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공학석사 학위 논문

RuO<sub>2</sub>-loaded TiO<sub>2</sub> nanotube array electrodes for  
efficient electrocatalytic gas evolution

이산화티타늄 나노튜브 어레이에 로딩된  
이산화루테늄 전극의 전기화학적 기체발생 촉매특성

2018 년 8 월

서울대학교 대학원

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RuO<sub>2</sub>-loaded TiO<sub>2</sub> nanotube array electrodes for  
efficient electrocatalytic gas evolution

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이 논문을 공학석사학위논문으로 제출함

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## **Abstract**

# **RuO<sub>2</sub>-loaded TiO<sub>2</sub> nanotube array electrodes for efficient electrocatalytic gas evolution**

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Ruthenium dioxide (RuO<sub>2</sub>) has an advantage of various chemical reactions like dehydrogenation, gas phase oxidation of HCl, and chloro-alkali process. In order to enhance stability of RuO<sub>2</sub>-based catalysts, the use of TiO<sub>2</sub> is successful in recent years. In general, nanostructured scaffolds with the large relative surface area are adopted in the catalytic reactions for maximizing the number of active sites. For the electrocatalytic reactions, however, the scaffold should be conducting enough so that the charges required for the redox reaction can be transported to the surface of the loaded RuO<sub>2</sub> catalysis. In the same context, TiO<sub>2</sub> nanotube arrays (NTAs) can be a promising scaffold for the CER

reaction, because it can transport charges (as evidenced in the solar cell or PEC applications) and it can be a good combination with RuO<sub>2</sub> (as evidenced by DSA<sup>®</sup>). In addition, the nanoscale morphologies (*e.g.* tube length, pore diameter, and wall thickness), crystalline structure (*e.g.* crystalline phase and preferred orientation), and the electrical properties (*e.g.* conductivity) can be precisely controlled by the processing parameters.

In this study, we firstly report the RuO<sub>2</sub>-loaded TiO<sub>2</sub> NTAs as an efficient nanostructure electrode for the electrocatalytic CER process. Nanostructuring is well-known for enhancing the catalysts activity, we design TiO<sub>2</sub> based nanostructure to investigate more active catalysts. The samples have been prepared electrochemically (*i.e.* electrochemical anodization for preparing TiO<sub>2</sub> NTAs and electrochemical deposition for loading RuO<sub>2</sub>) and the dependence of the CER performance on the materials properties of the composite electrodes such as the crystallinity and electrical conductivity have been investigated. It has been found that the conductivity of the electrode under the anodic polarization is essential for achieving good CER performance, and the black TiO<sub>2</sub> prepared by annealing as-anodized NTAs under an Ar atmosphere has been found to be the best scaffold for the RuO<sub>2</sub> catalysis.

**keywords: Chlorine Evolution Reaction(CER), TiO<sub>2</sub> nanotube arrays (TiO<sub>2</sub> NTAs), Ruthenium dioxide, Heterogeneous Catalysis, Electrochemical analysis.**

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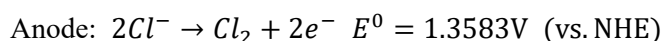
# Chapter 1. Introduction

## 1.1 Chlorine Evolution Reaction (CER)

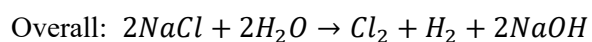
### 1.1.1 Chlor-alkali process

The chlor-alkali industry for producing chlorine itself as a chemical is obviously one of the largest industrial electrochemical processes featured by the annual production of more than 70 million tons.<sup>1-3</sup> Besides the chlorine production, the CER is becoming more and more important for emerging applications based on the electrochemical advanced oxidation process such as the water purification,<sup>4</sup> sterilization,<sup>5</sup> and the ballast water treatment.<sup>6</sup> Also, chlorine gas is a gas used for various chemical reactions. It uses for synthesizing polyvinyl chloride (PVC), various chlorinated polymers (eg, polyvinylidene chloride (PVDC), Polychloroprene) and the precursor for various organic synthesis and inorganic synthesis.<sup>4</sup>

The chlor-alkali process is a process of electrolyzing brine to obtain chlorine gas and sodium hydroxide (NaOH). The following reactions occur at the cathode and anode.



Cathode:  $2\text{H}_2\text{O} + 2e^- \rightarrow \text{H}_2 + 2\text{OH}^- \quad E^0 = 0.8277\text{V (vs NHE)}$  However, in the mercury cell, NaHg formation reaction ( $2\text{Na}^+ + 2\text{Hg} + 2e^- \rightarrow 2\text{NaHg}$ ) occurs.



Currently commercialized processes include mercury process, diaphragm process, and membrane process. The previous two processes are older than membrane processes and have been developed in Europe and the US, respectively. The membrane process is a process developed in Japan.<sup>4</sup> The schematic diagram for each process is as follows. **(Figure 1, 2, 3)**<sup>7</sup>

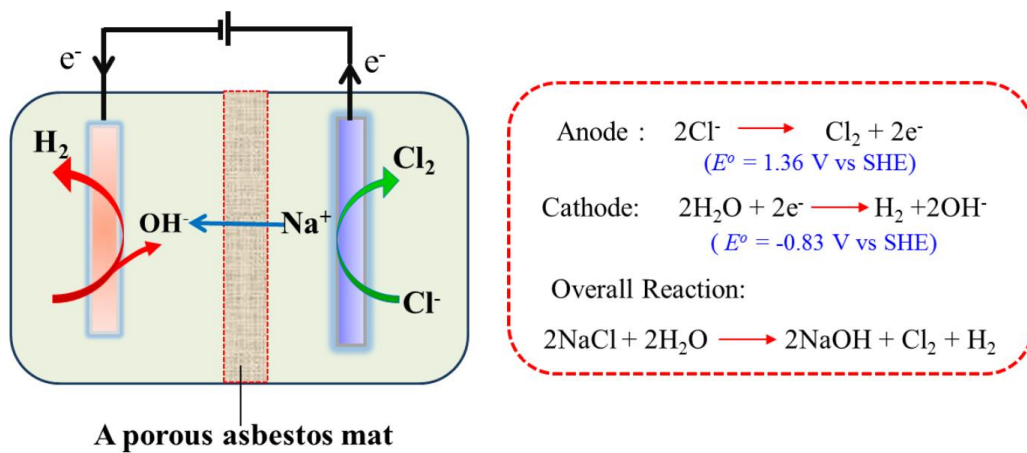
First, in the case of the diaphragm process,  $Na^+$  is permeable to the asbestos layer to form NaOH. However, asbestos acts as a physical barrier between the two electrodes, allowing the movement of water and ions. Therefore,  $Cl^-$  ions in brine can be passed over to make NaCl, and OH-ions formed in the anode can be passed to the cathode to increase the pH, causing selectivity problems with Oxygen Evolution.

Second, in the mercury process, NaHg amalgam is formed instead of the reduction reaction of water in the reduction electrode. Because it is a membrane-free process, it can be driven at a high current density even if the voltage is the same. However, the use of mercury is decreasing due to pollution problems.

Third, there is a membrane process. The diaphragm process uses a membrane instead of asbestos, and the cation exchange resin, nafion, solves the NaCl impurity problem.



Chlor-alkali process is mainly carried out under the following conditions which is summarized in **Table 1**.<sup>8</sup> As can be seen in the table, it is an electrochemical process and therefore takes place at much higher temperature and current density conditions. Ruthenium-based catalysts, which are particularly stable and therefore far superior to other catalysts with stability, have been used predominantly.



**Figure 1. A schematic of the operation mechanism of the diaphragm cell. In the conventional diaphragm cell, a porous asbestos mat is used to separate the anodic reaction of CER and the cathodic reaction of HER, where NaOH is simultaneously formed in the cathodic compartment. [7]**

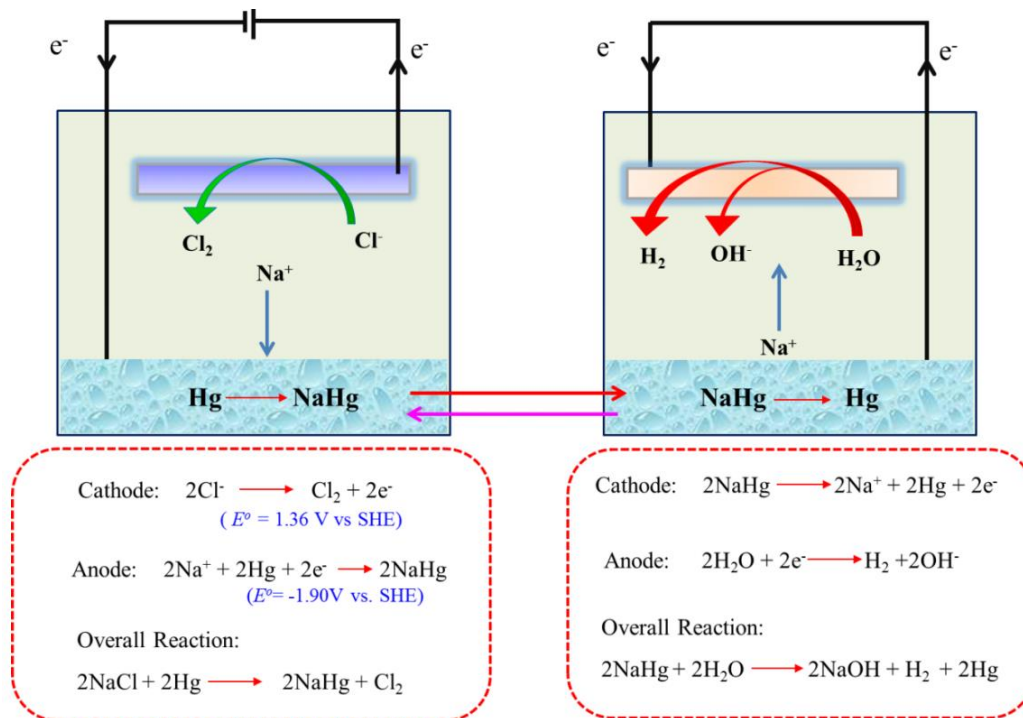


Figure 2. A schematic of the operation mechanism of the mercury cell. [7]

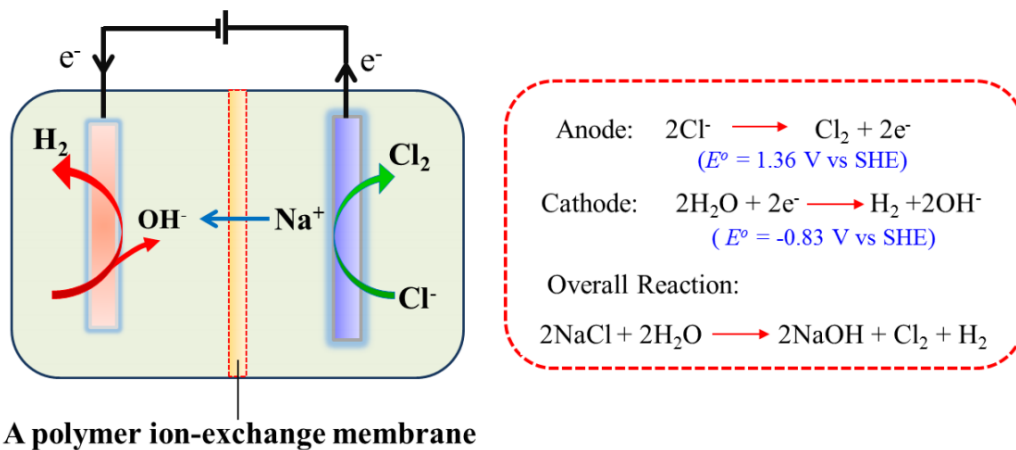


Figure 3. A schematic of the operation mechanism of the membrane cell. [7]

cell voltage (V)	2.4–2.7
current density ( $\text{kA m}^{-2}$ )	1.5–7
temperature ( $^{\circ}\text{C}$ )	90
NaCl concentration in the anolyte ( $\text{g dm}^{-3}$ )	200
anolyte pH	2–4
NaOH concentration in the catholyte (wt %)	32

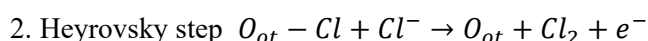
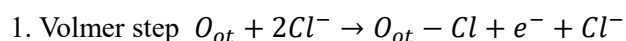
**Table 1. Typical chlorine evolution reaction reaction conditions. [8]**

### 1.1.2 Mechanism of chlorine evolution reaction

Chlorine evolution reaction can occur in various catalysts (RuO<sub>2</sub>, IrO<sub>2</sub>, PtO<sub>2</sub>, etc.), and the mechanism has been mainly explored in the most successful RuO<sub>2</sub> or RuO<sub>2</sub>-TiO<sub>2</sub> composite. So how does chlorine evolution occur on RuO<sub>2</sub> catalysts?

In recent years, Over group has explored what is happening on the single crystal RuO<sub>2</sub> (110) plane through various calculations and supported experimental evidence.<sup>9-10</sup> They argue that, as reported by other groups<sup>11-12</sup>, the Tafel slope at low overvoltages and at high overvoltages are different and can be explained by first-principles calculations.

The crystal structure of RuO<sub>2</sub> is as follows. (**Figure 4**)<sup>9</sup> Among them, there are three kinds of sites that are considered as active sites of catalysts. First is the unsaturated Ru site (Ru<sub>cus</sub>). As the oxidation progresses, Oxygen sticks to this, and the oxygen atoms protruding outward are called O<sub>ot</sub>. In the case of RuO<sub>2</sub>, O<sub>ot</sub> is the main active site and is a catalyst capable of generating chlorine through two steps. The two steps are as follows.



The Volmer step is the process of making a reaction intermediate called OCl with Cl<sup>-</sup> on the O<sub>ot</sub>, and the Heyrovsky step is the process of finally producing the Cl<sub>2</sub> gas with Cl<sup>-</sup> attached to the reaction intermediate. If the overvoltage is small, the second step (Heyrovsky step) is the step to determine the reaction rate (rate-determining step: RDS). However, if the overvoltage is large, the first step, the volmer step, determines the

reaction rate It is shown through thermodynamic calculation that it is a step. The change of the tafel slope according to the overvoltage is explained by various methods such as the amount of Cl on the surface. However, the calculation shows that the RDS changes depending on the overvoltage. (**Figure 5**)<sup>10</sup>

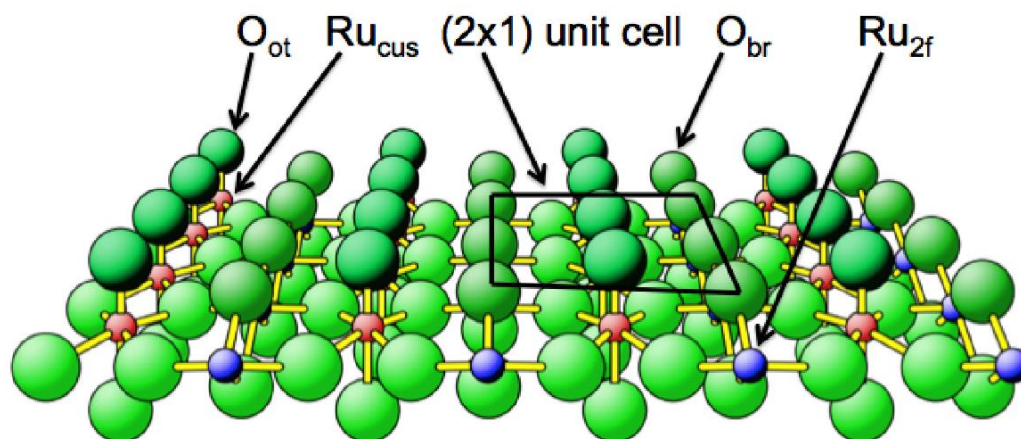


Figure 4. (2×1) surface unit cell of RuO<sub>2</sub>(110). Undercoordinated ruthenium atoms of the RuO<sub>2</sub>(110) surface are denoted by Ru<sub>cus</sub> and Ru<sub>2f</sub>. Adsorbates bridging two Ru<sub>2f</sub> atoms are indicated with the index “br” and adsorbates in terminal position on Ru<sub>cus</sub> atoms with the index “ot” (on-top). red spheres: ruthenium 1-fold cus atoms (Ru<sub>cus</sub>), blue spheres: ruthenium 2-fold cus atoms (Ru<sub>2f</sub>), green spheres: oxygen atoms. [9]



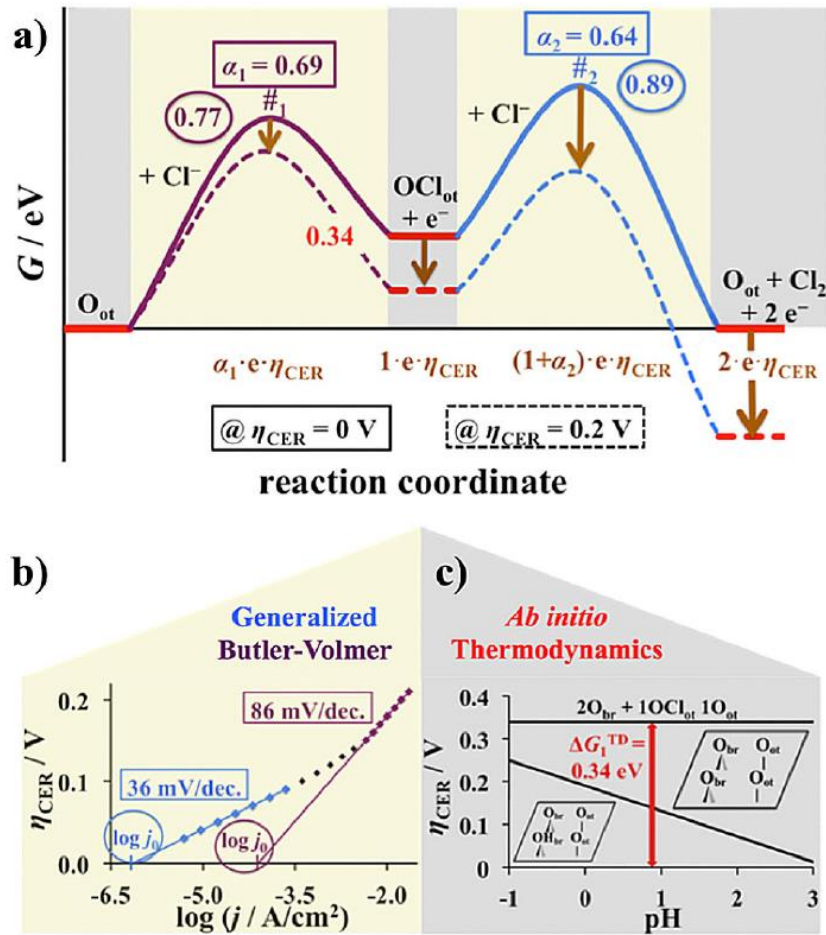


Figure 5. a) the free-energy profile along the reaction coordinate at different applied overpotentials. ( $\eta_{CER} = 0V, 0.2V$ , respectively) b) Experimental Tafel plot for a wide range of overpotentials, exhibiting two characteristic linear Tafel regions with Tafel slopes of 36 and 86 mV/dec. c) Ab initio thermodynamics provides the Pourbaix diagram that summarizes the stable surface configurations depending on the pH value and the applied overpotential. Under CER conditions, a fully-oxygen covered RuO<sub>2</sub>(110) surface is energetically preferred. [10]

### 1.1.3 Recent research trend and literature review

Ruthenium oxide ( $\text{RuO}_2$ ) has been known as one of the best heterogeneous catalysis for the anodic chlorine evolution reaction (CER). In spite of the excellent catalytic properties, however, the biggest issue of the  $\text{RuO}_2$ -based catalysis is the high materials cost. Therefore, the commercial CER catalysis widely used in the industry is the Dimensionally Stable Anodes (DSA<sup>®</sup>) consisting of 70-mole% rutile  $\text{TiO}_2$  and 30-mole%  $\text{RuO}_2$ , which exhibits minimal loss of performance with minimal use of  $\text{RuO}_2$ . In addition, the presence of  $\text{TiO}_2$  has been known to enhance the stability under the anodic polarization during the CER process.<sup>13-14</sup>

#### Research Trends

In the case of CER, much research has been done on mechanisms.<sup>15-16</sup> Various mechanisms have been proposed (**Table 2**)<sup>17</sup> and recent studies have shown that thermodynamic calculations and first principles can better explain experimental results. In addition, many studies on selectivity have been carried out since  $\text{Cl}_2$  chemistry can cause various chemical species to proceed in aqueous solution (**Figure 6**)<sup>8</sup>, and the problem of oxygen generation at the oxidation electrode always follows. Surprisingly, selectivity is also closely related to stability. As the selectivity to  $\text{Cl}_2$  increases, there is less current associated with OER, which leads to slower degradation of the oxide and improved stability. There are two major factors that affect selectivity.<sup>8</sup> First, it is a process condition (pH, temperature, the current density of the electrolyte, the  $\text{Cl}^-$  concentration

of the electrolyte, etc.). The second is the structure and composition of the anode. Various studies have confirmed that selectivity and efficiency are affected by what anode is, what doping is, what amount of Ru is, and so on. The results are summarized as follows.

1. The partial current of OER can be significantly lowered in the case of an electrolyte added with HCl.<sup>18-19</sup>
2. The lower the pH, the more kinetics of OER are inhibited. Therefore, it is preferable to measure in acidic conditions.<sup>20</sup>
3. The higher the  $Cl^-$  concentration, the better the current efficiency.<sup>21</sup> This can be explained by the increase of adsorption due to mass transfer enhancement.
4. The higher the current density, the lower the selectivity.<sup>20</sup>
5. When the pH is low in the  $Cl^-$ -rich electrolyte, the formation of soluble chloride is closely related to degradation.<sup>22</sup> However, if the pH is higher (base condition), there seems to be a different degradation mechanism.
6. The corrosion of DSA is minimum between  $pH = 2$  and  $3$ .<sup>19</sup> This can be explained by the pourbaix diagram (**Figure 7**).<sup>23</sup> Because conversion from  $RuO_2$  to  $RuO_4$  is important to explain degradation mechanism.
7. The factor related to the stability of DSA is the OER partial current. The higher the partial current of OER, the more Ru oxidation and corrosion increases.<sup>8</sup> The degradation mechanism of  $RuO_2$  associated with OER is shown in the figure below. (**Figure 8**)<sup>24</sup> As

the anodic polarization is overprotected,  $\text{RuO}(\text{OH})_2$  formed on the surface is converted into  $\text{RuO}_4^{2-}$ , and the amount of Ru is gradually decreased. However, the current density of CER and stability of electrode were not related to each other.<sup>8</sup> It is not a problem that the current density of the CER increases, but the occurrence of other side reactions such as OER is a key factor in deterioration.

