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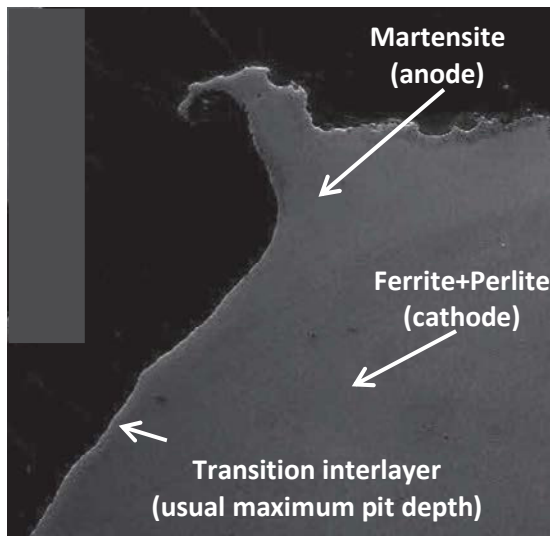


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Highlights:

- Corrosion studies of TMT bars in simulated pore solutions and in concrete slabs.
- The outer martensite acts as anode and the core as cathode when both parts of the bar are coupled.
- The core material does not meaningfully increase the corrosion rate of the outer martensite.
- The usual depth of the pits is related to the microstructure of the TMT bars.
- Once the pits reach the martensite-core interlayer, they tend to progress by mouth widening.

Graphical abstract



# Influence of the microstructure of TMT reinforcing bars on their corrosion behavior in concrete with chlorides

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## **Abstract**

Thermomechanically treated (TMT) carbon steel bars, often known as TempCore™ bars, are commonly used as reinforcements in concrete structures. TMT causes the formation of a martensite case in the outer surface of the bars, increasing their hardness, while the remaining ferritic-perlitic core maintains the typical ductility of hot rolled bars. In this work, the effect of this TMT induced microstructure on the development of pitting attacks in chloride media has been analyzed in depth. Electrochemical impedance spectroscopy (EIS) measurements and polarization curves have been carried out in simulated pore solutions to understand the effect of the presence of different phases in the microstructure and to quantify the strength of the galvanic couple that the outer martensite can form with the inner core. Moreover, accelerated corrosion tests in chloride contaminated concrete slabs have been performed. Bars from six different slabs where corrosive attack has been forced for different times have been studied. The shape of the main pits in the bars corroded in concrete has been analyzed through optoelectronic microscopy and the results obtained prove that the depth of the attack is related to the microstructure of the TMT bars.

**Keywords:** corrosion; pitting; chloride; concrete; thermomechanical treatment; carbon steel; galvanic coupling.

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## 1. Introduction

Reinforcing steel bars are usually embedded in concrete to increase the tensile properties of this material. They tend to corrode in chloride contaminated environments, being this problem one of the main causes of in-service failure of the structure. The initiation period of corrosion is the time needed for these depassivating ions to diffuse through the concrete cover and reach a critical concentration on the surface of the rebar high enough to cause the onset of the corrosion. This period usually implies the most significant part of the service life of the structures in marine atmospheres and its length depends on the porosity, thickness and other characteristics of the concrete cover [1,2]. Moreover, the microstructure and chemical composition of the bars can also affect the critical chloride content and other aspects very relevant for in-service performance of the structure, as the location and morphology of the attack.

Cold rolled carbon steel bars can offer higher mechanical strengths than traditional hot rolled bars [3,4], but the former are less ductile than the latter. Moreover, the stresses in the microstructure of cold rolled bars can make them more prone to corrosion, as it has been determined by mass loss tests carried out in solutions [5], and they present worse after-fire mechanical properties [3,4]. To increase the mechanical properties of hot rolled carbon steel bars, the addition of microalloying elements as well as thermomechanical treatment (TMT), can be used [6]. The addition of carbon in amounts ranging between 0.3 and 0.5% hardens the steel, but its bendability and weldability decrease [7], and, when considered that range of carbon contents the carbon equivalent can easily overpass the limit of 0.5% fixed in standards as EN10080 [8].

TMT bars, often known as TempCore™ bars, are manufactured by passing the red heated steel -just after the rolling process- through a chamber with a control water flow that quenches the outer surface of the bars, while their core remains hot as austenite [9]. A martensite case is formed in the outer part of the bar. Then, in the core, the austenite is transformed into ferrite and perlite through a slow cooling, while the heat dissipated from the center of the bar to the surface causes the self-tempering of the previously formed martensite [10]. The martensitic case formed in the outer surface of the bars increases their hardness [11], while the remaining ferritic-perlitic core maintains the typical ductility of hot rolled bars. The final strength of the TMT rebars depends on the thickness of the outer tempered martensitic case as well as on the distribution of other phases inside the core of bar [12]. Nowadays, the use of TMT

65 carbon steel bars has become common for reinforcement of concrete structures in  
66 Europe.

67 There are studies published on the influence of the microstructure of TMT  
68 carbon steel bars on the fracture mode and ultimate tensile strength of the bars [9].  
69 Moreover, TMT bars have shown better results in tensile and impact tests than direct  
70 air-cooled microalloyed hot rolled bars [13]. The influence of high-temperature  
71 exposure on the mechanical properties of the TMT bar is a point that has also been  
72 studied [3,14], with their results being worse than those shown for traditional hot-rolled  
73 carbon steel bars [3]. The fatigue performance of TMT bars has also been investigated  
74 [15].

75 The corrosion performance of the steel reinforcements is another key factor for  
76 the in-service performance of the structures. The alkaline solution inside the concrete  
77 pore should be able to guarantee the chemical durability of the steel. However, factors  
78 such as the presence of chlorides [16] or the decrease of the pore solution pH caused  
79 by carbonation [17] often provoke the active corrosion of the reinforcing steel bars.  
80 Microalloying elements that are able to improve moderately the corrosion resistance in  
81 saline solutions of the steel bars can also be added to TMT bars [18].

82 There is a corrosion study carried out with TMT bars where weight losses after  
83 sea water and fresh water immersions were measured [5]. The results obtained in this  
84 research suggest that the corrosion resistance of TMT bars could be higher than that of  
85 conventional hot rolled reinforcing bars. Another corrosion study with TMT bars also  
86 reports weight losses in NaCl solutions [6]. Recent preliminary results on the effect of  
87 the galvanic coupling between TMT and conventional reinforcement steels on their  
88 corrosion performance in simulated pore solutions have also been published [19].

89 Moreover, it has been conclusively proved that the morphology of the pits is a  
90 key factor influencing the tensile [20-22] and the fatigue [23,24] behaviors of the  
91 reinforcing bars, and so, it determines the likelihood of dangerous pathologies or in-  
92 service failures for the structures. The relationship between the microstructure of the  
93 reinforcing bars and their pit morphology has been analyzed in depth for stainless steel  
94 corrugated bars in simulated pore solutions, demonstrating that the size and  
95 distribution of the pits is related to different stresses and grain sizes caused by the  
96 forming process [25]. There are also previous studies about corrosion development of  
97 carbon steel in concrete [26,27], but they have not considered the possible influence of  
98 the specific microstructure that appears in the bars after TMT.

99 The frequent use of TMT bars and the clear interest of corrosion performance  
100 evidence the need for obtaining more complete information about how the phases  
101 present in their microstructure can influence the development of the attack in the bars.  
102 In this work, the influence of the microstructure originated by the TMT on the corrosion  
103 behavior of reinforcing bars is analyzed in solution tests, using different electrochemical  
104 techniques. The relative corrosion resistance of the phases present in the bars, their  
105 interaction and the resulting impact on the corrosion mechanism are analyzed. There  
106 are several factors implied in the onset and development of the corrosion of steel in  
107 concrete that are impossible to replicate in solution tests [28]. Hence, bars are heavily  
108 corroded in concrete slabs for different times, and a morphological analysis of the  
109 shape of the main pits detected is carried out to verify the results obtained in solution  
110 about the influence of the microstructure in the development of the pits.

## 111 2. Experimental

112 Carbon steel TMT bars type B-500-SD (EN 10080 [8] and UNE 36065 [29]) with  
113 12-mm of diameter were used for this study. The chemical composition of the bars was  
114 determined from X-ray fluorescence and combustion infrared detection of C and S,  
115 which can be seen in **Table 1**. The alloying content of these bars makes their carbon  
116 equivalent 0.45%—calculated using the expression previously given by other authors  
117 [9,30]-. The Cu content detected (higher than 0.2%) is enough to assume a slight  
118 corrosion inhibition effect, based on previous published studies [18].

119 The microstructure of cross-sectional views of the bars was observed in  
120 metallographically prepared samples etched using Nital (5% HNO<sub>3</sub> in ethanol).  
121 Microhardness Vickers HV0,1 (100 gf) profiles were carried out in the cross-sections of  
122 the bars. Measurements started about 50 μm from the ribbed surface of the bar and  
123 they were performed each 100 μm. For this study, a Zwick Roell Indentec machine was  
124 used. Localized hardness measurements complete the information about the  
125 microstructure of the bars and can inform about possible residual stresses. These are  
126 aspects that can affect the corrosion performance of different areas of the bar.

