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2	Immobilization of $\beta$ -cyclodextrin in ethylene-vinyl alcohol copolymer for active
3	food packaging applications
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5	Carol López-de-Dicastillo <sup>1</sup> , Miriam Gallur <sup>2</sup> , Ramón Catalá <sup>1</sup> , Pilar Hernandez-Muñoz <sup>1</sup> ,
6	Rafael Gavara*'
7	
8	<sup>4</sup> Packaging Lab, Instituto de Agroquímica y Tecnología de Alimentos, CSIC
9	Apdo. de correos 73, 46100 Burjassot, SPAIN, <u>rgavara@iata.csic.es</u>
10	
11	<sup>2</sup> IIENE, Parque Tecnologico, c/Albert Einstein, 1, 46980 Paterna, SPAIN
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#### ABSTRACT

Current developments in active food packaging are focusing on incorporating agents 30 31 into the polymeric package walls that will release or retain substances to improve the 32 quality, safety and shelf-life of the food. Because cyclodextrins are able to form 33 inclusion complexes with various compounds, they are of potential interest as agents to 34 retain or scavenge substances in active packaging applications. In this study,  $\beta$ -35 cyclodextrin (BCD) was successfully immobilized in an ethylene-vinyl alcohol copolymer with a 44% molar percentage of ethylene (EVOH44) by using regular 36 37 extrusion with glycerol as an adjuvant. Films with 10%, 20% and 30% of BCD were 38 flexible and transparent. The presence of the agent slightly increased the glass transition 39 temperature and the crystallinity percentage of the polymer, that is to say, it induced 40 some fragility and a nucleating effect. The water vapor, oxygen and carbon dioxide 41 barrier properties of the materials containing  $\beta$ CD were determined and compared with 42 those of the pure polymeric material. Permeability to these three permeants increased 43 with the addition of  $\beta$ CD due to the presence of discontinuities in the matrix and to the internal cavity of the oligosaccharide. Also the CO<sub>2</sub>/O<sub>2</sub> permselectivity increased with 44 45 the addition of  $\beta$ CD. Finally, the potential effect of the composites in the food aroma 46 was analyzed. The materials with  $\beta$ CD preferentially sorbed apolar compounds such as 47 terpenes. This characteristic could be useful in active packaging applications for 48 preferentially retaining undesired apolar food components like hexanal or cholesterol.

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50 Keywords: β-cyclodextrin, EVOH copolymer, extrusion, immobilization, DSC,
51 retention of organic compounds, gas permeation.

#### **INTRODUCTION**

54 Active food packaging is one of the most dynamic emerging technologies that the food 55 industry is investigating as an alternative to traditional food techniques (intense heat 56 treatments, salting, acidification, drying, chemical preservation, etc.) for several uses, 57 especially combined with other technologies such as MAP, radiation, pulsed electric 58 fields, high pressure treatments, etc. Active food packaging is defined as the technology 59 in which the packaging system plays an active role in food preservation and quality 60 during the marketing process. Examples of active packaging technologies include the 61 use of oxygen scavengers, carbon dioxide or ethylene emitters and scavengers, ethanol 62 releasers, amine or aldehyde scavengers, and antimicrobial or antioxidant agents.

63 In many present-day active packaging technologies the active agent is placed in the 64 package with the food, in a small sachet, pad or device manufactured from a permeable 65 material which allows the active compound to achieve its purpose but prevents direct 66 contact with the food product, protecting the food from contamination or degradation. 67 Active packaging developments are now focusing on incorporating the agents into the 68 polymeric matrices which constitute the package walls; the resulting materials act by 69 releasing substances which have a positive effect on the food or by retaining undesired 70 substances from the food or the internal atmosphere of the package.

71 Because cyclodextrins (CDs) are able to form inclusion complexes with various 72 compounds, they present a potential interest as agents to retain or scavenge substances 73 such as odors, bitter compounds, lactose, cholesterol, etc., or to add aromas, colors, or 74 functional ingredients whose release could enhance the quality of the packaged product 75 and extend its shelf-life.

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Cyclodextrins (CDs) are cyclic oligosaccharides composed of several glucose units (6 units in  $\alpha$ CD, 7 units in  $\beta$ CD or 8 units in  $\gamma$ CD) linked by  $\alpha$ -(1-4) bonds. They are enzyme-modified starch derivatives with molecules which present amphipathic ring structures: the hydrophilic groups are on the outside of the molecular cavity, the 2- and 3-OH groups on the wider rim and the 6-OH group on the narrower, while the hydrophobic inner surface includes the ether-like anomeric oxygen atoms and the C3-H and C5-H hydrogen atoms. In aqueous solution, this hydrophobic cavity contains about 3 (αCD), 7 (βCD) or 9 (γCD) poorly held and easily displaceable water molecules.<sup>1</sup> The
water in the cavity has low density, as the cavities are large enough to accommodate
several more molecules. Thus, the cyclodextrin molecules may bind suitably-sized nonpolar aliphatic and aromatic compounds such as aroma compounds and lipophilic drugs.
They may bind in 1:1, 2:1 and 1:2 ratios, depending on the molecules involved.