8. It has been reported that as the active surface increases, local current density decreases and selectivity increases.<sup>21</sup> The surface area was mainly controlled by the size control of  $\text{RuO}_2$  particles. In this study, the  $\text{TiO}_2$  nanotube array was used to increase the active surface.

9. It can be seen that the selectivity of OER increases as the loading amount of the catalyst increases.<sup>21</sup>

10. Other materials besides  $\text{RuO}_2$  have also been reported for CER activity.  $\text{IrO}_2$ <sup>25</sup>,  $\text{PdO}$ <sup>26</sup>, and  $\text{CoOx}$ <sup>27</sup> is mainly investigated. In addition,  $\text{RuO}_2$  composite materials containing  $\text{SnO}_2$ <sup>28</sup>,  $\text{Sb}_2\text{O}_5$ <sup>29-30</sup>, and  $\text{TiO}_2$ <sup>31</sup> have been reported. In the case of  $\text{RuO}_2$ ,  $\text{TiO}_2$  was found to be advantageous in terms of cost and stability, but the pure phase was more advantageous in the case of  $\text{IrO}_2$ .  $\text{PdO}$  has not been explored much, but it has proved to be more advantageous than RTO ( $\text{RuO}_2$ - $\text{TiO}_2$  mixed oxide) in terms of stability and efficiency. As  $\text{CoOx}$  has been reported as a good catalyst for OER, it has poor selectivity compared to other materials, and there is even corrosion due to decomposition of  $\text{HClO}$  (hypochlorite decomposition). Due to the high price of Ru-based materials, substitution with non-noble

metals such as Co has been studied extensively, but there has not yet been a successful case of Ru over Ti-mixed RTO.

11. In addition to changing materials, many attempts have been made to change the electronic structure through doping. In particular, there have been many attempts to improve selectivity by doping various elements such as Zn<sup>32-33</sup>, Ni<sup>34</sup>, Mg<sup>35</sup>, Fe<sup>36</sup>, Co<sup>27</sup> and Sn<sup>36</sup> into RuO<sub>2</sub>.

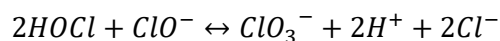
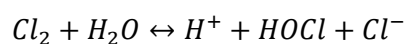
12. As a result, the RTO composition of RuO<sub>2</sub> mixed with TiO<sub>2</sub> has more advantages in terms of activity, selectivity, stability, and cost than other catalysts.

13. In recent years, processes using catalysts using Mn-based cheap materials have been introduced in academia, eliminating membranes.<sup>7</sup> **(Figure 9)**

No.	Mechanism	Author	Year
(1)	$2\text{Cl}^- \rightleftharpoons \text{Cl}_2(\text{surf}) + 2\text{e}^-$ $\text{Cl}_2(\text{surf}) \rightarrow \text{Cl}_2(\text{bulk})$	R. G. Erenburg, L. I. Krishtalik et al.	1972 [27]
(2)	$\text{Cl}^- \rightleftharpoons \text{Cl}_{ad} + \text{e}^-$ $2\text{Cl}_{ad} \rightarrow \text{Cl}_2$	G. Faita and G. Fiori	1972 [38]
(3)	$\text{Cl}^- \rightleftharpoons \text{Cl}_{ad} + \text{e}^-$ $2\text{Cl}_{ad} \rightarrow \text{Cl}_2$ and $\text{Cl}_{ad} + \text{Cl}^- \rightarrow \text{Cl}_2 + \text{e}^-$	R. G. Erenburg, L. I. Krishtalik et al.	1972 [50]
(4)	$\text{Cl}^- \rightleftharpoons \text{Cl}_{ad} + \text{e}^-$ $\text{Cl}_{ad} \rightarrow (\text{Cl}_{ad})^+ + \text{e}^-$ $(\text{Cl}_{ad})^+ + \text{Cl}^- \rightleftharpoons \text{Cl}_2$	R. G. Erenburg, L. I. Krishtalik et al.	1975 [36]
(5)	$\text{Cl}^- \rightleftharpoons \text{Cl}_{ad} + \text{e}^-$ $\text{Cl}_{ad} + \text{Cl}^- \rightarrow \text{Cl}_2 + \text{e}^-$	L. J. J. Janssen et al.	1977 [51]
(6)	$\text{RuO}_2 + \text{H}_2\text{O} \rightarrow \text{RuO}_3 + 2\text{H}^+ + 2\text{e}^-$ $\text{RuO}_3 + \text{Cl}^- \rightarrow \text{RuO}_2(\text{ClO}_{ad})^+$ $(\text{ClO}_{ad})^+ + \text{Cl}^- \text{ (or Cl}^-) + 2\text{H}^+ \rightarrow \text{Cl}_2 + \text{H}_2\text{O}$	J. Augustynski et al.	1978 [40]
(7)	$\text{Cl}^- \rightleftharpoons \text{Cl}_{ad} + \text{e}^-$ $\text{H}_2\text{O} \rightarrow \text{OH} + \text{e}^-$	D. A. Denton, J. A. Harrison et al.	1979 [52]
(8)	$\text{O}_{ad} + \text{Cl}^- \rightarrow \text{OCl}_{ad} + \text{e}^-$ $\text{OCl}_{ad} + \text{Cl}^- \rightarrow \text{O}_{ad} + \text{Cl}_2 + \text{e}^-$	L. K. Burke and J. F. O'Neill	1979 [45]
(9)	$(\text{M}^n) \rightleftharpoons (\text{M}^{n+1}) + \text{e}^-$ $(\text{M}^{n+1}) + \text{Cl}^- \rightarrow (\text{M}^{n+1})\text{Cl}_{ad} + \text{e}^-$ $(\text{M}^{n+1})\text{Cl}_{ad} + \text{Cl}^- \rightleftharpoons (\text{M}^n) + \text{Cl}_2$	L. I. Krishtalik	1981 [46]
(10)	$\text{H}_2\text{O} \rightleftharpoons \text{OH}_{ad} + \text{H}^+ + \text{e}^-$ $\text{M-OH}_{ad} + \text{Cl}^- \rightarrow \text{M(OH)Cl} + \text{e}^-$ $\text{HOCl} + \text{HCl} \rightleftharpoons \text{Cl}_2 + \text{H}_2\text{O}$	L. I. Krishtalik and R. G. Erenburg	1981 [41]
(11)	$\text{M-OH}_{ad} \rightleftharpoons \text{M-OH} + \text{H}^+$ $\text{M-OH} \rightleftharpoons \text{M-O} + \text{H}^+ + \text{e}^-$ $\text{M-OCl} + \text{Cl}^- + \text{H}^+ \rightleftharpoons \text{M-OH} + \text{Cl}_2$ or $\text{M-OCl} + \text{Cl}^- \rightleftharpoons \text{M-O} + \text{Cl}_2 + \text{e}^-$	R. G. Erenburg	1984 [53]
(12)	$\text{O}_{ad} + \text{Cl}^- \rightarrow \text{O}_{ad}\text{-Cl}^- + 2\text{e}^-$ or $\text{O}_{br} + \text{Cl}^- \rightarrow \text{O}_{br}\text{-Cl}^- + 2\text{e}^-$	T. Hepel et al.	1986 [44]
(13)	$\text{Cl}_2$ diffusion limitation	V. V. Losev et al.	1989 [35]
(14)	$\text{M}^Z + \text{H}^+ \rightleftharpoons \text{MH}^{Z+1}$ $\text{M}^Z \rightleftharpoons \text{M}^{Z+1} + \text{e}^-$ $\text{M}^{Z+1} + \text{Cl}^- \rightleftharpoons \text{MCl}^{Z+1} + \text{e}^-$ $\text{MCl}^{Z+1} + \text{Cl}^- \rightleftharpoons \text{M}^Z + \text{Cl}_2$ $2\text{MCl}^{Z+1} \rightleftharpoons 2\text{M}^{Z+1} + \text{Cl}_2$	J. L. Fernandez et al.	2002 [47, 54, 55]
(15)	Radical spillover mechanism	S. Ferro et al.	2002 [17]
(16)	$\text{RuO}_2$ nanocrystals	J. Jirkovsky et al.	2006 [16]
(17)	$\text{M}^Z\text{-OH}_2^+ \rightleftharpoons \text{M}^{Z+1}\text{-OH} + \text{H}^+ + \text{e}^-$ $\text{M}^{Z+1}\text{-OH} + \text{Cl}^- \rightleftharpoons \text{M}^{Z+1}\text{-OHCl} + \text{e}^-$ $\text{M}^{Z+1}\text{-OHCl} + \text{Cl}^- + \text{H}^+ \rightleftharpoons \text{M}^Z\text{-OH}_2^+ + \text{Cl}_2$ $\text{M}^{Z+1}\text{-OHCl} + \text{Cl}^- \rightleftharpoons \text{M}^{Z+1}\text{-OH} + \text{Cl}_2 + \text{e}^-$	M. Thomassen et al.	2006 [48]
(18)	pH dependence in different surface orientation	E. Guerrini, S. Trasatti	2006 [42]
(19)	$\text{O}_{ad}\text{-O}_{ad} + 2\text{Cl}^- \rightarrow (\text{O}_2)_{ad}\text{-Cl} + \text{Cl}^- \rightarrow \text{O}_{ad}\text{-O}_{ad} + \text{Cl}_2(\text{g}) + 2\text{e}^-$	H. A. Hansen et al.	2010 [29]

**Table 2. Various mechanisms proposed for chlorine evolution reaction. [17]**

species	name	Cl oxidation state
$\text{Cl}^-$ (aq)	chloride (ion)	-1
$\text{Cl}_3^-$ (aq)	trichloride ion	-1, 0
$\text{HCl}$ (g) or (aq)	hydrochloric acid	-1
$\text{Cl}_2$ (g) or (aq)	chlorine gas	0
$\text{HOCl}$ (aq)	hypochlorous acid [or chloric (I) acid]	+1
$\text{ClO}^-$ (aq)	hypochlorite (ion) [or chloric (I) ion]	+1
$\text{Cl}_2\text{O}$ (g)	chlorine monoxide	+1
$\text{HClO}_2$ (aq)	chlorous acid	+3
$\text{ClO}_2^-$ (aq)	chlorite (ion)	+3
$\text{ClO}_2$ (g)	chlorine dioxide	+4
$\text{ClO}_3^-$ (aq)	chlorate (ion)	+5
$\text{ClO}_4^-$ (aq)	perchlorate (ion)	+7



**Figure 6. Various chlorine species during chlorine evolution and three main reactions in chlorine chemistry. [8]**

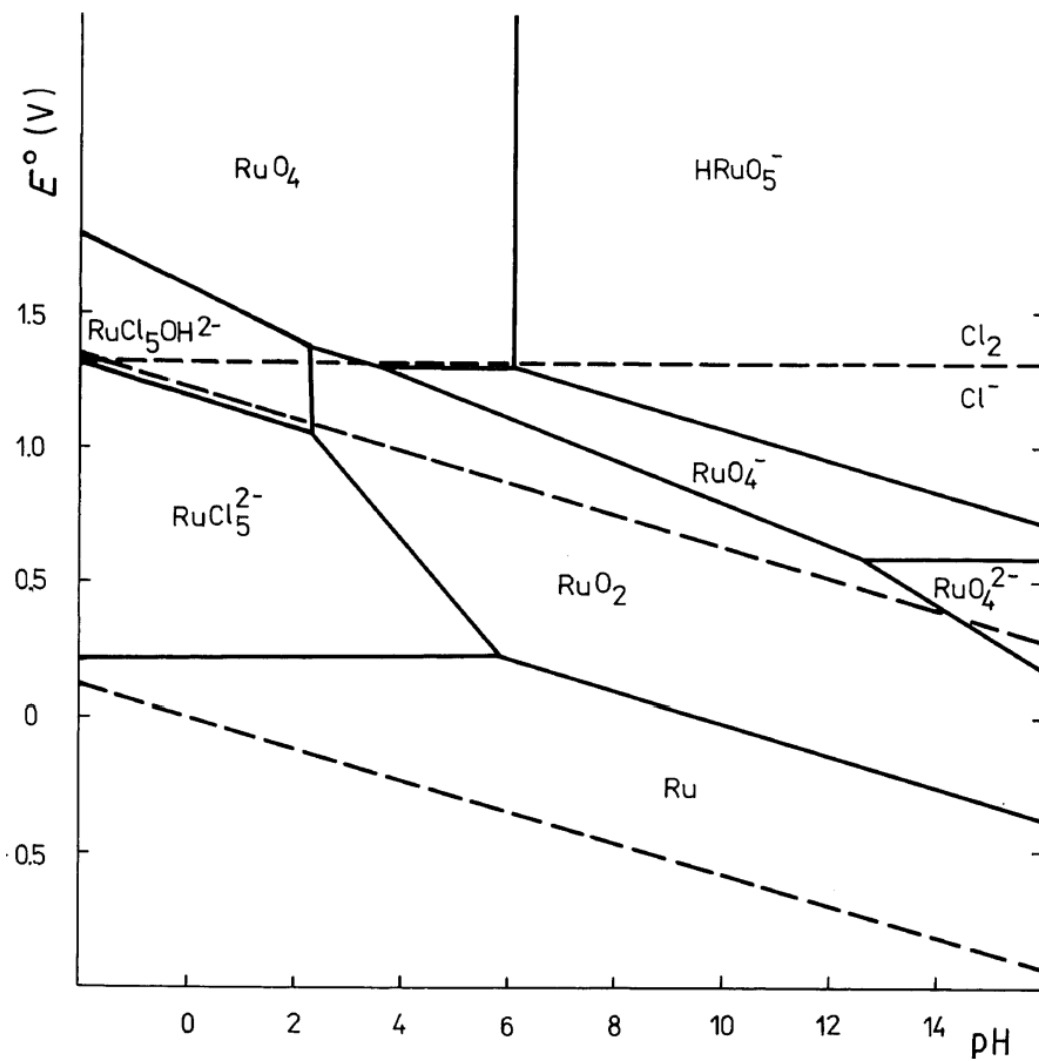


Figure 7. Pourbaix diagram for ruthenium in concentrated NaCl solution (25°C, 265g/dm<sup>3</sup> NaCl). [23]



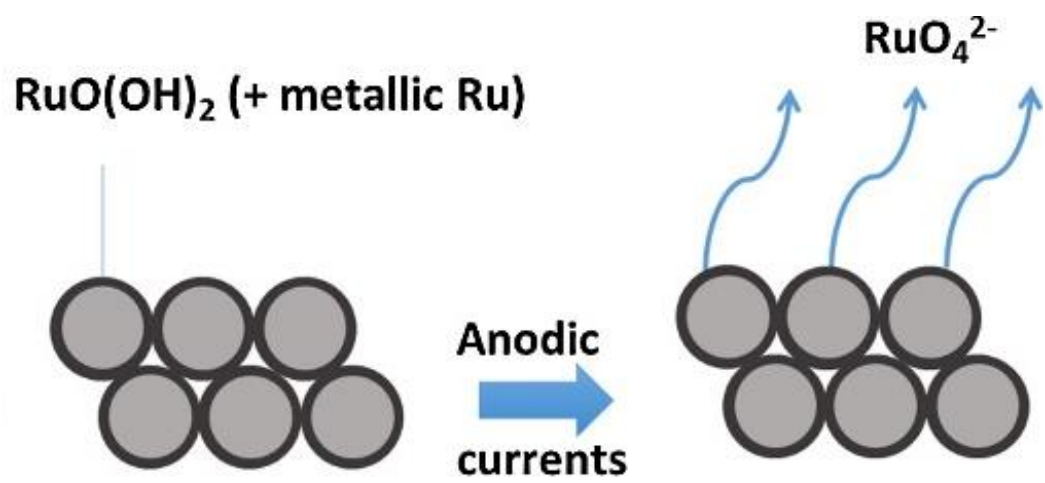


Figure 8. Corrosion of  $\text{RuO}_2$ -based materials under anodic current. [24]

factor	selectivity for oxygen evolution	refs	comment
modified composition	decrease	36, 158, 162, 167, 169, and 173	several modified coatings exist
increased surface area	increase	69	related to decrease in $j_{loc}$ ?
larger coating crystallite particle size	decrease	78	related to increase in $j_{loc}$ ?
higher oxide loading	increase	75	
less Ru in RTO coating	decrease	67, 68, 75, 139, 154, 161, and 171	same effect as decreased $j_0$ for reaction 11? Connected to increased chlorate formation <sup>36,143,150,154</sup>
decreased $j_0$ for reaction 11	decrease	69, 150, 159, and 167	but reaction 11 not only source
IrO <sub>2</sub> substitution	decrease?	74	doped into RTO; dorrosion products might increase selectivity in practice
Co substitution	decrease?	78	doped into RuO <sub>2</sub> ; <sup>82,83,189</sup> saw increase
SnO <sub>2</sub> substitution	decrease	69, 71, 147, and 172	doped into RuO <sub>2</sub> <sup>69,172</sup> or together with Pd <sup>71</sup>
HfO <sub>2</sub> substitution	increase	69	doped into RuO <sub>2</sub>
Zn substitution	increases	181, 182, and 189	doped into RuO <sub>2</sub>
Ni substitution	decrease	77	doped into RuO <sub>2</sub>
Mg substitution	decrease	193	doped into RuO <sub>2</sub>
Fe substitution	decrease?	180	doped into RuO <sub>2</sub> , high Cl <sub>2</sub> selectivity in Ar-saturated solutions
overlayer material	decrease	60	overlayer of Pt mixed with IrO <sub>2</sub>
support material	possible effect	8 and 179	

**Table 3. Summary of RuO<sub>2</sub>-based composite materials activity and selectivity. [8]**

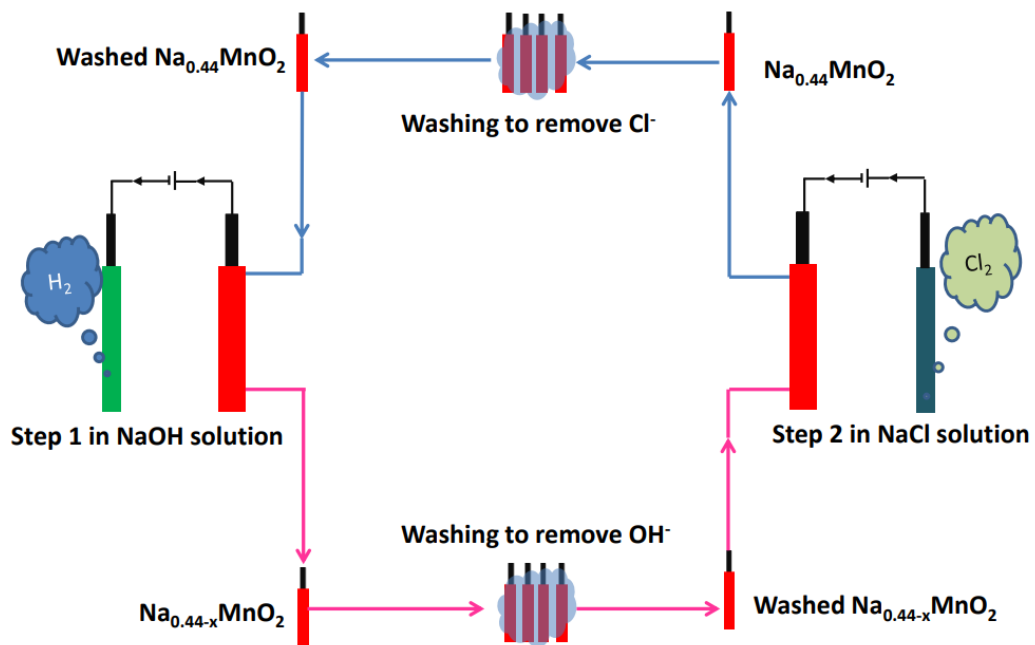


Figure 9. conceptual process scheme of the novel two step chlor-alkali process. [7]

## 1.2 TiO<sub>2</sub> nanotube arrays (TiO<sub>2</sub> NTAs)

### 1.2.1 Brief outline of TiO<sub>2</sub>

Titanium dioxide (TiO<sub>2</sub>) is widely investigated due to its good stability (including corrosion resistance) and physical properties and biocompatibility. Especially, it is widely used in pigment<sup>37</sup>, sunscreens<sup>38-39</sup>, paints<sup>40</sup>, ointments, and toothpaste<sup>41</sup>. In energy-related application, Fujishima and Honda first reported as the photocatalytic splitting of water under UV light.<sup>42</sup> In chlorine evolution reaction, the presence of TiO<sub>2</sub> has been known to enhance the stability under the anodic polarization during the CER process.<sup>13-14</sup> In addition, TiO<sub>2</sub> is often used as an additive in conjunction with SnO<sub>2</sub> to enhance the selectivity of CER with respect to oxygen evolution reaction (OER).<sup>20</sup> In fact, it has been reported that up to about 70% TiO<sub>2</sub> increases selectivity rather than impairing the catalytic properties of RuO<sub>2</sub>. This is because TiO<sub>2</sub> lowers the partial current due to OER which may prevent dissolution.<sup>13-14</sup>

TiO<sub>2</sub> often has four polymorphs. tetragonal rutile, tetragonal anatase, orthorhombic brookite, and monoclinic TiO<sub>2</sub>.<sup>43</sup> (**Figure 10**) In addition, polymorphs at high pressure, or less common structure have been reported as well.<sup>44</sup> Of these, rutile is the most thermodynamically stable phase formed at high temperatures<sup>45</sup>, while the remainder is formed at a slightly lower temperature. TiO<sub>2</sub> nanotube arrays are amorphous in the as-dep condition<sup>46</sup> and can be transformed to anatase or rutile when annealed.<sup>47</sup> But for rutile, it needs to be heat treated at very high temperatures (> 800°C).<sup>47</sup> Although it has

been reported that when the heat treatment is performed at a temperature of 900°C or higher, the TiO<sub>2</sub> nanotube array is completely changed to rutile, but the shape of the TiO<sub>2</sub> nanotube array is not maintained.<sup>47</sup> Not only TiO<sub>2</sub> nanotube arrays, Mo oxide nanotube arrays have also been observed to break the shape of nanotubes during high-temperature heat treatment.<sup>48</sup> This is because the crystal structure is changed and lattice strain is generated and thus strain is generated. In addition, rutile is the most thermodynamically stable phase in the bulk system<sup>45</sup>, but at the nanoscale, many experimental and theoretical studies support that the most stable phase is anatase.<sup>49</sup> Therefore, in the case of TiO<sub>2</sub> nanotube arrays, many studies related to anatase have been conducted.

