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Effects of Heat and Mass Transfer on MHD Free Convection Flow Near a Moving Vertical Plate of a Radiating and Chemically Reacting Fluid

Kalidas Das*Department of Mathematics,
Kalyani Government Engineering College, Kalyani,
Nadia, West Bengal, PIN:74125,
India

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The problem of unsteady MHD free convection flow and mass transfer of a viscous, electrically conducting and chemically reacting incompressible fluid in presence of thermal radiation and under the influence of uniform magnetic field applied normal to an infinite vertical plate, which moves with time dependent velocity is studied. The primary purpose of this study was to characterize the effects of thermal radiative heat transfer, magnetic field parameter, chemical reaction rate constant etc on the flow properties. The fluid is also assumed to be gray; emitting absorbing but non scattering medium and the optically thick radiation limit is considered. The solutions of the present problem are obtained in closed form by Laplace transform technique and the expressions for velocity, temperature, concentration, skin friction, rate of heat and mass transfer has been obtained. Some important applications of physical interest for different type motion of the plate are discussed. The results obtained have also been presented numerically through graphs to observe the effects of various parameters and the physical aspects of the problem.

Keywords: free convection, mass transfer, thermal radiation, chemically reacting fluid, MHD flow, Laplace transforms.

Introduction

The study of effects of magnetic field on free convection flow is important in liquid metals, electrolytes and ionized gasses. At the high temperature attained in some engineering devices, gas, for example, can be ionized and so becomes an electrical conductor. The ionized gas or plasma can be made to interact with the magnetic field and alter heat transfer and friction characteristic. Recently, it is of great interest to study the effect of magnetic field on the temperature distribution and heat transfer when the fluid is not only an electrical conductor but also when it is capable of emitting and absorbing thermal radiation. The radiation effect on MHD flow and heat transfer have become more important industrially. At high operating temperature, radiation effect can be quite significant. Many processes in engineering areas occur at high temperature and a knowledge of radiation heat transfer becomes very important for the design of the pertinent equipment. Nuclear power plants, gas turbines and the various propulsion devices for aircraft, missiles, satellites and space vehicles are examples of such engineering areas. Heat transfer by thermal radiation is becoming of greater importance when we are concerned with space applications, higher operating temperatures and also power engineering.

Extensive research work has been obtained on MHD free convection flow near vertical plate or surface with different boundary conditions [1,4]. Several investigations have been carried out on problem of heat transfer by radiation as an important application of space and temperature

*kd_kgec@rediffmail.com

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related problems. Grief et al. [5] obtained an exact solution for the problem of laminar convective flow in a vertical heated channel in the optically thin limit. In the optically thin limit, the fluid does not absorb its own emitted radiation which means that there is no self absorption but the fluid does absorb radiation emitted by the boundaries. The forced convective flow in a horizontal channel permeated by uniform vertical magnetic field taking radiation into account considered by Viskanta [6]. Gupta et al. [7] investigated the effect of radiation on the combined free and forced convection of an electrically conducting fluid flowing inside an open ended vertical channel in presence of uniform magnetic field for the case of optically thin limit. Soundalgakar et al. [8] generalized the problem by considering the effect of radiation on the natural convection flow of a gas past a semi infinite plate using the Cogly Vincentine Gilles equilibrium model (Cogly et al. [9]). Later many workers [10–17], under different boundary conditions analyzed the effect of radiation using the Rosseland diffusion approximation for mixed convection of an optically dense viscous incompressible fluid in presence of magnetic field. Das et al. [18] discussed the effect of radiation on MHD free convection flow of a chemically reacting fluid. Das et al. [19] extended the problem to included the effect of mass transfer on MHD free convection flow of a chemically reacting fluid through a porous medium. The effects of the phenomenon of mass transfer on a free convection flow near an infinite vertical porous plate which moves with time dependent velocity have been studied by Toki [20]. Recently Das et al. [21] studied the heat and mass transfer effects on the unsteady MHD free convection flow near a moving vertical plate in porous medium. Das et al. [22] extended the problem by considering the effect of thermal radiation on MHD free convection flow past an infinite vertical plate which moves with time dependent velocity.

In this study we consider the problem of the unsteady free convection flow and mass transfer of an optically thin viscous, electrically conducting and chemically reacting incompressible fluid near an infinite vertical plate which moves with time dependent velocity in presence of transverse uniform magnetic field and thermal radiation. A general exact solution for the partial differential equation governing these flows is obtained with the aid of the Laplace transform technique. Furthermore, this general solution is applied for the most important cases of flow.

1. Mathematical Formulation of the Problem

Consider unsteady free convection flow and mass transfer of a viscous incompressible, electrically conducting, radiating and chemically reacting fluid along an infinite non-conducting vertical plate in presence of a uniform transverse magnetic field B_0 applied in the direction of the flow. Let x -axis be along the plate in the upward direction and the y -axis normal to it (Fig. 1). Also let us assume that the magnetic Reynolds number is much less than unity so that the induced magnetic field is neglected in comparison to the applied magnetic field. Initially for time $t \leq 0$, the plate and the fluid are at the same constant temperature T_∞ in a stationary condition, with the same species concentration C_∞ at all points. Subsequently ($t > 0$), the plate is assumed to be accelerating with a velocity $U_0 f(t)$ in its own plane along the x -axis; instantaneously the temperature of the plate and the concentration are raised to T_w and C_w respectively which are hereafter regarded as constant. For free convection flows, here we also assume that all the physical properties of the fluid is to be in the direction of the x -axis, so the physical variables are functions of the space co-ordinate y and time t only.