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90 This unique structure enables CDs to form inclusion complexes, entrapping all or part 91 of a 'guest' molecule inside their cavities, principally by means of weak forces such as 92 van der Waals, dipole-dipole interactions, and hydrogen bonding. While the height of 93 the cyclodextrin cavity is the same for all three types, the number of glucose units 94 determines the internal diameter of the cavity and its volume. Based on these 95 dimensions,  $\alpha$ CD can typically complex low molecular weight molecules or compounds 96 with aliphatic side chains,  $\beta$ CD will complex aromatics and heterocycles and  $\gamma$ CD can 97 accommodate larger molecules such macrocycles and steroids. BCD is the seven-98 glucose cyclic oligosaccharide which has been on the GRAS list since 1992. It has a 99 cavity at the center of the molecule which allows complex formation with a wide 100 variety of organic molecules. BCD is nontoxic, edible, nonhygroscopic, chemically 101 stable and easy to separate, and overall is readily available at a low cost.

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103 Cyclodextrins have a wide range of applications in the food and pharmaceutical 104 industries. Food ingredients, bioactive compounds, or flavor compounds can be 105 complexed by CDs to protect them against oxidation, light-induced reactions, heatpromoted decomposition, loss by volatility, or sublimation, or to reduce undesired 106 tastes/odours.<sup>2,3</sup> Empty  $\beta$ CD is also being used in the food industry to entrap or remove 107 undesirable compounds such as bitter components from coffee and tea.<sup>4</sup> milk casein 108 hydrolysate,<sup>5</sup> ginseng extract,<sup>6</sup> or grapefruit or mandarin juices.<sup>7</sup> Reducing the 109 cholesterol in food is probably the main commercial use of  $\beta$ CD in the food sector.<sup>8</sup> 110

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Several applications have been described in which cyclodextrins or cyclodextrin derivatives have been immobilized in different polymeric supports. Cyclodextrin glucanotransferase has been immobilized onto a surface-modified polyethylene which has then been used to produce cyclodextrins from corn starch.<sup>9</sup> Modified cyclodextrins with different substituents (hydroxyl, acetyl, silanes ...) to improve polymer compatibility have been used to increase water permeability and reduce migration in
 extruded polyethylene and polypropylene films.<sup>10</sup>

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120 In this study, BCD was immobilized in an ethylene-vinyl alcohol copolymer and the 121 resulting materials were studied for their potential use in active packaging. Ethylene-122 vinyl alcohol copolymers (EVOHs) are a family of semicrystalline random copolymers 123 widely used in the food-packaging sector due to their outstanding properties as gas 124 barriers to oxygen and organic compounds (solvents and food aromas), as well as their considerable chemical resistance and high transparency.<sup>11</sup> The major drawback of these 125 materials in this application is their moisture sensitivity, which causes a significant 126 127 decrease in their gas barrier properties. Nevertheless, this water sensitivity can be useful 128 in the development of active packages for food, as food humidity is a potential 129 mechanism to trigger their activity. EVOH was selected as the vehicle for immobilizing 130 βCD because of its hydrophilicity and polarity. EVOH should present good chemical 131 compatibility with the external surface of the cyclodextrin molecule and the interior can 132 be used to design active packages based on the release of complexed agents or the 133 retention of undesirable food components.

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In this study, EVOH films containing  $\beta$ CD were prepared by conventional extrusion and the resulting materials were studied in order to characterize the effect of cyclodextrin addition on the most relevant properties of EVOH as a packaging material, namely its morphological, thermal and barrier properties.

139	MATERIALS AND METHODS				
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141	Chemicals and Reagents				
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143	Ethylene vinyl alcohol copolymer with a 44% ethylene molar content (EVOH44) was				
144	gently supplied by The Nippon Synthetic Chemical Company, (Osaka, Japan). Reagent-				
145	grade ethanol, $\alpha$ -pinene, d-limonene, linalool, citral, ethyl caproate, 2-nonanone,				
146	octanal, methyl-isobuthyl ketone, n-hexanal, n-hexanol, silica gel, magnesium chloride				
147	MgCl <sub>2</sub> .6H <sub>2</sub> O, magnesium nitrate Mg(NO <sub>3</sub> ) <sub>2</sub> .6H <sub>2</sub> O, sodium nitrite NaNO <sub>2</sub> , and sodium				
148	chloride NaCl were provided by Sigma (Madrid, Spain). Nitrogen, carbon dioxide and				
149	oxygen were provided by Abelló-Linde (Valencia, Spain)				
150					
151	$\beta CD$ was purchased from Wacker Fine Chemicals, S.L.(Barcelona) and glycerol from				
152	Sigma (Madrid). Water was obtained from a Milli-Q Plus purification system				
153	(Millipore, Molsheim, France).				
154					
155	Film Preparation				
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157	EVOH films containing $\beta$ CD were obtained by two methods: flat extrusion and				
158	compression molding. In both methods, cyclodextrins at different concentrations (10, 20				
159	and 30%) were incorporated into a hydrophilic EVOH44 material.				
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161	For the flat extrusion process, a glycerol-CD paste was prepared, mixed with the				
162	polymer pellets and melt-blended during extrusion. The mixture of the three				
163	components was extruded on a Brabender DSE 20/40 co-rotating twin screw extruder				
164	(Plastograph, Dusseldorf, Germany) at 200°C with a screw speed of 100 rpm. The				
165	resulting films were ca. 50 micrometers thick, although the thickness of every sample				
166	was individually measured with a digital Mitutoyo micrometer (Metrotec, San				
167	Sebastian, Spain) before testing.				
168					
169	For the compression molding process, the EVOH polymer was ground with a knife mill				
170	and sieved, then mixed with the cyclodextrin powder and compression-molded in a hot				