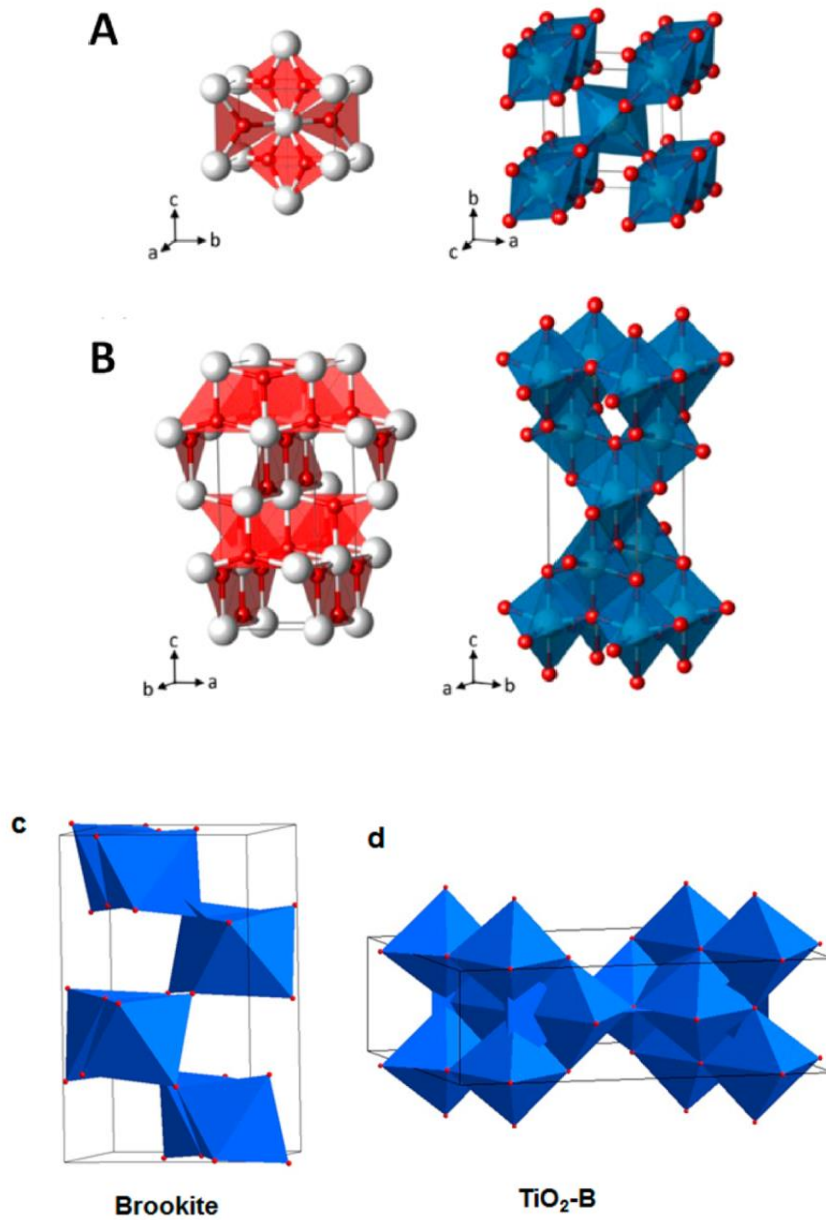


Figure 10. polyhedral representation of rutile(A) and anatase(B) and other unit cell structure (brookite: c,  $\text{TiO}_2\text{-B}$ : d) [50-51]

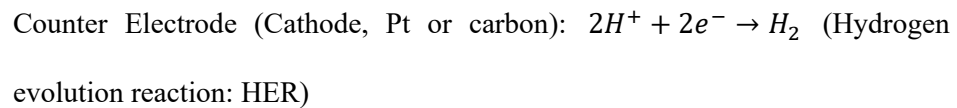
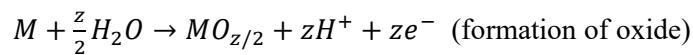
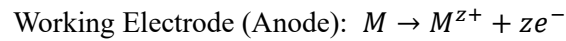
### 1.2.2 Self-organized TiO<sub>2</sub> Nanotube arrays

There are many ways to make TiO<sub>2</sub> nanotubes. (Figure 11) It can be divided into solution-based approaches, vapor-based approaches, templated growth and electrochemical methods.<sup>50</sup> Solution-Based Approaches include hydrothermal/solvothermal methods, sol-gel methods, surfactant-assisted methods, microwave assisted methods, sonochemical synthesis, high temperature pyrolysis and electrospinning methods. Solution-based approach is low cost, and simple process, but it still has a disadvantage that it is not easy to control morphology or control physical properties.<sup>50</sup> Vapor-based approaches include chemical / physical Vapor Deposition (CVD / PVD), atomic layer deposition(ALD)-related methods, and pulsed laser deposition. Since it grows at a high temperature in a vacuum condition, it has good crystallinity and it is a great advantage that it can precisely control composition and growth site with a catalyst or a precursor.<sup>50</sup> However, it has a disadvantage of being expensive and having a bad scalability. Templated growth is a method of controlling morphology by using a porous template. The biggest advantage is that growth does not have a large effect on the crystal surface of the material. However, there is a disadvantage that crystallinity is not good and purity is not easy to control. Electrochemical methods can grow TiO<sub>2</sub> nanotube arrays directly on Ti metal, and it is not difficult to control length or pore size. Many people have tried it because it is simple, low-cost, and excellent in scalability.

The origin of the electrochemical process of forming TiO<sub>2</sub> nanotube arrays dates back to the formation of the Alumina porous layer. Anodic Aluminum Oxide (AAO) was

first reported by Rummel<sup>52</sup> and Baumann<sup>53</sup>, and has attracted much interest from researchers. Especially, various anodization methods (mild anodization (MA), hard anodization (HA), pulse anodization (PA), cyclic anodization (CA)) have been studied, especially for templates or platform as energy storage<sup>54-56</sup>, photovoltaic<sup>57-58</sup>, photonic applications<sup>59-60</sup>, biomedical applications<sup>61-62</sup>, etc.). In 1999, Zwillig and co-workers demonstrated that TiO<sub>2</sub> nanotube arrays can be synthesized for the first time using fluorine-containing electrolytes.<sup>63</sup> The formation of nanotube arrays in this manner has also been applied to other valve metals and alloys (Hf<sup>64</sup>, Ta<sup>57</sup>, W<sup>65</sup>, Nb<sup>66</sup>, Zr<sup>67</sup>, Fe<sup>68</sup>, Mo<sup>48</sup>, TiW<sup>69</sup> etc).

A simple mechanism for making TiO<sub>2</sub> nanotube arrays is as follows. (**Figure 12**)<sup>70</sup>





Oxidation takes place at the working electrode, leading to a change from pure metal to metal oxide. At the counter electrode, reduction occurs, so hydrogen ions contained in the electrolyte are reduced and hydrogen gas is observed. Depending on various electrolyte conditions (temperature, pH, applied potential, electrolyte or organic, fluoride contents, viscosity, etc.), the kinetic of the reactions occurring on the working electrode can be controlled, It plays a key role. There are three possible scenarios for the growth of the oxide depending on the conditions of the electrolyte. **(Figure 12)**<sup>71</sup>

Scenario 1: If oxide is completely dissolved in the electrolyte, electropolishing of the metal layer will be observed.

Scenario 2: If oxide does not dissolve in electrolyte at all, compact oxide is formed.

Scenario 3: If the oxide partially dissolves in the electrolyte, the  $M^{z+}$  cation can be solvated Under certain conditions the formation and dissolution of the oxide will be in a steady state to form a nanotube or porous layer.

The current of anodization can be obtained by using a high field approximation, and the ionic current density is determined by the thickness of the barrier. The growth of the oxide depends on the rate at which the  $M^{z+}$  ions migrate outward and the  $O^{2-}$  ions moving inward from the water to the metal. **(Figure 12)** In general, the growth of oxide is related to the magnitude of the electric field, and the equation is given by

$$I = Ae^{BE}, E = \frac{\Delta U}{d}$$

where  $I$  is the current,  $\Delta U$  is the voltage across the oxide layer of thickness  $d$ , and  $A$  and  $B$  are material-dependent constants.<sup>72</sup>

If a compact oxide is formed, the electric field is greatly reduced as the thickness of the oxide layer becomes thicker, which interferes with ion migration, and the growth of the oxide is stopped at any moment. This is given by  $d = 2.5 \text{ nm} / V * U$  in  $\text{TiO}_2$ .<sup>73</sup>

As in Scenario 3, when the oxide partially melts, metal cations will form with  $F$  anions and solvated to form water-soluble  $MF^{6-}$ . When these chemical solvents and oxides form a steady state, a porous film is formed.

Generally, a hexagonal nanopore cell (honeycomb structure) is formed in a  $\text{TiO}_2$  nanotube array. How does the nanotube form? This is related to the chemical nature of  $\text{TiF}^{6-}$ . First, the  $F$ -ion is smaller, so it can diffuse faster than the larger  $O^{2-}$  ion. Because of this, an  $F$ -rich layer is formed at the metal / oxide interface and a tube shape is formed as water easily dissolves these layers. In contrast, in the case of  $Al$ ,  $Al$ -fluoride is not well soluble in water, so a porous form is better formed.

### 1.2.2.1 Factors affecting the morphology of TiO<sub>2</sub> NTAs

#### 1. H<sub>2</sub>O-based (aqueous) vs. organic-based

In the case of H<sub>2</sub>O-based electrolytes, the chemical etching rate is faster than the organic-based ones, so the steady state is reached sooner and the length is limited. The maximum growth is reported to be about 2.5 micrometers.<sup>74</sup> On the other hand, an organic-based electrolyte can grow up to 100 micrometers, and the pore radius can grow larger.<sup>75</sup> In addition, organic-based electrolytes can slow the dissolution of cell boundaries because the chemical etching rate is significantly slower, which is advantageous for making highly ordered structures. The nature of the organic material also depends on whether it is based on dimethyl sulfoxide (DMSO) or on ethylene glycol (EG). Single-walled NTAs are created based on DMSO<sup>76</sup>, whereas double-walled NTAs are created based on EG.<sup>47</sup> **(Figure 13)**

#### 2. Temperature

Growth occurs more slowly because the kinetic associated with ion migration is worse at lower temperatures. In addition, if the temperature is very low, it can be observed that the nanotubes are grown not in nanotubes but in chemical etching.<sup>77</sup> As a result of the observation of the composition, the nanocolumn is composed of an F<sup>-</sup> rich composition and is easily etched by water. **(Figure 13)**

### 3. Presence or absence of complexing agent

When complexing agents such as lactic acid<sup>78</sup> or EDTA<sup>79</sup> are used,  $Ti^{4+}$  ions are caught, which prevents  $Ti^{4+}$  ions from diffusing into the inner wall. As a result, the thickness of the bottom layer becomes thinner and the thickness of the barrier oxide becomes thinner, so that a higher electric field is required than usual. So we can observe a phenomenon that grows longer than when no complexing agent is added. In addition, dielectric breakdown is not observed at a relatively large voltage. **(Figure 13)**

### 4. Concentration and pH of $F^-$ ion

The concentration of F ion and pH are also related to the dissolution of the oxide layer. The lower the pH, the faster the dissolution rate. Also, the higher the concentration of fluoride, the faster the dissolution rate of the oxide layer.<sup>80</sup> **(Figure 13)**

### 5. aging effect

As the anodization progresses more and more, the  $TiF_6^{6-}$  complex is formed in the electrolyte, which increases the ionic concentration and increases the conductivity of the electrolyte.<sup>81</sup> As a result, the longer the length of the  $TiO_2$  nanotubes is, the longer the anodization is repeated. In addition, the increased  $TiF_6^{6-}$  concentration has the effect of slowing the rate of chemical dissolution and increasing the maximum oxide length.<sup>82</sup> **(Figure 13)**

## 6. Voltage

Voltage is often known to have a proportional relationship with diameter.<sup>83</sup> Higher voltages increase the strength of the electric field through the oxide layer and affect the migration and diameter of the ions. However, if the electric field reaches a certain threshold value, the diffusion of water becomes a rate-determining step and the voltage and potential are inversely proportional to each other. (**Figure 13**)

## 7. Time

The length of the TiO<sub>2</sub> nanotubes can be controlled with time, and the maximum length of the TiO<sub>2</sub> nanotubes is determined by the steady state. Sometimes it takes a long time to observe the shape of the nanograss.<sup>80</sup> (**Figure 13**)

## 8. Presence of pre patterning

If you do pre-patterning, you can observe that the tube grows in a more well-ordered form.<sup>84</sup> The most common method is the double anodization method, which is also derived from AAO growth.<sup>85</sup> In addition, pre-patterns can be created using Focused Ion Beam (FIB)<sup>86</sup> or other nanoimprinting methods such as stamping.<sup>87</sup> (**Figure 13**)

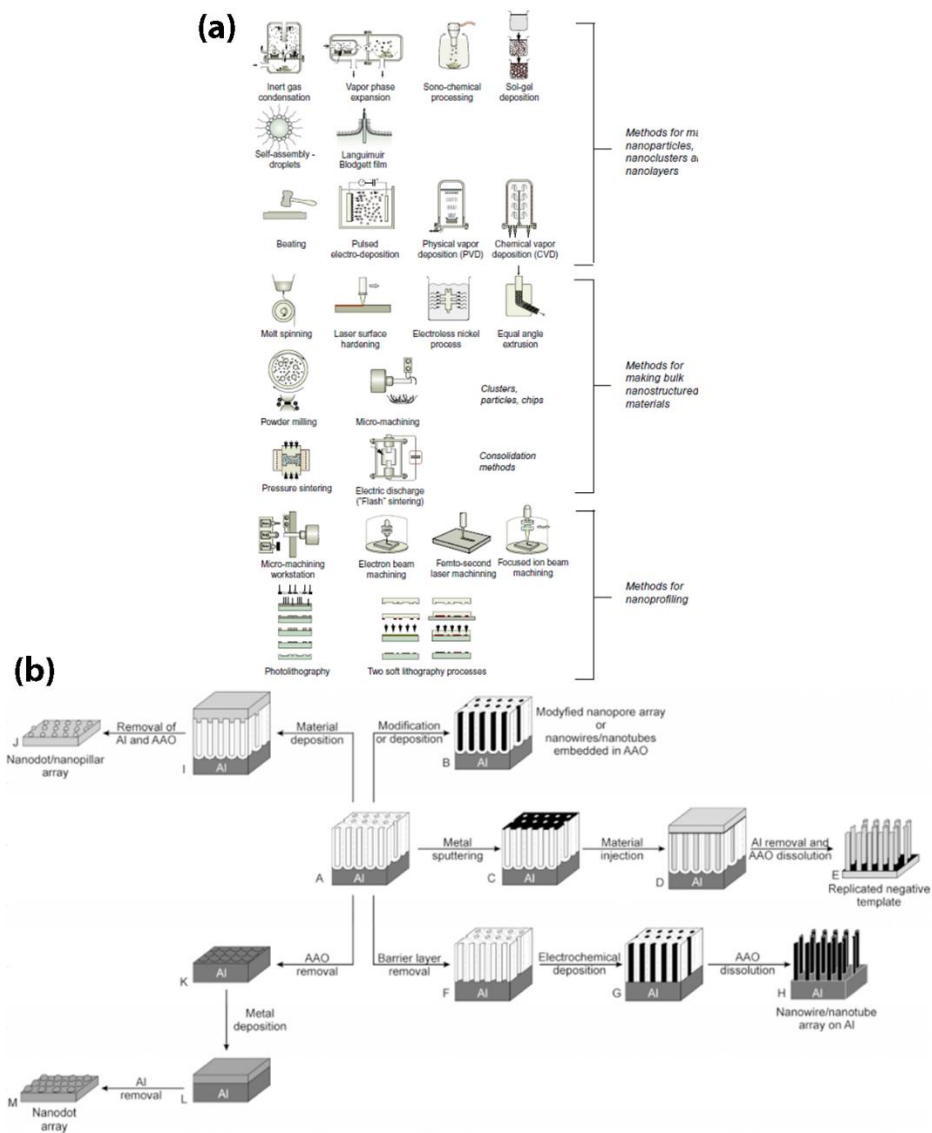


Figure 11. Summary of synthesis methods for  $\text{TiO}_2$  nanomaterial. (a) general method for synthesizing nanomaterials [88] (b) AAO- assisted templated synthesis. [89]

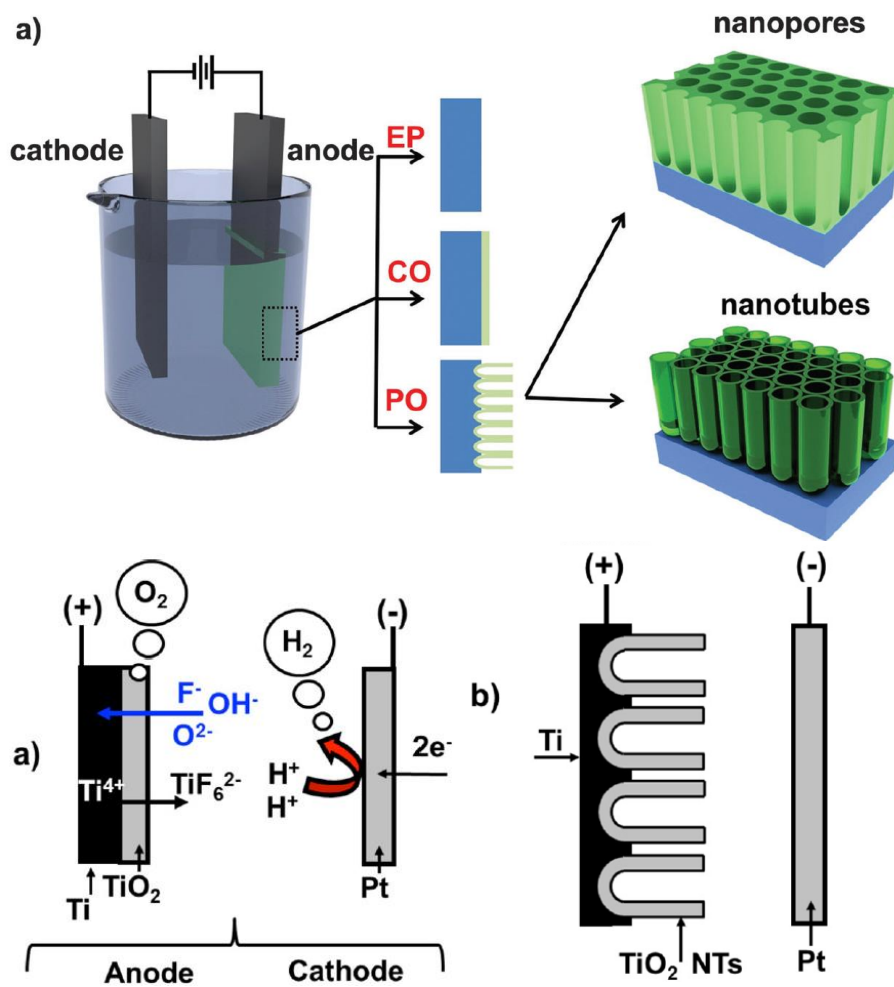


Figure 12. Three possible scenarios for electrochemical anodization schematic view of reactions that occur during the anodization. [70-71]

