# Effect of Antioxidant and Pro-oxidant on the Stability of Microencapsulated Squalene by Spray Drying

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#### ABSTRACT

Natural hydrocarbon compounds are extremely in high demand across various applications. For instance, squalene (SQ) is widely used in cosmetic and food supplement industries, due to beneficial health components. The aim of this study was to investigate the potentials of antioxidant addition on the physical properties, as well as SQ stability in spray-dried powder at various oil droplet diameters  $(0.3 - 4 \mu m)$ . Rosemary oil extract served as antioxidant, while iron (II) sulfate accelerated the oxidation. Subsequently, SQ stability was evaluated at four separate temperatures, termed 25, 50, 70, and  $105^{\circ}$ C, after one month storage. Also, the morphological structures of the samples were characterized with scanning electron microscopy (SEM). The results showed the oil droplet diameter influenced the physical properties of SQ, as lesser droplet sizes were known to enhance material strength. Furthermore, antioxidant inclusion proved to be effective in inhibiting oxidation, particularly in powders with large oil droplet diameter. The high regression coefficients (R<sup>2</sup> > 0.97) and reduced chi-square confirmed Weibull model acceptance in predicting the retention of SQ content.

Keywords: Encapsulation; oil-droplet diameter; spray drying; squalene oil; stability

# INTRODUCTION

Sea foods are very rich in practically all fundamental supplements and micronutrients needed to maintain a balanced health. An essential micronutrient includes the squalene (SQ), a natural hydrocarbon compound known to occur in plants and animals, with diverse physiological capabilities (Hosomi *et al.*, 2012). In animals, SQ exists abundantly in the liver oil of deep-sea shark (60 wt %), while in plants, considerable amounts are present in olive oil (Naziri *et al.*, 2014). This substance is predominantly applied in cosmetic and functional foods industries, as a result of notable beneficial health components.

However, due to high level of unsaturation, SQ is easily influenced by certain factors, including

temperature, moisture content, oxygen, and metals, leading to oxidation and degradative retention. This condition potentially causes rancidity and off-flavor, specifically in food products. Therefore, to solve the problem, microencapsulation technique is commonly employed, where a core material e.g. lipid, is enclosed by a polymeric compound, called the microencapsulating agent, to form an emulsion, followed by drying the resulting sample to generate microcapsules (Paramita *et al.*, 2012). The process tends to control the release rate of core materials, and also support the protection against oxidation (Munin & Edwards-Lévy, 2011). Several microencapsulation studies using spray drying and the application to functional oils have been conducted, although, very few focused on SQ encapsulation. The wall materials, including maltodextrin (MD) with different dextrose equivalent (DE), are important factors influencing the morphology of spray-dried powder. In the formation of the encapsulated powder, the use of emulsifiers become very essential. In addition, casein shows this ability by the interaction with the samples and stabilization of emulsion droplets (Jayasundera *et al.*, 2009). However, Shen *et al.* (2010) reported the strength of fish oil microencapsulation was significantly improved with blends of chitosan, modified starch, and glucose.

Apart from the wall factor, core material retention primarily depends on droplet size during emulsification. *Lesser dimensions contribute to* lower surface oil content, and in turn, results to higher retention, oxidation, and stability. Among other homogenization methods, high-pressure successfully produced small oil-droplets (Samani & Naji, 2019). The process possibly causes protein deterioration and relatively high operating costs, and therefore becomes a major concern this study seeks to address by identifying a novel and relatively inexpensive approach, but of superior quality.

