



Finite Heterogeneous Rate Constants for the Electrochemical Oxidation of VO^{2+} at Glassy Carbon Electrodes

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The electrochemical oxidation of VO^{2+} at planar glassy carbon electrodes is investigated via stationary and rotating linear sweep voltammetry as well as via chronoamperometry. It is demonstrated that introducing finite kinetic rate constants into the Butler-Volmer equation captures the experimentally observed concentration dependence of the ordinate intercept in Koutecký-Levich plots that cannot be explained by using the classical model. This new concept leads to a three-term Koutecký-Levich equation considering mass transport limitations, Butler-Volmer kinetics, as well as finite heterogeneous kinetics simultaneously. Based on these findings it is pointed out that stationary linear sweep voltammetry followed by an irreversible Randles-Ševčík analysis is not sufficient for deducing the electrode kinetics of the VO^{2+} -oxidation. In contrast, it is verified experimentally and theoretically that a Tafel analysis will still provide reasonable values of $k^0 = 1.35 \cdot 10^{-5}$ cm/s and $\alpha = 0.38$, respectively. Finally, it is shown that introducing the concept of finite heterogeneous kinetics into the theory of stationary linear sweep voltammetry also explains the failure of the irreversible Randles-Ševčík relation leading to an extension of the classical model and providing insight into the electrochemical oxidation reaction of VO^{2+} .

Keywords: vanadium redox-flow batteries, rotating disc electrode, linear sweep voltammetry, Koutecký-Levich analysis, Tafel analysis

1. INTRODUCTION

In vanadium redox flow battery (VRFB) research, stationary¹ linear sweep voltammetry (S-LSV) and stationary cyclic voltammetry (S-CV) are the most prevalent techniques used for the fast assessment of the kinetic performance of surface-modified carbon felt electrodes, and numerous studies have been published on that topic (Flox et al., 2013a,b; Gao et al., 2013; Hammer et al., 2014; Suárez et al., 2014; Liu et al., 2015; Park and Kim, 2015; He et al., 2016, 2018; Kim et al., 2016; Park et al., 2016; Ryu et al., 2016; Zhang et al., 2016; Zhou et al., 2016; González et al., 2017; Jiang et al., 2017; Ghimire et al., 2018; Xiang and Daoud, 2019; Yang et al., 2019). However, regarding the complex diffusion domain inside a felt electrode, the common approach of relating the peak-to-peak separation of an S-CV curve to the electrodes' kinetics (valid for a planar electrode in semi-infinite diffusion space only; Matsuda and Ayabe, 1954; Nicholson and Shain, 1964; Nicholson, 1965) does not seem to be appropriate. Applying the irreversible Randles-Ševčík relation for deducing the intrinsic kinetics of a felt electrode is also not possible since (a) the

¹ Stationary refers to an electroanalytical experiment without any forced convection of the electrolyte.

electrochemically active electrode area of the fiber network is unknown or at least uncertain and (b) the variation of the peak height with respect to the potential sweep rate becomes ambiguous when non-planar electrodes are involved (Aoki et al., 1983, 1984, 1985; Aoki, 1988). Since the majority of publications are dedicated to felt electrodes and respective diffusion domain effects rarely receive sufficient attention (Menshykau and Compton, 2008; Smith et al., 2015; Peinetti et al., 2016; Tichter et al., 2019a), literature values of the intrinsic vanadium redox kinetics might spread over orders of magnitude, as discussed recently in the paper by Friedl and Stimming (2017). Unfortunately, studies involving planar electrodes providing a well-defined, semi-infinite diffusion domain are unpopular in case of the VRFB system and a quantification of the intrinsic kinetics of novel electrode materials usually remains untested (Oriji et al., 2004; Han et al., 2011; Li et al., 2011, 2012, 2013, 2014; Jin et al., 2013; Dai et al., 2017). Compared to S-CV/LSV measurements at planar electrodes, studies using a rotating disc electrode (RDE) are even more unpopular (Zhong and Skyllas-Kazacos, 1992; Oriji et al., 2004). This is somewhat astonishing since they are well established in other fields of energy conversion (e.g., the fuel cell community) and can provide valuable information on the proceeding electrode reactions. With this paper we present a recent and comprehensive study on the oxidation reaction of VO^{2+} at electrochemically activated glassy carbon electrodes involving stationary and rotating linear sweep voltammetry as well as chronoamperometry. It is demonstrated that a Koutecký-Levich analysis of the RDE limiting currents yields a theoretically unexpected non-zero ordinate intercept proportional to the inverse VO^{2+} concentrations. Furthermore, it is shown that interpreting S-LSV data in terms of the irreversible Randles-Ševčík relation leads to values in the electron transfer coefficient α that contradict the findings from Tafel analysis of RDE data. We account for these two unexpected features simultaneously by introducing finite heterogeneous kinetic rate constants into the Butler-Volmer equation. Based on this idea, a three-term Koutecký-Levich equation is derived, allowing for unraveling mass transport, Butler-Volmer electrode kinetics and finite heterogeneous electron transfer kinetics. In this manner, the maximum heterogeneous rate constant for the oxidation reaction of VO^{2+} is found to be $k_{\text{max}} = 2.6 \cdot 10^{-2}$ cm/s. By including the estimated maximum rate constant into the theory of stationary linear sweep voltammetry, we also propose a model that captures the deviations of the experimental S-LSV data from the ideal irreversible Randles-Ševčík behavior. Finally, it is shown mathematically that the classical Tafel analysis of RDE data is unaffected by the limited electron transfer kinetics and should therefore be preferred for kinetic characterization.

