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# Hydrogen from wastewater by photocatalytic and photoelectrochemical treatment

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## Abstract

In recent years, the intensification of human activities has led to an increase in waste production and energy demand. The treatment of pollutants contained in wastewater coupled to energy recovery is an attractive solution to simultaneously reduce environmental pollution and provide alternative energy sources. Hydrogen represents a clean energy carrier for the transition to a decarbonized society. Hydrogen can be generated by photosynthetic water splitting where oxygen and hydrogen are produced, and the process is driven by the light energy absorbed by the photocatalyst. Alternatively, hydrogen may be generated from hydrogenated pollutants in water through photocatalysis, and the overall reaction is thermodynamically more favourable than water splitting for hydrogen. This review is focused on recent developments in research surrounding photocatalytic and photoelectrochemical hydrogen production from pollutants that may be found in wastewater. The fundamentals of photocatalysis and photoelectrochemical cells are discussed, along with materials, and efficiency determination. Then the review focuses on hydrogen production linked to the oxidation of compounds found in wastewater. Some research has investigated hydrogen production from wastewater mixtures such as olive mill wastewater, juice production wastewater and waste activated sludge. This is an exciting area for research in photocatalysis and semiconductor photoelectrochemistry with real potential for scale up in niche applications.

Keywords: Hydrogen production, wastewater, photocatalysis, photoelectrochemical cell

## 1. Introduction

The current society is based on a linear production route, where the extraction of raw matter follows its industrial conversion into products, and its disposal as waste. This linear practice creates long-term problems because resources are limited and inefficiently used. The impact of

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3 this approach includes climate crisis, water pollution and reduction of biodiversity. Therefore, it is  
4 necessary to adopt different strategies conforming to the circular economy concept, where products  
5 and materials are in the economy as long as possible.  
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9 Wastewater has a great potential for resource recovery, being a source of nutrients such as  
10 phosphorus and nitrogen, materials including precious metals, and also a potential source for  
11 energy recovery. Conventional wastewater treatment plants are energy intensive. Energy can be  
12 extracted from wastewater in diverse forms, including electricity, heat or fuels, as methane or  
13 hydrogen. Biogas production by anaerobic digestion is one of the most utilized methods for energy  
14 recovery from wastewater [1]. In this process, bacteria degrade the organic waste in the absence  
15 of oxygen to produce biogas, a gas mixture mostly composed of methane and carbon dioxide.  
16 Anaerobic digestion has been and is widely used in wastewater treatment plants around the world.  
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20 Hydrogen production is another promising approach to energy recovery from wastewater.  
21 Hydrogen is considered as clean energy carrier for the transition to a decarbonized society fuelled  
22 by renewable energy. Its use in combustion or fuel cells generates only water resulting in zero  
23 carbon emissions and the high gravimetric heating value makes hydrogen a competitive energy  
24 carrier. In 2019, the International Renewable Energy Agency (IRENA) reported that more than  
25 95% of hydrogen production comes from fossil fuel based processes, such as steam-methane  
26 reforming and oil and coal gasification [2]. This fact highlights the urgent need to develop  
27 alternative and sustainable H<sub>2</sub> production processes, which may include recovery from wastewater.  
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31 Hydrogen can be generated from wastewater using biological processes. Wastewater has a high  
32 organic content making it a good candidate for hydrogen production via fermentation. Possible  
33 biohydrogen production methods include photo-fermentation and dark fermentation [3]. In photo-  
34 fermentation, photosynthetic bacteria powered by sunlight transform organic compounds into  
35 hydrogen and CO<sub>2</sub>. Dark fermentation is a complex process in which several groups of bacteria  
36 participates in a series of biochemical reactions to convert organic substrate into biohydrogen.  
37 Often, dark fermentation is coupled to photo-fermentation; the organic acids, by-products of dark  
38 fermentation, are then converted to hydrogen by the photosynthetic bacteria during photo-  
39 fermentation [4]. An alternative bio-based technology to recover energy from wastewater is the  
40 use of Microbial Fuel Cells (MFC). MFC use bacteria on the anode to oxidize the organic matter  
41 and inject electrons, where these electrons can be used to produce electricity or hydrogen at the  
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3 cathode. MCF are considered a promising technology for wastewater treatment and energy  
4 recovery; however the slow electron transfer, low power generation, membrane fouling and low  
5 rate of microbes growth impede the rapid scaling-up of MFC [5,6].  
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9 Among non-biological processes, an interesting approach is the use of photocatalysis to produce  
10 hydrogen from wastewater. Photoexcitation of the photocatalyst results in charge carrier formation  
11 with the necessary electrochemical reduction potentials to drive hydrogen evolution. In 1972,  
12 Fujishima and Honda reported for the first time photoelectrolytic water splitting to produce  
13 hydrogen and oxygen using a UV excited single crystalline TiO<sub>2</sub> electrode [7]. Since then, research  
14 in the photocatalysis field gained attention producing a substantial number of studies. While  
15 extensive research has been carried out in either photocatalytic hydrogen production or  
16 degradation of organic compounds, only a limited number of studies focus on hydrogen production  
17 from the degradation of components in wastewater. Therefore, this review is aimed to emphasise  
18 the relevance of this approach, as promising application for the simultaneous recovery of energy  
19 and the removal of pollutants from wastewater.  
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29 The present article starts with an overview of the fundamentals, materials and the parameters used  
30 to evaluate the performance of photocatalytic processes (section 2) and photoelectrochemical cells  
31 (section 3). The following section reviews hydrogen production from several wastewater  
32 compounds, which are categorized in groups, using both photocatalysis and photoelectrochemistry  
33 (section 0). This section focuses in discussing materials used, possible mechanisms and  
34 performance of these processes. Finally, this review concludes with a critical evaluation of the  
35 current limitations on this field and future opportunities.  
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## 41 42 **2. Photocatalysis**

### 43 44 *2.1 Fundamentals*

45 In photocatalysis, a semiconductor is irradiated with photons with energy equal to or greater than  
46 the band gap energy, resulting in the excitation of electrons from the valence band (VB) to the  
47 conduction band (CB). The photo-excited electron leaves a positively charged hole in the VB.  
48 These charge carriers are referred to as an electron-hole pair. The charge carriers can recombine  
49 in the semiconductor bulk dissipating energy as heat or light or they can migrate to the surface of  
50 the semiconductor. At the surface, they can undergo charge transfer processes driving redox  
51 reactions with chemical species which are adsorbed at the surface of the photocatalyst.  
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Photocatalysis has been widely studied for the degradation of organic pollutants, extensive information can be found in previous reviews [8–11]. The organic pollutants can either undergo direct oxidation by holes, indirect oxidation by reactive oxygen species including hydroxyl radicals, or they may be transformed by a reductive route involving CB electrons. The most employed electron acceptor in photocatalytic oxidation reactions is molecular oxygen since it is abundant in the air and is reasonably soluble in aqueous solutions. The oxygen is reduced by the CB electrons to form the superoxide radical anion ( $O_2^{\bullet-}$ ). Subsequent reduction reactions lead to  $H_2O_2$ ,  $\bullet OH$ , and eventually  $H_2O$ . A representation of this process is shown in figure 1(a).

Photocatalysis has also been investigated for hydrogen production through water splitting, as detailed described in several reviews [12–15]. In this application, the photogenerated holes are used to oxidize the water molecules to evolve oxygen, while the photo-generated electrons in the CB reduce protons and evolve hydrogen, as shown in figure 1(b). However, photocatalytic hydrogen production from water splitting is a challenging reaction because it is thermodynamically unfavourable ( $\Delta G^\circ = +237 \text{ kJ mol}^{-1}$ ) requiring a high energy input and the transfer of four electrons. It should be recognised that technically, uphill thermodynamic processes are photosynthetic, however, to avoid confusion, in this review both uphill and downhill reactions will be referred as photocatalytic. Hydrogen production from the oxidation of other compounds with reactions requiring less energy or being thermodynamically favourable ( $\Delta G^\circ < 0$ ) have also been investigated. This is schematically represented in figure 2. These compounds can donate electrons and scavenge the VB holes while also acting as a source of protons. There are many compounds present in wastewater that could act as a hydrogen source.

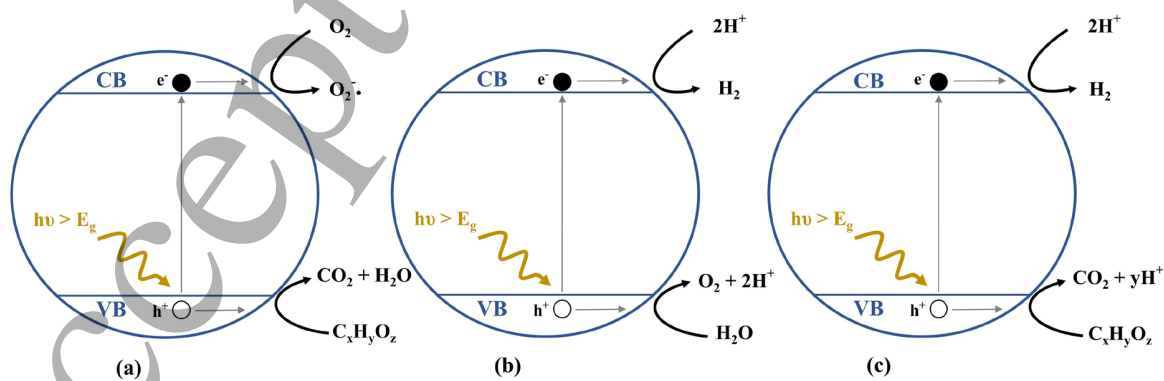


Figure 1. Schematic representation of photocatalytic process. (a) Photocatalytic degradation of organic pollutants with oxygen as the electron acceptor. (b) Photocatalytic water splitting. (c) Photocatalytic oxidation of pollutant with H<sub>2</sub> evolution as the reduction reaction.

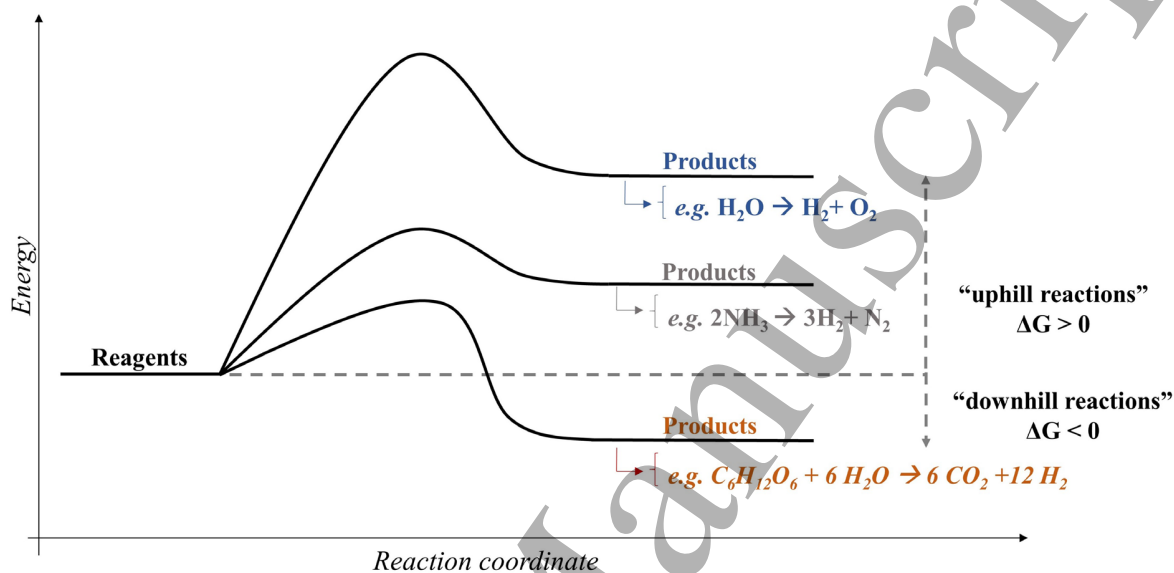
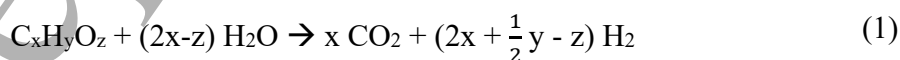


Figure 2. Thermodynamic energy diagram with examples for hydrogen production from water, ammonia, and glucose.