Under the above assumptions, the fully developed flow of a radiating and chemically reacting fluid is governed by the following set of equations,

$$\frac{\partial u}{\partial t} = \nu \frac{\partial^2 u}{\partial y^2} + g\beta(T - T_\infty) + g\beta^*(C - C_\infty) - \frac{\sigma B_0^2 u}{\rho}, \quad (1.1)$$

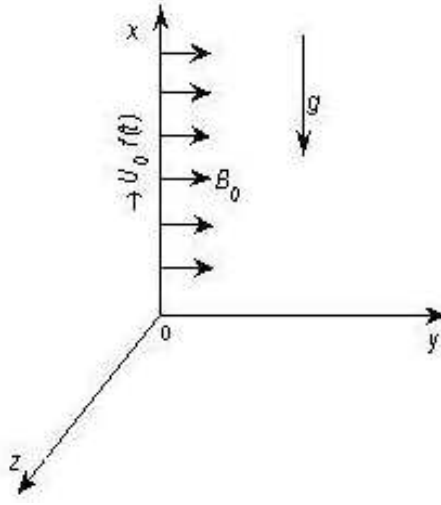


Fig. 1. A schematic of the problem and coordinate system

$$\rho c_p \frac{\partial T}{\partial t} = \kappa \frac{\partial^2 T}{\partial y^2} - \frac{\partial q_r}{\partial y}. \quad (1.2)$$

$$\frac{\partial C}{\partial t} = D \frac{\partial^2 C}{\partial y^2} - k_r C. \quad (1.3)$$

The initial and boundary conditions are

$$\left. \begin{aligned} u = 0, T = T_\infty, C = C_\infty \quad \forall \quad y \geq 0, t \leq 0, \\ u = U_0 f(t), T = T_w, C = C_w \quad \text{at} \quad y = 0, t > 0, \\ u \rightarrow 0, T \rightarrow T_\infty, C \rightarrow C_\infty \quad \text{as} \quad y \rightarrow \infty, t > 0, \end{aligned} \right\} \quad (1.4)$$

where u is the velocity in the x -direction, ρ the density, g the acceleration due to gravity, β the volumetric coefficient of thermal expansion, β^* the volumetric coefficient of expansion for concentration, T the temperature of the fluid near the plate, C is the species concentration, c_p the specific heat at constant pressure, κ the thermal conductivity, q_r the radiative flux, ν the kinematic coefficient of viscosity, σ the electrical conductivity, D the chemical molecular diffusivity and k_r the chemical reaction rate constant.

In the optically thick limit, the fluid does not absorb its own emitted radiation, that is there is no self absorption but it does absorb radiation emitted by the boundaries. It has been shown by Cogly et al. [9] that in the optically thick limit for a non gray gas near equilibrium that

$$\frac{\partial q_r}{\partial y} = 4(T - T_\infty) \int_0^\infty K_{\lambda\omega} \left(\frac{de_{b\lambda}}{dT} \right)_\omega d\lambda = 4I_1(T - T_\infty), \quad (1.5)$$

where $K_{\lambda\omega}$ is the absorption coefficient, $e_{b\lambda}$ is the Planck function and the subscript ω refers to values at the wall.

To reduce the above equations into non-dimensional form, let us introduce the following

dimensionless variables and parameters:

$$\left. \begin{aligned} u' &= \frac{u}{U_0}, t' = \frac{tU_0^2}{\nu}, y' = \frac{yU_0}{\nu}, \theta' = \frac{T - T_\infty}{T_w - T_\infty}, C' = \frac{C - C_\infty}{C_\omega - C_\infty}, \\ M &= \frac{\sigma B_0^2 \nu}{\rho U_0^2}, P_r = \frac{\mu c_p}{\kappa}, G_r = \frac{\nu g \beta (T_w - T_\infty)}{U_0^3}, G_m = \frac{\nu g \beta^* (C_\omega - C_\infty)}{U_0^3}, \\ F &= \frac{4I_1 \nu^2}{\kappa U_0^2}, K_r = \frac{k_r \nu^2}{DU_0^2}, S_c = \frac{\nu}{D}, \end{aligned} \right\} \quad (1.6)$$

where G_r is thermal Grashof number, G_m is the mass Grashof number, S_c is Schmidt number, M is magnetic field parameter, P_r is the Prandtl number, F is the radiation parameter, K_r is the chemical reaction rate parameter.

With the help of (1.6), the governing equations (1.1)–(1.3) reduce to (dropping the primes),

$$\frac{\partial u}{\partial t} = \frac{\partial^2 u}{\partial y^2} + G_r \theta + G_m C - Mu, \quad (1.7)$$

$$P_r \frac{\partial \theta}{\partial t} = \frac{\partial^2 \theta}{\partial y^2} - F \theta, \quad (1.8)$$

$$S_c \frac{\partial C}{\partial t} = \frac{\partial^2 C}{\partial y^2} - K_r C. \quad (1.9)$$

The corresponding initial and boundary conditions in non-dimensional form are

$$\left. \begin{aligned} u &= 0, \theta = 0, C = 0, \quad \forall \quad y \geq 0, t \leq 0, \\ u &= f(t), \theta = 1, C = 1 \quad \text{at} \quad y = 0, t > 0, \\ u &\rightarrow 0, \theta \rightarrow 0, C \rightarrow 0 \quad \text{as} \quad y \rightarrow \infty, t > 0. \end{aligned} \right\} \quad (1.10)$$

The system(1.7)–(1.9) of differential equations, subject to the boundary conditions (1.10), includes the effect of free convection and mass transfer on the flows near a moving isothermal vertical plate.