2. EXPERIMENTAL SECTION

2.1. Electrochemical Measurements

The oxidation of VO^{2+} was investigated at electrochemically activated glassy carbon surfaces. The electrochemical activation was performed according to the conditioning given in **Table 1**. As an electrolyte solution, 2 M H_2SO_4 (ROTIPURAN® Ultra

TABLE 1 | Overview of all linear sweep (LSV) and chronoamperometry (CA) measurements with corresponding pretreatments.

	Stationary-LSV	Rotating-LSV	Stationary-CA
ω / rpm	0	100, 123, 156, 204, 278, 400, 625	0
v / mV s^{-1}	70, 60, 50, 40, 30, 20, 10	20	0
E vs. $E_{\text{Ag/AgCl}}$ / V	1–1.7	1–1.7	1.65
Conditioning	15 s, –0.2 V 30 s break 20 s, 0.7 V	15 s, –0.2 V at 1,600 rpm 30 s break, 5 s 0.7 V	15 s, –0.2 V at 1,600 rpm, 60 s break

95%, Carl Roth) with different concentrations of VO^{2+} [0.00, 0.02, 0.04, 0.06, and 0.08 M, Vanadium(IV) sulfate oxide hydrate, 99.9% (metals basis), Alfa Aesar] was used. All measurements were performed in a three electrode setup consisting of a Ag/AgCl reference (saturated, 198 mV vs. SHE), a Pt-mesh counter electrode, and a glassy carbon disc (7 mm diameter, embedded into a PEEK cylinder) working electrode. Data was acquired using a PalmSens Em-Stat potentiostat (PalmSens). The working electrode was connected to a control panel (MetrohmAutolab® RDE-2) to adjust the rotation speed during the measurements.

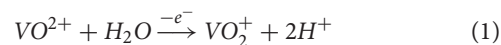
2.2. Pretreatment of the Electrode

Prior to each measurement, the glassy carbon electrode was polished in two successive steps (step 1: 1.0 micron, BUEHLER 40-10081 and step 2: 0.05 micron, BUEHLER 40-10083). Electrochemical activation was performed under rotation in a chronoamperometric three-step sequence (step 1: 2 V vs. E_{Ref} for 15 s, step 2: –1 V vs. E_{Ref} for 5 s, step 3: 2 V vs. E_{Ref} for 5 s, each step at $\omega = 1,600$ rpm). Subsequently, S-LSV, R-LSV, and S-CA measurements were performed as given in **Table 1**.

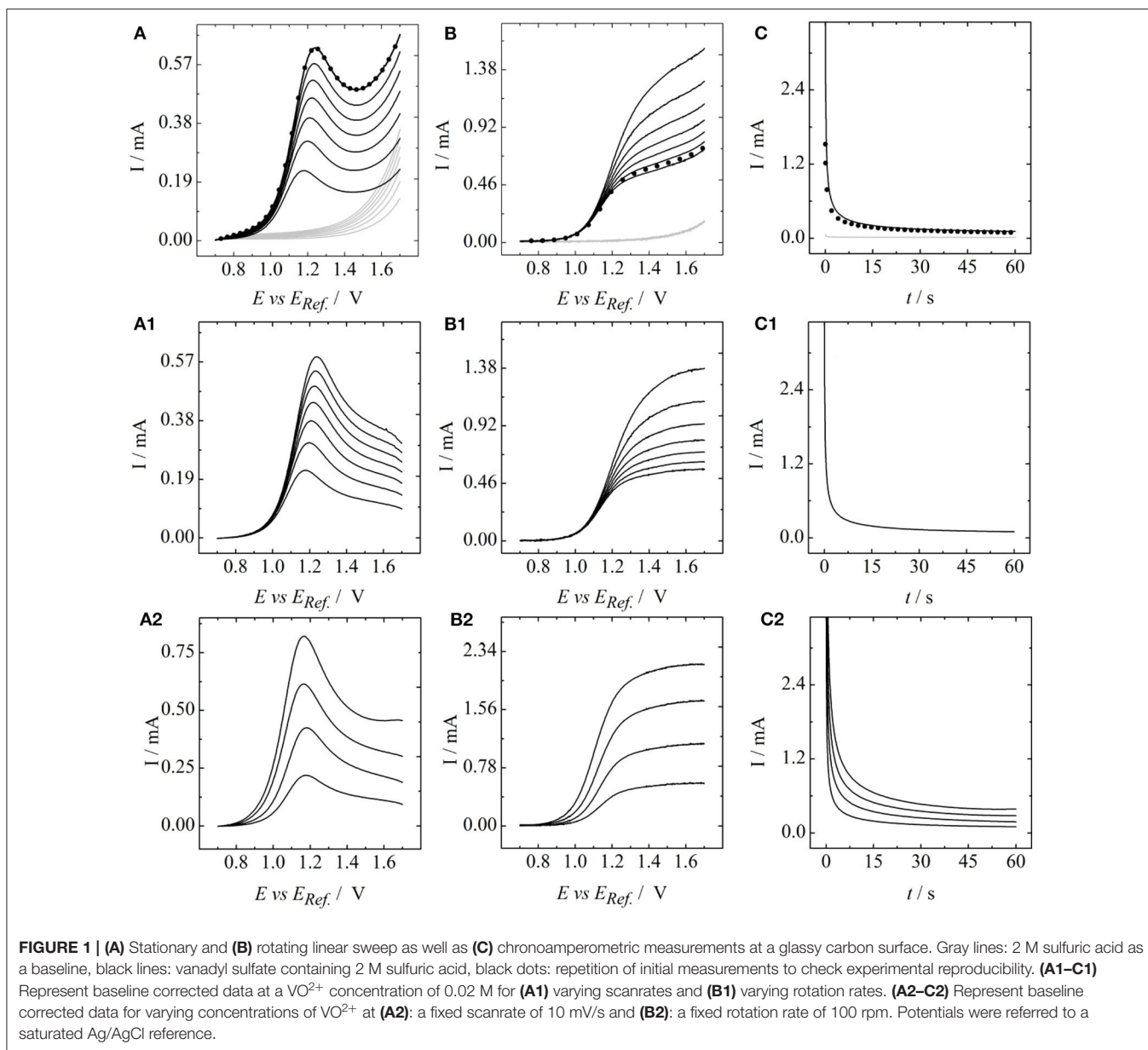
3. RESULTS AND DISCUSSION

3.1. RDE Measurements

The desired reaction of this study, the electrochemical oxidation of VO^{2+} , can be formulated as