Most studied compounds have been organics, but this is also possible with inorganic compounds as e.g. ammonia. In this application, the photo-generated holes are used to oxidize the unwanted compounds, which can take place through direct oxidation or indirect oxidation via hydroxyl radicals ( $\bullet\text{OH}$ ). The photo-generated electrons reduce the protons to form hydrogen. A schematic representation of this process is shown in figure 1(c), with the oxidation of a generic organic compound. The photocatalytic oxidation of organic substances to form hydrogen is also referred as photoreforming and it follows the general equation given in (1).



The ability of a semiconductor to perform the desired redox reactions depends on the band gap energy and the band edge potentials for the VB and the CB. For the reactions to be thermodynamically possible, the CB edge potential should be more negative than the desired reaction reduction potential and the VB edge potential should be more positive than the desired

reaction oxidation potential. In the water splitting reaction, the CB should be more negative than the hydrogen evolution reaction (HER) potential (0 V vs. NHE at pH 0), and the VB should be more positive than the oxygen evolution potential (+1.23 V vs NHE at pH 0). While in the reactions with oxidation of wastewater compounds, the conduction band needs to be more positive than the oxidation potential of the waste compounds and pollutants. These potentials are more negative than the potential for water oxidation, requiring less energy for the overall reaction. The CB and VB of several semiconductor materials, together with the oxidation and reduction potential of these reactions are given in figure 3.

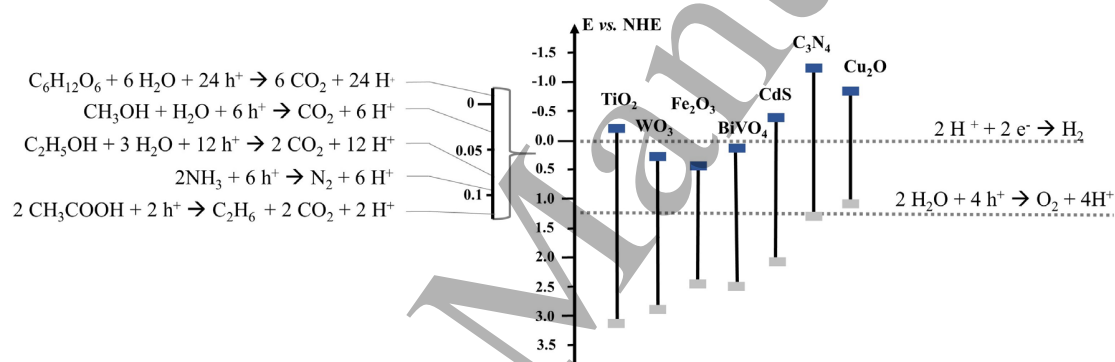


Figure 3. Band gap position of semiconductors in relation to oxidation and reduction reactions from wastewater compounds. Energy levels were previously reported in [16–22].

The ideal semiconductor material for photocatalytic hydrogen production from wastewater compounds would have the following general requirements: suitable band edges position, good light absorption, efficient charge transport, chemical and photochemical stability, low overpotentials for the desired reduction and oxidation reactions, low cost and being abundant. It is important to consider that almost half of the incident solar energy on the earth's surface is in the visible region ( $400 \text{ nm} < \lambda < 800 \text{ nm}$ ), and therefore, for solar applications the photocatalyst should be able to utilise both the UV and visible photons.

## 2.2 Materials

While a wide range of materials have been investigated for photocatalytic hydrogen production [12–15], the present review will focus on the materials reported for  $\text{H}_2$  production coupled to the

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3 oxidation of pollutants found in wastewater. Titanium dioxide is the most reported photocatalyst  
4 to investigate the coupling of H<sub>2</sub> production to the degradation of compounds found in wastewater  
5 [23–30]. Other materials as cadmium sulphide [31,32] and graphitic carbon nitride [33,34] have  
6 also been reported for H<sub>2</sub> production from wastewater compounds.  
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11 Titanium dioxide (TiO<sub>2</sub>) is employed in a wide variety of fields, ranging from energy applications  
12 such as hydrogen production and CO<sub>2</sub> reduction, to environmental applications as water treatment,  
13 air purification and water disinfection [35]. TiO<sub>2</sub> exists as three different polymorphs: anatase,  
14 rutile and brookite. Its properties include high photo-activity, low cost, low toxicity and good  
15 chemical and thermal stability. Nevertheless, it suffers from having a high electron-hole  
16 recombination and a large band gap. TiO<sub>2</sub> band gap is 3.2 eV for anatase, 3.0 eV for rutile, and  
17 ~3.2 eV for brookite [35]. This wide band gap limits the light absorption to the ultraviolet range,  
18 which just accounts for 4-5 % of the solar spectrum, consequently, limiting its practical  
19 application.  
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28 Developments to improve light absorption of TiO<sub>2</sub> include doping, metal deposition, dye  
29 sensitization and coupled semiconductors [16]. Non-metal doping has been extensively  
30 researched, being nitrogen one of the most promising non-metal dopants that has achieved visible  
31 light absorption [36]. Nitrogen is easily inserted in the TiO<sub>2</sub> structure since it has a high stability,  
32 small ionization and its atomic size is similar to oxygen [37]. Other promising non-metal dopants  
33 are carbon and sulphur [38,39]. Alternatively, the generation of oxygen rich TiO<sub>2</sub> has been reported  
34 to produce an increase in the Ti-O-Ti bond strength and a upward shift in the VB, achieving visible  
35 light absorption [40]. Doping with metals as chromium, cobalt, vanadium and iron has also been  
36 reported to improve the light absorption [16]. Dye sensitization has been considered as one of the  
37 most effective strategies to extend the spectral response into the visible region, benefiting from the  
38 knowledge of dye sensitized solar cells. Moreover, coupling TiO<sub>2</sub> with other semiconductors has  
39 also resulted in an improvement of the light absorption and a reduction of the recombination losses  
40 [41].  
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51 A commercially available TiO<sub>2</sub> product, Degussa (Evonik) P25, has been often used as a  
52 benchmark in research. It contains a combination of the polymorphs anatase and rutile with  
53 proportions of around 80 % anatase and 20 % rutile. This configuration enhances the photoactivity  
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3 since the rutile phase, which has a more positive conduction band potential, can act as electron  
4 sink for the photogenerated electrons of the anatase phase [16].  
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8 When TiO<sub>2</sub> is used for HER, usually metal co-catalysts are added. Since the work function of noble  
9 metals is typically larger than TiO<sub>2</sub>, the photogenerated electrons transfer from the semiconductor  
10 CB to the metal [35]. Pt has been one of the most used co-catalysts for HER since it has the largest  
11 work function among the noble metals, creating a stronger electron trapping ability and has a low  
12 activation energy for proton reduction [16,35]. Pt co-catalyst ability strongly depends in its particle  
13 size and loading [35].  
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18 Cadmium sulphide (CdS) is a widely researched visible light photocatalyst. It has been  
19 investigated in diverse applications, such as hydrogen production, carbon dioxide reduction to  
20 hydrocarbons or pollutants degradation [20]. CdS is characterized by a narrow bandgap of 2.4 eV,  
21 which enables the absorption of light until 516 nm [20]. It exhibits good photochemical properties  
22 and quantum efficiency [42,43]. However, it suffers from photo-corrosion, since the  
23 photogenerated holes react with the sulphur ions oxidizing them to sulfur [44]. CdS low stability  
24 makes difficult its application in industry. Some of the strategies to improve CdS stability and  
25 inhibit photo-oxidation include the addition of surface protective layers, constructing  
26 heterojunctions and combining them with microporous and mesoporous materials [31,45].  
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35 Graphitic carbon nitride (g-C<sub>3</sub>N<sub>4</sub>) has received lot of attention as visible light photocatalyst, and  
36 it has been reported to be a promising photocatalyst for a diverse number of applications including  
37 H<sub>2</sub> production [46]. g-C<sub>3</sub>N<sub>4</sub> is usually produced by thermal condensation of nitrogen-rich  
38 precursors. Its polymeric nature allows the modification of properties such as morphology,  
39 conductivity and electronic structure which modifies the bandgap energy and bandgap edges  
40 potential position [21]. g-C<sub>3</sub>N<sub>4</sub> photocatalytic activity and efficiency have been improved using  
41 several strategies. Heteroatom doping and copolymerization have been employed to modify the  
42 electronic band structure to enhance light absorption [47]. Moreover, the heterojunction with other  
43 semiconductors as CdS [48] or TiO<sub>2</sub> [49] have been reported to achieve an improved separation of  
44 the photogenerated charges [21].  
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### 52 *2.3 Efficiency*

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54 The photocatalytic performance can be evaluated using quantum efficiency. The quantum  
55 efficiency or yield is defined as the useful photo-conversion events per absorbed photons at a  
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3 determined wavelength. The useful events are usually calculated by the reaction rate. This is given  
4 in (2) where  $r$  is the reaction rate given in number of molecules converted per second, and  $\Phi_{pa}$   
5 is the flux of absorbed photons expressed as number of photons per second. However, it is  
6 challenging to determine the absorbed photons in the semiconductor. Therefore, the external or  
7 apparent quantum efficiency, which is also referred as photonic yield, is usually used instead [50].  
8 It can be defined as the useful events per incident photons in the system at a determined  
9 wavelength. This expression is given in (3), where  $r$  is the reaction rate given in number of  
10 molecules converted per second and  $\Phi_{pi}$  is the flux of incident photons expressed as number of  
11 photons per second. The incident photons can be measured using radiometric or actinometric  
12 procedures. Moreover, the external quantum efficiency takes into account the efficiency of the  
13 overall process including the efficiency of the material absorbing photons as well as catalysing the  
14 reaction and the efficiency of the reactor design [50].  
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$$QE(\lambda) = \frac{r}{\Phi_{pa}} \quad (2)$$

$$EQE(\lambda) = \frac{r}{\Phi_{pi}} \quad (3)$$

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34 If one is using a polychromatic irradiation source then the Formal Quantum Efficiency (FQE)  
35 should be reported, normally integrating the number of photons which can be utilised by the  
36 semiconductor in question. Of course, for many semiconductors the true solar efficiency will be  
37 very low due to only a small proportion of the solar spectrum being utilised.  
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42 Additionally, the performance of a photocatalytic hydrogen production process can also be  
43 evaluated using the solar-to-hydrogen conversion efficiency ( $\eta_{STH}$ ), which relates chemical  
44 hydrogen energy produced to the solar energy. This expression is shown in (4), where  $\Phi_{H_2}$  is the  
45 hydrogen rate in  $\text{mol s}^{-1} \text{m}^{-2}$ ,  $G_{H_2}^\circ$  the Gibbs free energy of hydrogen formation and  $P$  is the photon  
46 flux in  $\text{mW cm}^{-2}$  measured for a light source with a spectra equal to air mass global (AM) 1.5 [51].  
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$$\eta_{STH} = \left[ \frac{\Phi_{H_2} \cdot G_{H_2}^\circ}{P} \right]_{AM\ 1.5G} \quad (4)$$

