

Catalytic non-thermal plasma reactor for decomposition of dilute chlorobenzene

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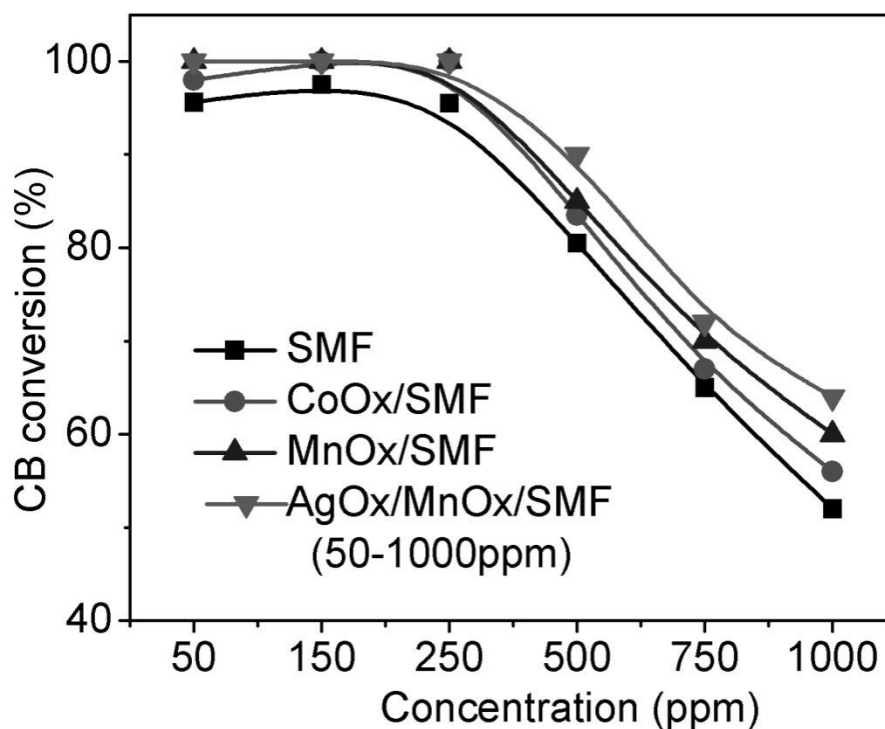


Fig. S1. Conversion of CB vs. concentration varied between 50 to 1000 ppm at a fixed SIE -530

(J/I)

