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25 ABSTRACT

26 Glycerol is an interesting feedstock for biomaterials such as biofuels and bioplastics 27 because of its abundance as a by-product during biodiesel production. Here we 28 demonstrate glycerol metabolism in the nitrogen-fixing species Azotobacter vinelandii 29 through metabolomics and nitrogen-free bacterial production of biopolymers, such as 30 poly-D-3-hydroxybutyrate (PHB) and alginate, from glycerol. Glycerol-3-phosphate was 31 accumulated in A. vinelandii cells grown on glycerol to the exponential phase, and its 32 level drastically decreased in the cells grown to the stationary growth phase. A. 33 vinelandii also overexpressed the glycerol-3-phosphate dehydrogenase gene when it 34 was grown on glycerol. These results indicate that glycerol was first converted to 35 glycerol-3-phosphate by glycerol kinase. Other molecules with industrial interests, such 36 as lactic acid and amino acids including γ -aminobutyric acid, have also been 37 accumulated in the bacterial cells grown on glycerol. Transmission electron microscopy 38 revealed that glycerol-grown A. vinelandii stored PHB within the cells. The PHB 39 production level reached 33% per dry cell weight in nitrogen-free glycerol medium. 40 When grown on glycerol, alginate-overproducing mutants generated through chemical 41 mutagenesis produced two-fold the amount of alginate from glycerol than the parental 42 wild-type strain. To the best of our knowledge, this is the first report on bacterial 43 production of biopolymers from glycerol without addition of any nitrogen source.

44

46 **INTRODUCTION**

Azotobacter vinelandii is a free living, nitrogen-fixing bacterium.^{1,2} One of the 47 48 remarkable characteristics of this species is that it can grow sufficiently in a nitrogen-free minimal medium.³ In A. vinelandii, nitrogenases prerequisite for nitrogen 49 50 fixation catalyze the reduction of nitrogen to ammonia using a large amount of energy derived from ATP hydrolysis.^{4,5} In the recently determined genome sequence of A. 51 *vinelandii*, three different types of nitrogenases have been identified.² In addition, it has 52 53 been established that A. vinelandii has the potential to produce industrially useful 54 biopolymers, including extracellular alginate and intracellular poly-D-3-hydroxybutyrate (PHB).⁶⁻⁹ Alginate is a linear polysaccharide consisting of (1-4)-β-D-mannuronic acid 55 56 and α -L-guluronic acid. Commercially available alginate is classically derived from 57 seaweed, although two bacterial genera, Pseudomonas and Azotobacter, are expected to be potential alginate producers.⁸ PHB belongs to the polyhydroxyalkanoate (PHA) 58 59 family of polyesters, and many bacterial species accumulate PHAs as intracellular 60 granules for energy storage.¹⁰ PHAs are also promising alternatives to plastics because of their biodegradability, biocompatibility, and thermoplasticity.^{6,11} Hence, A. vinelandii 61 62 is considered to be an attractive bacterium for production of two industrially useful biopolymers, alginate and PHB, in the absence of nitrogen sources.^{6,9,12-14} 63

The biosynthetic pathways for alginate and PHB production in *A. vinelandii* have previously been reviewed by Galindo *et al.*⁶ As shown in Fig. 1, alginate is synthesized from fructose 6-phosphate by many enzymes encoded by the *alg* cluster,^{8,15} whereas PHB is synthesized in three steps from acetyl-CoA and three *phb* genes are essential for synthesis.¹⁶ The regulatory mechanisms for the production of these biopolymers have been analyzed.¹⁶⁻²⁵ Thus, the biopolymers are expected to be produced from excess 70 and/or unused resource by A. vinelandii.