2. Solution of the Problem

In order to obtain the analytical solution of the system of differential equations (1.7)–(1.9) subject to the initial and boundary conditions (1.10), we shall use the Laplace transformation technique.

Thus the general solutions of the present problem for the temperature $\theta(y,t)$, the species concentration $C(y,t)$ and the velocity $u(y,t)$ for $t > 0$ are given by

$$\theta(y,t) = \frac{1}{2} \left[e^{-y\sqrt{F}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{P_r}{t}} - \sqrt{\frac{Ft}{P_r}} \right) + e^{y\sqrt{F}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{P_r}{t}} + \sqrt{\frac{Ft}{P_r}} \right) \right], \quad (2.1)$$

$$C(y,t) = \frac{1}{2} \left[e^{-y\sqrt{K_r}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{S_c}{t}} - \sqrt{\frac{K_r t}{S_c}} \right) + e^{y\sqrt{K_r}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{S_c}{t}} + \sqrt{\frac{K_r t}{S_c}} \right) \right], \quad (2.2)$$

$$u(y,t) = \Phi(y,t) + A(y,t) + B(y,t), \quad (2.3)$$

where

$$\Phi(y,t) = L^{-1} [f(\bar{s})e^{-ay}], f(\bar{s}) = L[f(t)], \quad (2.4)$$

$$\begin{aligned}
 A(y, t) = & \frac{G_r}{2a_1} e^{c_1 t} \left[e^{-y\sqrt{b_1}} \left\{ \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{b_1 t} \right) - \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{P_r}{t}} - \sqrt{\frac{b_1 t}{P_r}} \right) \right\} + \right. \\
 & \left. + e^{y\sqrt{b_1}} \left\{ \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{b_1 t} \right) - \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{P_r}{t}} + \sqrt{\frac{b_1 t}{P_r}} \right) \right\} \right] + \\
 & + \frac{G_r}{2a_1} \left[e^{-y\sqrt{F}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{P_r}{t}} - \sqrt{\frac{Ft}{P_r}} \right) + e^{y\sqrt{F}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{P_r}{t}} + \sqrt{\frac{Ft}{P_r}} \right) \right] - \\
 & - \frac{G_r}{2a_1} \left[e^{-y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{Mt} \right) + e^{y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{Mt} \right) \right], \tag{2.5}
 \end{aligned}$$

$$\begin{aligned}
 B(y, t) = & \frac{G_m}{2a_2} e^{c_2 t} \left[e^{-y\sqrt{b_2}} \left\{ \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{b_2 t} \right) - \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{S_c}{t}} - \sqrt{\frac{b_2 t}{S_c}} \right) \right\} + \right. \\
 & \left. + e^{y\sqrt{b_2}} \left\{ \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{b_2 t} \right) - \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{S_c}{t}} + \sqrt{\frac{b_2 t}{S_c}} \right) \right\} \right] + \\
 & + \frac{G_m}{2a_2} \left[e^{-y\sqrt{K_r}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{S_c}{t}} - \sqrt{\frac{K_r t}{S_c}} \right) + e^{y\sqrt{K_r}} \operatorname{erfc} \left(\frac{y}{2} \sqrt{\frac{S_c}{t}} + \sqrt{\frac{K_r t}{S_c}} \right) \right] - \\
 & - \frac{G_m}{2a_2} \left[e^{-y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{Mt} \right) + e^{y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{Mt} \right) \right] \tag{2.6}
 \end{aligned}$$

and $a_1 = M - F$, $b_1 = \frac{MP_r - F}{P_r - 1}$, $c_1 = \frac{M - F}{P_r - 1}$, $a_2 = M - K_r$, $b_2 = \frac{MS_c - K_r}{S_c - 1}$, $c_2 = \frac{M - K_r}{S_c - 1}$.

Since non-dimensional temperature $\theta(y, t)$ and non-dimensional species concentration $C(y, t)$ is clearly described in (2.1) and (2.2), so we shall confine ourselves to non-dimensional velocity $u(y, t)$ for various types of $f(t)$. Here the expressions (2.3)–(2.6) are the general solutions of the present problem which include the effects of heating (cf. term A), diffusion (cf. term B) and the motion of the plate.

3. Applications of the General Solution

In this section we now consider some important cases of flow as given below:

Case (i): motion of the plate with uniform velocity. Let $f(t) = H(t)$. Heaviside unit function, then

$$\bar{f}(s) = L[f(t)] = \frac{1}{s}. \tag{3.1}$$

In this case we observe that the result (2.1), (2.2) are unaffected and the expression (2.3) for $u(y, t)$ becomes

$$u(y, t) = \frac{1}{2} \left[e^{-y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{Mt} \right) + e^{y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{Mt} \right) \right] + A(y, t) + B(y, t), \tag{3.2}$$

where $A(y, t)$, $B(y, t)$ are given from equation (2.5), (2.6).

