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Author(s)	Li, RY; Fang, HHP
Citation	Critical Reviews In Environmental Science And Technology, 2009, v. 39 n. 12, p. 1081-1108
Issued Date	2009
URL	http://hdl.handle.net/10722/124556
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Heterotrophic Photo Fermentative Hydrogen Production

Ru Ying Li and Herbert H. P. Fang*

Department of Civil Engineering, The University of Hong Kong

Pokfulam Road, Hong Kong

Fax: 852-2559-5337; email: hrechef@hkucc.hku.hk

ABSTRACT

This article reviews the state-of-the-art of heterotrophic photo fermentative hydrogen production, an infantile technology for wastewater treatment. Five tables were compiled from data scattered in literature, including bacteria strain, substrate, reactor design, maximum volumetric and specific production rates ($\text{ml-H}_2/\text{l/h}$ and/or $\text{ml-H}_2/\text{g-VSS/h}$), yield as compared to stoichiometry (%), culture volume (ml), cell density (g-VSS/l), light source and intensity (W/m^2 or klux). Operational parameters discussed include light source and light intensity, pH, temperature, substrates, nitrogen source, trace metal elements, inhibitors, and reactor design, followed by a discussion on the outlook of this technology.

KEY WORDS: hydrogen, fermentation, heterotrophic, phototrophic, wastewater.

I. INTRODUCTION

Despite their detrimental effects on air pollution and global warming, fossil fuels are still the main source of energy supply for the world economy even though their reserves are depleting rapidly. This has led to the search for alternative energy sources, among which hydrogen has attracted much attention recently. Hydrogen has an energy yield of 122 kJ/g, about 2.75 times higher than those of hydrocarbons (Kapdan and Kargi, 2006), and may be used directly for combustion or generating electricity by fuel cells. It is an ideal fuel from the environment point of view, producing only water as by-product in the energy producing process. Many have predicted that hydrogen may become the main source of energy for the 21th century economy (Rifkin, 2002).

Hydrogen is conventionally produced by either electrolysis of water or thermocatalytic reformation of hydrocarbons. Heterotrophic microbiological production of hydrogen has, however, attracted research interests due to its potential ability of degrading organic pollutants (Yetis et al., 2000; Li and Fang, 2007). Microbial production of hydrogen is often classified into two categories depending on whether light is required: dark fermentation and photo fermentation (Levin et al., 2004). Dark fermentation may, due to thermodynamic limitation, convert no more than 40% of the chemical energy in the organic pollutants into hydrogen in the absence of light, producing organic acids, mainly acetate and butyrate, and alcohols as by-products. Photo-fermentation may, on the other hand, potentially be able to convert acids and alcohols, which are the by-products of dark fermentation, into hydrogen using light as energy source. The latter process produces little organic

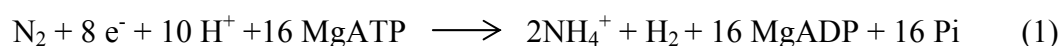
residues and thus is potentially applicable for wastewater treatment (Das and Veziroğlu, 2001).

Unlike methanogenic fermentation, which has been commercialized for wastewater treatment for two decades with thousands of full-scale installation worldwide (Fang and Liu, 2002), fermentation of wastewater for hydrogen production remains at the infantile stage. Most of related studies were conducted using dark fermentation, as summarized in a recent review article (Li and Fang, 2007). Studies of photo fermentative wastewater treatment were conducted mostly for suspended pure cultures using single substrates, with a few exceptions for mixed cultures and multi-substrate.

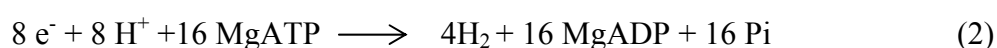
This article aims to review the enzymatic reactions of heterotrophic photo fermentative hydrogen production and the state-of-the-art of this infantile technology for wastewater treatment. Five tables were at first compiled for photo fermentative hydrogen production data scattered in literature, including bacteria strain, substrate, reactor design (batch or continuous), maximum volumetric and specific production rates ($\text{ml-H}_2/\text{l/h}$ and/or $\text{ml-H}_2/\text{g-VSS/h}$), yield as compared to stoichiometry (%), culture volume (ml), cell density (g-VSS/l), light source and intensity (W/m^2 or klux). Table 1 was compiled for data on suspended growth of pure cultures, Table 2 for suspended growth of mixed cultures, Table 3 for combined photo-fermentative culture and others, Table 4 for immobilized cultures, and Table 5 for mutated cultures.

II. ENZYMATIC REACTIONS OF PHOTO FERMENTATIVE HYDROGEN PRODUCTION

Heterotrophic photo fermentative hydrogen production by purple non-sulfur bacteria is catalyzed by nitrogenase (Das and Veziroğlu, 2001; Melis and Melnicki, 2006). In the presence of molecular nitrogen (N₂), this enzyme which is composed of two proteins, i.e. dinitrogenase and dinitrogenase reductase (Burris, 1991; Orme-Johnson, 1992), reduces N₂ into ammonium (NH₄⁺), as follows (Peters et al., 1995):



where Pi represents orthophosphate. However, in the absence of N₂, nitrogenase may catalyze the following reaction resulting in the production of hydrogen:



All phototrophic hydrogen-producing bacteria have a nitrogenase consisting of a cofactor (encoded by the gene *nif*) made of iron (Fe) and molybdenum (Mo) (Smith, 2002), including *Rhodobacter sphaeroides* (Haaker et al., 1982), *Rhodobacter capsulatus* (Siemann et al., 2001), *Rhodospirillum rubrum* (Ludden and Burris, 1978) and *Rhodopseudomonas palustris* (Arp and Zumft, 1983). Three species, i.e. *R. capsulatus* (Schneider et al., 1991; Gollan et al., 1993; Siemann et al., 2002), *R. rubrum* (Lehman and Roberts, 1991) and *R. palustris* (Zumft and Gastillo, 1978; Larimer et al., 2003), have additional nitrogenases (Eady and Leigh, 1994) consisting of cofactors made of FeFe (encoded by gene *anf*; Chisnell et al., 1988) and/or FeV (encoded by the gene *vnf*; Hales et al., 1986). Genes *vnf* and *anf* are activated only under Mo-limiting condition.

