

18 **Abstract**

19 The production of prebiotic galactooligosaccharides (GOS) from lactose has been widely
20 studied whereas the synthesis of new prebiotic oligosaccharides with improved properties as
21 those derived from lactulose is receiving an increasing interest. Understanding the mechanism
22 of enzymatic oligosaccharides synthesis from lactulose would help to improve the quality of
23 the products in a rational way as well as to increase the production efficiency by optimally
24 selecting the operating conditions. A detailed kinetic model describing the enzymatic
25 transgalactosylation reaction during lactulose hydrolysis is presented here for the first time.
26 The model was calibrated with the experimental data obtained in batch assays with two
27 different β -galactosidases at various temperatures and concentrations of substrate. A complete
28 system identification loop, including model selection, robust estimation of the parameters by
29 means of a global optimization method and computation of confidence intervals was
30 performed. The kinetic model showed a good agreement between experimental data and
31 predictions for lactulose conversion and provided important insights into the mechanism of
32 formation of new oligosaccharides with potential prebiotic properties.

33

34 **Keywords:** kinetic models, lactulose, transgalactosylation, model selection, parameter
35 estimation, identifiability analysis.

36

37 **1. - Introduction**

38 The increased awareness about the relationship between the activity of colon bacteria and
39 health has lead to the enrichment of some food with prebiotics, defined as “selectively
40 fermented ingredients that allow specific changes, both in the composition and/or activity in
41 the gastrointestinal microflora that confer benefits upon host well-being and health”
42 (Roberfroid, 2007). The beneficial properties of galactooligosaccharides (GOS) on the gut
43 microflora, particularly as prebiotics, are well-known and a number of studies about their
44 enzymatic production by the conversion of lactose catalyzed by β -galactosidases from
45 different origin have been addressed (Iwasaki et al., 1994; Chen et al., 2003; Kim et al.,
46 2004). The hydrolysis process and the transgalactosylation reaction of lactose take place
47 simultaneously making the mechanism very complicated. Effective models for GOS synthesis
48 are of great interest since they would allow GOS production to be optimized (Gosling et al.,
49 2010), thus, different authors have developed kinetic models to explain the formation of these
50 interesting compounds (Mahoney, 1998; Boon et al., 1999; Kim et al., 2004). However, data
51 fitting for this type of models can be very challenging and the identifiability of candidate
52 models should be checked in parallel to model calibration. Further, the standard use of local
53 optimization methods for parameter estimation, such as Levenberg-Marquardt, can result in
54 convergence to local solutions. Therefore, a proper derivation of kinetic models for this type
55 of systems requires the analysis of possible correlations among parameters and the utilization
56 of robust and efficient methods for model calibration.

57 Prebiotic carbohydrates escape digestion in the upper gastrointestinal tract and are fermented
58 by bacteria in the colon, leading to the proliferation of bacteria that are beneficial for health in
59 humans. Because the place where fermentation mainly occurs (proximal or distal colon) is an
60 important factor influencing the extent of the prebiotic effect (Delzenne, 2003), the
61 development of new types of functional carbohydrates with specific fermentation properties

62 seems to be of interest. Lactulose is a well known disaccharide with excellent prebiotic
63 activity that it is mainly consumed by the bacteria of the proximal colon (Tuohy et al, 2002).
64 Therefore, it is reasonable to assume that lactulose-derived oligosaccharides originated during
65 enzymatic hydrolysis of lactulose might be bioactive carbohydrates slowly fermented and,
66 therefore, with higher colonic persistence than lactulose (Cardelle-Cobas et al., 2008). Thus,
67 recently, in our research group, enzymatic transgalactosylation of lactulose with β -
68 galactosidases from the commercial preparations Lactozym 3000L HP-G and Pectinex Ultra
69 SP-L was studied and new structures such as 6'-galactosyl-lactulose and 1-galactosil-lactulose
70 were characterized for the first time (Martinez-Villaluenga et al., 2008; Cardelle-Cobas et al.,
71 2008). In spite of these studies, no systematic investigation has been done on the kinetic of
72 formation of these compounds. Therefore, we focused the present study on the development
73 of a mathematical model to describe the kinetics of oligosaccharide synthesis and lactulose
74 hydrolysis with the β -galactosidases from Lactozym 3000L HP G and Pectinex Ultra SP-L at
75 various temperatures and substrate concentrations.

76

77 **2. - Materials and methods**

78 *2.1. - Batch reactions*

79 Time-course reactions for hydrolysis and transgalactosylation of lactulose with the β -
80 galactosidase from Pectinex Ultra SP-L produced by *Aspergillus aculeatus* were carried out at
81 333 K for 24 h with initial lactulose concentrations of 0.73, 1.33 and 1.93 M, in 0.1 M sodium
82 phosphate buffer, pH 6.5 and 16 U/mL of β -galactosidase. The influence of temperature was
83 studied at 313, 323 and 333 K with 1.33 M as initial concentration of lactulose (Cardelle-
84 Cobas et al., 2008).

85 For the β -galactosidase of Lactozym 3000L HP-G produced by *Kluyveromyces lactis*, the
86 assays were carried out with a initial concentration of lactulose of 0.73, 1.33 and 1.93 M in

87 0.05 M potassium phosphate buffer and 1 mM of $MgCl_2$, pH 6.5, 3 U/mL of enzyme, 323 K
88 and 24 h of reaction (Martinez-Villaluenga et al., 2008). The influence of temperature was
89 also studied with 0.73 M of initial lactulose at 313 and 323 K.

90 Lactulose solutions were heated before the enzyme was added and maintained at the required
91 temperature throughout all of the experiments. Reactions were performed in individual
92 Eppendorf tubes incubated in an orbital shaker at 300 rpm. Samples were taken at different
93 time intervals and the enzyme was inactivated by heating the sample in water bath at 100 °C
94 for 5 min. The samples were stored at -18°C for subsequent analysis. All assays were
95 performed in duplicate.

96 The carbohydrate composition of the reaction mixtures was determined by High Performance
97 Liquid Chromatography with Pulsed Amperometric Detection (HPAEC-PAD) on an ICS2500
98 Dionex system. Acquisition and processing of data were achieved with Chromeleon software
99 version 6.7 (Dionex Corp., Sunnyvale, CA). Separations were performed at room
100 temperature, following the method of Splechna et al. (2006). Detection time and voltage
101 parameters were set according to waveform A (Dionex. Technical Note 21).

102 2.2. - *Kinetic modeling and estimation of model parameters*

103 Given a kinetic model and a set of experimental data, the aim of parameter estimation is to
104 calibrate the model so as to reproduce the experimental data in the best possible way.
105 Calibration of nonlinear models is usually a very challenging task due to nonconvexity that
106 may be overcome by the use of global optimization techniques. However, the key question
107 when trying to identify the parameters of a model is not only whether the model fits the
108 experimental data but also whether the computed parameters are uniquely determined
109 (Schittkowski, 2007). This question is often neglected leading to models that are able to
110 accurately fit the data but with meaningless parameters due to their huge confidence intervals
111 that are not always computed. In order to develop a proper mechanistic model, a complete

112 system identification loop has to be performed (Ljung, 1999). This includes collecting the
113 experimental data, choosing the model structure(s), defining a quality criterion (cost
114 function), optimizing the parameters with respect to the chosen fitting criterion, evaluating the
115 uncertainty of the estimated parameters and validating the results questioning each of the
116 steps in case the model is proven to be inadequate.

117 *2.2.1- Model selection*

118 The model was selected on the basis of the existent literature about the lactose hydrolysis and
119 transgalactosylation. Moreover, the principle of parsimony, stating that “things should not be
120 multiplied beyond necessity” was also taken into account (Posada and Buckley, 2004). In
121 order to select the most adequate among nested models, the Akaike information criterion
122 (Akaike, 1974), containing a penalty function for increase in the number of parameters, was
123 used in this work. On the other hand, sometimes there is prior knowledge indicating a more
124 complex phenomenological model than statistical criteria allows. Thus, simplifying the model
125 structure may lead to arbitrary values for the phenomenological parameters with unrealistic
126 optimistic evaluation of their uncertainty. In these cases, it is advisable to fix the
127 nonidentifiable parameters to some nominal values coming from the literature or other
128 reliable sources and fit the rest of them.

129 In conclusion, the discrimination between competing models is a delicate task where a
130 compromise between the goodness of the fit, the mechanistic significance and the quality of
131 the estimated parameters in terms of confidence intervals should be achieved.

132 *2.2.2. - Cost function for model calibration*

133 Once the characterization of the model has been performed, the identification problem is
134 stated as the optimization of a scalar cost function $J(p)$ with respect to the model parameters,
135 p . The cost function is usually a certain weighted distance measure between the experimental
136 values corresponding to the measured variables, represented by the vector \tilde{y} , and the

137 predicted values for those variables, represented by the vector y . Therefore, the optimal value
138 of p will depend on the cost function chosen. The most widely used cost function (Walter and
139 Pronzato, 1997), the weighted least squares criterion, was considered here:

$$140 \quad J(p) = \sum_{i=1}^{NE} \sum_{j=1}^{NV} \sum_{k=1}^{NM_{ij}} \frac{(\tilde{y}_{ijk} - y_{ijk}(p))^2}{\sigma_{ijk}^2} \quad (1)$$

141 where σ_{ijk} correspond to the standard deviation of the experimental data, NE is the number of
142 experiments, NV the number of variables and NM_{ij} the number of sampling points per variable
143 and experiment. In this way, data with high standard deviation will have less impact on the
144 solution than those determined more accurately. The weighting factors can be chosen
145 iteratively. If the minimization of the initially chosen cost function leads to a model with an
146 unsatisfactory behavior in some region, the weighting factors associated with this zone could
147 be increased in order to improve it (at the cost of deteriorating the fit somewhere else).

148 In this study, the experimental data were fitted to the proposed model using the SSm GO
149 toolbox, a global optimization metaheuristic based on Scatter Search developed for parameter
150 estimation in nonlinear dynamic biochemical systems (Egea et al., 2007; Rodriguez-
151 Fernandez et al., 2006a).

152 2.2.3. - *Identifiability analysis*

153 In order to guarantee the quality of the estimated parameters, a practical identifiability
154 analysis should be performed. This study aims to answer the question: given a model
155 structure, would the parameters of the model be uniquely identified from the available
156 (limited and noisy) data? (Jacquez and Greif, 1985; Audoly et al., 2001). There are mainly
157 two aspects to be checked on a detailed identifiability analysis: sensitivity analysis and
158 parameter correlation.