Case (ii): motion of the plate with single acceleration. Let $f(t) = tH(t)$, then

$$\bar{f}(s) = \frac{1}{s^2}. \tag{3.3}$$

In this case also we observe that the result (2.1), (2.2) remain in the same form but the expression (2.3) for $u(y, t)$ takes the following analytical form :

$$\begin{aligned}
 u(y, t) = & \frac{1}{2} \left[\left(t - \frac{y}{2\sqrt{M}} \right) e^{-y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{Mt} \right) + \left(t + \frac{y}{2\sqrt{M}} \right) e^{y\sqrt{M}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{Mt} \right) \right] + \\
 & + A(y, t) + B(y, t), \tag{3.4}
 \end{aligned}$$

where $A(y, t)$, $B(y, t)$ are given from equation (2.5), (2.6).

Case (iii): motion of the plate with periodic acceleration. For this case, let $f(t) = H(t) \cos(\omega t)$, then

$$\bar{f}(s) = \frac{s}{s^2 + \omega^2}. \quad (3.5)$$

Then the expression (2.1), (2.2) remains again in the same form but, instead of (2.3), we get the following analytical expression:

$$\begin{aligned} u(y, t) = & \frac{1}{4} e^{i\omega t} \left[e^{y\sqrt{M+i\omega}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{(M+i\omega)t} \right) + e^{-y\sqrt{M+i\omega}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{(M+i\omega)t} \right) \right] + \\ & + \frac{1}{4} e^{-i\omega t} \left[e^{y\sqrt{M-i\omega}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} + \sqrt{(M-i\omega)t} \right) + e^{-y\sqrt{M-i\omega}} \operatorname{erfc} \left(\frac{y}{2\sqrt{t}} - \sqrt{(M-i\omega)t} \right) \right] + \\ & + A(y, t) + B(y, t), \end{aligned} \quad (3.6)$$

where $A(y, t)$, $B(y, t)$ are given from equation (2.5), (2.6).

It should be noted that our results of case (i) are identical with those of Das[22].

4. Skin Friction

Knowing the velocity field, we now study the effect of t, P_r, M, F etc. on the skin friction. In non-dimensional form, it is given by

$$\begin{aligned} \tau = - \left(\frac{\partial u}{\partial y} \right)_{y=0} = & - \left(\frac{\partial \Phi}{\partial y} \right)_{y=0} + \frac{G_r}{a_1} e^{c_1 t} \left[\sqrt{b_1} \left\{ \operatorname{erf}(\sqrt{b_1 t}) - \operatorname{erf} \left(\sqrt{\frac{b_1 t}{P_r}} \right) \right\} + \frac{1}{\sqrt{\pi t}} e^{-b_1 t} - \sqrt{\frac{P_r}{\pi t}} e^{-\frac{b_1 t}{P_r}} \right] - \\ & - \frac{G_r}{a_1} \left[\sqrt{M} \operatorname{erf}(\sqrt{Mt}) + \frac{1}{\sqrt{\pi t}} e^{-Mt} \right] + \frac{G_r}{a_1} \left[\sqrt{F} \operatorname{erf} \left(\sqrt{\frac{Ft}{P_r}} \right) + \sqrt{\frac{P_r}{\pi t}} e^{-\frac{Ft}{P_r}} \right] + \\ & + \frac{G_m}{a_2} e^{c_2 t} \left[\sqrt{b_2} \left\{ \operatorname{erf}(\sqrt{b_2 t}) - \operatorname{erf} \left(\sqrt{\frac{b_2 t}{S_c}} \right) \right\} + \frac{1}{\sqrt{\pi t}} e^{-b_2 t} - \sqrt{\frac{S_c}{\pi t}} e^{-\frac{b_2 t}{S_c}} \right] - \\ & - \frac{G_m}{a_2} \left[\sqrt{M} \operatorname{erf}(\sqrt{Mt}) + \frac{1}{\sqrt{\pi t}} e^{-Mt} \right] + \frac{G_m}{a_2} \left[\sqrt{K_r} \operatorname{erf} \left(\sqrt{\frac{K_r t}{S_c}} \right) + \sqrt{\frac{S_c}{\pi t}} e^{-\frac{K_r t}{S_c}} \right]. \end{aligned} \quad (4.1)$$

When the plate is moving with uniform velocity then,

$$\left(\frac{\partial \Phi}{\partial y} \right)_{y=0} = - \left\{ \sqrt{M} \operatorname{erf}(\sqrt{Mt}) + \frac{1}{\sqrt{\pi t}} e^{-Mt} \right\}. \quad (4.2)$$

Again when the plate is moving with single acceleration then,

$$\left(\frac{\partial \Phi}{\partial y} \right)_{y=0} = - \left\{ \sqrt{M} \left(t + \frac{1}{2M} \right) \operatorname{erf}(\sqrt{Mt}) + \sqrt{\frac{t}{\pi}} e^{-Mt} \right\}. \quad (4.3)$$

Lastly when the plate is moving with periodic acceleration then,

$$\begin{aligned} \left(\frac{\partial \Phi}{\partial y} \right)_{y=0} = & - \frac{1}{2\sqrt{t}} \left[e^{i\omega t} \sqrt{(M+i\omega)} \operatorname{erf} \sqrt{(M+i\omega)t} + \right. \\ & \left. + e^{-i\omega t} \sqrt{(M-i\omega)} \operatorname{erf} \sqrt{(M-i\omega)t} \right] - \sqrt{\frac{t}{\pi}} e^{-Mt}. \end{aligned} \quad (4.4)$$