III. HETEROTROPHIC PHOTO FERMENTATIVE HYDROGEN-PRODUCING BACTERIA AND SLUDGE

Phototrophic bacteria are mainly classified into two categories, i.e. purple bacteria and green bacteria, excluding several isolates without clear taxonomic position (Sasikala and Ramana, 1995). Each category may be further divided into sulfur and non-sulfur bacteria. Among the four groups, only the purple non-sulfur bacteria, which carry out anoxygenic photosynthesis using simple organic acids and sugars as substrate, are potentially useful for wastewater treatment. For the remaining groups, purple sulfur bacteria and green sulfur bacteria are autotrophic, using sulfide or elemental sulfur as electron donor, and thus are of little interest to environmental engineers for biological wastewater treatment. For the green non-sulfur bacteria, only one species, i.e. *Chloroflexus aurantiacus* (Gogotov et al., 1991), is known to be able to produce hydrogen.

Purple non-sulfur bacteria are heterotrophic and thus may be useful for the removal of organic pollutants in water. Those capable of producing hydrogen from organic substrates include the fresh water species *R. sphaeroides* (Fascetti et al., 1998), *R. capsulatus* (Ooshima et al., 1998), *R. palustris* (Oh et al., 2004) and *R. rubrum* (Najafpour et al., 2004), and the marine species *Rhodovulum sp.* (Yamada et al., 1998; Matsunaga et al., 2000), *Rhodovulum sulfidophilum* (Maeda et al., 2003), and *Rhodobacter marinus* (Yamada et al., 1996).

III.A. Pure Cultures

Most studies of heterotrophic photo fermentative hydrogen production were conducted for pure cultures. Results compiled in Table 1 show that most studies were conducted using fresh water species, particularly *R. sphaeroides* and *R. capsulatus*. The rate of hydrogen production varied drastically, from 1.0 to 713.0 ml/l/h or 0.7 to 250.0 ml/g/h, depending on the bacteria species, substrates, and operation conditions. The highest volumetric rate of 713 ml/l/h was achieved by *Rhodovulum* sp. using malate (Matsunaga et al., 2000), and the highest specific rate of 250 ml/l/h by *R. sphaeroides* from glucose (Zhu et al., 2001).

For *R. sphaeroides*, the highest hydrogen production rate, 240.0 ml/l/h (171 ml/g/h) was achieved by strain RV using lactate in batch experiment (Nakada et al., 1995). Such a relatively high rate could be attributed to the high light intensity (720 W/m²), or the reactor design (flat with a thickness of 0.5 cm), or its small scale (30 ml). For comparison, using the same bacteria treating a wastewater from sugar refinery mixed with malate in a continuous reactor had a substantially lower hydrogen production rate (1.0 ml/l/h or 0.71 ml/g/h) (Yetis et al., 2000).

For *R. capsulatus*, the hydrogen production rates varied from 12.5 to 75.0 ml/l/h or 19.1 to 130.0 ml/g/h. In a continuous reactor, *R. capsulatus* produced hydrogen at the rates of 12.5-21.0 ml/l/h and 33.0-38.9 ml/g/h using mixed organic acids (Shi and Yu, 2006). The highest volumetric and specific rates were from the degradation of lactate (Hillmer and Gest, 1977a; 1977b).

For *R. palustris*, the hydrogen production rates varied from 1.6 to 24.9 ml/l/h or 2.5 to 82.7 ml/g/h. The highest volumetric rate of 24.9 ml/l/h was achieved using butyrate (Chen et al., 2007), and the specific rate of 82.7 ml/g/h from lactate (Barbosa et al., 2001). *R. palustris* R1 was unable to produce hydrogen from butyrate (Barbosa et al., 2001).

R. rubrum was able to produce hydrogen from organic acids, such as lactate (Zürcher and Bachofen, 1979) and malate (Miyake et al., 1982), as well as CO (Klasson et al., 1993; Najafpour et al., 2004). In addition to the aforementioned four bacteria, *Rubrivivax gelatinosus* (Maness and Weaver, 2002; Mérida et al., 2004) was also found able to produce hydrogen from CO and carbohydrates. Using starch as substrate, the phototrophic hydrogen production rates by *R. gelatinosus* were 7.8-11.3 ml/l/h and 7.0-17.0 ml/g/h (Mahakhan et al., 2005).

Table 1 also shows that several marine species are able to produce hydrogen from organic acids, sugars and PHB (poly- β -hydroxybutyrate). Among them, *Rhodovulum* sp. NKP160471R had the highest hydrogen production rate up to 713.0 ml/l/h from malate using a high light intensity of 1800 W/m² (Matsunaga et al. 2000). Other marine species produced hydrogen at rates ranging 3.0-68.6 ml/l/h (Ike et al., 1999; Kawaguchi et al., 2002; Maeda et al., 2003).

III.B. Mixed Cultures

Table 2 shows that very little information has been reported on hydrogen production by mixed cultures of phototrophic bacteria. Most of the hydrogen production rates ranged 4-10 ml/l/h, with a noticeable exception of 20.3 ml/l/h achieved using lactate

as substrate by a mixed sludge, in which only one phototrophic bacteria strain, *R. marinum* A-501 (99% similarity) was isolated (Ike et al., 1999). All cases in Table 2 were conducted in batch reactors with only one exception using a continuous reactor, in which a high rate of 17.4 ml/l/h was achieved (Zhang et al., 2002).

III.C. Co-cultures

Most phototrophic hydrogen-producing (PHP) bacteria use simple organic acids and sugars as substrate. Producing hydrogen from complex organic pollutants in municipal, agricultural and industrial wastewaters may require co-cultures of dark and photo fermentative bacteria. The former converts complex organic pollutants into acids and sugars, which subsequently become substrates to the latter for hydrogen production. Some of these dark fermentative bacteria may either be hydrogen producers, such as *Clostridium butyricum* (Zhu et al., 2001), and non-hydrogen producers, such as *Cellulomonas* (Odom and Wall, 1983), *Vibrio fluvialis* (Ike et al., 1999) and *Lactobacillus amylovorus* (Kawaguchi et al., 2001). Table 3 lists the parameters in hydrogen production by various co-cultures.

Studies have also been conducted for other kinds of bacteria to form co-cultures with PHP bacteria. *Halobacterium salinarum* produces protons upon illumination for PHP bacteria, resulting in an increase of hydrogen production by 4-6 folds (Zabut et al., 2006). *Vibrio fluvialis* T-522 was able to induce hydrogen production by *R. marinum* A-501 from acetic acid and ethanol via an unknown mechanism (Ike et al., 1999). Some co-culture may result in the increase of light conversion efficiency in hydrogen production (Kondo et al., 2002b)

III.D. Immobilized Cultures

A number of studies were conducted for immobilized PHP bacteria which may have several advantages over suspended bacteria, such as increasing cell density in the reactor, reducing washout, improving effluent quality (Tsygankov, 2001) and protecting cells from toxicity, such as NH_4^+ and heavy metals (Zhu et al., 2001).