159 The sensitivity analysis indicates which parameters are the most important and most likely to
160 affect the predictions of the model. For the sake of simplicity, in this work, we applied a

161 linear sensitivity analysis which consists of calculating a linear approximation of how much a
 162 variable changes due to a given change in a parameter. In order to make these measures
 163 comparable for parameters and states of different order of magnitude, relative measures were
 164 used where the sensitivity function is normalized by the value of the parameter and the state:

$$165 \quad S_{\theta,j} = \frac{p_{\theta}}{y_j} \frac{\partial y_j}{\partial p_{\theta}} \quad (2)$$

166 For very simple cases, the visual analysis of the relative sensitivity plots can be enough to
 167 determine the relative importance of the parameters. However, that becomes intractable when
 168 the size of the problem increases and a quantitative justification is needed for establishing a
 169 parameters ranking. Brun et al. (2001) recommend the use of the measure δ_{θ}^{msqr} as a ranking
 170 criterion in the context of weighted least squares estimation:

$$171 \quad \delta_{\theta}^{msqr} = \sqrt{\sum_{i=1}^{NE} \sum_{j=1}^{NV} \sum_{k=1}^{NM_{ij}} S_{\theta,ijk}^2} \quad (3)$$

172 A large value of the sensitivity index means that a change in the parameter p_{θ} has an
 173 important effect on the model outcome. This makes the parameter p_{θ} identifiable with the
 174 data available if all the other parameters are fixed and the larger the sensitivity the more
 175 accurately a single parameter can be identified. Therefore, values of critical parameters can be
 176 refined while parameters having a little effect can be simplified or even ignored (Karnavas et
 177 al., 1993).

178 Although necessary, high parameter sensitivity is not enough to ensure the identifiability of
 179 the model. In the case of several parameters, the sensitivity functions of the parameters have
 180 to be linearly independent. In this study, the degree of linear dependence among the
 181 sensitivity functions was measured by means of a correlation analysis based on the Fisher
 182 Information Matrix (*FIM*) as described in Rodriguez-Fernandez et al. (2006b). Correlations
 183 among parameters close to +1 or -1, mean that the parameters are not individually identifiable

184 because a change in one parameter can be compensated by changes in the other parameters. In
185 that case, an infinite number of parameter sets fitting the experimental data with the same
186 accuracy would exist, thus the confidence intervals would be very large. For this reason, the
187 model should be reduced by fixing some of the parameters to their nominal values or by
188 properly grouping some sets.

189 *2.2.4. - Confidence intervals*

190 After fitting the parameters p to the experimental data, it is important to obtain a measure of
191 the quality of the estimators. In principle, the objective is to obtain the probability distribution
192 of the estimated parameters or an adequate characterization of it, for instance, by computing
193 different percentiles of the distribution. However, in most of the cases this distribution is
194 unknown, therefore, it is necessary to obtain an approximation of it.

195 A widely used method for describing the confidence intervals of the estimated parameters is
196 the one based on the *FIM*. Nevertheless, this method presents important disadvantages due to
197 its linear nature; therefore in this work, the bootstrap method (Joshi et al., 2006), which
198 provides a more robust approximation, was used.

199 **3. - Results and discussion**

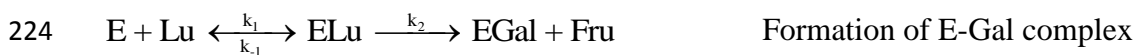
200 *3.1. - Establishment of the kinetic model*

201 Since no previous studies exist on the mechanism of formation of oligosaccharides derived
202 from lactulose, we first hypothesized that it is similar to the synthesis of GOS from lactose.
203 Thus, according to the models available in the literature (Boon et al., 1999; Kim et al., 2004),
204 lactulose (Lu) would act as both, substrate and glycosyl acceptor being mainly acceptor to
205 form trisaccharides (Tri) when the concentration is high. Moreover, galactose (Gal) would be
206 bound to the free enzyme to form the galactosyl-enzyme complex (EGal) for further
207 transgalactosylation reactions with galactose or fructose (Fru) as acceptors to produce
208 galactosyl-galactose disaccharides (GalGal) and galactosyl-fructose disaccharides (GalFru).

209 In addition, the synthesis of disaccharides and trisaccharides was assumed to be reversible.
 210 Unlike other models, mutarotation of galactose (Bakken et al., 1992) and separate production
 211 of tri- and tetrasaccharides (Iwasaki et al., 1994) were not taken into account since this would
 212 increase the number of parameters leading to identifiability problems. The formation of
 213 monosaccharide-enzyme complexes (EI) avoiding the advance of the transgalactosylation
 214 reaction was subject to further investigation.

215 Moreover, the experimental results obtained with the β -galactosidase from Pectinex Ultra SP-
 216 L, showed that the compound 6'-galactosyl-lactulose was the main trisaccharide formed,
 217 while 6-galactobiose was the disaccharide formed in the highest proportion. Therefore, only
 218 the formation of galactosyl-galactose (GalGal) disaccharides was taken into account. In
 219 addition, the inhibition assays showed that only galactose caused competitive inhibition on
 220 the formation of trisaccharides when the lowest concentration of lactulose was used in the
 221 experiments.

222 On the basis of these theoretical considerations and our experimental data, the following
 223 scheme was proposed for the reactions with the β -galactosidases from Pectinex Ultra SP-L:



229 Once the enzymatic reactions were proposed, and before starting the estimation of parameters,
 230 the experimental results were checked based on the sugar residue balance. Thus, it can be
 231 determined that, the materials, in each experiment, were conserved for the galactose (Gal) and

232 fructose (Fru) moiety with an error lower than 10% based on the following conservation
 233 equations:

234 Galactose moiety: $[Lu]_0 - [Lu] \approx [Gal] + 2[GalGal] + 2[Tri]$

235 Fructose moiety: $[Lu]_0 - [Lu] \approx [Fru] + [Tri]$

236 The balance equation for the enzyme is $[E] = [E]_0 - [EI] - [ELu] - [EGal]$

237 where $[Lu]_0$ is the initial mole concentration of substrate.

238 Thus, the differential equations for the reactions showed above are:

239
$$\frac{d[Lu]}{dt} = -k_1 [Lu][E] + k_{-1} [ELu] - k_3 [EGal][Lu] + k_{-3} [Tri][E] \quad (4)$$

240
$$\frac{d[Gal]}{dt} = -k_4 [EGal][Gal] + k_{-4} [GalGal][E] + k_6 [EGal] - k_{-6} [Gal][E] - k_7 [Gal][E] + k_{-7} [EI] \quad (5)$$

241
$$\frac{d[Fru]}{dt} = k_2 [ELu] \quad (6)$$

242
$$\frac{d[Tri]}{dt} = k_3 [EGal][Lu] - k_{-3} [Tri][E] \quad (7)$$

243
$$\frac{d[GalGal]}{dt} = k_4 [EGal][Gal] - k_{-4} [GalGal][E] \quad (8)$$

244
$$\begin{aligned} \frac{d[E]}{dt} = & -k_1 [Lu][E] + k_{-1} [ELu] + k_3 [EGal][Lu] - k_{-3} [Tri][E] + k_4 [EGal][Gal] \\ & - k_{-4} [E][GalGal] + k_6 [EGal] - k_{-6} [E][Gal] + k_7 [E][Gal] - k_{-7} [EI] \end{aligned} \quad (9)$$

245
$$\frac{d[ELu]}{dt} = k_1 [Lu][E] - k_{-1} [ELu] - k_2 [ELu] \quad (10)$$

246
$$\begin{aligned} \frac{d[EGal]}{dt} = & k_2 [ELu] - k_3 [EGal][Lu] + k_{-3} [Tri][E] - k_4 [EGal][Gal] \\ & + k_{-4} [E][GalGal] - k_6 [EGal] + k_{-6} [E][Gal] \end{aligned} \quad (11)$$

247
$$\frac{d[EI]}{dt} = k_7 [Gal][E] - k_{-7} [EI] \quad (12)$$

248 In order to validate the proposed model, equations [4-12] were fitted to the available data
 249 from the experiments with the β -galactosidase of Pectinex Ultra SP-L at different lactulose
 250 concentrations (0.73, 1.33 and 1.93 M), temperature being constant (333 K), aiming to find

251 the best set of parameters able to describe the oligosaccharides synthesis at any initial
252 concentration of lactulose among the considered range.

253 Some of the studies found in the literature (Chen et al., 2003) consider the quasi-steady-state
254 approach for the intermediate complexes (in this work EGal and ELu). Therefore, in this
255 preliminary screening, it was also assumed that $d[\text{EGal}]/dt \approx 0$ and $d[\text{ELu}]/dt \approx 0$. The fit
256 obtained following these considerations presented some deficiencies, in particular for the
257 prediction of fructose and galactose concentration so, unlike other authors, the quasi-steady-
258 state approximation was not taken into account. In addition, it can be observed that, the
259 enzyme-lactulose (ELu) complex was minimally formed in the reaction mixture in
260 comparison with the EGal complex. Since the ELu almost did not participate in the reaction,
261 it was removed from the model as well as the parameters corresponding to the coefficients for
262 the formation and hydrolysis (k_1 and k_{-1}) of ELu.

263 The relevance of the inhibition by galactose is not clear in the literature. While authors as
264 Mozaffar et al. (1984) and Bakken et al. (1992) claim its importance, others as Boon et al.
265 (1999) consider it negligible under their experimental conditions. In this work, the model
266 without inhibition was considered as a submodel of the one with inhibition and the Akaike's
267 criterion was computed for both models making use of the experimental data. The value of the
268 criterion for the model including inhibition is higher than the one of the model without it, so it
269 can be said that the fit of the data is not significantly better than that obtained with the model
270 without inhibition. Therefore, the inhibition was not considered on the model and the
271 reactions were consequently simplified.

272 *3.2. - Model calibration for the Pectinex experiments*

273 Once the mechanistic model was selected, the resulting equations were fitted to the data of
274 three experiments with the β -galactosidase of Pectinex Ultra SP-L at the different lactulose
275 concentrations (0.73, 1.33 and 1.93 M) at 333 K. The measured species were lactulose,

276 fructose, trisaccharides, galactose and galactosyl-galactose disaccharides at six sampling
277 times (0, 1, 3, 5, 7 and 24 hours). The kinetic coefficients (k_1 , k_3 , k_{-3} , k_4 , k_{-4} , k_6 and k_{-6}) and
278 the initial concentration of the enzyme were optimized by means of the SSm GO toolbox,
279 using the weighted least squares criterion as cost function. The data predicted with the
280 estimated set are in good agreement with the experimental data for the five species measured,
281 so it was used to analyze the practical model identifiability.

282 The sensitivity analysis (see Figure 1) shows that the model is influenced by changes on each
283 of the eight estimated parameters. However, the correlation matrix presented in Figure 2
284 indicates that the correlations between k_3 , k_4 and k_6 and their reverse coefficients (k_{-3} , k_{-4} and
285 k_{-6} , respectively) are very high. In order to minimize this identifiability problem, the reverse
286 constants (k_{-3} , k_{-4} and k_{-6}) were set to a nominal value and only the direct ones were
287 estimated. As a result, almost the same fit was achieved (only 3% worse) and the
288 identifiability and confidence intervals were strongly improved. Since no relevant values for
289 the inverse constants were found in the literature, the assigned ones were somehow arbitrary.
290 The value of the estimated constants and their confidence intervals for the best fit are shown
291 in Table I. As can be observed in Figure 3, the fits for this enzyme for different initial
292 concentrations of lactulose (0.73 M (A), 1.33 M (B) and 1.93 M (C)), showed a good
293 agreement between the predicted and the experimental data. Moreover, the mathematical
294 model is able to accurately predict the higher production of disaccharides and trisaccharides
295 when the initial concentration of lactulose increases.