The joint application of antioxidants and wall materials in microencapsulation is perceived as an effective method in preventing oxidation. Rosemary oil extract serves as a natural antioxidant commonly employed to delay lipid oxidation in fish oil/emulsion systems (Yang et al., 2016). Also, Terpinc et al., (2009) previously determined the antioxidant activity in a mixture of linoleic acid and β-carotene. The reports showed high content of phenolic extract (final concentration of 0.04 mg/mL) contributed to reduce  $\beta$ -carotene bleaching. Meanwhile, iron (Fe<sup>2+</sup>/Fe<sup>3+</sup>) was applied as an influential accelerator for the oxidation of fat, despite obtaining lesser concentration. In addition, the metal iron was observed in every production stage, from raw to packing materials, particularly in foods, irrespective of other sources, including tap water and steel processing tools. Furthermore, Wu et al. (2016) involved iron (II) chloride to promote lipid oxidation in krill oil-in-water emulsions. The results showed the iron, as a prominent pro-oxidant, triggered a rapid increase in lipid hydroperoxide, after barely a day storage.

The objective of this study is to investigate the effect of oil droplet diameter on the stability of encapsulated SQ in spray-dried powder, and also to evaluate the potentials of antioxidant in preventing oxidation. Subsequently, pro-oxidant was introduced as a new variable to provide further comprehension on the influence of oxidant variables on the system. In summary, three oil droplet diameters and three oxidant variables were utilized to generate and then analyze SQ in spray-dried dusts, particularly in the surface oil content, powder morphology, and product stability at various storage temperatures.

# MATERIALS AND METHODS

# Materials

Squalene was purchased from Tokyo Chemical Industry Co., Ltd and maltodextrin (MD) from Matsutani Chemical Industry Co., Ltd, Hyogo. Also, sodium caseinate (NC) and lecithin (LT) were mutually acquired from Miyoshi Oil & Fat Co., Ltd, while Rosemary oil extract as antioxidant (Anti), was purchased from Mitsubishi-Chemical Foods Corporation, both also in Tokyo. The iron (II) sulfate heptahydrate ( $Fe_2SO_4$ ) as pro-oxidant (Pro), and other substances were procured from Wako Pure Chemical Industries, Ltd, Osaka. These companies are all situated in Japan.

# Methods

# **Preparation of feed emulsions**

A 3 x 3 factorial experimental design was employed in the experiments with oil droplets of small diameter (Sd), medium (Md), and large (Ld). Also, the variables included 2 wt% RM (Anti), and 100 ppm Fe<sub>2</sub>SO<sub>4</sub> (Pro), but with no oxidant as a reference (Ref). Table 1 represents the sample code names and experimental designs. Furthermore, total solid content is comprised of 40 wt% SQ, 3 wt% NC, 54.6–56.6 wt% MD, and 0.4 wt% LT. However, MD with DE of 19 served as wall material (Ghani *et al.*, 2017), while NC associated with LT were employed as an emulsifier (Hoang Thi *et al.*, 2013).

The MD and NC were dispersed in distilled water, using Bio shaker (BR – 13 UM Taitec, Saitama, Japan) 110 rpm at 50 °C, and was reserved overnight for complete dissolution. Subsequently, oil-in-water emulsions were prepared by adding SQ previously mixed with LT, to separate aqueous phase. Moreover, for antioxidant (Anti) variable, RM was combined with SQ and LT, while for pro-oxidant (Pro),  $Fe_2SO_4$  was added to the distilled water prior to MD and NC.

However, the samples were subjected to Polytron Rotor-stator (PT 6100 Kinematica GA, Littau, Switzerland), operating at 8000 rpm for 3 minutes with 30-s intervals for every minute at room temperature. The homogenized emulsions were further processed to high-pressure homogenizer (HJP-25001K Sugino, Uozu, Japan) at 100 MPa at 50 °C for two cycles, in an effort to obtained smaller oil-droplet diameters.