plate Carver press (Carver, Wabash, IN, USA) at a temperature of 190°C. The material
was compression-molded at 190°C and 20 bars for 1 minute, then the pressure was
increased to 200 bars. After a total of 4 minutes, the material was cooled for 2 minutes.
The films obtained were ca. 100 micrometers thick.

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176 The film samples were vacuum-packed in aluminum/LDPE bags and stored at room 177 temperature until the moment of analysis. The morphology of the composite, the degree 178 of immobilization of  $\beta$ CD, the thermal properties and the gas, water vapor and organic 179 compound barrier properties were studied.

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## 181 Morphology

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The materials were analyzed by Electronic Scanning Microscopy (SEM), using a Hitachi model S-4100 with a BSE AUTRATA detector and EMIP 3.0 image trapping. After being completely dried, the samples were broken up to investigate their crosssection. A cylindrical aluminum stub cut like a straight-backed chair, on which the film was fixed using a double-sided copper tape, was used in a specific way to observe the morphology of the cross section. The stubs holding the films were then coated with gold.

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### 191 Migration studies

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193 Since cyclodextrins are partially water soluble and the first objective is to use the 194 material for active food packaging, a preliminary study of cyclodextrin release from the 195 films was carried out by determining the global migration from the polymer into water, 196 as an aqueous food simulant, following EU regulations (UNE-EN 1186-3) with slight modifications.<sup>12,13</sup> In brief, 4-cm<sup>2</sup> samples of each of the films obtained were immersed 197 198 in 100 mL of freshly distilled Millipore water for periods of 1 and 10 days at 40°C and 199 the global migration values were determined on days 1 and 10 by calculating the weight loss according to the method prescribed in the applicable EC directives <sup>14-16</sup>. All the 200 201 samples were measured in triplicate.

- 203 Thermal Analysis
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Thermal properties were determined with a DSC Model Q2000 from TA Instruments (New Castle, DE, EEUU). Thermograms were obtained from -50°C to 250°C with a 10°C/min heating ramp. The glass transition and melting point temperature and enthalpy were calculated.

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## 210 Barrier Properties

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#### 212 Water vapor

WVP tests were carried out at 35, 50, 65, 75 and 100% RH and 23°C using permeability 213 214 cups (Elcometer, Manchester, UK) according to ISO 2528. Aluminum cups were filled 215 with 7 g of silica gel and sealed with vacuum silicon grease (Sigma, Barcelona, Spain) 216 and the film to be tested. The film was fixed with a flat Viton ring, an aluminum ring 217 and three press-screws. The cups were then stored in desiccators containing saturated 218 salt solutions to ensure the required relative humidity: magnesium chloride 219 MgCl<sub>2</sub>.6H<sub>2</sub>O, magnesium nitrate Mg(NO<sub>3</sub>)<sub>2</sub>.6H<sub>2</sub>O, sodium nitrite NaNO<sub>2</sub>, sodium 220 chloride NaCl and water for humidities of 35, 50, 65, 75 and 100% respectively. The 221 cups were weighed daily, and the plot of the weight increment over time provided the 222 water vapor transmission rate. These values were divided by the water pressure gradient 223 and multiplied by the sample thickness to obtain the water vapor permeability value.

The water sorption of the prepared films was also measured. Film samples were cut, put on aluminum dishes and placed in the above mentioned desiccators. The samples were weighed daily until constant. The films were then dried for 48 h at 60°C under vacuum and weighed. The sorption values were calculated as the water gain per 100 g of dry sample.