71 A. vinelandii is known to assimilate various carbon sources. Sucrose, glucose, 72 fructose, mannose, sorbitol, mannitol, glycerol, gluconate, and acetate can all be used as the sole carbon source for cell growth.^{26,27} Furthermore, some of them are also used for 73 biopolymer production.²⁶ However, little information exists on bacterial glycerol 74 75 metabolism including biopolymer production in a nitrogen-free environment. Glycerol 76 is generated as a major by-product during biodiesel production, and its efficient 77 utilization is now sought in various areas of food, pharmaceutical, agricultural, and 78 environmental research. Moreover, microorganism-mediated conversion of glycerol to 79 other valuable materials is being developed worldwide. Production of hydrogen, ethanol, 80 butanol, 1,3-propanediol, propionic acid, and PHAs has previously been undertaken 81 using bacteria.^{28,29}

To the best of our knowledge, no report exists on glycerol utilization in a nitrogen-free environment. Moreover, glycerol metabolism and production of biopolymers from glycerol in *A. vinelandii* remain to be clarified. The present study involves metabolomics-based identification of the glycerol metabolic pathway in *A. vinelandii* and the bacterial production of biopolymers from glycerol in a nitrogen-free environment.

88

89 **RESULTS AND DISCUSSION**

90 Sucrose and glycerol metabolism. Metabolites in *A. vinelandii* cells grown on sucrose 91 or glycerol were analyzed by a capillary electrophoresis time-of-flight mass 92 spectrometry (CE-TOFMS) (Tables 1 and 2). Small amounts of glucose-, fructose-, and 93 glycerol-related metabolites, but not glycerol-3-phosphate accumulated in the cells

94 (Table 1). Considerable amounts (400 pmol/OD₆₀₀ ml) of glycerol-3-phosphate were 95 detected in the glycerol-grown cells collected at the exponential growth phase, whereas 96 its level drastically decreased (82 pmol/OD₆₀₀ ml) in cells collected at the stationary 97 growth phase. Moreover, the dihydroxyacetone phosphate level in the glycerol-grown 98 cells was much higher than that in the sucrose-grown cells. These results suggest that 99 glycerol was first catabolized to glycerol-3-phosphate, then to dihydroxyacetone 100 phosphate, and finally converged into the glycolytic pathway. Because cell growth on 101 glycerol was slower than that on sucrose as described later, accumulation of 102 glycerol-3-phosphate was considered to be a rate-limiting step.

In the recently determined genome sequence of A. vinelandii strain DJ,² putative 103 genes for glycerol uptake and degradation were found at a locus containing four genes, 104 105 glpF, glpK, glpR, and glpD. GlpF and GlpR are annotated as putative glycerol-uptake 106 and -repressor proteins, respectively, whereas GlpK and GlpD are annotated as glycerol 107 kinase and glycerol-3-phosphate dehydrogenase, respectively. Although GlpK and GlpD 108 are classified into a group involved in phospholipid metabolism according to genome 109 annotation, metabolomics in the present study demonstrated that glycerol and 110 glycerol-3-phosphate were substrates of GlpK and GlpD, respectively, and that both 111 enzymes were necessary for glycerol metabolism.

112 Two pathways were postulated for the conversion of glycerol to dihydroxyacetone 113 phosphate. One is through glycerol-3-phosphate and the other through dihidroxyaceton. 114 A number of microorganisms can use glycerol as the sole carbon source through 115 dihydroxyacetone.²⁹⁻³¹ Furthermore, the genome sequence of *A. vinelandii* revealed the 116 presence of glycerol dehydrogenase- and dihydroxyacetone kinase-like genes (Fig. 1). 117 Hence, a dehydrogenase for glycerol and one for glycerol-3-phosphate were assayed to 118 determine the main glycerol assimilation pathway. However, no activity of either 119 enzyme was detected in the bacterial cell extract, possibly due to their low protein 120 expression level. Hence, transcription levels of the genes of the two dehydrogenases 121 were monitored by quantitative PCR (Fig. 2). As shown in Fig. 2A, the total RNA of 122 bacteria grown in all conditions was extracted without degradation. In the case of the 123 glycerol-3-phosphate dehydrogenase gene (Fig. 2B left), the cells grown to the 124 exponential growth phase showed higher gene expression than those grown to the 125 stationary growth phase. In bacteria grown to the exponential growth phase, gene 126 expression in the glycerol medium was 38-fold higher than that of bacteria grown in the 127 sucrose medium. In contrast, the glycerol dehydrogenase gene was transcribed at basal 128 levels in bacteria grown to the exponential growth phase in media (Fig. 2B right). The 129 expression of glycerol dehydrogenase in all cases tested was extremely low, but near the 130 detectable limit for our experimental conditions (data not shown). These metabolomic 131 and quantitative PCR results demonstrate that the glycerol-3-phosphate pathway is 132 predominant in A. vinelandii.