	Variables				
Sample names	Total solids (wt%)	Homogenization process	Atomizer speed during spray drying (rpm)		
Sd-Ref	40	rotor stator + high pressure	10,000		
Sd-Anti	40	rotor stator + high pressure	10,000		
Sd-Pro	40	rotor stator + high pressure	10,000		
Md-Ref	60	rotor stator	30,000		
Md-Anti	60	rotor stator	30,000		
Md-Pro	60	rotor stator	30,000		
Ld-Ref	40	rotor stator	10,000		
Ld-Anti	40	rotor stator	10,000		
Ld-Pro	40	rotor stator	10,000		

#### Table 1. Experimental design applied for microencapsulated SQ production

# **Emulsion Viscosity**

The viscosity of feed emulsions was measured at 50 °C, using R/S plus rheometer (DVII+ Brookfield Engineering Lab, Inc. MA, USA) equipped with rotating cone plate. Individual sample was analyzed in triplicate, with a new substance for separate replicate.

# **Spray Drying**

This process was performed in a pilot-plant spray dryer (Ohkawara L-8 spary dryer Kakouki Co. Ltd. Yokohama, Japan) armed with rotary atomizer. The inlet and outlet temperatures was set to 140 °C and 80-90°C, respectively, while feed flow rate was specified at 25 mL/min, although, air flow rate was adjusted to 110 kg/h. Consequently, precipitates from spray drying were stored prior to analysis at -30 °C in an aluminum bag under a nitrogen atmosphere.

# **Oil Droplet Size Distribution**

The oil droplet diameter in both emulsion or spraydried powder, and particle diameter distribution was determined, using laser diffraction particle size analyzer (SALD-7100 Shimadzu Corp., Kyoto, Japan) equipped with a batch sample cell. Diameter distribution refers to the ratio of certain particle size to the total volume of sample. The distance is believed to be uniform for a narrow distribution. However, to determine oil droplet diameter in either emulsion or spray-dried powder, the sample was first dissolved in distilled water prior to inclusion into matrix, with the aim of destroying the wall materials, while for powder particle, 2-Methyl-1propanol was introduced in place of distilled water. Each sample was analyzed in triplicate and the mean values of the volume mean diameter ( $D_{4,3}$ ) with confidential intervals of 95% was reported.

#### **Moisture Content**

The moisture content evaluation of separate samples was performed with halogen moisture analyzer (Mettler Toledo, Ohio, America) at 160 °C. Also, each sample was analyzed in triplicate.

# Scanning Electron Microscopy (SEM)

Scanning electron microscopy (SEM; JSM 6060 JEOL Ltd., Tokyo, Japan) was employed to observe an enlarged image of the morphology and cross-section of encapsulated SQ. Prior to analysis, these samples were obtained by manual fracturing, using mortar and pestle, and were then coated with Pt-Pd, under a magnetron sputter (MSP-1S IXRF Systems Inc, Texas, USA) operating at accelerated current of 30 mA for 1 – 2 minutes. Furthermore, magnification to present the general morphology and cross-sectional image were specified at 200 and 2,500 times, respectively.

#### **Encapsulated Yield**

Encapsulated yield is the ratio of oil successfully captured from the matrix to the total oil in powder. However, to determine this value, total and surface oil of SQ were first evaluated, according to Shiga *et al.* (2014) with slight modification. To measure surface oil content, 100 mg of SQ powder was dissolved in 4 ml of hexane solution, using Eyela Mixture (CM-1000 Tokyo Rikakikai Co. LTD.) at 1,600 rpm for 15 minutes. Also, to ascertain total oil content, similar sample quantity was first dissolved in 4 ml of dimethylformamide (DMF) prior to extraction, in order to destroy the wall materials. Subsequently, centrifugation was conducted, using Tabletop Centrifuge 2410 (Kubota Corp., Tokyo, Japan) operated at 3,000 rpm for 10 minutes.

Chromatographic separation in hexane phase was performed with GC-FID (GC-2010 Shimadzu Corp., Kyoto, Japan) equipped with ULBON HR-1 ( $\emptyset$ 0.25 mm x 30 m x 0.5 µm) column and operated as follows: SPL (Injector) Temp., 280 °C; Column Temp., 270 °C; FID (Detector) Temp., 300 °C; carrier gas, nitrogen; and retention time: 13 minutes.

