

1	Synthesis of prebiotic carbohydrates derived from cheese whey				
2	permeate by a combined process of isomerization and				
3	transgalactosylation				
4	Running title: Synthesis of prebiotic carbohydrates from cheese whey				
5	permeate				
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26 Abstract

27 BACKGROUND: Lactose from cheese whey permeate (WP) was efficiently 28 isomerized to lactulose using egg shell, a food-grade catalyst, and the subsequent 29 transgalactosylation reaction of this mixture with β -galactosidase from *Bacillus* 30 *circulans* gave rise to a wide array of prebiotic carbohydrates derived from lactose 31 and lactulose.

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33 **RESULTS: Lactulose, which was obtained by the efficient isomerization of the WP** 34 (16% in weight, respect to the initial amount of lactose), showed a great resistance 35 to the hydrolytic action of β -galactosidase from *B. circulans* that preferentially hydrolyzed lactose, acting as galactosyl donor and acceptor. Lactulose had 36 37 capacity as acceptor leading to the formation of lactulose-derived oligosaccharides. 38 The enzymatic synthesis was optimized by studying reaction conditions such as 39 pH, temperature, time, enzyme, and carbohydrate concentration. The maximum 40 formation of galactooligosaccharides, with degree of polymerization from 2 to 4, was achieved after 5 h of reaction at pH 6.5, 50 °C with 300 g kg⁻¹ of carbohydrates 41 and 3 U mL⁻¹ of β -galactosidase. 42

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44 CONCLUSION: These findings indicate that the transgalactosylation of
45 isomerized WP with β-galactosidase from *B. circulans* could be a new and efficient
46 method to obtain a mixture with a 50% of potentially prebiotic carbohydrates
47 composed of lactulose, and galactooligosaccharides derived from lactose and
48 lactulose.

49 Keywords: isomerization, lactulose, galactooligosaccharides, transgalactosylaction,
50 *Bacillus circulans*, whey permeate.

INTRODUCTION

52

53 Cheese whey is the most abundant by-product of the dairy industry and its disposal in 54 the environment causes important drawbacks because of its high biochemical oxygen 55 demand. Consequently, it is normally spray dried and used as low-value products, such as feed for animals, or food supplement.¹ Alternatively, it is processed by ultrafiltration 56 57 to yield whey protein concentrate and whey permeate (WP), the latter being an 58 inexpensive by-product comprising mainly lactose and salts. Unlike whey proteins that 59 find immediate food applications, the WP has so far been of little value probably due to its high salt content.²⁻³ Therefore, its profitable use constitutes a relevant activity from 60 61 the economic and environmental point of view.

The use of WP to produce lactose derivatives including lactulose, lactitol, 62 lactobionic acid, tagatose and sialyllactose has long been of industrial interest.⁴⁻⁵ In the 63 64 last few years, an increasing interest in the consumption of prebiotic carbohydrates has been observed so that the production of new bioactive oligosaccharides is currently 65 garnering much attention for their potential use as functional ingredients.⁶ Today one of 66 67 the most promising uses of WP is the synthesis of prebiotic galactooligosaccharides 68 (GOS) from transgalactosylation of lactose catalyzed by β -galactosidases (EC 3.2.1.23) of microbial origin.⁷⁻¹⁰ Among them, β-galactosidase from *Bacillus circulans* has shown 69 70 to have the ability to produce GOS with a good yield from model systems consisting of lactose in buffered solutions.¹¹⁻¹³ However, scarce studies dealing with the production of 71 GOS from cheese WP using β -galactosidase of *B. circulans* have been carried out.¹⁴ In 72 73 this sense, it is noteworthy to indicate that substantial differences, in terms of yield and 74 oligosaccharide composition, between the production of GOS from model systems 75 consisting of lactose in buffered solutions and from WP could be expected due to the influence of other permeate ingredients, such as mineral salts.¹⁵⁻¹⁸ Furthermore, 76

considering the relationship between the structure and prebiotic activity of
oligosaccharides,¹⁹⁻²⁰ the synthesis of new lactulose-derived oligosaccharides have
recently been reported in order to find new prebiotics with improved or complementary
properties.²¹⁻²⁶