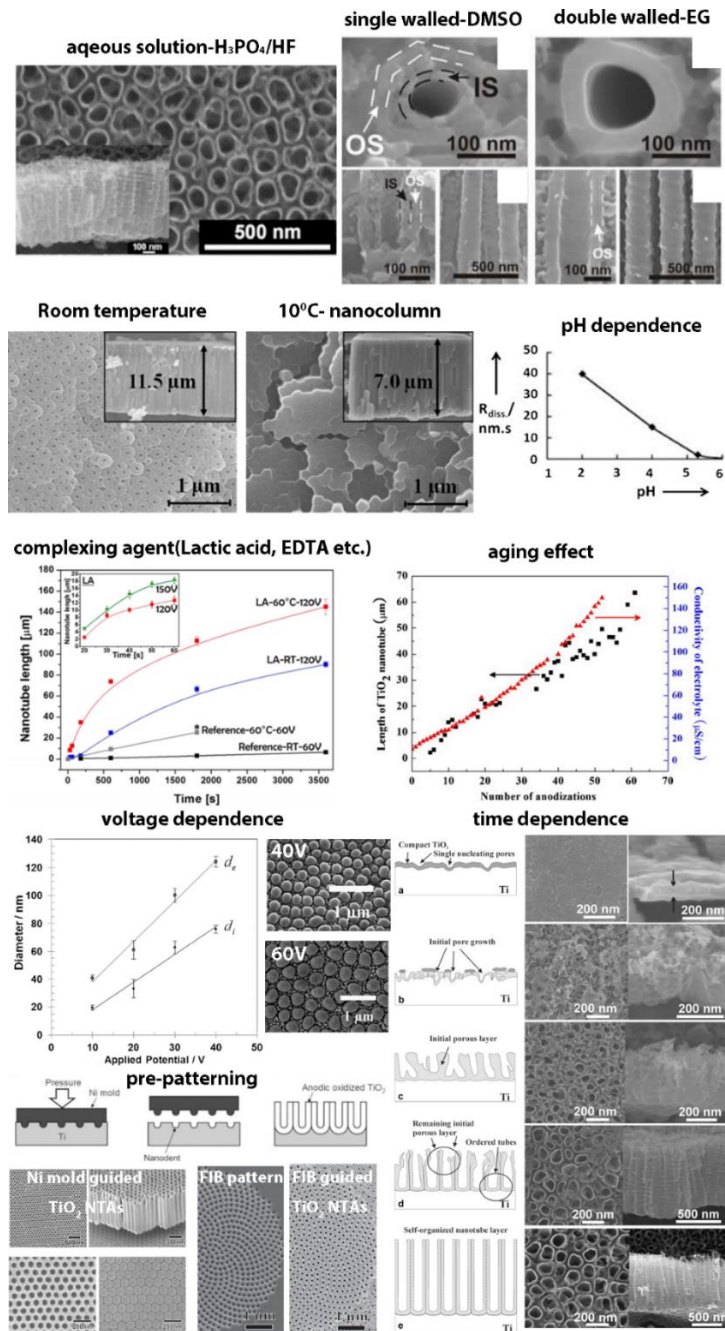
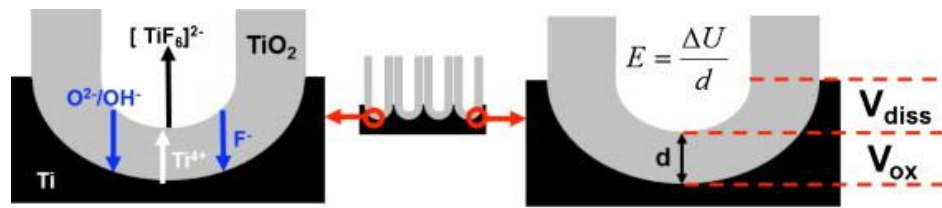


Figure 13. Factors that affect the morphology of  $\text{TiO}_2$  nanotube arrays [75, 77, 90, 78, 80, 86, 87]

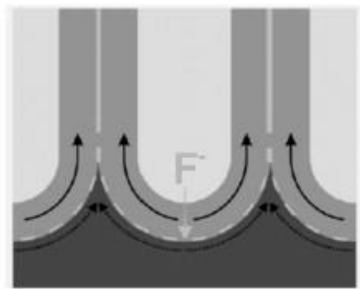


### 1.2.3 Mechanistic regime

There are two main mechanisms that explain the formation of TiO<sub>2</sub> nanotube arrays. (**Figure 14**)<sup>70</sup> One is the field-assisted dissolution model and the other is the flow mechanism model. The field-assisted dissolution model describes that the oxide layer is formed in both the metal / oxide interface and the oxide / electrolyte after the pore is first initiated, and the electric field is concentrated inside the pore, causing dissolution centering thereon Model. Recently, the flow mechanism model has been proposed to explain other phenomena. The pore initiation of TiO<sub>2</sub> nanotube arrays differs slightly depending on the type of electrolyte. In the case of aqueous solution, both Ti<sup>4+</sup> injection into the electrolyte and dissolution of the oxide layer by F<sup>-</sup> ion contribute to the electrolyte, whereas in the organic solvent, the chemical dissolution becomes very small and the pore is formed only under special circumstances. Recent studies have reported that morphological instability leading to pore initiation and self-order occurs in certain oxide formation efficiencies. In this model, plastic flow and stress associated with volume expansion are not important. However, a model has been recently proposed in which a pore is formed by perturbation between an oxide layer and an electrolyte. As a result, TiO<sub>2</sub> nanotube arrays using organic solvents have been shown to play an important role in complex formation of pores by ejection of Ti and field-assisted dissolution of oxide layers by F<sup>-</sup> ions.



a) Field assisted dissolution: at stage III of i-t curve  $V_{ox} \cong V_{diss}$



b) Flow model mechanism:  
forming oxide being pushed  
upwards

Figure 14. Two representative model of formation of  $TiO_2$  NTAs. [70]

#### 1.2.4 Black TiO<sub>2</sub> and modification of physical properties of TiO<sub>2</sub> NTAs

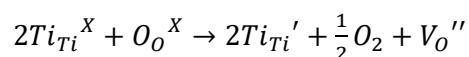
In general, the anatase phase is known to be the largest electron mobility phase.<sup>91-</sup>  
<sup>92</sup> For this reason, applications related to the conduction of electrons such as solar cells<sup>93</sup>  
and photoelectrochemical cells<sup>94</sup> are related to anatase. However, rutile has an advantage  
in synthesizing single crystals because rutile is the most thermodynamically stable  
phase.<sup>95</sup>

In the case of TiO<sub>2</sub> nanotube arrays, both amorphous and anatase phases have a  
similar band gap of 3.2 eV. Despite similar band gaps, the properties associated with  
photoelectrochemical reactions such as solar cells are quite different. The electrical  
conductivity of TiO<sub>2</sub> differs greatly depending on the measurement method, as indicated  
in the previous review literature.<sup>46</sup> Especially, there is a big difference when measured in  
a 2 points geometry and 4 points geometry. (**Table 4**) Comparing the results of 4point  
measurements with bulk, it can be seen that the resistance is smaller in case of nanotube.  
In addition, electrical conductivity measurements using the impedance method can be  
explained by the high defect density of anodic TiO<sub>2</sub> nanotubes, which is slower to  
transport in bulk than transport at grain boundaries. It is also observed that the dependence  
of temperature on TiO<sub>2</sub> nanotubes is proportional to  $T^{-1/4}$ , and it is predicted that electrons  
are transported by Mott variable range hopping conduction mechanism in TiO<sub>2</sub> nanotubes.  
This implies that the TiO<sub>2</sub> nanotube system is a strongly disordered system with a  
localized charge-carrier state. (**Figure 15**)

In addition, these TiO<sub>2</sub> nanotubes can be doped in a variety of ways, making it easy to change their conductivity. The overall research trends related to this are summarized in **Figure 16**.<sup>96-97</sup> We used Ar annealing and Ar/H<sub>2</sub> annealing, which are the easiest methods to preserve defects in the TiO<sub>2</sub> nanotube array.

In particular, TiO<sub>2</sub> can produce defects (Ti<sup>3+</sup> and oxygen vacancies) when subjected to heat treatment in a reducing atmosphere or vacuum, and the color of the TiO<sub>2</sub> varies greatly. Of these, TiO<sub>2</sub> with black color is called black TiO<sub>2</sub>. Black TiO<sub>2</sub> was first reported by Chen in 2011 and reported as a photocatalyst with improved optical properties.<sup>98</sup>

TiO<sub>2</sub> NTAs also show a change in the color of TiO<sub>2</sub> when subjected to a heat treatment in a reducing atmosphere or in a vacuum containing hydrogen, and the formula in which the defect is made is as follows.<sup>99</sup>



(Kroger-Vink Notation for crystal defects)

the symbol for the atom involved, or V if the site is vacant;

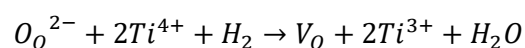
a superscript indicating the net charge:

- • for charge +1,

- X for zero net charge,

- ' for charge -1;

As can be seen from the equation,  $Ti^{4+}$  ion loses one electron to become  $Ti^{3+}$ , and oxygen is converted into oxygen, and the remaining two electrons occupy oxygen vacancy. In the case of hydrogen atmosphere, the following reaction formula is obtained.<sup>100</sup>



Hydrogenation is accomplished by the simultaneous formation of O vacancy and  $Ti^{3+}$  center.

These oxygen vacancies and  $Ti^{3+}$  can be confirmed by various methods. More roughly, it can be confirmed by shift of the XPS spectrum, and more directly by electron paramagnetic resonance (EPR). In addition, we confirmed that it was blue shifted through Raman and confirmed that this is  $Ti^{3+}$  center. In the EPR method, the oxygen vacancy is confirmed with high accuracy (g-value = 2) but the  $Ti^{3+}$  center is hard to ascertain accurately.<sup>101-102</sup> In addition, we confirm that the charge carrier is increased by the Mott-schottky method or indirectly by the difference of UV-vis spectrum. (**Figure 17**)

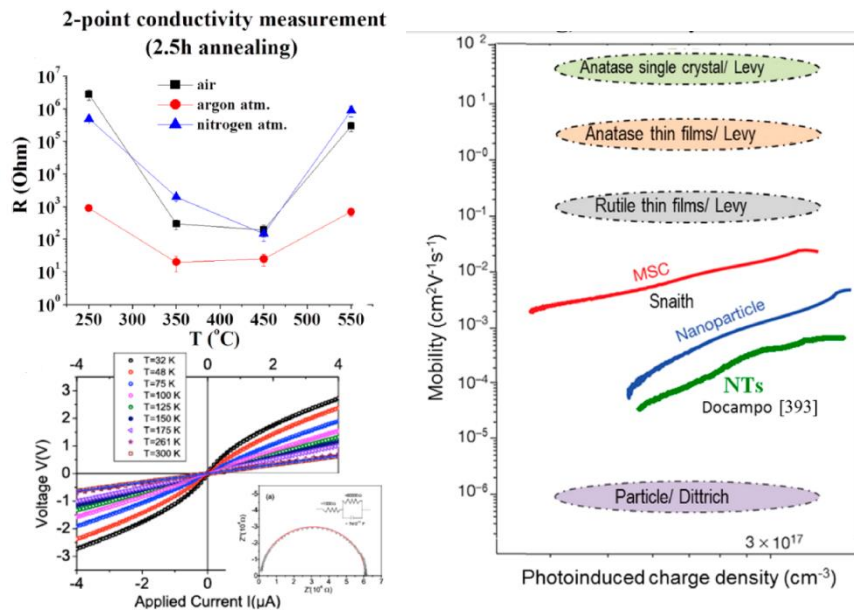


Figure 15. Electrical properties of TiO<sub>2</sub> NTAs. [46]

	TiO <sub>2</sub> NTAs	Polycrystalline bulk anatase	Single crystalline bulk anatase
Resistivity	10 <sup>-2</sup> ohm·cm / 10 <sup>2</sup> ~10 <sup>7</sup> ohm·cm*	10 <sup>2</sup> ~10 <sup>7</sup> ohm·cm	1.5 ohm·cm
Ref	103-104 * 2 point measurement	105-106	92

**Table 4 Summary of TiO<sub>2</sub> resistance measurement**

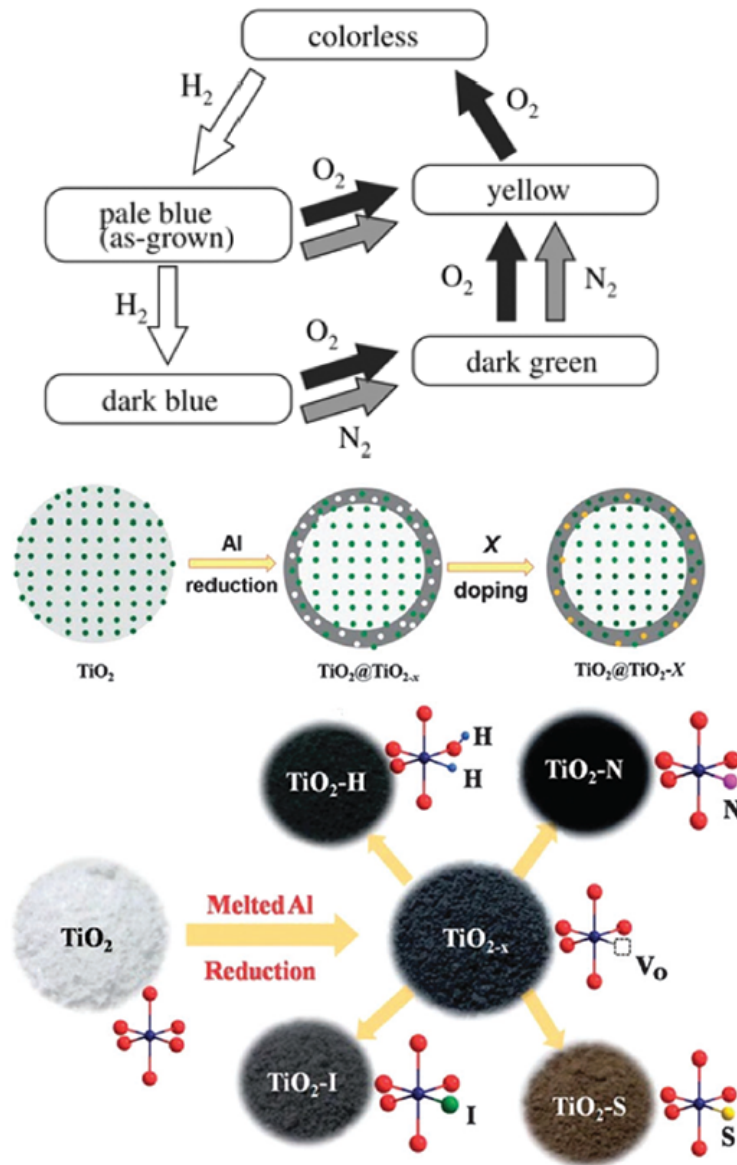


Figure 16. Summary of various doped TiO<sub>2</sub> and its color change characteristics. [96-97]



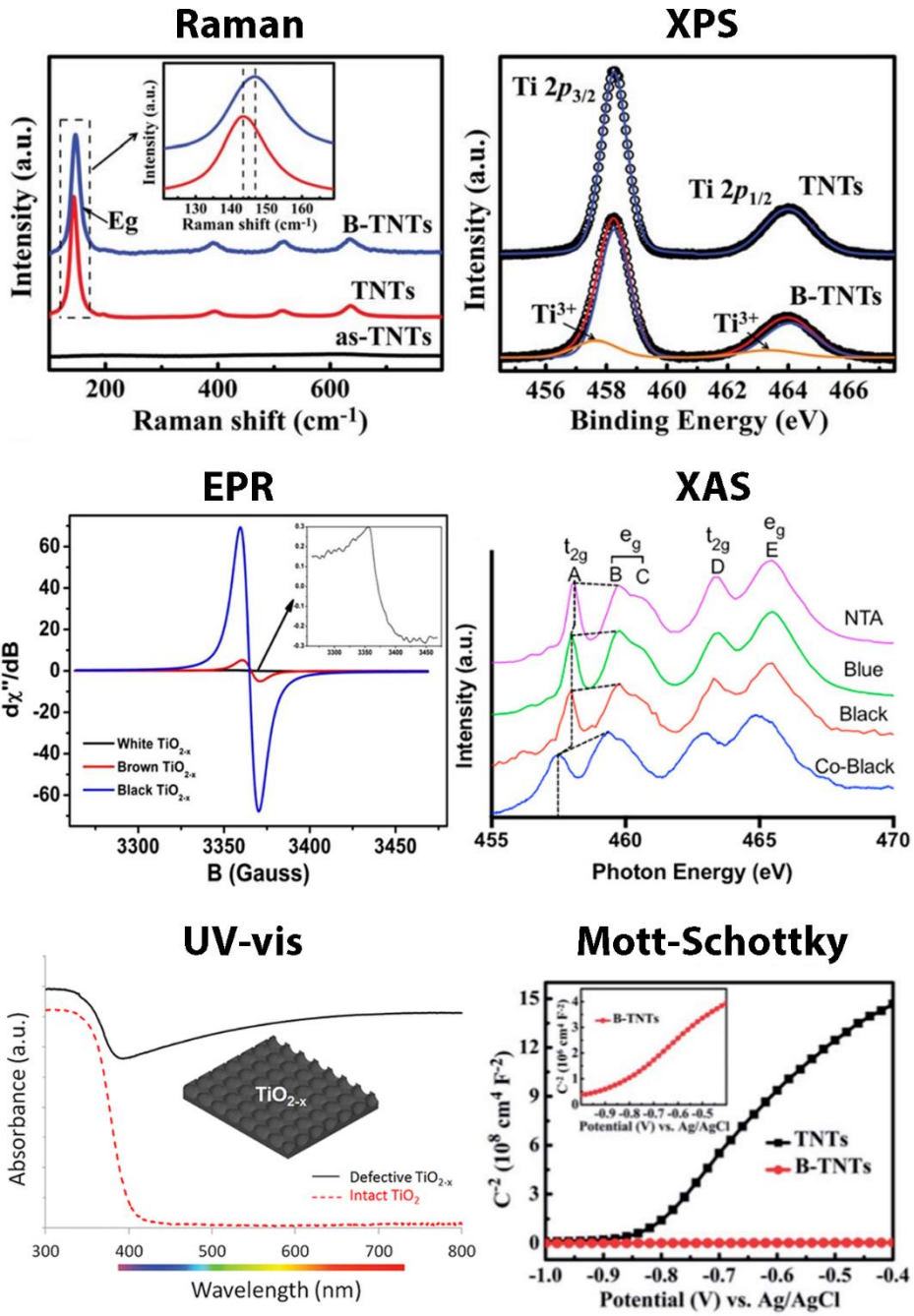


Figure 17. Various methods to identify defect in black TiO<sub>2</sub> NTAs. [101-102]

## 2. Experimental Details

### 2.1. Preparation of TiO<sub>2</sub> nanotube arrays (TiO<sub>2</sub> NTAs)

TiO<sub>2</sub> nanotube arrays were synthesized by two-step electrochemical anodization of Ti foil (thickness 0.25 mm, 99.99% trace metals basis (Aldrich)). Before anodization, Ti foils were degreased by sonication in acetone, ethanol and deionized water. The samples were anodized in electrolytes containing Ethylene glycol, 0.25wt% NH<sub>4</sub>F and 2.5vol% water. In the first-step anodization, the Ti sheet was anodized at various voltage (30V~70V) for 2hour at room temperature, and then the as-grown TiO<sub>2</sub> nanotube arrays were removed ultrasonically. The same samples underwent the second-step anodization for 30min. After anodization, the samples were cleaned with deionized water and dried under gentle nitrogen stream. Next, the pores of the TiO<sub>2</sub> nanotube arrays were widened by immersing the films in formamide solution containing 0.15M NH<sub>4</sub>F and 3.5wt% water at 72°C for 10min followed by cleaning water. b- TiO<sub>2</sub> was obtained by annealing the samples in H<sub>2</sub>(4%)/Ar atmosphere at 450°C for 1h with a heating rate 5°C/min. c- TiO<sub>2</sub> was obtained by annealing in air at 450°C for 1h with a heating rate 5°C/min.

## **2.2. Preparation of the RuO<sub>2</sub>@NTAs electrode**

Ruthenium oxide nanoparticles were deposited onto NTAs by pulsed electrodeposition (PED). RuO<sub>2</sub> electrodeposition underwent at -1mA/cm<sup>2</sup> in a three-electrode configuration with 50ms on time, and 1s off time using NTAs as the working electrode, Pt wire as the counter electrode, and a saturated calomel electrode (SCE) as a reference electrode. The electrolyte consists of RuCl<sub>3</sub>·xH<sub>2</sub>O (10mM) and KCl (0.5M) dissolved in deionized water. After RuO<sub>2</sub> electrodeposition, the fabricated samples were annealed in air at 200°C for 3h with heating rate 5°C/min.

### **2.3. Materials Characterization**

The morphology of the film was characterized by Field Emission Scanning Electron Microscopy (FE-SEM, JEOL, JSM-7600F) with Energy Dispersive X-ray Spectrometer. X-ray diffraction (XRD) patterns were collected to identify the phase of the fabricated electrode. To investigate the chemical oxidation states of the samples, X-ray photoelectron spectroscopy (XPS, SIGMA PROBE (VG, UK)). To calibrate the binding energy of the samples, C 1s photoelectron peak (284.5eV) was used. The detailed crystallographic structure and morphology is studied by Transmission electron microscopy (JEOL, JEM-2100F).

## 2.4. Electrochemical measurements

The fabricated electrodes were characterized by cyclic voltammetry (CV) in a three-electrode system consisting of fabricated electrode, Pt wire and saturated calomel electrode (SCE) as working electrode, counter electrode and reference electrode respectively. The schematic view of electrochemical setup is down below. **(Figure 18)**<sup>107</sup> To perform hydrogen evolution reaction (HER) test, the nitrogen purged 0.5M H<sub>2</sub>SO<sub>4</sub> electrolyte was used. For chlorine evolution reaction (CER) test, 5M NaCl (pH=2) was employed as electrolyte. The electrical double layer capacitance (EDLC) of electrodes were carried out by using cycling between 0.2V and 0.4V vs RHE at various scan rates of 10mV/s, 25mV/s, 50mV/s, 100mV/s and 200mV/s. The current density at 0.3V vs RHE and the corresponding scan rates were linearly plotted.

The ferrocene (Fe(C<sub>2</sub>H<sub>5</sub>)) solution (2mM) is prepared by dissolving ferrocene in acetone. To reduce the resistance of solution, 0.3M tetrabutylammonium tetrafluoroborate ([Bu<sub>4</sub>N] BF<sub>4</sub>) is used as supporting electrolyte. For each ferrocene solution, the cyclic voltammetry was recorded in the potential range of 0.6V<sub>SCE</sub> to 1.2V<sub>SCE</sub> at 10mV/s scan rate.

Vanadium redox couple solution is prepared by dissolving 0.1M VOSO<sub>4</sub> in 3M sulfuric acid. For each solution, the cyclic voltammetry was conducted in the potential range of -0.75V<sub>SCE</sub> to 0.75V<sub>SCE</sub> at 50mV/s scan rate.