### 3. Photoelectrochemical cells

#### 3.1 Fundamentals

An approach to enhance the efficiency of photocatalysis is the use of electrochemically assisted photocatalysts in a photoelectrochemical cell (PEC). In this configuration, the oxidation and reduction reactions are performed by two different electrode materials that are connected through an external circuit. The oxidation is driven by the holes in the (photo)anode, while the electrons travel from the photoanode through the external circuit to the (photo)cathode, where the reduction reaction takes place. This process is schematically represented in figure 4. When a photoelectrochemical cell is utilized to produce a fuel (e.g. hydrogen) from solar energy it can be referred as photosynthetic cell. Similarly, when the photoelectrochemical cell is employed to produce electricity from the photodegradation of substances, it can be defined as photo fuel cell [52]. In systems where wastewater compounds are being oxidized in a PEC to generate H<sub>2</sub>, depending on the thermodynamics of reaction, the system can also produce electricity and therefore being a combination of both cells; not clearly defined as one or the other. Moreover, a system without applied bias, where hydrogen is produced by a flow of current, could also be considered a photo fuel cell.

Photoelectrochemical cells can be used with different configurations, i.e. semiconductor photoanode with metallic cathode, semiconductor photocathode with metallic anode, or photoanode with photocathode. These cells are driven by the potential difference between the Fermi levels of the two electrodes. For a typical n-type semiconductor photoanode, the Fermi level is close to the CB while for a typical p-type semiconductor photocathode the Fermi level is close to the VB [53]. If the photoelectrochemical cell uses a dark anode or cathode, these potentials are ideally dependent on the reaction oxidation and reduction reaction potentials, respectively. If the reaction oxidation and reduction potentials have the right positions with respect to the CB and VB, the cell produces electric power in open circuit voltage. When this is not the case, an external voltage can be applied to drive the reactions.

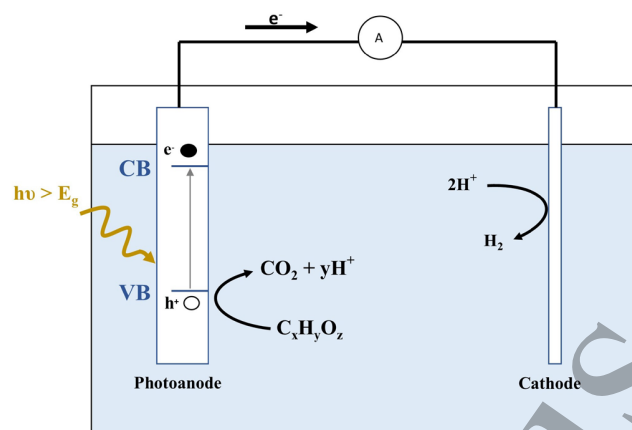


Figure 4. Schematic representation of a photoelectrochemical cell, containing a photoanode and a dark cathode, for the oxidation of a generic organic and  $H_2$  production.

With electrochemically assisted photocatalysis, an external electrical bias can be applied to assist the reactions. This may allow the use of semiconductors photoanodes with more positive CB potentials than the  $H^+/H_2$  reaction and which would not drive HER purely photocatalytically.

### 3.2 Materials

Titanium dioxide is the most used photoanode material for  $H_2$  production from wastewater compounds [54–57]. Other photoanode materials that have also been used for  $H_2$  production are tungsten trioxide, bismuth vanadate and hematite [58–60]. Concerning the cathode material, platinum is widely used [54,55,61,62], while cuprous oxide is a common choice for photocathode [57].

#### 3.2.1 Photoanodes

Titanium dioxide ( $TiO_2$ ), is as well the most used semiconductor material for photoanodes. Its properties and applications have been described in the previous section. When compared with other photoanodes semiconductor materials as tungsten trioxide, bismuth vanadate or hematite, titanium dioxide shows good charge transport properties and a very high hole diffusion length, which is in the order of  $10^4$  nm [58]. However,  $TiO_2$  has one of the lowest theoretical solar-to-hydrogen (STH) conversion efficiency just accounting for around 2.2 %, due to its excitation being limited to the UV region [59]. One of the strategies studied to improve activity and reduce

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3 recombination losses, is to synthesize one- or two-dimensional nanostructures which increases the  
4 specific surface area and decreases internal resistance. A very popular approach is the nano-  
5 engineering of  $\text{TiO}_2$  to form either dispersed or aligned self-organised nanotubes (TNT) [63].  
6 Other used strategies include non-metal doping, co-catalyst deposition, dye sensitization and  
7 coupled semiconductors as explained previously [16].  
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12 Tungsten trioxide ( $\text{WO}_3$ ), is a very popular metal oxide semiconductor used for photoanodes. It  
13 has been extensively researched for water splitting applications. It has a bandgap of 2.5-2.8 eV,  
14 absorbing light in the visible range up to 500 nm which accounts for 12 % of the solar radiation  
15 on earth surface [60]. Its theoretical STH conversion efficiency is around 4.8% [58], and it has a  
16 modest hole diffusion length of around 150 nm [58]. Moreover, its conduction band is positioned  
17 at positive potentials of around +0.4 V vs. NHE [17], therefore a bias is necessary to drive the  
18 HER. Unfortunately, its stability is limited to acidic environment [58]. Some strategies to improve  
19 the activity of  $\text{WO}_3$  include the enhancement of light absorption with anion doping as C [64] or N  
20 [65] or forming heterojunctions with other semiconductors as  $\text{WO}_3/\text{BiVO}_4$  [66].  
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29 Bismuth vanadate ( $\text{BiVO}_4$ ), is the most popular visible light absorption semiconductor used as  
30 photoanode, it attracted interest for water-splitting applications.  $\text{BiVO}_4$  occurs in three  
31 polymorphs, from which monoclinic scheelite is the one being used as photoanode. It has a  
32 bandgap of 2.4 eV, a high theoretical STH conversion efficiency of 9.1% [59] and its conduction  
33 band potential is located slightly under than the HER potential [67]. However, it suffers from an  
34 extensive electron-hole recombination and a low charge mobility, consequently a bias is always  
35 necessary to obtain significant photocurrents [59]. In order to increase  $\text{BiVO}_4$  carrier concentration  
36 doping with elements as Mo or W has been studied [68,69]. Other strategies to improve  $\text{BiVO}_4$   
37 activity include the loading of co-catalysts as Co-Pi [70] to decrease the bias potential and help  
38 the oxidation reaction or the heterojunction with other semiconductors as  $\text{SnO}_3$  or  $\text{WO}_3$  to have a  
39 more efficient electron-hole separation [71,72].  
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49 Hematite ( $\alpha\text{-Fe}_2\text{O}_3$ ), is considered a very promising metal oxide photoanode since it has a narrow  
50 bandgap of around 2 eV, allowing to absorb light beyond 600 nm [59]. Therefore, its maximum  
51 theoretical STH conversion efficiency is around 15% [19]. Moreover,  $\alpha\text{-Fe}_2\text{O}_3$  presents a good  
52 chemical stability and it is inexpensive and abundant. Its conduction band is situated at positive  
53 potentials of around 0.4 V vs NHE [19], therefore, it is necessary to apply a bias to drive hydrogen  
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3 production. Nevertheless, it has a very low hole diffusion length of around 2-4 nm and a low  
4 electron mobility which limits its performance [60]. Strategies to improve  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> conductivity  
5 and activity include, doping with elements as W, Mo and Nb [73–75], loading of co-catalysts as  
6 Co-Pi or Ni(OH)<sub>2</sub> [55,76] or surface passivation with Al<sub>2</sub>O<sub>3</sub> [77].  
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### 10 11 3.2.2 Photocathodes

12 Contrary to the case of photoanodes, the choice of p-type materials for photocathodes is limited  
13 due to their low stability in contact with the electrolyte [78]. Some strategies to improve the  
14 performance of the photocathode include the use of protective layers that improve stability and the  
15 deposition of co-catalysts to enhance the reduction ability [79–81].  
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20 Cuprous oxide (Cu<sub>2</sub>O), is a popular photocathode choice, it has a band gap of 2 eV and a theoretical  
21 STH conversion efficiency of 18% [80]. Its conduction band is well positioned for water reduction,  
22 around 0.7 V vs NHE more negative than hydrogen evolution potential [22]. However, the  
23 potentials for reduction from Cu<sub>2</sub>O to Cu and oxidation to CuO are within the band gap, reducing  
24 its stability [82]. There are several research studies that had improved its stability adding protective  
25 layers as ZnO [79]. Moreover, co-catalysts as Pt had been added to enhance the reduction activity  
26 [80].  
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32 Copper based chalcogenide semiconductors have also been proposed as promising photocathodes  
33 for hydrogen production [83]. One of them is CuIn<sub>x</sub>Ga<sub>1-x</sub>Se<sub>2</sub> (CIGS) which has a tuneable  
34 composition, with a band gap ranging from 1 eV to 1.7 eV and a large absorption coefficient [81].  
35 Their activity have been enhanced adding protective layers and co-catalysts such as Pt [84].  
36 However, CIGS include In and Ga which are scarce and expensive elements. Another type of  
37 chalcogenide photocathode is Cu<sub>2</sub>ZnSnS<sub>4</sub> (CZTS), which has earth abundant elemental  
38 constituents, high absorption coefficient and small band gap, however; it suffers from low long-  
39 term stability [85]. The research to improve its activity has also focused into surface modification,  
40 adding protecting layers as TiO<sub>2</sub> and co-catalysts as Pt [81].  
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### 49 3.2.3 Dark cathode electrocatalysts

