

NIH Public Access

Author Manuscript

Ultrasound Med Biol. Author manuscript; available in PMC 2012 November 01.

Published in final edited form as:

Ultrasound Med Biol. 2011 November ; 37(11): 1952–1957. doi:10.1016/j.ultrasmedbio.2011.08.012.

Precision Manufacture of Phase-Change Perfluorocarbon Droplets using Microfluidics

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Abstract

Liquid perfluorocarbon droplets have been of interest in the medical acoustics community for use as acoustically activated particles for tissue occlusion, imaging, and therapeutics. To date, methods to produce liquid perfluorocarbon droplets typically result in a polydisperse size distribution. Since the threshold of acoustic activation is a function of diameter, there would be benefit from a monodisperse population to preserve uniformity in acoustic activation parameters. Through the use of a microfluidic device with flow focusing technology, the production of droplets of perfluoropentane with a uniform size distribution is demonstrated. Stability studies indicate that these droplets are stable in storage for at least two weeks. Acoustic studies illustrate the thresholds of vaporization as a function of droplet diameter, and a logarithmic relationship is observed between acoustic pressure and vaporization threshold within the size ranges studied. Droplets of uniform size have very little variability in acoustic vaporization threshold. Results indicate that microfluidic technology can enable greater manufacturing control of phase change perfluorocarbons for acoustic droplet vaporization applications.

Keywords

acoustic droplet vaporization; ultrasound; monodisperse; perfluoropentane; microfluidic

Introduction

Acoustic Droplet Vaporization Agents

In acoustic droplet vaporization (ADV), acoustic pressure delivered to a liquid droplet by an ultrasound (US) transducer provides the additional energy necessary to induce a liquid-to-gas phase transition. This phase transition allows for unique applications that are not possible with standard microbubble contrast agents, since ADV agents exhibit a very large

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volume change after activation. Additionally, ADV agents are typically poorly echogenic in their liquid form, but highly echogenic as gas bubbles.

The basic construction of an ADV agent consists of a volatile liquid core that can be converted to a gas with additional energy. Typically, ADV droplets consist of perfluorocarbons (PFC) such as perfluoropentane (PFP)(Zhang et al. 2010), perfluorohexane (PFH)(Giesecke and Hynynen 2003, Fabiilli et al. 2010), or perfluorocatae (Fabiilli *et al.* 2009). The most commonly employed perfluorocarbons, PFP and PFH, have boiling points near physiological temperatures (29 °C and 56 °C, respectively). Recently, stabilization and ADV capability of droplets of liquid perfluorobutane (boiling point of -1.7 °C) has been demonstrated (Sheeran et al. 2011).

Producing droplets in the micron and sub-micron range increases the Laplace pressure exerted on the liquid core, enabling small droplets to be maintained in liquid form even above their vaporization temperature. The addition of a stabilizing shell reduces droplet coalescence and increases stability of the emulsions. (Kripfgans *et al.* 2005, Rapoport *et al.* 2009a, Sheeran et al. 2011) Commonly utilized methods of producing PFC droplets include sonication or high-speed mechanical agitation of the host solution, which typically results in a polydisperse population (Fabiilli et al. 2010, Rapoport et al. 2010).

Acoustic Droplet Vaporization Applications

Liquid perfluorocarbon droplets have been shown to provide ultrasound image contrast (Kripfgans et al. 2002, Marsh *et al.* 2007), although the backscatter is notably less than similarly sized microbubble agents. One of the first commercial applications of perfluorocarbon droplets for ultrasound contrast enhancement was Echogen (Sonus Pharmaceuticals), a perfluoropentane emulsion (Quay 1996). Clinical trials for Echogen were abandoned in 2000 prior to FDA approval.

Once vaporized, ADV agents are readily detectable by an imaging system even at low concentrations. In very small amounts, droplets when converted to bubbles through ADV could act as point beacons for phase aberration corrections (Apfel 1998, Haworth *et al.* 2008). The unique advantages of ADV droplets in the hundred nanometer size range is that they have the potential to extravasate from the vasculature and into the tissue, enabling ADV based contrast imaging or therapy to extend beyond the vascular space, where traditional microbubbles cannot access (Rapoport *et al.* 2007, Rapoport et al. 2009b, Sheeran et al. 2011.).