Electrochemical impedance measurements to obtain the Mott-Schottky plot, using a conventional three-electrode system and a computer-controlled multichannel potentiostat (PARSTAT MC 1000, Princeton Applied Research, USA).

The donor density of b-TiO<sub>2</sub> substrate can be measured through the capacitance measurement. Using Mott-Schottky equation, the carrier density is calculated as follows.

$$\frac{1}{C^2} = \frac{2}{eA^2\varepsilon\varepsilon_0N_D} \left[ (U_S - U_{FB}) - \frac{k_B T}{e} \right]$$

Where C is the space charge capacitance, A is the geometric area of electrode,  $N_D$  is the donor carrier density, e is the elementary charge,  $\varepsilon_0$  is the permittivity of the free space,  $\varepsilon$  is the dielectric constant of the electrode material(=48 for anatase TiO<sub>2</sub>),  $U_S$  is the applied potential,  $U_{FB}$  is the flat band potential,  $k_B$  is the Boltzmann constant and T is the temperature.

To determine electrochemical characters of interface between electrode and interface, electrochemical impedance spectra (EIS) was measured under various potential from -1V to 2V vs SCE at fix frequency, 1000Hz. When voltage applied electrodes, the electrical capacitance and resistance are defined below. **(Figure 19)**<sup>108</sup> The electrochemical impedance spectroscopy (EIS) is a useful tool for analyzing the electrochemical properties of interfaces. The impedance method is a method of recording a change in capacitance and resistance by applying a small alternating voltage. Electrochemical reactions often occur between the electrodes and the electrolyte, which can be analyzed by the impedance method. When the electrode is negatively charged on a flat electrode, the circuit corresponding to the schematic diagram is as follows. **(Figure 19)**

Also, the impedance value at this time is given by the following equation. <sup>108</sup>

$$Z(\omega) = R_s + \frac{R_p + \sigma\omega^{-\frac{1}{2}}}{\sigma\omega^{\frac{1}{2}}(C_d + 1)^2 + \omega^2 C_d^2 (R_p + \sigma\omega^{-\frac{1}{2}})^2} + j \frac{\left[ \omega C_d (R_p + \sigma\omega^{-\frac{1}{2}})^2 + \sigma\omega^{-\frac{1}{2}} (C_d \sigma\omega^{\frac{1}{2}} + 1) \right]}{(C_d \sigma\omega^{\frac{1}{2}} + 1)^2 + \omega^2 C_d^2 (R_p + \sigma\omega^{-\frac{1}{2}})^2}$$

Here,  $\omega = 2\pi f$ ,  $f$  is frequency,  $j = \sqrt{-1}$ , and

$$\sigma = \frac{RT}{\sqrt{2}n^2 F^2 A} \left( \frac{1}{D_O^{\frac{1}{2}} C_O(x, t)} + \frac{1}{D_R^{\frac{1}{2}} C_R(x, t)} \right)$$

where  $A$  is the electrode area,  $C_s$  are concentrations of subscripted species at a distance  $x$  from the

electrode surface, and  $t$  is time

When the frequency goes to infinity, the following equation can be used.

$$Z(\omega) = R_s + \frac{R_p}{1 + \omega^2 C_d^2 R_p^2} - j \frac{\omega C_d R_p^2}{1 + \omega^2 C_d^2 R_p^2} = Z'(\omega) - jZ''(\omega)$$

Conversely, when the frequency converges to 0, it becomes simpler as follows.

$$Z(\omega) = R_s + R_p + \sigma\omega^{-\frac{1}{2}} - j(\sigma\omega^{-\frac{1}{2}} + 2\sigma^2 C_d) = Z'(\omega) - jZ''(\omega)$$

The nyquist plot shows the real part on the x axis and the imaginary part on the y axis. In general, it can be confirmed that a semicircle is formed at a high frequency and a linear shape is formed at a low frequency. In this case, it is possible to derive a different graph depending on the ratio of the electron transfer rate to the diffusion rate. **(Figure 20)**<sup>108</sup>

In TiO<sub>2</sub> nanotube arrays, two types of models are commonly used. **(Figure 21)**<sup>109-110</sup> Recently, the second model is successful because in most cases wall is very conductive due to its thin thickness(~10nm). So we selected the second model to investigate TiO<sub>2</sub> nanotube array interface.



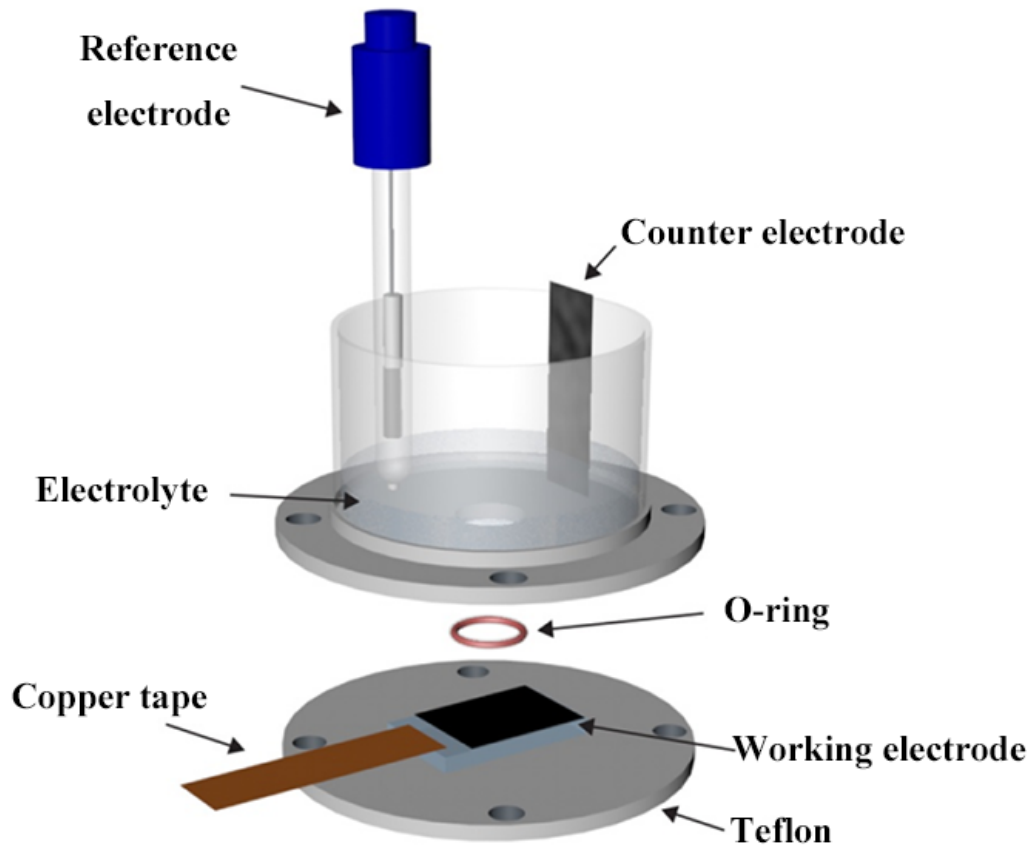


Figure 18. Schematic view of 3-electrode system used in our study. [107] This system is also applied in fabrication of anodized  $\text{TiO}_2$ .

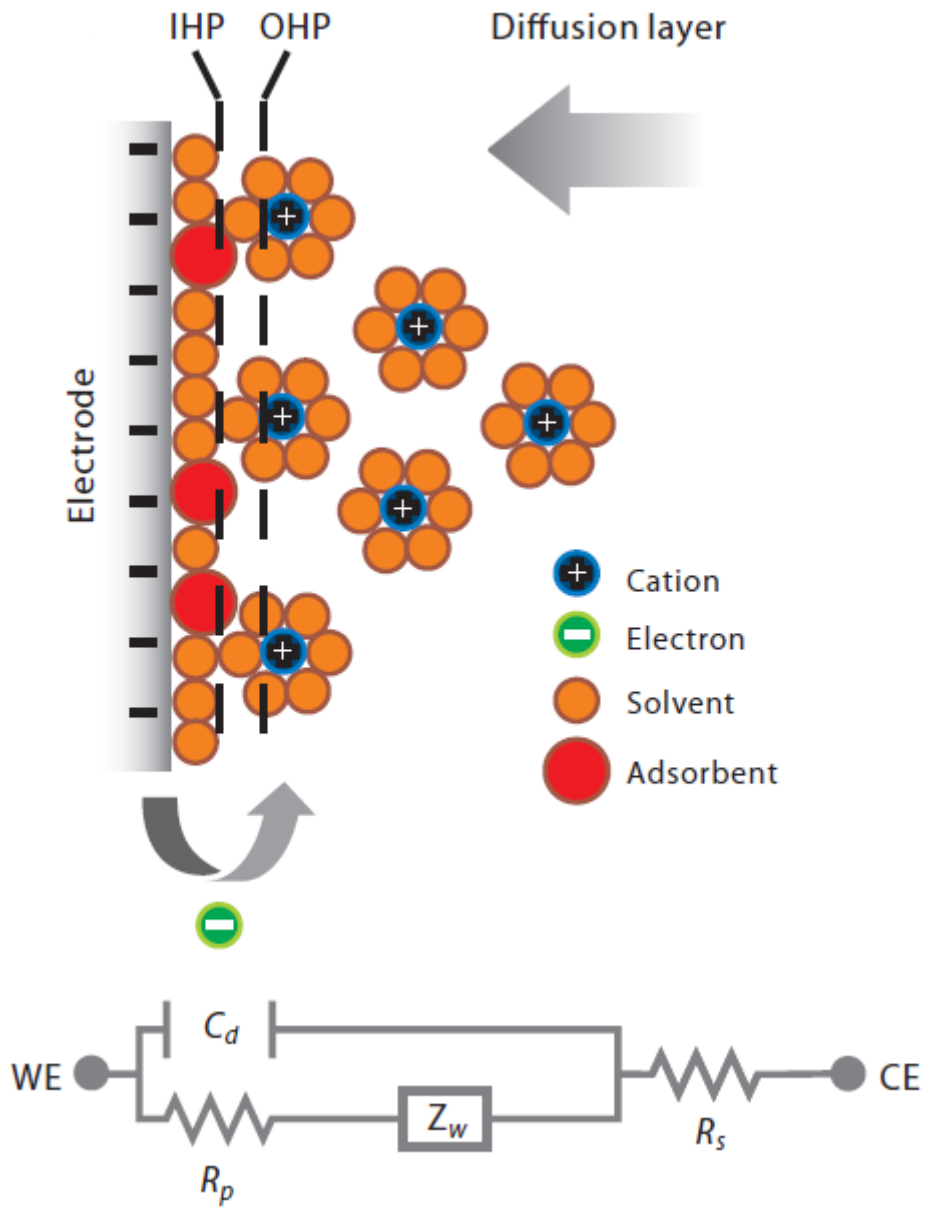


Figure 19. General schematic view of electrolyte and electrode interface. [108]

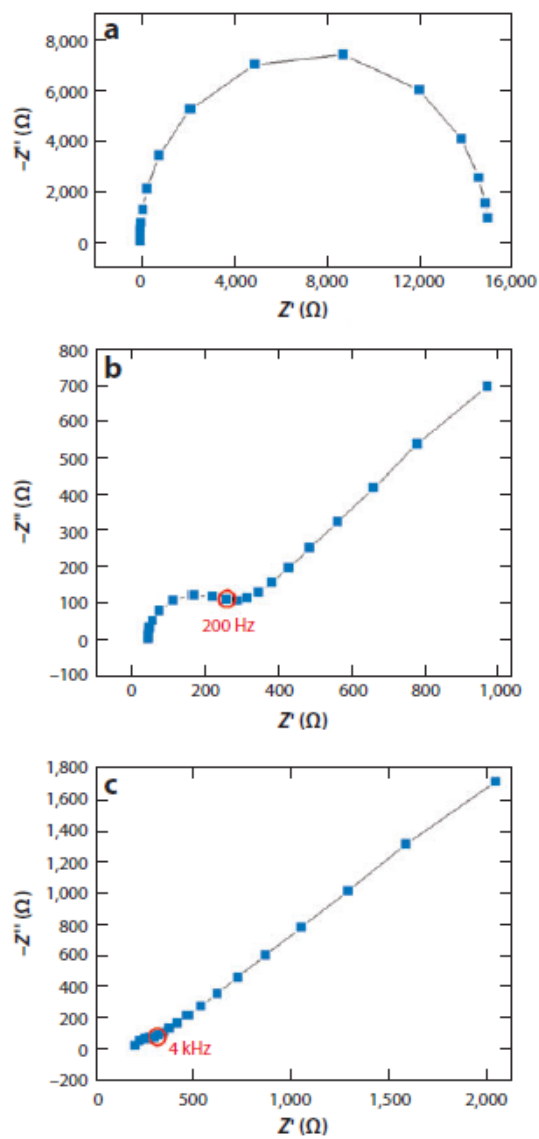


Figure 20. Three typical cases of electrochemical impedance spectroscopy (a) fast diffusion rate compared to electron transfer rate, (b) similar diffusion compared to electron transfer rate, (c) slow diffusion compared to electron transfer rate. [108]

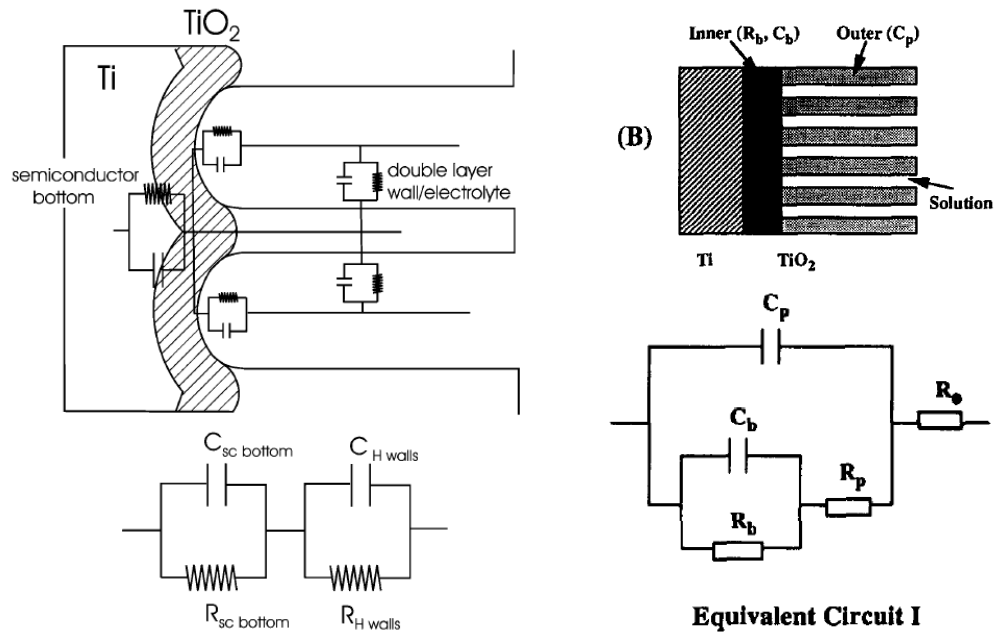


Figure 21. Two typical cases of model of  $\text{TiO}_2$  nanotube arrays. [109-110]

## 3. Results and discussion

### 3.1 Preparation of TiO<sub>2</sub> NTAs

#### 3.1.1 voltage dependence of TiO<sub>2</sub> NTAs

First, the current profile seen in typical TiO<sub>2</sub> nanotube array formation is as follows. As shown in the **Figure 22**, the current decreases dramatically as TiO<sub>2</sub> is formed, and steady state is reached at some moment and a constant current is maintained. At this time, it is known that the rate of formation and dissolution of oxide is the same.<sup>111</sup> The reason for the dullness in the graph is that chemical dissolution does not occur constantly when initial pore is generated. When 2nd anodization is performed, we can obtain a graph similar to the typical anodization process.

The magnitude of the diameter produced by varying the applied voltage was investigated with the same electrolyte conditions. TiO<sub>2</sub> nanotubes are known to increase in diameter as the voltage increases. This is because the electric field affects the migration of ions as they increase and affects the diameter. As the voltage increases, the electric field also increases and the higher electric field weakens the Ti-O bond and promotes chemical dissolution by the F-ion. This creates a dimple of larger diameter, which increases the outer diameter. (**Figure 23**) In addition, as the applied voltage increases, the wall thickness also increases, which can be explained by the increase in the thickness of the barrier oxide.

In addition, it can be seen that the length of the TiO<sub>2</sub> nanotubes linearly increases as the applied time becomes longer. (**Figure 24**)

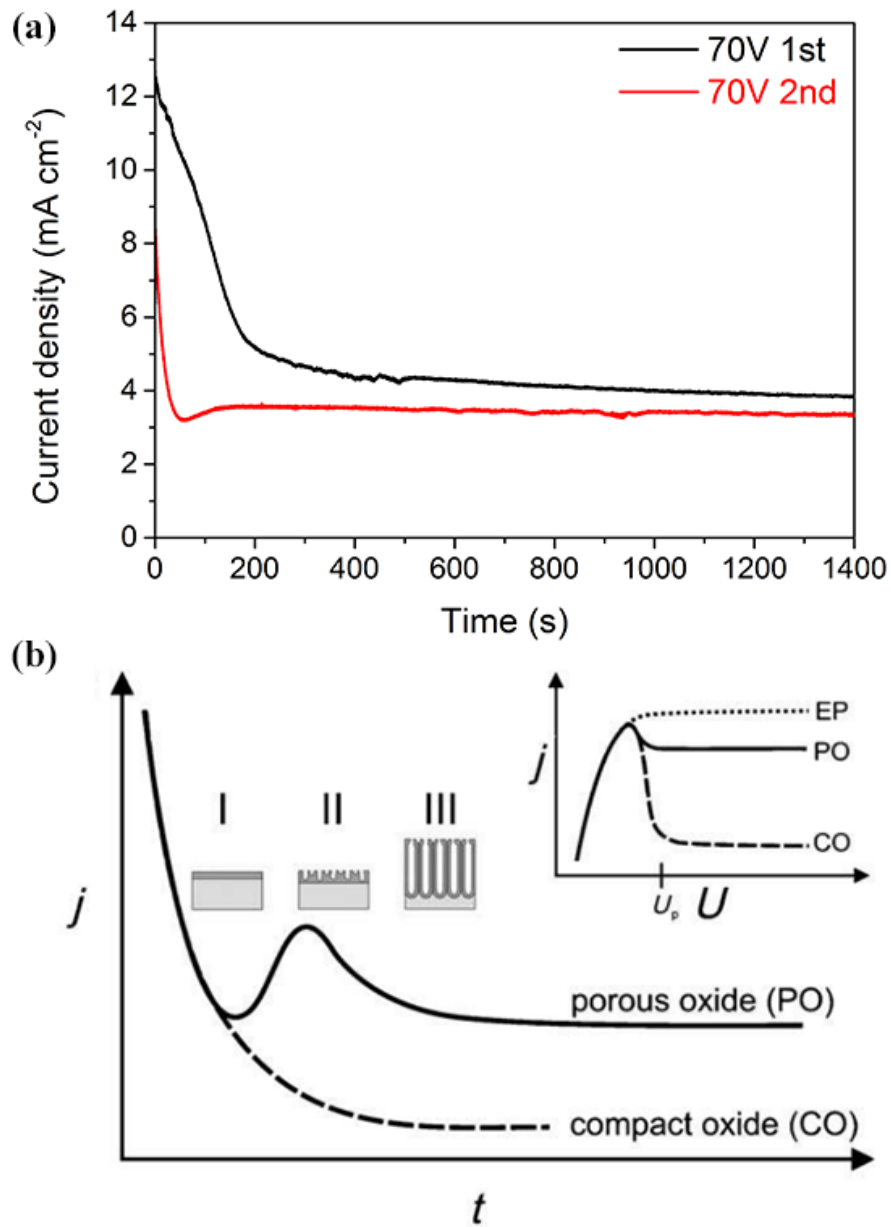
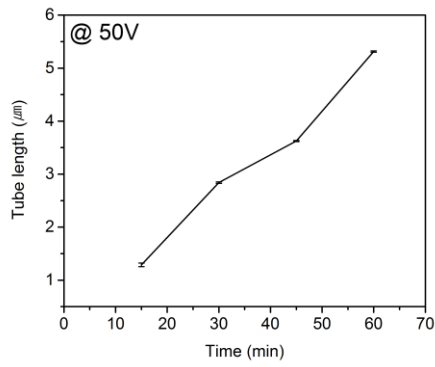
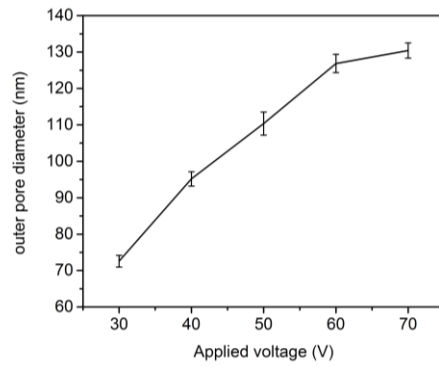
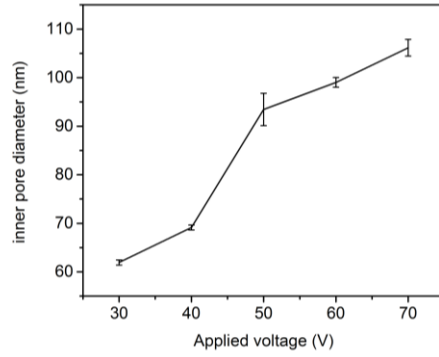
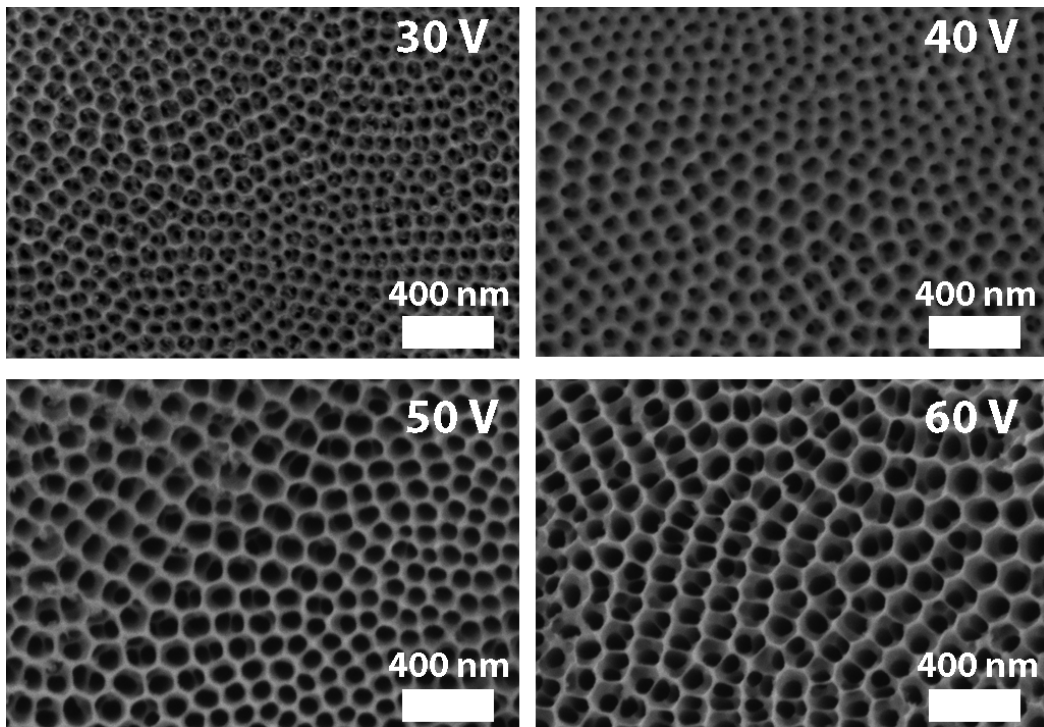