Sucrose metabolites, such as fructose 6-phosphate, mannose 6-phosphate, mannose 134 1-phosphate, and GDP mannose, were detected even in glycerol-grown *A. vinelandii* 135 (Table 1). This result indicates that gluconeogenesis, which involves the conversion of 136 fructose 1,6-biphosphate to fructose 6-phosphate, occurred in the bacteria. In addition, 137 occurance of gluconeogenesis in *A. vinelandii* demonstrates its potential for producing 138 alginate concomitantly with PHB from glycerol, which is described later.

No conspicuous rate-limiting metabolites were identified between fructose
140 1,6-biphosphate and acetyl CoA (Table 1). However, accumulation of pyruvic acid (42.5
141 pmol/OD₆₀₀ ml) was observed in glycerol-grown cells collected at the exponential

142 growth phase. Pyruvic acid is an important precursor for many metabolites, including ethanol, acetyl CoA, and lactic acid.³² In the present study, A. vinelandii produced large 143 144 amounts of lactic acid in all cases, especially in glycerol-grown cells (Table 2), and 145 levels of several amino acids accumulated in glycerol-grown cells were higher than 146 those in sucrose-grown cells. Both glutamine and glutamic acid were considerably 147 produced in all cases, especially in glycerol-grown cells collected at the exponential 148 growth phase. Arginine, lysine, and proline are synthesized from glutamic acid in most 149 bacteria. A similar accumulation profile of these amino acids was observed in A. 150 vinelandii, as shown in Table 2. Thus, A. vinelandii demonstrated the potential for 151 amino acid production under nitrogen-free conditions. Furthermore, γ -aminobutyric acid (GABA), a neurotransmitter of clinical interest,³³ was stored in the cells grown to the 152 153 exponential growth phase in sucrose and glycerol. Because bacteria-produced GABA is 154 known as a molecule of intracellular pH management due to decarboxylation of glutamic acid,³⁴ this molecule is suggested to play an important role in the 155 156 neutralization of organic acids accumulated in the cells.

Metabolomic analysis performed in the present study supported the role of the metabolic pathway predicted previously, as shown in Fig. 1. In addition, based on results of the present study, *A. vinelandii* is promising as a potential producer of many useful materials, such as amino acids, GABA, lactic acid, and biopolymers, in a nitrogen-free environment.

162

163 **PHB production.** PHB accumulation was investigated in wild-type (WT) *A. vinelandii* 164 grown on sucrose or glycerol. In addition, the mutant $\Delta algD$ cells, which have a 165 disrupted alginate synthetic gene *algD*, were also subjected to the PHB assay because

166 PHB and alginate productions are thought to be competitive. First, intracellular PHB 167 granules were monitored by transmission electron microscopy (TEM) (Fig. 3). Similar 168 to many PHB-producing bacteria, WT cells produced white and globular PHB granules, 169 which were found in both sucrose- and glycerol-grown cells. On the other hand, 170 globular PHB granules were scarcely observed and apparently degraded in $\Delta algD$ cells.

The time course of cell growth and PHB production are shown in Fig. 4. In the sucrose medium, WT and $\Delta algD$ cells showed similar growth profiles (Fig. 4A). Cell growth of both strains exceeded an OD₆₀₀ of 14. However, the lag phase of both strains grown on glycerol was longer than that on sucrose. WT growth reached an OD₆₀₀ of 6.12, whereas that of $\Delta algD$ reached an OD₆₀₀ of 16.8.