The aim of this work was to develop a new approach based on the combined process of isomerization of lactose present in cheese WP using a food-grade catalyst (egg shell) and the subsequent enzymatic transgalactosylation with β -galactosidase from *B. circulans* avoiding intermediate purification steps of lactulose, and contributing to the improvement of the production of a range of potential bioactive oligosaccharides. In consequence, data reported in this work could help to broaden the use of cheese WP for the efficient production of functional carbohydrates.

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MATERIALS AND METHODS

90 Chemical and reagents

91 Reagents employed for chromatography analysis, including standards (glucose, 92 galactose, fructose, lactose, lactulose, raffinose, stachyose, and β-phenyl-glucoside) 93 were obtained from Sigma (St. Louis, USA). Acetonitrile (HPLC grade) was purchased 94 from Lab-scan (Gliwice, Poland). All other chemicals were of analytical grade. Ultrapure water quality (18.2 M Ω cm), with 1–5 ppb TOC and <0.001 EU mL⁻¹ of 95 96 pyrogen levels was produced in-house, using a laboratory water purification Milli-Q 97 Synthesis A10 system (Millipore, Billerica, Massachusetts, USA) and was used 98 throughout.

99 β-galactosidase from *Bacillus circulans* (Neutral Lactase) was acquired from 100 Biocon (Barcelona, Spain). Lactase activity was 3000 U mL⁻¹, where 1 unit is the 101 amount of enzyme required to hydrolyze 1 µmol of lactose per minute at a working 102 temperature of 50 °C, and a lactose concentration of 300 g kg⁻¹ at pH 6.0 with 0.05 mol 103 L^{-1} of buffer phosphate.

104

105 Egg shell powder

White egg shells were washed with tap water to remove all adhering albumen, dried at 107 105 °C for 24 h and ground in a ball mill (Mixer Mill MM 200, Retsch GmbH & Co. 108 KG, Haan, Germany) at 800 rpm (13.3 Hz), for 15 min. Resulting egg shell powder had 109 a particle size of approximately 5 μ m, and was stored in glass vials in a dry place at 110 room temperature prior to be used.

111

112 Physical-chemical characterization of cheese whey permeate

An industrial bovine cheese WP powder with a lactose content of 810 g kg⁻¹ was kindly supplied by the dairy industry Reny Picot (Navia, Spain). The pH of reconstituted WP was measured using a pH meter (MP 230, Mettler-Toledo, Barcelona, Spain) at a concentration of 300 g kg⁻¹.

117

118 Isomerization reaction

The isomerization reaction was performed as previously reported by Montilla et al.²⁷ 119 120 with some modifications. A permeate powder solution at a concentration of 300 g kg⁻¹ 121 lactose was prepared with Milli-Q water. Sample was stirred at 750 rpm, 60 °C for 30 122 min, and then, it was cooled down at room temperature and the pH adjusted to 6.8 by adding 2 mol L⁻¹ NaOH. Afterwards, 100 g of this sample was placed in a 250 mL 123 124 round-bottom flask provided with an additional necked sampling inlet and 3 g of egg shell powder was added. The flask was immersed in a glycerol bath at 120 °C, stirred at 125 126 300 rpm and refluxed at 98 °C for 180 min. Boiling start (5 min) was considered as zero

time of reaction. Samples (30 mL) were taken at 0, 60, 90, 120, 150 and 180 min. Reaction was stopped by cooling down with an ice-water bath. Egg shell was removed by centrifugation at 5000g and 20 °C for 10 min. Supernatant was collected, lyophilized, and stored at -18 °C until further analysis. Isomerization reaction was carried out in duplicate and analyses were performed twice for each isomerization treatment.