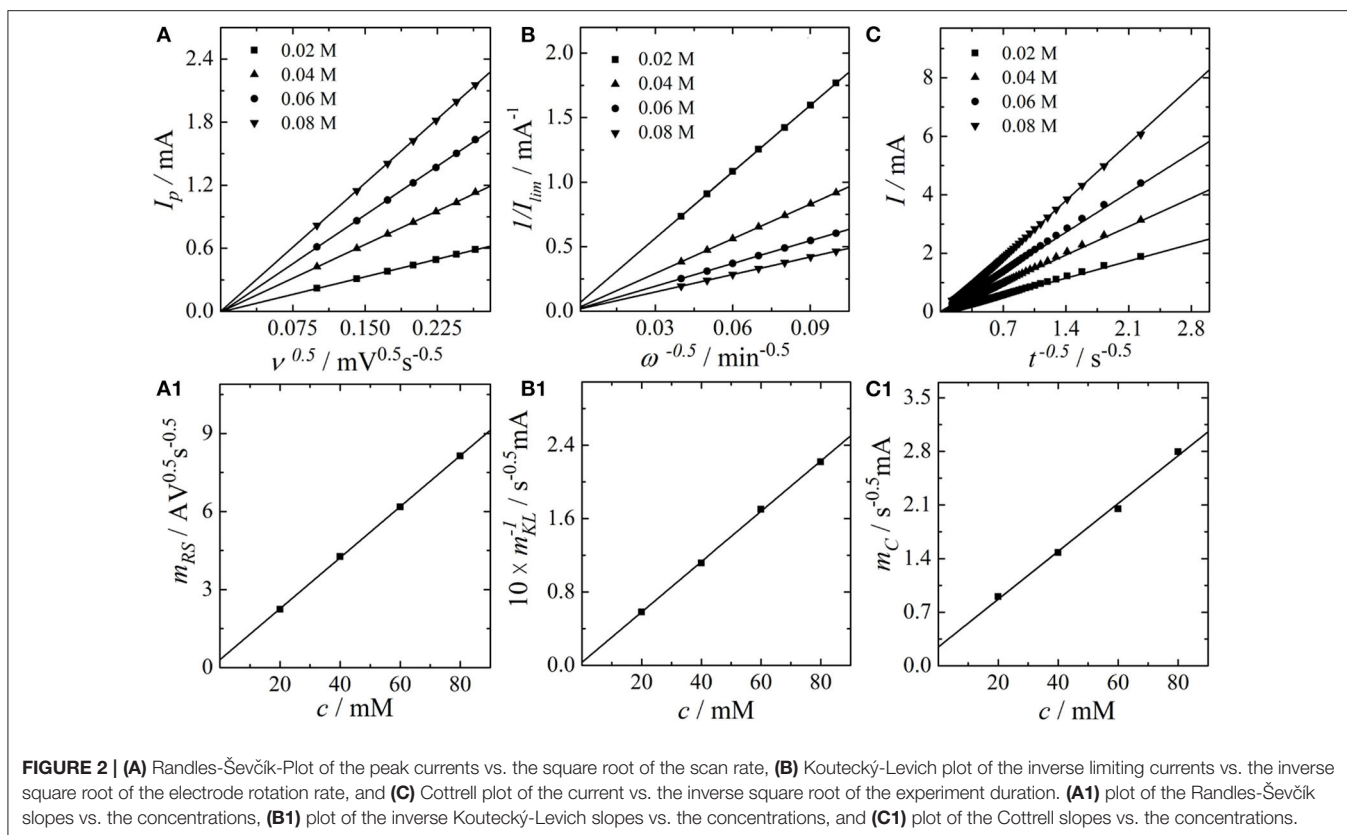
and has a standard electrode potential of $E^0 - E_{\text{SHE}} = 0.995$ V. To eliminate errors resulting from parasitic reactions such as the carbon corrosion or the oxygen evolution reaction, the datasets obtained for vanadium containing electrolytes were corrected by the corresponding vanadium-free baselines in pure 2 M sulfuric acid. This entirely subtractive correction is based on the assumption that any parasitic reactions proceed in parallel and do not impair the desired oxidation



of VO_2^+ . Furthermore, it holds only under the presumption that the electrode area is independent of the applied electrode potential. These assumptions are considered reasonable as long as the upper potential limit does not allow for the formation of gaseous oxygen, which was ensured throughout the entire study. This correction is illustrated for the electrolyte containing 0.02 M vanadyl sulfate in **Figure 1A**: stationary and **Figure 1B**: rotating linear sweep as well as the **Figure 1C**: chronoamperometric measurements. Gray lines represent the baseline in pure 2 M sulfuric acid solution and black lines the measurements in 2 M sulfuric acid containing 0.02 M vanadyl sulfate. The corresponding baseline corrected curves are shown in **Figures 1A1–C1**. Baseline corrected data at the different vanadyl sulfate concentrations are depicted in

Figures 1A2–C2. In the S-LSV measurements (**Figure 1A2**) a potential sweep rate of $\nu = 10$ mV/s was used. The rotation rate in the R-LSV experiments in **Figure 1B2** was set to $\omega = 100$ rpm.