Table 4 summarizes parameters of hydrogen production by immobilized cultures of PHP bacteria as in Tables 1-3, plus additional information such as the media and maximum hydrogen production rate based on irradiation area ($\text{ml}/\text{cm}^2/\text{h}$). Of all the tested media, agar and alginate gels were most common for cell entrapment. The hydrogen production rates ranged 0.14-0.35 $\text{ml}/\text{cm}^2/\text{h}$, and the volumetric rates were 50.0-127.0 $\text{ml}/\text{l}/\text{h}$. The specific rates of 140-696 $\text{ml}/\text{g}/\text{h}$ for the immobilized cells by agar are much higher than the 0.7-250.0 $\text{ml}/\text{g}/\text{h}$ reported for suspended cultures (Table 1). Adding other ingredients into the media might produce various effects: cationic polymer alleviated the inhibitory effect of NH_4^+ and chitosan increased hydrogen production rate by 20-30% (Zhu et al., 1999b). The main drawback of gels is that substrate needs to diffuse through the gel matrix, resulting in a decrease of the hydrogen production rate.

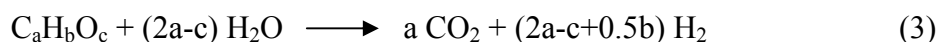
Porous glass (Tsygankov et al., 1994) and polyurethane form (Fedorov et al. 1998) have also been used as the support media for PHP bacteria. They are chemically stable, inert to microorganisms, and transparent to light. The hydrogen production rates of 210-310 $\text{ml}/\text{l}/\text{h}$ by these media were much higher than the 1-75 $\text{ml}/\text{l}/\text{h}$ for most of the suspended cultures (Table 1) and the 50-127 $\text{ml}/\text{l}/\text{h}$ for the PHP bacteria immobilized by agar or alginate.

III.E. Genetically Modified Cultures

A number of studies have been conducted for hydrogen production by genetically modified cultures. Results in Table 5 show that genetically removing uptake hydrogenase from *R. capsulatus* could increase its hydrogen production by 30-100% (Krahn et al., 1996; Ooshima et al., 1998; Kim et al., 2004), and mutating the light harvesting system of *R. sphaeroides* P3 might increase the hydrogen production rate by 50-150% (Vasilyeva et al., 1999; Kondo et al., 2002a).

IV. SUBSTRATES

Production of hydrogen from organic acids and sugars may be expressed as follows:



The efficiency of such process is often expressed by the ratio between the actual amount of hydrogen produced and the stoichiometric amount determined from Equation (3).

Results in Tables 1-5 show that most studies of photo-hydrogen production were conducted in batch reactors using organic acids as single substrate, including lactate, malate, acetate, butyrate, and even aromatic acids such as benzoate, cinnamate, mandelate, and benzoylformate (Fibler et al., 1995). Among the tested substrates, lactate and malate had better hydrogen yield than other acids. Using lactate as substrate, hydrogen yields of over 80% were achieved by suspended *R. capsulatus*

IR3 (He et al., 2005) and by *R. sphaeroides* GL-1 immobilized in polyurethane foam (Fedorov et al., 1998). Using malate as substrate, a yield of 68% was reported for *R. capsulatus* ST410 (Ooshima et al., 1998). Yields were generally lower using acetate and butyrate as substrate, likely due to the formation of intracellular PHB (Koku et al., 2002) which competed with hydrogen for electrons (Khatipov et al., 1998). Most of the yields from acetate and butyrate by the suspended pure cultures ranged only 8-20% (Table 1). *R. palustris* P4 (Oh et al., 2004) and *Rhodopseudomonas* sp. HCC2037 (Barbosa et al., 2001) had yields of about 70% from acetate, whereas *R. palustris* R1 could not produce hydrogen from butyrate (Barbosa et al., 2001). Yields of about 67% were also reported for acetate and butyrate by immobilized cultures (Mao et al., 1986).

Results in Tables 1-5 show that carbohydrates, such as glucose, sucrose, starch and cellobiose, had yields in general below 10%.

A few studies were conducted using mixed acids as substrate or treating the acids-rich effluent of dark fermentation. Using pure cultures, hydrogen yields ranging 33-46% were obtained by suspended cells with hydrogen production rates ranging 12.5-21.0 ml/l/h (Shi and Yu, 2005 and 2006). Higher hydrogen yields (53-64%) and production rates (79-115 ml/l/h) were achieved using immobilized pure cultures (Mao et al., 1986). Using mixed cultures, the yield ranged 12-22% (Zhang et al., 2002; Takabatake et al., 2004).

Several attempts were made to produce hydrogen by photo fermentation from actual wastewaters. Rates of hydrogen production were low (1-6 ml/l/h) when tested against

sugar refinery wastewater (Yiğit et al., 1999; Yetis et al., 2000) and olive mill wastewater (Eroğlu et al., 2004). Higher rates were obtained (respectively, 14.9 and 78.8 ml/l/h) treating a tofu wastewater by a suspended co-culture of *R. sphaeroides* and *Clostridium butyricum* (Zhu et al., 2002), and by immobilized *R. sphaeroides* (Zhu et al., 1999a).

V. OPERATIONAL PARAMETERS

Several operational parameters are crucial to the optimal production of hydrogen, including light source and light intensity, pH, temperature, substrates, nitrogen source, trace metal elements, and inhibitors.

V.A. Light Source and Light Intensity

Most of photo fermentative hydrogen production used light with a wavelength in the range of 400-950 nm (Akkerman et al., 2002). Various light sources have been used, including simulated sunlight (Wakayama et al., 1998), tungsten lamp (Nakada et al., 1995; Fascetti et al., 1998; Zhu et al., 2001), halogen lamp (Barbosa et al., 2001; Kim et al., 2004), and fluorescent lamp (Matsunaga et al., 2000). Some used monochromatic light by specific filters (Takabatake et al., 2004).

Light intensity may be measured by either W/m^2 or lux. The conversion between the two units varies substantially, depending on the wavelength of light (Neumann et al., 2003). Without knowing the specific wavelength, one may assume 1 W/m^2 is equivalent to 30-100 lux (Nakada et al., 1995; Ooshima et al., 1998; Ko and Noike,

2002). Most of the studies in Tables 1-5 used light intensity in the range of 100-300 W/m² (or 6-10 klux).