50 The selection of a cathode for hydrogen evolution reaction benefits from an extensive research in  
51 the electrochemistry field. HER involves the adsorption of a proton on the electrocatalyst surface  
52 and the desorption of hydrogen. For this reason, following Sabatier principle, the optimal catalytic  
53 activity will be achieved with a catalyst that achieves intermediate binding energy between the  
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3 substrate and the catalyst [86]. The catalyst activity is as well dependent on the pH of the  
4 electrolyte, and in general, HER activities in alkaline electrolyte are lower than in acid.  
5 Consequently, the majority of the research is done in acid environment. For HER, the catalyst  
6 closer to the optimum intermediate binding energy is Pt. Platinum has generally the best  
7 performance as hydrogen production catalyst, it has a low overpotential and high reaction rates in  
8 acidic environment [61]. Pt foil and wires, together with Pt supported carbon are the most common  
9 cathodes used in the studies for H<sub>2</sub> production from driven photoelectrochemical oxidation of  
10 substances in wastewater.  
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17 Other catalysts with a good performance are Ru, Rh, Ir and Pd. However, all these noble metal  
18 catalysts, together with Pt, have a high cost and they are scarce, which makes challenging their  
19 large-scale application. Different approaches have been widely researched to find electrocatalysts  
20 with low cost and good performance. Two strategies that have been used to improve activity and  
21 reduce the cost of using noble metal catalysts are nanostructuring the catalyst to achieve a large  
22 surface to volume ratio, and forming alloys which reduce the catalyst loading [87,88].  
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29 Non-noble metal alloys have also been used for HER, Ni-based electrodes are preferred cathodes  
30 for hydrogen production in basic environment as Ni-Mo [88]. Transition metals chalcogenides as  
31 carbides and phosphides have also showed HER activity. Chalcogenides as MoS<sub>2</sub> showed activity  
32 for HER due to their sulphided Mo-edges with and overpotential close to Pt [89]. Similarly, WS<sub>2</sub>  
33 also demonstrates HER activity [90] as well as their selenides forms MoSe<sub>2</sub> and WSe<sub>2</sub> [91].  
34 Tungsten carbides such as WC and W<sub>2</sub>C, exhibit promising potential as HER catalysts [92].  
35 Phosphides as CoP and Ni<sub>2</sub>P are among the most HER active non-noble electrocatalysts[93,94].  
36 Alternatively, non-metals electrocatalysts options have also been explored as heteroatom doped  
37 graphene nanosheets [94] or carbon nitride [95].  
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### 45 *3.3 Efficiency*

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47 When evaluating the performance of photoelectrochemical cells, the external quantum efficiency  
48 is also referred as Incident Photon to Current Efficiency (IPCE), and the number of successful  
49 events can be evaluated by the photo-electrical current generated. This expression is given in (5),  
50 where  $\lambda$  is the wavelength of irradiation in nm, J is the photocurrent density given in mA cm<sup>-2</sup>, P  
51 is the photon flux in mW cm<sup>-2</sup> at a particular  $\lambda$ , h is Plank's constant and c is the speed of light in  
52 vacuum [53].  
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$$EQE(\lambda) = IPCE(\lambda) = \frac{\Phi_e}{\Phi_{pi}} = \frac{J \cdot hc}{\lambda \cdot P_\lambda} \quad (5)$$

Moreover, when evaluating the performance of photoelectrochemical cells,  $\eta_{STH}$  can also be determined from the photocurrent density generated. This expression is shown in (6) where  $J$  is the photocurrent density given in  $\text{mA cm}^{-2}$ ,  $V$  is the required potential in  $V$  derived from Gibbs free energy,  $\eta_f$  is the HER faradaic efficiency and  $P$  is the light power in  $\text{mW cm}^{-2}$  measured with a light source with a spectra equal to air mass global (AM) 1.5 [51]. It is important to note that  $J$  needs to be measured between the working and counter electrode in a 2 electrode PEC configuration. No bias potential should be applied in the evaluation of  $\eta_{STH}$ . Whenever a bias potential is applied between working and counter electrode to drive the reaction, the Applied Bias Photon to Current Conversion Efficiency (ABPE) can be derived, as shown in (7) [51]. In this expression  $V_{bias}$  is the applied voltage in  $V$ , which is subtracted from the required potential derived from Gibbs energy.

$$\eta_{STH} = \left[ \frac{J \cdot V \cdot \eta_f}{P} \right]_{AM\ 1.5G} \quad (6)$$

$$ABPE = \left[ \frac{J \cdot (V - V_{bias}) \cdot \eta_f}{P} \right]_{AM\ 1.5G} \quad (7)$$

For wastewater treatment applications, an UV source is commonly used as oppose to solar irradiation; therefore the power coming from the sun should be replaced by the power of the UV source.

#### 4. H<sub>2</sub> production from wastewater

Wastewater includes every water stream that has been polluted by human utilization, therefore, its chemical composition varies greatly depending on its origin. Domestic wastewater, which derives from urban areas, is generally rich in microorganism, organic materials, metals, and nutrients as phosphorous or nitrogen [96]. These effluents are usually treated at municipal wastewater



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3 treatment plants. On the contrary, industrial effluents are diverse, being originated by very  
4 different processes. Some industrial wastewaters have a similar chemical composition than  
5 domestic wastewater and can be treated in urban wastewater treatment plants, while other  
6 industrial effluents contain substances that need a specific and complex treatment process, as  
7 persistent organics, antibiotics or metals [97]. Finally, agricultural activities generate wastewater  
8 with a high content of nitrogen compounds, due to excessive use of fertilizers and intensive  
9 farming [98], although agricultural wastewater normally cannot be collected and treated.

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16 These wastewaters, originated by human activities, need to be treated to avoid pollution and protect  
17 the ecosystems. Therefore, coupling the production of hydrogen with the removal of pollutants  
18 represents a promising option to recover energy from wastewater and at the same time managing  
19 the water pollution issue. This section describes the studies that produced hydrogen coupled to the  
20 degradation of wastewater compounds, including the materials used and the possible mechanisms.  
21 The reviewed wastewater substances include nitrogen compounds, saccharides, phenolic  
22 compounds, alcohols, organic acids, aldehydes, and complex mixtures from oil mill wastewater,  
23 juice production wastewater and sludge from wastewater treatment plants.

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4.1 Nitrogen compounds

Ammonia and urea, along with nitrates and nitrites, contribute to nitrogen pollution. Nitrogen pollution of water has deleterious effects including eutrophication and toxicity to the organisms living in the water body. The hazardous concentration of nitrogen in wastewater originate from diverse sources, as intensive farming and excessive fertilizer use [98]. Additionally, high nitrogen concentrations can also be found in either domestic and municipal sewage sludge and in wastewater from some industries [99].

In water, un-ionized ammonia ( $\text{NH}_3$ ) exists in pH dependent equilibrium with ionized ammonium ( $\text{NH}_4^+$ ), having a pKa of 9.25, when the pH is lower than the pKa,  $\text{NH}_4^+$  is the major form and when the pH is higher than the pKa is  $\text{NH}_3$  the major form. Therefore, one of the research focuses has been to determine which of the forms would have a higher photocatalytic oxidation rate. Several studies have revealed that ammonia in neutral form presents better oxidation rates compared to ionized ammonium [23,100,101]. Nemoto *et al.* investigated the pH effect in the photocatalytic ammonia oxidation, testing a pH range from 0.68 to 13.7 [23]. The study reports that the evolution of gaseous products ( $\text{N}_2$  and  $\text{H}_2$ ) increased between the pH 9 and 10 and peaked

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3 at pH around 11, due to higher oxidation rates with neutral ammonia. Zhu *et al.* reported how the  
4 oxidation rates obtained were proportional to the initial concentration of  $\text{NH}_3$  and not the total  
5 content of  $\text{NH}_3$  and  $\text{NH}_4^+$  [100]. From this study, it was concluded that high oxidation rates are  
6 obtained when ammonia is in neutral form, even if better photocatalytic activity could be expected  
7 with positively ionized  $\text{NH}_4^+$  and a negative photocatalyst surface charge, which occurs when the  
8 pH is higher than the photocatalyst point of zero charge and lower than the ammonium pKa. Wang  
9 *et al.* compared the photocatalytic activity in acidic, basic and neutral environment using g- $\text{C}_3\text{N}_4$   
10 as photocatalyst and reported higher rate of photocatalytic ammonia oxidation in basic solutions  
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The most studied photocatalyst for ammonia oxidation has been  $\text{TiO}_2$  [23,102–104], covering how  
the co-catalyst material affects the activity and product selectivity [23,102–104] and determining  
the possible reaction mechanism on  $\text{H}_2$  production from ammonia decomposition [103]. Nemoto  
*et al.* compared the activity of  $\text{TiO}_2$  loaded with  $\text{RuO}_2$ , Pt and both  $\text{RuO}_2$  and Pt as co-catalysts for  
photocatalytic ammonia oxidation and hydrogen production [23]. The results showed that the  $\text{N}_2$   
gas produced was similar for all the co-catalysts; however, the  $\text{H}_2$  production varied significantly.  
The photocatalyst loaded with Pt achieved the highest  $\text{H}_2$  production and an external quantum  
yield of 5.1 % at 340 nm, while the system with both co-catalysts produced a small amount of  $\text{H}_2$ .  
The system loaded with  $\text{RuO}_2$  did not produce any  $\text{H}_2$ , showing that  $\text{RuO}_2$  cannot reduce protons  
to form hydrogen. Altomare and Selli studied how the conversion and selectivity of ammonia  
oxidation to  $\text{N}_2$  would be affected by the deposition of noble metals (Pt, Pd, Au and Ag) on the  
 $\text{TiO}_2$  photocatalyst [102]. The experiments showed that all the metal-modified photocatalysts had  
better catalytic performance than the bare  $\text{TiO}_2$ , with the exception of  $\text{Au}/\text{TiO}_2$ . The loaded  
photocatalyst that showed higher ammonia removal was  $\text{Ag}/\text{TiO}_2$  and the one that showed better  
selectivity towards  $\text{N}_2$  was  $\text{Pd}/\text{TiO}_2$ . This latter study did not link the oxidation of ammonia to  $\text{H}_2$   
production. Yuzawa *et al.* studied the mechanism of decomposition of ammonia to produce  
dinitrogen and hydrogen using  $\text{TiO}_2$  photocatalyst loaded with Pt, Rh, Pd, Au, Ni and Cu [103]. Pt  
presented the best activity with high production rate of  $\text{H}_2$  and  $\text{N}_2$  and Cu the worse. The study  
concluded that the metal with larger work function would easily accept the photo-excited electrons  
to produce hydrogen. The mechanism proposed consisted in the predominant adsorption of  
ammonia to the Lewis acid site and some to the hydroxyl groups in  $\text{TiO}_2$ . The  $\text{TiO}_2$  is irradiated  
generating holes and electrons, where the holes migrate to the surface and the electrons to the Pt

site. The photogenerated holes oxidize the adsorbed  $\text{NH}_3$  to form amide radicals and protons, while the amide radicals can produce hydrazine. The hydrazine could produce diazene that would be decomposed to form  $\text{N}_2$  and  $\text{H}_2$ . The photogenerated electrons reduce the protons to form hydrogen in Pt [103]. This mechanism is represented in figure 5. Shiraishi *et al.* investigated the photocatalytic hydrogen production from ammonia using  $\text{TiO}_2$  loaded with Au and Pt [104]. Pt-Au/ $\text{TiO}_2$  showed a growth in hydrogen production rate compared to Pt/ $\text{TiO}_2$ , suggesting that alloying Au to Pt resulted in a decrease of the Schottky barrier height at the interface between metal and  $\text{TiO}_2$ . The catalyst with the highest  $\text{H}_2$  production rates consisted in a homogeneous mixture of 10 % mol of Au and 90 % mol of Pt loaded on  $\text{TiO}_2$ .