176 Figure 4B indicates the time course of intracellular PHB accumulation (per dry cell). 177 The intracellular PHB level in WT cells grown on sucrose as well as glycerol reached 178 approximately 33%. Interestingly, the PHB level of $\Delta algD$ cells grown on either source 179 initially increased, but subsequently decreased. As shown in Fig. 4A, PHB was 180 degraded in *AalgD* cells. A. vinelandii is known to convert from vegetative cells to cysts 181 under unfavorable environments for growth, and PHB has been observed in the cyst-forming cells as a probable energy and carbon storage material.¹⁴ Although the 182 183 reasons for PHB degradation have yet to be determined, the necessity for PHB might 184 waver due to the lack of alginate production following cyst formation. Production of PHB and alginate is closely regulated in A. *vinelandii*.¹⁰ The results obtained herein may 185 186 provide valuable hints on the relationships among alginate, PHB, and cyst formation.

187 Although A. vinelandii grown on glucose together with nitrogen sources synthesizes
 188 much PHB (74% per dry cell),³⁵ and some bacteria such as *Burkholderia cepacia*,³⁶
 189 *Chelatococcus daeguensis*,³⁷ *Cupriavidus necator* (formerly *Ralstonia eutropha*),^{38,39}

190 Paracoccus denitrificans,⁴⁰ Pseudomonas oleovorans,⁴¹ and Zobellella denitrificans,⁴² 191 have also been known to produce PHB from glycerol with nitrogen sources, the 192 bacterial production of PHB from glycerol without a nitrogen source contributes to 193 green chemistry.

194

195 Alginate production. The alginate production level was determined in A. vinelandii 196 grown on sucrose or glycerol. The sucrose-grown cells obtained at the stationary phase 197 produced alginate at 0.3–0.4 mg/ml, whereas those grown in the glycerol medium 198 produced enhanced levels of approximately 0.5 mg/ml. To elevate the alginate 199 production level, a random NTG-treated mutation library was used to screen 200 alginate-overproducing mutants. Unlike for PHB, it was easy to select 201 alginate-overproducing mutants because these mutants seemed to form high mucoid 202 colonies. More than 100 mutants were isolated as high mucoid colonies in comparison 203 with WT colonies.

204 One of the mutants (MT1) was subjected to TEM analysis after preparation of cell 205 thin section (Fig. 5A). Recently, A. vinelandii cells were demonstrated to be equipped 206 with a special secretion system for alginate through formation of cell-surface blebs. 207 These blebs containing alginate are formed on the bacterial cell surface and are subsequently released around the cells.⁴³ MT1 cells formed a large number of blebs on 208 209 the cell surface (Fig. 5A). On the other hand, few blebs were observed on WT cells (Fig. 210 5B). Thus, WT cells were subjected to scanning electron microscopy (SEM) analysis. A 211 few blebs were observed on the cell surface (Fig. 5C). The time course of alginate 212 secretion for WT and MT1 cells grown on glycerol is characterized in Fig. 6. Cell 213 growth (3.97 at OD_{600}) of MT1 at 96 h was lower than that (6.64 at OD_{600}) of WT (Fig. 6A). In contrast, alginate secretion by MT1 cells (0.87 mg/ml) was higher than that by
WT cells (0.52 mg/ml) (Fig. 6B). This result indicates that MT1 cells have the potential
for more alginate production through improvement in their growth conditions.

In conclusion, this is the first report on glycerol metabolism in *A. vinelandii* analyzed through the metabolomic approach. The results indicate that *A. vinelandii* grown on glycerol, but in the absence of any nitrogen source, may be useful for producing many substances, including amino acids and biopolymers (especially PHB and alginate), with industrial interests.

222

223 MATERIALS AND METHODS

224 Bacteria and culture conditions. The bacterial strains used in the present study are 225 listed in Table 3. Cells of WT A. vinelandii ATCC 12837 and an alginate-deficient mutant with a disruption of $algD (\Delta algD)^{43}$ were grown aerobically in a minimal 226 227 glycerol medium, i.e., modified Burk's medium (G-MB; 20 mg/ml glycerol, 200 µg/ml 228 NaCl, 50 µg/ml CaSO₄, 200 µg/ml MgSO₄ 7H₂O, 2.9 µg/ml Na₂MoO₄ 2H₂O, 27 µg/ml 229 FeCl₃, 0.66 mg/ml K₂HPO₄, and 0.16 mg/ml KH₂PO₄) at 30°C with agitation of 120 strokes per min. Sucrose (20 mg/ml) was also used for a carbon source instead of 230 231 glycerol in G-MB (S-MB).