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133 Oligosaccharide synthesis

134 Enzymatic synthesis of oligosaccharides from isomerized whey permeate (IWP) using β-galactosidase from *B. circulans* was carried out under different reaction conditions 135 136 such as pH (5.5, 6.5, and 7.4), temperature (40, 50, and 60 °C), enzyme concentration $(1.5, 3, \text{ and } 6 \text{ U mL}^{-1})$, carbohydrate concentration (100, 300, and 500 g kg⁻¹ 137 reconstituted in milli-Q water), and time (1, 3, 5, 8 and 24 h). Reactions were performed 138 139 at a final volume of 1.5 mL in microtubes incubated in an orbital shaker at 300 rpm. 140 Aliquots (250 µL) were withdrawn from the reaction mixture at the different times and 141 immediately immersed in boiling water for 5 min to inactivate the enzyme. Samples 142 were stored at -18 °C for subsequent analysis. Besides, another assay using WP or lactulose (300 g kg⁻¹) as substrate, at 50 °C, pH 6.5 and enzyme concentration 3 U mL⁻¹ 143 144 was carried out. Enzymatic reactions were made in duplicate and analyses were 145 performed twice for each enzymatic treatment.

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147 Chromatographic determination of carbohydrates

148 GC analysis

149 Sample preparation

150 200 μ L of sample was made up to 2 mL with water in a volumetric flask and was 151 filtered using a 0.45 μ m syringe filter (Symta, Madrid, Spain). 0.2 mg phenyl- β -D- 152 glucoside was added to 100 μ L of filtrate as internal standard and the mixture was dried 153 at 38–40 °C in a rotary evaporator. These samples were analyzed by two different GC 154 systems as described below.

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156 Gas chromatography with FID detection (GC-FID)

157 The dried mixtures were treated with 100 μ l of N-trimethylsilylimidazole to silylate the 158 carbohydrates; the reaction was completed in 30 min at 70 °C. Silylated carbohydrates 159 were extracted with 0.3 mL of hexane and 0.3 mL of water. Volume of 1 μ l of the 160 organic phase containing silyl derivatives were injected into the column.

161 The trimethylsilyl ethers of carbohydrates were analyzed as has been previously described using an Agilent Technologies 7890A gas chromatograph equipped with a 162 163 commercial fused silica capillary column SPB-17, bonded, crosslinked phase (50% 164 diphenyl/50% dimethylsiloxane; 30 m \times 0.32 mm inside diameter \times 0.5 µm film) (Supelco, North Harrison Road, Bellefonte, PA, USA).²⁸ Separation was performed at 165 235 °C for 9 min, followed by an increase of up to 280 °C at a rate of 15 °C min⁻¹ and 166 167 keeping this temperature for 30 min. Injector and detector temperatures were 280 °C. Injections were carried out in split mode (1:30), using 1 mL min⁻¹ of nitrogen as carrier 168 169 gas. Data acquisition and integration were performed using Agilent Chem-Station Rev. 170 B.03.01 software (Wilmington, DE).

To study the response factor relative to the internal standard, solutions containing glucose, galactose, lactose and lactulose were prepared over the expected concentration range in samples. The identities of carbohydrates were confirmed by comparison with relative retention times of standard samples. The amount of remaining lactose, lactulose, glucose and galactose in the isomerization and transgalactosylation mixtures were expressed as g kg⁻¹. 177 Gas chromatography-mass spectrometry (GC-MS)

178 Selected samples of isomerized and/or transgalactosylated permeate were also analyzed 179 by GC-MS. An Agilent Technologies 7890A gas chromatograph coupled to a 5975C 180 MSD quadrupole mass detector (Agilent Technologies, Wilmington, DE, USA) was employed. The trimethylsilyl oxime, prepared as described by Cardelle-Cobas et al.,²⁹ 181 182 were separated using an HP-5 MS fused-silica capillary column ($30m \times 0.25 mm$) 183 internal diameter \times 0.25 µm film thickness) coated with 5% phenylmethylsilicone (J&W) 184 Scientific, CA, USA). The helium flow rate was 1 mL min⁻¹. The initial oven temperature was 180 °C and increased to 315 °C at a heating rate of 3 °C min⁻¹ and held 185 186 for 20 min. The injector temperature was 280 °C. Injections were made in the split mode 187 (1:40). The mass spectrometer was operated in EI mode at 70 eV. Mass spectra were 188 acquired using Agilent ChemStation MSD software (Wilmington, DE, USA).

