



Well-dispersed Pd–Sn nanocatalyst anchored on TiO₂ nanosheets with enhanced activity and durability for ethanol electrooxidation

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ABSTRACT

Novel Pd₁–Sn_x/TiO₂ nanosheets catalyst with higher activity and durability for ethanol oxidation (EOR) was obtained by NaBH₄ co-reduction method in direct ethanol fuel cells (DEFCs). The electrochemical performance tested under alkaline conditions illustrates that the prepared Pd₁–Sn_{0.6}/TiO₂ NSs catalyst presents outstanding activity (3381 mA mg⁻¹_{Pd}) and excellent CO anti-poisoning ability for EOR. Meanwhile, the residual current density of Pd₁–Sn_{0.6}/TiO₂ NSs nanocatalyst (1207 mA mg⁻¹_{Pd}) is 8.5 times of the Pd/C (JM) catalyst (142 mA mg⁻¹_{Pd}) after the durability test of 5000 s for EOR. Additionally, the Pd₁–Sn_x/TiO₂ nanosheets show prominent electrocatalytic activity in EOR comparison with Pd/TiO₂ nanosheets and Pd–Sn nanocatalysts. Thus, Pd and Sn doped in TiO₂ nanosheets not only display excellent electrocatalytic, but also reduce the cost of Pd, which have some reference value for DEFCs.

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1. Introduction

Direct ethanol fuel cells (DEFCs), as low operation temperature power sources for facile handling, storage and transportation, have drawn widespread attention as that their renewable biomass, low noise, non-toxic, and high efficiency [1–5]. So far, Pd has been considered significantly to the evolution of fuel cell catalysis as an efficient noble metal for the alkaline ethanol oxidation reactions [1,6–10]. Nevertheless, the surfaces with unmodified Pd nanoparticles suffer from several major problems, which lead to a sluggish reaction kinetics and serious carbon monoxide (CO) byproduct poisoning with influence on catalytic activity [11–13]. To solve those problems, Pd-based nanoparticles have been prepared through four main approaches: controlling the shape and size, incorporating organic material additives, selecting the proper support materials and adding oxyphilic elements in Pd-based catalysts [14–19]. These methods were mainly applied to obtain Pd-based electrocatalysts with large surface area, sufficient activity and long-term electrochemical stability. Meanwhile, Pd-based catalysts have stronger anti CO poisoning ability, which is

different from Pt-based catalysts, and it can surmount catalyst poisoning effect in EOR [20–24].

In recent years, Pd-based catalysts with second metals such as Sn [25], Ni [20], Au [26] and Ru [27] or with metal oxides (SnO [28], SnO₂ [29], CeO₂ [30], NiO [31], MgO [31], etc), exhibited more excellent catalytic performance compared to their monometallic counterparts. Some studies manifested that introduction of oxyphilic elements to enhance the catalytic stability were ascribed to the ligand and synergistic effect [19,22]. Among these additives, Sn can furnish oxygen-containing groups to improve the catalytic durability because of the bifunctional mechanism between Sn and Pd [32,33]. Moreover, binding strength of CO–Pd could be weakened by the probable mechanism that the O₂ binding strength to Sn particles was increased due to the electron donation to Pd by Sn nanoparticles [34]. Moreover, there are formation of OH radicals in catalytic process, which can transform CO oxidation into CO₂ [11,35].

Nevertheless, the individual Pd–M (M = Sn, Ni, Ru, Rh, Fe, Au, etc) nanoparticles easily aggregate [36,37], which dramatically decreases the utilization efficiency of Pd–M and thus the active sites of the catalyst cannot be fully utilized. To overcome this issue, preparation of highly dispersed and narrow particle size nanoparticles by different methods such as Microwave method, ultrasonic irradiation, electrodeposition reduction, etc [36,38–40]. Unfortunately, the synthesis methods mentioned above make them