296 *3.3. - Model calibration for the Lactozym experiments*

297 Since the developed model was able to fit the experimental data corresponding to the
298 synthesis of lactulose-derived oligosaccharides with the β -galactosidase from Pectinex Ultra
299 SP-L, it was interesting to analyze if the same model could describe the synthesis of
300 oligosaccharides with the β -galactosidase of Lactozym 3000L HP G used in previous studies

301 about the formation of new compounds using lactulose as substrate (Martinez-Villaluenga et
302 al., 2008). For this enzyme, experimental data at different concentrations of lactulose (0.73-
303 1.93 M) and different temperatures (313 and 323 K) were also available. The
304 chromatographic profile obtained with this enzyme was quite similar to that obtained for the
305 synthesis of oligosaccharides with Pectinex Ultra SP-L but the amount of compounds was
306 different. Thus, in these assays, two trisaccharides were obtained in a major proportion, the
307 6'-galactosyl-lactulose and the 1-galactosil-lactulose. In this way, the same kinetic model
308 with the same assumptions (absence of inhibition at high concentrations of Lu, formation of
309 galactosyl-galactose type disaccharides...) was fitted to the data corresponding to three
310 experiments at the same temperature (323 K) and different initial concentrations of lactulose
311 (0.73, 1.33 and 1.95 M).

312 The production of disaccharides was small and it increased with increasing time of reaction
313 for both enzymes at all temperatures. This production showed a pretty linear trend for
314 Pectinex Ultra SP-L but for Lactozym 3000L HP G the concentration seemed to be zero or at
315 least non measurable during the first 4-6 hours at high concentrations of enzyme, presenting
316 sudden increases afterwards. This made the fitting of the disaccharides very difficult with the
317 available model and, at the same time, they strongly influence the value of the objective
318 function due to the small standard deviation of these points (despite the fact that at this low
319 concentration the experimental errors are known to be quite high). That makes the estimation
320 to neglect other species that are more important for this study, so the weights of the objective
321 function were manually tuned in order to avoid this bias.

322 The sensitivity analysis for the best set of parameters obtained with these data and the tuned
323 objective function showed a significantly smaller sensitivity of the model output to the
324 reverse parameters (k_{-3} , k_{-4} and k_{-6}) than to the direct ones and a very high sensitivity to the
325 initial concentration of the enzyme. Moreover the correlation between k_1 and the reverse

326 constants is equal to one so, following the previous scheme, the reverse constants (k_{-3} , k_{-4} and
327 k_{-6}) were set to a nominal value.

328 The value of the best set of parameters and their confidence intervals are shown in Table I. As
329 expected, the value found for k_1 is higher than that estimated for Pectinex Ultra SP-L at 333 K
330 since the decrease in the concentration of lactulose and the increase in the concentration of
331 fructose are faster for Lactozym 3000L HP G at 323 K. The values found for the formation of
332 trisaccharides (k_3) and disaccharides (k_4) were in the same order of magnitude, which means
333 that, in this case, both galactose and lactulose are good glycosyl acceptors to form these
334 compounds. In contrast, for Pectinex Ultra SP-L at 333 K, the value of k_3 was higher than k_4
335 indicating that lactulose acts as a better acceptor than galactose, which explains the fact that,
336 under the assayed conditions, more trisaccharides are formed at a faster reaction rate. Figure 4
337 shows the good agreement found between the experimental data and the predicted values for
338 the best fit, supporting the goodness of the model.

339 *3.4. - Modeling the temperature dependence*

340 To complete this study, a more complex scheme allowing handling experiments at different
341 temperatures was included into the model. As a first approach, the rate constants (k_1 , k_3 , k_{-3} ,
342 k_4 , k_{-4} , k_6 and k_{-6}) were assumed to follow the Arrhenius equation:

$$343 \quad k = K_0 e^{-Ea/RT} \quad (13)$$

344 where Ea = Activation energy (J/mol)

345 K_0 = pre-exponential factor

346 R = ideal gas constant (8.3 J/mol K)

347 T = temperature (K)

348 The expression of the Arrhenius equation for the direct and inverse reactions was employed in
349 the model as in the following example:

350 Formation of trisaccharides: $k_3 = K_{03} e^{-Ea3/RT}$

351 Hydrolysis of trisaccharides: $k_{-3} = K_{03i} e^{-E_{a3i}/RT}$

352 The rate expressions for the proposed model, above mentioned, were fitted simultaneously for
353 the five different experiments carried out with the β -galactosidase of Pectinex Ultra SP-L at
354 various initial concentrations of substrate (0.73, 1.33 and 1.93 M) and temperatures (313, 323
355 and 333 K). The concentration of enzyme and the pH remained constant in all the
356 experiments. Each experiment described the lactulose, fructose, galactose, trisaccharide and
357 disaccharide evolution in time. Figure 5 shows the experimental data and the model prediction
358 for the three batch experiments. As can be seen, a good agreement was obtained between the
359 experimental and simulated values.

360 The final concentration of trisaccharides increases as the temperature increases being
361 maximum at 333 K. This phenomenon is captured by the model and reflected on the value of
362 the parameters, E_{a3} is greater than E_{a3i} , meaning that the formation of trisaccharides is favored
363 by the temperature. In the case of the disaccharides, the opposite effect is observed; the final
364 concentration is smaller for higher temperatures. Accordingly, E_{a4i} is larger than E_{a4} meaning
365 that the inverse reaction is favored by the temperature more than it is the direct reaction.
366 Therefore, the production of disaccharides decreases at high temperatures.

367 The same procedure was followed for the synthesis of oligosaccharides by the β -galactosidase
368 of Lactozym 3000L HP G. Thus, the data coming from four experiments at different lactulose
369 concentrations (0.73, 1.33 and 1.93 M) and temperatures (313 and 323 K) were fitted using
370 the same kinetic model. Simulated values were plotted as continuous lines in Figure 6, while
371 experimental results are given as symbols, showing the good agreement obtained for this
372 enzyme. In this case the available temperatures were only two, therefore, the fitting of the
373 model was more challenging and the decreasing of disaccharides formation with the
374 temperature was not captured properly. That explains why E_{a4} is larger than E_{a4i} even if the
375 final concentration of disaccharides is slightly smaller at 323 K than at 313 K. Regarding the

376 trisaccharides, their behavior is properly captured. The data show that lactulose is a better
377 acceptor of glycosyl at 313 K than at 323 K and the estimated parameters point out in the
378 same direction, E_{a3i} is larger than E_{a3} . Since the constant of the inverse reaction increases with
379 the temperature, the amount of trisaccharides will also decrease.

380 The numeric values obtained for the best fit in the temperature-dependent model for the two
381 enzymes used in this work are showed in Table II. It is worth noting that, the correlation
382 found between the different parameters, especially between the pre-exponential factors and
383 their corresponding activation energy for the Arrhenius equations are very close to 1, so it
384 cannot be stated that these sets of parameters are the only ones providing a good fit to the
385 experimental data. This is due to, in one hand, to the difficulties inherent to the Arrhenius
386 equation structure already reported by other authors as Pritchard and Bacon (1978). On the
387 other hand, the limited amount of experimental data (*i.e.* for the β -galactosidase only data at
388 two different temperatures and with a difference of only 10°C) makes the identification even
389 harder.

390 Table III shows the reaction rates coefficients calculated from the best parameters obtained
391 for the proposed model at a fixed temperature. The temperatures selected were those for
392 which a maximum formation of trisaccharides was obtained, i. e., 333 K for the Pectinex
393 Ultra SP-L and 313 K for the Lactozym 3000L HP G. Although identifiability results indicate
394 a strong dependence of the direct and reverse constants, we can indicate for all calculated
395 parameters at the most favorable temperature among the range of this study for the formation
396 of trisaccharides, a set of parameters that give an approximation of the behavior of both
397 enzymes in the formation of oligosaccharides derived from lactulose. As can be seen in the
398 table, for the β -galactosidase of Lactozym 3000L HP G the fitted reaction rate coefficient for
399 the formation of the EGal complex was much higher than that obtained for the β -
400 galactosidase of Pectinex Ultra SP-L, indicating a higher rate of formation and, therefore, a

401 faster decrease in lactulose concentration in the reaction medium when Lactozym 3000L HP
402 G is used as source of β -galactosidase. For Pectinex Ultra SP-L, the fitted reaction rate
403 coefficient for the formation of trisaccharides (k_3) was found to be higher than that for
404 disaccharides (k_4) and the values found for the reverse reactions (k_{-3} and k_{-4}) were similar.
405 Therefore, for the β -galactosidase of Pectinex Ultra SP-L at 333 K, it is possible to establish
406 that lactulose acts a better glycosyl acceptor to form trisaccharides but these are more easily
407 broken down; galactose is a poorer acceptor than lactulose but has more chances to form
408 disaccharides at lower concentrations of lactulose and the disaccharides originated are much
409 more stable. On the contrary, in the case of Lactozym 3000L HP G, the fitted reaction rate
410 coefficient for trisaccharide formation (k_3) was similar to that found for disaccharides (k_4)
411 being the values obtained for the reverse reactions (k_{-3} , k_{-4}) strikingly different. Thus, for the
412 β -galactosidase of Lactozym 3000L HP G, both lactulose and galactose are good glycosyl
413 acceptors to form trisaccharides and disaccharides, being the latter more rapidly hydrolyzed
414 and, therefore, less stable.

415 **4. - Conclusions**

416 The proposed model can describe the oligosaccharide synthesis using the β -galactosidases
417 from Pectinex Ultra SP-L (*A. aculeatus*) and Lactozym 3000L HP-G (*K. lactis*) at several
418 temperatures and initial concentrations of lactulose. The experimental data are in good
419 agreement with the predictions of the developed model. In accordance with the experimental
420 data, the kinetic parameters describing the reversible oligosaccharide synthesis are of different
421 magnitude for both β -galactosidases, since they produce different amounts and types of
422 oligosaccharides. The formation of trisaccharide was favored in the synthesis of
423 oligosaccharides using lactulose as substrate and Pectinex Ultra SP-L, whereas the formation
424 of disaccharides was higher when the β -galactosidase from Lactozym 3000L HP G was used
425 as enzyme. Moreover, the formation of trisaccharides is larger at high temperatures when

426 using Pectinex Ultra SP-L (maximum at 333 K) even though the formation of disaccharides is
427 larger at lower temperatures. In the case of the Lactozym 3000L HP-G, the production of both
428 di- and trisaccharides is higher at 313 K (the minimum temperature used for the experiments).
429 This is the first time that a complete system identification loop, including model selection
430 using the Akaike criterion, robust estimation of the parameters by means of a global
431 optimization method and computation of confidence intervals is performed for the kinetic
432 study on the formation of new oligosaccharides with potential prebiotic properties. Important
433 insights into the mechanism of formation of new oligosaccharides with potential prebiotic
434 properties were obtained from the developed model that could ultimately be used to select the
435 optimal operating conditions for increasing the efficiency of the production or for the
436 selective formation of a target di- or trisaccharide.