# Stability of the SQ Oil Powder

The SQ powders were reserved for one month at 25, 50, 70, and 105 °C in a drying oven (SA 460 Masuda Corp., Osaka, Japan). Also, SQ was then sampled

and extracted at predetermined time to measure the remaining amount of total oil.

Retention (R) = 
$$\frac{(\text{remaining amout of SQ})}{(\text{initial amount of SQ in the powder})}$$
 (1)

The SQ retention is expected to gradually decrease during storage, as shown by the retention graph. In addition, Weibull distribution function was then employed to describe the degradation. This model is widely applied in food engineering, due to the simplicity and flexibility in estimating the parameters (Corzo *et al.*, 2010). The Weibull distribution function for this research is determined in Eq. (2)

$$R = \exp\left[-(kt)^n\right] \tag{2}$$

where *R* [-] is the SQ retention, *t* (day) is the storage time, k (day<sup>1</sup>) is the degradation rate constant, and *n* is the parameter for degradation mechanism.

#### Statistical analysis

The SQ properties were subjected to variance analysis (ANOVA) with 95 % significance level, using IBM SPSS Statistics 23 software (SPSS Inc., Chicago, IL). As the requirements for homogeneity of variances were satisfied, Tukey test was performed to examine sample variation.

#### **RESULTS AND DISCUSSIONS**

# Oil Droplet Size Distribution aand Moisture Content

Figure 1 and Table 2 represent SQ oil characteristics in emulsions and spray-dried powders, respectively. Separate experimental designs produced mixtures characterized by varying mean oil droplet size, in both media. The solutions prepared with high-pressure (Sd) were monomodal and also obtained the narrowest distribution (p < 0.05) and were distinguished by the smallest  $D_{a,a}$  around 0.2 µm (n=3). Meanwhile, with only rotor-stator homogenizer (Md and Ld), the blends were shown to be bimodal and all acquired wider  $D_{43'}$ compared to Sd (p < 0.05), almost 10 times bigger. This result was similar to previous research by Shiga et al. (2017), although, with significantly unstable mean diameters  $D_{4,3}$ . The graph illustrated the distribution of Md and Ld to overlap each other, but after spray drying, the variation became more pronounced.

The powders prepared by rotor-stator homogenizer, and with sufficient concentration (Md), were observed to be monodal with  $D_{4,3}$  around 1 µm (n = 3). These samples apparently obtained smaller oil-droplet diameter and narrower distribution, compared to Ld (p < 0.05). The results confirmed previous researches, where abundant solid content triggered greater viscosity, and then relatively homogeneous droplet sizes. Higher emulsion viscosity tends to restrict the oil droplets, therefore, leading to the inability to form bigger droplet sizes, particularly in spray drying (Carmona *et al.*, 2013; Jafari *et al.*, 2008). The addition of both antioxidant



Figure 1. Oil-droplet size distributions of SQ in emulsions (a) in spray-dried powders (b). Black symbol represent reference, gray symbol represent antioxidant, and white symbol pro-oxidant, With Sd:  $\bullet$ , $\bigcirc$ , $\bigcirc$ ; Md:  $\blacktriangle$ , $\triangle$ , $\triangle$ ; Ld:  $\blacksquare$ , $\Box$ , $\Box$ 