5. Nusselt Number

An important phenomenon in this study is to understand the effect of t , F and P_r on the nusselt number. In non-dimensional form, the rate of heat transfer is given by

$$N_u = - \left(\frac{\partial \theta}{\partial y} \right)_{y=0} = \sqrt{F} \operatorname{erf} \left(\sqrt{\frac{Ft}{P_r}} \right) + \sqrt{\frac{P_r}{\pi t}} e^{-\frac{Ft}{P_r}}. \quad (5.1)$$

6. Sherwood Number

Another important physical quantities of interest is the Sherwood number whose non-dimensional form is

$$S_h = - \left(\frac{\partial C}{\partial y} \right)_{y=0} = \sqrt{K_r} \operatorname{erf} \left(\sqrt{\frac{K_r t}{S_c}} \right) + \sqrt{\frac{S_c}{\pi t}} e^{-\frac{K_r t}{S_c}}. \quad (6.1)$$

We study the effects of t , S_c and K_r on Sherwood number numerically in the next section for better understanding.

7. Numerical Results and Discussion

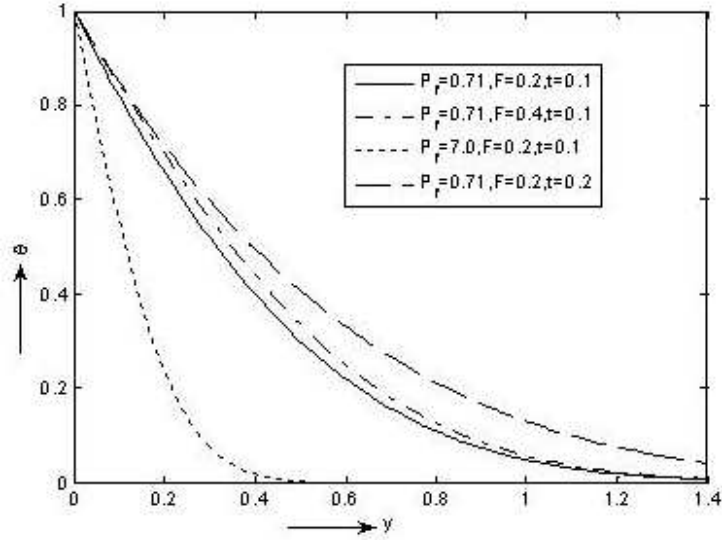


Fig. 2. Effects P_r , F and t on concentration distribution

To understand the physical meaning of the problem, we have computed the expression for the velocity $u(y, t)$, the temperature $\theta(y, t)$ and concentration $C(y, t)$ for the case of air $P_r (= 0.70)$ and water $P_r (= 7.0)$ and for different values of magnetic field parameter M , the radiation parameter F , the chemical reaction rate constant K_r , Schmidt number S_c and time t . The purpose of the numerical result given here is to assess the effects of different parameters upon the nature of the flow, temperature and concentration etc.

Fig. 2 depicts the temperature profiles against y (distance from plate). We observe that the temperature for air is greater than that of water, which is due to the fact that thermal

conductivity of fluid decreases with increasing P_r . We observe that the temperature decreases with increasing F and increases with increasing t . The temperature profiles are in good agreement with the results obtained in case of Das [22].

For various values of Schmidt number S_c , chemical reaction rate constant K_r and time t , the concentration profiles are shown in Fig. 3. The concentration distribution decreases at all points of the flow field with the increase of the chemical reaction rate constant. It is seen from figure that an increase in the Schmidt number leads to an decrease in the concentration but it increases with increasing time. The concentration profiles closely agree with those of Das [22]. Applying numerical values into the expressions of exact solutions for the velocity, we get the

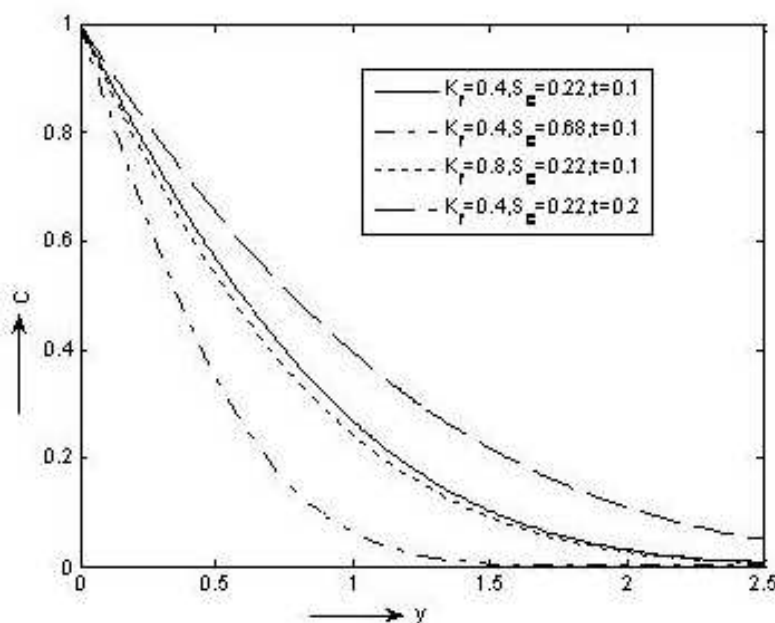


Fig. 3. Effects S_c , K_r and t on temperature profile

velocity profiles of air flows near vertical plate. Figs. 4 and 5 correspond to the plates moving with uniform velocity and with single acceleration respectively. Also Fig. 6 corresponds to the plates which are moved with periodic acceleration. It is seen from these figures that increasing values of F , K_r leads to fall in velocity but an increase of M leads to an increase in velocity of air. In case of Das [22], the magnetic parameter M shows reverse effect.