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520

521 **LIST OF FIGURES:**

522 FIGURE 1.- Local relative sensitivity of the eight parameters involved on the model
523 describing the lactulose conversion with β -galactosidase of Pectinex Ultra SP-L at constant
524 temperature.

525 FIGURE 2.- Correlation matrix of the eight parameters involved on the model describing the
526 lactulose conversion with β -galactosidase of Pectinex Ultra SP-L at constant temperature.

527 FIGURE 3.- Time-course reactions for lactulose conversion with β -galactosidase of Pectinex
528 Ultra SP-L with three different initial concentrations of lactulose (A) 0.73 M, (B) 1.33 M and
529 (C) 1.93 M and temperature of 333 K. Symbols are the points of experimental data and lines
530 are the predicted values for the best fit of the quasi-steady state model.

531 FIGURE 4.- Time-course reactions for lactulose conversion with β -galactosidase of Lactozym
532 3000L HP G with three different initial concentrations of lactulose (A) 0.73 M, (B) 1.33 M
533 and (C) 1.93 M and temperature of 323 K.

534 FIGURE 5.- Time-course reactions for lactulose conversion with β -galactosidase of Pectinex
535 Ultra SP-L with initial concentration of lactulose of 1.93 M and different temperatures (A)
536 313 K, (B) 323 K and (C) 333 K.

537 FIGURE 6.- Time-course reactions for lactulose conversion with β -galactosidase of Lactozym
538 3000L HP G with initial concentration of lactulose of 0.73 M and different temperatures (A)
539 313K and (B) 323K.

540

541 **TABLE CAPTIONS:**

542 Table I.-Optimal parameter for the hydrolysis of lactulose and synthesis of oligosaccharides
543 by the β -galactosidase from Pectinex Ultra SP-L (*Aspergillus aculeatus*) and Lactozym 3000L
544 HP G (*Kluyveromyces lactis*)

545

546 Table II.-Optimal parameter for the hydrolysis of lactulose and synthesis of oligosaccharides
547 by the β -galactosidase from Pectinex Ultra SP-L (*Aspergillus aculeatus*) and Lactozym 3000L
548 HP G (*Kluyveromyces lactis*)

549

550 Table III.-Reaction rate coefficients for the optimal temperature of formation of trisaccharides
551 by the β -galactosidases from Pectinex Ultra SP-L (333K) and Lactozym 3000L HP G (313K)

Table I.-Optimal parameter for the hydrolysis of lactulose and synthesis of oligosaccharides by the β -galactosidase from Pectinex Ultra SP-L (*Aspergillus aculeatus*) and Lactozym 3000L HP G (*Kluyveromyces lactis*)

Parameter	Estimated values	Estimated values
	<i>A. Aculeatus</i> (Pectinex Ultra SP-L)	<i>K. Lactis</i> (Lactozym 3000L HP G)
k_1	$3.6 \cdot 10^0 \pm 7.8 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$	$2.2 \cdot 10^2 \pm 5.9 \cdot 10^1 \text{ M}^{-1}\text{h}^{-1}$
k_3	$8.8 \cdot 10^0 \pm 1.6 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$	$3.4 \cdot 10^{-1} \pm 8.4 \cdot 10^{-2} \text{ M}^{-1}\text{h}^{-1}$
k_{-3}	$1.0 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$1.0 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$
k_4	$1.8 \cdot 10^0 \pm 3.4 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$	$2.9 \cdot 10^{-1} \pm 7.7 \cdot 10^{-2} \text{ M}^{-1}\text{h}^{-1}$
k_{-4}	$1.0 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$1.0 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$
k_6	$3.3 \cdot 10^0 \pm 6.3 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$	$4.4 \cdot 10^{-1} \pm 1.0 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$
k_{-6}	$1.0 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$1.0 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$
E_0	$1.5 \cdot 10^{-1} \pm 1.5 \cdot 10^{-2} \text{ M}$	$1.0 \cdot 10^{-1} \pm 1.9 \cdot 10^{-2} \text{ M}$

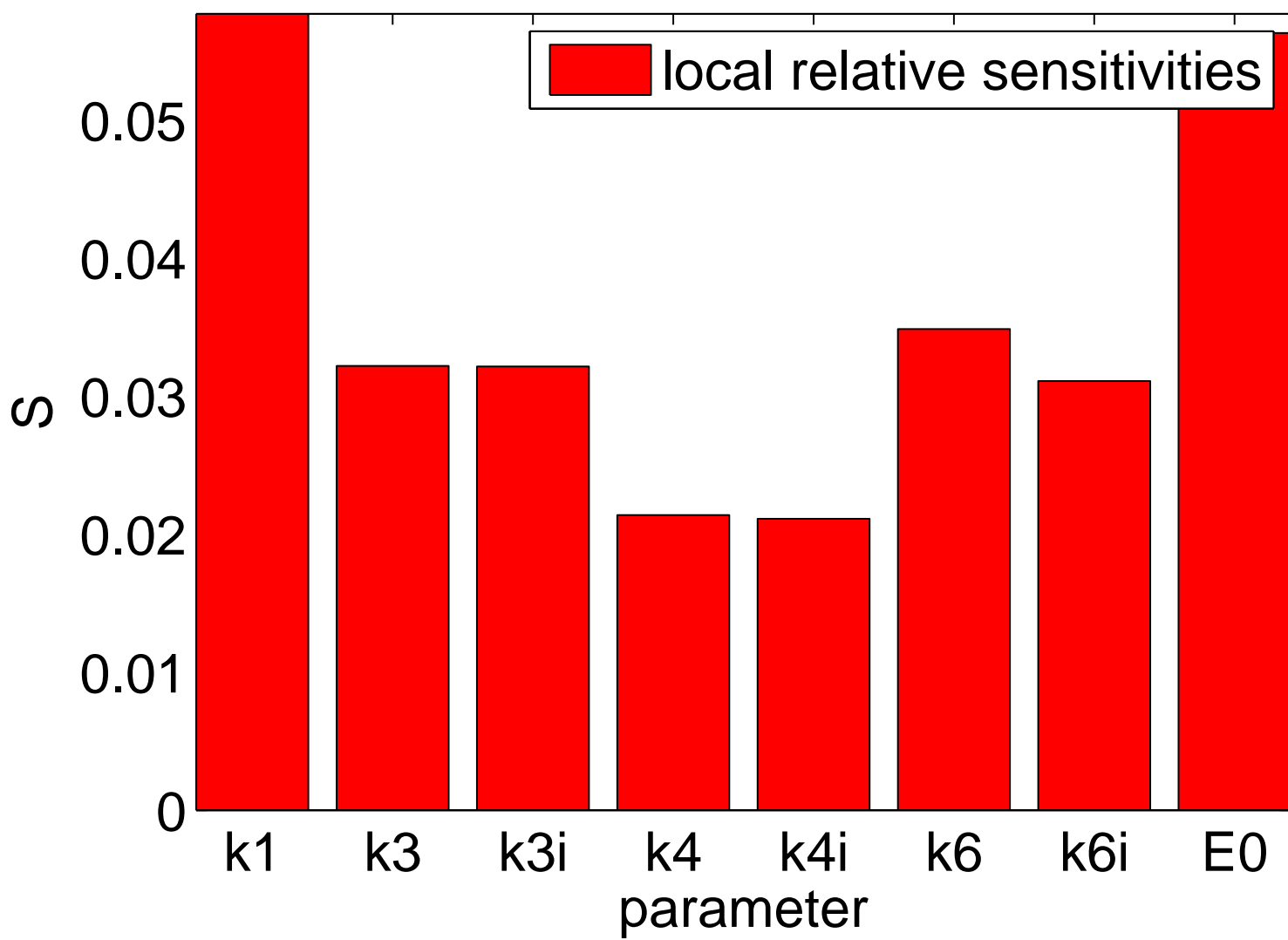
Table II.-Optimal parameter for the hydrolysis of lactulose and synthesis of oligosaccharides by the β -galactosidase from Pectinex Ultra SP-L (*Aspergillus aculeatus*) and Lactozym 3000L HP G (*Kluyveromyces lactis*)