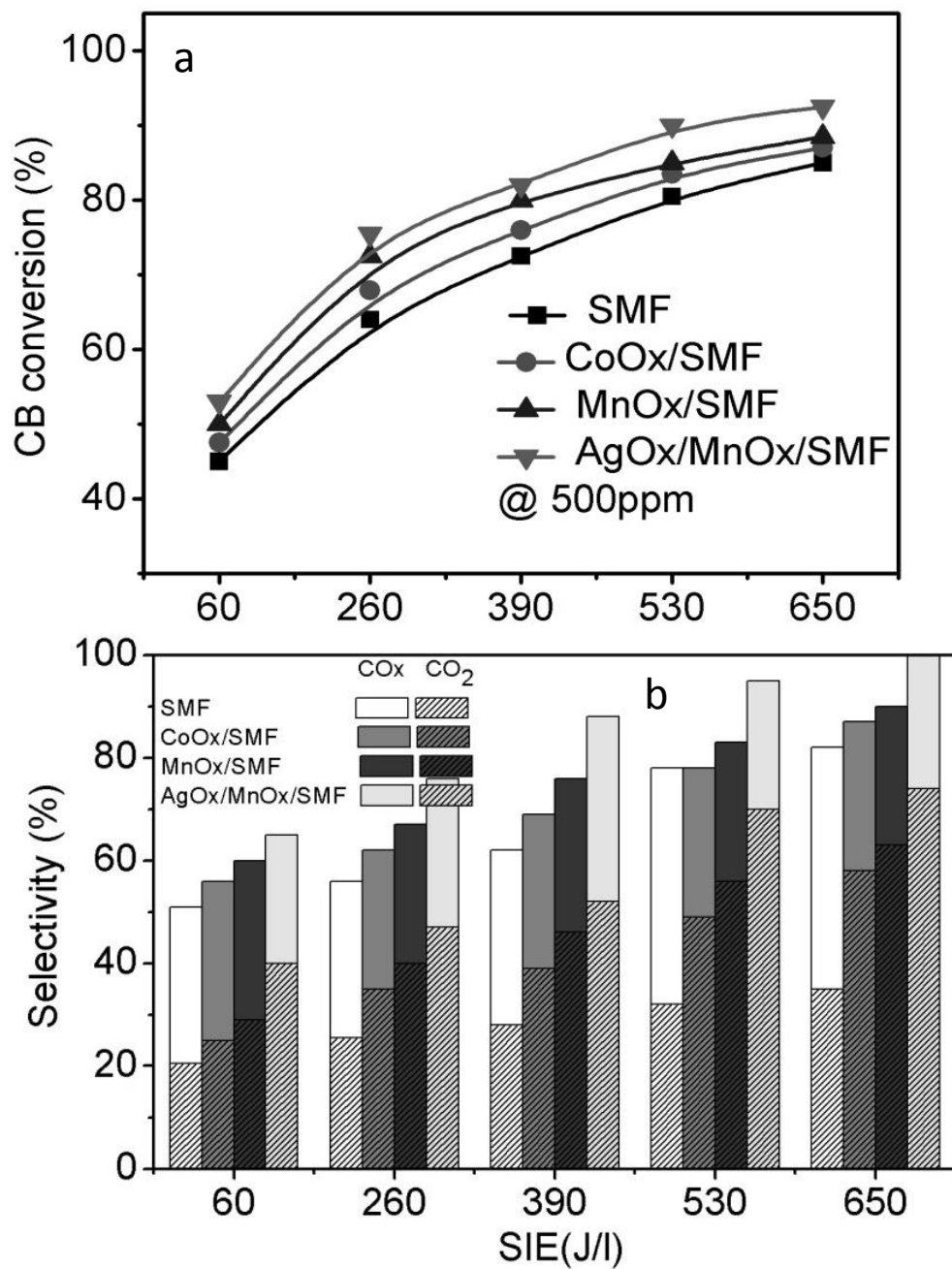


Fig. S2. Influence of SMF modification and SIE on (a) conversion and (b) selectivity to CO_x and CO₂ during removal of 500 ppm CB (SIE 60–650 J/l)

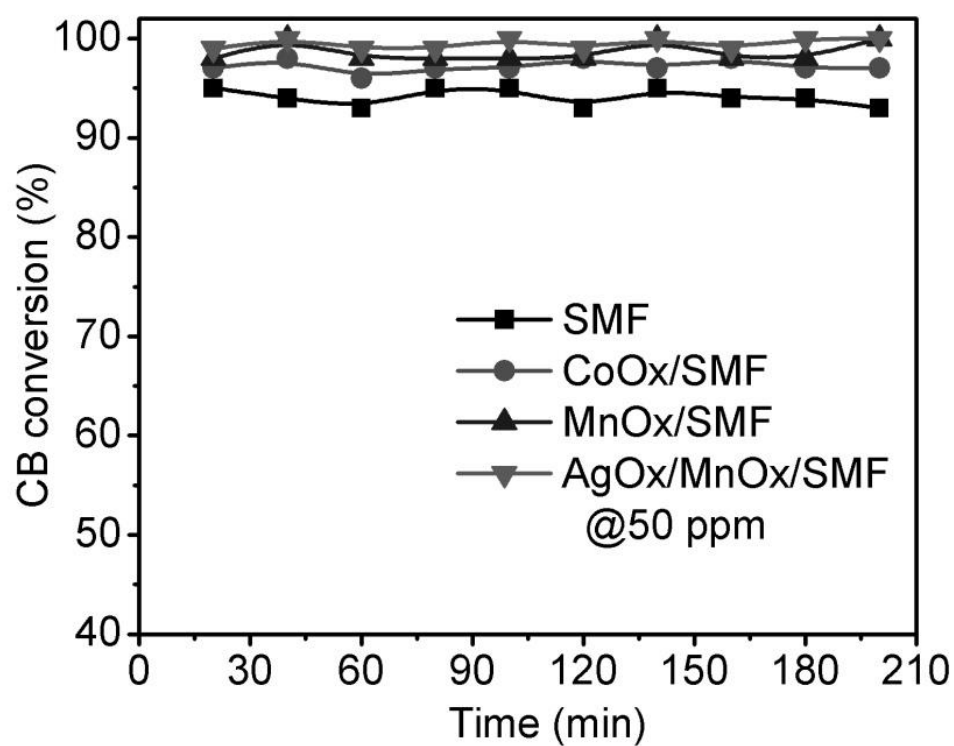


Fig. S3. Performance of NTP reactor as a function of time during conversion of 50 ppm of CB at 530 (J/l)