232

233 **Metabolome analysis.** Metabolome analysis was supported by Human Metabolome 234 Technologies (Tsuruoka, Japan). Precultured WT cells were inoculated in 50 ml fresh 235 S-MB or G-MB, and grown to the exponential or stationary growth phase. To reach the 236 stationary growth phase, cells were grown in each medium for 84 h. To reach the 237 exponential growth phase, cells were grown in S-MB and G-MB for 40 and 60 h 238 (approximately 1.2 at OD_{600}), respectively. The cells were harvested by centrifugation 239 $(5700 \times g, 4^{\circ}C, 5 \text{ min})$, and were washed twice with 10 ml pure water. Each cell pellet 240 was homogenized in 2 ml methanol. After homogenization, chloroform (1.6 ml) was 241 added to 1.6 ml of cell extract, and the mixture was well agitated. Aqueous and 242 chloroform layers were separated by centrifugation (2300 $\times g$, 4°C, 5 min), and the aqueous layer was subjected to ultrafiltration (9100 $\times g$, 4°C, 120 min) using the 243 244 Ultrafree-MC UFC3 LCC (molecular weight cut-off, 5000; Millipore, Bedford, MA). 245 The filtrate was dried and resolved in 50 µl of pure water. Metabolites were identified 246 and quantified using CE-TOFMS system (Agilent Technologies, Santa Clara, CA).

247

248 Enzyme assay. Dehydrogenases for glycerol and glycerol-3-phosphate were assayed according to a previously described method.⁴⁴ Briefly, WT cells were inoculated in 50 249 250 ml of fresh S-MB or G-MB, and cultured to the exponential or stationary growth phase. 251 The cells were washed twice with 10 mM potassium phosphate buffer (pH 7.0), and 252 resuspended in 2 ml of the same buffer. The cells were ultrasonically disrupted at 4°C 253 and 9 kHz for 10 min (Insonator model 201M; Kubota, Tokyo, Japan). Insoluble 254 substances were removed by centrifugation (20,000 $\times g$, 4°C, 15 min), and the 255 supernatant was used as the cell extract for analysis. The cell extract (20 µl) was mixed 256 with 10 mM (final concentration) potassium phosphate buffer (pH 7.0), 5 mM substrate 257 (glycerol or glycerol-3-phosphate), and 0.5 mM coenzyme (NAD⁺ or NADP⁺). The 258 change in the absorbance of the reaction mixture at a wavelength of 340 nm was 259 monitored at 30°C for 10 min.

260

261 Quantitative PCR. Total RNA extraction, in vitro cDNA synthesis, and quantitative

262 PCR were performed to monitor the expression levels of specific genes in the bacterial 263 samples. A. vinelandii grown in S-MB or G-MB was harvested at the exponential and 264 stationary growth phases. Total RNA was extracted using the standard hot phenol 265 method. DNA degradation and subsequent RNA purification were performed using the 266 RNase-Free DNase Set (Qiagen, Tokyo, Japan) and an RNeasy Mini Kit (Qiagen), 267 respectively. cDNA, synthesized from a 200 ng RNA sample as using the ReverTra Ace 268 qPCR RT Kit (Toyobo, Osaka, Japan) according to the manufacturer's instructions, was used as a template. Quantitative PCR was performed using the SYBR Premix Ex Taq 269 270 GC (Takara Bio, Shiga, Japan) and the LineGene instrument (Toyobo).