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230 Oxygen

231 The oxygen permeation rates of the materials were determined at 50 and 90% RH and 232 23°C using a OXTRAN Model 2/21 ML Mocon (Lippke, Neuwied, Germany). The film 233 samples were first conditioned at the RH of the experiment in the desiccators described 234 above. Two identical samples were then placed in the apparatus for analysis. The 235 samples were conditioned in the cells for 6 hours, then the transmission values were 236 determined every 45 min. After the permeation tests were completed, continuous 237 permeation experiments were carried out on each sample to determine the diffusion 238 coefficient (D). From the transmission rate values measured during the transient state,

the value of D was assessed from the solution to Fick's second law for the boundary
 conditions of an isostatic permeation experiment.<sup>17</sup>

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## 242 *Carbon dioxide*

The carbon dioxide permeation rates of the materials were determined at 50 and 90% 243 244 RH and 23°C using an isostatic permeation test.<sup>18</sup> In brief: a stainless-steel cell with two chambers separated by the film to be tested was used. A constant gas stream was passed 245 through each chamber. The permeant gas, carbon dioxide, flowed through the upper 246 247 chamber while the carrier gas, nitrogen, flowed through the lower chamber at the 248 required relative humidity and drove the permeated molecules to the detector system. 249 To humidify the gases, a stream of gas was bubbled through a gas washing bottle filled 250 with water and then mixed with a second stream of dry gas. Flowmeters (Dakota 251 Instruments, Orangeburg, USA), needle valves (Swagelok, Solon OH, USA), and digital 252 hygrometers were used to adjust and control the gas streams. At the exit from the lower 253 chamber, the flowrate of carrier gas was measured by a mass flowmeter (Dakota 254 Instruments, Orangeburg, USA). The concentration of CO<sub>2</sub> in this stream was analyzed 255 by gas chromatography. A HP5890 gas chromatograph (Agilent Technologies, 256 Barcelona, SPAIN) equipped with a manual injection valve, a Chromosorb 102, 80/100 257 mesh, 12'x 1/8' column (Teknokroma, Barcelona, Spain), and a thermal conductivity 258 detector was used. The GC was calibrated by injecting known amounts of carbon 259 dioxide. Once the cell had been assembled, the carrier gas was passed through both 260 chambers for at least 6 hours to remove all gases present in the cell during handling and 261 equilibrate the film to the humidity of the test. At time zero, the permeant gas started to 262 flow into the upper chamber. The concentration of carbon dioxide in the lower chamber 263 was monitored until constant, that is to say, until the stationary state was established. 264 The gas permeability (P) was calculated as follows:

$$265 \qquad P = \frac{c_{CO2} \cdot f \cdot \ell}{A \cdot \Delta P}$$

Where  $c_{CO2}$  is the volume concentration of  $CO_2$  in the stationary state, f is the carrier gas flow in m<sup>3</sup>/s,  $\ell$  is the film thickness in m, A is the film area in m<sup>2</sup>, and  $\Delta P$  is the difference in the partial pressure of  $CO_2$  in the stationary state between the two chambers, measured in Pa.

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271 Organic compounds

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The organic compound retention capacity of the films and the effect of the addition of  $\beta$ CD were also studied. A hydroalcoholic solution (5% ethanol) of several organic compounds commonly found in food aromas was prepared at an initial concentration of 200 ppm (mg/L). The organic compounds selected were  $\alpha$ -pinene, d-limonene, linalool, citral, ethyl caproate, 2-nonanone, octanal, methyl-isobuthyl ketone, n-hexanal and nhexanol. The solution was then further diluted (to 5 ppm) with distilled water. The  $\beta$ CD and the EVOH-based film materials were exposed to this solution as follows:

a) To determine the preferential sorption of the  $\beta$ CD, 1 g of cyclodextrin was added to 30 mL of the same solution. The vial was closed with a PTFE/rubber septum and stored at room temperature for 15 days with constant stirring. The concentration of  $\beta$ CD exceeded the molar concentration of the different compounds by a factor of 500.

284 b) To determine the sorption capacity of the films, 10 pieces measuring 2x2 cm, 285 separated by glass rings, were threaded onto a stainless steel wire, immersed in 30 mL 286 of distilled water and stored for 1 day at 40°C to remove all releasable BCD molecules 287 from the samples. Then, the threaded samples were removed from the vial, thoroughly 288 rinsed with water, dried for 48 hours under vacuum and immersed in 30 mL of a 5ppm 289 solution of hexanal, d-limonene and  $\alpha$ -pinene, and stored for 15 days at room 290 temperature. Parallel samples were prepared by dispersing 0.02 g of BCD in 30 mL of 291 the solution, which corresponds to the molar content of organic compounds in the 292 sample and is similar to the  $\beta$ CD content in the EVOH-10 $\beta$ CD sample. All the samples 293 were prepared in triplicate.

294 The concentration of organic compounds present in the organic solution after the 295 storage period was evaluated by gas chromatography. Three 5 mL fractions of the 296 hydroalcoholic solution from each sample were placed in glass vials closed with 297 PTFE/rubber septa. A Supelco 65-µm DVB/PDMS solid phase microextraction (SPME) 298 fiber (Teknokroma, Barcelona, Spain) was exposed to the liquid solution for 10 min and 299 immediately desorbed for 5 min in the injector of a HP5890 gas chromatograph (Agilent 300 Technologies, Barcelona, Spain) equipped with a 30 m, 0.32 mm, 0.25 µm TRB-5 301 capillary column (Teknokroma, Barcelona, Spain). The chromatographic conditions 302 were as follows: He as carrier gas, 1/20 split injection, 210 and 300 °C injector and 303 detector temperatures, 5 min at 40°C, first heating ramp to 60°C at 3°C/min, second 304 heating ramp to 200°C at 10°C/min, and 5 min at 200°C. The gas chromatograph was