Figure 22. (a) Obtained current profile characteristics and (b) typical current-time characteristics.[111]



**Figure 23. Voltage dependence of pore diameter(inner/outer), Time dependence of tube length**

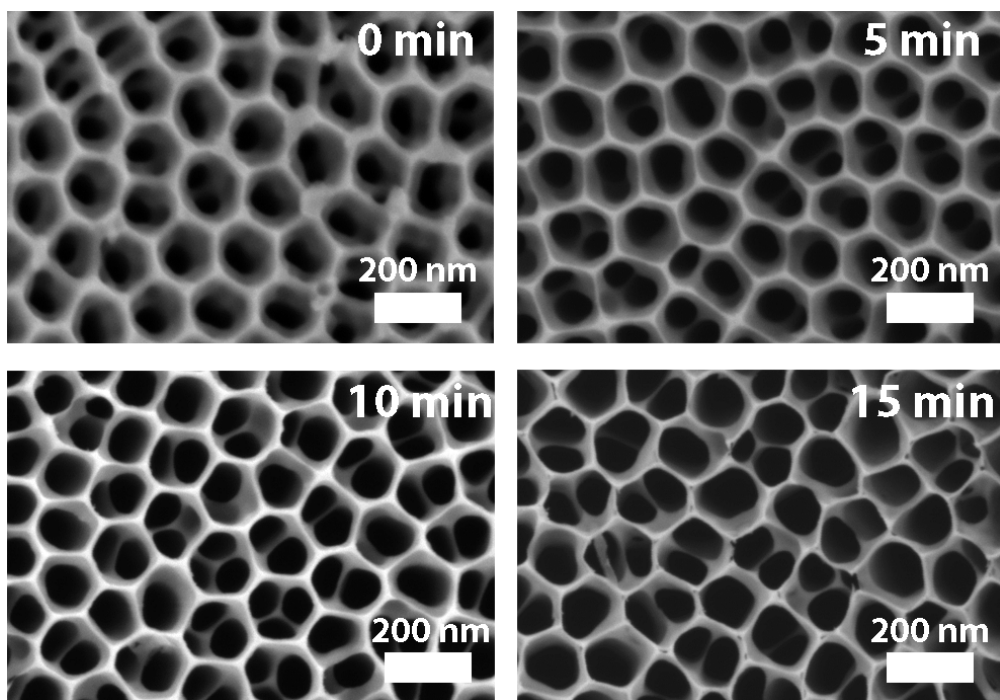




**Figure 24. Comparison of samples which is made under different voltages**

### **3.1.2 effect of pore widening**

The TiO<sub>2</sub> nanotube array can be chemically treated to enlarge the bore and eliminate the tube wall. This is called the pore widening process and is generally performed in a solution containing F<sup>-</sup> ions. Because F<sup>-</sup> ions are known to dissolve TiO<sub>2</sub> even during the anodization process, a solution containing F<sup>-</sup> ions can dissolve some of the TiO<sub>2</sub> nanotube arrays made. During the pore widening process, the length of the nanotubes decreases slightly and the thickness of the tube wall decreases. It is clearly shown in SEM images. **(Figure 25)**

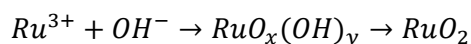
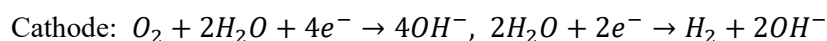


**Figure 25. Comparison of samples which is different in pore widening time.**

## 3.2 Preparation of TiO<sub>2</sub>@RuO<sub>2</sub> electrodes

### 3.2.1 pulse electrodeposition and constant current electrodeposition

In the TiO<sub>2</sub> nanotube array, electrodeposition method was used to load the catalyst. The electrochemical reactions for depositing RuO<sub>2</sub> through electrodeposition are as follows.<sup>112-113</sup>



An OH<sup>-</sup> generating reaction takes place near the cathode, where Ru<sup>3+</sup> meets Ru-based hydroxide. RuO<sub>2</sub> may be formed when the oxidation proceeds a little more. Cathodic pulses give Ru<sup>4+</sup> reduction to Ru. According to the pourbaix diagram (**Figure 26**)<sup>114</sup>, the lower the pH, the more stable the Ru metal, and the higher the pH, the more thermodynamically stable oxyhydroxide. Our RuCl<sub>3</sub> precursor can effectively inhibit the deposition of Ru metal due to its high pH. In addition, even when Ru metal is deposited, it can be confirmed that RuO<sub>2</sub> is sufficiently converted through the heat treatment process.

Typical methods of electrodeposition include constant current deposition and constant voltage deposition. In the case of deposition at a constant voltage, since the

thermodynamic potential is controlled, the desired reaction can be promoted. However, it is difficult to precisely control how much charge contributes to deposition. We experimented with a constant current to control the amount of loading RuO<sub>2</sub> loading.

In the case of deposition by a general constant current method, it can be observed that the deposition does not proceed well because the electrolyte does not enter the nanotube structure well. However, when the deposition is performed by the pulse method, it is easy to observe the deposition of the electrolyte into the nanotube and the deposition of RuO<sub>2</sub> in the nanotube by SEM or TEM. (**Figure 27**)

This process can be illustrated as follows. (**Figure 28**) In the case of pulse electrodeposition with a well-diffused electrolyte, the reaction to RuO<sub>2</sub> occurs well, whereas in the case of a constant current method in which the electrolyte does not diffuse for a long time, RuO<sub>2</sub> grows only on the top of the nanotube. This makes it impossible to use the advantage of enlarging the specific surface area, and the characteristics also deteriorate.

The model describing pulse electrodeposition is as follows. Often, using the pulse method has two advantages: First, it removes the electrical double layer around the cathode, allowing the electrolyte to transfer to the nanostructure. Second, if the current is very high, it may allow time for ions to diffuse well into the depletion region near the electrode. For this reason, electrodeposition is performed using a pulse. Eventually, the pulse duration ( $T_{on}$ ) should be less than the time at which the concentration of the reactants at the interface is zero ( $\tau$ ), and be much longer than the time to fill the electrical double

layer (EDL) capacitance ( $T_c$ ), which is prerequisite to occur faradaic reaction. Also, the time to turn off the pulse ( $T_{off}$ ) should allow enough time to discharge the electrical double layer ( $T_d$ ). These conditions can be written as follows.

$$T_c < T_{on} < \tau$$

$$T_{off} \gg T_d$$

Where  $T_c$  is the EDL charging time,  $T_d$  is the discharging time, and  $\tau$  is the migration time, which means the time it takes for the interfacial concentration to drop to zero. These values are given by the following formula.<sup>115-116</sup>

$$T_c = \frac{17}{J_p}$$

$$T_d = \frac{120}{J_p}$$

$$\tau = \frac{\pi D C_0^2 (nF)^2}{4J_p^2}$$

Where  $J_p$  is peak current density of pulse (unit :  $A/m^2$ ), and the unit of  $T_c$  and  $T_d$  is  $\mu s$ .  $D$  is diffusion coefficient of metallic ion, which have a value about  $10^{-6} \text{ cm}^2/s$ .  $C_0$  is the bulk concentration of the given ions (mol/L),  $n$  is the number of electron engaged in electrodeposition,  $F$  is Faraday's number (96486C/mol). When we put the relevant parameters ( $J_p=10A/m^2=1mA/cm^2$  10mM  $Ru^{3+}$  ion), in our experiment) into the equation related to the formation of  $RuO_2$  leads to the following parameters:

$$T_c = 1.7\mu\text{s}, T_d = 12\mu\text{s}, \tau = 2.92\text{s}$$

Therefore, we select the  $T_{\text{on}}$  as 50ms,  $T_{\text{off}}$  as 1s respectively.

The voltage profile of pulse electrodeposition is as shown below (**Figure 29**). As shown in transient voltage profile, the hydrogen evolution is not detected, which indicates no mass transfer limit during electrodeposition. If hydrogen evolution or other side reaction occurs, the voltage profile changes. (**Figure 30**)<sup>117</sup>

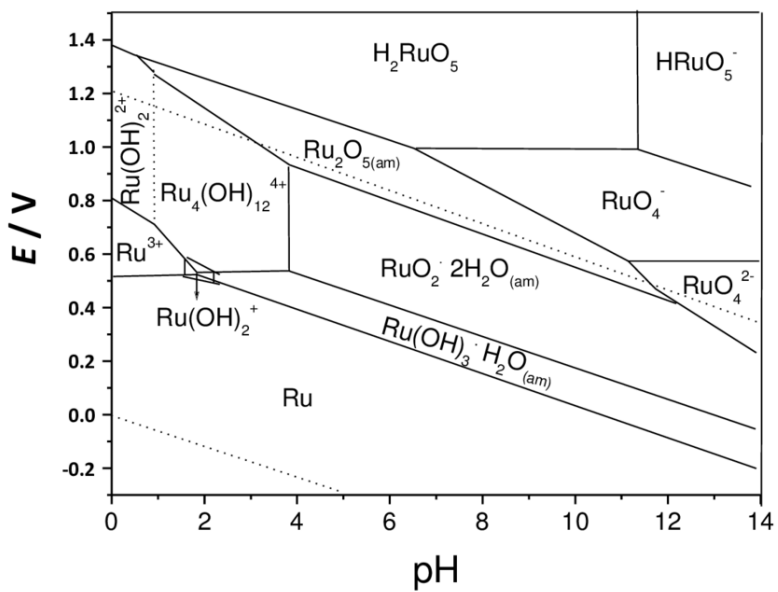
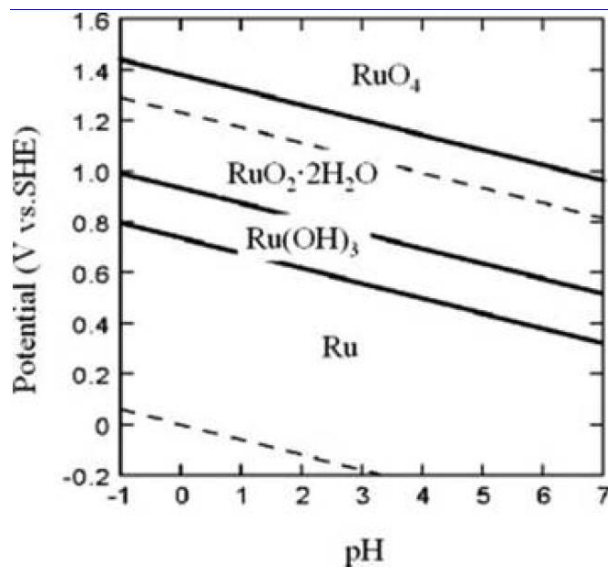
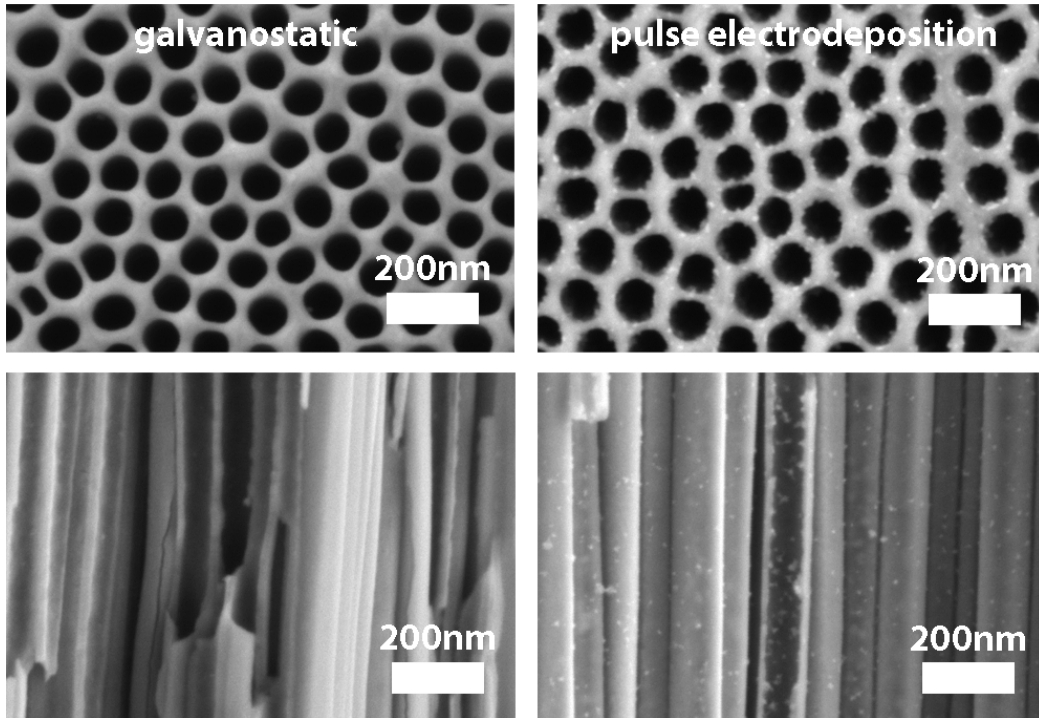


Figure 26. Pourbaix diagram of Ru-H<sub>2</sub>O system. This graph indicates thermodynamically stable phases at a given voltage and pH. [114]





**Figure 27. Comparison of  $\text{TiO}_2@\text{RuO}_2$  electrodes which is fabricated by constant-current method and pulse electrodeposition.**

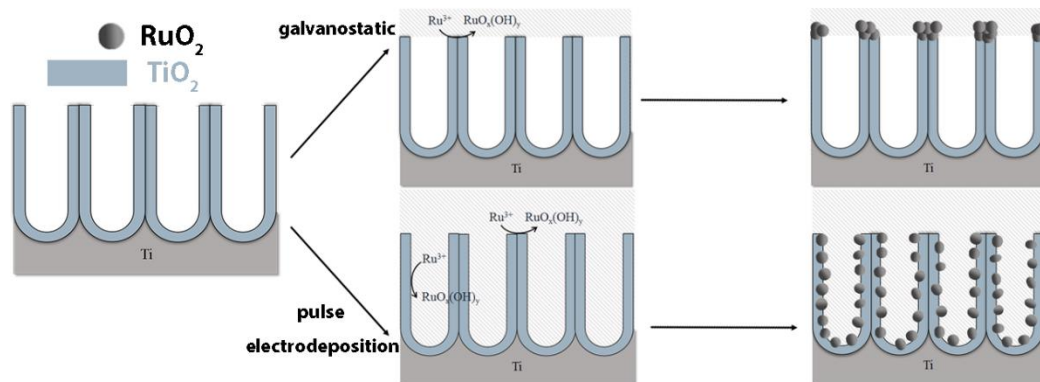
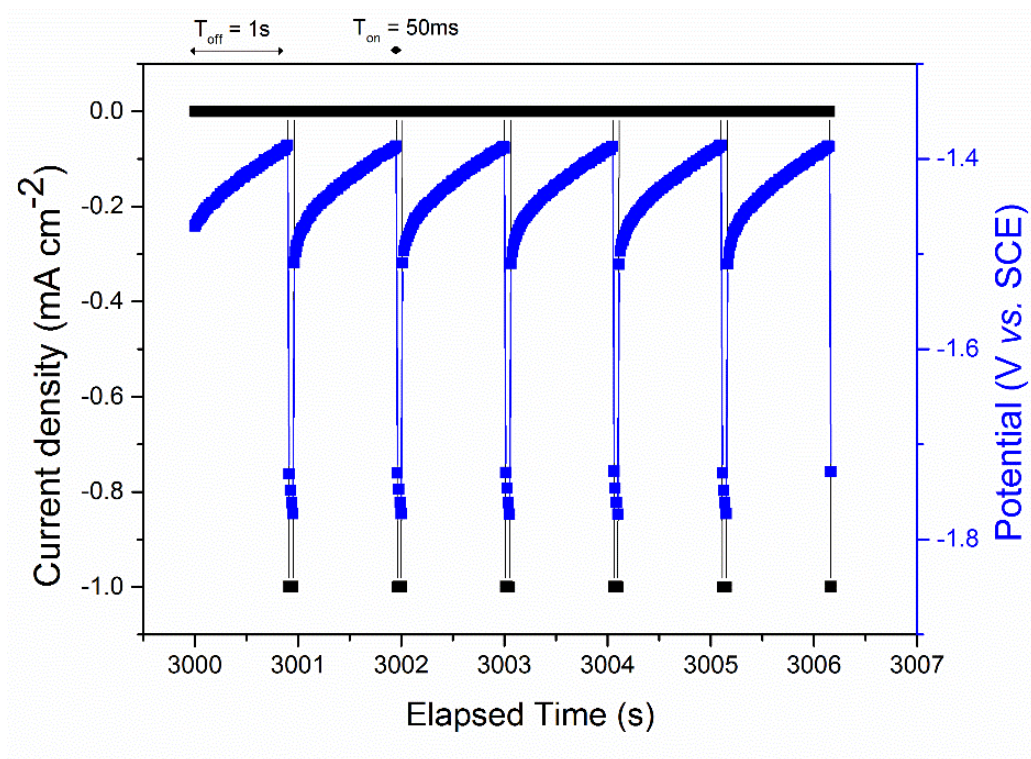
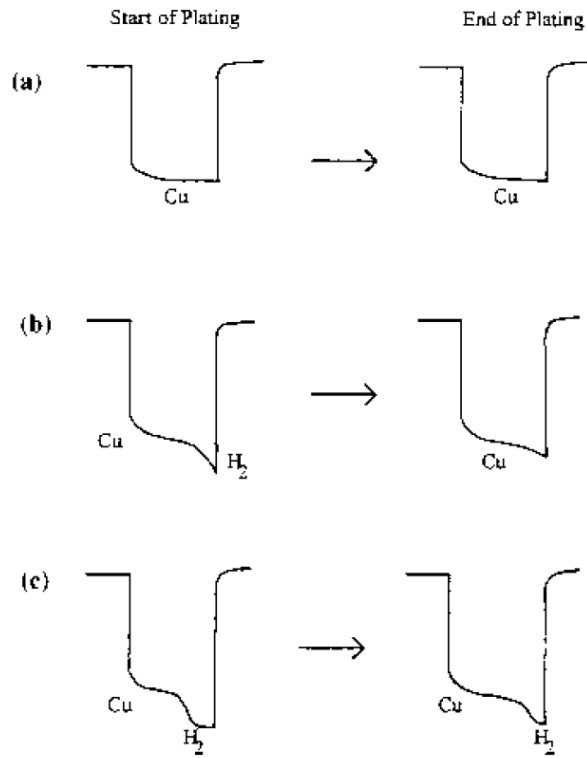


Figure 28. Schematic view of pulse electrodeposition and galvanostatic electrodeposition.