One of the most well studied applications of ADV is embolotherapy. This technique enables the intentional creation of an occlusion in a specific tissue to limit blood flow. This has been proposed to treat renal cell carcinoma, to reduce blood loss for hypervascular tumors, and to treat hemhorrhage (Kripfgans *et al.* 2002, Zhang et al. 2010). Kripfgans *et al.* (2005) demonstrated that a filtered emulsion of droplets which is intra-arterially injected can reduce kidney perfusion by 70 %. This level of organ perfusion reduction has the ability to cause ischemic necrosis for therapeutic applications, or can enhance the utility of radiofrequency tissue ablation by minimizing thermally dissipative effects due to reduced flow (Kripfgans *et al.* 2005). A second application of ADV agents is site-specific therapeutics, where the goal is to deliver a potent agent only to the disease site while minimizing systemic effects. The ADV-mediated delivery of a chemotherapeutic drug directly to the tumor has been shown to mediate regression of ovarian and breast cancer (Rapoport *et al.* 2009a). ADV agents that have the ability to carry a therapeutic payload to a desired vessel could be combined with vessel occlusion upon activation to allow for an increase in residence time of the therapeutic agent (Fabiilli *et al.* 2010).

With spatial and temporal control over ADV agent activation, ADV agents can be used as a nucleation site for high-intensity focused ultrasound (HIFU) tumor ablation. During HIFU, the microdroplets can be activated to increase the therapeutic effect or decrease the treatment time (Zhang and Porter 2010, Zhang *et al.* 2011).

Considerations of ADV agent size distribution

The size of ADV agents is an important factor in determining the vaporization threshold and the biodistribution. The Antoine equation predicts a negative logarithmic relation between droplet size and activation energy, where larger droplets require less energy to vaporize than smaller droplets (Rapoport *et al.* 2009b). Most who have characterized ADV-based agents have evaluated a polydisperse droplet population. While general trends in thresholds have been observed, polydispersity in droplet sizes has led to a variability in the vaporization threshold measured for studies that examine a bulk population of ADV droplets. Additionally, the larger droplets vaporize at lower energies and the resulting bubbles can influence the threshold energy for the smaller droplets (Lo *et al.* 2007), confounding in-vitro characterization of vaporization thresholds. Since microbubbles combined with high acoustic pressures can lead to unwanted bioeffects (Miller *et al.* 2008), it may be desirable to perform ADV at the minimum acoustic pressure required. A polydisperse sample may require a higher pressure to efficiently vaporize the entire population due to smaller droplets requiring more energy.

For micron-sized ADV agents, one of the primary applications is vessel occlusion, where it may be important to have a well characterized distribution of droplet sizes to target a specific vascular diameter while not affecting other vessels (Kripfgans et al. 2005). For the same reasons, a droplet designed for imaging applications that is too large could lodge in the lungs or other organs after IV injection, leading to undesired vessel occlusion. All of these limitations are motivating reasons for precise size control of ADV agents.

Previous studies to improve the size distribution characteristics of perfluorocarbon droplets have involved microfluidic sorting (Huh et al. 2007) and filtering (Kripfgans *et al.* 2005). The microfluidics platform is well known for the ability to create particles (Xu et al, 2005), droplets (Tan *et al.* 2004, Xu *et al.* 2006, Teh *et al.* 2008), microbubbles (Hettiarachchi *et al.* 2007), and multi-layer/multi component compositions (Hettiarachchi *et al.* 2009, Wang *et al.* 2011) of uniform size. In this manuscript, we assess the feasibility for producing a monodispersed ADV agent through a microfluidic technique, in order to achieve uniform activation thresholds.

Materials and Methods

Reagent Preparation

Liquid Perfluoropentane was purchased from FluoroMed, L.P. (Round Rock, Texas). Lipid solutions were created using a 9:1 molar ratio of 1,2-distearoyl-sn-glycero-3-phosphocholine (DSPC) (Avanti Polar Lipids, Alabaster, AL) and 1,2-distearoyl-sn-glycero-3-phosphoethanolamine-N[methoxy-(polyethylene glycol)-2000] (DSPE-PEG2000) (Avanti Polar Lipids, Alabaster, AL) in a 110 mL solution of deionized water (DI), glycerol (Fisher Scientific, Pittsburgh, PA), propylene glycol (Fisher Scientific, Pittsburgh, PA), and pluronic F-68 (Sigma-Aldrich Corporation, St. Louis, MO).

