
294 particles.



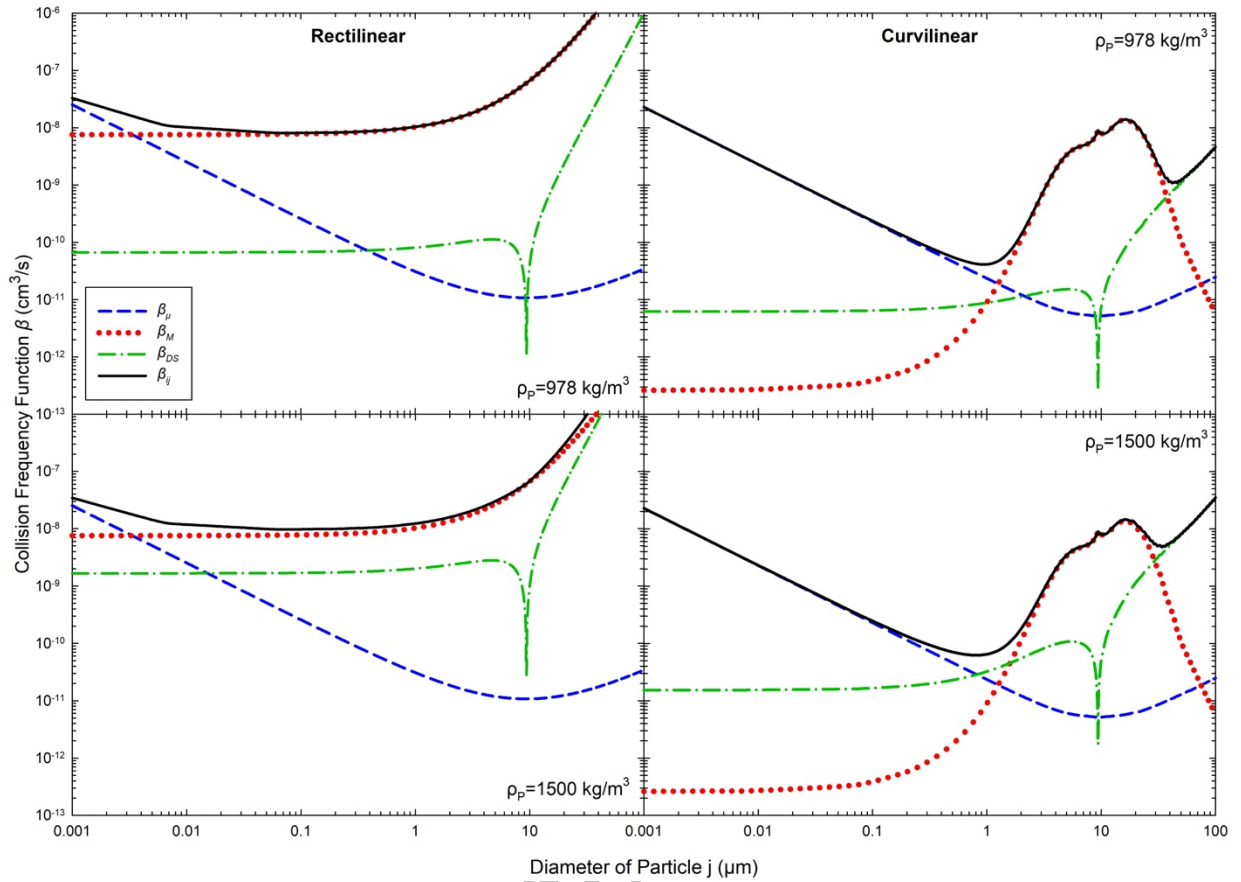
295 More polymer was required when the pH was 7.5 than for the same conditions at pH 6.2. For  
296 instance, when the algal concentration is 100,000 cells/mL and Fe(VI) = 50  $\mu$ M, the required mass of  
297 polymer for pH 6.2 and 7.5 is 83  $\mu$ g and 135  $\mu$ g respectively. Overall, the addition of Fe(VI) did not  
298 obviate the need for downstream coagulation, as assessed by the LCA. More polymer was required after  
299 Fe(VI) was added to allow van der Waals forces to govern, and to destabilize the particles. This is more  
300 evident at pH 6.2. The increase in the amount of polymer required is likely due to the increase in the total  
301 number of particles and concentration of surfaces on a  $\mu\text{m}^2/\text{mL}$  basis from Fe(VI), and the limited  
302 formation of positively charged iron-hydrolysis products from ferrate resultant iron (Deng et al., 2018;  
303 Goodwill et al., 2015; Lv et al., 2018).