It can be seen that increasing the scan rate (**Figure 1A1**) or the rotation rate (**Figure 1B1**) at fixed VO_2^+ -concentration results in a set of curves starting at the same kinetic origin. In contrast, an increase in the concentrations, as shown in **Figures 1A2, B2**, results in a negative shift of the entire LSV curves. This is expected, as the exchange current is proportional to the analyte concentration. In case of the S-LSVs a peak current with constant peak position is obtained for the different concentrations, whereas in case of the R-LSVs the limiting current scales linearly with respect to the concentrations. The



chronoamperometric measurements of **Figure 1C2** also show a linear scaling of the current with the concentrations. Based on the datasets of **Figures 1, 2A** shows a Randles-Ševčík plot, **Figure 2B** a Koutecký-Levich plot and **Figure 2C** a Cottrell plot for the different concentrations of VO^{2+} . In all cases straight lines are obtained. At this point we want to draw the reader's attention to the experimentally observed ordinate intercepts in the Koutecký-Levich plots in particular. These are not expected from a theoretical point of view and will be discussed in detail in section 3.2. Based on the data of **Figures 2A–C, A1, C1** depict the slopes obtained from the analysis in **Figures 2A, C**, plotted versus the corresponding concentrations of VO^{2+} . A plot of the inverse slope of **Figure 2B** versus the analyte concentration leads to **Figure 2B1**. In all cases a linear concentration dependence is obtained, providing a slope that corresponds to the second partial derivatives of the Koutecký-Levich eq. 3, the irreversible Randles-Ševčík eq. 2 and the Cottrell equation eq. 4, respectively.

$$I_R'' = \frac{\partial^2 I_R}{\partial c \partial v^{1/2}} \quad (2)$$

$$I_K'' = \frac{\partial^2 I_K}{\partial c \partial \omega^{1/2}} \quad (3)$$

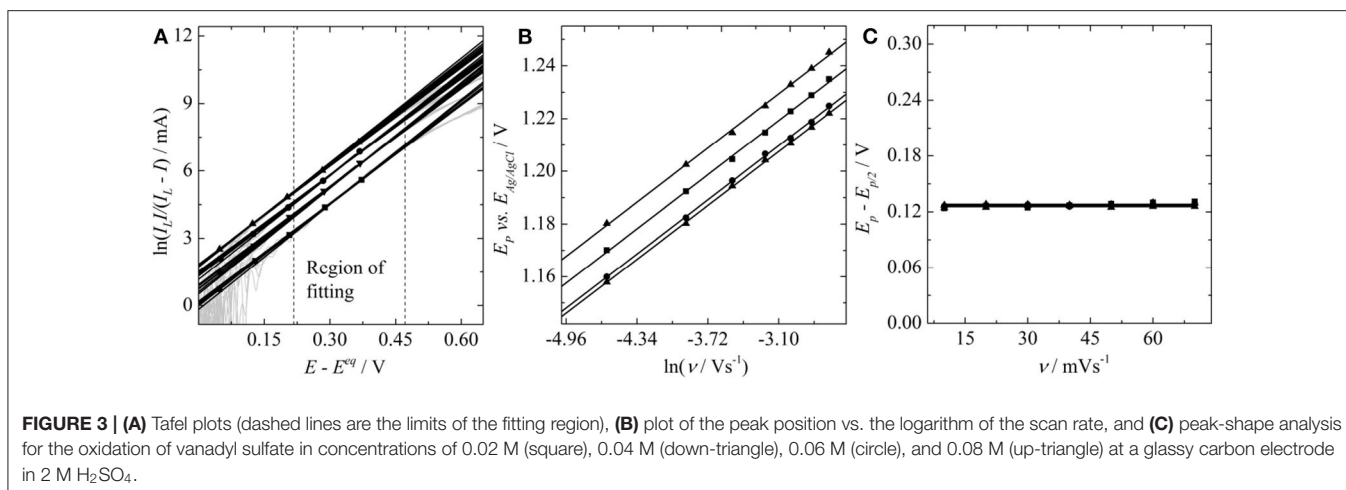
$$I_C'' = \frac{\partial^2 I_C}{\partial c \partial t^{-1/2}} \quad (4)$$

These second partial derivatives are used in the following section for further analysis.

By combining the second partial derivative of the Cottrell equation with the second partial derivative of the Koutecký-Levich equation, we obtain the diffusion coefficient of the VO^{2+} -ion via

$$D = 489\eta \left(\frac{I_K''}{I_C''} \right)^6. \quad (5)$$

Compared to the classical Koutecký-Levich or Cottrell analysis, this expression appears to be superior in estimating diffusion coefficients since (a) it does not depend on the active electrode area (which might differ from the geometric area) and (b) it accounts for different analyte concentrations as well. Furthermore, it is not necessary to know the value of n a priori. Following this strategy, we determine the diffusion coefficient of the VO^{2+} -cation in 2 M H_2SO_4 to a value of $2.26 \cdot 10^{-6} \text{ cm}^2/\text{s}$, in good agreement with the average value given in Zhong and Skyllas-Kazacos (1992) and slightly smaller than the value reported in our recent study (Tichter et al., 2019b), which was obtained from S-CV fitting of a felt electrode. A similar combination of the second partial derivative of the irreversible Randles-Ševčík equation obtained from **Figure 2A1** with the second partial derivative of the Cottrell



equation allows for a determination of the electron transfer coefficient as

$$\alpha = 1.294 \frac{RT}{nF} \left(\frac{I_p''}{I_C''} \right)^2 \quad (6)$$

Nevertheless, it has to be noted that this expression requires the values of n to be known (in the present case it is assumed that $n = 1$). Via Equation (6), we estimate the electron transfer coefficient for the electrochemical oxidation of VO²⁺ at the glassy carbon electrode to $\alpha = 0.32$. At this stage we highlight the importance of the baseline correction as shown in **Figure 1**, which was necessary in order to remove additively scaling parasitic currents. However, we refer to an alternative way for estimating α , which is independent of the current magnitude and is outlined in the early findings of Matsuda and Ayabe (1954). There, the authors propose that it is possible to obtain the electron transfer coefficient for an electrochemically irreversible reaction (taking place at a planar electrode in semi-infinite diffusion space) by analyzing the peak shape and the peak position of a S-LSV curve via Equations (7) and (8) only. Also in this context, however, the value of n has to be known.