The reported optimum light intensity varied among species and even among strains of the same species. In general, the optimum light intensity was in the range of 30-100 W/m² or 5-8 klux. The reported optimum light intensities were 5 klux for *R. sphaeroides* O.U.001 (Sasikala et al., 1991), 28-32 W/m² for *R. sphaeroides* KD131 (Kim et al., 2006), 30 W/m² or more for *Rhodovulum* sp. (Matsunaga et al., 2000), 3 klux (35 W/m² given by the author) for *R. capsulatus* ST410 (Ooshima et al., 1998), and 6-8 klux for *R. palustris* (Yang et al., 2002).

High intensity of light may inhibit hydrogen production for some bacteria. The inhibitory intensities were reported as 400 W/m² for *R. sphaeroides* KD131 (Kim et al., 2006), and 9 klux for *R. palustris* (Yang et al., 2002). However, light intensities as high as 1800 W/m² did not cause any inhibitory effect for *Rhodovulum* sp. (Matsunaga et al., 2000), and 10 klux for *R. sphaeroides* O.U.001 (Sasikala et al., 1991).

The reported photo efficiency, which is percentage of photo energy radiated onto the reactor being utilized for the formation of hydrogen, was mostly below 10%. This is one of the drawbacks needs to be overcome for the further development of photo fermentative hydrogen production, unless the free sunlight is used. In a few exceptional cases, higher photo efficiencies (up to 35%) were achieved when using low intensity light (13-45 W/m²) (Akkerman et al. 2002). However, at such level of light intensity, hydrogen was produced at unrealistic rates about 90% lower than those

under the normal intensity of 1800 W/m².

In addition, the illumination pattern also affected hydrogen production by some PHP bacteria. Koku et al. (2003) found that more hydrogen was produced in reactors which were illuminated in on-off cycles, simulating the day-night pattern of solar radiation, than those under continuous illumination.

V.B. pH

The reported optimum pH varied among species: pH 7.2 for *R. sphaeroides* VM81 (Margaritis and Vogrinetz, 1983), pH 7.0-7.5 for *R. sphaeroides* O.U.001 (Sasikala et al., 1991; Sasikala et al., 1995), pH 7.4-7.6 for *R. sphaeroides* KD131 (Kim et al., 2004; Kim et al., 2006), and pH 8.5-9.0 for *R. capsulatus*, (Tsygankov and Laurinavichene, 1996). The reported optimal pH for mixed cultures were substrate dependent: pH 7.0-8.0 for acetate, and pH 8.0-9.0 for butyrate (Fang et al., 2005).

V.C. Temperature

Reported data showed that 30-40°C is in general the optimum range of temperature. The reported optimum ranges were 30-40°C for *R. sphaeroides* O.U.001 (Sasikala et al., 1991), 30-37°C for *R. palustris* (Yang et al., 2002), and 30°C for *R. capsulatus* (He et al., 2006).

V.D. Substrates

Effects of substrates concentration were studied mainly for organic acids. Using malate as substrate, the optimum concentrations were 30 mM for *R. sphaeroides* O.U.001 (Sasikala et al., 1991), and 60 mM for *R. capsulatus* ST410 (Ooshima et al.,

1998). Using lactate, the hydrogen production rate increased with concentration up to 50 mM for *R. sphaeroides* O.U.001 (Sasikala et al., 1991). Using acetate, the optimum concentrations were 30-50 mM for *R. palustris* (Yang et al., 2002) but hydrogen production was repressed completely at 100 mM of acetate. While another strain *R. palustris* P4 achieved similar rate and yield regardless of the acetate concentrations in the range of 12-55 mM (Oh et al., 2004). The optimum concentration of 11 mM was reported for a mixed phototrophic sludge using butyrate (Fang et al., 2005), and 39 mM of glucose for *R. sphaeroides* VM81 (Margaritis and Vogrinetz, 1983). Using benzoate as substrate, the optimum concentration was 3.0 mM for immobilized *R. palustris* (Fibler et al., 1995).

Substrates used for cell cultivation may also affect hydrogen production. Hillmer and Gest (1977b) found that *R. capsulatus* grown on C₄ dicarboxylic acids (i.e. malate, fumarate, and succinate) were able to produce hydrogen from these acids as well as lactate and pyruvate, but those grown on lactate, pyruvate or glycerol could not produce hydrogen from C₄ dicarboxylic acids.

V.E. Trace Metal Elements

Since photo heterotrophic hydrogen production is catalyzed by nitrogenase, which consists of a cofactor made of iron (Fe) and molybdenum (Mo), the availability of these two elements is of great significance. Hydrogenase in PHP bacteria is generally accepted as the metabolic antagonist of nitrogenase, assuming to function in the direction of hydrogen uptake (Koku et al., 2002). Nickel is necessary for the synthesis of hydrogenase (Doyle and Arp, 1988), implying that the presence of nickel may promote the hydrogenase synthesis and therefore inhibit hydrogen production.

Stimulation of phototrophic hydrogen production by the addition of Mo^{6+} and Fe^{2+} has been demonstrated by many studies (Kim et al., 1980; Krahn et al., 1996; Fascetti et al., 1998). The Mo^{6+} and Fe^{2+} concentrations commonly used for hydrogen production are 0.3 mg/l and 2.4 mg/l, respectively, as originally suggested by Ormerod et al. (1961) for *R. rubrum*. Studies on the concentration effect of Mo^{6+} and Fe^{2+} are still very limited. Kars et al. (2006) found that *R. sphaeroides* O.U.001 produced most hydrogen at 1.6 mg/l Mo^{6+} and 5.6 mg/l Fe^{2+} , and yet Lee and Yu (2005) found hydrogen production by *R. palustris* WP3-5 was independent of Mo^{6+} concentration. Yang et al. (2002) found that Fe^{3+} at 2.8 mg/l was optimal for hydrogen production by *R. palustris*, but significantly inhibited hydrogen production at 6.7 mg/l. Yang et al. (2002) also found that Ni^{2+} at 0.2-0.4 mg/l repressed hydrogen production completely.

V.F. Nitrogen Sources

Although NH_4^+ is the common N source for fermentation, it inhibits nitrogenase activity and thus cannot be used for phototrophic hydrogen production. An early study (Hillmer and Gest, 1977a) found that *R. capsulatus* favored glutamate, serine, and alanine among the 19 tested amino acids, as N source for hydrogen production. However, glutamate has remained as the most common source of N. Sasikala et al. (1995) found that high N/C ratios (2/3 or above) would completely inhibit hydrogen production due to the accumulation of NH_4^+ released from deamination of amino acids. The N/C ratio in feed solution in most studies was kept below 0.18, as used by Hillmer and Gest (1977a). On the other hand, Eroğlu et al. (1999) compared the hydrogen production by *R. sphaeroides* using glutamate and malate as N and C

sources, and found the optimal N:C ratio was 0.03 (corresponding to a molar malate:glutamate ratio of 15:2).