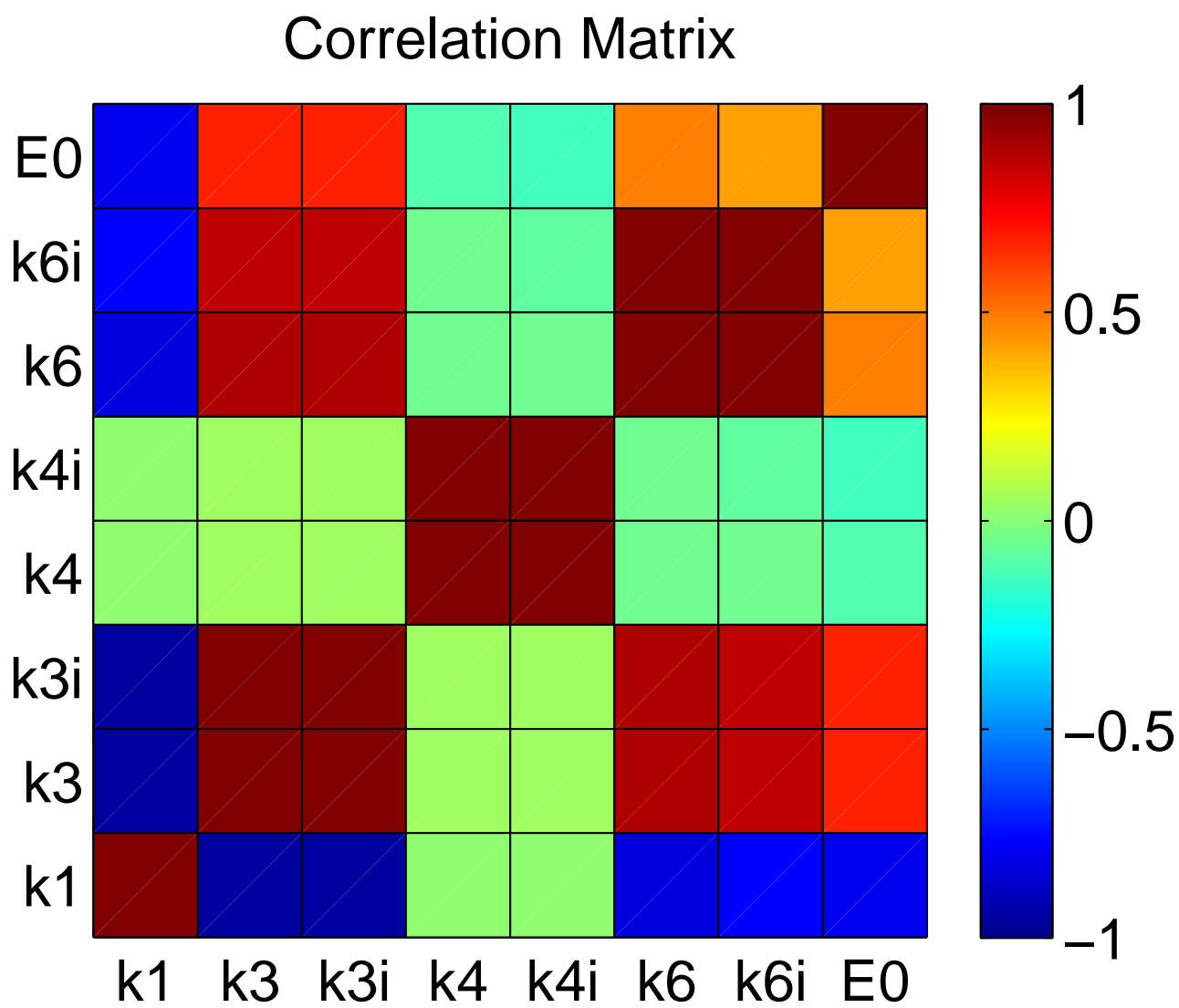
Parameter	Estimated value	Estimated value
	<i>A. aculeatus</i> (Pectinex Ultra SP-L)	<i>K. lactis</i> (Lactozym 3000L HP G)
k_{01}	$3.8 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$4.8 \cdot 10^3 \text{ M}^{-1}\text{h}^{-1}$
k_{03}	$1.9 \cdot 10^4 \text{ M}^{-1}\text{h}^{-1}$	$1.4 \cdot 10^1 \text{ M}^{-1}\text{h}^{-1}$
k_{03i}	$1.5 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$1.1 \cdot 10^6 \text{ M}^{-1}\text{h}^{-1}$
k_{04}	$3.2 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$	$2.6 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$
k_{04}	$5.3 \cdot 10^5 \text{ M}^{-1}\text{h}^{-1}$	$1.2 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$
k_{06}	$1.9 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$2.1 \cdot 10^1 \text{ M}^{-1}\text{h}^{-1}$
k_{06}	$1.1 \cdot 10^5 \text{ M}^{-1}\text{h}^{-1}$	$1.4 \cdot 10^3 \text{ M}^{-1}\text{h}^{-1}$
E_{a1}	$1.3 \cdot 10^4 \text{ J/M}$	$9.7 \cdot 10^3 \text{ J/M}$
E_{a3}	$2.2 \cdot 10^4 \text{ J/M}$	$9.0 \cdot 10^3 \text{ J/M}$
E_{a3i}	$1.0 \cdot 10^3 \text{ J/M}$	$2.8 \cdot 10^4 \text{ J/M}$
E_{a4}	$1.0 \cdot 10^3 \text{ J/M}$	$4.1 \cdot 10^3 \text{ J/M}$
E_{a4i}	$2.3 \cdot 10^4 \text{ J/M}$	$3.0 \cdot 10^2 \text{ J/M}$
E_{a6}	$1.4 \cdot 10^4 \text{ J/M}$	$8.4 \cdot 10^3 \text{ J/M}$
E_{a6i}	$2.2 \cdot 10^4 \text{ J/M}$	$6.4 \cdot 10^3 \text{ J/M}$
E_0	$2.0 \cdot 10^{-1} \text{ M}$	$6.6 \cdot 10^{-2} \text{ M}$

Table III.-Reaction rate coefficients for the optimal temperature of formation of trisaccharides by the β -galactosidases from Pectinex Ultra SP-L (333K) and Lactozym 3000L HP G (313K)

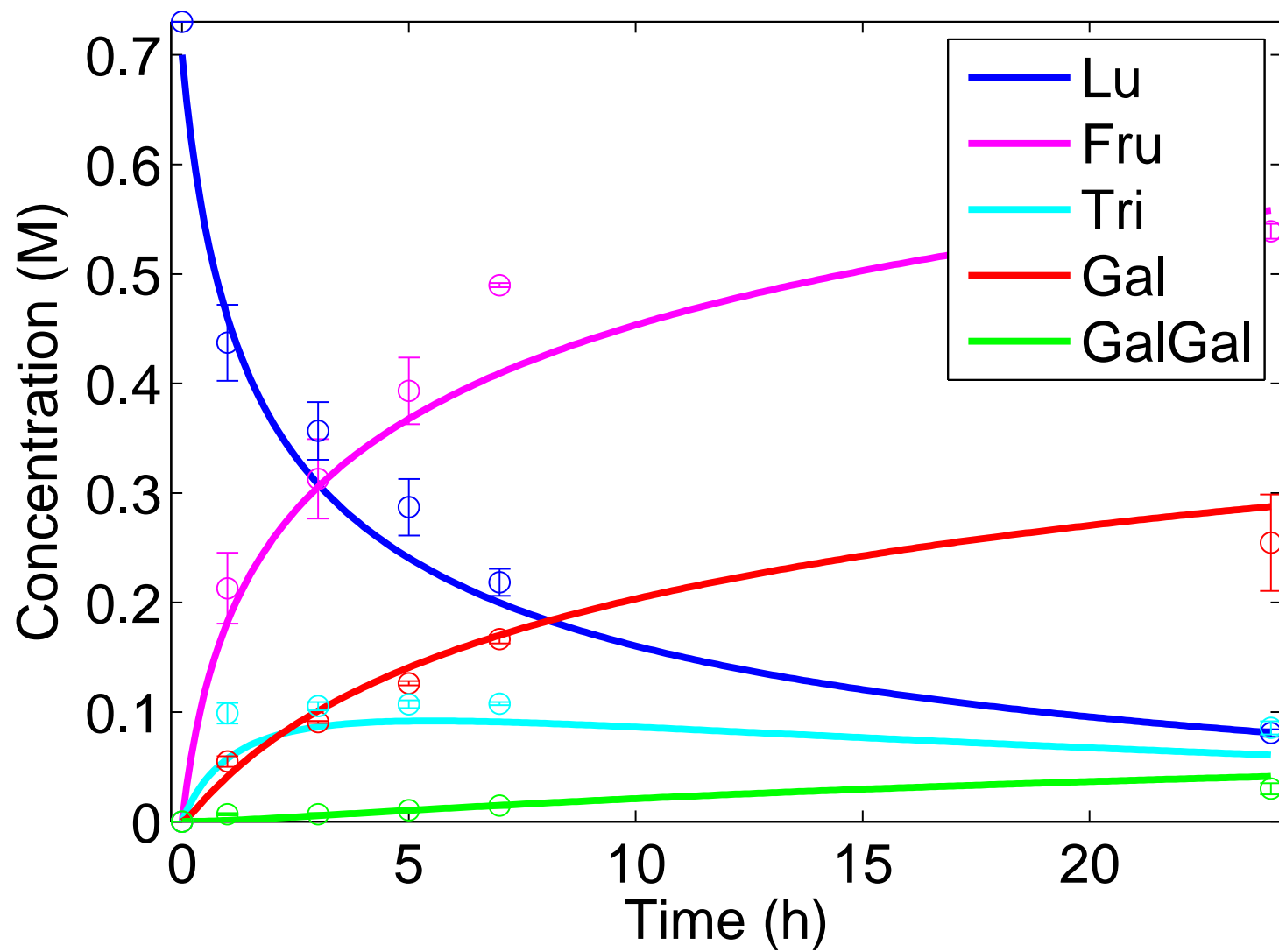
Reaction rate constants	Rate coefficients values	
	<i>A. aculeatus</i> (Pectinex Ultra SP-L)	<i>K. lactis</i> (Lactozym 3000 L HP-G)
k_1	$2.8 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$	$1.1 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$
k_3	$6.4 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$	$4.4 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$
k_3	$1.1 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$2.3 \cdot 10^1 \text{ M}^{-1}\text{h}^{-1}$
k_4	$2.3 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$	$5.4 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$
k_{-4}	$1.3 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$	$1.1 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$
k_6	$1.3 \cdot 10^0 \text{ M}^{-1}\text{h}^{-1}$	$8.3 \cdot 10^{-1} \text{ M}^{-1}\text{h}^{-1}$
k_{-6}	$4.0 \cdot 10^1 \text{ M}^{-1}\text{h}^{-1}$	$1.2 \cdot 10^2 \text{ M}^{-1}\text{h}^{-1}$

Figure(s)