127 For the electrochemical corrosion tests carried out in solution, two types of  
128 samples were used: a) samples from the corrugated surface of the TMT bars, labelled  
129 as “Ribbed surface”; and b) samples machined from TMT bars where the martensite  
130 case had been fully removed, labelled as “Core”. The “Core” cylinders had a diameter  
131 of 9 mm. Both types of samples were cut into 3-cm long cylinders, as can be seen in

132 **Figure 1.** The surface of the “Ribbed surface” samples was mechanically cleaned  
133 before the tests to erase any oxide formed due to the atmospheric exposure of the as-  
134 received bars, using a Dremel Multipro tool. The mill-scale of the surface of the “Ribbed  
135 bars” was kept after this soft cleaning process. Before being immersed in the testing  
136 solution, a copper wire was glued to one of the cross-sections of each sample using  
137 silver paint. Then, both cross-sections were covered with epoxy coating to avoid their  
138 interference in the measurement results.

139 The testing solution used to simulate that contained inside the pores of a  
140 chloride contaminated concrete [19] was 0.1 M NaOH, 0.3 M KOH and 0.15 M NaCl.  
141 The pH of this solution was 13.2. Four different samples have been tested for each  
142 steel in each type of electrochemical measurement.

143 The galvanic current flowing between “Ribbed surface” and “Core” samples in  
144 this solution was measured using a 263A Potentiostat/Galvanostat from PAR. For this  
145 measurement, the ratio of the surfaces Ribbed surface/Core was 1.66.

146 Polarization curves and electrochemical impedance spectroscopy (EIS)  
147 measurements were carried out for the “Ribbed surface” and “Core” samples in the  
148 previously detailed solution. Moreover, these electrochemical tests were also  
149 performed in short-circuited samples of “Core” and “Ribbed surface” connected through  
150 a wire. This third type of samples will be called “Galvanic couple” hereafter. Those  
151 techniques have been used in the field for decades and allow to obtain a very sensitive,  
152 reliable information about the kinetics and mechanism of electrochemical processes.

153 A three-electrode cell was used in these studies. A saturated calomel electrode  
154 (SCE) was used as reference electrode, and an AISI 316 stainless steel coiled wire as  
155 counter electrode. The open circuit potential (OCP) of all the samples was allowed to  
156 stabilize for 45 min in the testing solution. Then, the non-destructive EIS tests were  
157 carried out at OCP and, finally, the polarization curves were performed. EIS  
158 measurements were carried out from 100 kHz to 10 mHz applying a sinusoidal  
159 perturbation of 10 mV<sub>rms</sub>. The polarization curves started at -200 mV from the  
160 previously determined OCP, and the potential was increased towards more anodic  
161 values at a rate of 0.5 mV/s. The Tafel slopes in the polarization curves were  
162 calculated from  $\pm 70$  mV vs.  $E_{\text{corr}}$  (corrosion potential) to higher overpotentials. Those  
163 electrochemical measurements were done using a Solartron Analytical  
164 Potentiostat/Galvanostat from Ametek. More information about the background of  
165 electrochemical tests can be found elsewhere [31,32]



166 With the aim of checking the results of electrochemical techniques, TMT steel  
167 reinforcements were extensively corroded in concrete. 50-cm long bars of the same  
168 ribbed TMT steel were used to perform corrosion studies in concrete slabs with 500 x  
169 265 x 100 mm dimensions. Six slabs were manufactured, embedding in each one 10  
170 steel bars with a 37-mm distance between each bar. The cement used was CEM II/B-L  
171 32.5 N, and the water/cement ratio was 0.45. The cement/sand/coarse aggregate  
172 ratios used were 1/2/3. A 3.3%  $\text{CaCl}_2$  regarding the weight of cement was also added  
173 to the mixture, as other authors have previously done to increase the chloride content  
174 in mortars and concretes [33]. The regions of the bars close to the concrete-air  
175 interface were protected with an isolating tape, with an approximately 25-cm length of  
176 the bar exposed to corrosion inside the concrete. In **Figure 2**, an image of one of the  
177 reinforced concrete slabs manufactured for performing the present research can be  
178 seen.

179 After casting, the 6 slabs were cured at high relative humidity and room  
180 temperature for 28 days, and then the corrosion of the rebar was accelerated by  
181 impressed currents. Bars embedded in the different slabs were submitted to  
182 accelerated corrosion for 6 different times (70, 120, 160, 220, 280 and 350 days) to  
183 achieve different levels of attack. The current density in each of the bars was initially 80  
184  $\mu\text{A}/\text{cm}^2$ . This corrosion density was about one order of magnitude higher than the  
185 corrosion rates determined for in-service structures exposed to chloride environments  
186 and high relative humidity [34]. The method was already used and described in  
187 previous studies [35,36]. As the slabs cracked extensively, especially for the longer  
188 tests, the used power sources were unable to keep this current densities. For the slabs  
189 corroded more than 160 days, the supplied currents decreases down to about 10  
190  $\mu\text{A}/\text{cm}^2$ . After the accelerated corrosion tests in concrete, the slabs were broken, and  
191 the oxides generated on the surface of the reinforcing bars were cleaned using a HCl  
192 solution inhibited with urotropine. The main pits in each bar were identified and their  
193 morphology was characterized by optoelectronic microscopy, with the measurements  
194 done using an Olympus DSX500. Optoelectronic microscopy is a technique that has  
195 recently been used to characterize the morphology of pits and evaluate its  
196 dangerousness in other materials [37]. Moreover, scanning electron microscopy (SEM)  
197 was used to check the relationship between pit depth and microstructure.

### 198 3. Results and discussion

#### 199 3.1. Electrochemical characterization in solution

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In **Figure 3**, optical microscopy images corresponding to etched cross-sections of the TMT bars can be observed. In **Figure 3a**, the outer case -with a clearly darker microstructure after the attack- can be easily distinguished from the inner region of the corrugated bar. In **Figure 3b**, obtained at higher magnifications, it can be checked that the inner core of the bar is formed by ferrite and perlite, as corresponds to a steel with a C content as that shown in **Table 1** and which has been cooled from the austenitic state at a slow enough cooling rate. **Figure 3c** shows the transition region between the core and the outer case. The thickness of the transition interlayer seems to be much reduced, which suggests that the quenching procedure to form the outer layer has been carried out adequately [9]. The presence of bainite in this interlayer has been often mentioned in previous literature [13], but, for the studied bars, it is difficult to assure with reliability the presence of this phase. Moreover, other authors have neither found noticeable bainite in the microstructure of the bars nor have predicted its presence by the modeling of the TMT process [11]. The microstructure observed in the transition zone is compatible with ferritic and perlitic phases, which close to the martensite case would become finer -with a smaller grain size- than in the bulk of the bar (**Figure 3b**). In **Figure 3d**, the typical microstructure of martensite, obtained by the quenching and tempering of the surface during bar manufacture, can be observed.

There exists a clear relationship between microstructure, stresses and micromechanical properties. As the corrosion behavior of the bars can be very dependent on microstructure and stresses, a micromechanical study has been carried out. Some representative microhardness profiles obtained measuring from the surface of the bars towards regions where the micromechanical properties become stable can be seen in **Figure 4**. These results show a plateau with the highest hardness for regions close to the surface, proving the improvement in this property caused by the formation of martensite (**Figure 3d**). The thickness of this high hardness region depends on the exposure time to the water cooling during the martensite formation and on the cooling-water flow rate [11]. The length of the highest hardness plateau slightly oscillates (**Figure 4**). This result is coherent with the slight dispersion in the thickness of the outer martensite case observed in different sections of the bars and that can be guessed in images as that shown in **Figure 3a**. This lack of uniformity for the outer case could be related to the dispersion in the prior austenite grain sizes in the red heated steel during the bar processing [11]. Moreover, if the microhardness profiles start from a rib of the surface, the highest hardness plateau is defined at slightly higher values, probably because the faster cooling rate of this particular region causes the

235 formation of a finer grain martensite. The decrease in hardness after the plateau is very  
236 steep, which corresponds to the observations in **Figure 3c**.

237 There is also another plateau for the lowest measured hardness (**Figure 4**).  
238 The microhardness values can be considered completely stable from a surface  
239 distance higher than about 2.2 mm, if the profiles start from a point between ribs.  
240 Obviously, this stabilization distance is much higher if the measurement starts in a rib.  
241 Between this plateau of complete stabilization and the decrease in hardness  
242 corresponding to the transition zone, a region of hardness slightly higher than that of  
243 the plateau can be observed. This region with slightly higher hardness can be identified  
244 with finer perlite and ferrite than in the bulk material observed close to the martensite  
245 (**Figure 3**).

246 In chloride-containing solutions that, because of their pH, simulate those  
247 contained inside the concrete pores, there is a galvanic current density flowing  
248 between samples from the “Ribbed surface” and from the “Core” of the bars -as those  
249 shown in **Figure 1**- when they are short-circuited. The sign of the measured current  
250 always shows that the martensite from the surface of the ribbed bars acts as anode  
251 against the material in the core. Time records with oscillations and small transitories, as  
252 those shown in **Figure 5**, can be seen in this kind of experiments. To calculate the  
253 galvanic current density ( $i_{galv}$ ), the surface of the anodic samples -that is to say, the  
254 area of the “Ribbed surface” samples- has been used. The mean values of  $i_{galv}$   
255 determined from the different current distributions registered in the different  
256 experiments performed always ranged between 0.7 and 1.0  $\mu A/cm^2$ . These results are  
257 coherent with the preferential corrosion of the martensite case of TMT rebars in  
258 chloride contaminated concrete reported in other works [35,36].

259 Polarization curves have been performed in simulated pore solution to obtain  
260 information about the relative corrosion rate of the different microstructures and how  
261 their short-circuiting can affect it. Moreover, a careful analysis of these curves can also  
262 give relevant information about the process determining the corrosion kinetics.  
263 Examples of the polarization curves obtained for “Ribbed surface” and “Core” samples  
264 can be seen in **Figure 6**. Moreover, an example of one of the curves obtained for  
265 “Galvanic couple” samples has also been included in the figure. All the curves are quite  
266 similar, and they can be considered typical for systems that corrode actively at  
267 moderate rates.