V.G. Inhibitors

Molecular O₂ and N₂, as well as NH₄⁺, are known inhibitors to phototrophic hydrogen production. Molecular O₂ adversely affects the nitrogenase activity and thus hydrogen production as found by Ooshima et al. (1998) for the *Rhodovulum* sp. and by Matsunaga et al. (2000) for *R. capsulatus*. The presence of 1-4% of O₂ reduced hydrogen production by 50% for two strains of *R. capsulatus* (Krahn et al., 1996). However, Koku (2002) found that such effect was irreversible for *R. sphaeroides*, whereas Hochman and Burris (1981) and Goldberg et al. (1987) found the effect reversible for *R. capsulatus* and *R. rubrum*, and for *R. sphaeroides*, respectively.

The presence of molecular N₂ inhibits the hydrogen formation enzymatic activity of nitrogenase (Ooshima et al., 1998). However, such an inhibitory effect seems to be reversible. Ormerod et al. (1961) found that hydrogen production by *R. rubrum* was completely inhibited by N₂, but the activity was fully recovered once N₂ was replaced by helium.

Ionic NH₄⁺ may stimulate hydrogen production activity in trace amounts but may cause inhibition at higher concentrations. Hydrogen production by the suspended culture of *Rhodopseudomonas* sp. from acetate was stimulated by 1 mM NH₄⁺, but was inhibited by 50% with 5 mM NH₄⁺ and 100% with 15 mM NH₄⁺ (Hoekema et al., 2002); however, such an inhibition effect appeared also to be reversible. Zhu et al. (2001) found that hydrogen production by the suspended culture of *R. sphaeroides*

RV using lactate was repressed 50% at 10 mM of NH_4^+ , whereas the immobilized *R. sphaeroides* had the highest hydrogen production with 5 mM NH_4^+ and was not inhibited by NH_4^+ at 10 mM (Zhu et al., 1999b). This suggests that immobilized cells are more resistant to the toxicity of NH_4^+ .

VI. REACTOR DESIGN

The key design concern is to maximize the surface-volume ratio of the reactor for uniform illumination (Ogbonna and Tanaka, 2001). Most studies on photo hydrogen production were conducted in laboratory scale in batches using either tubes (Margaritis and Vogrinetz, 1983), serum bottles (Fang et al., 2005), flat flasks (Zhu et al., 2001), water-jacketed columns (Eroğlu et al., 1999), or plate reactors (Kondo et al., 2002b; Kondo et al., 2006). A novel design using optical fibers to transmit light from an external source was demonstrated recently (Chen et al., 2006).

Continuous photobioreactors in columned and spherical configurations have been used for hydrogen production. These reactors were generally equipped with a water jacket for temperature control and operated in the complete-mix mode (Yetis et al., 2000; Zhang et al., 2002; Shi and Yu, 2006).

VII. OUTLOOK

Although the technical feasibility of producing hydrogen from organic substrates by photo fermentation has been demonstrated, the development of this technology is still at its infantile stage. Large scale production of hydrogen from wastewater using

sunlight as source of photo energy is still a remote target. Based on the review for over 100 related papers, it is obvious that some aspects are crucial for the further development of this technology and warrant further studies. Firstly, further research should be carried out using mixed cultures from environmental samples treating mixed substrates. Secondly, reactor designs should be improved for better capture of light, and operational parameters, such as the HRT, pH, and substrates concentration, should be further optimized. Thirdly, photo hydrogen production under daily on-off illumination of sunlight should be examined. And lastly, further studies should be conducted to combine dark and photo fermentations into a single package for hydrogen production from wastewater.

ACKNOWLEDGEMENTS

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The authors wish to thank the Hong Kong Research Grants Council for the financial support of this study (HKU 7106/04E and 7129/05E), and Ru Ying Li wishes to thank RGC for the research assistantship and HKU for the postgraduate studentship.

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Table 1. Hydrogen production by suspended cells of the pure culture of PHP bacteria

Microorganisms	Substrates	Reactor type	Max. H ₂ rate (ml/l/h)	Max. H ₂ rate (ml/g/h)	Yield (%)	Culture volume (ml)	Cell density (g/l)	Light source	Light intensity		Reference
									W/m ²	klux	
<i>R. sphaeroides</i> VM81	Glucose	Batch	2.2	3.5	3.5	11	0.64	Incandescent	10		Margaritis and Vogrinetz, 1983
<i>R. sphaeroides</i> RV	Lactate	Batch	240.0	171.0	19.6	30	1.30-1.50	Tungsten	720	40	Nakada et al., 1995
<i>R. sphaeroides</i> RV	Lactate	Batch	-	-	-	2	1.00	Halogen (800 and 850 nm)	80		Vasilyeva et al., 1999
<i>R. sphaeroides</i> RV	Glucose	Batch	75.0	250.0	17.0	200	0.30	Tungsten		8.5	Zhu et al., 2001
<i>R. sphaeroides</i> RV	Lactate	Batch	30	65.2	26.1	165	0.46	Tungsten	300		Kondo et al., 2002a
<i>R. sphaeroides</i> RV	Lactate	Batch	19.1	31.9	-	800	0.60	Tungsten	300		Kondo et al., 2006
<i>R. sphaeroides</i> RV	Acetate +propionate +butyrate	Batch	0.8 ml/h/vial	-	-	-	-	Incandescent	165	5	Ko and Noike, 2002
<i>R. sphaeroides</i> RV	VFAs from fermentation of fruit and vegetable wastes	Continuous (HRT 25h) (8-10 d)	48.0	100.0	-	1000	0.48	Tungsten		10	Fascetti et al., 1998
<i>R. sphaeroides</i> O.U.001	Malate	Batch	12.0	2.4	42.4	400	5.00	Tungsten	200		Eroğlu et al., 1999
<i>R. sphaeroides</i> O.U.001	Malate	Batch	8.0	10.0	36.0	400		Tungsten	150-250		Koku et al., 2003
<i>R. sphaeroides</i> O.U.001	Sugar refinery wastewater	Batch	6.4	-	-	50	-	N.S.	200		Yiğit et al., 1999
<i>R. sphaeroides</i> O.U.001	Sugar refinery wastewater	Batch	3.8	0.9	-	150	4.40	N.S.	200		Yetis et al., 2000