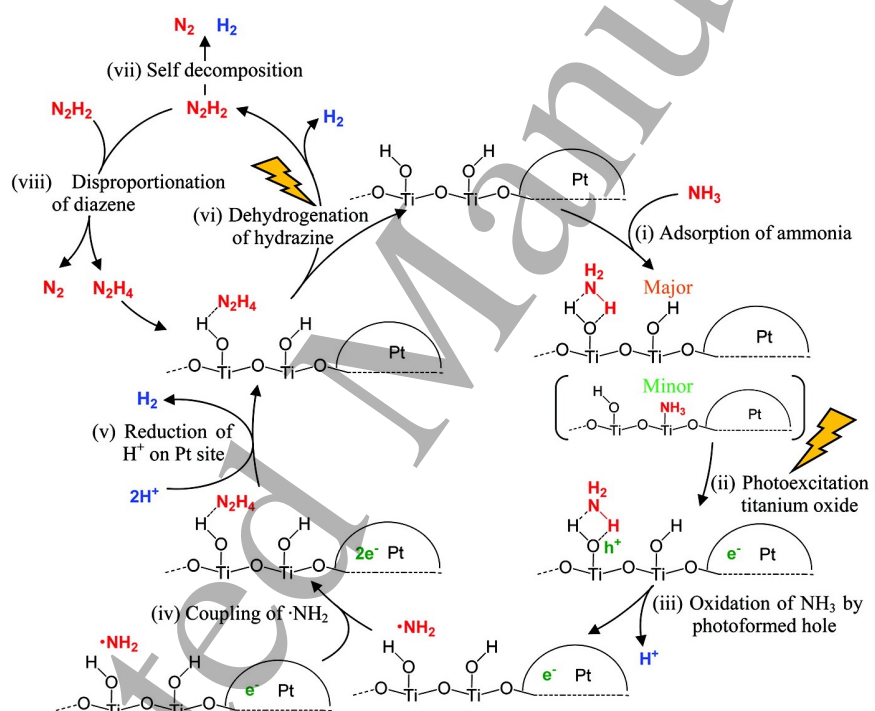


Figure 5. Suggested mechanism for photocatalytic ammonia degradation using Pt loaded on  $\text{TiO}_2$ . Figure has been reprinted from reference [103] with permission from the American Chemical Society.

Photocatalytic ammonia oxidation has also been reported using metal free photocatalyst. Wang *et al.* used an atomic single layer g- $\text{C}_3\text{N}_4$  as photocatalyst, achieving an ammonia removal of 80% of the initial concentration [101]. Both hydroxyl radicals and photogenerated holes were suggested

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3 to be responsible for the ammonia oxidation; in this study ammonia oxidation was not coupled to  
4 H<sub>2</sub> production.  
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7 The number of research papers reported on ammonia oxidation using photoelectrochemical cells  
8 is reduced compared to photocatalysis [54,105]. Wang *et al.* used highly ordered TiO<sub>2</sub> nanotube  
9 arrays as a photoanode and Pt foil as cathode [105], reporting an ammonia removal of 99.9%  
10 under an applied bias of 1.0 V (not coupled to H<sub>2</sub> production). Kaneko *et al.* used nanoporous TiO<sub>2</sub>  
11 film as photoanode, formed by P25 deposited on FTO glass and a Pt foil as a cathode [54]. The  
12 experiments showed a 150  $\mu\text{A cm}^{-2}$  photocurrent and a production of 194 ml of H<sub>2</sub> and 63 ml of  
13 N<sub>2</sub> after 2 hours with no bias applied under a pH of 14.1.  
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17 The reported studies of H<sub>2</sub> production driven by photocatalytic or photoelectrochemical oxidation  
18 of urea are scarce and their main focus is proving the feasibility of the process [24,55,106]. They  
19 include the study of surface modification and co-catalyst loading. Moreover, a comparison of the  
20 H<sub>2</sub> production rate from oxidation of urea, ammonia and formamide has also been studied [56].  
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24 Kim *et al.* investigated the effect of dual surface photocatalyst modification in the production of  
25 hydrogen and oxidation of urea [24]. TiO<sub>2</sub> modified with both a noble metal, Pt, and an anion  
26 adsorbate [24]. The results showed that F-TiO<sub>2</sub>/Pt achieved higher H<sub>2</sub> production rates than  
27 Pt/TiO<sub>2</sub>, besides, F-TiO<sub>2</sub> did not show any H<sub>2</sub> production, highlighting the combined effect of  
28 surface anions and metal deposits to reduce charge recombination and improve electron transfer.  
29 Moreover, the effect of other anions as Cl<sup>-</sup>, ClO<sup>-</sup> and Br<sup>-</sup> was studied, resulting in only F<sup>-</sup> to have  
30 an enhancement effect, Cl<sup>-</sup> and ClO<sup>-</sup> had no effect and Br<sup>-</sup> inhibited the hydrogen production. These  
31 results were explained by the surface complexation among acidic Ti(IV) sites and basic anions,  
32 which is dependent on the hardness of the anions, being only F<sup>-</sup> the one that has higher hardness  
33 than OH<sup>-</sup>. Furthermore, experiments with deuterated urea were performed, showing that H<sub>2</sub>  
34 production comes mainly from water molecules while urea acts as an electron donor.  
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38 Wang *et al.* studied the feasibility of hydrogen production driven by urea or urine oxidation in a  
39 photoelectrochemical cell [55]. In this work, the suitability of two photoanodes was studied, TiO<sub>2</sub>  
40 nanowires and  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> nanowires, both loaded with Ni(OH)<sub>2</sub> as urea oxidation co-catalyst. Pt was  
41 used as counter electrode. The viability of solar driven urea oxidation with Ni/TiO<sub>2</sub> as photoanode  
42 was reported using an unbiased cell, producing a current density of 0.35 mA cm<sup>-2</sup>. Moreover, the  
43 feasibility of using directly urine was also studied, resulting in comparable results to urea,  
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3 highlighting the possibility of driving the production of hydrogen with the oxidation of urine. The  
4 effect of loading  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> with Ni(OH)<sub>2</sub> was studied, showing a negative shift in the onset potential  
5 of 400 mV, suggesting that Ni(OH)<sub>2</sub> is an efficient catalyst for urea oxidation. However, the use  
6 of  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> as photoanode required an external bias due to the low position of its conduction band.  
7 Xu *et al.* investigated as well the role of Ni(OH)<sub>2</sub> as a co-catalyst in the photoelectrochemical  
8 oxidation of urea, not coupled to the production of hydrogen [106], by using a photoanode formed  
9 by Ti-doped  $\alpha$ -Fe<sub>2</sub>O<sub>3</sub> and loaded with Ni(OH)<sub>2</sub>. The addition of Ni(OH)<sub>2</sub> reduced the onset  
10 potential by 100 mV and increased the photocurrent density by 4 times, showing the enhanced  
11 effect of the use of Ni(OH)<sub>2</sub> as urea oxidation co-catalyst.  
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19 Pop *et al.* focused their study in the comparison of the hydrogen production rates driven by  
20 oxidation of three nitrogen compounds found in wastewater: ammonia, urea and formamide [56].  
21 The cell configuration combined a nanoparticulate TiO<sub>2</sub> photoanode and a mixture of carbon paste  
22 dispersing platinum nanoparticles as cathode in the same electrode. This configuration was  
23 unbiased and used under UV illumination. The detected hydrogen production after 4 hours was  
24 about 30, 140 and 240  $\mu$ mol in presence of ammonia, formamide and urea, respectively. From  
25 these results, urea proved to be the best choice for photoelectrochemical hydrogen production.  
26 Additionally, a cell configuration with a separated photoanode and cathode, applying 0.5 V bias  
27 was also tested. The results from the two configurations were compared after 50 min, in which the  
28 biased configuration reported a H<sub>2</sub> production rate of 2.7  $\mu$ mol min<sup>-1</sup> while the unbiased  
29 configuration reported a rate of 1.4  $\mu$ mol min<sup>-1</sup>, highlighting the improved charge separation  
30 induced by the use of a bias.  
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#### 41 4.2 Saccharides

42 Different saccharides compounds can be found wastewater; among them, cellulose is commonly  
43 found in domestic wastewater and effluents from industries as the paper industry [107].  
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47 Kawai and Sakata demonstrated the feasibility of producing hydrogen from Saccharides  
48 (C<sub>6</sub>H<sub>12</sub>O<sub>6</sub>)<sub>n</sub>, as saccharose (n=2), starch (n  $\approx$  100) and cellulose (n  $\approx$  1000 to 5000), using a  
49 photocatalyst formed by RuO<sub>2</sub>/TiO<sub>2</sub>/Pt. A quantum yield of 1 % at 380 nm was reported for  
50 cellulose in 6 M NaOH [108]. Moreover, Kondarides *et al.* studied the hydrogen production from  
51 the photocatalytic reforming of several compounds including cellulose using an Pt/TiO<sub>2</sub>  
52 photocatalyst, proving the potential of cellulose for H<sub>2</sub> production [25]. Speltini *et al.* investigated  
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3 the photocatalytic hydrogen production from cellulose using a Pt/TiO<sub>2</sub> photocatalyst [109]. The  
4 study showed higher H<sub>2</sub> production rates with neutral pH and reported a H<sub>2</sub> production of 54 μmol  
5 under UV-A irradiation. A degradation mechanism was also reported suggesting that cellulose  
6 depolymerizes and converts into glucose and other water-soluble products. Caravaca *et al.*  
7 researched the photocatalytic H<sub>2</sub> production from cellulose using different metals as co-catalysts  
8 loaded in TiO<sub>2</sub>. The H<sub>2</sub> production was reported highest with Pd and lowest with Ni and Au,  
9 following the trend Pd > Pt > Ni ~ Au [110]. Even the H<sub>2</sub> production using Ni as co-catalyst was  
10 lower compared to the noble metals Pd and Pt, it was in the same magnitude, highlighting the  
11 possibility of using a no noble metal as co-catalyst. Moreover, the study suggested the possibility  
12 of the hydrolysis of cellulose taking place during photo irradiation to produce glucose, which could  
13 follow different pathways to produce hydrogen.  
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23 The photoreforming of glucose, which is proposed to be an intermediate in the cellulose  
24 photoreforming process has been reported in several studies [25,26,111–113]. Kondarides *et al.*  
25 studied the hydrogen production from the photocatalytic reforming glucose using an Pt/TiO<sub>2</sub>  
26 photocatalyst, reporting an external quantum efficiency of 63 % at 365 nm [25]. Fu *et al.* studied  
27 the effect of different parameters as pH and co-catalyst material and proposed a mechanism for the  
28 hydrogen production from photocatalytic reforming of glucose using a metal loaded photocatalyst  
29 [26]. The study reported the effect of different co-catalysts loaded in TiO<sub>2</sub>, showing all of them a  
30 better activity than the bare TiO<sub>2</sub>; the best activity was obtained using Pd and Pt and the worse  
31 with Ru and Au, following the trend Pd > Pt > Au ≈ Rh > Ag ≈ Ru. Moreover, the variation of pH  
32 over a wide range resulted in an increasing H<sub>2</sub> production rate with increasing pH, with a plateau  
33 region from pH 5 to 9 and maximum peak at pH 11. The pK<sub>a</sub> of glucose is around 12.3; therefore,  
34 higher rates of glucose oxidation are produced with glucose in its molecular form. In the proposed  
35 mechanism, the glucose is adsorbed preferentially in the uncoordinated Ti atoms through its  
36 hydroxyl group; it dissociates and then it is oxidized by a photogenerated hole. The radicals  
37 generated attack other glucose molecules, forming R-CHOH, which are deprotonated and further  
38 oxidized to [R-COOH]<sup>-</sup> by the radical •OH. Lastly, [R-COOH]<sup>-</sup> species are photo-oxidized by a  
39 hole to generate CO<sub>2</sub> via a photo-Kolbe reaction [26]. This mechanism is presented in figure 6.  
40 Chong *et al.* investigated the glucose photoreforming mechanism using Rh/TiO<sub>2</sub> photocatalyst,  
41 reporting the production of arabinose, erythrose, glyceraldehyde, gluconic acid and formic acid  
42 (together with CO and CO<sub>2</sub> gas) [111]. In the suggested mechanism, glucose is oxidised into  
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arabinose, then further oxidised into erythrose and ultimately into glyceraldehyde. These oxidation reactions take place through  $\bullet\text{OH}$  radicals, which leads to the generation of formic acid and hydrogen. Subsequently, formic acid is converted into CO or CO<sub>2</sub>. Imizcoz and Puga studied photocatalytic hydrogen production from glucose using TiO<sub>2</sub> loaded with different metals as Au, Ag, Pt and Cu [112]. The study reported a catalyst efficiency following the trend Pt>Au>Cu>Ag, without significant differences between Cu and Au, proposing Cu as an inexpensive co-catalyst for hydrogen production. Bahadori *et al.* researched the hydrogen production from glucose photoreforming using CuO or NiO loaded TiO<sub>2</sub> as photocatalyst [113]. The highest hydrogen production yield reported was 9.7 mol g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup> using 1 wt% CuO on P25.