Identification of trimethylsilyloximes derivatives of carbohydrates was carried
out by comparison of their relative retention times and mass spectra with those of
standard compounds previously derivatized.

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193 Liquid chromatography with refraction index detector (HPLC-RID)

Samples of isomerized and transgalactosylated permeate were diluted with acetonitrile:water (50:50%, v:v), filtered using a 0.45 μ m syringe filter (Symta), and analyzed on an Agilent Technologies 1260 series HPLC system (Boeblingen, Germany). The separation of carbohydrates was carried out with a Kromasil[®] column (100-NH₂; Akzo Nobel, Brewster, NY) (250 mm x 4.6 mm, 5 μ m particle size) (using acetonitrile:water (75:25, v:v) as the mobile phase and eluted in isocratic mode at a flow rate of 1.0 mL min⁻¹ for 50 min. Injection volume was 50 μ L (~800 μ g of total 201 carbohydrates). Data acquisition and processing were performed using the Agilent202 ChemStation software (Agilent Technologies, Germany).

Carbohydrates in the reaction mixtures were initially identified by comparing the 203 204 retention times (t_R) with those of standard sugars. Quantitative analysis was performed 205 by the external standard method, using calibration curves in the range 0.01-10 mg for glucose (quantification of monosaccharides), lactose (disaccharides), raffinose 206 207 (trisaccharides) and stachyose (tetrasaccharides). All analyses were performed in 208 duplicate, obtaining relative standard deviation RSD values below 10% in all cases. 209 Amount of different carbohydrates present in the reaction mixtures were expressed as 210 weight percentage of the total carbohydrate content.

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RESULTS AND DISCUSSION

213 Isomerization of whey permeate using egg shell as catalyst

214 In order to carry out the isomerization reaction, an industrial cheese WP was used and 215 egg shell was chosen as catalyst instead of chemical reagents such as borates, sodium 216 aluminate or hydroxides, due to its multiple advantages, i.e., lower quantity of required 217 catalyst, easy removal of the egg shell by centrifugation or filtration as compared to 218 homogeneous catalysts, lower formation of products derived from side-reactions, and 219 relatively good yields of isomeric disaccharides. For that purpose, 3 g of egg shell were 220 added to 100 g of reconstituted cheese WP (equivalent to 30 g of lactose) and the 221 mixture was kept under reflux following the previous studies reported by Montilla et al.²⁷. According to GC-FID analyses, an optimal production of lactulose was reached 222 223 within 150 min of reaction. The carbohydrate composition of reaction mixture after isomerization was: galactose 7.0 g kg⁻¹, glucose 1.0 g kg⁻¹, epi-lactose 1.1 g kg⁻¹, 224 lactulose 48.2 g kg⁻¹ and lactose 209.1 g kg⁻¹, thus, a 16.1% of lactulose with respect to 225

the initial amount of lactose was obtained under the assayed conditions. Similar yield (18% of lactulose with respect to the initial amount of lactose) was obtained by Montilla $et al.^{27}$ using milk permeate concentrated.

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230 Transgalactosylation of isomerized cheese whey permeate using β-galactosidase

231 from Bacillus circulans

The effect of pH, temperature and enzyme concentration on formation of GOS was studied for initial carbohydrate concentration of 300 g kg⁻¹. The effect of substrate concentration, from 100 to 500 g kg⁻¹, was also assayed.