<i>R. sphaeroides</i> O.U.001	Sugar refinery wastewater +malate	Continuous (HRT 80d)	1.0	0.7	-	400	1.40	N.S.	200	Yetis et al., 2000	
<i>R. sphaeroides</i> O.U.001	Sugar refinery wastewater +malate	Continuous (HRT 32d)	3.0	3.1	-	400	0.97	N.S.	200	Yetis et al., 2000	
<i>R. sphaeroides</i> O.U.001	Olive mill wastewater	Batch	4.0	9.8	-	400	0.41	Tungsten	200	Eroğlu et al., 2004	
<i>R. sphaeroides</i> KD131	Malate	Batch	33.8	-	36.7	50	3.1-3.4 OD ₆₆₀	Halogen	8	Kim et al., 2004	
<i>R. sphaeroides</i> KD131	Lactate	Batch	16.7	-	18.1	50	2.8 OD ₆₆₀	Halogen	8	Kim et al., 2004	
<i>R. sphaeroides</i> KD131	Acetate	Batch	4.9	-	8.0	50	3.1 OD ₆₆₀	Halogen	8	Kim et al., 2004	
<i>R. sphaeroides</i> KD131	Glucose	Batch	7.6	-	4.1	50	3.64 OD ₆₆₀	Halogen	8	Kim et al., 2004	
<i>R. capsulatus</i> B10S	N.S.	Batch	74.0	-	-	1	2 OD ₆₀₀	N.S.	-	-	Krahn et al., 1996
<i>R. capsulatus</i> B100	Malate	Batch	37.7	-	25.0	5	-	Tungsten	6	Ooshima et al., 1998	
<i>R. capsulatus</i> B100	Acetate	Batch	26.2	-	53.0	5	-	Tungsten	6	Ooshima et al., 1998	
<i>R. capsulatus</i> IR3	Lactate	Batch	19.4	29.8	84.8	3000	0.65	Incandescent	-	-	He et al., 2005
<i>R. capsulatus</i> IR3	Lactate	Batch	52.5	105.0	68.2	1000	0.50	Incandescent	-	-	He et al., 2006
<i>R. capsulatus</i> JP91	Lactate	Batch	38.5	41.8	52.7	1000	0.92	Incandescent	-	-	He et al., 2006
<i>R. capsulatus</i> Z-1 (Growing cells)	Glucose	Batch	-	88.0	32.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	
<i>R. capsulatus</i> Z-1 (Growing cells)	Fructose	Batch	-	100.0	27.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	
<i>R. capsulatus</i> Z-1 (Growing cells)	Sucrose	Batch	-	60.0	6.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	

<i>R. capsulatus</i> Z-1 (Growing cells)	Lactate	Batch	-	130.0	72.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	
<i>R. capsulatus</i> Z-1 (Growing cells)	Pyruvate	Batch	-	130.0	68.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	
<i>R. capsulatus</i> Z-1 (Growing cells)	Malate	Batch	-	90.0	56.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	
<i>R. capsulatus</i> Z-1 (Growing cells)	Succinate	Batch	-	100.0	72.0	60	0.4 OD ₆₆₀	Incandescent	10.8	Hillmer and Gest, 1977a	
<i>R. capsulatus</i> Z-1 (Resting cells)	Lactate	Batch	75.0	75.0	-	2.5	1.0-1.2	Incandescent	10.8	Hillmer and Gest, 1977b	
<i>R. capsulatus</i> Z-1 (Resting cells)	Pyruvate	Batch	41.0	41.0	-	2.5	1.0-1.2	Incandescent	10.8	Hillmer and Gest, 1977b	
<i>R. capsulatus</i> Z-1 (Resting cells)	Malate	Batch	58.0	58.0	-	2.5	1.0-1.2	Incandescent	10.8	Hillmer and Gest, 1977b	
<i>R. capsulatus</i> Z-1 (Resting cells)	Fumarate	Batch	25.0	25.0	-	2.5	1.0-1.2	Incandescent	10.8	Hillmer and Gest, 1977b	
<i>R. capsulatus</i> Z-1 (Resting cells)	Succinate	Batch	71.0	71.0	-	2.5	1.0-1.2	Incandescent	10.8	Hillmer and Gest, 1977b	
<i>R. capsulatus</i>	Acetate +propionate +butyrate	Batch	14.7	19.1	32.6	150	0.77	N.S.	-	-	Shi and Yu, 2005
<i>R. capsulatus</i>	Acetate +propionate	Continuous (HRT 72 h) (20 d)	21.0	38.9	45.9	1500	0.54	N.S.	-	-	Shi and Yu, 2006
<i>R. capsulatus</i>	Acetate +propionate +butyrate	Continuous (HRT 72 h) (10 d)	17.0	37.8	45.0	1500	0.45	N.S.	-	-	Shi and Yu, 2006
<i>R. capsulatus</i>	Effluent from acidogenic H ₂ production reactor	Continuous (HRT 72 h) (10 d)	12.5	33.0	40.0	1500	0.38	N.S.	-	-	Shi and Yu, 2006
<i>Rhodobacter</i> strain 8703	Lactate	Batch	131.0	151.0	-	50	0.78- 0.96	N.S.	10	Mao et al., 1986	
<i>R. palustris</i> R1	Lactate	Batch	9.1	82.7	12.6	150	0.11	Halogen and tungsten	102	Barbosa et al., 2001	

<i>R. palustris</i> R1	Malate	Batch	5.8	52.7	36.0	150	0.11	Halogen and tungsten	102	Barbosa et al., 2001	
<i>R. palustris</i> R1	Butyrate	Batch	Nil	Nil	Nil	150	0.11	Halogen and tungsten	102	Barbosa et al., 2001	
<i>R. palustris</i> R1	Acetate	Batch	2.2	20.0	14.8	150	0.11	Halogen and tungsten	102	Barbosa et al., 2001	
<i>R. palustris</i>	Acetate	Batch	22.1	-	-	-	1.23 OD ₆₆₀	N.S.	6-8	Yang et al., 2002	
<i>R. palustris</i> P4	Acetate	Batch	1.6	9.8	60.0-70.0	50	0.17	N.S.	2.5	Oh et al., 2004	
<i>R. palustris</i> WP3-5	Acetate	Batch	8.7	3.0	25.0	500	2.90	halogen	95	Chen et al., 2006	
<i>R. palustris</i> WP3-5	Acetate	Batch	6.8	2.5	20.8	500	2.70	Optical fiber and halogen	95	Chen et al., 2006	
<i>R. palustris</i> WP3-5	Acetate	Batch	17.1	9.5	49.5	500	1.80	Optical fiber and halogen and tungsten	95	Chen et al., 2006	
<i>R. palustris</i> WP3-5	Butyrate	Batch	24.9	28.4	57.4	100	0.88	Tungsten	10	Chen et al., 2007	
<i>R. rubrum</i>	Lactate	Continuous (HRT 74h)	65.0	20.0	64.5	1000	3.0-3.5	Tungsten	300	Zürer and Bachofen, 1979	
<i>R. rubrum</i>	Malate	Batch	48.0	-	10.2	180	-	Tungsten	10	Miyake et al., 1982	
<i>Rubrivivax gelatinosus</i> SB24	Starch	Batch	7.8-11.3	7.0-17.0	-	23	-	-	Nil	10	Mahakhan et al., 2005
<i>Rhodopseudomonas</i> sp. HCC2037	Lactate	Batch	10.7	23.8	9.6	150	0.45	Halogen and tungsten	145	Barbosa et al., 2001	
<i>Rhodopseudomonas</i> sp. HCC2037	Malate	Batch	1.1	2.4	6.6	150	0.45	Halogen and tungsten	145	Barbosa et al., 2001	
<i>Rhodopseudomonas</i> sp. HCC2037	Butyrate	Batch	7.6	16.9	8.4	150	0.45	Halogen and tungsten	145	Barbosa et al., 2001	