268 During the anodic polarization, the Tafel behavior (that is to say, the charge  
269 transfer control of the process) is found in the narrow range where a linear relationship  
270 among the potential and logarithm of the anodic current density is linear. For the  
271 studied systems, this occurs up to overpotentials of 120 mV or somewhat higher. At  
272 higher anodic overpotentials, the current almost slows down and its increase diverts  
273 from the Tafel behavior. This indicates the influence of another phenomenon different  
274 from the charge transfer in the anodic semireaction. The cathodic branches of the  
275 curves always shown a typical Tafel behavior that can be seen from potentials about  
276 25 mV higher than the onset of the curves to about 70 mV vs.  $E_{\text{corr}}$ .

277 In **Figure 7**, the most relevant data that can be calculated from curves as those  
278 shown in **Figure 6** are plotted. The average values as well as the standard deviations  
279 of the experimental data obtained have been plotted. In **Figure 7a**, it can be seen that  
280 the  $E_{\text{corr}}$  determined for the different types of samples are typical of active steel  
281 following the probabilistic criterion proposed by the ASTM C876 standard [38]. For the  
282 solution used in the present study, the traditional  $[\text{Cl}^-]/[\text{OH}^-]$  ratio employed to calculate  
283 the critical chloride and the depassivation of the steel has a value of 0.375. Previous  
284 published studies show a huge dispersion in this value, depending on the testing  
285 conditions and the method used to detect the depassivation [39]. In tests carried out in  
286 simulated pore solution using electrochemical techniques, a value of 0.35 has been  
287 determined as critical [40], so the testing solution used in the present research is  
288 somewhat above it. The more innovative  $[\text{Cl}^-]/[\text{OH}^-]^3$  ratio with a critical value fixed at  
289 1.25 has recently been proposed as more reliable [41]. This value has been  
290 determined in chloride solutions with different NaOH concentrations and  
291 electrochemical techniques. The simulated pore solution used in the present research  
292 has a  $[\text{Cl}^-]/[\text{OH}^-]^3$  ratio of 2.3, so it is logical that the bars corrode actively. There is some  
293 dispersion for measured  $E_{\text{corr}}$  values for the same type of samples. Bearing in mind the  
294 overlapping of the error bars, it could be concluded that the  $E_{\text{corr}}$  of the three studied  
295 types of samples are similar from a statistical point of view.

296 The corrosion current densities ( $i_{\text{corr}}$ ) are also very similar for the three types of  
297 samples (**Figure 7a**). All the measured  $i_{\text{corr}}$  are about one order of magnitude higher  
298 than  $0.1 \mu\text{A}/\text{cm}^2$ , which is usually assumed to be a limit value for determining the onset  
299 of corrosion of carbon steel reinforcements [42]. The average value for the “Ribbed  
300 surface” is higher than for the “Core” (**Figure 7a**).

301 The most relevant information that can be drawn from the obtained polarization  
302 curves are the Tafel slopes. In **Figure 7b**, it can be seen that, for the three systems,

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303 the anodic Tafel slopes ( $b_a$ ) are always higher than the cathodic Tafel slopes ( $b_c$ ). This  
304 fact means that the anodic process is the most hindered, and the  $i_{corr}$  is more controlled  
305 by anodic semireaction than by the cathodic one. At any rate, as the difference  
306 between  $b_a$  and  $b_c$  is not huge, a mixed control of the corrosion rate must be assumed,  
307 with a lower influence of the cathodic process.  $b_a$  is clearly higher for the “Core” than  
308 for other samples. This indicates that the anodic process is less favored in the ferrite  
309 and perlite than in the martensite. The  $b_a$  values allow to explain the  $i_{galv}$  observed  
310 (**Figure 5**) and the preferential corrosion of the martensite. On the other hand,  $b_c$   
311 values are quite similar for all the studied systems, which implies that the oxygen  
312 reduction, that is the cathodic process in this medium, is not clearly easier on the  
313 microstructure of one surface than on the other. So, the cathodic reaction is not more  
314 favored on the ferrite-perlite than on the martensite. The  $i_{galv}$  observed in experiments  
315 such as that in **Figure 5** can only be justified by the higher trend of the martensite to  
316 locate the anodic reaction, while the cathodic process is not preferentially located  
317 neither on the outer martensite nor in “Core” material.

318 Hence, a galvanic couple is formed between martensite and ferrite, but its  
319 performance does not coincide with that of the most well-known galvanic couples,  
320 which are formed by metals with very different  $E_{corr}$ . In the case under study, the anodic  
321 process is mainly located in the martensite, but the cathodic process is not specially  
322 favored on any of the surfaces (as their  $b_c$  are very similar). For this reason, it is  
323 necessary to use only the surface of the martensite in the “Galvanic couple” samples to  
324 obtain reliable corrosion rates for the electrochemical tests. If the  $i_{corr}$  for the “Galvanic  
325 couple” in **Figure 7a** is re-calculated using only the surface of the martensite instead of  
326 the surface of both short-circuited samples, the average  $i_{corr}$  value increases up to a  
327 value similar to that of the “Ribbed surface”.

328 On the other hand, the highest  $E_{corr}$  observed for the “Galvanic couple” must  
329 correspond to an increase in the cathodic area in these samples. The ferrite-perlite acts  
330 preferentially as a cathode, while the martensite also keeps cathodic activity besides  
331 locating preferentially the anodes. A higher cathodic area shifts the cathodic process to  
332 higher current intensities, and then the current balance between the anodic and the  
333 cathodic semireactions appears at higher potentials (higher  $E_{corr}$ ).

334 These results informs than, when the pits go deep down to the core of the bar,  
335 a galvanic couple is formed between the martensite and the ferrite-perlite, being this  
336 last type of microstructure cathodically protected. So, once the corrosion has reached

337 the core of the bars, the attack should tend to develop preferentially through the  
338 martensite.

339 However, it could be assumed that the cathodic protection of the ferrite-perlite  
340 would increase the corrosion rate of the martensite, but, in fact, it does not seem  
341 feasible. Due to the steep anodic branch observed in the polarization curve for the  
342 “Ribbed samples” (**Figure 6**) and the small increase in the  $E_{corr}$  that takes place due to  
343 formation of “Galvanic couple”, the foreseeable increase in the  $i_{corr}$  for the “Galvanic  
344 couple” is lower than the experimental dispersion determined for this parameter for the  
345 corroding systems studied. Thus, short-circuiting ferrite-perlite with martensite would  
346 not meaningfully increase the corrosion rate of the martensite in spite of the formed  
347 galvanic couple. In addition, it should be borne in mind that, when the short-circuiting  
348 takes place between the material of the core and that of the case because of a pit, the  
349 ratio anodic area/cathodic area is high, so the ability of the ferrite-perlite phase to  
350 increase the corrosion rate of the martensite will become quite reduced. Hence, the  
351 microstructure of TMT bars seems adequate to limit the development of very specially  
352 dangerous forms of corrosion. Anyway, it cannot be forgotten that inside the pits many  
353 chemical changes takes place (acid hydrolysis of the corrosion products, decrease on  
354 the oxygen amount, cells of ionic concentrations, etc.) that affect the eventual kinetic of  
355 the process [16], making the real development of the attack in structures a very  
356 complex process, dependent of many environmental factors.

357 With the aim of obtaining more information about the corrosion mechanism and  
358 the influence of the bar microstructure on it, EIS studies have been carried out.  
359 Examples of the EIS spectra obtained for the “Ribbed surface”, “Core” and “Galvanic  
360 couple” samples are shown, as Bode and Nyquist diagrams, in **Figure 8**. To obtain an  
361 adequate simulation of spectra like these, a circuit equivalent as that proposed in  
362 **Figure 9** has been necessary. In this circuit,  $R_{sol}$  is the solution resistance between the  
363 counter electrode and the working electrode, and its influence can be seen at the  
364 highest frequencies. The electric behavior of the passive layer is simulated by the  $R_{pas}$   
365 and  $CPE_{pas}$ . Identification of the influence of the passive layer with the time constant  
366 that appears in the spectra at medium-high frequencies is commonly found in previous  
367 literature [43,44].  $R_{pas}$  simulates the electrical resistance of the passive layer and  
368  $CPE_{pas}$  simulates its non-ideal capacitive behavior. The simulation fixes the  $CPE_{pas}$   
369 impedance using two values: the  $C_{pas}$ , which is the capacitance determined for the  
370 passive layer and  $n_{pas}$  that is an empirical coefficient whose values can range between  
371 0 and 1, being 1 when the behavior is ideal. The corrosion activity is identified with the  
372 phenomena which appear in the spectra at lower frequencies. The process is simulated

373 with elements that correspond to the charge transfer resistance inside the pits,  $R_{pit}$ , and  
374 the capacitive behavior of the double layer inside the pits,  $CPE_{pit}$ . The  $CPE_{pit}$  is a  
375 constant phase element whose electrical performance is simulated using  $C_{pit}$  and  $n_{pit}$ .  
376 Moreover, to obtain a good simulation of the experimental data at the lowest  
377 frequencies, it is necessary to include a Warburg element related to the diffusion  
378 impedance through a finite thickness ( $W_s$ ). The  $W_s$  impedance is simulated using three  
379 parameters,  $W_s$ -R,  $W_s$ -P and  $W_s$ -T.  $W_s$ -R can be identified with the resistance  
380 associated to the process,  $W_s$ -P is a coefficient whose value is 0.5 for ideal process,  
381 but can be lower for real processes, and  $W_s$ -T is the ratio between the square of the  
382 effective diffusion thickness and the diffusion coefficient of the specie. The equivalent  
383 circuit used to simulate the results is similar to the one already used to simulate the  
384 electrochemical behavior of corroding steel in concrete [43,45].