304 The surface charge of the ferrate resultant particles and algae system was also impacted by cell  
305 lysing. As the algal cells are lysed, IOM is released. IOM mainly consists of proteins, polysaccharides,  
306 and lipids (Brown et al., 1997; Pivokonsky et al., 2006) that behave as anionic and non-ionic  
307 polyelectrolytes (Bernhardt and Clasen, 1991; Ma et al., 2012b), and thus can hinder aggregation,  
308 resulting in more cationic polymer required for particle destabilization (Chen and Yeh, 2005; Plummer  
309 and Edzwald, 2002). The surface charge as assessed by ZP trended with the evidence of lysing depicted in  
310 Figure 1 and Figure SI-3. The most negative changes in FI correspond to the near zero and positive zeta  
311 potentials, while the most positive changes in FI correspond to the most negative zeta values. From these  
312 results, Fe(VI)-induced IOM release is an important factor in coagulation within the algae-Fe(VI) system.  
313 When IOM is released, zeta potentials become more negative due to the negative charge of released IOM.  
314 Conversely, release of IOM followed by subsequent oxidation, which only occurred at pH 6.2, yields less  
315 negative ZP values. This agrees with previous research that stated *M. aeruginosa* cells are increasingly  
316 negatively charged with increasing pH (Hadjoudja et al., 2010). The addition of cationic polymer after  
317 pre-oxidation was always necessary to achieve a SCV of 0 on the LCA; however, some zeta potential  
318 values were positive for instances where the SCV was not 0. Different full-scale operations have different  
319 protocols for determining their basis for sufficient coagulation. For instance, a SCV of 0 is not necessarily

320 required for acceptable coagulation at the full-scale. In the majority of experimental conditions, Fe(VI)  
321 alone may be inadequate for both oxidation and coagulation processes at the pH values chosen. However,  
322 decreasing the pH below 6.2 could allow the Fe(VI)-algae system to become less stable, or more  
323 conducive to aggregation. The addition of acid and ferrate together as an advanced oxidation process has  
324 recently been explored (Manoli et al., 2017). Hydrolyzing metal salt coagulants will also decrease pH.

### 325 **3.3. Effect on Collision Frequency**

326 Figure 4 illustrates the rate of rectilinear and curvilinear collisions between a Fe(VI) and algal  
327 particle for a range of incident particle diameters and two particle densities after oxidation of 100,000  
328 cells/mL of algae by 50  $\mu\text{M}$  of Fe(VI). The x-axis denotes the particle size diameter of the particle  
329 colliding with an average size Fe(VI)-algae particle (9.38  $\mu\text{m}$ ). The y-axis represents the rate of collisions  
330 for each particle size pair per  $\text{cm}^3/\text{s}$ , for each collision mechanism (Brownian motion –  $\beta_{\mu}$ , fluid shear –  
331  $\beta_M$ , differential sedimentation –  $\beta_{DS}$ , and total –  $\beta_{ij}$ ). The curvilinear models differ from the rectilinear in  
332 that they apply a set of correction factors that account for hydrodynamic retardation and other short-range  
333 effects in particle collisions due to mixing (Han and Lawler, 1992). The dominant mode of collision is  
334 defined as the top line closest to the total collision frequency function for a certain range of particle sizes.