<i>Rhodopseudomonas</i> sp. HCC2037	Acetate	Batch	25.2	56.0	72.8	150	0.45	Halogen and tungsten	145	Barbosa et al., 2001
<i>Rhodobium</i> <i>marinum</i> A-501	Glucose	Batch	5.3	-	7.2	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
<i>Rhodobium</i> <i>marinum</i> A-501	Maltose	Batch	3.3	-	4.5	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
<i>Rhodobium</i> <i>marinum</i> A-501	Sucrose	Batch	3.0	-	4.1	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
<i>Rhodobium</i> <i>marinum</i> A-501	Lactate	Batch	9.1	-	12.4	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
<i>Rhodobium</i> <i>marinum</i> A-501	Malate	Batch	5.7	-	7.8	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
<i>Rhodobium</i> <i>marinum</i> A-501	Lactate +algal extract	Batch	68.6	114.0	47.9	65	0.60	Tungsten	330	Kawaguchi et al., 2002
<i>Rhodobium</i> <i>marinum</i> A-501	Lactate	Batch	26.5	44.2	29.2	65	0.60	Tungsten	330	Kawaguchi et al., 2002
<i>Rhodovulum</i> sp. NKPB160471R	Malate	Batch	713.0	230.0	-	12	3.10	Fluorescent	1800	Matsunaga et al., 2000
<i>Rhodovulum</i> sp. NKPB160471R	Malate	Semi-batch (Micro- aerobic) (150 h)	26.7-31	8.6-10.0	-	500	3.10	Fluorescent	34.5	Matsunaga et al., 2000
<i>Rhodovulum</i> <i>sulfidophilum</i> WT	PHB	Batch	33.0	-	-	190	6.85 OD ₆₆₀	Incandescent	190	Maeda et al., 2003

Table 2. Hydrogen production by suspended cells of the mixed culture of PHP bacteria

Organisms	Substrates	Reactor type	Max. H ₂ rate (ml/l/h)	Max. H ₂ rate (ml/g/h)	Yield (%)	Culture volume (ml)	Cell density (g/l)	Light source	Light intensity (W/m ²)	Reference
Mixed culture Sludge BC1	Starch	Batch	9.6	-	13.0	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Glucose	Batch	4.9	-	6.6	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Maltose	Batch	4.3	-	5.9	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Cellobiose	Batch	5.3	-	7.2	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Sucrose	Batch	4.5	-	6.1	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Acetate	Batch	13.7	-	18.7	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Lactate	Batch	20.3	-	27.6	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Malate	Batch	6.5	-	8.8	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed culture Sludge BC1	Glycerol	Batch	3.9	-	5.3	65	0.6 OD ₆₆₀	Tungsten	330	Ike et al., 1999
Mixed phototrophic sludge culture	Synthetic wastewater (acetate +butyrate+ ethanol)	Continuous (HRT 25h) (30d)	17.4	5.6	12.0	450	3.10	Tungsten	90-150	Zhang et al., 2002
Mixed phototrophic sludge culture	Acetate	Batch	6.7	16.8	62.5	100	0.40	Tungsten	200	Fang et al., 2005
Mixed phototrophic sludge culture	Butyrate	Batch	5.3	13.2	37.0	100	0.40	Tungsten	200	Fang et al., 2005
Mixed culture of PSB	Acetate +propionate +butyrate	Batch	4.0	5.2	22.0	-	0.77	Blue light	-	Takabatake et al., 2004

Table 3. Hydrogen production by co-culture of PHP bacteria with other bacteria*

Organisms		Substrates	Max. H ₂ rate (ml/l/h)	Yield (%)	Culture volume (ml)	Cell density (g/l) (PHP/FB [#])	Light source	Light intensity W/m ² klux		Reference
PSB	Fermentative bacteria									
<i>R. capsulatus</i> B100	<i>Cellulomonas</i> sp. ATCC 21399	Cellulose	-	35.8	20	-	Incandescent	-	-	Odom and Wall, 1983
<i>R. capsulatus</i> ST410 (Hup ⁻ mutant)	<i>Cellulomonas</i> sp. ATCC 21399	Cellulose	-	51.7	20	-	Incandescent	-	-	Odom and Wall, 1983
<i>R. sphaeroides</i> RV (co-immobilization)	<i>Clostridium butyricum</i> IFO 3847	Glucose	41.0	4.1	200	1.5/1.3	Tungsten		8.5	Zhu et al., 2001
<i>R. sphaeroides</i> RV (co-immobilization)	<i>Clostridium butyricum</i> IFO 3847	Tofu wastewater	14.9	-	200	1.9/1.7	Tungsten		8.5	Zhu et al., 2002
<i>R. sphaeroides</i> O.U.001	<i>Halobacterium salinarum</i> S9	Malate	27.0	-	400	-	Tungsten	150		Zabut et al., 2006
<i>Rhodobium marinum</i> A-501	<i>Vibrio fluvialis</i> T-522	Algal starch	8.6	52.0	65	-	Tungsten	330		Ike et al., 1999
<i>Rhodobium marinum</i> A-501	<i>Lactobacillus amylovorus</i>	Algal starch in <i>D. tertiolecta</i>	38.0	60.8	65	0.6/0.5	Tungsten	330		Kawaguchi et al., 2001
<i>Rhodobium marinum</i> A-501	<i>Lactobacillus amylovorus</i>	Algal starch in <i>C. reinhardtii</i>	20.8	52.3	65	0.6/0.5	Tungsten	330		Kawaguchi et al., 2001

*All studies were in batch.