$$\alpha = \frac{1.85RT}{nF(E_p - E_{p/2})} \quad (7)$$

$$\alpha = \frac{RT}{2nF} \left(\frac{\partial I_p}{\partial \ln(v)} \right)^{-1} \quad (8)$$

Another, and probably the most straightforward way for obtaining the electron transfer coefficient is given in terms of a Tafel-analysis of RDE data (Equation 9).

$$\alpha = \frac{RT}{nF} \left(\frac{\partial \ln\left(\frac{I_L}{I_L - I}\right)}{\partial (E - E^{eq})} \right) \quad (9)$$

TABLE 2 | Values of the electron transfer coefficient α , estimated from Tafel-, Randles-Ševčík-, and Matsuda-Ayabe analysis.

	0.02 M	0.04 M	0.06 M	0.08 M
$\alpha(A)$	0.381	0.383	0.375	0.381
$\alpha(B)$	0.385	0.385	0.385	0.386
$\alpha(C)$	0.371	0.376	0.371	0.368

In order to deduce α , **Figure 3A**: a Tafel plot, **Figure 3B**: a plot of the peak position versus the logarithm of the scan rate and **Figure 3C**: the peak shape analysis for the oxidation of vanadyl sulfate at a glassy carbon electrode. The values of the electron transfer coefficient are listed in **Table 2**.

All the values of α given in **Table 2** are close to $\alpha = 0.38$ and therefore diverge significantly from the value of $\alpha = 0.32$ determined by Equation (6). No dependence of α on the concentrations is observed. Consequently, the average of the α value is taken for all individual concentrations. Thus, analyzing the dependence of the peak-potential on the logarithm of the scan rate according to Equation (7) yields $\alpha = 0.385$, the shape analysis according to Equation (8) leads to $\alpha = 0.372$, and a Tafel analysis provides $\alpha = 0.38$. Furthermore, a Tafel analysis provides the standard heterogeneous rate constant to $k^0 = 1.35 \cdot 10^{-5}$ cm/s. The significant deviation in the α values given in **Table 2** from the findings involving Equation (6) as well as the unexpected non-zero ordinate intercepts in Koutecký-Levich analysis will be discussed in the following subsections.

3.2. Concept of Finite Heterogeneous Kinetics

The experimentally observed non-zero ordinate intercepts obtained in Koutecký-Levich plots are the main motivation for the following considerations. Such a behavior cannot be explained with the classical Koutecký-Levich model (Equation 10), since a limiting current, or better, a hydrodynamic limiting current caused by mass transfer limitations—corresponds to infinitely fast reaction kinetics forcing $I_{kin}^{-1} \rightarrow 0$. Consequently,

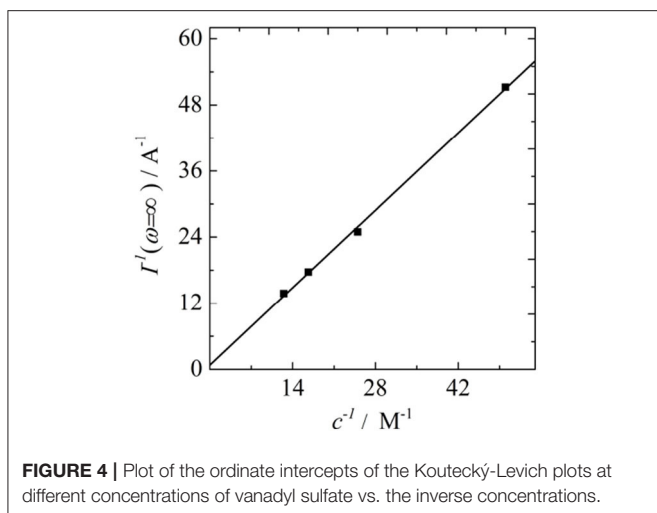


FIGURE 4 | Plot of the ordinate intercepts of the Koutecký-Levich plots at different concentrations of vanadyl sulfate vs. the inverse concentrations.

the extrapolation to infinite rotation rate will actually give a zero-ordinate intercept.

$$\frac{1}{I_K} = \frac{1}{I_{kin}} + \frac{1}{0.201nFACD^{2/3}\eta^{-1/6}\sqrt{\omega}} \quad (10)$$

However, we propose that a current plateau, usually associated with the hydrodynamic limiting current, can also be reached by a limitation of the heterogeneous reaction kinetics itself. Thus, the term I_{kin}^{-1} will become small and constant, but it will not approach zero. The current plateau achieved under these circumstances will always be lower than the hydrodynamic limiting current, which is indeed what is observed experimentally. By calculating the hydrodynamic limiting current with the classical Koutecký-Levich equation using the previously obtained value of D , the estimated hydrodynamic limiting current values are always larger than their experimentally measured analogs. Thus, we suggest that for implementing the concept of a maximum kinetic current into the Koutecký-Levich equation, a third and additively scaling inverse current term that does neither depend on the overpotential, nor on the rotation rates is required. Subsequently, it needs to be clarified whether or not this extra quantity will depend on the analyte concentrations. By thoroughly examining the Koutecký-Levich plots for the different concentrations of VO^{2+} we found a linear relation between the ordinate intercepts and the inverse analyte concentration, which is depicted in **Figure 4**. Consequently, we propose that the maximum kinetic current has to be considered as a linear function of the concentration. Assuming that the slope of the line in **Figure 4** can be expressed in terms of the maximum kinetic current, which we define by $I_{max} = nFAck_{max}$, we obtain a maximum heterogeneous rate constant of $k_{max} = 0.026$ cm/s. This hypothetical limit is the starting point for further considerations, where the idea of finite kinetics will be introduced into the Butler-Volmer equation.