	Emulsions		Spray-dried powders		
Samples	Volume mean diameter $(D_{4,3})$ , (µm)	Viscosity (mPa.s)	Volume mean diameter (D <sub>4,3</sub> ), (µm)	Powder diameters ( <i>Dv<sub>0.9</sub></i> ), (μm)	Moisture Content (%)
Sd – Ref	$0.21 \pm 0.11^{b}$	3.96 ± 0.28 <sup>b</sup>	0.26 ± 0.00ª	$50.56 \pm 0.12^{e}$	2.12 ± 0.22 <sup>a</sup>
Sd – Anti	0.20 ± 0.11ª	6.44 ± 0.46°	$0.34 \pm 0.01^{\circ}$	$54.66 \pm 0.10^{9}$	$2.35 \pm 0.15^{\text{abc}}$
Sd – Pro	$0.21 \pm 0.11^{b}$	2.83 ± 0.15ª	$0.27 \pm 0.11^{b}$	$53.80 \pm 0.20^{f}$	$2.73 \pm 0.21^{cd}$
Md – Ref	$1.35 \pm 0.25^{d}$	$68.77 \pm 4.14^{de}$	$1.03 \pm 0.21^{e}$	37.45 ± 0.19 <sup>b</sup>	$2.55 \pm 0.15^{bcd}$
Md – Anti	$1.26 \pm 0.17^{\circ}$	$64.19 \pm 2.43^{d}$	$0.92 \pm 0.18^{d}$	38.45 ± 0.18°	$2.78 \pm 0.09^{de}$
Md – Pro	1.25 ± 0.19°	$81.94 \pm 5.15^{e}$	$1.00 \pm 0.19^{e}$	$34.86 \pm 0.20^{a}$	$2.80 \pm 0.03^{de}$
Ld – Ref	$2.47 \pm 0.29^{f}$	2.92 ± 0.27ª	$3.74 \pm 0.07^{\circ}$	$44.84 \pm 0.10^{d}$	$2.32 \pm 0.15^{ab}$
Ld – Anti	$2.11 \pm 0.30^{e}$	2.91 ± 0.29ª	$3.53 \pm 0.07^{f}$	$61.13 \pm 0.18^{h}$	$2.18 \pm 0.01^{ab}$
Ld – Pro	$2.37 \pm 0.31^{f}$	2.97 ± 0.42ª	$3.69 \pm 0.08^{fg}$	$51.42 \pm 0.34^{h}$	$3.17 \pm 0.09^{\circ}$

Table 2. Characteristics of emulsions and spray-dried powders of SQ oil

Data represent mean  $\pm$  standard deviation (n = 3)

Different letters in the same row indicate significant differences (p < 0.05) among samples.





Figure 2. Encapsulated yield of SQ in spray-dried powders

and pro-oxidant were proven to generate constraints to the distribution of oil droplet diameter, in emulsions and spray-dried powders. These conditions matched the report by Liu *et al.* (2015), where only slight variations were detected on mean particle diameters. Furthermore, Wu *et al.* (2016) indicated the use of iron to promote oxidation on krill oil, produced minimal effect on physical stability of emulsions. In the case of moisture content in spray-dried powders, the entire samples occur between the range of 2 - 3% and the dimensional variables were not able to influence the powder diameters. However, the addition of antioxidant showed slightly greater oil droplet width, probably due to similar introduction believed to instigate a decline in the ratio of sodium caseinate to carbohydrate, as well as in the accessibility to stabilize



Figure 3. SEM Images of powder surface structures at 200 times (a) and 2,500 times magnification (b)

air/water interface during atomization (Hogan *et al.*, 2001).

#### **Encapsulated Yield**

Previous study reported a lower encapsulated SQ to total oil ratio, denoting a higher surface oil (Frascareli *et al.*, 2012), but with more air exposure, vulnerability to evaporation, and loss of core materials. Figure 2 showed the encapsulated yield in spray-dried powders, where larger oil droplet diameter tends to lower this ratio (p < 0.05). The results supported the provision by Jafari *et al.* (2008), where emulsions with larger droplet size were more susceptible to droplet breakdown during atomization, and this generates a more extensive surface oil in the microcapsules produced.

#### Morphology of Visualization of Spray-dried Powder by SEM

Figure 3 shows the SEM images of SQ surface and cross-section in spray-dried powders. In general, the entire dusts possess similar rounded surfaces, as described by separate authors (Gallardo *et al.*, 2013; Pourashouri *et al.*, 2014). Powders with substantial oil droplet diameters (Ld) was assumed to agglomerate and adhere to each other, or form a larger mass, compared to the rest samples. The agglomeration was probably due to surface oil existence, known to trigger the formation of permanent link (Frascareli *et al.*, 2012). This further confirmed the previous results discussed above, as the absolute cross-sectional images showed vacuoles inside the sample, as evident in multiple-core capsules, where during the drying state, core materials were expanded and distributed throughout the wall. Meanwhile, the center portion appeared vacant or void (Jafari *et al.*, 2008). However, extensive oil droplet size indicates a narrower distance between oil and powder surface, therefore, the oil is possibly oxidized.