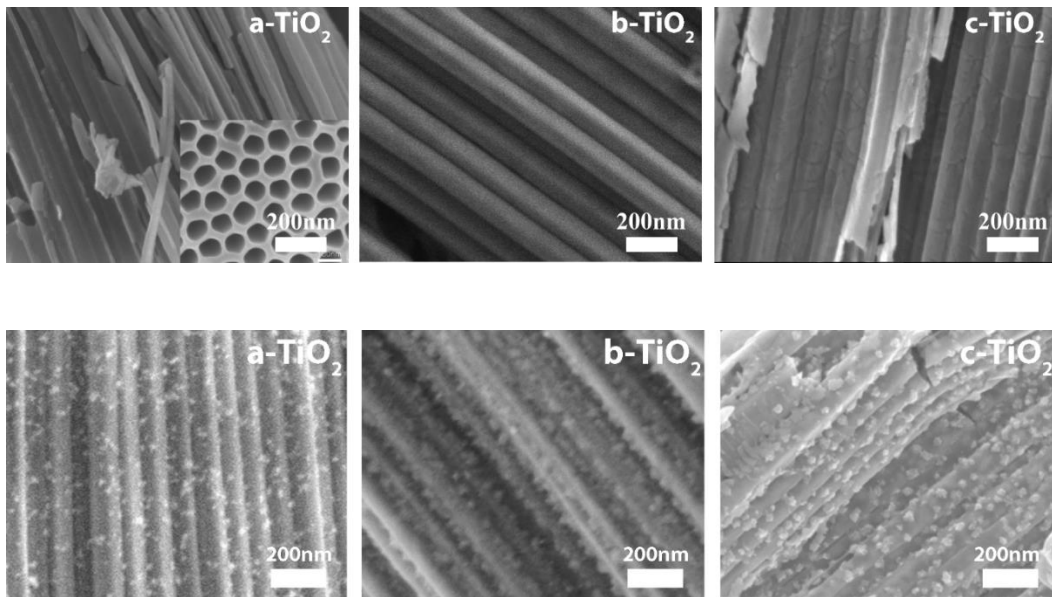
**Figure 29. Potential transients during pulse electrodeposition.**



**Figure 30. Potential transients during different condition of pulse electrodeposition. (a) no mass transfer limit (b) non steady-state (transient) mass transfer limit (c) steady-state mass transfer limit. [117]**

### 3.2.2 effect of annealing condition

TiO<sub>2</sub> nanotube arrays tend to change their electrical properties according to the heat treatment conditions. When RuO<sub>2</sub> is deposited on a TiO<sub>2</sub> nanotube array, the electrodeposition configuration may also change. However, as the nanotube arrays were annealed, the shape of the deposition did not change significantly. **(Figure 31)** This is because the cathodic pulse is used for deposition. TiO<sub>2</sub> nanotube arrays vary in their properties depending on the heat treatment conditions, but they are not significantly different in anodic and cathodic environments. As evidence for this, Vanadium redox couple cyclic voltammetry was confirmed. **(Figure 39a)** As it is shown here, the current flowing in the reduction potential does not change much. Other studies also show that there is no significant difference in conductivity at the reductive potential.<sup>118</sup>



**Figure 31. Morphology of TiO<sub>2</sub>@RuO<sub>2</sub> electrodes which fabricated under different heat treatment.**

### 3.3 Characterization of TiO<sub>2</sub>@RuO<sub>2</sub> electrodes

#### 3.3.1 Materials characterization

**Figure 32a** show the X-ray diffraction (XRD) patterns of the bare- and RuO<sub>2</sub>-loaded TiO<sub>2</sub> NTAs with various annealing conditions. The amorphous as-anodized NTAs (a-TiO<sub>2</sub>; amorphous TiO<sub>2</sub>) crystallize to the anatase phase after annealing (c-TiO<sub>2</sub>; crystalline TiO<sub>2</sub>), which is consistent with the literatures. It has been reported that the anatase-to-rutile phase transformation can be facilitated under the reducing atmosphere. However, in our study, the NTAs annealed under the reducing atmosphere (b-TiO<sub>2</sub>; black TiO<sub>2</sub>) still maintain the anatase phase, while their color change to black (inset of Fig. 26a). This observation indicates that the annealing condition is enough for the crystallization of the anatase phase and for generating a significant amount of defects (or color centers) in the lattice of anatase crystals, but not enough for the anatase-to-rutile phase transformation. It should be noted that no peaks from the RuO<sub>2</sub> crystals can be observed from the XRD patterns of RuO<sub>2</sub>-loaded TiO<sub>2</sub> NTAs. However, the existence of the RuO<sub>2</sub> can be confirmed by the X-ray photoelectron spectroscopy (XPS) shown in **Figure 32b, c**. **Figure 32b** exhibits a typical Ru 3d spectrum of the RuO<sub>2</sub>, where a peak associated with RuO<sub>2</sub> (280.37eV, 284.54eV), shake-up feature (i.e., Ru3d peak at 282.35eV, 286.55eV), and RuOH (283.3eV).<sup>119-121</sup> Also, C 1s (284.5eV and 297.4eV) is observed due to carbon contamination of the samples. **Figure 32c** also shows a typical O 1s spectrum of RuO<sub>2</sub>, where the peak at 529.1 eV is assigned to lattice oxygen in RuO<sub>2</sub>. Other peaks at 530eV

and 531.1eV are associated with OH and H<sub>2</sub>O, respectively.<sup>122</sup> Due to water affinity of RuO<sub>2</sub>, chemisorbed atomic oxygen can be observed. Therefore, it can be concluded that the RuO<sub>2</sub> has deposited successfully on the TiO<sub>2</sub> NTA electrode.

Additionally, the O 1s spectra of b-TiO<sub>2</sub> and c-TiO<sub>2</sub> compared in **Figure 33a**. It can be seen that c-TiO<sub>2</sub> is shifted toward high binding energy compared to b-TiO<sub>2</sub> indicating the density of the electron is reduced. This results can be associated with decrease of oxygen vacancy in c-TiO<sub>2</sub>. When RuO<sub>2</sub> is deposited onto TiO<sub>2</sub> nanotube arrays, the peak at 462.2eV due to ruthenium oxide can be observed. This is the result which confirms the deposition of RuO<sub>2</sub>. **Figure 33b** shows Ti 2p spectra of b-TiO<sub>2</sub> and c-TiO<sub>2</sub>. Ti 2p spectra also shows that c-TiO<sub>2</sub> is shifted toward high binding energy as compared to b-TiO<sub>2</sub>. This may also be related to the presence of Ti<sup>3+</sup> defects in b-TiO<sub>2</sub>.

**Figure 34** displays the electron microscopy images of the bare- and RuO<sub>2</sub>-loaded TiO<sub>2</sub> NTAs. The vertically aligned as-anodized TiO<sub>2</sub> NTAs (a-TiO<sub>2</sub>) with an average pore diameter of 100 nm and an average tube length of 4 μm can be prepared after the anodization process (**Figure 34a**), and their morphology does not change significantly after annealing regardless of the atmosphere (**Figure 34b, c**). It can be confirmed from the SEM images (**Figure 34d**) that the nano-sized RuO<sub>2</sub> catalysts are successfully deposited on the TiO<sub>2</sub> NTAs, which is consistent with the XPS analysis (**Figure 34b, c**). It is obvious from **Figure 34e, f** that the density and size of the RuO<sub>2</sub> nanoparticles increases with increasing number of deposition cycles (*i.e.* longer deposition), and thus the amount of RuO<sub>2</sub> catalysts loaded on the TiO<sub>2</sub> NTAs also increases. In addition to the



SEM analysis, the TEM/EDS analysis (**Figure 34g, h**) reveals that the RuO<sub>2</sub> catalysts are uniformly deposited on the surface of the TiO<sub>2</sub> NTAs.

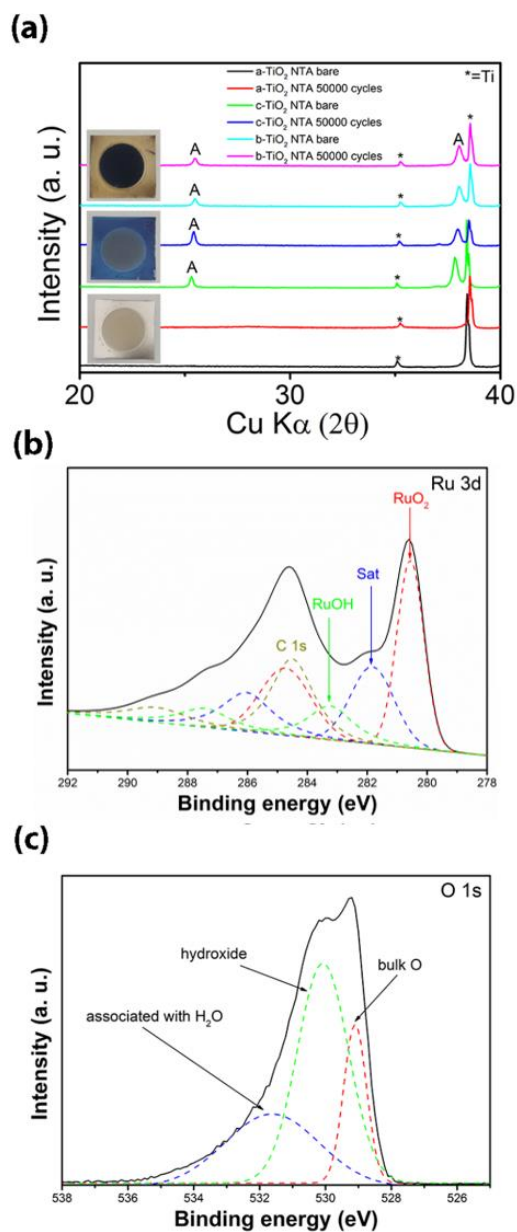


Figure 32. (a) XRD spectra of c-TiO<sub>2</sub> NTAs, different loading of RuO<sub>2</sub> (insets: optical image of a-TiO<sub>2</sub>, c-TiO<sub>2</sub>, b-TiO<sub>2</sub> NTAs) (b) XPS Ru 3d spectra of c-TiO<sub>2</sub>@RuO<sub>2</sub> 50000 pulse cycles (c) XPS O 1s spectra of c-TiO<sub>2</sub>@RuO<sub>2</sub> 50000 pulse cycles.

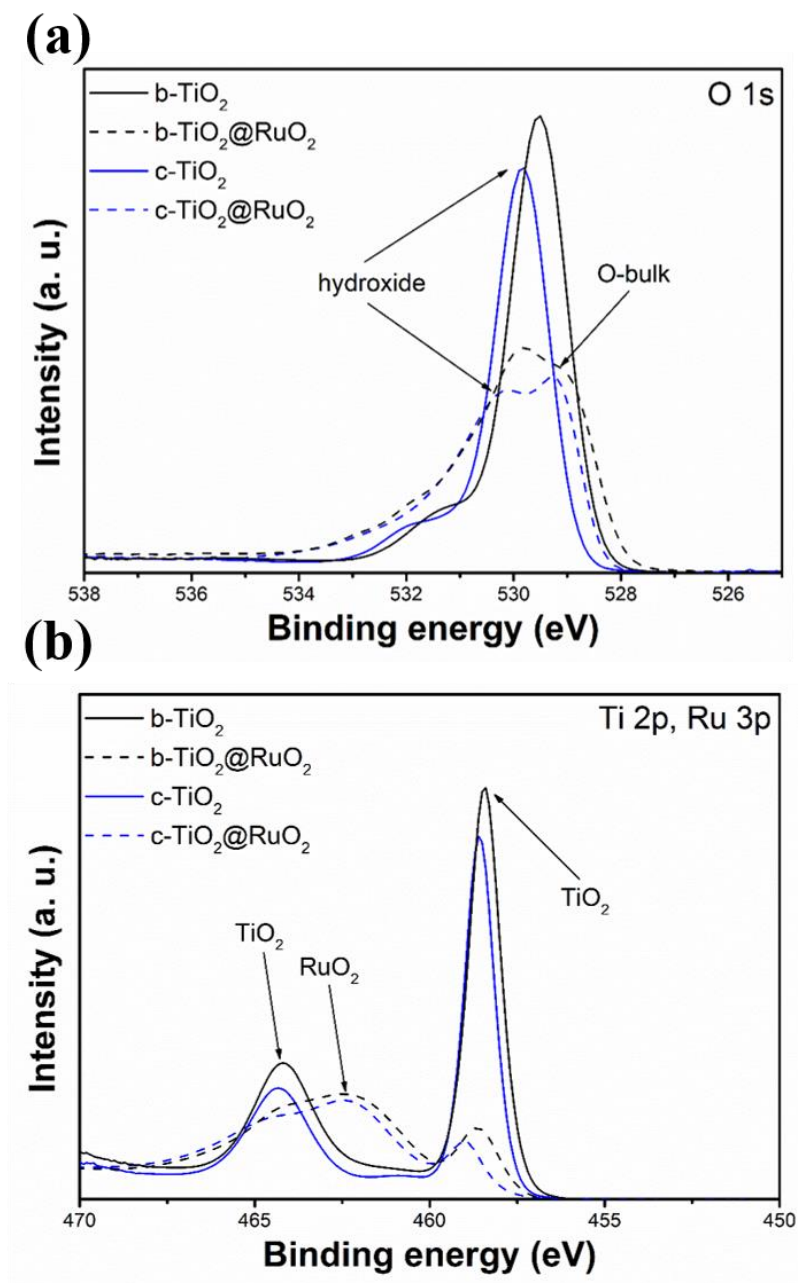
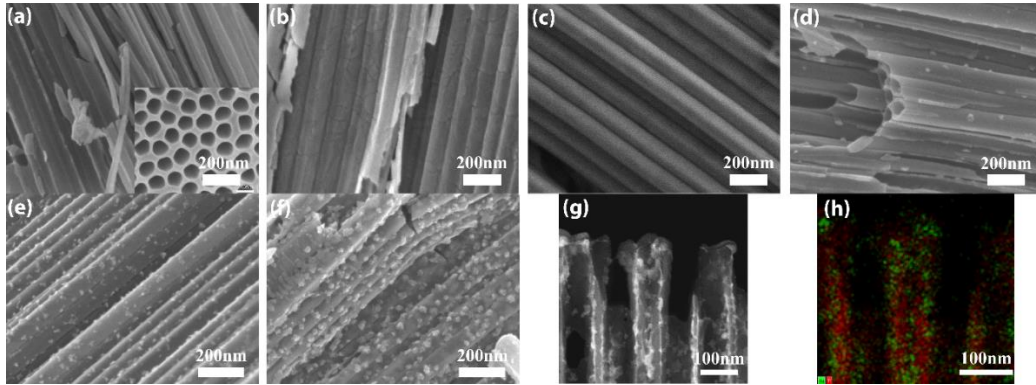


Figure 33. Comparison of (a) XPS O 1s spectra of b-TiO<sub>2</sub> and c-TiO<sub>2</sub>, (b) XPS Ti 2p spectra of b-TiO<sub>2</sub> and c-TiO<sub>2</sub>



**Figure 34. SEM image of (a) a-TiO<sub>2</sub>@ RuO<sub>2</sub> 10000 pulse cycles (inset: top view of the same sample) (b) a-TiO<sub>2</sub>@ RuO<sub>2</sub> 30000 pulse cycles (c) a-TiO<sub>2</sub>@ RuO<sub>2</sub> 50000 pulse cycles (d) c-TiO<sub>2</sub>@ RuO<sub>2</sub> 50000 pulse cycles (e) c-TiO<sub>2</sub>@ RuO<sub>2</sub> 50000 pulse cycles (f) a-TiO<sub>2</sub>@ RuO<sub>2</sub> 50000 pulse cycles. TEM image of (g) c-TiO<sub>2</sub>@ RuO<sub>2</sub> 50000 pulse cycles (h) EDS mapping of selected area.**

## 3.3.2 Electrochemical analysis

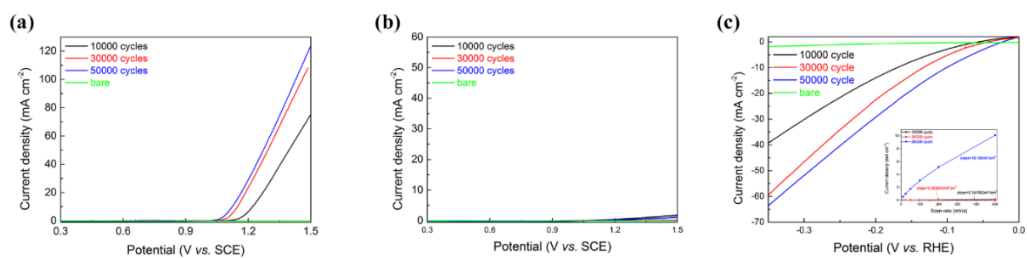
### 3.3.2.1 Evaluation of catalytic activity

**Figure 35** compares the electrocatalytic properties of the RuO<sub>2</sub>-loaded TiO<sub>2</sub> NTAs. Bare TiO<sub>2</sub> NTAs without RuO<sub>2</sub> catalysts do not show electrocatalytic activity regardless of the annealing condition. The chlorine evolution reaction (CER) activity of RuO<sub>2</sub>-loaded a-TiO<sub>2</sub> NTAs (Fig. 28a) increases with increasing amount of RuO<sub>2</sub> loading. The overpotential of current density at 10mA/cm<sup>2</sup> is 134mV, 160mV, 233mV in order of decreasing loading content. This is due to the increase of the electrochemical surface area. In spite of the reasonable CER activity, the a-TiO<sub>2</sub> NTAs are not stable during the electrochemical reaction (**Figure 36**). Although the c-TiO<sub>2</sub> NTA arrays and b-TiO<sub>2</sub> NTAs arrays exhibit better stability than the amorphous counterpart (**Figure 36**), the RuO<sub>2</sub>-loaded c-TiO<sub>2</sub> NTAs do not show the CER activity at all (**Figure 35b**). This is a somewhat unexpected result, because the same electrode shows reasonable catalytic activity when used for HER (**Figure 35c**). Given that the charge transfer or the redox reaction at the RuO<sub>2</sub>/electrolyte interface is good enough, it is likely that the conductivity of the supporting electrode (*i.e.* c-TiO<sub>2</sub> NTAs) results in the poor CER activity. This hypothesis makes sense, because the anatase TiO<sub>2</sub> is known to exhibit much higher electrical conductivity under cathodic potentials (*e.g.* HER) than anodic potentials (*e.g.* CER).<sup>118</sup> In the same context, the b-TiO<sub>2</sub> NTAs can be a good candidate for both of CER and HER,

because they are crystalline (anatase phase) and the reduced TiO<sub>2</sub> generally shows higher conductivity than the stoichiometric counterparts.<sup>104</sup> The carrier concentration of the b-TiO<sub>2</sub> NTAs determined from the capacitance measurement (*i.e.* Mott-Schottky plot) is higher than the c-TiO<sub>2</sub> NTAs by 5 orders-of-magnitude, indicating that the b-TiO<sub>2</sub> is a degenerated semiconductor with high conductivity (**Figure 37**). Also, its value is well consistent in the literature.<sup>123</sup> Although nanostructures exaggerate donor density because of its high electrochemical surface area,<sup>101</sup> in case which has similar nanostructures, it is possible to compare the relative amounts. As shown in **Figure 37**, the slopes of the graph are positive, indicating that annealed TiO<sub>2</sub> NTAs are n-type semiconductors. This result matches well compared to other literature.<sup>124</sup> In case of b-TiO<sub>2</sub>, the charge density was drastically increased compared with c-TiO<sub>2</sub>. This may be explained the non-stoichiometry nature of as-grown TiO<sub>2</sub> NTAs. As previous paper demonstrated<sup>125</sup>, the as-grown TiO<sub>2</sub> NTAs have high number of defects, therefore after Ar-annealed, the defective nature is preserved. This may be attributed to high donor density of b-TiO<sub>2</sub>.

**Figure 38** compares the HER and CER activities of c-TiO<sub>2</sub> NTAs and b-TiO<sub>2</sub> NTAs in the presence of the RuO<sub>2</sub> catalyst. As can be expected from the CV curves, both of them show reasonable HER activity. Interestingly, the RuO<sub>2</sub>-loaded b-TiO<sub>2</sub> NTAs exhibit a good CER activity if the amount of the catalyst is good enough (*i.e.* 50000 cycles). The overpotentials of the current density 10 mA/cm<sup>2</sup> and 100 mA/cm<sup>2</sup> are 130mV and 425mV, respectively, which is comparable to the reported values of RuO<sub>2</sub>-based CER catalysts (**Table 5, Figure 39**). Therefore, it can be concluded that the b-TiO<sub>2</sub> NTAs are

very promising scaffold and supporting electrode for loading electrocatalysts especially working under universal potentials like CER and HER. (summarized in **Table 6**)



**Figure 35. Monitoring CER activity of a) a-TiO<sub>2</sub>@RuO<sub>2</sub> NTAs b) c-TiO<sub>2</sub>@RuO<sub>2</sub> NTAs and HER activity of c) c-TiO<sub>2</sub>@RuO<sub>2</sub> NTAs (insets: electrochemical surface area measurement)**



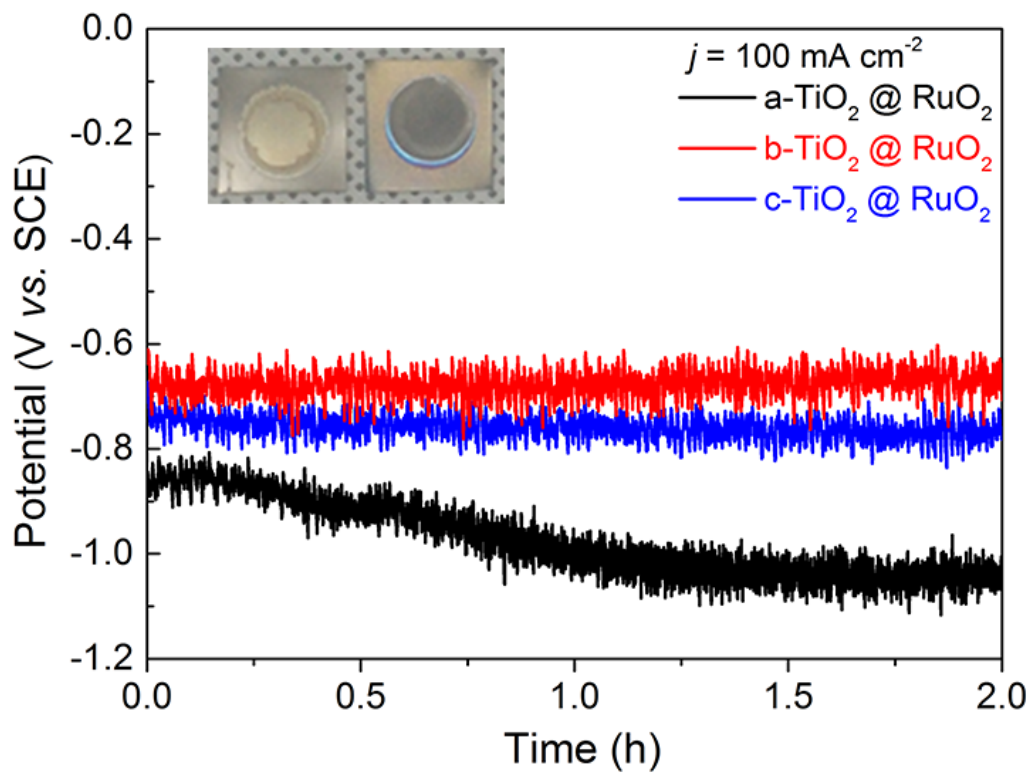


Figure 36. stability test comparison between two samples and their optical images.