Figs. 7–9 depict skin-friction against time t for different values of M , F and K_r . It is observed that the skin friction decreases with increasing F , K_r and t but effect is reverse for M . So wall shear stress decreases with increasing radiation parameter, chemical reaction rate constant and also time. Thus the results are identical with those of Das [22]

Nusselt number is presented in Fig. 10 against time. It decreases with time but increases with increasing the radiation parameter. Also Nusselt number for $P_r = 7$ is higher than that of $P_r = 0.71$.

In Fig. 11, Sherwood number is presented against time t for different values of S_c and K_r . We observed that Sherwood number increases with increasing S_c and K_r which is just the reverse of the results obtained in case of Das [22].

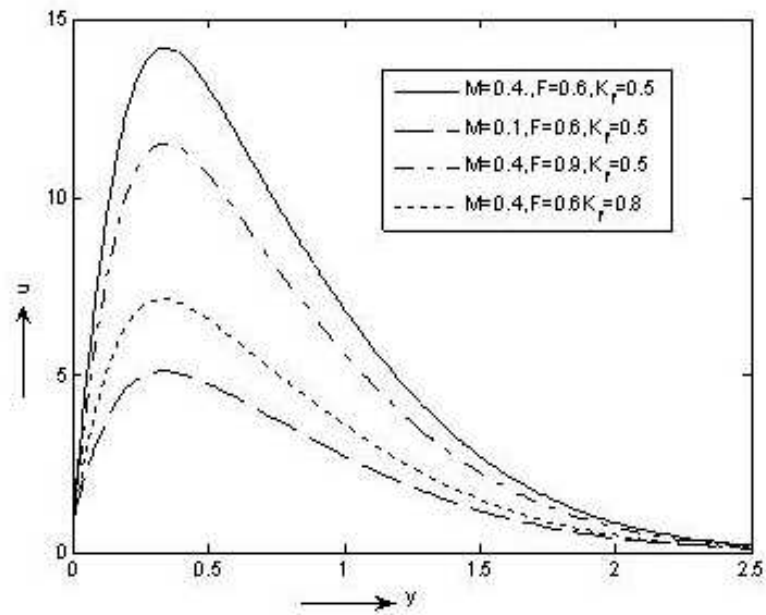


Fig. 4. Velocity profile when the plate moves with uniform velocity

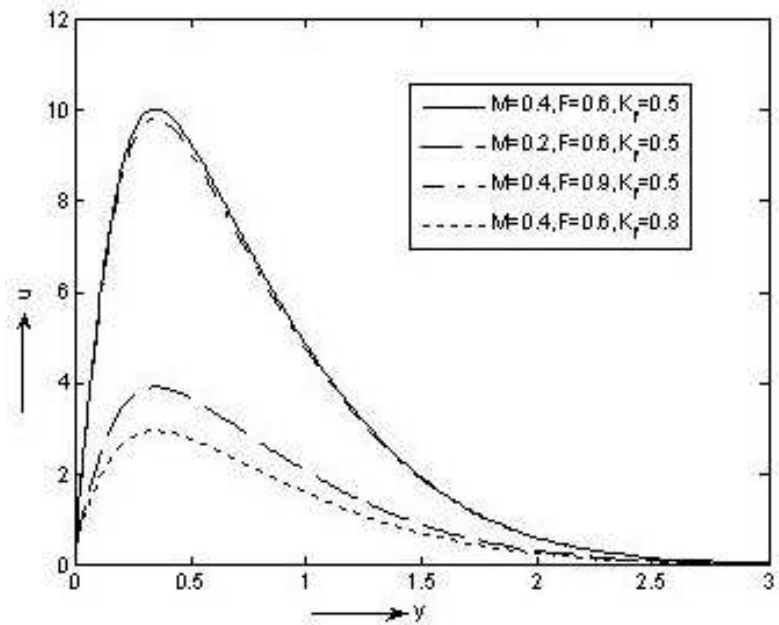


Fig. 5. Velocity profile when the plate moves with single acceleration

8. Conclusion

In this study, the effect of thermal radiation and chemical reaction on MHD free convection flow and mass transfer near a moving vertical plate is presented. A general analytical solution