3.3. Theoretical Discussion

First, we recall the classical Butler-Volmer equation as

$$I = nFAk^0 \left(c_{red,s} e^{\alpha\xi} - c_{ox,s} e^{-(1-\alpha)\xi} \right), \quad (11)$$

where $\xi = nF(E - E^0)/RT$ denotes the dimensionless electrode potential and $c_{red,s}$ and $c_{ox,s}$ denote the surface concentrations of the electrochemically active species. Other variables have their usual meaning. An introduction of a maximum achievable rate constant k_{max} yields

$$I = nFAk^0 \left(c_{red,s} \frac{k_{max} e^{\alpha\xi}}{k_{max} + k^0 e^{\alpha\xi}} - c_{ox,s} \frac{k_{max} e^{-(1-\alpha)\xi}}{k_{max} + k^0 e^{-(1-\alpha)\xi}} \right). \quad (12)$$

It is readily seen that Equation (12) reduces to Equation (11) when k_{max} becomes very large which corresponds to the case of no kinetic limitations. In contrast, if k_{max} is comparably small, the effect of kinetic limitations can be expected to be more prominent. Equation (12) is the starting point for all further considerations.

3.3.1. Rotating Electrode Polarography With Finite Kinetics

Introducing the above definition of the maximum kinetic current as

$$I_{max} = nFAc_b k_{max}, \quad (13)$$

where the index b represents the bulk concentration, as well as the exchange current as

$$I^{eq} = nFAk^0 c_{red,b} e^{a\xi} = nFAc_{ox,b} k^0 e^{-(1-\alpha)a\xi}, \quad (14)$$

where $a = nF(E^{eq} - E^0)/RT$ is the dimension-less equilibrium potential, we get

$$I = I^{eq} \left(\frac{c_{red,s}}{c_{red,b}} \frac{I_{max,an} e^{\alpha(a-\xi)}}{I_{max,an} + I^{eq} e^{\alpha(a-\xi)}} - \frac{c_{ox,s}}{c_{ox,b}} \frac{I_{max,ca} e^{-(1-\alpha)(a-\xi)}}{I_{max,ca} + I^{eq} e^{-(1-\alpha)(a-\xi)}} \right). \quad (15)$$

For a rotating electrode we substitute the steady state formalism $c_{red,s}/c_{red,b} = 1 - I/I_{L,an}$ and $c_{ox,s}/c_{ox,b} = 1 - I/I_{L,ca}$ with $I_{L,an}$ and $I_{L,ca}$ being the anodic and cathodic limiting currents expressed by the Levich equation. Since the backward reaction can be neglected at absolute overpotentials larger than $118/n$ mV, Equation (15) can be simplified for an exemplary anodic reaction to

$$I = I^{eq} \left(\left(1 - \frac{I}{I_{L,an}} \right) \frac{I_{max,an} e^{\alpha(a-\xi)}}{I_{max,an} + I^{eq} e^{\alpha(a-\xi)}} \right) \quad (16)$$

This expression can be rearranged to give the following desired three-term Koutecký-Levich equation

$$\frac{1}{I} = \frac{1}{I_{kin}} + \frac{1}{I_{L,an}} + \frac{1}{I_{max}}. \quad (17)$$

The first two terms in Equation (17) form the classical Koutecký-Levich equation, whereas the third term $1/I_{max}$ contains the maximum rate constant and is therefore responsible for the non-zero ordinate intercept in Koutecký-Levich plots. As k_{max} tends to infinity, the third term vanishes, and Equation (17) reduces to the classical expression. Unifying the term of the hydrodynamic limiting current with the maximum kinetic current, the latter two terms in Equation (17) provide the measured limiting current $I_{lim,me}$ as

$$I_{lim,me} = \frac{I_{lim,an}I_{max,an}}{I_{lim,an} + I_{max,an}}. \quad (18)$$

Consequently, the unlimited kinetic current can be obtained from measured data as

$$\ln(I_{kin}) = \ln\left(\frac{I_{lim,me}I}{I_{lim,me} - I}\right) = \ln(I^{eq}) + \frac{\alpha nF(E - E^{eq})}{RT}, \quad (19)$$

which is in principle just a rearranged version of Equation (18) as well as an alternative form of the conventional “mass transfer correction” described by Equation (9). This underlines that even if the heterogeneous kinetics are finite, the value of α and I^{eq} (and thus k^0) can still be determined by using Tafels law if the current gets normalized properly to its limiting value.

3.3.2. Stationary Electrode Polarography With Finite Kinetics

If the model of finite kinetic rate constants is valid for a rotating electrode, it has to apply also to stationary measurements. In analogy to the limiting currents of an RDE experiment it can be assumed that the finite electrode kinetics will reduce the peak height in a S-LSV curve, which would in turn explain the misleading results of α obtained from the classical Randles-Ševčík analysis. To support this assumption, the theory of stationary electrode polarography, accounting for finite heterogeneous kinetics, will be re-derived in this paragraph. Starting again with Equation (12) and replacing the surface activities by their known expressions of the convoluted current for semi-infinite planar diffusion as

$$c_{red,s} = c_{red,b} - \frac{1}{nFA\sqrt{\pi D}} \int_0^t \frac{I(\tau)}{\sqrt{t-\tau}} d\tau \quad (20)$$