FB: Fermentative bacteria or other bacteria

Table 4. Hydrogen production by immobilized cultures of PHP bacteria

Organisms	Support materials	Substrates	Reactor type	Max. H ₂ rate (ml/cm ² /h)	Max. H ₂ rate (ml/l/h)	Max. H ₂ rate (ml/g/h)	Yield (%)	Culture volume (ml)	Cell density (g/l)	Light intensity		Reference
										W/m ²	klux	
<i>Rhodopseudomonas</i> strain 2604	2% agar	Butyrate	Batch	0.26	87.4	510	67.0	70	0.7-1.0	10	Mao et al., 1986	
<i>Rhodopseudomonas</i> strain 2613	2% agar	Acetate	Batch	0.25	86.7	506	67.0	70	0.7-1.0	10	Mao et al., 1986	
<i>Rhodopseudomonas</i> strain 2613	2% agar	Mixture of acetate, butyrate & lactate	Batch	0.34	115.2	672	64.0	70	0.7-1.0	10	Mao et al., 1986	
<i>Rhodopseudomonas</i> strain 2806	2% agar	Lactate	Batch	0.24	81.6	476	71.0	70	0.7-1.0	10	Mao et al., 1986	
<i>Rhodobacter</i> strain 8703	2% agar	Butyrate	Batch	0.32	110.1	642	67.0	70	0.7-1.0	10	Mao et al., 1986	
<i>Rhodobacter</i> strain 8703	2% agar	Lactate	Batch	0.35	119.3	696	77.0	70	0.7-1.0	10	Mao et al., 1986	
<i>Rhodobacter</i> strain 8703	2% agar	Mixture of acetate, butyrate & lactate	Batch	0.23	79.2	462	53.0	70	0.7-1.0	10	Mao et al., 1986	
<i>R. sphaeroides</i> RV	2% agar	Tofu wastewater	Batch	0.21	78.8	597	15.0	200	0.66	8	Zhu et al., 1999 a	
<i>R. sphaeroides</i> RV	2% agar	Glucose	Batch	0.14	50.0	167	13.6	200	1.5	8.5	Zhu et al., 2001	
<i>R. sphaeroides</i> RV	2% agar	Tofu wastewater	Batch	0.20	74.7	393	-	200	1.9	8.5	Zhu et al., 2002	
<i>R. sphaeroides</i> RV	1% chitosan + 2% agar	Lactate	Batch	0.24	90.0	180	36.0	200	2.5	8.5	Zhu et al., 1999 b	

<i>R. sphaeroides</i> RV	0.5% chitosan + 2% agar	Lactate	Batch	0.23	85.0	170	34.0	200	2.5	8.5	Zhu et al., 1999 b
<i>R. sphaeroides</i> RV	2% agar	Lactate	Batch	0.19	70.0	140	25.0	200	2.5	8.5	Zhu et al., 1999 b
<i>R. sphaeroides</i> RV	Porous glass	Succinate	Continuous	0.065	310.0	-	55.0	-	11.2	300	Tsygankov et al., 1994
<i>R. sphaeroides</i> GL-1	Polyurethane foam	Lactate	Continuous (HRT 43.5 h) (35 d)	0.17	210.0	-	86.0	200	-	300	Fedorov et al., 1998
<i>R. palustris</i> DSM 131	Sodium alginate (50 µm bead)	Benzoate	Batch	-	112.0	6.7	88.0	30	10.0	10	Fißler et al., 1995
<i>R. palustris</i> DSM 131	Sodium alginate (50 µm bead)	Cinnamate	Batch	-	127.0	7.6	86.0	30	10.0	10	Fißler et al., 1995
<i>R. palustris</i> DSM 131	Sodium alginate (50 µm bead)	Mandelate	Batch	-	71.7	4.3	60.0	30	10.0	10	Fißler et al., 1995
<i>R. palustris</i> DSM 131	Sodium alginate (50 µm bead)	Benzoylformate	Batch	-	65.0	3.9	57.0	30	10.0	10	Fißler et al., 1995

Table 5. Hydrogen production by mutants of PHP bacteria*

Organisms	Substrates	Max. H ₂ rate (ml/l/h)	Max. H ₂ rate (ml/g/h)	Yield (%)	Culture volume (ml)	Cell density (g/l)	Light source	Light intensity		Reference
								W/m ²	klux	
<i>R. sphaeroides</i> P3 (mutant of RV)	Lactate	-	-	-	2	1.0	Halogen (800 and 850 nm)	80		Vasilyeva et al., 1999
<i>R. sphaeroides</i> MTP4 (Reduced pigment mutant of RV)	Lactate	46.0	100.0	40.0	165	0.46	Tungsten	300		Kondo et al., 2002a
<i>R. sphaeroides</i> MTP4 (Reduced pigment mutant of RV)	Lactate	21.2	35.4	-	800	0.60	Tungsten	300		Kondo et al., 2006
<i>R. sphaeroides</i> KD131 <i>Hup</i> ⁻ / <i>Phb</i> ⁻ mutant	Malate	45.8	-	49.9	50	2.9 OD ₆₆₀	Halogen		8	Kim et al., 2004
<i>R. sphaeroides</i> KD131 <i>Hup</i> ⁻ / <i>Phb</i> ⁻ mutant	Lactate	25.0	-	27.2	50	1.8 OD ₆₆₀	Halogen		8	Kim et al., 2004
<i>R. sphaeroides</i> KD131 <i>Hup</i> ⁻ / <i>Phb</i> ⁻ mutant	Acetate	7.7	-	12.6	50	1.4 OD ₆₆₀	Halogen		8	Kim et al., 2004
<i>R. sphaeroides</i> KD131 <i>Hup</i> ⁻ / <i>Phb</i> ⁻ mutant	Glucose	12.4	-	6.7	50	1.9 OD ₆₆₀	Halogen		8	Kim et al., 2004
<i>R. capsulatus</i> B10S <i>Hup</i> ⁻ mutant	N.S.	94.1	-	-	1	2 OD ₆₀₀	N.S.	-	-	Krahn et al., 1996
<i>R. capsulatus</i> ST-410 (<i>Hup</i> ⁻ mutant of B100)	Malate	100.0	140.0	68.0	5	-	Tungsten		6.6	Ooshima et al., 1998
<i>R. capsulatus</i> ST-410 (<i>Hup</i> ⁻ mutant of B100)	Acetate	41.0	-	84.0	5	-	Tungsten		6	Ooshima et al., 1998
<i>R. capsulatus</i> ST-410 (<i>Hup</i> ⁻ mutant)	Malate	59.0	107.0	8.1	550	0.55	Tungsten	60		Katsuda et al., 2000

*All studies were in batch.