385 In steel embedded in chloride contaminated concrete, a diffusion impedance  
386 through a semi-infinite thickness is often identified at low frequencies. It has been  
387 assumed that this impedance reflects the influence that the diffusion impedance of  
388 oxygen through the concrete cover can have on the corrosion process. In solution tests  
389 such as those performed in this study, the access of oxygen to the rebar surface is  
390 higher and this hypothesis could be discarded, at least at moderate  $i_{corr}$  (**Figure 7a**).  
391 The diffusion of ions through the oxide layer has also been previously proposed as  
392 being responsible for the presence of diffusion impedance at the lowest-frequency part  
393 of the spectra in simulated pore solutions [41] and in concrete [44]. Hence, the  $W_s$   
394 impedance could correspond to the diffusion through surface oxides. The polarization  
395 results (**Figure 6**) are coherent with this hypothesis, because of the region defined at  
396 anodic overvoltages and high current densities where the  $i$  hardly increases its values  
397 when  $E$  increases, and that can easily be identified with a current diffusion limit (related  
398 to  $W_s$ -R) and somewhat higher than  $i_{corr}$ .

399 Due to their higher order of magnitude, the parameters that have the most  
400 determining effect on the corrosion rate are  $R_{pit}$  and  $W_s$ -R, which have been highlighted  
401 in bold in **Table 2**. For all the studied systems,  $R_{pit}$  is higher than  $W_s$ -R, so the charge  
402 transfer resistance inside the pits can be identified as the rate determining step.  
403 However, the difference between  $R_{pit}$  and  $W_s$ -R is so small that it would be a sizeable  
404 mistake to omit the influence of the ions diffusion through the oxide. The global  
405 impedance of the process at low-frequencies (essentially  $R_{pit}+W_s$ -R) shows values for  
406 "Ribbed surface" that are half of those obtained for the "Core", matching the trend  
407 obtained for the  $i_{corr}$  (**Figure 7a**).

408 3.2. Study of the bars corroded in concrete

1  
2 409 The influence of the microstructure on the development of the pits has been  
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4 410 checked carrying out accelerated tests in concrete. The long-term, aggressive tests  
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6 411 carried out pretended to cause corrosive attacks that reach the ferrite-perlite core of the  
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8 412 bars. In **Table 3**, information regarding the development of the corrosion process in the  
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10 413 reinforcements and the size of the cracks can be seen. The supplied charge increases  
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12 414 in a non-linear way with the length of the tests, as this parameter is affected by the  
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14 415 onset and development of cracks in the concrete. Cracks suppose a clear obstacle for  
15  
16 416 the current flow between the steel bars and the cathode. Thus, the current density that  
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18 417 flows through extensively cracked slabs (at the end of the longest tests) is always lower  
19  
20 418 than that initially applied. The corrosion rates have been calculated from the mass  
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22 419 losses determined after the tests. It can also be seen that, though the mass losses of  
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24 420 the bars increase with the length of the test, the corrosion rates decrease. This can be  
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26 421 easily related to the decrease on the current that flows after concrete cracking.

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28 422 The minimum values for current efficiencies (**Table 3**) have been calculated  
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30 423 assuming that the Fe is always oxidized to FeO. The highest values calculated for  
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32 424 efficiency range of each slab corresponds to the theoretical assumption that all the Fe  
33  
34 425 is oxidized to Fe(III). The additional formation of compounds more oxidized than FeO,  
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36 426 as Fe<sub>2</sub>O<sub>3</sub> or Fe<sub>3</sub>O<sub>4</sub>, cannot be discarded, especially when the steels are exposed to the  
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38 427 air through the cracks. Anyhow, the use of part of the current for other electrochemical  
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40 428 reactions, as water evolution, can also be considered, and these phenomena would  
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42 429 affect the efficiency too.

43  
44 430 Macroscopic images of the corrosion that has taken place in the slabs, after the  
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46 431 oxides have been removed, are shown in **Figure 10**. It can be seen that big pits tend to  
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48 432 develop in the corrugated surface of the bars. The SEM images in **Figure 11**,  
49  
50 433 corresponding to one of the pits, allow to verify that the attack tends to initially develop  
51  
52 434 through the martensite, forming a slightly jagged surface on this phase due to the  
53  
54 435 attack (**Figure 11a**). When the corrosion reaches the thin interlayer formed between  
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56 436 the martensite and the ferritic and perlitic region, the deepening of the attack seems  
57  
58 437 restrained and the bottom of the pit becomes smother (**Figure 11b**).

59  
60 438 To perform a more exhaustive study regarding the pit morphology of TMT bars  
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62 439 in chloride contaminated concrete, the depth and surface area of the main pits detected  
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64 440 in corroded reinforcing TMT steel have been measured using optoelectronic  
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66 441 microscopy. Images such as that shown in **Figure 12** are obtained for the main pits  
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68 442 formed in the bars. The mass loss of each studied pit plotted in **Figures 13** and **14** has



443 been calculated from the volume of the pit given by its optoelectronic characterization  
444 and using the density of the steel. Numerous pits whose mass losses differ more than  
445 two orders of magnitude –in grams- have been considered for this study.

446 In **Figure 13**, it can be seen that the increase in volume of the pits is clearly  
447 associated to an increase in the area of the pits mouths. Pits whose areas vary more  
448 than two orders of magnitude –in mm<sup>2</sup>- have been detected. The pits with the highest  
449 individual mass losses and with the highest mouth areas appear in bars embedded in  
450 the slabs that have been corroded for the longest times.

451 At any rate, the results in **Figure 14** prove that the pits associated to the lowest  
452 mass losses tend to have maximum depths lower than that of the martensitic case,  
453 confirming the observation carried out for images like that in **Figure 11a**.

454 The obtained results suggest that the attack initially takes place in the  
455 martensitic case and that, when the corrosion reaches the martensite-ferrite interlayer,  
456 the pits tend to continue their growth by mouth widening through the martensitic case.  
457 Only when the pits become very big, can this trend disappear, due to loss of galvanic  
458 effect that would cause the increase of the ohmic drop between preferential anode or  
459 cathodes. Obviously, if the ionic electrolyte disappears between the different  
460 microstructures by concrete cracking, the galvanic effect on the corrosion would also  
461 disappear.

462 In **Figure 14**, the relationship between the volume/mass loss of each  
463 characterized pit and its maximum depth is plotted. The pit depth is a parameter that,  
464 for the pits most easily detectable by visual inspection, varies slightly. All the obtained  
465 values from the pit depth differ in less than one order of magnitude, though the volume  
466 of the pits is quite different. Moreover, most of the determined maximum pit depths are  
467 between 1-2 mm. If it is born in mind that the software always takes into account the  
468 maximum height appearing in the image as a reference for calculating the depth of the  
469 pits, and that the height of ribs and nerves often influence this value, it is obvious that  
470 the calculated maximum pit depth matches the thickness where the typical  
471 microstructure of the core appears (**Figure 3**) and the lowest hardness plateau onsets  
472 (**Figure 4**). Thus, these data confirm observations as those in **Figure 11b**, which  
473 suggest that the attack tends to be stopped in the transition interlayer. The fact that  
474 sometimes values for the pit depth slightly higher than the typical values obtained for  
475 the martensitic case of the studied TMT steel have been obtained with this technique  
476 could suggest that, for the biggest pits, the cathodic protection that the martensite  
477 offers to the ferrite and perlite would disappear. This can be due to the ohmic drop that

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478 should appear between the bottom of the pit and the outer surface for the biggest pits.  
479 Moreover, the progress of the pits could also be affected by the concrete cracking  
480 (**Table 3**) that, for the longest tests, may expose directly part of the reinforcing steel to  
481 the atmosphere

482 The results obtained in the laboratory, from solution tests where TMT bars  
483 corrode at moderate corrosion rate, match with those obtained from tests in concrete  
484 where TMT bars corrode at very high corrosion rate. However, the morphology of the  
485 pits in the accelerated tests in concrete can be affected by factors such as the high  
486 anodic polarizations under the attack has been developed. Hence, it would be  
487 interesting to check these results with an additional study of the pitting morphologies  
488 that can appear in TMT bars real structures in different in-service aggressive exposure.

#### 489 **4. Conclusions**

490 The results obtained in this study reveal how the microstructure characteristic of  
491 TMT affects the development of the pits in concrete or simulated pore solutions with  
492 chlorides. The main conclusions that can be drawn the results obtained are:

- 493 • The  $i_{\text{corr}}$  of the martensite is slightly higher than that of the ferrite-perlite in  
494 solution tests and their  $E_{\text{corr}}$  are similar.
- 495 • The galvanic coupling between the martensite and the ferrite-perlite in solution  
496 tests proves that the martensite tends to act as anode and the ferrite-perlite as  
497 cathode.
- 498 • The anodic semireaction of the martensite is more hindered than the cathodic  
499 one in the testing solution, so a small increase in the cathodic surface that a pit  
500 reaching to the core would imply, does not cause a meaningful increase in the  
501 corrosion rate of the outer case.
- 502 • The EIS results obtained in solution inform that the charge transfer inside the  
503 pores is the most determining phenomenon for the corrosion rate, but there  
504 exists a mixed control. The influence of the diffusion impedance through the  
505 oxide layer should also be considered.
- 506 • Results obtained in concrete prove that the depth of the attack is determined by  
507 the microstructure of the TMT bars. Once the corrosion has reached the ferritic-

508 perlitic core, the attack tends to progress mainly by pit widening until the volume  
509 of the pit is very large and/or the concrete cover cracks.