$$c_{ox,s} = c_{ox,b} + \frac{1}{nFA\sqrt{\pi D}} \int_0^t \frac{I(\tau)}{\sqrt{t-\tau}} d\tau \quad (21)$$

we obtain

$$\frac{I(t)}{nFAk^0k_{max}} = \frac{c_{red,b}e^{\alpha\xi(t)}}{k_{max} + k^0e^{\alpha\xi(t)}} - \frac{c_{ox,b}e^{-(1-\alpha)\xi(t)}}{k_{max} + k^0e^{-(1-\alpha)\xi(t)}} - \frac{1}{nFA\sqrt{\pi D}} \left[\frac{e^{\alpha\xi(t)}}{k_{max} + k^0e^{\alpha\xi(t)}} + \frac{e^{-(1-\alpha)\xi(t)}}{k_{max} + k^0e^{-(1-\alpha)\xi(t)}} \right] \int_0^t \frac{I(\tau)}{\sqrt{t-\tau}} d\tau. \quad (22)$$

Defining a new constant $k_{fin} = k^0/k_{max}$ and taking the definition of the dimensionless rate constant and the dimensionless current as

$$\Lambda = \frac{k^0\sqrt{RT}}{\sqrt{nFvD}} \quad (23)$$

$$\chi(\xi) = \frac{I(\xi)}{nFAc_{red,b}\sqrt{\frac{nFvD}{RT}}} \quad (24)$$

we obtain the following integral equation (Equation 25).

$$\frac{\chi(\xi)}{\Lambda} \frac{1 + k_{fin}(e^{\alpha\xi} + e^{-(1-\alpha)\xi}) + k_{fin}^2e^{\xi(2\alpha-1)}}{e^{\alpha\xi} + e^{-(1-\alpha)\xi} + 2k_{fin}e^{\xi(2\alpha-1)}} = \frac{(1 - e^{a-\xi}) + k_{fin}(1 + e^a)e^{-(1-\alpha)\xi}}{1 + e^{-\xi} + 2k_{fin}e^{-(1-\alpha)\xi}} - \frac{1}{\sqrt{\pi}} \int_0^\xi \frac{\chi(\xi)}{\sqrt{\xi-\zeta}} d\zeta \quad (25)$$

The desired dimension-less current function $\chi(\xi)$ can be evaluated accurately as Riemann-Stieltjes integral after eliminating the singularity in the denominator similar to Nicholson and Shain (1964). In case of no kinetic limitations it is obvious that $k_{max} \rightarrow \infty$ and thus $k_{fin} \rightarrow 0$. Therefore, Equation (25) condenses to the expression (Equation 26) of (Matsuda and Ayabe, 1954):

$$\frac{\chi(\xi)}{\Lambda} \frac{1}{e^{\alpha\xi} + e^{-(1-\alpha)\xi}} = \frac{(1 - e^{a-\xi})}{1 + e^{-\xi}} - \frac{1}{\sqrt{\pi}} \int_0^\xi \frac{\chi(\xi)}{\sqrt{\xi-\zeta}} d\zeta. \quad (26)$$

3.3.3. Simulation of Data

In this section, Equation (25) is used for simulating stationary LSV responses that are subsequently evaluated using the irreversible Randles-Ševčík relation as well as Equations (7) and (8) in order to reproduce the experimentally observed error. For the simulation we took $\alpha = 0.38$ and $k^0 = 1.35 \cdot 10^{-5}$ cm/s as extracted from the Tafel plots of **Figure 3A** and $k_{max} = 0.026$ cm/s as extracted from **Figure 4** as well as the estimated value of $D = 2.26 \cdot 10^{-6}$ cm²/s. Simulations were performed using our in-house developed software Polarographica (Tichter and Schneider, 2019). The calculated voltammograms as well as the corresponding Randles-Ševčík plot, conducted peak-shape analysis, and plotted the dimensionless peak potential vs. the scan rate, as shown in **Figure 5**.

Analyzing the simulated dataset of **Figure 5** gives $\alpha = 0.343$ for the Randles-Ševčík analysis, $\alpha = 0.371$ for the peak shape analysis and $\alpha = 0.378$ for the plot of the peak potential vs. the logarithm of the scan rate. This confirms our expectation, that significant deviations from the original α value are obtained as soon as finite kinetics are present. Furthermore, it shows that the largest error in α is obtained by the classical Randles-Ševčík analysis which captures the experimentally observed trend. Consequently, we conclude that, in stationary potential sweep