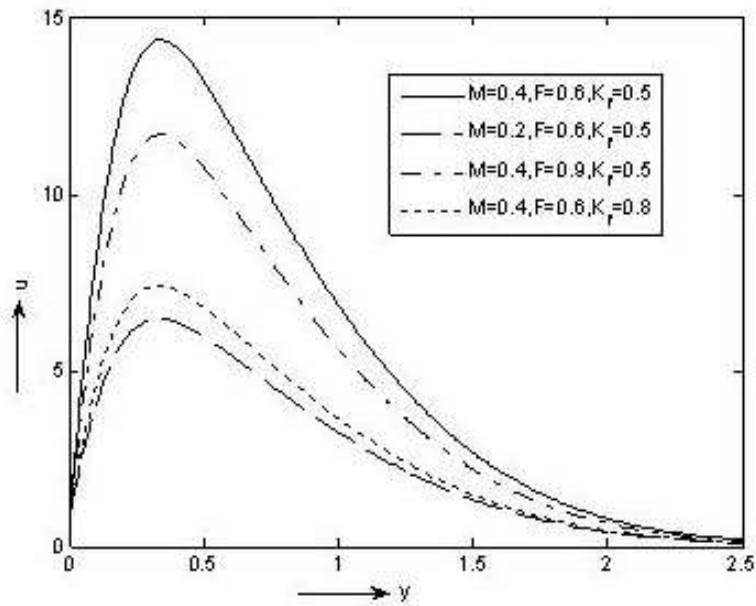


Fig. 6. Velocity profile when the plate moves with periodic acceleration

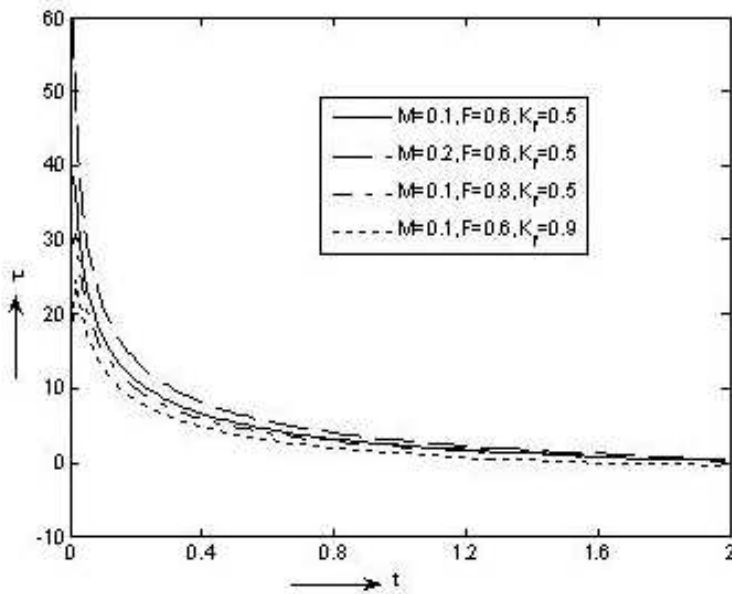


Fig. 7. Skin-friction when the plate moves with uniform velocity

for the problem has been determined without any restriction. Some important applications from the point of view of physical interest was discussed. Also we study a physical example for evaluation of the numerical values of the velocity, temperature and concentration for the case of air ($P_r = 0.71$) and water ($P_r = 7.0$) and observed that the temperature decreases with increasing F and increases with increasing t . The concentration distribution of the flow field decreases at