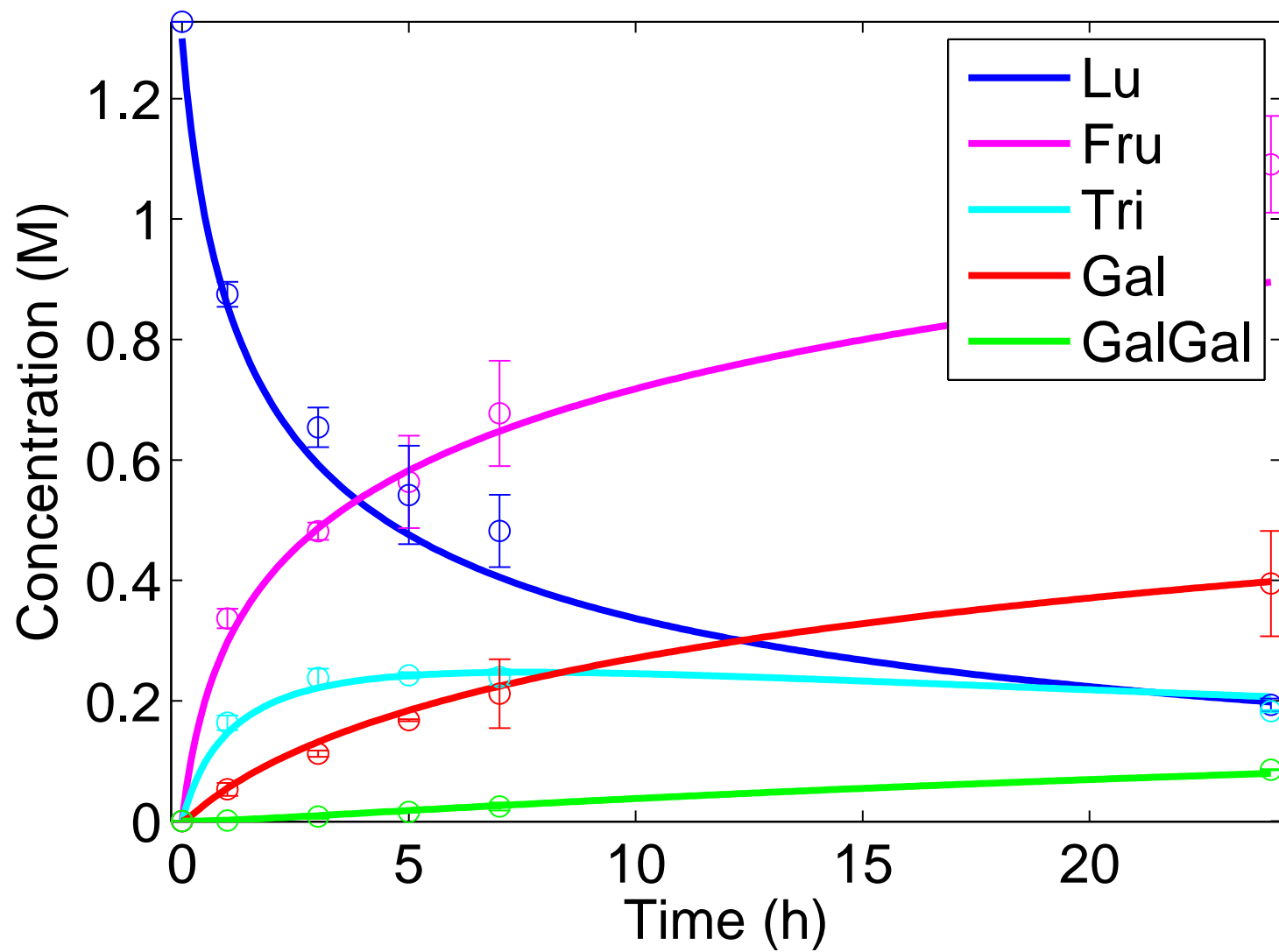




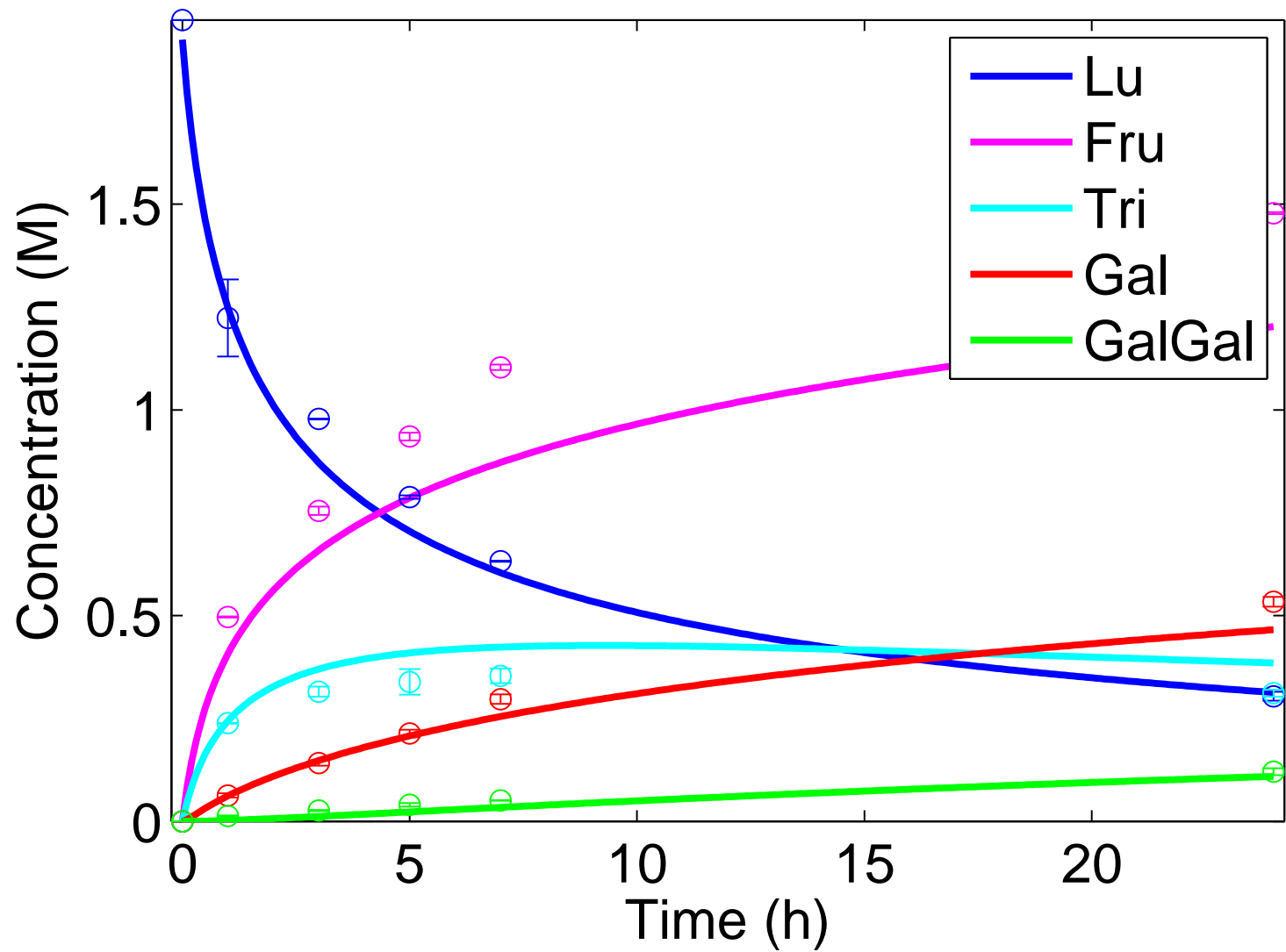
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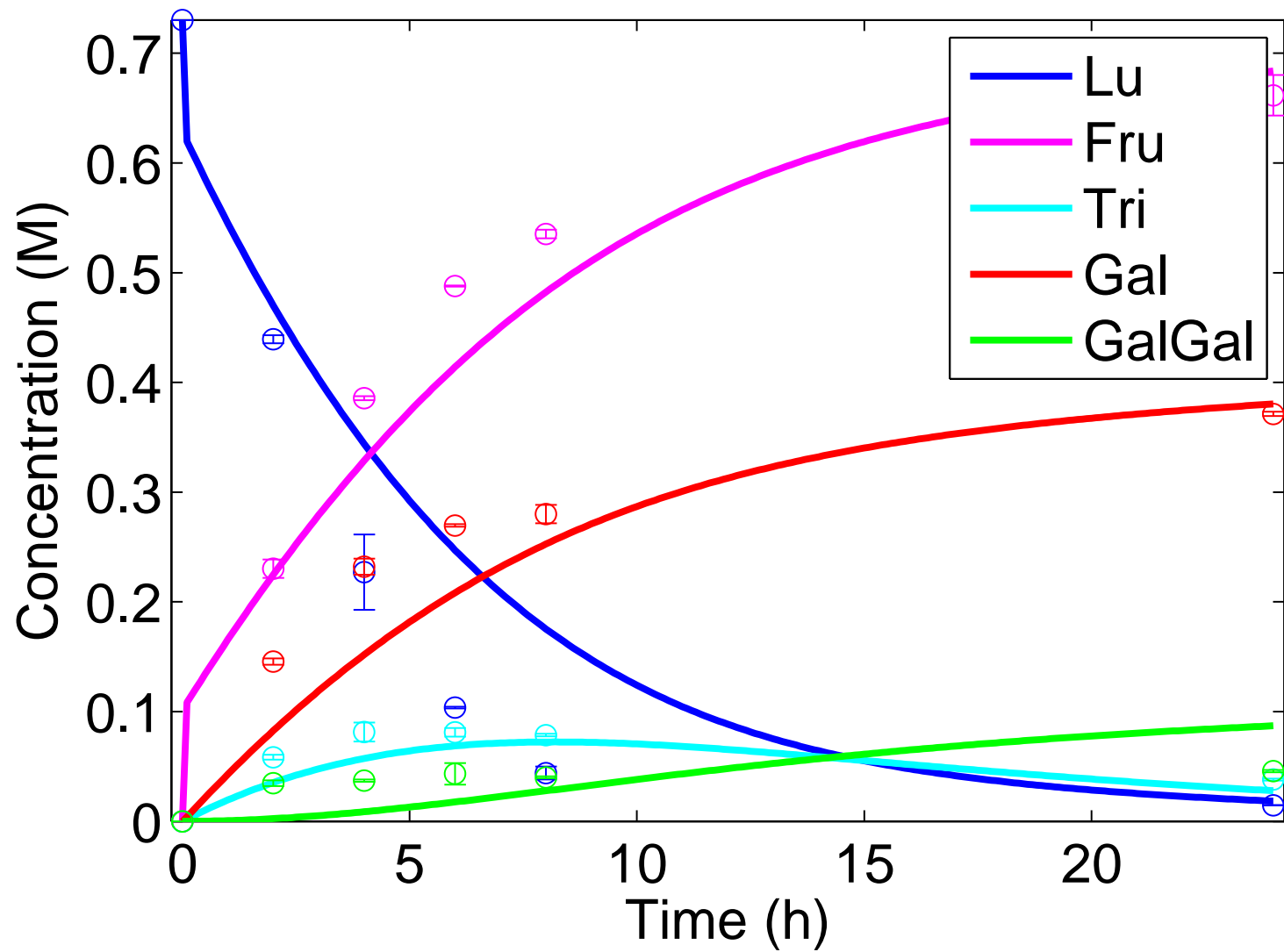
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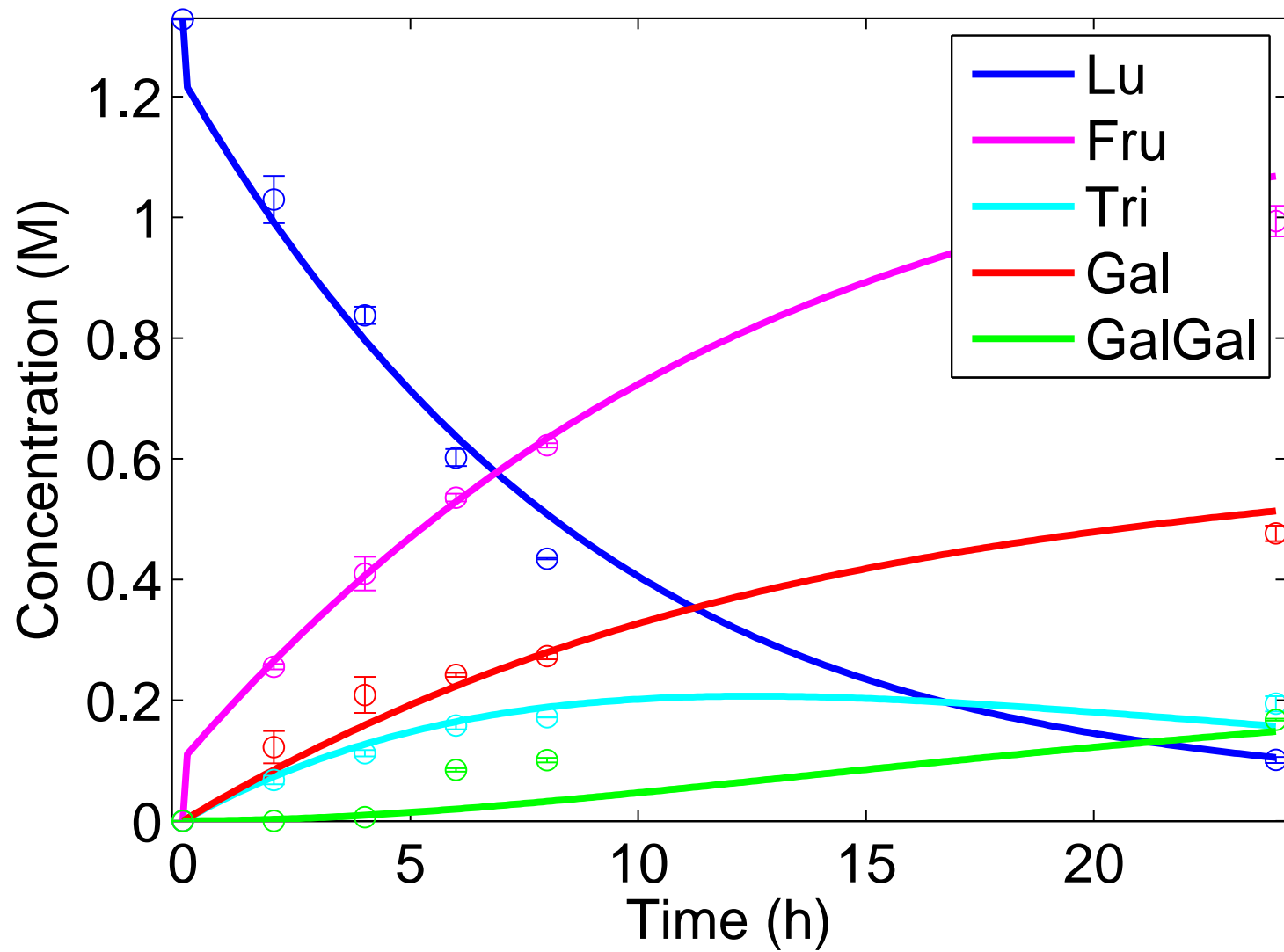