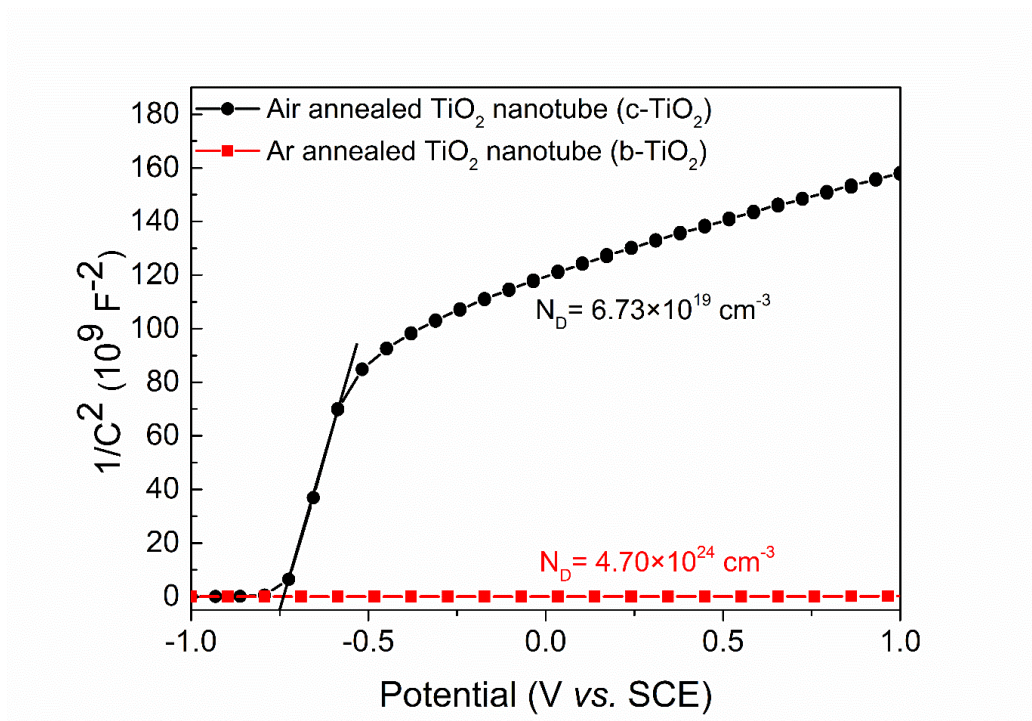
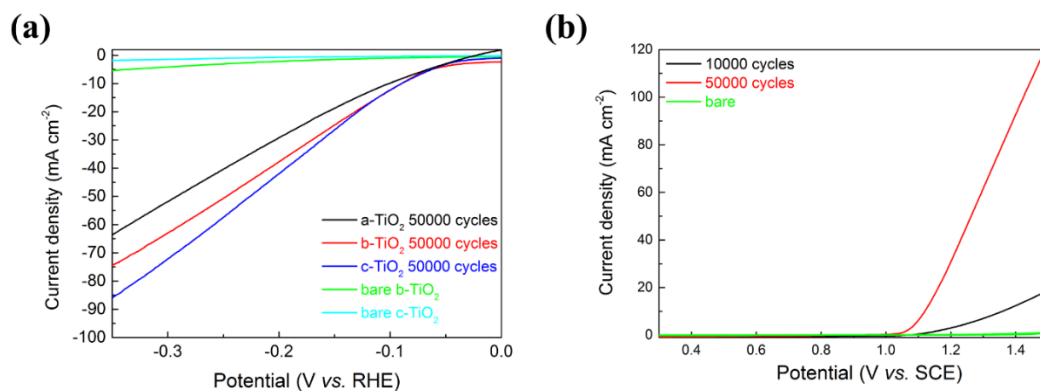


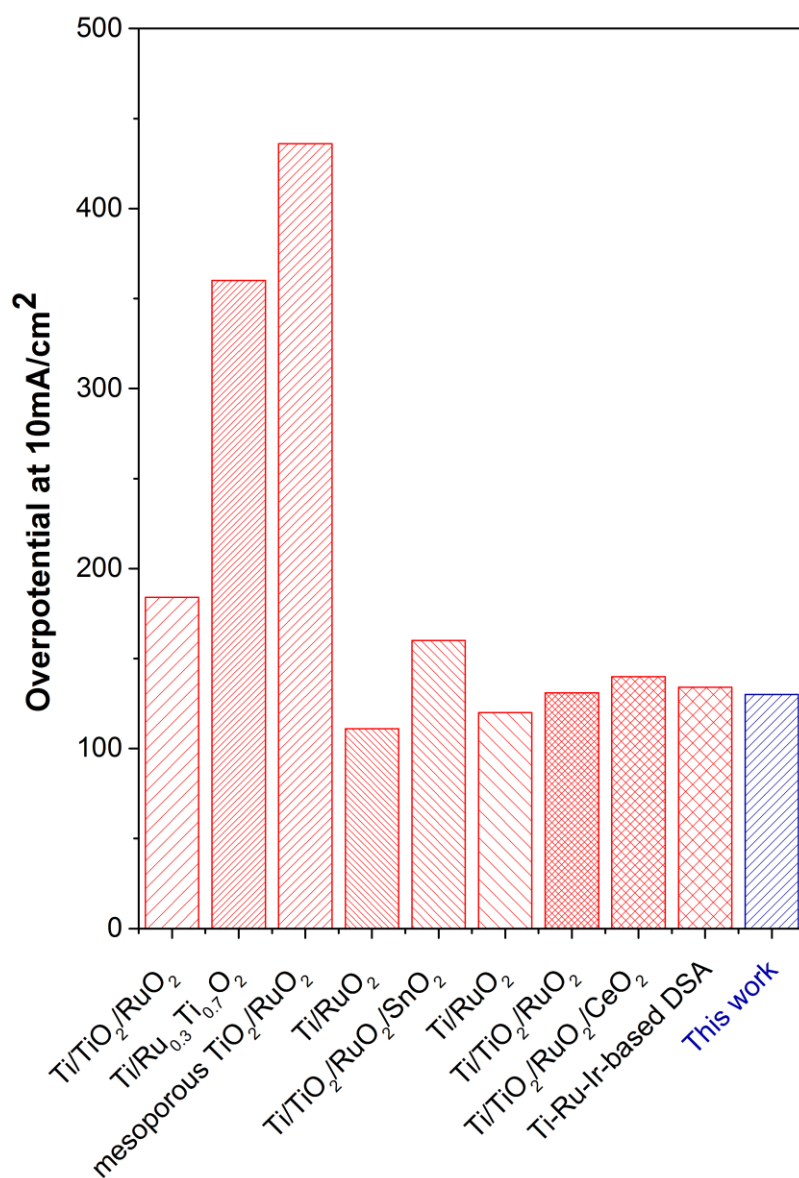
Figure 37. Mott-Schottky plot at a fixed frequency of 1kHz on annealed TiO<sub>2</sub> NTAs.



**Figure 38. LSV scan of b-TiO<sub>2</sub>@RuO<sub>2</sub> NTAs in a) 0.5M H<sub>2</sub>SO<sub>4</sub> with scan rate 10mV/s.  
b) 5M NaCl (pH=2) with scan rate 10mV/s**

material	$\eta_{10\text{mA}/\text{cm}^2}$	$\eta_{100\text{mA}/\text{cm}^2}$	synthesis condition	evaluation condition	ref
Ti/RuO <sub>2</sub>	-	447mV	thermal decomposition	5M NaCl, pH=2, RT	126
macroporous TiO <sub>2</sub> /RuO <sub>2</sub>	-	270mV	thermal decomposition method with several sizes of PS microspheres	5M NaCl, pH=2, RT	127
Ti/TiO <sub>2</sub> /RuO <sub>2</sub>	184mV	-	spray pyrolysis	5M NaCl, pH=2, RT	128
Ti/Ru <sub>0.3</sub> Ti <sub>0.7</sub> O <sub>2</sub>	360mV	-	-	3.5g/L NaCl	129
mesoporous TiO <sub>2</sub> /RuO <sub>2</sub>	436mV	676mV	pore templating with micelles of amphiphilic block-copolymers	4M NaCl, pH=3, 40 °C	130
Ti/RuO <sub>2</sub>	111mV	-	thermal decomposition	5M NaCl, 30 °C	131
Ti/TiO <sub>2</sub> /RuO <sub>2</sub> /SnO <sub>2</sub>	160mV	-	painting/baking	5M NaCl, 20 °C	132
Ti/RuO <sub>2</sub>	120mV	-	sol-gel	5M NaCl, pH=2, RT	133
Ti/TiO <sub>2</sub> /RuO <sub>2</sub>	131mV	-	sol-gel	5M NaCl, pH=2, RT	134
Ti/TiO <sub>2</sub> /RuO <sub>2</sub> /CeO <sub>2</sub>	140mV	-	thermal decomposition	5M NaCl, pH=2, RT	135
Ti–Ru–Ir-based dimensionally stable anode	134mV	453mV	purchased by Bayer Materials, Leverkusen, Germany	4M NaCl, pH=2, RT	136
Ti/TiO <sub>2</sub> NTAs/RuO <sub>2</sub>	130mV	425mV	electrochemical process	5M NaCl, pH=2, RT	This work

**Table 5. Compilation of CER performance metrics for Ru-based catalyst synthesized under different condition.**



**Figure 39. Comparison of CER overpotential at 10mA cm<sup>-2</sup> with other Ru-based electrocatalyst reported in the literature.**

material	CER		HER	
	performance	stability	performance	stability
a-TiO <sub>2</sub> @RuO <sub>2</sub>	O	O	O	X
b-TiO <sub>2</sub> @RuO <sub>2</sub>	O	O	O	O
c-TiO <sub>2</sub> @RuO <sub>2</sub>	X	-	O	O

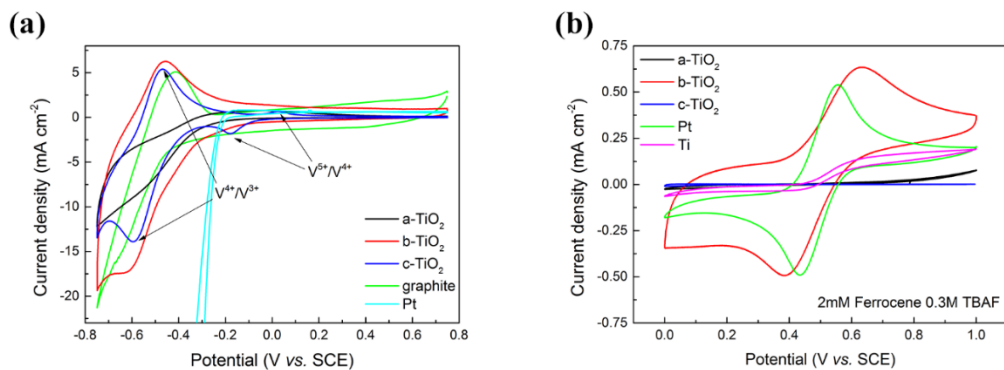
**Table 6. Summary of catalytic activity and stability of each TiO<sub>2</sub> NTAs@RuO<sub>2</sub> electrodes**

### 3.3.2.2 Evaluation of conductivity under different bias

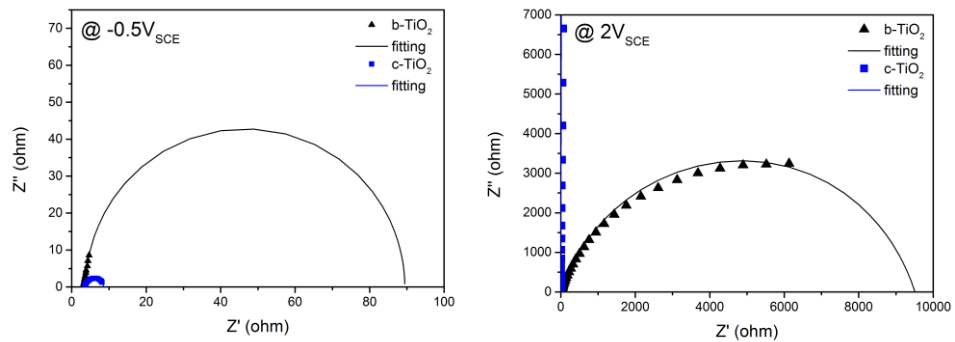
In order to investigate the more about the conductivity of the supporting electrode, cyclic voltammograms (CV) of the various supporting electrodes without RuO<sub>2</sub> using two different redox couples (**Figure 40**) were measured. Ferrocene and vanadium solutions were chosen for investigating CER (*i.e.* anodic potential) and HER (*i.e.* cathodic potential), respectively. As can be seen from Fig. 4a, all of the TiO<sub>2</sub> NTAs show clear V<sup>3+</sup>/V<sup>2+</sup> redox peaks with high current density regardless of the annealing condition, indicating that the electrical conductivity under cathodic potentials is good enough. This result is consistent with the observation that all samples show reasonable HER activity. On the other hand, the c-TiO<sub>2</sub> NTAs essentially no current under anodic potentials, indicating that the electrical conductivity is very poor. This result can explain why the RuO<sub>2</sub>-loaded c-TiO<sub>2</sub> NTAs do not exhibit CER activity at all. It should be noted that the b-TiO<sub>2</sub> NTAs exhibit much larger current density and clear redox peaks, which must be very promising for CER. Such a different potential-dependence of the electrical conductivity between c-TiO<sub>2</sub> and b-TiO<sub>2</sub> can also be observed from the electrochemical impedance spectroscopy (EIS) shown in **Figure 41**. Furthermore, based on the obtained spectrum, equivalent circuit was constructed and fitting was performed, and electrochemical parameters were derived based on the circuit. The model we used is in **Figure 21b**, and recently other researchers fitted the impedance spectrum in a basic environment.<sup>137</sup> The shape and pattern of the spectrum were similar to those of this study, and similar values were obtained. As can be seen in **Table 7**, the resistance between the

barrier and the electrolyte is significantly reduced under the anodic region when the heat treatment is carried out in argon. On the other hand, under cathodic region, the resistance between the barrier and the electrolyte is similar, or the b-TiO<sub>2</sub> NTAs are slightly worse, which can be related to the slightly improved hydrogen evolution reaction activity of c-TiO<sub>2</sub> NTAs as shown in **Figure 38a**. The fact that the TiO<sub>2</sub> NTA has a large change in conductivity under anodic/cathodic voltage has been extensively investigated in other studies,<sup>118</sup> and representative results are attached to the **Figure 42**.

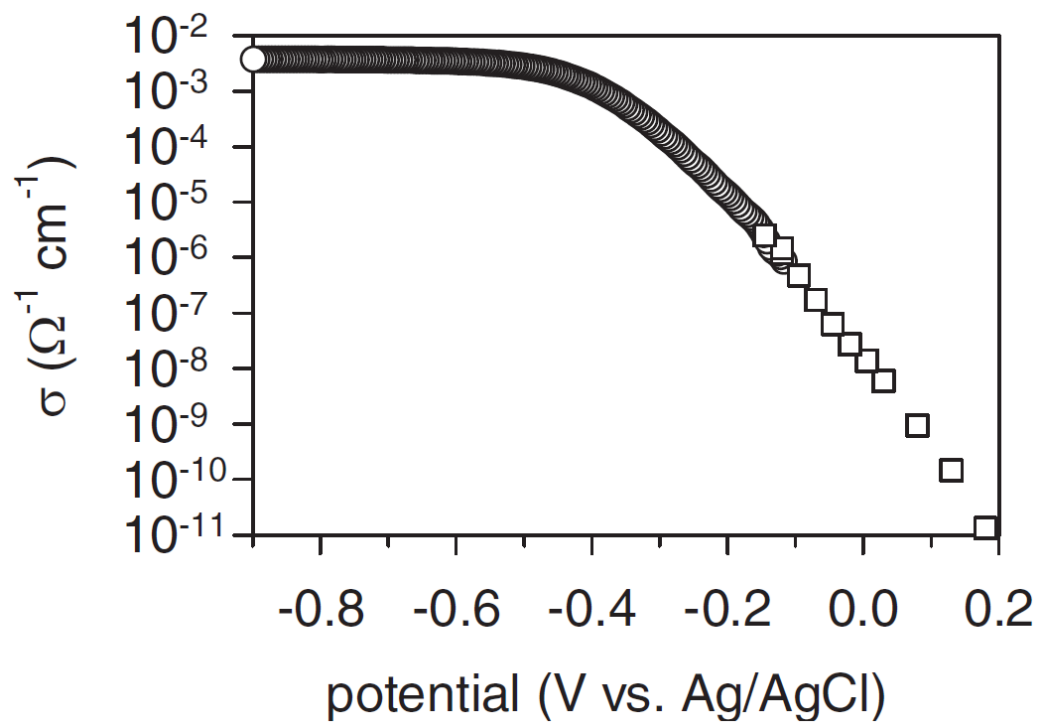




**Figure 40. (a) CV scan of each TiO<sub>2</sub> substrate, Pt and graphite (electrolyte: 0.1M VOSO<sub>4</sub> supported by 3M H<sub>2</sub>SO<sub>4</sub>) (b) CV scan of each TiO<sub>2</sub> substrate, Pt and Ti (electrolyte: 2mM Ferrocene supported by TBAF)**



**Figure 41. Electrochemical impedance spectroscopy. (a) Nyquist plot at  $-0.5V$  (vs. SCE) (b) Nyquist plots of the impedance data for c-TiO<sub>2</sub> and b-TiO<sub>2</sub> at  $2V$  (vs. SCE)**



**Figure 42. Electronic conductivity of TiO<sub>2</sub> NTAs obtained from EIS data under different bias (pH=2) [118]**

Materials	applied voltage (V)	C <sub>b</sub> (μF)	R <sub>b</sub> (ohm)	C <sub>i</sub> (μF)	R <sub>i</sub> (ohm)
	2V	97.214	<b>8921</b>	1574.3	<b>584.1</b>
b-TiO <sub>2</sub>	OCV (0.37V)	674	9983	195.8	40919
	-0.5V	14267	11.7	5294.3	74.53
	2V	3.0646	4651000	0.17936	7570100
c-TiO <sub>2</sub>	OCV (0.29V)	234.02	14863	36.554	196030
	-0.5V	6820.5	<b>2.487</b>	8276.2	<b>2.53</b>

**Table 7. Electrochemical parameters of TiO<sub>2</sub> NTAs electrode obtained by EIS.**

## 4. Conclusions

The electro-catalytic performance of  $\text{TiO}_2$  NTAs@ $\text{RuO}_2$  for chlorine evolution was investigated.  $\text{RuO}_2$  nanoparticle was successfully deposited onto  $\text{TiO}_2$  NTAs by pulse electrodeposition. By varying the annealing condition of  $\text{TiO}_2$  NTAs, electrochemical properties of  $\text{TiO}_2$  NTAs were changed, affecting the catalytic properties. Because of inferior charge transfer property under anodic condition, c- $\text{TiO}_2$ @ $\text{RuO}_2$  electrode shows poor CER performance. On the other hand, Ar annealed b- $\text{TiO}_2$ @ $\text{RuO}_2$  electrode shows high performance in both HER and CER. This is ascribed to the decrease of charge transfer resistance. In order to make  $\text{TiO}_2$  NTAs as good support material for universal potential, the use of Ar-annealed black  $\text{TiO}_2$  is necessary.

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## Abstract in Korean

### 국 문 초 록

이산화 루테늄 ( $\text{RuO}_2$ )은 탈수소화 반응, 염산의 산화반응 및 클로로 알칼리(chlor-alkali) 공정과 같은 다양한 화학 반응에 널리 쓰이고 있다. 일반적으로, 이산화 루테늄계 촉매의 안정성을 향상시키기 위해, 이산화 티타늄( $\text{TiO}_2$ )을 사용한다. 특히, 나노 구조는 촉매 활성 부위를 늘린다는 점에서 촉매 반응을 향상시키는데 많이 사용되었다. 그러나 전기 촉매 반응의 경우, 촉매를 담지 하는 담지체가 충분히 전도성이 있어서 산화 환원 반응에 필요한 전하를 전달할 수 있어야 한다. 이런 이유 때문에  $\text{TiO}_2$  나노 튜브 격자(NTAs)는 전하를 수송 할 수 있는 능력(태양 전지 또는 광 전기화학 반응에서 입증됨.),  $\text{RuO}_2$  와의 높은 친화성 (치수 안정성 전극에의 응용) 때문에 염소발생반응을 위한 좋은 담지체로 사용될 수 있다. 또한, 나노 튜브 격자는 전기 산화 방법을 이용해 나노 구조를 정밀하게 조절할 수 있으며, 결정성이나 배향, 전기적 특성들을 제어할 수 있다.

이에, 본 연구에서는 최초로 이산화 루테늄을 증착한 이산화 티타늄 나노 튜브 격자를 염소발생반응을 위한 전극으로 제안한다. 나노 튜브 격자는 전기화학적 양극산화방법으로 만들었으며, 열처리 조건에 따른

결정성 및 전기전도도와와의 관계를 탐구하였다. 양극 분극 하의 전극의 전도성은 효율적인 염소 발생을 위해 필수적이며, 결합 조절을 통해 양극 분극 하에서의 전도성을 확보하였다. 특히, 아르곤 분위기 하에서 열처리된 나노 튜브 격자를 제조함으로써 흑색 나노 튜브 격자를 제작할 수 있었다. 또한, 이 담지체는 다양한 pH, 넓은 범위의 전압에서 안정적으로 촉매 특성을 낼 수 있는 가장 좋은 전극인 것을 확인하였다.

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주요어 : 염소발생반응(CER), 이산화티타늄 나노튜브 어레이, 이산화 루테튬, 불균일계 촉매, 전기화학적 분석  
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