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236 Effect of pH

237 Three values within the optimum pH range given by the manufacturer (i.e. pH 7.4, the 238 value of permeate after the isomerization reaction, 6.5 and 5.5) were assayed at 50 °C with 3 U mL⁻¹ of β -galactosidase. Formation of GOS from IWP was monitored by 239 240 HPLC-RID as it is shown in Fig. 1. As expected, the order of elution was according to 241 the degree of polymerization of carbohydrates. Thus, monosaccharides eluted at 7-10 242 min, disaccharides at 11-20 min, trisaccharides around 22-33 min and tetrasaccharides 243 above 33 min. Additionally, it cannot be ruled out the presence of pentasaccharides in 244 minor amounts since the β -galactosidase from *B. circulans* has shown the capacity of producing pentasaccharides.³⁰ Glucose (Glc, peak 1), galactose (Gal, peak 2), lactulose 245 246 (Lu, peak 3) and lactose (Lac, peak 5), were identified by comparison of their retention times from those of commercial standards; β -D-Gal*p*-(1 \rightarrow 6)-Glu (allolactose), was 247 248 identified by comparison with the standard previously isolated in our laboratory.³¹ Formed disaccharides could tentatively be assigned to galactosyl-disaccharides with 249 250 links β -(1 \rightarrow 2), β -(1 \rightarrow 3), according to previous studies on transgalactosylation of

251 lactose by β-galactosidase from *B. circulans*.¹² While the principal trisaccharide, β-D-252 Gal*p*-(1→4)-Lac (peak 6), was identified by comparison with the standard previously 253 synthesized in our laboratory.³¹

254 Fig. 2 shows the time-course of β -galactosidase-catalyzed reaction at pH 5.5, 6.5 255 and 7.4. The lactose concentration quickly decreased from the start of the reaction to 24 256 h (Fig. 2a), being this decrease more slowed down at pH 7.4. Hydrolysis of lactose was 257 very efficient (from 79% at the initial time to 17% after 24 h at pH values 6.5 and 5.5) 258 and gave rise to the formation of glucose and a smaller quantity of galactose, regardless 259 the studied pH value (Fig. 2b), which is indicative of the transfer of galactose to form 260 GOS. Although the lactose hydrolysis rate was similar at pH 5.5 and 6.5, the amount of 261 free galactose at pH 6.5 was lower and, consequently, the GOS formation (tri- and 262 tetrasaccharides) was higher and faster than at pH 5.5 (Fig. 2c). Moreover, during the 263 first five hours of reaction, the trisaccharides were the most abundant carbohydrates 264 formed, followed by the disaccharides and the tetrasaccharides, respectively. 265 Nevertheless, after 24 h of reaction, the disaccharides were the predominant saccharides 266 formed, presumably due to the partial degradation of the tri- and tetrasaccharides, as 267 well as to the continuous synthesis of disaccharides (Fig. 2c). Thus, the maximum 268 formation of GOS, which led to a 40% of total sugars (w:w), was achieved after 5 h of 269 reaction at pH 6.5, whilst it was needed 8 h of reaction to the maximum formation of 270 GOS, i.e. 38% of total sugars (w:w), at pH 5.5 (Fig. 2a). Other studies on 271 transgalactosylation of whey permeate solutions by β -galactosidase from *B. circulans* reported yields ranging from 12 to 31%.^{15, 32}. Cheng et al.³ using similar reaction 272 273 conditions to the reported in this work, but with lactose solutions, obtained 34% of GOS 274 yield. Other studies carried out with lactose solution and β -galactosidase from B.

circulans, but different reaction conditions, obtained considerable lower yields ranging
 from 6 to 26%, ^{9,11,12}