50 mg of DPSC and 19.6 mg DSPE-PEG2000 were dissolved in chloroform. The chloroform was then evaporated with N_2 , after which 50 mL of DI was added and the resulting solution was sonicated for 20 minutes. After sonication, 47 mL DI, 2 mL glycerol,

1 mL propylene glycol, and 10 mL pluronic F-68 were added. The solution was vortex mixed for 1 minute and then sonicated for 10 minutes.

Microfluidic Device Fabrication

The process for developing the microfluidic wafer has been previously described by Hettiarachchi *el al.* (2009). Briefly, the channels were created using Illustrator (Adobe, San Jose, CA) and printed (20,000 dpi) by CAD/Art Services (Brandon, OR). In a clean room, the wafer was first oxidized in oxygen plasma then spin-coated with a UV curable epoxy (SU-8-25, MicroChem, Newton, MA). On exposing the wafer to UV light, the channel patterns develop to use as a negative for device production.

With the wafer in a petri dish, Polydimethylsiloxane (PDMS) (Dow Corning, Midland, MI) and a curing agent were poured over the wafer at a 10:1 ratio, respectively. This was then placed under vacuum for 24 hours and then cured at 60°C overnight. After the PDMS was cured, the individual microfluidic devices were removed from the wafer. The individual microfluidic device and a clean microscope slide (2947-75×25, Corning, Corning, NY) were placed in a plasma cleaner (Harrick Plasma, Ithaca, NY) and exposed to a plasma field under a controlled pressure of 500 millitorr for 3 minutes. On completion of the plasma cleaning process, the PDMS and glass slide were immediately joined, forming complete microchannels. One minute after the bond was established, DI water was injected into the channels to create a hydrophilic environment.

Microfluidic Experimental Apparatus

The microfluidic experimental apparatus was set up similar to that as described previously by Kaya *et al.* (2010). Briefly, the microfluidic device was secured to a moving stand on an inverted microscope (Olympus 1×71 microscope, Center Valley, PA), and viewed with a $50 \times NA = 0.5$ objective. A high speed camera (Fastcam APX-RS, Photron, Inc., San Diego, CA) was used to capture images and videos of the device output. Reagents were injected from syringes into device channels through Tygon S-54-HL tubing (Saint-Gobain Performance Plastics, Akron, OH). Calibrated syringe pumps (Harvard Apparatus, Holliston, MA) were used to control rate of material flow in individual microchannels.

Sample Production

To produce uniform samples, the PFP flow rate was fixed at a constant value and the lipid flow rate was increased until the smallest stable droplets were formed. The system was allowed to stabilize for 5 minutes before collection, since pressure changes in the system required a few minutes to equalize. This process was repeated across a range of different flow rates, as described in Table 1. In order to determine the production rate for the microfluidic device, high-speed video analysis of the droplet production was performed. Time stamps enabled the determination of droplet production rate.

Acoustic Experimental Apparatus

The experimental setup to determine droplet vaporization thresholds was similar to that previously described by (Sheeran *et al.* 2011). Briefly, a heated water bath maintained at 37° C was connected to an inverted microscope. Droplets were injected through a nearly acoustically and optically transparent microcellulose capillary tube with an inner diameter of 200 µm (Spectrum Labs, Inc., Greensboro, NC). A 5 MHz piston transducer (IL0506HP, Valpey Fisher Corp., Hopkinton, MA) was positioned in the water bath confocally with a water immersion microscope objective (100×, NA=1.0). The output of the ultrasound transducer was calibrated by inserting a needle-hydrophone (HNA-0400, Onda Corp., Sunnyvale, CA) into the experimental system at the exact location where the samples are

positioned during activation studies (the focus of the microscope objective). Droplets were exposed to single 10-cycle sinusoidal pulses, while the ultrasound pressure was increased incrementally until droplet vaporization was observed. The procedure was repeated for at least 20 droplets from each size distribution to verify droplet size and threshold.