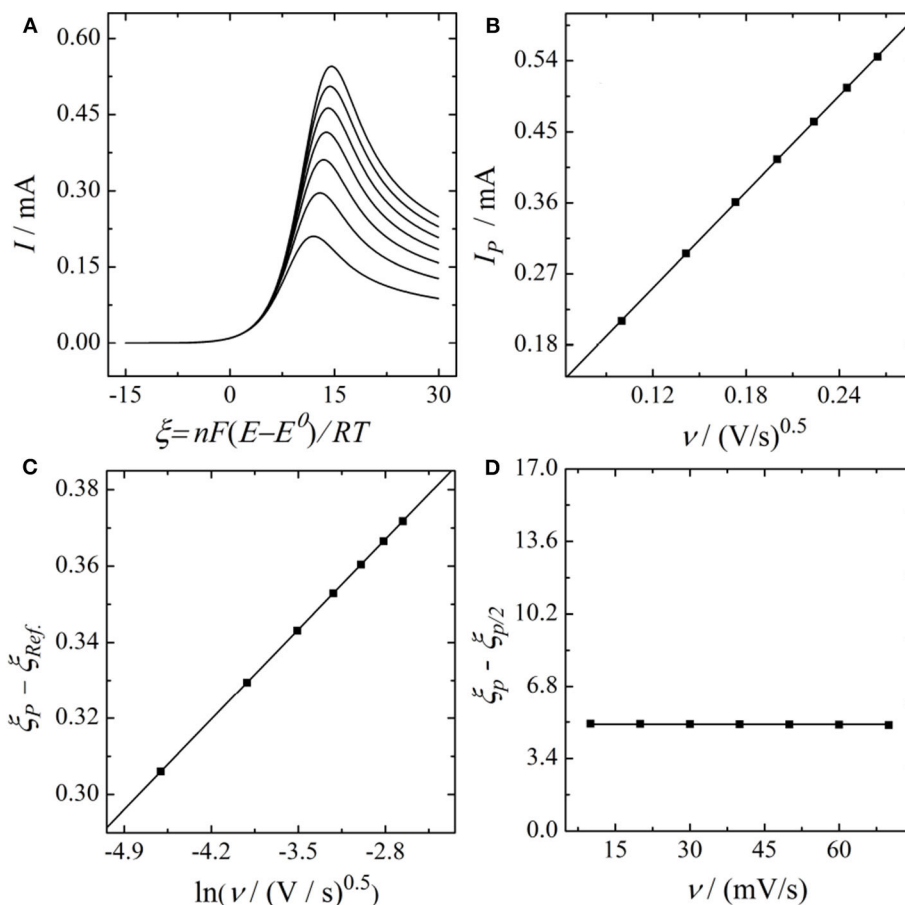


FIGURE 5 | (A) S-LSV curves, **(B)** Randles-Ševčík Plot, **(C)** Matsuda-Ayabe analysis, and **(D)** peak shape analysis of an electrochemical reaction (the oxidation of VO^{2+} with finite kinetics simulated for the set of parameters obtained previously via Tafel analysis and Kouteck-Levich analysis).

experiments, the finite heterogeneous kinetics predominantly affect the current magnitude. Nevertheless, it has to be noted that also the accuracy of the shape analysis and the plot of the peak potential vs. the scan rate are affected by the kinetic limitations, even if these deviations are minor. Based on these findings we finally conclude that S-LSV measurements are not well-suited for estimating the electrode kinetics in a straightforward way, even if planar electrodes are involved. In contrast, since Tafel analysis of RDE data is independent of the finite electrode kinetics, we refer it as a more reliable way for investigating electrode kinetics.

3.3.4. Practical Relevance of Finite Kinetics

In the previous sub-paragraphs, the experimental verification and theoretical treatment of finite heterogeneous electrode kinetics were introduced. However, so far, we have not yet discussed the practical relevance and the possible origin of such a limitation. When regarding an electrode reaction like the electrochemical oxidation of VO^{2+} , the classical analysis usually accounts for Butler-Volmer electron transfer kinetics coupled to

mass transfer only. Consequently, no intermediate reaction steps are considered. Such additional reaction steps might be, however, responsible for the finiteness of the electrode reaction kinetics. In this context one might think of (a) an adsorption/desorption of the electrochemically active vanadium species preceding or following the electron transfer or (b) of rearrangements in the solvate shell of the vanadium ions which have to occur before an electrochemical reaction can proceed. However, since we do not have any experimental evidence for either scenario (a) or (b), we do not attempt to speculate about possible reaction mechanisms at this stage. In contrast, we want to underline that analyzing the kinetic limit of an electrochemical reaction with the strategy outlined in this paper can offer valuable insights in the intrinsic activity of novel catalyst materials, since an overpotential independent performance indicator is obtained. In this manner, our strategy might also lead to a better understanding of intermediate reaction steps. Therefore, it can be extraordinarily important for the experimentalists community when screening alternative catalyst materials for possible applications in a VRFB.

4. SUMMARY AND CONCLUSIONS

The kinetics of the $\text{VO}^{2+}/\text{VO}_2^{2+}$ redox couple was investigated at planar glassy carbon electrodes via rotating and stationary linear sweep voltammetry as well as stationary chronoamperometry. A combination of the Koutecký-Levich equation with the Cottrell equation allowed for a precise determination of the diffusion coefficient of the vanadyl cation, leading to $D = 2.26 \cdot 10^{-6} \text{ cm}^2/\text{s}$. A similar combination of the irreversible Randles-Ševčík equation with the Cottrell equation provided an electron transfer coefficient of $\alpha = 0.32$. Contrary, calculating the electron transfer coefficient via Tafel analysis of RDE data provided $\alpha = 0.38$. This deviation in the electron transfer coefficient as well as the experimentally observed non-zero ordinate intercepts in Koutecký-Levich plots, which cannot be explained by the classical model are explained simultaneously by introducing the concept of finite heterogeneous electron transfer kinetics into the Butler-Volmer equation. In this manner, a three term Koutecký-Levich type equation was derived, which allows for the determination of the maximum kinetic rate constant to $k_{\text{max}} = 0.026 \text{ cm/s}$. By considering the modified Butler-Volmer equation as the boundary condition for stationary electrode polarography, the experimentally observed deviation in the electron transfer coefficients could be simulated as well. Based on the modified

version of the Butler-Volmer equation it was shown that Tafel analysis of RDE data will not be affected by the finite heterogeneous kinetics. Therefore, we concluded that the Tafel analysis in a rotating disc electrode setup is the most accurate method to determine the kinetic parameters of a reaction.

DATA AVAILABILITY STATEMENT

The raw data supporting the conclusions of this article will be made available by the authors, without undue reservation.

AUTHOR CONTRIBUTIONS

TT carried out the data acquisition and conception, developed the theory, and wrote the manuscript. JS carried out the conception and scientific discussion and wrote the manuscript. CR carried out the scientific supervision and wrote the manuscript. All authors contributed to the article and approved the submitted version.

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Conflict of Interest: The authors declare that the research was conducted in the absence of any commercial or financial relationships that could be construed as a potential conflict of interest.

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