Other semiconductor materials as WO<sub>3</sub> and  $\alpha\text{-Fe}_2\text{O}_3$  have also been studied using a photoelectrochemical cell for hydrogen production from photoreforming of glucose. Esposito *et al.* reported how a thin film WO<sub>3</sub> photoanode presented a good photocatalytic activity for H<sub>2</sub> production from glucose photoreforming using a tandem cell device [114]. Wang *et al.* investigated the possibility of using Ni(OH)<sub>2</sub> as co-catalyst for glucose oxidation (not coupled to H<sub>2</sub> production) in a photoelectrochemical cell, reporting an increased activity for Ni(OH)<sub>2</sub> loaded in  $\alpha\text{-Fe}_2\text{O}_3$  [62].

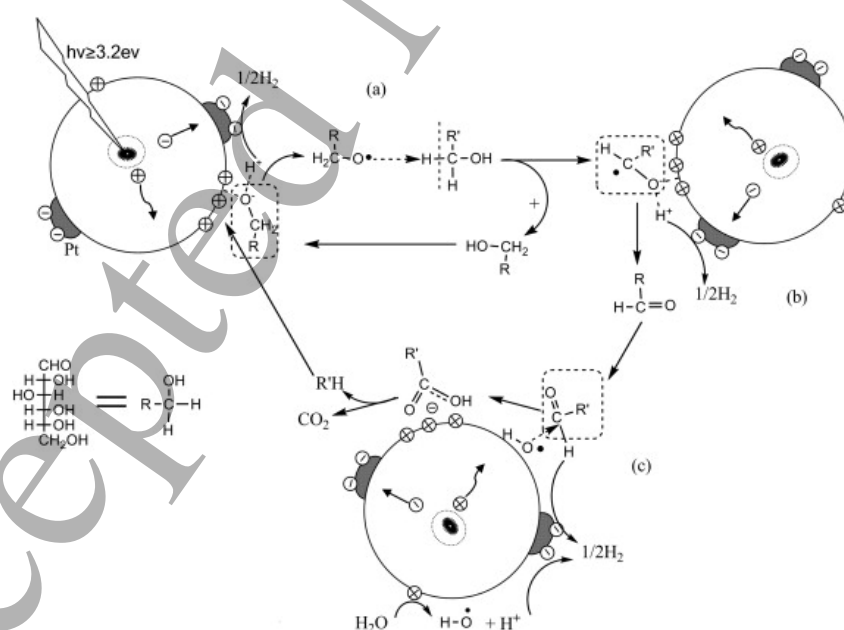


Figure 6. Proposed mechanism for photoreforming of glucose on Pt loaded TiO<sub>2</sub>. This figure has been reprinted from reference [26] with permission from Elsevier.

### 4.3 Phenolic compounds

Phenolic compounds are found in significant quantities in wastewater from effluents of several industries as oil refining, petrochemicals, resin manufacturing and pulp, but also in agricultural and domestic wastewaters [97,115]. Phenolic compounds are considered toxic and its discharge without treatment produces harmful effects in the aquatic systems [116]. The photocatalytic degradation of phenolic compounds has been widely studied [117]. However, only few cases coupled the photocatalytic oxidation of phenolic compound to H<sub>2</sub> production [24,27,33,57,118–120], demonstrating the feasibility of this process.

Hashimoto *et al.* investigated the photocatalytic H<sub>2</sub> production in presence of different aliphatic and aromatic compounds with suspended Pt/TiO<sub>2</sub> [27], demonstrating the production of hydrogen in presence of phenol. Moreover, the study showed an increased rate of H<sub>2</sub> production in presence of phenol in alkaline conditions over acidic conditions. Languer *et al.* reported that the photocatalytic phenol degradation over TiO<sub>2</sub> nanotubes produced hydrogen at a rate of about 0.06 μmol h<sup>-1</sup> cm<sup>-2</sup> [119]. Kim *et al.* demonstrated the feasibility of hydrogen production coupled to photocatalytic degradation of 4-chlorophenol [24]. The study involved the activity comparison of the following photocatalysts: TiO<sub>2</sub>/Pt, F-TiO<sub>2</sub>/Pt and P-TiO<sub>2</sub>/Pt. The highest H<sub>2</sub> production rate was obtained with F-TiO<sub>2</sub>/Pt and the lowest with TiO<sub>2</sub>/Pt. However, the good activity of F-TiO<sub>2</sub>/Pt was limited to acidic region since the fluorides desorb at the alkaline region. P-TiO<sub>2</sub>/Pt had higher H<sub>2</sub> production range than TiO<sub>2</sub> for all the pH range. Lv *et al.* used S doped two-dimensional g-C<sub>3</sub>N<sub>4</sub> for the photocatalytic hydrogen production from phenol, achieving a H<sub>2</sub> production rate of 127.4 μmol/h and an external quantum efficiency of 8.35 % at 400 nm [33].

In photoelectrochemical cells, several photoanodes materials have been tested. Wu *et al.* studied the effect of the photoanode and photocathode materials on the voltage and current generated in the phenol degradation and hydrogen production [57]. Different photoanode and photocathode nanostructures, as nanorods (NRs), nanoparticles (NPs) and nanowires (NWAs) were tested from TiO<sub>2</sub>, CdS, CdSe and Cu<sub>2</sub>O. It was demonstrated that the open circuit voltage depends not only on the Fermi level between the photoelectrodes, but also on crystal facet for the same semiconductor materials with different microstructures. The best phenol removal efficiency was achieved with the combination of the photoanode TiO<sub>2</sub> NRs/FTO-C/Cu<sub>2</sub>O and the photocathode C/Cu<sub>2</sub>O NWAs/Cu. This combination reached a phenol removal rate of 84.2 % and an overall hydrogen



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3 production rate of  $86.8 \mu\text{mol cm}^{-2}$  in 8 hours. Park *et al.* demonstrated the feasibility of hydrogen  
4 production driven by the photoelectrochemical degradation of phenol using improved multi-  
5 layered  $\text{BiO}_x\text{-TiO}_2/\text{Ti}$  electrodes [118]. The electrodes were formed by an under layer of  $\text{TaO}_x\text{-}$   
6  $\text{IrO}_x$ , a middle layer of  $\text{BiO}_x\text{-SnO}_2$ , and an upper layer of  $\text{BiO}_x\text{-TiO}_2$  which covered on both sides  
7 of Ti foil. The study showed that bismuth doping, even at high concentration, increased  $\text{TiO}_2$   
8 conductivity, while preserving the original photoelectrochemical properties. Li *et al.* studied the  
9 photoelectrocatalytic hydrogen production in presence of phenol using  $\text{Bi/BiVO}_4$  as photoanode  
10 [120]. The study reported a hydrogen production rate of  $27.8 \mu\text{mol cm}^{-2} \text{h}^{-1}$ .  
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#### 12 4.4 Alcohols

13 Although alcohols are not expected to be abundant and common substances in municipal  
14 wastewater, they may be present in some industrial wastewater [121]. The production of  $\text{H}_2$  from  
15 photocatalytic oxidation of alcohols has been extensively studied, mainly methanol, ethanol, and  
16 glycerol oxidation.  
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18 Kawai and Sakata demonstrated the feasibility of producing hydrogen by photoreforming of  
19 methanol [122]. The study reports the highest  $\text{H}_2$  production rate Pt and an apparent quantum yield  
20 of 44 % at 380 nm with a photocatalyst formed by  $\text{RuO}_2/\text{TiO}_2/\text{Pt}$ . In the proposed reaction  
21 mechanism, methanol forms an intermediate, formaldehyde, which further oxidises to formic acid  
22 and finally decomposes to  $\text{CO}_2$  and  $\text{H}_2$ . Chiarello *et al.* studied the effect of loading different noble  
23 metal co-catalysts to a  $\text{TiO}_2$  photocatalyst in the photoreforming of methanol [123]. Among the  
24 investigated co-catalysts (Ag, Au and Pt), Pt showed the highest hydrogen production rate.  
25 Moreover, Naldoni *et al.* studied the difference between loading  $\text{TiO}_2$  photocatalyst with Au or Pt,  
26 concluding that photogenerated electrons are more easily transferred to the Pt nanoparticles to  
27 reduce protons, than to Au [124]. Chen *et al.* studied the mechanism of the photocatalytic reaction  
28 of methanol for hydrogen production on  $\text{Pt/TiO}_2$  [125]. The proposed mechanism (figure 7)  
29 involves the formation of  $\text{H}_2$  on Pt sites, in which the proton transfer to the Pt sites is mediated by  
30 the adsorbed water and methanol molecules. Most of the protons that form  $\text{H}_2$  in the Pt sites come  
31 from water and not methanol. The study demonstrates that the surface species of  $\text{CH}_2\text{O}$ ,  $\text{CH}_2\text{OO}$   
32 and  $\text{HCOO}$  were formed. Moreover, an increase in Pt loading generated a decrease on methanol  
33 adsorption, which suggest that Pt atoms occupy sites for methanol adsorption [125]. Ismael studied  
34 the use of a Ru doped  $\text{TiO}_2$  photocatalyst for the hydrogen production from methanol, reporting an  
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enhancement on the activity due to the decrease in the band gap and a larger surface area. The highest activity was reported doping with of 0.1 % mol of Ru. In another study, Chen *et al.* reported the possibility of using a low cost photocatalyst formed by carbon coated Cu/TiO<sub>2</sub> (C/Cu/TiO<sub>2</sub>) for hydrogen production from methanol [126]. This photocatalyst produced a H<sub>2</sub> yield of 269.1 μmol h<sup>-1</sup> which is comparable to 290.8 μmol h<sup>-1</sup>, the yield produced with Pt/TiO<sub>2</sub>.