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TABLES

**Table 1.** Chemical composition of the studied B-500-SD bars.

Chemical composition (%)						
C	Mn	S	Si	Cu	Ni	Fe
0.21	0.86	0.02	0.29	0.34	0.09	Balance
			0.02			<0.001
						V
						Mo
						0.02
						0.001
						Balance

**Table 2.** Results obtained from the simulation of the EIS spectra obtained in simulated pore solution.

	$R_{sol}$ ( $\Omega \cdot cm^2$ )	$R_{pas}$ ( $\Omega \cdot cm^2$ )	$C_{pas}^{pas}$ ( $\mu F \cdot cm^{-2} \cdot s^{-n-1}$ )	$n_{pas}$	$R_{pit}$ ( $k\Omega \cdot cm^2$ )	$C_{pit}^{pit}$ ( $\mu F \cdot cm^{-2} \cdot s^{-n-1}$ )	$n_{dl}$	$Ws-R$ ( $k\Omega \cdot cm^2$ )	$Ws-T$ (s)	$Ws-P$
<b>Ribbed surface</b>	$7.1 \pm 0.5$	$13 \pm 5$	$78 \pm 24$	$0.81 \pm 0.03$	$5 \pm 2$	$151 \pm 56$	$0.77 \pm 0.01$	$4 \pm 1$	$85 \pm 7$	$0.50 \pm 0.01$
<b>Core</b>	$6.7 \pm 0.4$	$13 \pm 1$	$32 \pm 5$	$0.89 \pm 0.04$	$13 \pm 5$	$48 \pm 5$	$0.87 \pm 0.03$	$7 \pm 1$	$9 \pm 5$	$0.43 \pm 0.03$
<b>Galvanic couple</b>	$7.6 \pm 0.5$	$14 \pm 2$	$7 \pm 2$	$0.80 \pm 0.01$	$11 \pm 1$	$100 \pm 5$	$0.78 \pm 0.01$	$7 \pm 2$	$19 \pm 4$	$0.50 \pm 0.01$

**Table 3.** Results of the reinforced concrete slabs submitted to accelerated corrosion.

	Accelerated corrosion time	Mass loss of the bars (%)	Corrosion rate of the bars ( $mg \cdot cm^{-2} \cdot day^{-1}$ )	Number of cracks	Maximum crack width range (mm)	Supplied charge ( $kC \cdot cm^{-2}$ )	Current efficiency (%)
<b>Slab 1</b>	70 days	$5.6 \pm 0.7$	$1.7 \pm 0.2$	3	0.2-0.6	4.8	88 - 132
<b>Slab 2</b>	120 days	$8.2 \pm 0.8$	$1.5 \pm 0.1$	5	0.3-1.1	8.2	74 - 111
<b>Slab 3</b>	160 days	$9.5 \pm 1.0$	$1.3 \pm 0.1$	3	1.0-1.4	9.8	73 - 109
<b>Slab 4</b>	220 days	$10.7 \pm 1.6$	$1.0 \pm 0.2$	4	1.7-3.0	12.3	65 - 97
<b>Slab 5</b>	280 days	$10.9 \pm 1.8$	$0.8 \pm 0.2$	6	0.6-5.0	9.8	84 - 126
<b>Slab 6</b>	350 days	$11.4 \pm 1.0$	$0.7 \pm 0.1$	7	2.0-6.0	11.4	76 - 114

## Figure legends

**Figure 1.** Image of the samples used for the electrochemical studies in simulated pore solution.

**Figure 2.** Image of one of the reinforced slabs that has been submitted to accelerated corrosion

**Figure 3.** Cross sectional images of the TMT reinforcing bar: a) whole cross-sectional view; b) microstructure of the core of the bar; c) microstructure of the transition region; d) microstructure of the outer region of the bar.

**Figure 4.** Microhardness profiles carried out on cross sections of the bars.

**Figure 5** Example of one of the registered time records corresponding to the  $i_{galv}$  flowing between samples of corrugated surface of the bars and samples from the core of the bars, when they are short-circuited and immersed in simulated pore solution.

**Figure 6.** Examples of polarization curves in simulated pore solution.

**Figure 7.** Results obtained from polarization curves as those shown in Figure 6: a) values corresponding to the  $i_{corr}$  and the  $E_{corr}$  of the studied samples; b) Tafel slopes calculated for the studied systems.

**Figure 8.** Examples of the EIS spectra obtained in simulated pore solution and plotted using a) Bode; and b) Nyquist diagrams.

**Figure 9.** Equivalent circuit used to simulate the obtained EIS spectra.

**Figure 10.** Macroscopic images of the bars corroded inside the concrete slabs after the acid etching cleaning: a) examples of the attack in some of the bars corroded for 220 days; b) big pits formed in the surface of one the bars corroded for 280 days.

**Figure 11.** Cross sectional views of pits generated in bars embedded in a chloride contaminated concrete slab. a) Pit with a moderate depth; b) Deep pit.

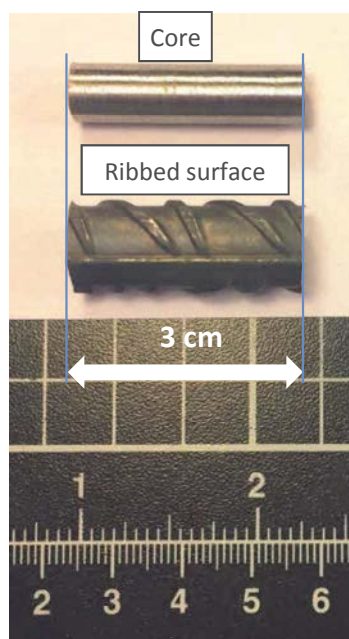
**Figure 12.** Example of the optoelectronic microscopy image for pit generated in a chloride contaminated concrete slab.

**Figure 13.** Relationship between the mass loss of each pit and its mouth surface. Results obtained from the optoelectronic characterization of the main pits formed on the six different studied chloride contaminated concrete slabs.

**Figure 14.** Relationship between the mass loss of each pit and its maximum depth. Results obtained from the optoelectronic characterization of the main pits formed on the six different studied chloride contaminated concrete slabs.