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272 Electron microscopy. TEM and SEM analyses were entrusted to Tokai Electron 273 Eicroscopy Analysis Co. (Nagoya, Japan). A. vinelandii was grown in S-MB or G-MB 274 media (30 ml of working volume) for 72 h. In the case of TEM analysis, the culture and 275 fixing solution A (2% paraformaldehyde, 2% glutaraldehyde, and 0.1 M potassium 276 phosphate buffer, pH 7.4) were mixed in a ratio of 1:1 (total 1 ml), and stored at 4°C for 60 min. Cell pellets were collected by centrifugation (5000 $\times g$, 4°C, 5 min). Fixing 277 278 solution B (2% osmium tetroxide and 0.1 M potassium phosphate buffer, pH 7.4) was 279 added to each cell pellet and agitated. Preparation of an ultrathin section and TEM 280 analysis using a JEM-1200EX instrument (JEOL, Tokyo, Japan) were carried out as described previously.⁴³ In the case of SEM analysis, the bacterial cells were prefixed at 281 282 4°C for 1 h by mixing the culture with an equal volume of fixative consisting of 4% 283 paraformaldehyde and 4% glutaraldehyde in 100 mM cacodylate buffer (pH 7.4). After 284 centrifugation, the bacterial cells were fixed at 4°C for 24 h with 2% glutaraldehyde in 285 0.1 M cacodylate buffer (pH 7.4), additionally fixed at 4°C for 2 h with 1% tannic acid

286 in 0.1 M cacodylate buffer (pH 7.4), and washed at 4°C with the same buffer. The fixed 287 cells were treated at 4°C for 3 h with 2% OsO₄ in 0.1 M cacodylate buffer (pH 7.4) and 288 dehydrated in a series of ethanol (50%, 70%, 90%, and 100%, each 30 min). After 289 dehydration, the cells were continuously dehydrated with 100% ethanol at room 290 temperature overnight. The cells were substituted into tert-butyl alcohol at room 291 temperature, followed by freeze drying under vacuum. The cells were coated with a thin 292 layer (60 nm) of osmium by an osmium plasma coater (NL-OPC80NS, Nippon Laser & 293 Electronics Laboratory, Nagoya, Japan). The cells were observed using a scanning 294 electron microscope (JSM-6340F, JEOL, Tokyo, Japan) at an acceleration voltage of 5.0 295 kV.

296

297 PHB detection. Intracellular PHB was detected according to a previously described procedure with slight modification.^{45,46} Dried cells were treated at 100°C for 140 min 298 with 1 ml chloroform containing 0.5% (w/v) benzoic acid as an internal standard and 1 299 300 ml methanol containing 3% sulfuric acid. After addition of 1 ml distilled water, each solution was agitated for 1 min and centrifuged (1000 $\times g$, 4°C, 5 min). The lower 301 302 organic solvent layer of each sample was subjected to gas chromatography (GC) 303 analysis using a GC-2014 instrument (Shimadzu, Kyoto, Japan) and a DB-5 column (30 304 $m \times 0.25 \text{ mm} \times 0.25 \text{ µm}$; Agilent Technologies). Helium was used as the carrier gas. 305 Detector and injector temperatures were set to 275 and 230°C, respectively. Initial and 306 end temperatures were set to 60 and 200°C, respectively, with a gradient of 8°C/min. An 307 authentic sample of PHB (Sigma, St. Louis, MO) was also treated as described above 308 and was used for the identification and quantitative determination of PHB.

309

310 Isolation of alginate-overproducing mutant. A. vinelandii was grown in G-MB to the 311 exponential growth phase (approximately 0.8 at OD_{600}), and the harvested cells 312 obtained by centrifugation were washed with MB buffer (i.e., MB without a carbon 313 source). To create random mutation in the species, the cells were treated with 50 µg/ml 314 N-methyl-N'-nitro-N-nitrosoguanidine (NTG; Sigma) at 30°C for 30 min. The NTG 315 solution was removed from the sample by centrifugation, and the cells were incubated 316 overnight in S-MB. After colony formation on an S-MB plate, the highly mucoid cells 317 were selected as candidates for alginate-overproducing mutants.

318

Alginate assay. Alginate was assayed according to the method of Knutson and Jeanes.⁴⁷ 319 320 Briefly, the culture broth (200 µl) was mixed with 0.5 M EDTA (12 µl) and 5 M NaCl (4 321 μ l). Cells were removed from the mixture by centrifugation (7000 $\times g$, room temperature, 322 5 min). The supernatant (87.5 µl) was mixed with an ice-chilled mixture of sulfuric acid 323 (732.5 μ l) and boric acid solution (17.5 μ l; 45 mM KOH and 1 M boric acid) as well as 324 0.1% (w/v) carbazol (25 µl). The mixture was incubated at 55°C for 30 min, and its 325 absorbance 530 nm was subsequently measured. The alginate concentration in the 326 culture broth was determined based on the calibration using seaweed alginate as a 327 standard.