277 Moreover, lactulose concentration moderately decreased only during the first 3 h 278 of reaction, (from 18% at 0 h to 10-11% at 3 h), and then remained fairly constant (10% 279 at 24h), indicating that β -galactosidase from *B. circulans*, in the presence of both 280 disaccharides, is prone to hydrolyze lactose instead of lactulose; the GC analyses of 281 these samples confirmed the scarce presence of fructose (<0.5% at 8 h). Thereby, the 282 slight decrease of lactulose could be mainly attributed to the formation of lactulose 283 derived oligosaccharides. This fact was corroborated by comparing the GC-MS profiles 284 of GOS obtained from WP and IWP treated with β -galactosidase of *B. circulans*, where 285 an additional trisaccharide probably corresponding to a galactosyl-lactulose derivate 286 was detected in the latter. This trisaccharide was also detected following 287 transgalactosylation of purified lactulose with β -galactosidase of *B. circulans* 288 (chromatogram not shown), and was identified by comparison with the standard β -D-Galp- $(1\rightarrow 4)$ -Lu also previously synthesized in our laboratory;³¹ this compound also 289 290 appeared in Fig.1 labeled as peak 7 and coeluted with β -D-Galp-(1 \rightarrow 4)-Lac. The MS 291 spectrum of the main lactulose-derived trisaccharide was characterized by the following 292 *m/z* ions in decreasing order of abundance: 204, 73, 361, 217, 205, 147, 191, 103, 129, 293 169, 321, 319, 271, 305, and 448. Whilst, the m/z ions from lactose-derived 294 trisaccharide (β -D-Gal*p*-(1 \rightarrow 4)-Lac) were: 204, 361, 73, 217, 205, 147, 191, 129, 103, 295 169, 271, 319, 451, 331, and 305. This means that ions m/z 321 and 448 were 296 characteristic for lactulose-derived trisaccharide, while ions m/z 451 and 331 were for β -297 D-Galp-(1 \rightarrow 4)-Lac.

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301 In addition to 50 °C, reactions at 40 and 60 °C, pH 6.5 with 3 U mL⁻¹ of β -galactosidase 302 were carried out. Lactose hydrolysis was accelerated at 50 and 60 °C in comparison to 303 40 °C (Fig. 3a), which is in concordance with the higher levels of glucose detected 304 throughout the reaction at 50 and 60 °C (Fig. 3b). Nevertheless, the levels of galactose 305 were higher at 40 °C than at 50 and 60 °C (Fig. 3b), which is in good agreement with the 306 fact that the formation of total GOS was higher and faster (maximum formation at 5 h) 307 at 50 °C (39.5 \pm 1.5%) and 60 °C (37.5 \pm 2.0%) than at 40 °C (35.6 \pm 2.0%) where the 308 maximum levels of GOS were obtained after 8 h of reaction (Fig. 3a). In consequence, 309 the commercial enzyme used in these assays seems to be more thermo-resistant than 310 that used by Boon *et al.*³⁰, who observed an inactivation on lactose hydrolysis after 90 311 min at 60 °C.

312 In addition, the different degrees of polymerization of GOS were also studied as 313 it is shown in Fig. 3c. Similar amounts of disaccharides were formed at the end of the 314 reaction carried out at 50 and 60 °C (24-25% of total sugars, w:w respectively), whilst 315 19% of disaccharides were found at 40 °C. The maximum levels of trisaccharides were 316 reached after 3 h of reaction at the three assayed temperatures, and then, a gradual 317 decrease with time was observed. A maximum of 21-22% of trisaccharides were 318 quantified at 40° and 50 °C, whilst only 15% were found at 60 °C. Similar quantities of 319 tetrasaccharides were obtained for the three temperatures (3-4% of total sugars), 320 although the maximum levels were achieved faster when the reaction was carried at 50 321 °C and 60 °C (3 h) than at 40 °C (5 h).

Although similar levels of total GOS were obtained at 50 °C and 60 °C (Fig. 3a), the temperature selected for the following analyses was 50 °C because higher amounts of tri- and tetrasaccharides were obtained. Mozaffar *et al.*¹¹ reported an optimum

325 temperature of 60 °C for two isoforms of β -galactosidase from *B. circulans*, although 326 these authors provided data of total GOS and no differentiation of degree of 327 polymerization was carried out.