Figure 1



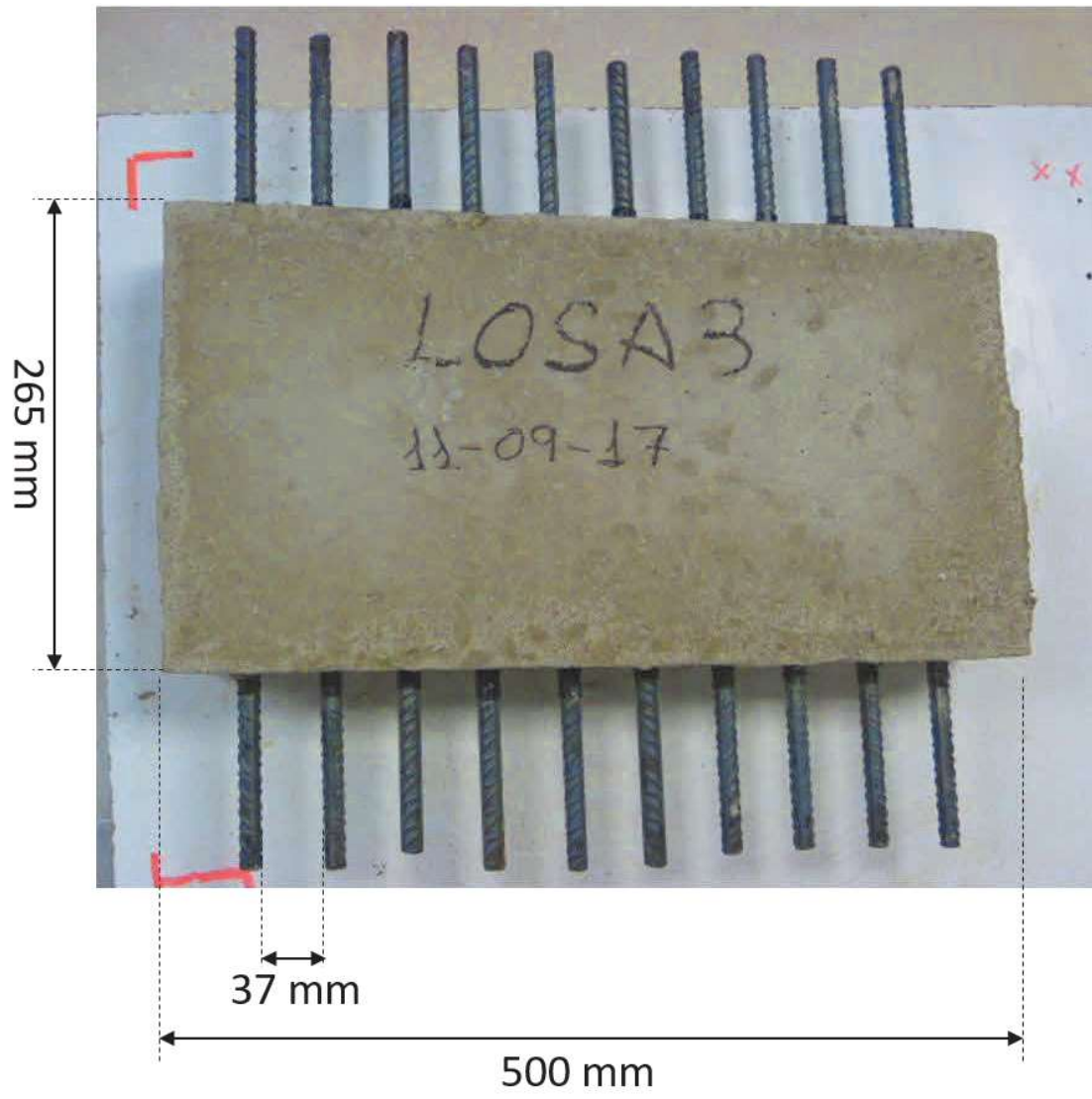


Figure 2

Figure 3

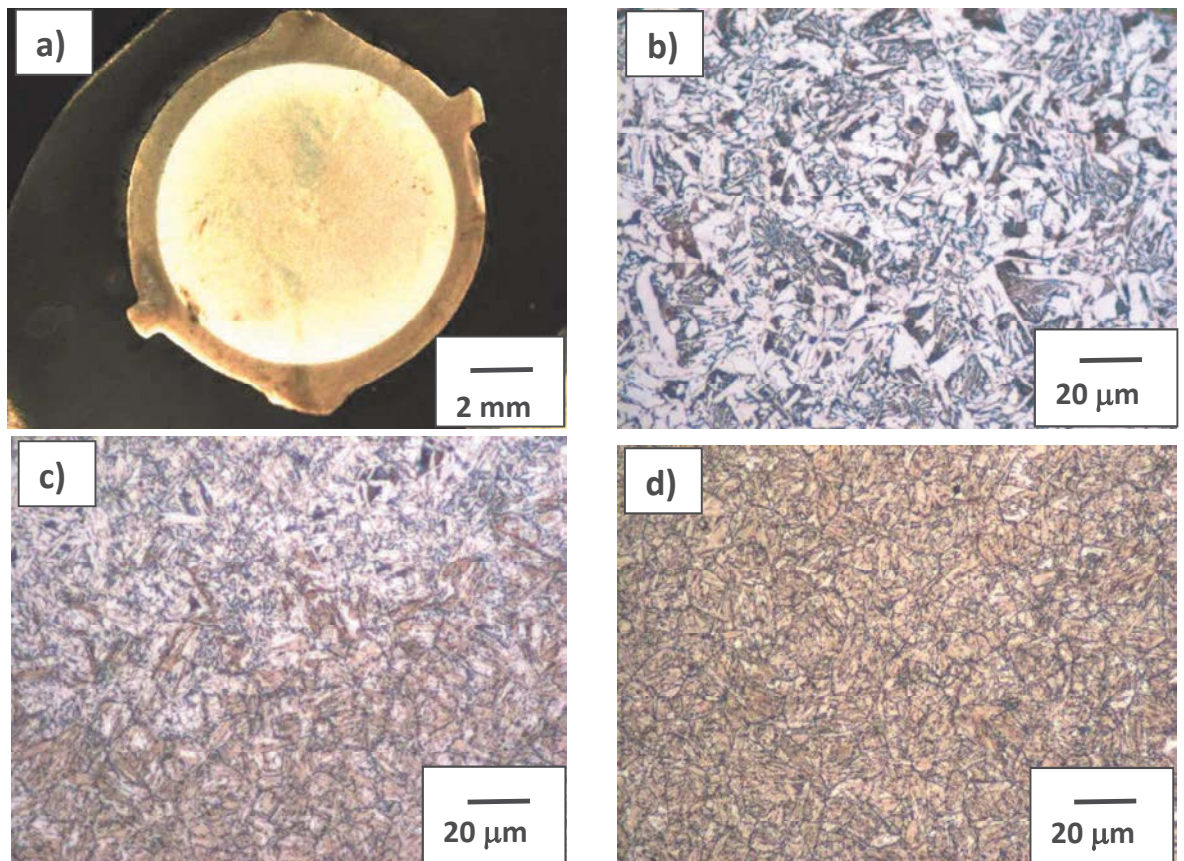


Figure 4

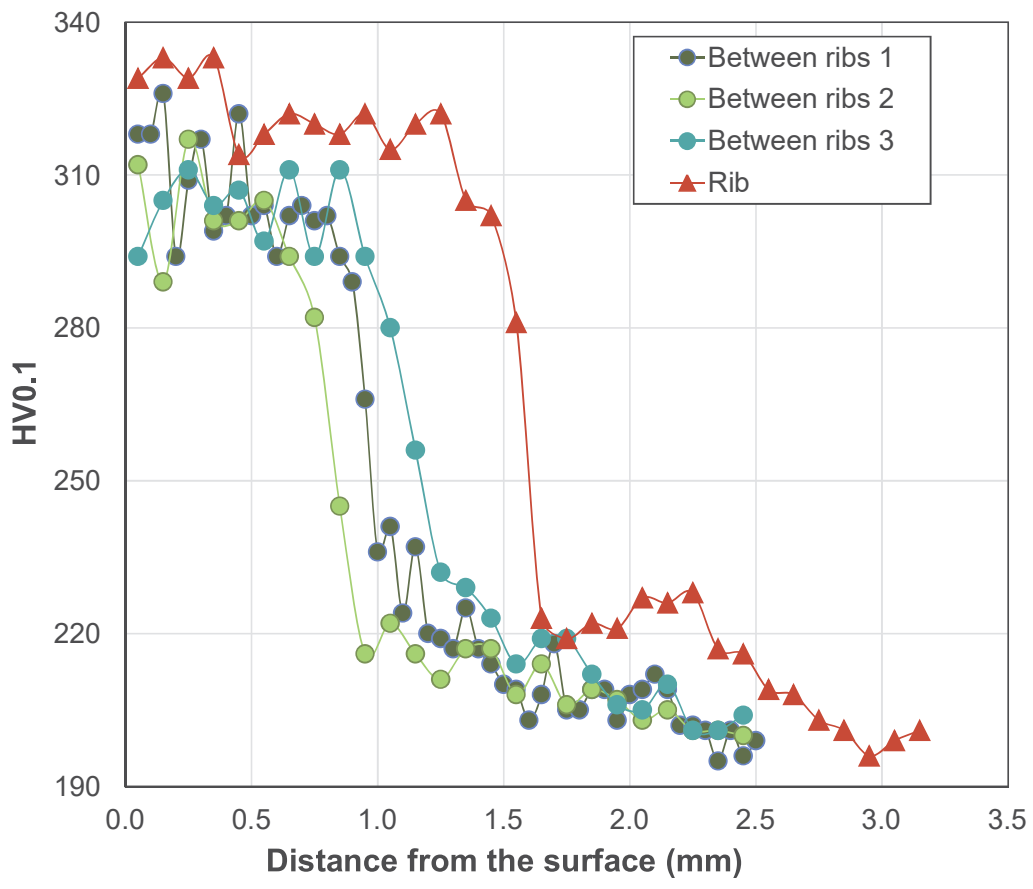


Figure 5

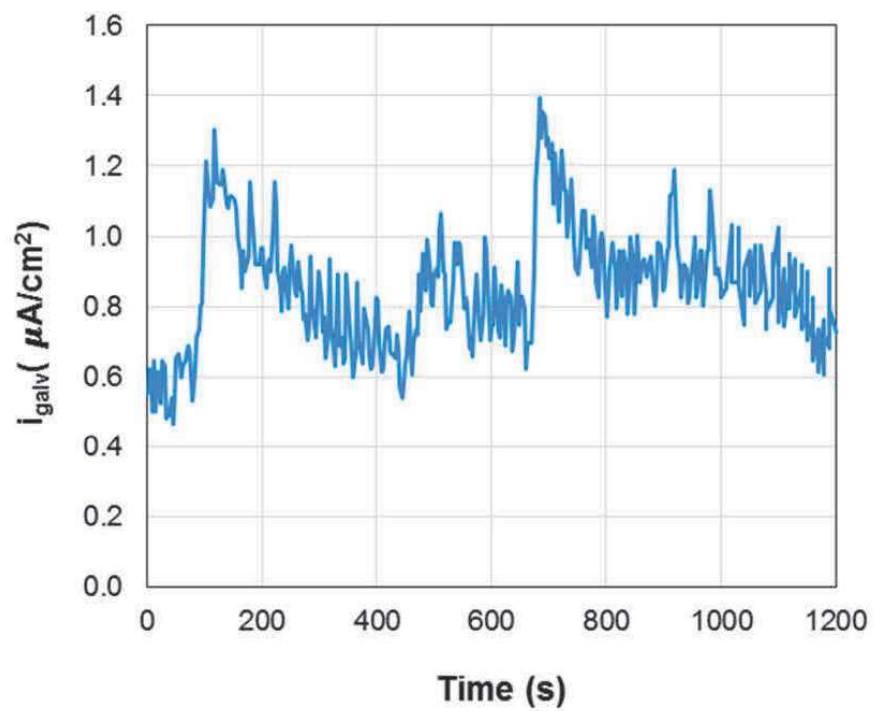