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hard to large-scale applications. Although the catalyst nanocomposites can be obtained using the co-reduction method, the catalyst aggregation is still unavoidable. Besides, it is possible to solve the catalyst aggregation and intolerable cost problems by selecting a suitable carrier (high surface areas, thermal conductivity and good chemical durability). It is well known that there are different degrees of carbon corrosion for all carbon materials, resulting in the deactivation of the catalyst. Therefore, it is important to look for a non-carbonaceous carrier to solve corrosion problem. In a recent study, metal oxides (SiO_2 [41], CeO_2 [30], TiO_2 [42], etc) are used as catalyst carriers, among which TiO_2 has stronger corrosion resistance ability and higher mechanical strength than conventional carbon black, and may play vital role in the catalytic process to provide oxygen-containing substances and fascinating chemical stability [43–45]. Unique two-dimensional TiO_2 nanosheets (TiO_2 NSs) are one of the primary conditions for the preparation of high-efficiency electrocatalysts as a carrier of immobilizing metal nanoparticles. And it is cheaper than the unmodified two-dimensional material graphene, and the preparation method is simpler [12]. Otherwise, previous research showed that the (001) surface of TiO_2 has more efficient active sites than the thermodynamically stable (101) surface [46–49]. In recent years, anatase TiO_2 nanocrystals/nanosheets with unique two-dimensional structure, which has more exposed high energy (001) patches, have been successfully formed in different reaction systems by using hydrofluoric acid as a capping agent [45,47]. Therefore, the partial anchoring of Pd and Sn with TiO_2 NSs is helpful to enhance the adsorption CO_2 and the band energy CO-Pd can be weakened to obtain excellent electrocatalytic performance [7,8].

Herein, a facile and general approach is developed for load bimetallic Pd–Sn nanoparticles on two-dimensional TiO_2 NSs. The Pd–Sn/ TiO_2 NSs catalysts with different proportion of precursors were prepared by in-situ chemical reduction of PdCl_2 and SnCl_2 on TiO_2 NSs. Compared to the Pd–Sn, Pd/ TiO_2 NSs and Pd/C (JM), the Pd–Sn/ TiO_2 NSs exhibit substantially enhanced activity and stability for EOR.

2. Preparation of catalysts

Fig. 1 shows the synthesis progress of Pd–Sn/ TiO_2 nanosheets, which mainly includes functional TiO_2 nanosheets synthesis, Pd and Sn nanoparticles in-site reduction anchored on TiO_2 nanosheets.

At first, the TiO_2 nanosheets (TiO_2 NSs) were obtained according to the reported procedures [48–50]. TBOT (5 mL) and HF (2 mL) were added with high-pressure reaction kettle (20 mL) after stirring for 1 h, then 5 mL of ethanol (Et) solution was slowly added dropwise into the above solution. The mixed solution was stirred magnetically for 30 min, then transferred to the oven and reacted at 180 °C for 16 h.

Secondly, the NH_2 -functionalized TiO_2 NSs precursors (f- TiO_2 NSs) were prepared according to references [47,48]. TiO_2 NSs (56 mg) were dispersed in ethanol (32 mL) after 2 h ultrasonic treatment. Then reacted with H_2O_2 (2 mL), ammonium hydroxide (2 mL) and 3-Aminopropyltrimethoxysilane (APTMS, 1.4 mL) for 12 h.

At last, the Pd–Sn/ TiO_2 nanosheets were obtained by PdCl_2 and SnCl_2 co-reduced on f- TiO_2 nanosheets. The f- TiO_2 NSs (10 mg) were dispersed in EG (10 mL) under sonication, and PdCl_2 (0.5 mL, 0.09 M) and SnCl_2 (1.5 mL, 0.0189 M) were added synchronously. Then, 0.5 M NaOH/EG rapidly adjust the pH of the mixed solution so that the value of pH is 10–10.5, followed by slowly adding 25 mL NaBH_4 (2.0 mg mL^{-1}). Then the solution was stirred at room temperature for 8 h. Finally, the Pd–Sn/ TiO_2 nanosheets were centrifuged and washed repeatedly with ethanol and ultrapure water. The dry products (4 mg) were dispersed in 2 mL ultrapure water to obtain a certain concentration of catalyst.