328

329 Effect of enzyme and substrate concentration

330 To determine the effect of the enzyme concentration on GOS production, in addition to 3 U mL⁻¹ of β -galactosidase, 1.5 or 6 U mL⁻¹ were also assayed at 50 °C, pH 6.5 and 331 300 g kg^{-1} of carbohydrates. Fig. 4a illustrates the remaining lactose content during the 332 333 time course of reaction. Results showed that the lowest assayed concentration of enzyme (1.5 U mL⁻¹) led to the lowest hydrolysis of lactose (27% of remaining lactose 334 335 after 24 h of reaction) and the subsequent lowest formation of monosaccharides (Fig. 336 4b). However, no differences on the lactose hydrolysis rate were found between 3 and 6 U mL⁻¹ of enzyme. Fig. 4c shows di, tri and tetrasaccharides yields throughout the 337 338 enzymatic reaction. Although the highest amount of formed trisaccharides was similar 339 for all enzyme concentration assayed (20-21%), the lowest trisaccharides formation rate was observed for 1.5 U mL⁻¹ enzyme concentration. Moreover, the hydrolysis rate of 340 341 oligosaccharides increased with the enzyme concentration assayed. Formation of 342 disaccharides constantly increased with the reaction time for the three enzyme 343 concentrations assayed. The highest disaccharide content (27%) was found after 24 h when the synthesis was performed with 6 U mL⁻¹ of enzyme. Generally, in enzyme-344 345 catalyzed reactions, the reaction rate is directly proportional to the enzyme 346 concentration until a certain amount which loses that proportionality. The same effect was obtained by Das *et al.*¹⁴ who reported that beyond the dose of 0.5% of a β -347 galactosidase from *B. circulans*, no further effect on GOS yield was observed. The same 348 effect was observed by other authors for different enzymes and substrated^{33,34} In our 349

assays, since the yields differences between the reactions with 3 and 6 U mL⁻¹ of enzyme were negligible, the minor amount of enzyme was chosen to reduce the cost of operation.

353 The last factor studied was the initial concentration of substrate; reactions with 100, 300 and 500 g kg⁻¹ of carbohydrates at 50 °C, pH 6.5, with 3 U mL⁻¹ of enzyme 354 355 were carried out. At the lowest substrate concentration, the reaction was too fast, and 356 after 5 h of reaction the remaining lactose was 14%. In this condition, the highest 357 amount of trisaccharides formed was 14% after 1 h of reaction, to be then quickly hydrolyzed. Nevertheless, when the highest concentration of carbohydrates (500 g kg⁻¹) 358 359 was used, the lactose hardly was hydrolyzed after 24 h of reaction. In assays performed with 6 U mL⁻¹ and 500 g kg⁻¹ of enzyme and carbohydrate concentration, respectively, 360 no improvement in GOS yields were obtained as compared to those reported by using 361 300 g kg⁻¹ of starting carbohydrate (data not shown). 362

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364 CONCLUSIONS

To summarize and according to the obtained results, the maximum formation of GOS was achieved after 5 h of reaction carried out at pH 6.5 and 50 °C with 300 g kg⁻¹ of carbohydrates and 3 U mL⁻¹ of β -galactosidase, giving rise to 24% monosaccharides, 25% lactose, 11% lactulose, and 40% GOS with DP 2-4 (and whose distribution was 16% formed disaccharides, 21% trisaccharides and 3% tetrasaccharides). These results highlight the formation of oligosaccharides with a different structure and, thus, with potentially different prebiotic properties.

372 Several papers have demonstrated that glycosidic linkages, monosaccharide 373 composition and degree of polymerization of GOS contribute toward the selectivity of 374 fermentation by beneficial bacteria.¹⁹⁻²⁰ In this context, the production of a mixture of prebiotics with a wide diversity of structural features might provide a value-added functional ingredient since it could broaden its positive effects on the modulation of gut microbiota. Likewise, the presence of lactulose, in addition to GOS, could provide an additional value to the final product since lactulose has shown to exert a series of biological activities, such as prebiotic action³⁵, improvement of the intestinal transit time³⁶, as well as other beneficial physiological actions, such as the treatment of chronic constipation, hepatic encephalopathy, or inflammatory bowel disease.³⁷