Liu *et al.* investigated the interaction between CuO<sub>x</sub>-TiO<sub>2</sub> and its effect on the photocatalytic production of hydrogen from methanol [127]. The highest H<sub>2</sub> production was reported with CuO<sub>x</sub>/TiO<sub>2</sub>-{0 0 1} which has the highest Cu<sub>2</sub>O dispersion and strongest interaction. Jiménez-Rangel *et al.* study the performance of g-C<sub>3</sub>N<sub>4</sub>/NiOOH/Ag as photocatalyst for the photoreforming of methanol, obtaining a maximum H<sub>2</sub> yield of 350.6 μmol/h. The hydrogen yield of the combined g-C<sub>3</sub>N<sub>4</sub>/NiOOH/Ag photocatalyst resulted significantly higher compared to the yield of g-C<sub>3</sub>N<sub>4</sub>, g-C<sub>3</sub>N<sub>4</sub>/NiOOH or g-C<sub>3</sub>N<sub>4</sub>/Ag alone [34]. Hojamberdiev *et al.* studied the use of a photocatalyst composed of g-C<sub>3</sub>N<sub>4</sub> Ni(OH)<sub>2</sub> and halloysite nanotubes for the production of hydrogen from methanol [128]. This photocatalyst presented a higher H<sub>2</sub> production rate (18.42 μmol h<sup>-1</sup>) than g-C<sub>3</sub>N<sub>4</sub>/Ni(OH)<sub>2</sub> (9.12 μmol h<sup>-1</sup>) or g-C<sub>3</sub>N<sub>4</sub> (0.43 μmol h<sup>-1</sup>). This enhancement was attributed to charge separation being the holes trapped by the halloysite nanotubes and the electrons transferred to Ni(OH)<sub>2</sub>.

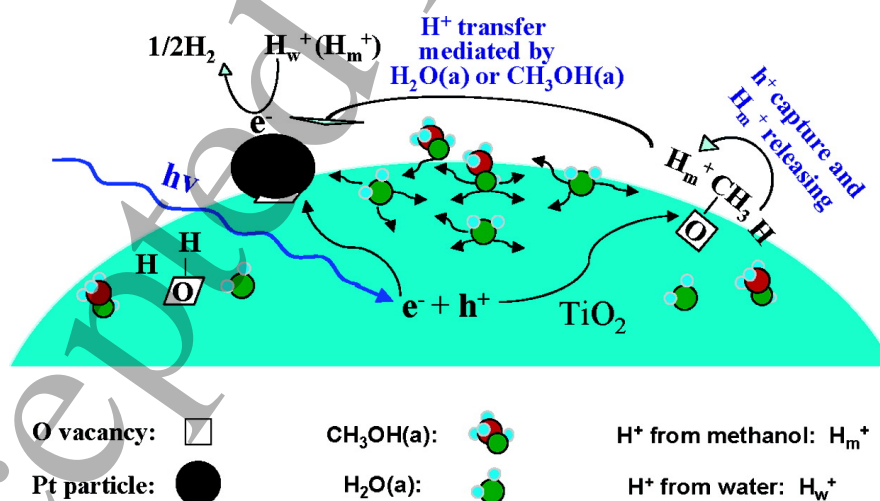


Figure 7. Proposed mechanism for the photoreforming of methanol on Pt loaded TiO<sub>2</sub>. This figure has been reprinted from reference [125] with permission from the American Chemical Society.

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3 Ethanol has been extensively studied as a sacrificial agent for H<sub>2</sub> production [25,31,32,129–135].  
4 Kawai and Sakata studied the photocatalytic production of hydrogen from ethanol [129]. The study  
5 reports the production of hydrogen, methane, and acetaldehyde. Moreover, different co-catalyst  
6 loaded in TiO<sub>2</sub> were studied as Ni, Pd, Pt and Rh, being Pt the one with the highest H<sub>2</sub> production  
7 rate and with a reported external quantum yield of 38 % at 380 nm. Kondarides *et al.* studied the  
8 hydrogen production from the photocatalytic reforming of ethanol with an Pt/TiO<sub>2</sub> photocatalyst,  
9 reporting an external quantum efficiency of 50 % at 365 nm [25]. Yang *et al.* researched the  
10 photocatalytic production of hydrogen from ethanol using metal loaded TiO<sub>2</sub> as photocatalyst and  
11 compared it to the H<sub>2</sub> production from other alcohols [130]. Pt and Pd presented higher H<sub>2</sub>  
12 production rates than Rh. Moreover, it was suggested that the hydrogen production over Pt/TiO<sub>2</sub>  
13 is governed by the solvation of the alcohol, following the H<sub>2</sub> production the following trend:  
14 methanol ≈ ethanol > propanol ≈ Isopropanol > n-butanol. Sola *et al.* investigated the effect of the  
15 morphology and structure of Pt/TiO<sub>2</sub> photocatalysts on the hydrogen production from ethanol  
16 [131]. The study showed an improved performance for the Pt/TiO<sub>2</sub> photocatalysts with higher  
17 surface area and lower pore size. The best performing photocatalyst was found to be Pt/TiO<sub>2</sub> with  
18 an average pore size of 29.1 nm and a surface area of 51 m<sup>2</sup> g<sup>-1</sup>, reporting an apparent quantum  
19 yield of 5.14%. Acetic acid, 2-3 butanediol and acetaldehyde were the main products in the liquid  
20 phase, finding a higher concentration of 2-3 butanediol with lower pore size. Puga *et al.* studied  
21 the hydrogen production from photocatalytic ethanol oxidation over Au/TiO<sub>2</sub>, obtaining as main  
22 products acetaldehyde in the liquid phase and H<sub>2</sub> in the gas phase with a volumetric proportion of  
23 99%, while the other gaseous product detected were CH<sub>4</sub>, C<sub>2</sub>H<sub>4</sub>, C<sub>2</sub>H<sub>6</sub>, CO and CO<sub>2</sub> [132].

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40 Deas *et al.* used Au loaded on TiO<sub>2</sub> nanoflowers as photocatalyst for hydrogen production from  
41 ethanol, reporting a hydrogen production rate of 24.3 mmol g<sup>-1</sup> h<sup>-1</sup>, compared to only 12.1 mmol  
42 g<sup>-1</sup> h<sup>-1</sup> obtained with Au/P25 [133]. This enhancement was ascribed to the thin and crystalline  
43 anatase sheets of the nanoflower petals which reduce the bulk recombination. Pajares *et al.*  
44 investigated the use of WC as TiO<sub>2</sub> co-catalyst for the photocatalytic hydrogen production from  
45 ethanol, reporting an enhancement of 40% the H<sub>2</sub> yield compared to P25 [134]. Zhang *et al.*  
46 investigated the effect of Ti<sup>3+</sup> defects of Au/TiO<sub>2</sub> on the hydrogen production from ethanol [135].  
47 The study reported an increased activity with higher defects, concluding that oxygen vacancies on  
48 TiO<sub>2</sub> rich in defects, facilitates the adsorption of ethanol and hole transfer. Ryu *et al.* studied the  
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3 photoreforming of ethanol using CdS attached on microporous and mesoporous silicas as  
4 photocatalyst. The study suggests that the photoactivity was dependent on the silica cavity size,  
5 which partially controls the CdS particle size [31]. Cebada *et al.* studied the use of Ni/CdS as  
6 photocatalyst for the hydrogen production from ethanol, proving that higher Ni content resulted in  
7 increased hydrogen production [32].  
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12 Antoniadou *et al.* studied the hydrogen production from ethanol using a photoelectrochemical cell  
13 chemically biased [136]. The cell had two compartments, with a TiO<sub>2</sub> photoanode in an acidic  
14 electrolyte compartment and a Pt cathode in alkaline electrolyte compartment. The study reported  
15 an IPCE of 96 % at 360 nm and proved that the photoreforming of ethanol is more efficient than  
16 photocatalytic water splitting. Adamopoulos *et al.* investigated the effect of adding a top layer of  
17 TiO<sub>2</sub> to a WO<sub>3</sub> photoanode in the hydrogen production from ethanol using a biased  
18 photoelectrochemical cell [137]. Carbon black loaded on carbon paper was used as cathode.  
19 Increased current density and hydrogen production were reported when using the  
20 TiO<sub>2</sub>/WO<sub>3</sub> bilayer photoanode; this improvement was ascribed to the lower number of  
21 recombination sites.  
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31 H<sub>2</sub> production from photoreforming of glycerol has also been widely studied [25,138–143].  
32 Kondarides *et al.* studied the hydrogen production from the photocatalytic reforming of glycerol,  
33 reporting an external quantum efficiency higher than 70 % at 365 nm with a Pt/TiO<sub>2</sub> photocatalyst  
34 and 1 M of glycerol [25]. Fu *et al.* studied the mechanism of photoreforming polyols as glycerol  
35 using a Pt/TiO<sub>2</sub> photocatalyst, proposing that just the H atoms connected to hydroxyl C atoms can  
36 form H<sub>2</sub> while the C atoms are oxidized to CO<sub>2</sub> [138]. For non-OH bonded C atoms, the bond H  
37 and C atoms form products in the form of alkanes as CH<sub>4</sub> or C<sub>2</sub>H<sub>6</sub>. Bowker *et al.* investigated the  
38 photocatalytic reforming of glycerol using Pd and Au modified TiO<sub>2</sub> and proposed a possible  
39 mechanism [139]. Hydrogen production rate from Pd was four times larger than the one of Au.  
40 The mechanism suggests that H<sub>2</sub> is produced through the dissociation of adsorbed glycerol  
41 molecules with the associated production of CO, when using Pd/TiO<sub>2</sub>. Subsequently, the CO reacts  
42 with oxygen radical at the metal surface to produce CO<sub>2</sub> freeing sites. Montini *et al.* studied the  
43 hydrogen production from glycerol using Cu/TiO<sub>2</sub> photocatalyst [140]. Hydrogen and carbon  
44 dioxide were the main products in gas phase, and 1,3-dihydroxypropanone and  
45 hydroxyacetaldehyde in liquid phase. Moreover, Chen *et al.* reported a quantum efficiency of  
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24.9% at 365 nm and hydrogen production rate of 17.6 mmol g<sup>-1</sup> h<sup>-1</sup> from glycerol using Cu/TiO<sub>2</sub> as photocatalyst [141]. Daskalaki and Kondarides studied the hydrogen production from photoreforming of glycerol over Pt/TiO<sub>2</sub>, reporting H<sub>2</sub> and CO<sub>2</sub> as the only products in gas phase and methanol and acetic acid as intermediates in liquid phase [142]. Naffati *et al.* reported a hydrogen production rate of 2091 μmol g<sup>-1</sup> from glycerol using a photocatalyst consisting of TiO<sub>2</sub> loaded with Pt and carbon nanotubes (CNT) [143].

Hydrogen production from glycerol has been also demonstrated using photoelectrochemical cells using a TiO<sub>2</sub> photoanode [144], or a TiO<sub>2</sub> photoanode functionalized with CdS [145].