328

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- 468

1 **FIGURE LEGENDS**

Figure 1. Putative synthetic pathway for PHB and alginate from glycerol in *A*. *vinelandii*. The genes involved in glycerol metabolism are also indicated.

4

5 **Figure 2.** Gene expression of glycerol-3-phosphate and glycerol dehydrogenases. (A) 6 Total RNA from *A. vinelandii* grown in G-MB or S-MB to the exponential and 7 stationary growth phases. (B) Relative gene expression of glycerol-3-phosphate (left) 8 and glycerol dehydrogenases (right). For quantitative PCR, cDNA synthesized from was 9 used as a template in all samples. The expression levels of both genes in S-MB at the 10 stationary phase were standardized as the relative expression of 1.

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Figure 3. PHB granules in *A. vinelandii* cells revealed by TEM. Bacteria were cultured
for 72 h in S-MB or G-MB as indicated.

14

15 **Figure 4.** Time course of PHB production by *A. vinelandii.* (A) Cell growth. (B) PHB 16 accumulation in dry cells. Open circles, WT grown on sucrose; closed circles, WT 17 grown on glycerol; open triangles, $\Delta algD$ grown on sucrose; closed triangles, $\Delta algD$ 18 grown on glycerol.

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Figure 5. Alginate-overproducing mutants of *A. vinelandii*. (A) TEM observation of
MT1 cells grown on glycerol. (B) TEM observation of WT cells grown on glycerol. (C)
SEM observation of WT cells grown on glycerol. Panels A' B', and C' are magnified
views of the regions of interest indicated in panels A, B, and C, respectively.

24

- **Figure 6.** Alginate production from glycerol-grown *A. vinelandii*. (A) Cell growth. (B)
- 2 Extracellular alginate. Circles, WT; triangles, alginate-overproducing mutant.

Figure 1.



Figure 2.



Figure 3.









Figure 6.



	Concentration (pmol/OD ₆₀₀ ml)			
	Sue	crose	Glyce	erol
Metabolite	Log phase	Stationary phase	Log phase	Stationary phase
Glucose 6-phosphate ^{*1}	18.7 (±4.2)	22.5 (±29.3)	22.6 (±5.2)	61.0 (±25.4)
6-Phosphogluconic acid	U. L.	U. L.	U. L.	U. L.
2-Keto-3-deoxy-6- phosphogluconic acid	N. D.	N. D.	N. D.	N. D.
Fructose 6-phosphate ^{*2}	8.3 (±1.7)	8.2 (±11.6)	13.9 (±6.3)	29.4 (±13.1)
Mannose 6-phosphate ^{*1}	18.7 (±4.2)	22.5 (±29.3)	22.6 (±5.2)	61.0 (±25.4)
Mannose 1-phosphate ^{*2}	8.3 (±1.7)	8.2 (±11.6)	13.9 (±6.3)	29.4 (±13.1)
GDP Mannose	0.3 (±0.1)	1.0 (±0.2)	2.1 (±0.6)	5.5 (±1.3)
GDP Mannuroic acid	N. D.	N. D.	N. D.	N. D.
Glycerol-3-phosphate	11.0 (±4.4)	4.6 (±3.1)	400.3 (±186.4)	82.0 (±61.9)
Dihydroxyacetone phosphate	0.8 (±0.2)	2.0 (±1.9)	12.6 (±5.3)	8.5 (±2.5)
Fructose 1,6-biphosphate	0.5 (±0.1)	1.3 (±0.1)		2.3 (±0.4)
Glyceraldehyde-3-phosphate	2.4 (±0.4)	1.7 (±1.0)	6.2 (±2.0)	7.6 (±0.6)
Glycerate 1,3-biphosphate	N. D.	N. D.	N. D.	N. D.
3-Phosphoglyceric acid	0.8 (±0.2)	5.0 (±4.1)	1.4 (±0.1)	10.3 (±5.5)
2-Phosphoglyceric acid	N. D.	N. D.	N. D.	N. D.
Phosphoenolpyruvic acid	U. L.	7.3 (±0.1)	U. L.	14.4 (±4.0)
Pyruvic acid	11.5 (±3.7)	9.7 (±3.7)	42.5 (±24.8)	12.7 (±14.2)
Acetyl CoA	2.5 (±1.5)	4.8 (±3.8)	2.3 (±0.2)	9.1 (±4.6)