- 305 calibrated by measuring hydroalcoholic solutions with known concentrations of the
- 306 organic compounds.
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310 311 **RESULTS AND DISCUSSION** 312 313 The objective of this work was to immobilize  $\beta$ CD molecules in the polymer matrix and 314 produce films with functional characteristics suitable for the production of active 315 packages for foods. 316 317 In a first attempt, EVOH powder was mixed with  $\beta$ CD and films were obtained by 318 compression molding at 190°C and 20 bar for four minutes. The resulting films were 319 translucent, brittle and heterogeneous, and the cyclodextrins were visible and 320 concentrated in some areas due to an insufficient mixture of polymer chains and 321 oligosaccharide molecules. Besides, the high migration results ruled out these materials 322 for food packaging applications. Therefore, no further tests were done on the materials 323 obtained by compression. 324 325 In the second procedure, the EVOH films were obtained by extrusion. To improve the 326 CD addition results, the CDs were first mixed with glycerol, then the resulting paste 327 was manually mixed with the polymer pellets before being sent to the extruder hopper. 328 The films obtained by this method were transparent and flexible, although some white 329 spots could occasionally be observed due to the presence of  $\beta$ CD aggregates. The final 330 thickness was in the  $50\pm10 \ \mu m$  range. This technique was used to obtain materials with 331 10, 20 and 30% BCD and 20% of glycerol, designated as EVOH-10BCD, EVOH-20BCD 332 and EVOH-30BCD, respectively. Blank samples of pure EVOH (EVOH) and EVOH 333 with 20% of glycerol (EVOH-20G) were also extruded for comparison and submitted to 334 the characterization and migration studies. 335 336 337 **Morphological analysis** 338 339 The phase morphology of the prepared materials was studied through scanning electron

339 The phase morphology of the prepared materials was studied through scanning electron 340 microscopy. The cryo-fracture surface was examined after drying the samples; Figure 1 341 shows an example of the SEM images obtained. Figure 1A presents the morphology of 342 the EVOH-20G sample used as control. As can be seen, the figure shows a continuous 343 homogeneous matrix without phasing. Figure 1B is the SEM image of an extruded 344 sample of EVOH with 30% of BCD (EVOH-30BCD). As can be seen, BCD particles of 345 different sizes (0.1-1.5  $\mu$ m) are dispersed within the polymer matrix, showing signs of 346 low compatibility at the interface. Also, the image shows the presence of particle 347 aggregates, which would explain the white spots observed in the films with the naked eye. Figure 1C is the image of a similar sample after immersion in water for 10 days. 348 349 Small holes in the fracture surface and some small particles can be seen in this picture, 350 as in Figure 1B. Nevertheless, in these samples there is no evidence of large particles or 351 particle aggregates, which suggests that they may have been released into the liquid 352 medium before the SEM analysis.

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## 354 Migration

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356 Since cyclodextrins are partially water soluble and the first objective is to use them in 357 an active food packaging material, a preliminary study of their release from the films 358 was carried out by determining the global migration from the polymer into water, as an aqueous food simulant, in accordance with EU regulations.<sup>14-16</sup> Film samples were 359 360 immersed in distilled water and the global migration values were measured on days 1 361 and 10. Figure 2 presents the results of the migration tests. As can be seen, all the CD 362 samples showed high global migration values when exposed to distilled water, the food 363 simulant indicated by EU regulations for non-acid aqueous food products due to the 364 slight water solubility of  $\beta$ CD.

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366 The samples with glycerol presented global migration values of about 2%. Since pure 367 EVOH samples presented negligible migration (not included in the figure), this 368 percentage can be assigned to the loss of plasticizer. However, it is much lower than had 369 been expected from the results reported for hydrophilic biopolymers such as proteins or polysaccharides,<sup>19,20</sup> where the glycerol used as the plasticizer was fully extracted from 370 371 the developed films. The low values observed in the present work can be interpreted as 372 indicating a high chemical affinity between this polyol and the EVOH copolymer, 373 resulting in a partition equilibrium which favors the polymer over the food simulant. 374 Also, the results show that the migration increases with exposure time, indicating a 375 release process controlled by diffusion.

377 The EVOH samples with BCD and glycerol presented higher migration values than 378 those containing only glycerol. The amount of substances released by the different films 379 increased with the initial BCD content. The method used in this assay was gravimetric 380 and therefore does not distinguish between glycerol, BCD or other residues and 381 additives. Nevertheless, considering that the release of glycerol should be similar in all 382 the samples, the amount of BCD released from the films was below 50% of the initial 383 content. Also, it was noticeable that the migration values for the samples containing 384 BCD were similar on days 1 and 10. This kind of effect matches up with the case of 385 migration processes limited to the more external zones of the polymeric sample. However, EVOH copolymers are high-barrier materials and although they become 386 plasticized by water, the diffusivity of organic molecules is very slow.<sup>21</sup> Bearing in 387 388 mind that BCD molecules are very large, cyclic and rigid, their diffusivity in this 389 material should be practically negligible. Considering the SEM images of the samples 390 before and after exposure to the food simulant (Figure 1), the larger particles and the 391 aggregated particles might be those most exposed to dissolution in the aqueous medium.