#### 4.5 Organic acids and aldehydes

Other compounds that can be part of the organic waste contained in wastewater are organic acids and aldehydes [146,147]. Patsoura *et al.* studied the hydrogen production and simultaneous degradation of formic acid, acetic acid and acetaldehyde over a Pt/TiO<sub>2</sub> photocatalyst [148]. The study reported a hydrogen production after 20 hours of 183.2 μmol from acetic acid and 72.5 μmol from acetaldehyde.

*Li et al.* researched the photocatalytic hydrogen production in presence of oxalic acid, formic acid and formaldehyde using a Pt/TiO<sub>2</sub> photocatalyst [28]. The study reported that the photocatalytic activity of these electron donors follows the trend of oxalic acid > formic acid > formaldehyde which agrees with the order of adsorption affinity of these electron donors on TiO<sub>2</sub>.

Imizcoz and Puga investigated the photoreforming of acetic acid using Cu/TiO<sub>2</sub> as photocatalyst [149]. Hydrogen production from acetic acid was enhanced by including a photoreduction step to control the oxidation stage of Cu. On the contrary, when Cu was used directly, its passivation resulted in a high decarboxylation, producing mainly CH<sub>4</sub> instead of H<sub>2</sub>.

#### 4.6 Wastewater mixtures

The feasibility of photocatalytic H<sub>2</sub> production from wastewater mixtures such as olive mill wastewater, juice production wastewater and waste activated sludge has been demonstrated [29,30,112,150].

Olive mill wastewater (OMW) contains a high load of organics varying from 40 to 220 g L<sup>-1</sup> [151].

The main components found on this wastewater are oil, grease, polyphenols and sugars [150].

Badawy *et al.* studied the photocatalytic degradation of OMW with simultaneous hydrogen production using nanostructured mesoporous TiO<sub>2</sub> as photocatalyst [29]. TiO<sub>2</sub> loading and pH were the main factors affecting the photocatalytic degradation and H<sub>2</sub> production in this study. The maximum hydrogen production was 38 mmol after 2 hours at a pH of 3 and a photocatalyst concentration of 2 g L<sup>-1</sup>. The organic pollutants contained in OMW enhanced the H<sub>2</sub> production, by scavenging holes and decreasing the electron hole recombination. Speltini *et al.* investigated the effects of factors as photocatalyst concentration, pH and OMW concentration in H<sub>2</sub> production, using Pt/TiO<sub>2</sub> as photocatalyst and UV-A irradiation [150]. The study reports an apparent quantum yield of 5.5 10<sup>-3</sup> at 366 nm and the production of 44 μmol of H<sub>2</sub> after 4 hours of UV-A irradiation, using a photocatalyst concentration of 2 g L<sup>-1</sup>, OMW concentration of 3.35 v/v, and a pH of 3. Moreover, the H<sub>2</sub> yield produced by OMW was compared to glucose, which have been considered a good sacrificial donor for H<sub>2</sub> production, and similar production rates were obtained.

Imizcoz and Puga demonstrated the feasibility of photocatalytic hydrogen production using wastewater from a juice production industry, which contains high amounts of saccharides [112]. The study reported a H<sub>2</sub> yield of 115 mol g<sub>cat</sub><sup>-1</sup> h<sup>-1</sup> using Au/TiO<sub>2</sub> as photocatalyst.

The simultaneous H<sub>2</sub> production and degradation of waste activated sludge from wastewater treatment processes was investigated by Liu *et al.*, using Ag/TiO<sub>2</sub> as photocatalyst, proving the possibility of this process [30].

All the materials used in the reviewed works for H<sub>2</sub> production by photocatalytic and photoelectrochemical oxidation of each wastewater component are summarize in table 1 and table 2.

Table 1. Summary of the materials used in the H<sub>2</sub> production from photocatalytic degradation of wastewater compounds.

Waste	Photocatalyst	Co-Catalyst	Maximum Efficiency (%)	Reference
Ammonia	TiO <sub>2</sub>	Pt or RuO <sub>2</sub>	EQE <sub>(340nm)</sub> = 5.1	[23]
	TiO <sub>2</sub>	Pt, Rh, Pd, Au, Ni or Cu	-	[103]
	TiO <sub>2</sub>	Pt-Au	-	[104]
Urea	F-TiO <sub>2</sub>	Pt	-	[24]
Cellulose	RuO <sub>2</sub> /TiO <sub>2</sub>	Pt	EQE <sub>(380 nm)</sub> = 1	[108]
	TiO <sub>2</sub>	Pt	-	[25]

	TiO <sub>2</sub>	Pt	-	[109]
	TiO <sub>2</sub>	Pd, Pt, Ni or Au	-	[110]
Glucose	TiO <sub>2</sub>	Pt	EQE <sub>(365 nm)</sub> = 63	[25]
	TiO <sub>2</sub>	Pd, Pt, Au, Rh, Ag or Ru	-	[26]
	TiO <sub>2</sub>	Rh	-	[111]
	TiO <sub>2</sub>	Pt, Au, Ag or Cu	-	[112]
	TiO <sub>2</sub>	CuO	-	[113]
Phenol	TiO <sub>2</sub>	Pt	-	[27]
	TiO <sub>2</sub>	-	-	[119]
	S-g-C <sub>3</sub> N <sub>4</sub>	-	EQE <sub>(400 nm)</sub> = 8.35	[33]
4-chlorophenol	F-TiO <sub>2</sub> or P-TiO <sub>2</sub>	Pt	-	[24]
Methanol	TiO <sub>2</sub> /RuO <sub>2</sub>	Pt or Pd	EQE <sub>(380 nm)</sub> = 44	[122]
	TiO <sub>2</sub>	Ag, Au or Pt	-	[123]
	TiO <sub>2</sub>	Au or Pt	FQE = 14	[124]
	Ru- TiO <sub>2</sub>	Pt	-	[127]
	TiO <sub>2</sub>	Pt	EQE <sub>(355 nm)</sub> = 2.9	[125]
	TiO <sub>2</sub> /C	Cu/C	-	[126]
	g-C <sub>3</sub> N <sub>4</sub>	NiOOH/Ag	-	[34]
	g-C <sub>3</sub> N <sub>4</sub>	Ni(OH) <sub>2</sub> / Al <sub>2</sub> Si <sub>2</sub> O <sub>5</sub> (OH) <sub>4</sub>	-	[128]
Ethanol	TiO <sub>2</sub>	Pt	EQE <sub>(365 nm)</sub> = 50	[25]
	TiO <sub>2</sub>	Ni, Pd, Pt or Rh	EQE <sub>(380 nm)</sub> = 38	[129]
	TiO <sub>2</sub>	Pt, Pd or Rh	FQE = 10	[130]
	TiO <sub>2</sub>	Pt	EQE = 5.14	[131]
	TiO <sub>2</sub>	Au	-	[129]
	TiO <sub>2</sub>	Au	-	[133]
	TiO <sub>2</sub>	Au	-	[135]
	TiO <sub>2</sub>	WC	-	[134]
	CdS	-	-	[31]
	CdS	Ni	-	[32]
Glycerol	TiO <sub>2</sub>	Pt	EQE <sub>(365 nm)</sub> = 70	[25]
	TiO <sub>2</sub>	Pt	-	[138]
	TiO <sub>2</sub>	Pd or Au	-	[139]
	TiO <sub>2</sub>	Cu	-	[140]
	TiO <sub>2</sub>	Cu	EQE <sub>(365nm)</sub> = 24.9	[141]
	TiO <sub>2</sub>	Pt	-	[142]
	TiO <sub>2</sub>	CNT-Pt	-	[143]
Formic acid	TiO <sub>2</sub>	Pt	-	[148]

	TiO <sub>2</sub>	Pt	-	[28]
Acetic acid	TiO <sub>2</sub>	Pt	-	[148]
	TiO <sub>2</sub>	Cu	-	[149]
Oxalic acid	TiO <sub>2</sub>	Pt	-	[28]
Acetaldehyde	TiO <sub>2</sub>	Pt	-	[148]
Formaldehyde	TiO <sub>2</sub>	Pt	-	[28]
OMW	TiO <sub>2</sub>	-	-	[29]
		Pt	EQE <sub>(366 nm)</sub> = 0.5	[150]
Juice industry wastewater	TiO <sub>2</sub>	Au	-	[112]
Sludge	TiO <sub>2</sub>	Ag	-	[30]

Table 2. Summary of the materials used in the H<sub>2</sub> production from degradation of wastewater compounds using photoelectrochemical cells.

Waste	Photoanode	(Photo)Cathode	Maximum Efficiency (%)	Reference
Ammonia	TiO <sub>2</sub>	Pt	-	[54]
	TiO <sub>2</sub>	Pt/C	-	[56]
Urea	Ni(OH) <sub>2</sub> loaded on TiO <sub>2</sub> or α-Fe <sub>2</sub> O <sub>3</sub>	Pt	-	[55]
	TiO <sub>2</sub>	Pt/C	-	[56]
Formamide	TiO <sub>2</sub>	Pt/C	-	[56]
Glucose	WO <sub>3</sub>	WC	EQE <sub>(600 nm)</sub> = 80	[114]
	Ni(OH) <sub>2</sub> loaded on α-Fe <sub>2</sub> O <sub>3</sub>	Pt	-	[62]
Phenol	TiO <sub>2</sub> NRs, TiO <sub>2</sub> NTs/Ti, CdS and CdSe	C/Cu <sub>2</sub> O/Cu and Cu <sub>2</sub> O	IPCE <sub>(380 nm)</sub> = 68	[57]
	BiO <sub>χ</sub> -TiO <sub>2</sub> /Ti	SS	-	[118]
	Bi/BiVO <sub>4</sub>	Pt	-	[120]
Ethanol	TiO <sub>2</sub>	Pt	IPCE <sub>(360nm)</sub> = 96	[136]
	TiO <sub>2</sub> /WO <sub>3</sub>	Carbon black	-	[137]
Glycerol	TiO <sub>2</sub>	Pt	-	[144]
	TiO <sub>2</sub> /CdS	Pt	-	[145]

## 5. Conclusions

This review has described the potential of wastewater as source for energy recovery, using photocatalytic oxidation of pollutants coupled to hydrogen production. The production of



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3 hydrogen from pollutants and wastes is energetically more favourable than the production of  
4 hydrogen from water splitting.  
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7 Using suspensions of photocatalytic particles has been the most common approach to date, while  
8 only a limited number of works have adopted the use of photoelectrochemical cells. PEC represent  
9 a promising option since this configuration reduces the recombination losses within the system.  
10 Up to now there has been limited research focused on the optimization of the design of  
11 photocatalytic reactors or photoelectrochemical cells to improve the overall system efficiency.  
12 More research is needed on materials that have already shown promising results for water splitting  
13 and which might show improved efficiencies as compared to pure  $\text{TiO}_2$  for hydrogen production  
14 from wastewater.  
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21 Only a few studies investigate hydrogen production coupled to the treatment of real or simulated  
22 wastewater and more studies are needed to assess the real application. It is extremely challenging  
23 to compare the performance from the different published works. Hydrogen production rates, when  
24 given, are measured under very different operating conditions and the quantum efficiencies are  
25 sometimes not reported. Therefore, following a systematic procedure in reporting photocatalytic  
26 performance would be beneficial for the evaluation of the different compounds. Nevertheless,  
27 hydrogen production linked to the treatment of pollutants in wastewater is an exciting area for  
28 research and may have true potential for scale up in niche applications.  
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