382 In conclusion, our results could contribute to the diversification of synthesized 383 oligosaccharides, indicating that a novel approach, based on the combined process of 384 isomerization of lactose from cheese WP using a food-grade catalyst (egg shell) and, 385 subsequent, enzymatic transgalactosylation with β -galactosidase from *B. circulans*, was 386 useful to produce a mixture composed of a 50% of potentially prebiotic carbohydrates 387 formed by lactulose, and GOS derived from lactose and lactulose. Both type of GOS 388 have proven to be an excellent alternative to monosaccharides to support growth of probiotic and improve their survival through the gastrointestinal tract.²⁶ 389

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Figure 1. HPLC-RID profile of carbohydrate mixture obtained by transgalactosylation reaction of isomerizated cheese whey permeate at pH 6.5, 50 °C for 5 h with βgalactosidase from *B. circulans* (3 U ml⁻¹) and initial carbohydrate concentration of 300 mg mL⁻¹. Identified peaks: glucose (Glc) (1); galactose (Gal) (2); lactulose (Lu) (3); lactose (Lac) (4), β-D-Gal*p*-(1→6)-D-Glc (allolactose) (5); β-D-Gal*p*-(1→4)-Lac (6); β-D-Gal*p*-(1→4)-Lu (7).



Figure 2. Effect of pH on hydrolysis of isomerized cheese whey permeate (300 mg mL⁻ of carbohydrates) and oligosaccharide production during the enzymatic treatment with β-galactosidase from *Bacillus circulans* (3 U mL⁻¹) at 50°C and pH (X) 7.4; (\blacksquare) 6.5; (\blacktriangle) 5.5. Vertical bars represent standard deviations (*n* = 4).



Figure 3. Effect of temperature on hydrolysis of isomerized cheese whey permeate (300 mg mL⁻¹ of carbohydrates) and oligosaccharide production during the enzymatic treatment with β-galactosidase from *Bacillus circulans* (3 U mL⁻¹) at pH 6.5 and (**X**) 40 °C; (**■**) 50 °C; (**▲**) 60 °C. Vertical bars represent standard deviations (n = 4).



Figure 4. Effect of enzyme concentration on hydrolysis of isomerized cheese whey permeate (300 mg mL⁻¹ of carbohydrates) and oligosaccharide production during the enzymatic treatment with β galactosidase from *Bacillus circulans* (X) 1.5 U mL⁻¹; (\blacksquare) 3 U mL⁻¹; (\blacktriangle) 6 U mL⁻¹ at 50°C pH 6.5. Vertical bars represent standard deviations (n =544 4).



Table 1. Content of galactose, glucose, <i>epi</i> -lactose, lactulose and lactose (mean \pm standard deviation, <i>n</i> =4) produced during heating at reflux of permeate powder solutions at a concentration of 300 g kg ⁻¹ , pH 6.8, and 30 g kg ⁻¹ of egg shell powder.								
Time	Galactose	Glucose	Epi-lactose	Lactulose	Lactose			
(min)	g kg ⁻¹							
0	0.8 ± 0.2	1.2 ± 0.2	n.d.*	n.d.	293.5 ± 5.1			
60	3.0 ± 0.2	1.1 ± 0.1	0.4 ± 0.1	22.4 ± 0.1	261.1 ± 4.6			
90	4.5 ± 0.5	1.0 ± 0.1	0.8 ± 0.1	32.0 ± 1.4	238.8 ± 8.0			
120	6.9 ± 0.3	1.2 ± 0.1	1.0 ± 0.1	38.3 ± 0.1	232.5 ± 5.8			
150	7.0 ± 0.2	1.0 ± 0.0	1.1 ± 0.0	48.2 ± 0.3	209.1 ± 1.9			
180	10.2 ± 0.2	1.0 ± 0.0	1.4 ± 0.0	43.9 ± 1.8	200.6 ± 3.8			
*n.d. No detected								