Stability Analysis

Droplets were stored at 4°C in 3mL vials until sampling. For analysis, a 25 microliter aliquot of droplets was placed on a glass slide, and images were captured with the Photron Fastcam camera. Size measurements were performed in Image J (NIH, Bethesda, MD) by comparison to a calibrated reticle (Edmund Industrial Optics, Barrington, NJ). A minimum of 50 droplets were measured for each population.

Results

The dimensions of the microfluidic device, material composition, and flow rates all have the ability to alter the composition of the resulting droplet. Due to the microfabrication process, there are small variations from device to device (we measured a 13% deviation in orifice widths across 10 devices). With this in mind, only one device was used for the duration of production to ensure that the dimensions of the device were unchanged. The material compositions also went unchanged to ensure that the droplets would experience a standardized reaction to the US pressure.

Precision Size Control

The flow rates were varied over five sets of conditions for the duration of the experiment to alter the droplet diameter. Results illustrated that by varying flow rates, the PFP population diameters could be carefully selected. In general, as the lipid flow rate was increased, droplet size decreased (Figure 1). As the PFP flow rate was increased, droplet size increased. Table 1 lists the flow rates, mean droplet size, standard deviation, and polydispersity index (Xu *et al.* 2006).

For the populations studied, the standard deviation was largest for the smallest droplets (SD=0.4 for the 7.4 micron population) and smallest for the largest droplets (0.3 for the 20.4 micron population). All populations had a polydispersity index of 5.1 or less.

Production Rate

The 20- μ L/min lipid and the 12.5 μ L/min PFP flow rates, which resulted in 20.4 micron droplets, had a production rate of 1.85×10^4 droplets produced per second (slowest production sample); whereas the 60 μ L/min lipid and 13.9 μ L/min PFP flows, which produced 7.4 micron droplets, had a production rate of 1.65×10^5 droplets per second (fastest production sample). Table 2 lists the production rates for the 5 samples.

Acoustic Responses

The five samples were diluted and injected into a cellulose microcapillary tube where droplets from each population were individually subjected to US. The US data showed that there was a distinct vaporization threshold pressure for each diameter (Figure 2). The data trend suggests a logarithmic relationship ($P = -1.80\ln(D) + 7.72$, $R^2 = 0.97$), as predicted by the Antoine equation.

Long-tem stability

Populations maintained a fairly low polydispersity over a two week time period (Table 1), and overall, the mean diameters of the populations drifted less than 4.6% (Figure 3). The

16.2 and 10.3 μ m mean diameter populations each maintained the same polydispersity, and the 20.4, 12.6, and 7.4 μ m mean diameter populations changed by a factor of 1.8, 1.3, and 1.9, respectively.

Discussion

The method described here demonstrates the potential of production of uniform-sized droplets for acoustic droplet vaporization utilizing microfluidics. Data illustrates that this technique enabled production of a population of droplets where each droplet responded similarly to the same acoustic parameters due to uniform size. One advantage of utilizing such uniform droplets would include the ability to use the lowest acoustic pressure possible for vaporization (since all droplets would respond similarly), thereby achieving the highest vaporization efficiency for the lowest acoustic pressure. Keeping the acoustic pressure as low as required would conform to the "As Low As Reasonably Achievable (ALARA) Principle" for clinical ultrasonics. Other potential advantages of uniform sized ADV agent production, although not demonstrated here, would be the ability to tailor droplet sizes for specific vessel occlusion, or to enable precision drug-loading for therapeutic-carrying ADV agents.

Microfluidic techniques have previously demonstrated unique utility in the controlled fabrication of droplets and microbubbles. The biggest limitation to this method to date is that the production rate is substantially slower than other droplet and microbubble production methods. Even for the fastest production method here, it would require nearly 3 hours to achieve 1×10^9 droplets (a similar order of magnitude to the concentration of microbubble contrast agents prepared by a mechanical agitation method). However, in the future microfluidic techniques may be scaled up to achieve higher throughput, although the need to maintain identical dimensions and flow rates to each orifice in order to preserve size uniformity presents a challenge. It should also be noted that although the smallest droplets described here were approximately 7 microns, which is likely too large for *in-vivo* application, this size was limited only by our particular system, and is not a fundamental limit of microfluidic droplet production. It is very reasonable to anticipate that by optimizing the channel dimensions, component flow rates, and the lipid/perfluorocarbon ratios, droplets much smaller than 7 microns can be prepared. Prior studies have illustrated microfluidic production of liquid droplets as small as 100 nanometers (Tan and Lee, 2005).