Figure 6

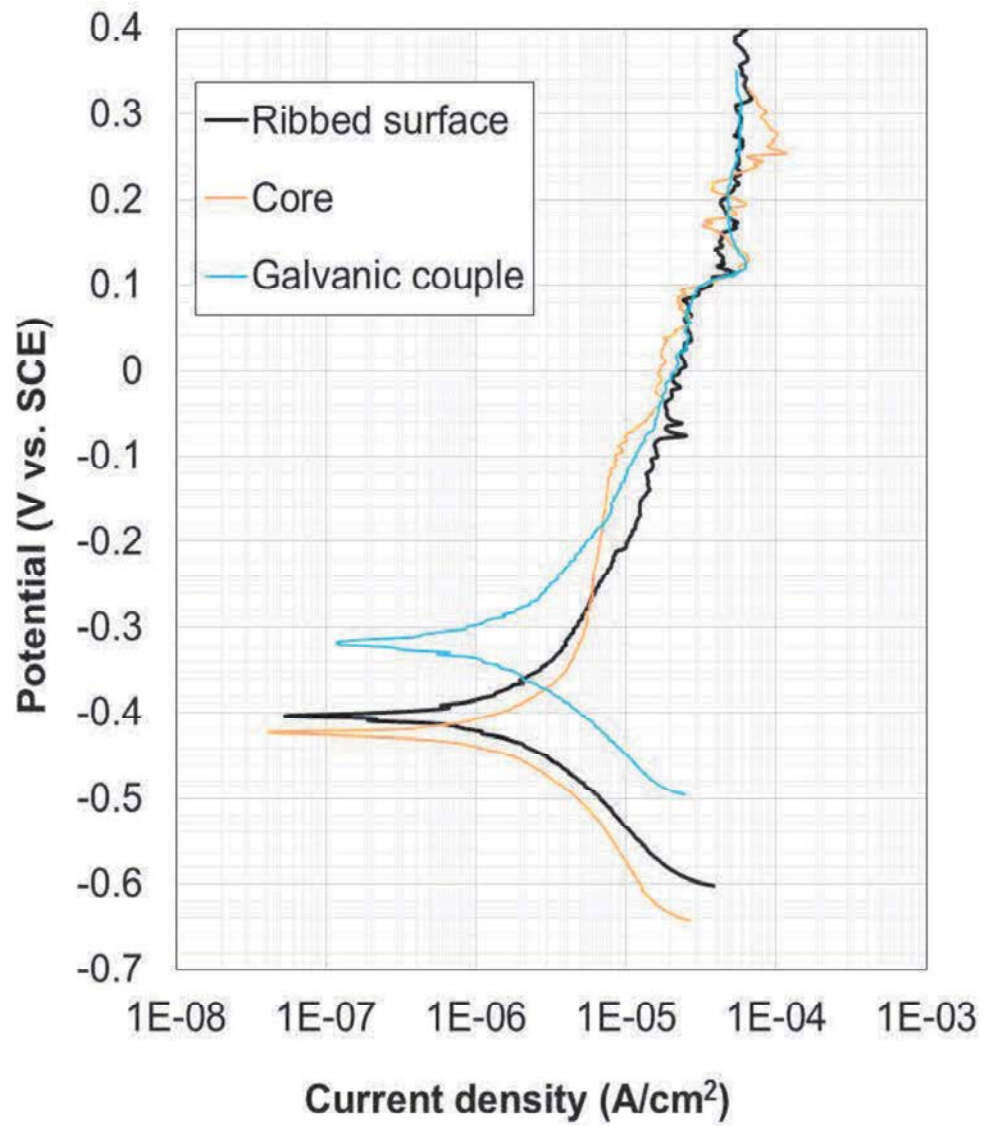


Figure 7

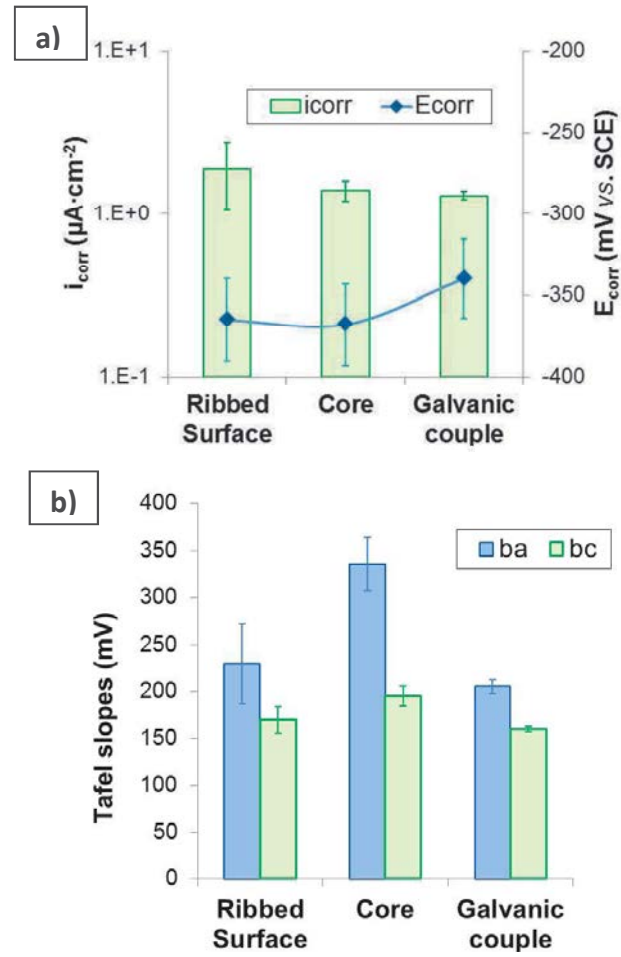


Figure 8

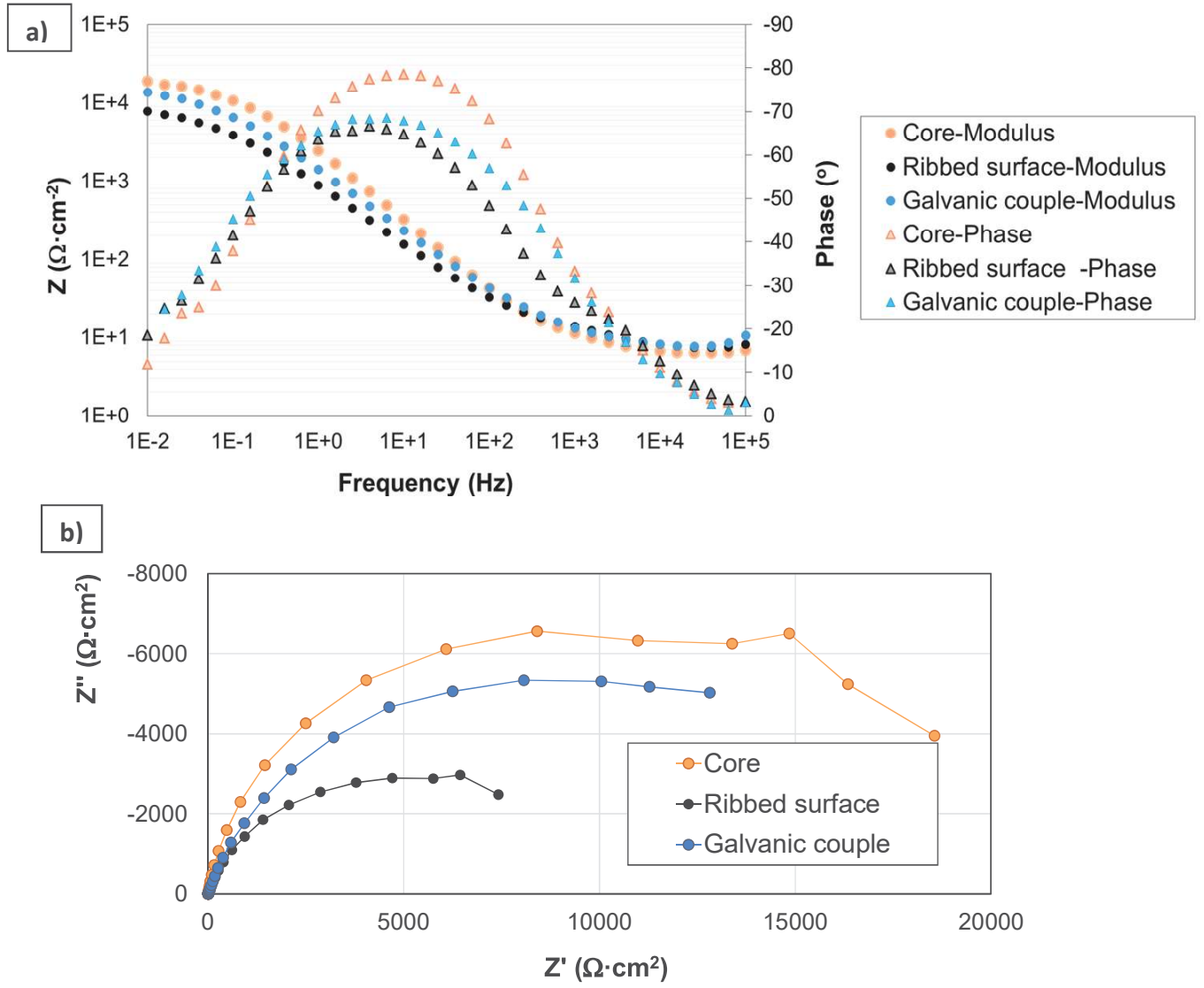




Figure 9

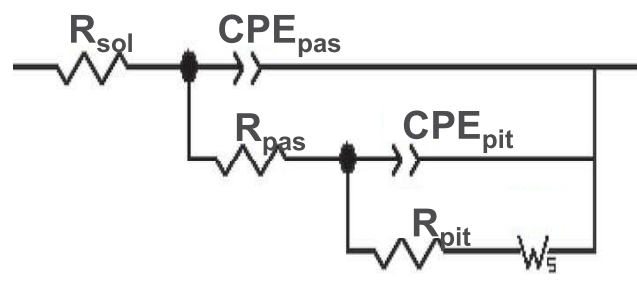