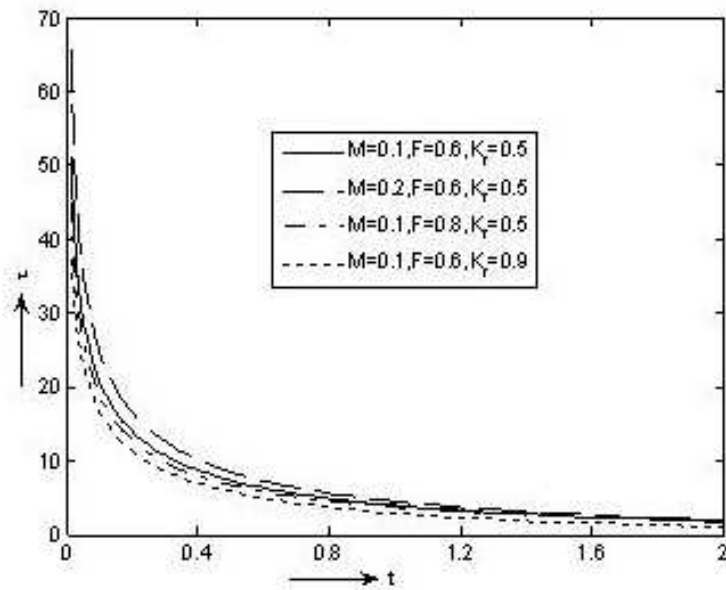


Fig. 8. Skin-friction when the plate moves with single acceleration

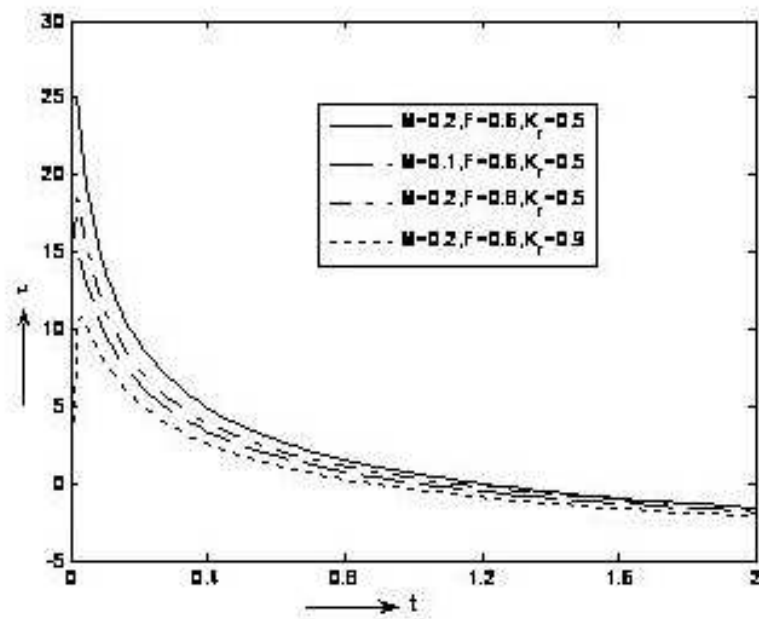


Fig. 9. Skin-friction when the plate moves with periodic acceleration

all points as the Schmidt number S_c and chemical reaction rate constant K_r increases. Also the velocity decreases with increasing F and K_r , while M shows the reverse effect. The skin friction coefficient decreases with increasing F , K_r and t but the effect is reverse for M . The rate of heat transfer for water is more than that of air and it increases with increasing the radiation

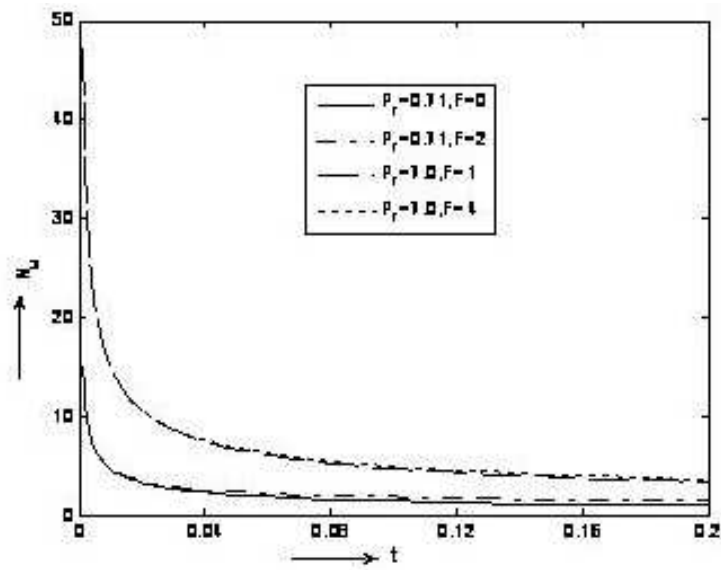


Fig. 10. Effects of P_r and F on Nusselt number

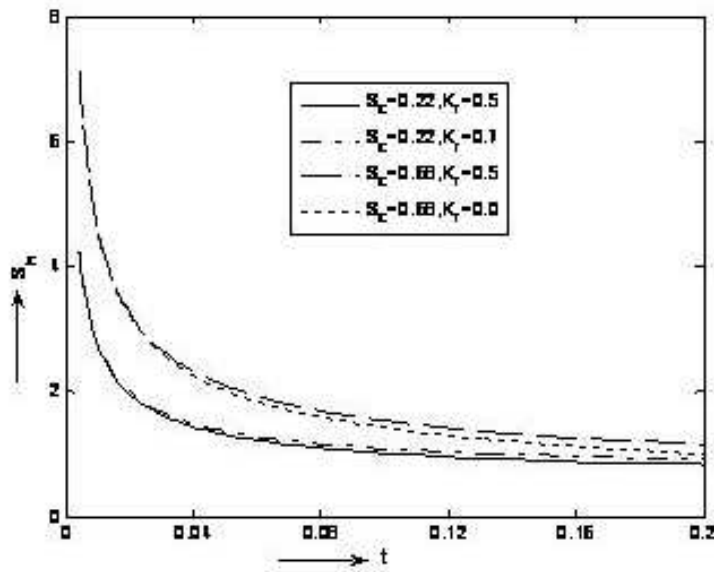


Fig. 11. Effects of S_c and K_r on Sherwood number

parameter. The rate of mass transfer increases with increasing S_c and K_r . To our knowledge, this work gives in close form the actual analytical solution of the MHD free convection flow and mass transfer of an optically thin and chemically reacting fluid which has wide application in power engineering and also in the study of vertical air flows into the atmosphere.

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Влияние тепло- и массопереноса на свободно конвективное МГД–течение вблизи вертикального движущегося слоя излучающей и химически реагирующей жидкости

Калидас Дас

Исследуется задача о нестационарном свободно конвективном МГД–течении и массопереносе вязкой, электропроводной и химически реагирующей несжимаемой жидкости при наличии теплового излучения и под влиянием однородного магнитного поля, приложенного перпендикулярно к бесконечному вертикальному слою, который движется с переменной скоростью. Основной целью данного исследования было рассмотреть влияние теплового излучения, магнитного поля и постоянной химической реакции на параметры течения. Предполагается, что жидкость является серой, излучающей, поглощающей, но не рассеивающей средой. Решение представленной задачи получено в замкнутой форме с использованием преобразования Лапласа. Приводятся выражения для скорости, температуры, концентрации, поверхностного трения и скоростей изменения тепло и массопереноса. Обсуждаются некоторые интересные физические явления, возникающие при различных типах движения слоя. Полученные результаты также представлены в виде графиков, которые показывают влияние различных параметров и физические аспекты задачи.

Ключевые слова: свободная конвекция, массоперенос, тепловое излучение, химически реагирующая жидкость, МГД–течение, преобразование Лапласа.