335

336 **Figure 4.** Collision frequency functions after oxidation of algal cells by ferrate in lab water matrix; 1 mM  
 337  $\text{HCO}_3^-$ , initial algal concentration  $\approx 100,000$  cells/mL,  $\text{Fe(VI)} = 50 \mu\text{M}$ . Each line represents a rectilinear  
 338 or curvilinear collision frequency function occurring due to  $\beta_\mu$ ,  $\beta_M$ ,  $\beta_{DS}$ , or  $\beta_{ij}$  over different diameters of  
 339 particle  $j$ . Experimental conditions:  $d_i = 9.38 \mu\text{m}$ ,  $\rho_P = 978 \text{ kg/m}^3$ , or  $1500 \text{ kg/m}^3$ ,  $T = 20^\circ\text{C}$ ,  $G = 55 \text{ s}^{-1}$ .

340 For the rectilinear model, when  $\rho_P = 978 \text{ kg/m}^3$ , Brownian motion dominates only when one particle  
 341 diameter is very small ( $< 0.005 \mu\text{m}$ ). When the particle size is  $\geq 0.005 \mu\text{m}$ , fluid shear, or mixing,  
 342 becomes the dominant coagulation mechanism, and differential settling never dominates. When the  
 343 particle density is increased,  $\beta_\mu$  is again dominant only when one particle diameter is very small ( $< 0.005$   
 344  $\mu\text{m}$ ). However, the particle size range in which  $\beta_M$  is the dominant coagulation mechanism decreases to  
 345 between  $0.005 \mu\text{m}$  and  $52 \mu\text{m}$ . Differential settling is then dominant when the incident particle is very  
 346 large ( $> 52 \mu\text{m}$ ). The rectilinear model predicts fluid shear as the dominate mechanism for most collisions

347 in the Fe(VI)-algae suspension. This is also true for varying algal concentrations, pH values, and Fe(VI)  
348 doses (Figure SI-5 and Figure SI-6).

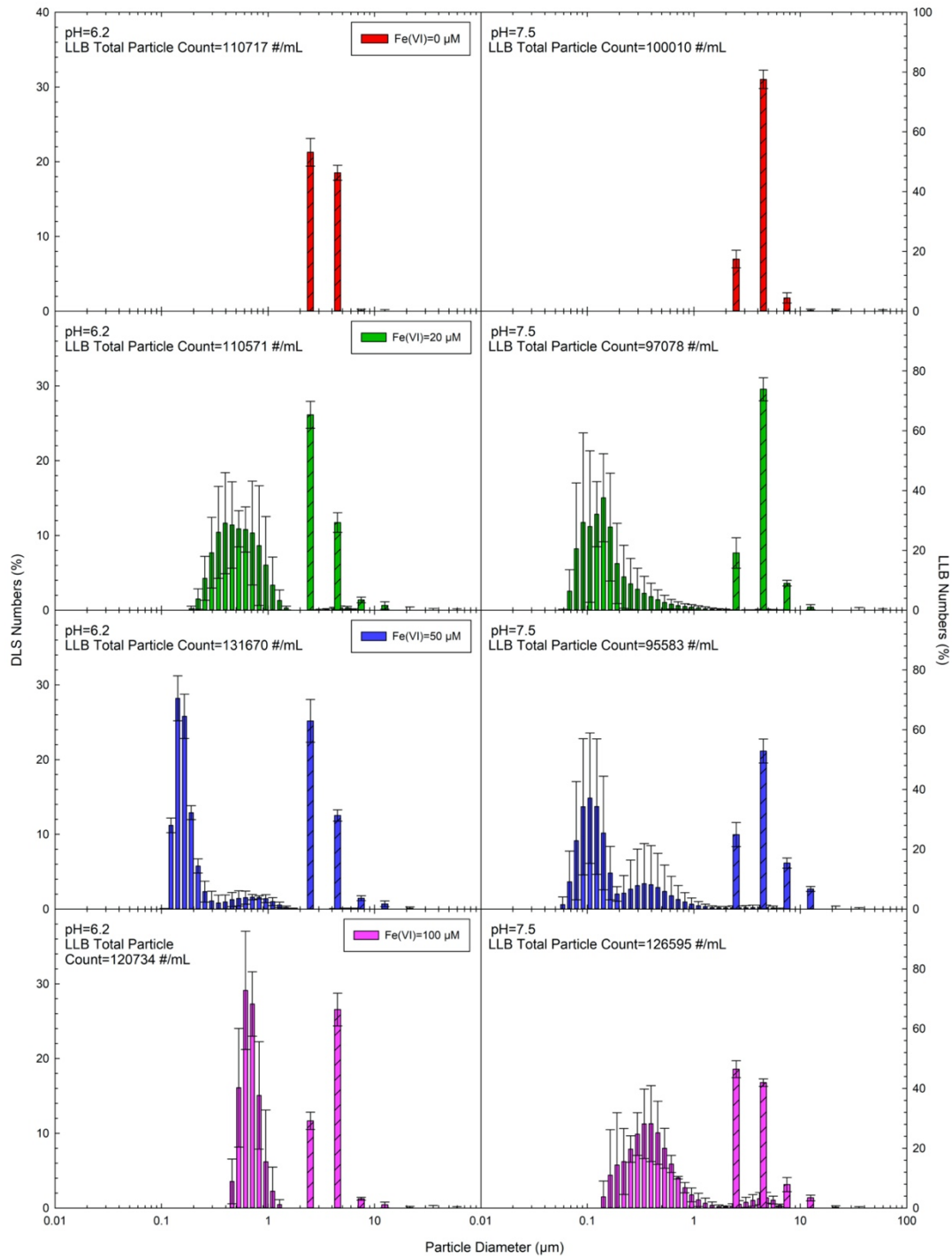
349 For the curvilinear models, Brownian motion dominates over an additional three orders of  
350 magnitude compared to the rectilinear model, regardless of particle density ( $< 1.3 \mu\text{m}$  and  $< 0.9 \mu\text{m}$ ). The  
351 range in which mixing dominates decreases to when particles are about 1 to  $30 \mu\text{m}$ , allowing  $\beta_{DS}$  to  
352 dominate over a larger range of particle diameters ( $> 30 \mu\text{m}$ ). This decreased importance of the mixing  
353 collision mechanism is the primary outcome of the curvilinear model (Han and Lawler, 1992).