Conclusion

A microfluidic device can produce monodisperse PFP/lipid droplets using flow focusing technology. Monodisperse PFP/lipid droplets that were subjected to US pressure waves showed a uniform ADV response. The relationship formed by droplet diameter and ADV threshold agreed with the expected negative logarithmic response based on the size of the droplets. Droplet populations produced with microfluidics were stable within the two week time period studied.

Acknowledgments

The authors would like to thank Jason Streeter for the preparation of the lipid solution and Roger Shih for the microfluidic wafer fabrication. Also, the authors appreciate the assistance from Dennis Given and Roshni Kothadia for their work in droplet characterization and data organization. This project was supported by R01EB008733 and R21EB011704.

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Figure 1.

High speed video frames of microfluidic droplet production at diameters of (A) 20.4 \pm 0.3 µm, (B) 16.2 \pm 0.5 µm, (C) 12.6 \pm 0.5 µm, (D) 10.3 \pm 0.4 µm, and (E) 7.4 \pm 0.4 µm, corresponding to lipid and PFP flow rates of lipid 40 µL/min; PFP 12.5 µL/min, lipid 31 µL/min; PFP 15 µL/min, lipid 40 µL/min; PFP 15 µL/min, lipid 50 µL/min; PFP 15 µL/min, and lipid 60 µL/min; PFP 13.9 µL/min, respectively.

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Figure 2.

Average pressure of vaporization vs. average droplet diameter. Error bars indicate standard deviations in pressure and diameter. The trendline is logarithmic.



Figure 3.

Microscopy images of droplets 1 week apart illustrating size stability. (A-E) 1 week after production - populations of mean diameter of (A) $20.4\pm0.3 \,\mu$ m, (B) $16.2\pm0.5 \,\mu$ m, (C) $12.6\pm0.5 \,\mu$ m, (D) $10.3\pm0.4 \,\mu$ m, and (E) $7.4\pm0.4 \,\mu$ m. (F-J) 2 weeks after production - populations corresponding to (A-E), respectively, with mean diameters of (F) $20.4\pm0.5 \,\mu$ m, (G) $15.5\pm0.5 \,\mu$ m, (H) $12.2\pm0.4 \,\mu$ m, (I) $10.8\pm0.4 \,\mu$ m, and (J) $7.5\pm0.7 \,\mu$ m.

Table 1

Polydispersity data for the five studied droplet populations from the day the droplets were created, three days, one week, and two weeks.

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		Creation Dat	а	
Lipid (µL/min)	PFP (µL/min)	Average (µm)	Standard Deviation	Polydispersity
20	12.5	20.4	0.3	1.5
31	15	16.2	0.5	3.4
40	15	12.6	0.5	3.9
50	15	10.3	0.4	3.5
60	13.9	7.4	0.4	5.1
		3 Day Data		
20	12.5	20.6	0.5	2.6
31	15	16.2	0.4	2.6
40	15	12.6	0.4	3.4
50	15	10.5	0.4	3.9
60	13.9	7.5	0.5	6.2
		1 Week Data		
20	12.5	20.4	0.5	2.6
31	15	15.5	0.4	2.8
40	15	12.6	0.4	3.1
50	15	10.7	0.4	3.4
60	13.9	7.5	0.4	4.7
		2 Week Data		
20	12.5	20.4	0.5	2.7
31	15	15.5	0.5	3.4
40	15	12.2	0.4	3.2
50	15	10.8	0.4	3.5
60	13.9	7.5	0.7	9.0

Table 2

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Production rates for droplets produced with microfluidics under varying input flow conditions.

in) Production Rate (droplets/s)	1.85×10^4	3.31×10^{4}	6.44×10^{4}	1.03×10^{5}	1.65×10 ⁵
PFP (µL/m	12.5	15	15	15	13.9
Lipid (µL/min)	20	31	40	50	60