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#### 393 Thermal Characterization

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Thermal properties are among the most important attributes of the material to be characterized for any polymer application, but are especially relevant in food packaging design since the materials can be exposed to various thermal processes, either alone or with the food product. DSC thermogram values for EVOH samples are shown in Figure 3 and the more relevant thermal properties are given in table 1.

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401 As Figure 3 shows, the thermograms of the samples containing BCD present several 402 differences with respect to the blank samples. The glass-transition temperature obtained 403 for pure EVOH was 46°C, in agreement with the Tg values reported in the literature on this material.<sup>22,23</sup> The addition of 20% glycerol brought a reduction in the Tg value of 404 405 ca. 3 °C. This effect was expected, although the plasticization caused by the addition of this agent was lower than that observed in other hydrophilic biopolymers.<sup>24,25</sup> The 406 407 addition of cyclodextrins to this 'plasticized' copolymer caused an increase in rigidity, 408 with 10-15 °C increments in Tg value The values were calculated by the onset of the 409 transition, since the end was hidden by the endothermic feature ascribed to enthalpy 410 relaxation. Figure 3 also shows that the crystallinity of EVOH was not affected by the

411 addition of glycerol. The melting temperature value and range and the melting enthalpy 412 were nearly identical. However, the incorporation of the cyclodextrins did influence the 413 melting behavior of the composite materials and, therefore, the copolymer morphology. 414 The presence of cyclodextrins in the polymer matrix reduced the melting temperature 415 and process enthalpy values. The endothermic minimum fell by 10-15 °C and the shape 416 of the endothermic depression differed, being wider with the addition of the 417 oligosaccharides. These changes can be interpreted as due to the cyclodextrins having a 418 nucleating effect, leading to a reduction in crystal size and a more imperfect crystalline 419 structure. The same effects of a lower melting temperature and a wider transition 420 temperature range were observable during the second heating. However, the Tg 421 transitions were not perceptible (no relaxation enthalpy), nor were they detected by the 422 equipment software.

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## 424 Barrier Properties

- 425
- 426 <u>Water vapor transport</u>
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# The transport of water vapor through the prepared materials was characterized by sorption and permeation experiments. The film samples were exposed to different humidity conditions and the water gain was determined as described in the experimental section.

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433 Figure 4 shows the results obtained in the sorption experiments. As expected, the water 434 uptake increased with the relative humidity in all the samples. The profile was an S-435 shape, convex at low humidity values and concave at high RH values, in agreement with previously reported isotherms for pure EVOH copolymers.<sup>26</sup> The addition of 436 437 glycerol caused a slight rise in the water gain of EVOH samples under all the RH 438 conditions tested. Nevertheless, the differences were not statistically different (p < 0.05). 439 With respect to the incorporation of cyclodextrins, the amount of sorbed water increased 440 with the BCD content, rising by a factor of 2 for samples with 10% and by a factor of 3 441 for samples with 30% RH. Solubility values were obtained for all the samples and RH 442 conditions. As can be seen, the solubility of the pure EVOH and EVOH-20G samples 443 remained fairly constant at ca. 0.02 Kg/[m<sup>3</sup>.Pa]. These values are in agreement with 444 published values for EVOH44, although the weak effect of glycerol on water uptake

445 was noticeable, in disagreement with the strong effects observed in other hydrophilic 446 biopolymers. The samples containing BCD presented values of between 0.04 and 0.06 Kg/[m<sup>3</sup>.Pa], well above the control samples. This increment could be a consequence of 447 448 two effects: a) the presence in the matrix of empty spots, as shown in the SEM images, 449 which could be filled with water molecules, and b) inclusion of water molecules in the 450 cavity of the BCD molecules. According to the literature,<sup>1</sup> the water uptake due to molecule inclusion inside the BCD cavity could account for up to 4% (w/w) for the 451 EVOH-30BCD samples, close to the amount sorbed by the pure copolymer. 452