354 A prior study conducted by Lv et al. (2018) concluded that sweep flocculation is the dominant  
355 collision mechanism in an ferrate system, based on typical coagulation process operating ranges  
356 developed by Amirtharajah and Mills (1982). However, this analysis did not consider the rate of  
357 differential setting and the hydrodynamic retardation and other short-range effects of particle collisions.  
358 Differential setting is a key component of sweep flocculation, and may be uniquely impacted by high  
359 number concentrations of algal particles with relative low density and corresponding settling velocities.  
360 The modeling results in Figure 4 demonstrate that  $\beta_{DS}$  is a dominant collision mechanism only when  
361 particles are quite large and relatively dense. Particle suspension results from Fe(VI) pre-oxidation of *M.*  
362 *aeruginosa* are polydisperse, and include significant contributions in the 0.1 to  $10 \mu\text{m}$  size range (see  
363 Figure 5). Therefore, the modeling results from Figure 4 indicate that fluid shear, not differential settling,  
364 is the important collision mechanism in the case of ferrate resultant particles colliding with *M. aeruginosa*  
365 cells. The importance of mixing for particle collisions will warrant attention to flocculation practices  
366 when using Fe(VI) for HABs.

### 367 **3.4. Particle Size**

368 Figure 5 shows the number particle size distribution counted by the DLS and LLB particle counter  
369 after ferrate oxidation for a particle size range from 0.01 to  $100 \mu\text{m}$ , for an initial algal concentration of  
370 100,000 cells/mL and 0, 20, 50, or  $100 \mu\text{M}$  of Fe(VI). The left y-axis displays the percent of the number  
371 of particles at a specific diameter counted by the DLS instrument, while the right y-axis displays the

372 percent counted by the LLB particle counter. Figure SI-7 depicts a similar set of results, but for an initial  
373 concentration of 20,000 cells/mL of algae.