Figure 10

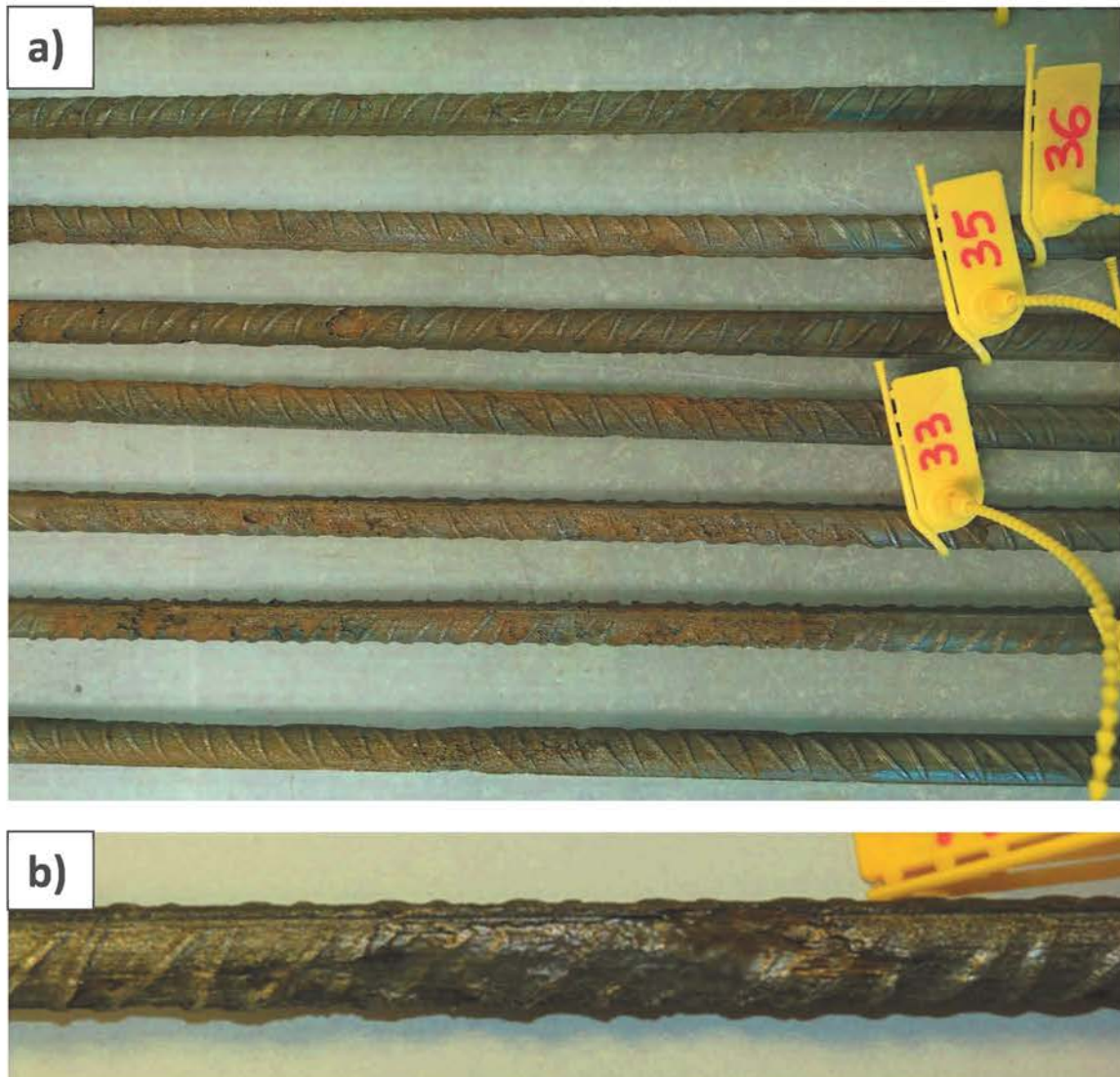


Figure 11

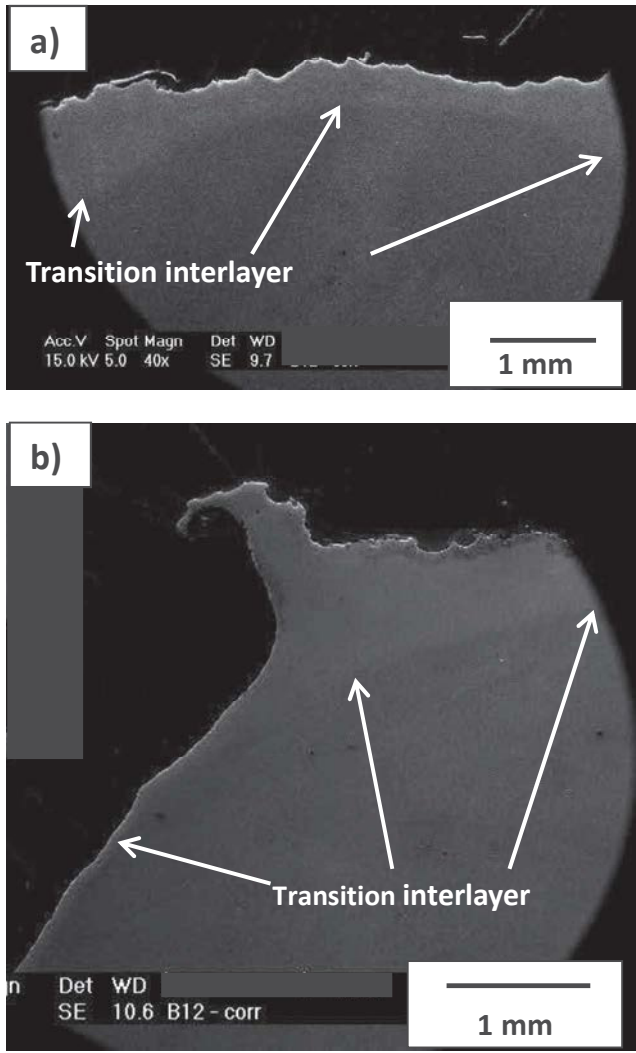


Figure 12

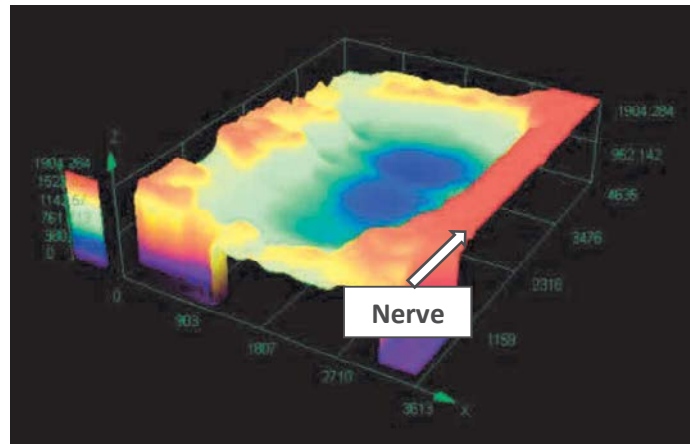


Figure 13

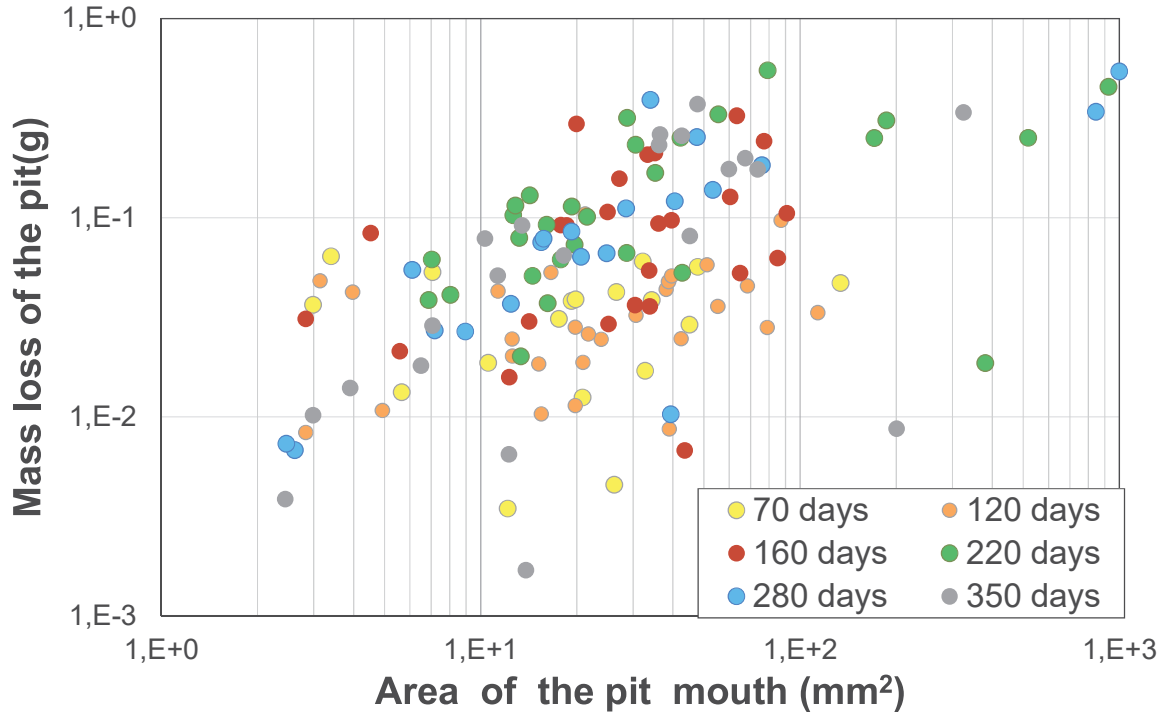


Figure 14