#### **Stability of Encapsulated SQ Powders**

Figure 4 shows SQ stability in spray-dried powders as a plot of SQ retention against incubation time. The upper row values indicated the incubation data at 25 and 50 °C, while for the bottom row, 70 and 105 °C were obtained. In addition, the graph of retention/degradation revealed an exponential tendency in the drying curves, and was validated, using Weibul distribution model. High determination coefficients and low  $x^2$  values (p > 0.05, not shown) suggests the model was suitable to predict the degradation of SQ retention in spray-dried powder, and from the parameters, e.g degradation rate constant and shape, the effect of oil droplet and oxidant variables are potentially comprehended (Eq. 2; data not shown). However, shape factor appears to be related to initial speed of mass transfer. Therefore, lesser parameter resulted to more degradation at the commencement of storage (Miranda et al., 2010).

In high temperatures, larger oil-droplet diameter tend to generate higher degradation rate constant (p < 0.05). Conversely, small diameter (Sd) showed relatively lowest degradation rates, compared to other sizes. As suggested by Ghani *et al.* (2016), this phenomenon was attributed to the oxidation reaction, due to the

propagative transfer rate of radical oxidation between oil droplets. Also, the mechanism of the oxidation and SQ degradation is, however, under investigation.

Based on the shape parameter results, addition of pro-oxidant is capable of accelerating oxidation in small diameter variables (Sd-Pro), but not for bigger oil-droplets without the inclusion (Ld-Ref and Md-Ref) (p > 0.05). These findings indicated extensive oil droplet appear more vulnerable to oxidation, particularly in extreme conditions, as supported by previous study on oxidative stability of encapsulated flaxseed oil (Shiga *et al.*, 2017) and *d-limonene* (Soottitantawat *et al.*, 2003). However,

the antioxidant did not show any significant difference in degradation rate constant, compared to other samples, even in powder with large diameter (Ld-Anti and Md-Anti). This confirmed the role of antioxidant in preventing oxidation (Jin *et al.*, 2019; Yeşilsu & Özyurt, 2019), and to also support powder with larger oil droplet diameter, in order to effectively perform similarly to small oil droplet. Furthermore, Weibull distribution has been applied as a common kinetic model to correlate degradation mechanism in solid-state reactions. This model was reported to successfully match the drying curve in the case of flavor release from spray-dried powder (Sultana & Yoshii, 2019).



Figure 4. Retention of SQ in spray-dried powders (Weibull distribution model). Black symbol represent reference, gray symbol represent antioxidant, and white symbol pro-oxidant, With Sd: ●, ○, ○; Md: ▲, △, △; Ld: ■, □, □

#### CONCLUSION

Based on results and discussion, this experiment has confirmed the influence of oil droplet diameter on the physical properties of squalene (SQ) in spraydried powders. These characteristics include oil droplet size distribution in emulsion and spray-dried powder, encapsulated yield, and powder morphology. Lesser droplet dimensions tend to reduce surface oil content, and instigate higher particle stability. Consequently, the addition of antioxidant and pro-oxidant did not observe any significant variation in the properties, but showed substantial effect on oxidative stability. Furthermore, minimal oil droplet size was proven to be relatively resistance to oxidation, initiated by involving prooxidant. Similarly, antioxidant was confirmed to be very effective in refraining oxidation occurrence, specifically in powder with large oil droplet diameter. Therefore, the optimum percentage of antioxidant added to SQ demands further discussions.

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# **CONFLICT OF INTEREST**

There is no conflict of interest regarding the publication of this article.

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