1	Table 1.	Intracellular	metabolites	determined	through	metabolomics.

2 U. L., undetectable level; N. D., not detectable under this experimental condition. ^{*1},

3 summation of glucose 6-phosphate and mannose 6-phosphate; *2, summation of fructose

4 6-phosphate and mannose 1-phosphate. Data are averages (\pm SD) of three experiments.

		Concentration	(pmol/OD ₆₀₀ ml)	
	Sucrose		Glycerol	
Metabolite	Log phase	Stationary phase	Log phase	Stationary phase
Ala	121.9 (±18.1)	95.0 (±61.3)	220.9 (±88.1)	114.1 (±35.9)
Arg	55.3 (±13.4)	19.7 (±26.0)	51.6 (±26.0)	93.7 (±16.4)
Asn	1.7 (±1.1)	U. L.	1.9 (±1.4)	5.9 (±7.4)
Asp	14.2 (±4.1)	4.9 (±3.8)	24.5 (±4.1)	24.3 (±28.1)
Cys	U. L.	U. L.	U. L.	U. L.
Gln	134.3 (±8.8)	146.3 (±180.5)	217.1 (±158.1)	184.1 (±73.3)
Glu	85.7 (±25.4)	75.4 (±112.6)	368.6 (±127.6)	134.3 (±106.9)
Gly	45.5 (±22.1)	9.5 (±5.4)	65.1 (±9.3)	70.3 (±84.6)
His	4.4 (±1.6)	1.4 (±0.8)	4.3 (±1.9)	13.3 (±12.8)
Ile	18.8 (±5.1)	1.1 (±0.5)	30.3 (±13.3)	8.9 (±11.7)
Leu	45.1 (±11.5)	1.7 (±0.7)	76.8 (±45.6)	13.0 (±17.3)
Lys	47.4 (±7.6)	13.1 (±12.9)	69.1 (±21.1)	83.5 (±32.1)
Met	7.8 (±1.8)	0.3 (±0.1)	8.5 (±5.9)	2.3 (±2.4)
Phe	7.5 (±2.9)	1.0 (±0.3)	14.9 (±8.1)	7.8 (±7.4)
Pro	15.4 (±3.3)	4.1 (±4.2)	28.2 (±5.7)	31.3 (±12.8)
Ser	58.5 (±36.7)	14.3 (±9.7)	68.1 (±23.7)	115.2 (±137.9)
Thr	39.3 (±9.8)	4.3 (±3.1)	65.0 (±25.8)	34.9 (±29.8)
Trp	2.0 (±1.0)	0.4 (±0.3)	2.0 (±1.0)	0.8 (±0.8)
Tyr	22.0 (±5.2)	3.5 (±3.2)	44.3 (±29.7)	20.7 (±10.3)
Val	121.6 (±37.6)	3.4 (±1.6)	168.8 (±100.8)	22.8 (±24.4)
γ-Aminobutyric acid (GABA)	113.9 (±39.6)	0.8 (±0.2)	238.9 (±278.8)	1.7 (±2.1)
Lactic acid	501.0 (±61.1)	530.5 (±309.1)	1239.3 (±507.3)	719.2 (±646.8)

1 Table 2. Intracellular amino acids and other organic acids.

2 U. L., undetectable level. Data are averages (\pm SD) of three experiments.

Bacterial strains	Characteristics or sequences	References
Azotobacter vinelandii ATCC 12837 (WT)	Wild type strain	ATCC
A. vinelandii ∆algD (∆algD)	Alginate-deficient strain with an insertion of the tetracycline resistance gene in chromosomal <i>algD</i> .	43
A.vinelandii MT1 (MT1)	Alginate-overproducing strain derivatized from WT by NTG treatment.	Present study

Table 3. Bacterial strains used in the present study. 1

2 ATCC, American Type Culture Collection.