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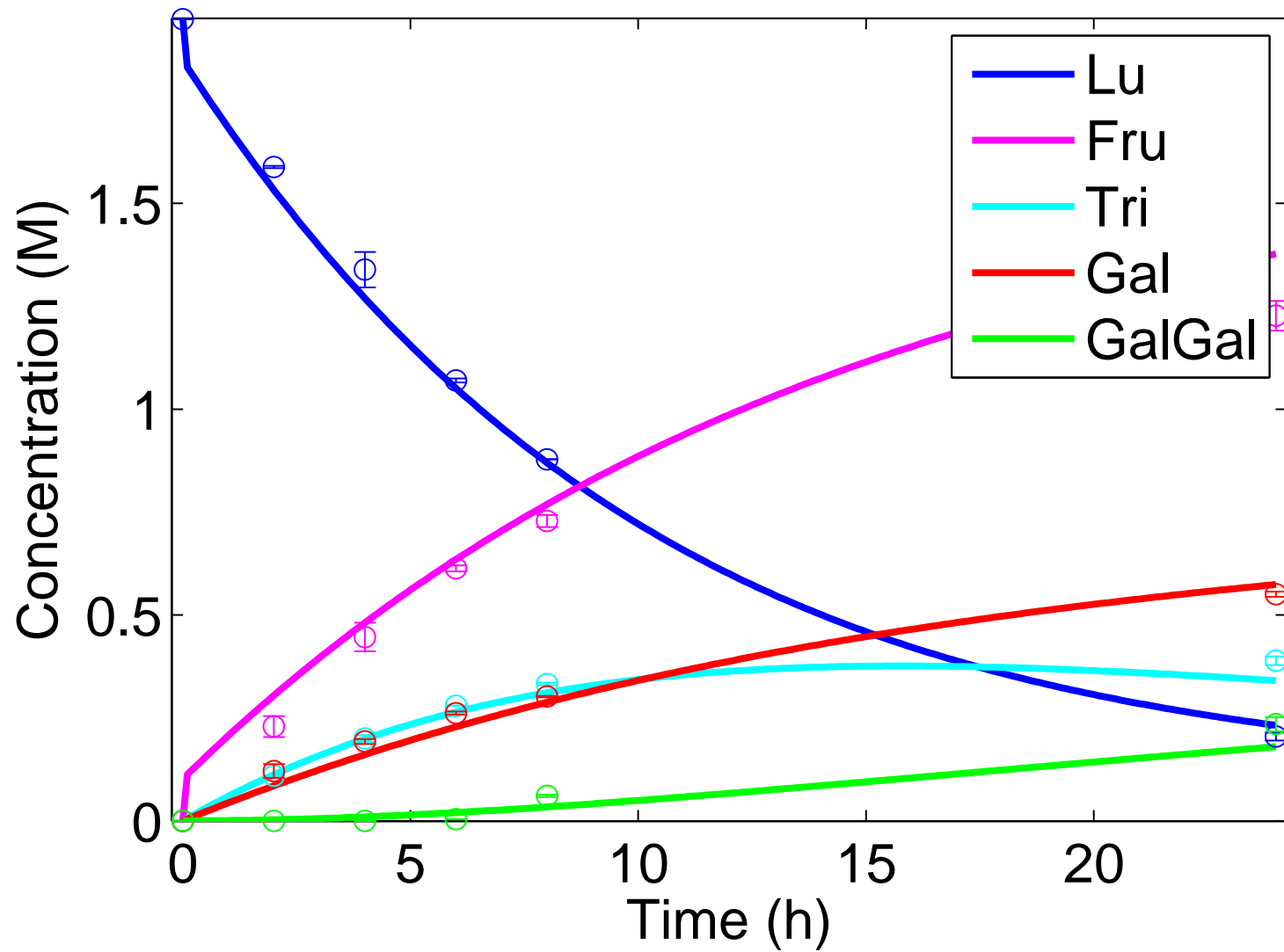
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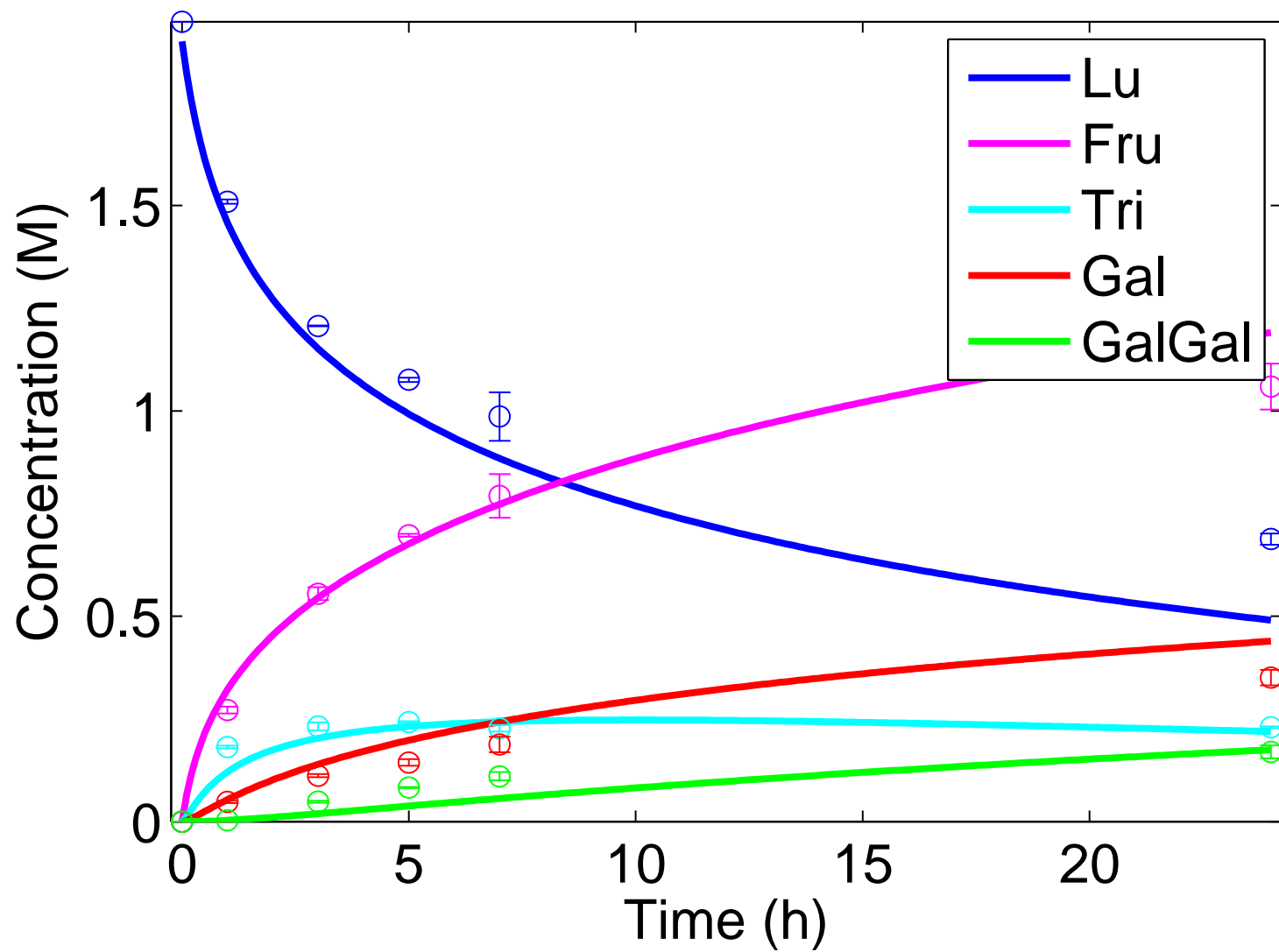
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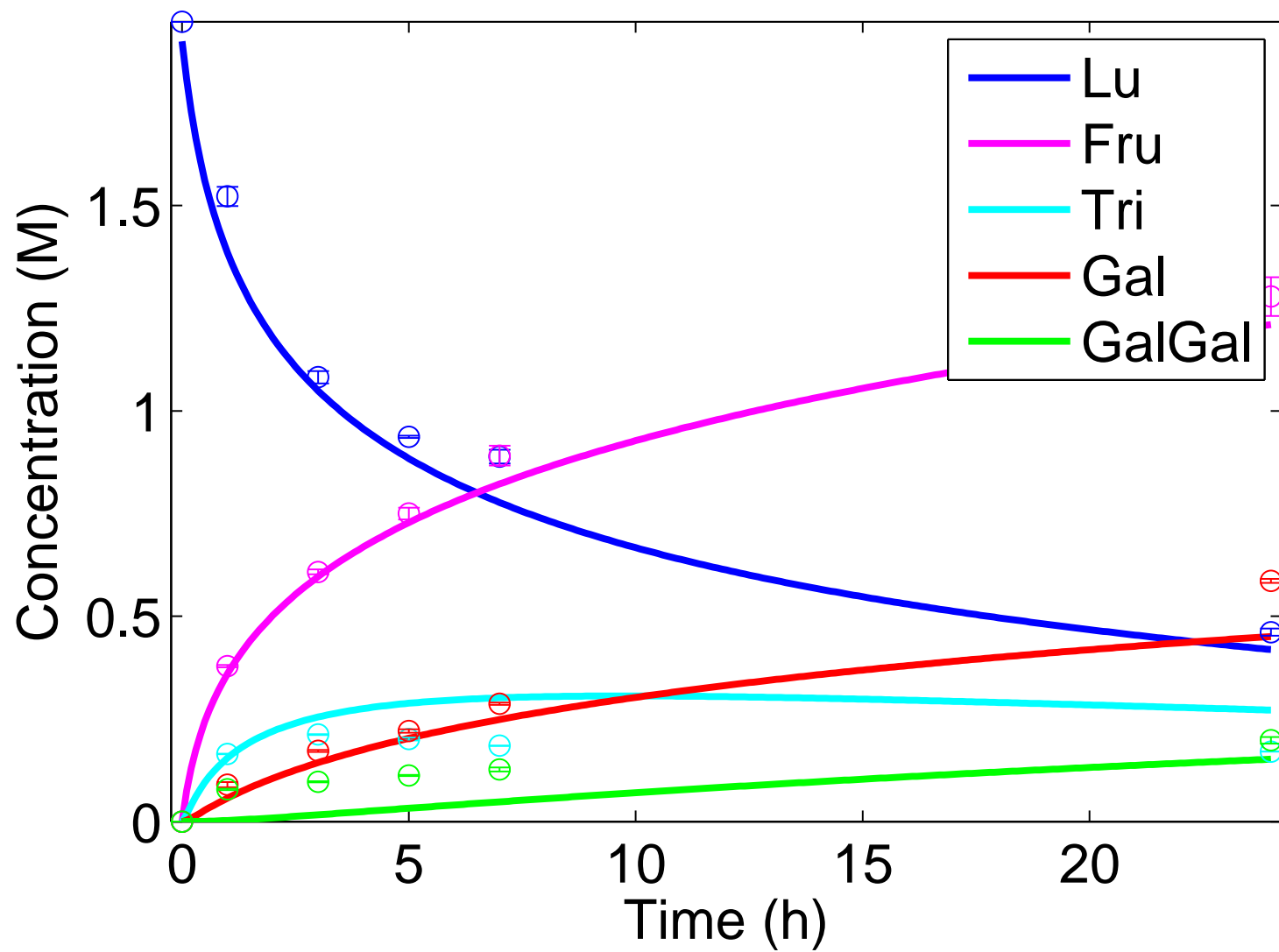