374

375 **Figure 5.** Number particle size distribution counted by the DLS and LLB particle counter for algal cells

376 and ferrate particles after ferrate pre-oxidation in laboratory water matrix; 1 mM HCO<sub>3</sub><sup>-</sup>, initial algal

377 concentration  $\approx 100,000$  cells/mL, pH = 6.2 or 7.5, Fe(VI) = 0, 20, 50, or 100  $\mu\text{M}$ . Each unhatched bar  
378 represents the mean of 7 measurements conducted by the DLS, counted in predefined size channels with  
379 error bars representing the positive and negative of one standard deviation. Each hatched bar represents  
380 the mean of 3 measurements conducted by the LLB particle counter, counted in predefined size channels  
381 with error bars representing the positive and negative of one standard deviation.

382 From the DLS data in Figure 5, an increase in particle size occurred with increasing Fe(VI) doses for  
383 both pH values, indicating aggregation. In addition, the increase in particle sizes is more pronounced at  
384 pH 6.2 than 7.5, consistent with surface charge analysis. The DLS approach also shows that at pH 6.2,  
385 almost all of the particles are larger than 200 nm, while at pH 7.5, a significant number of particles are  
386 less than 100 nm. A lower algal concentration yielded similar particle size results (Figure SI-7). The  
387 largest average particle size when algae = 20,000 cells/mL and 100,000 cells/mL occurred when Fe(VI) =  
388 50  $\mu\text{M}$  and 100  $\mu\text{M}$ . This implies that more ferrate is required for similar levels of aggregation as the  
389 algal concentration increases.

390 The PSDs from the LLB particle counter show that approximately 98% of particles counted had a  
391 diameter between 2 and 10  $\mu\text{m}$ , however, larger flocs were visually observed. These larger flocs likely  
392 exceeded the upper limit of the LLB instrument (125  $\mu\text{m}$ ). Particle distributions in this size range changes  
393 slightly as a result of Fe(VI). At pH 6.2, particle sizes increased by  $\sim 1.0$   $\mu\text{m}$  on average after Fe(VI) was  
394 added, while at pH 7.5, particle sizes only increased by 0.13  $\mu\text{m}$  on average. LLB results support better  
395 coagulation performance at pH 6.2. Again, the lower algal concentration produced comparable results  
396 (Figure SI-7). A decrease in the total number of particles after pre-oxidation was measured likely due to  
397 the formation of flocs  $> 125$   $\mu\text{m}$ . Iron fraction results show almost all Fe was operationally-defined as  
398 large (Figure SI-8). However, based on the PSDs, there are a significant number of particles  $< 10$   $\mu\text{m}$ .  
399 This confirms that Brownian motion and mixing play an important role in collisions between resultant  
400 particles.

#### 401 **4. Conclusions**

- 402 • Fe(VI) lyses algal cells at conditions relevant to common HABs in drinking water supply, and  
403 may serve as a novel, low capital-expenditure on-demand treatment approach to periodic HABs.
- 404 • Lysing and subsequent oxidation of AOM were a strong function of pH, not the overall Fe(VI)  
405 exposure (e.g. contact time). However, lysis and AOM oxidation would likely decrease in the  
406 presence of NOM.
- 407 • Fe(VI) pre-oxidation is capable of decreasing TN concentrations by subsequent oxidation of  
408 released IOM.
- 409 • Complete coagulation in the Fe(VI)-algae system is likely not occurring. Additional polymer is  
410 required in all cases to achieve a SCV of 0. However, a system at pH 6.2 is more conducive for  
411 coagulation than at pH 7.5.
- 412 • Fluid-shear is an important particle collision mechanism in the Fe(VI)-algae system.
- 413 • Fe(VI) increased resultant particle sizes. Resulting suspensions were polydisperse. In all cases,  
414 particle size increased with the addition of Fe(VI). However, the shift was more pronounced  
415 when pH was 6.2. A majority of the particles by mass were large.

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## 425 **Appendix A. Supplementary Data**

426 Supplementary data to this article can be found online.

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