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454 The water permeability through the films was also measured under different relative 455 humidity conditions; the results are plotted in Figure 5. As can be seen, all the samples 456 presented the same profile, showing the plasticizing effect of water at high humidities. 457 This effect is in agreement with previous reports in which water permeability was rather constant at low and medium humidity and increased rapidly in very humid 458 459 environments.<sup>26</sup> The addition of glycerol to EVOH produced a small increase in 460 permeability in all the conditions tested, which can be related to the presence of glycerol 461 in the sample and a slight plasticization caused by this polyol as reflected by the 462 reduction in Tg. The addition of cyclodextrins increased the water permeability of all 463 the samples, especially those with 20% and 30% BCD. This effect could have two 464 causes: a) higher water-solubility in these matrices, as shown in Figure 4, and b) an 465 increase in water diffusion resulting from the presence of voids in the matrices and in 466 the polymer/BCD interface. Using the definition of permeability as the product of 467 solubility and the diffusion coefficient (D), the diffusion coefficient can be estimated. At 75% RH, the D values of the control samples were in the  $4 \cdot 10^{-14}$  m<sup>2</sup>/s range, while 468 the D values for the samples with  $\beta$ CD rose to 6-7.10<sup>-14</sup> m<sup>2</sup>/s. At 90% RH, the addition 469 of  $\beta$ CD raised the D values from 8 to  $15 \cdot 10^{-14}$  m<sup>2</sup>/s. 470

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#### 473 Gas transport

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Permeability to oxygen and carbon dioxide was also evaluated under two relative humidity conditions: 50% and 90%. Figure 6 shows the values for all the samples. As can be seen, the addition of glycerol significantly increased the permeability to oxygen of the EVOH films, especially at low humidity. This effect was greater than for water

479 permeation and is most probably due to the effect of the plasticizer on the diffusivity of 480 this gas. To check this hypothesis, the diffusion coefficient was calculated by applying 481 the analytical solution to Fick's laws for the boundary conditions of an isostatic permeation process.<sup>17</sup> The results collected in Figure 7 show that the addition of 482 483 glycerol increased the D value by a factor of 10 at 50% RH. This increment was similar 484 to that in the EVOH sample caused by the plasticization of water at 90% RH. The 485 incorporation of cyclodextrins also increased the permeability of the samples to oxygen 486 compared to the pure EVOH sample. However, this increment was not as high as that 487 caused by the plasticizer. The profile obtained at 90% RH was very similar to that 488 obtained at 50%. With respect to oxygen diffusivity, the addition of BCD increased the 489 diffusion coefficient value in proportion to the BCD content.

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The effect of relative humidity on the diffusion coefficient of the EVOH sample shows the plasticization caused by water sorption.<sup>27</sup> This effect was less pronounced in the sample containing glycerol, since the material was partially plasticized by this agent. The effect is even smaller in the presence of BCD. Discontinuities in the matrix and transport through BCD cavities may be responsible for the greater diffusivity of the BCD films, where water uptake is a less important factor than in the polymeric matrix.

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498 Finally, the permeability of these materials to carbon dioxide was also measured, due to 499 the growing importance of this property in current packaging technologies (MAP, high 500 barrier packaging, active packaging, etc.). The results shown in Figure 6 present the 501 same profile as the oxygen permeability values. However, the permselectivity of the 502 EVOH was altered by the presence of BCD: the carbon dioxide permeability was 3-4 503 times higher than the oxygen permeability in the EVOH control samples, but 5-6 times 504 higher in the samples containing BCD. This might be caused by an increase in the 505 solubility of carbon dioxide in the composite matrices. Unfortunately, the experimental 506 method did not allow evaluation of D, which would have helped to confirm this 507 hypothesis.

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509 Transport of organic compounds

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511 It is well known that polymer-based packages have interactions with organic 512 compounds present in food. This characteristic, known as aroma scalping, may affect the sensory characteristics of the packaged food product, causing a reduction in aroma intensity or an unbalanced aroma due to the preferential retention of certain compounds. Therefore, in order to optimize the packaging design, it is important to study the potential food aroma interaction that a new material may present.

517 In this work, a preliminary experiment was carried out to study the relationship between 518 the polarity of the organic compounds and the complexation capacity of  $\beta$ CD. For this 519 purpose, BCD was added to a hydroalcoholic solution of several organic compounds at a 520 concentration of 5 ppm (w/v). The amount of oligosaccharide added was calculated to 521 achieve a molar ratio of 500/1 BCD/organic compounds. After two days of contact, the 522 samples were filtered and the concentration of non-encapsulated organic compounds (A<sub>free</sub>) was calculated by gas chromatography. The results were expressed as the value 523 524 of the equilibrium constant:

525 
$$K = \frac{[A_{complexed}]}{[A_{free}]}$$

The concentrations of complexed organic compounds (Acomplexed) were estimated by 526 527 subtraction from the nominal concentrations. Figure 8 presents the complexation 528 constant value as a function of the Hildebrand coefficient ( $\delta$ ), which is related to the polarity of substances.<sup>28</sup> As can be seen, the highest complexation values were obtained 529 530 for the most apolar compounds, those with the lowest Hildebrand coefficient values. 531 Approximately 90% of the  $\alpha$ -pinene and limonene molecules were complexed by  $\beta$ CD. 532 At the other extreme, the most polar compound tested, hexanol, presented the lowest K 533 value. Only 20% of the hexanol molecules formed inclusion complexes with the 534 oligosacharides. These results are in agreement with previous published results in which 535 terpenes and sesquiterpenes from various plant extracts were highly encapsulated and protected by  $\beta$ CD.<sup>29,30</sup> 536