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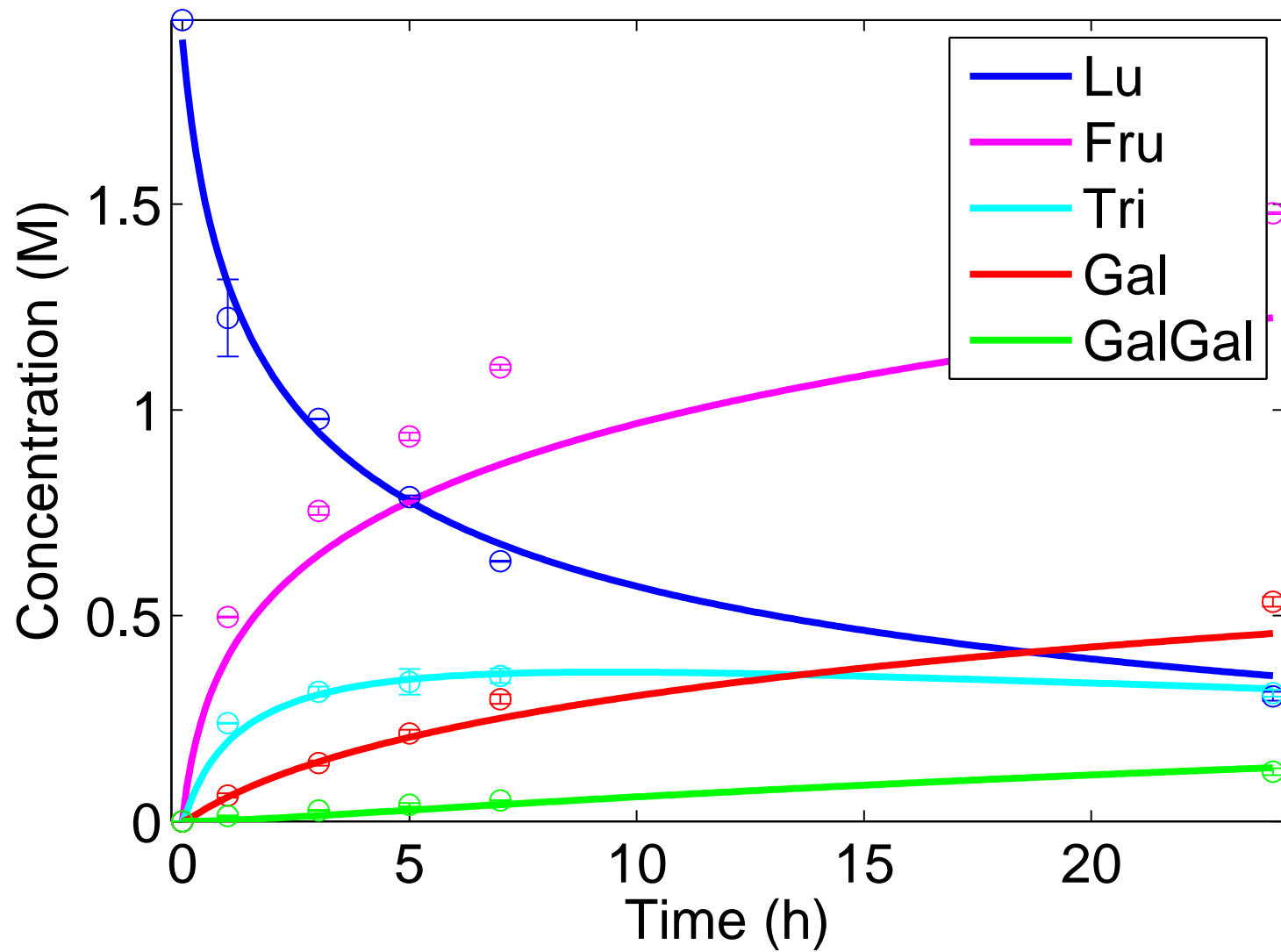
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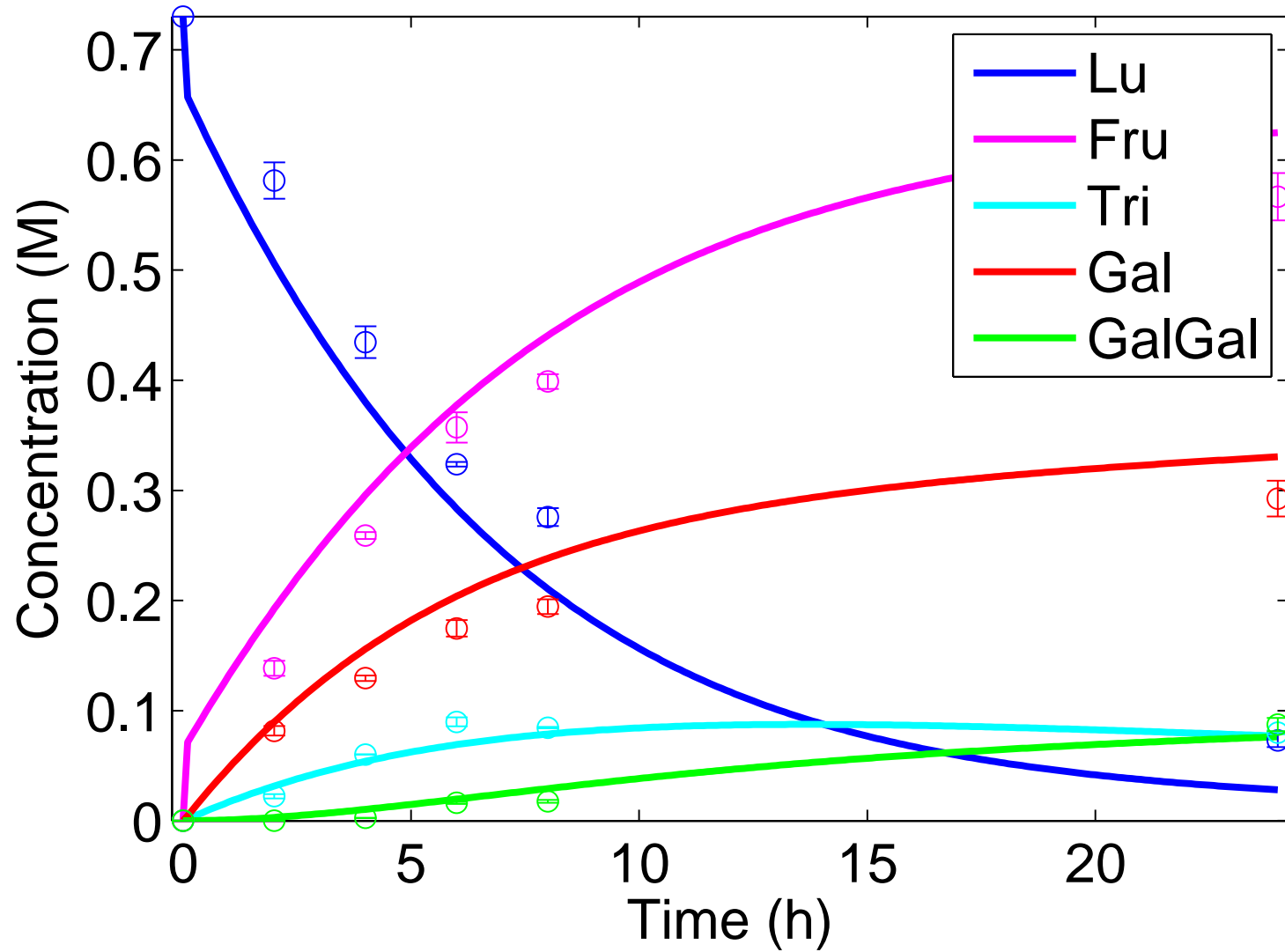
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