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538 Another set of experiments was prepared with the materials under development. Control 539 EVOH films and those containing βCD were immersed in water for 24 hours at 40°C 540 and then dried under vacuum for 48 hours to eliminate the cyclodextrine molecules 541 which are released from the films. In this way, the potential organic compound 542 complexation caused by released  $\beta$ CD can be considered negligible. Then, films were 543 immersed in hydroalcoholic solutions of pinene, limonene and n-hexanal. The two 544 terpenes were selected because of their great affinity for the  $\beta$ CD. The hexanal was 545 selected since it is an organic compound which is formed as a consequence of oxidative

546 degradation of fats, and scavenging it could be a potential application of the materials 547 for active food packaging. The amounts of film and of the hydroalcoholic solution were 548 selected to obtain a BCD/organic compounds molar ratio of 1:1, 2:1 and 3:1 for the 549 EVOH-10BCD, EVOH-20BCD and EVOH-30BCD respectively. For the control tests, a 550 similar sample was prepared with EVOH-20G as the control and another by adding 551  $\beta$ CD in a  $\beta$ CD/organic compounds molar ratio of 1:1. As Figure 9 shows, in all the 552 samples the highest retention was obtained with the most apolar compounds. It is 553 interesting to observe the sorption of components by the polymeric matrix. The quantity 554 retained by the polymer is similar or even higher in comparison to free cyclodextrins. 555 EVOH is known to be a high barrier material for organic compounds when dry, but it 556 has been reported that water plasticization severely damages the barrier properties of 557 this family of copolymers. Thus, EVOH with glycerol is highly plasticized when 558 immersed in the hydroalcoholic solution, and organic compounds can easily diffuse 559 though the matrix.

560 The materials developed in this study presented much higher retention values because 561 of complexation with immobilized cyclodextrins, mainly of terpenic compounds. This 562 high retention also provides confirmation of the availability of the BCD cavity for 563 sorption of compounds. Therefore, it may be concluded that EVOH materials containing 564 immobilized BCD, prepared by regular extrusion, can be used to design active food 565 packaging that uses the  $\beta$ CD cavity for the inclusion or retention of apolar organic 566 compounds. At present, these materials are being tested with real products to observe 567 their capacity to retain undesirable compounds such as hexanal or cholesterol.

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## 570 CONCLUSIONS

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 $\beta$ -Cyclodextrin was successfully immobilized in an ethylene-vinyl alcohol copolymer with a 44% molar percentage of ethylene by regular extrusion with the aid of glycerol to improve the dispersion of the oligosaccharide. Although the composite presented phase separation, the films were continuous and transparent and their thermal properties did not present great changes. The barrier properties to gases and water decreased slightly due to the increase of free volume in the matrix. Also, the CO<sub>2</sub>/O<sub>2</sub> permselectivity increased, attribute with interesting uses in MAP. It is noticeable that the presence of

- $\beta$ CD increased their apolar organic compound sorption capacity, a characteristic which
- 580 could be useful in active packaging design.

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666 667	LEGENDS TO FIGURES
668 669 670	Figure 1. Scanning electron micrographs of the materials: EVOH-20G (A), EVOH-30BCD before migration process (B) and EVOH-30BCD after migration (C).
671 672	Figure 2. Global migration from EVOH materials obtained by extrusion
673 674 675	Figure 3. DSC thermograms of the different EVOH-based materials during the first heating.
676 677 678	Figure 4. Water sorption rates (A) and solubility coefficients (B) of the different EVOH-based materials as a function of relative humidity.
679 680 681	Figure 5. Water vapor permeability of film samples at 23°C as a function of relative humidity
682 683 684	Figure 6. Oxygen and carbon dioxide permeability of film samples at 23°C, at 50% and 90% RH.
685 686 687	Figure 7. Oxygen diffusion coefficient values for the different film samples at 23°C, at 50% and 90% RH
688 689 690	Figure 8. Effect of the polarity of aroma compounds on the complexation capacity of $\beta$ CD.
691 692 693 694	Figure 9. Retention of volatile components by the different samples.

Table 1. Thermal properties of the materials developed: glass transition temperature (Tg in °C, \*: onset value), melting enthalpy ( $\Delta$ H in J/g), melting temperature (Tm in °C) and melting temperature range ( $\Delta$ Tm in °C).

	First heating				Second heating			
Material	Tg	$\Delta H$	Tm	$\Delta Tm$	Tg	$\Delta H$	Tm	$\Delta Tm$
EVOH	46.08	59.09	159.96	43.3	43.28	67.49	161.73	63.6
EVOH-20G	42.89	58.56	160.3	38.9	38.48	68.55	160.77	61.7
EVOH-10βCD	57.70*	55.42	141.53	64.7		49.25	147.76	64.4
EVOH-20βCD	56.94*	48.66	143.47	66.6		49.11	149.82	73.8
EVOH-30βCD	61.6*	47.7	149.15	89.7		45.85	151.87	81







Heat Flow >>Exo>>



Relative humidity (%)



**Relative humidity (%)** 