Pd–Sn/ TiO_2 nanosheets with different Pd/Sn ratios were obtained by controlling the amount of SnCl_2 and keeping the amount of PdCl_2 unchanged. The weight percent of Pd is around 22.30% for as-prepared $\text{Pd}_{1-\text{Sn}_x}/\text{TiO}_2$ NSs, while the weight percent of Sn for $\text{Pd}_{1-\text{Sn}_{0.25}}/\text{TiO}_2$ NSs, $\text{Pd}_{1-\text{Sn}_{0.6}}/\text{TiO}_2$ NSs and $\text{Pd}_{1-\text{Sn}_1}/\text{TiO}_2$ NSs catalysts is about 5.58%, 13.38% and 22.30%, respectively. At the same time, supplementary materials show the details of materials for catalysts preparation, physical and chemical characterization of

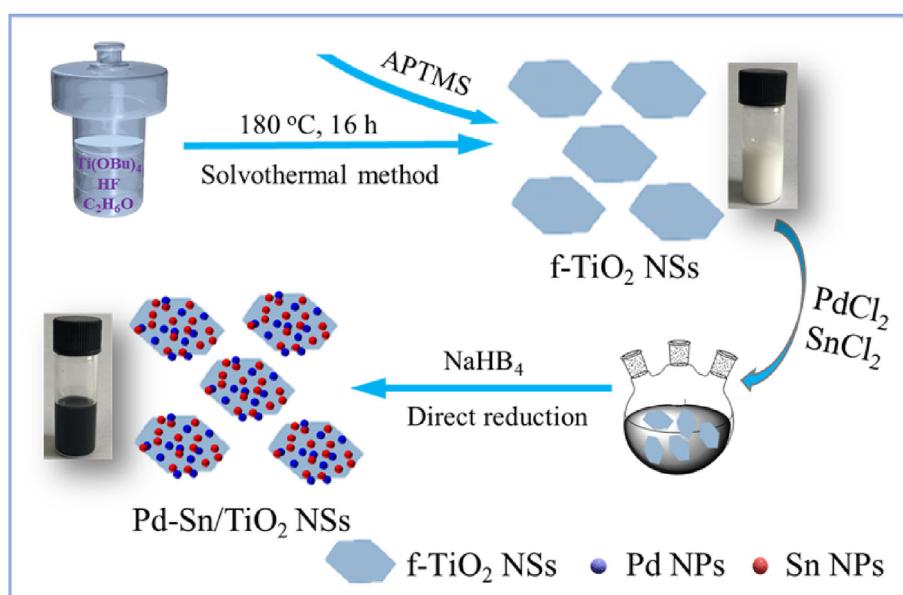


Fig. 1. Schematic diagram for the preparation of Pd–Sn/ TiO_2 NSs.

as-prepared catalysts.

3. Results and discussion

3.1. Structure of the Pd–Sn/TiO₂ NSs catalyst

The TEM images of the prepared TiO₂ NSs are shown in Fig. 2a. Results show that 2D ultrathin TiO₂ NSs with molecular-scale thickness can provide abundant active sites for EOR due to larger surface area. However, under the influence of the certain synergistic effect between Sn and TiO₂ NSs [41], Pd and Sn nanoparticles without obvious aggregation were co-reduced on the surface of 2D nanosheets (Fig. 2b). The surface roughness of the NSs is relevant to the uniform deposition of Pd and Sn on TiO₂ NSs. Meanwhile, the average diameter of Pd–Sn NPs (Fig. S1) is 5.0 ± 0.4 nm calculated by counting 100 random Pd–Sn NPs, as demonstrated by the histogram. The chemical composition of TiO₂ NSs and Pd–Sn/TiO₂ NSs

determined by EDX are shown in Fig. 2a–b. The Si peak roots from glass slides. Meanwhile, the peaks of Ti and O describe adequately TiO₂ NSs. The peaks of Pd and Sn belong to the Pd and Sn nanoparticles on the surface of TiO₂ NSs.

Meanwhile, as verified by HR-TEM image and EDX mapping (Fig. 2c), Pd and Sn NPs are evenly dispersed on TiO₂ NS. The dispersion of nanoparticles can not only help to obtain high specific activity electrocatalysts but also enhance catalyst utilization [19]. Besides, the EDX mapping indicated that Pd and Sn NPs alloy are partially formed. It is worth noting that the surface of TiO₂ NS capped by Pd and Sn are still partly exposed. As shown in Fig. 2d, Pd and Sn with interplanar lattice fringe spacing of 0.224 nm and 0.291 nm, respectively. Consistent with what spacing of (111) plane of rutile Pd and the spacing of plane (110) of Sn. The above results demonstrate that the prepared sample has high crystallinity, which makes the sample has good alkali resistance or acid resistance. Therefore, the catalyst may have excellent stability in the EOR

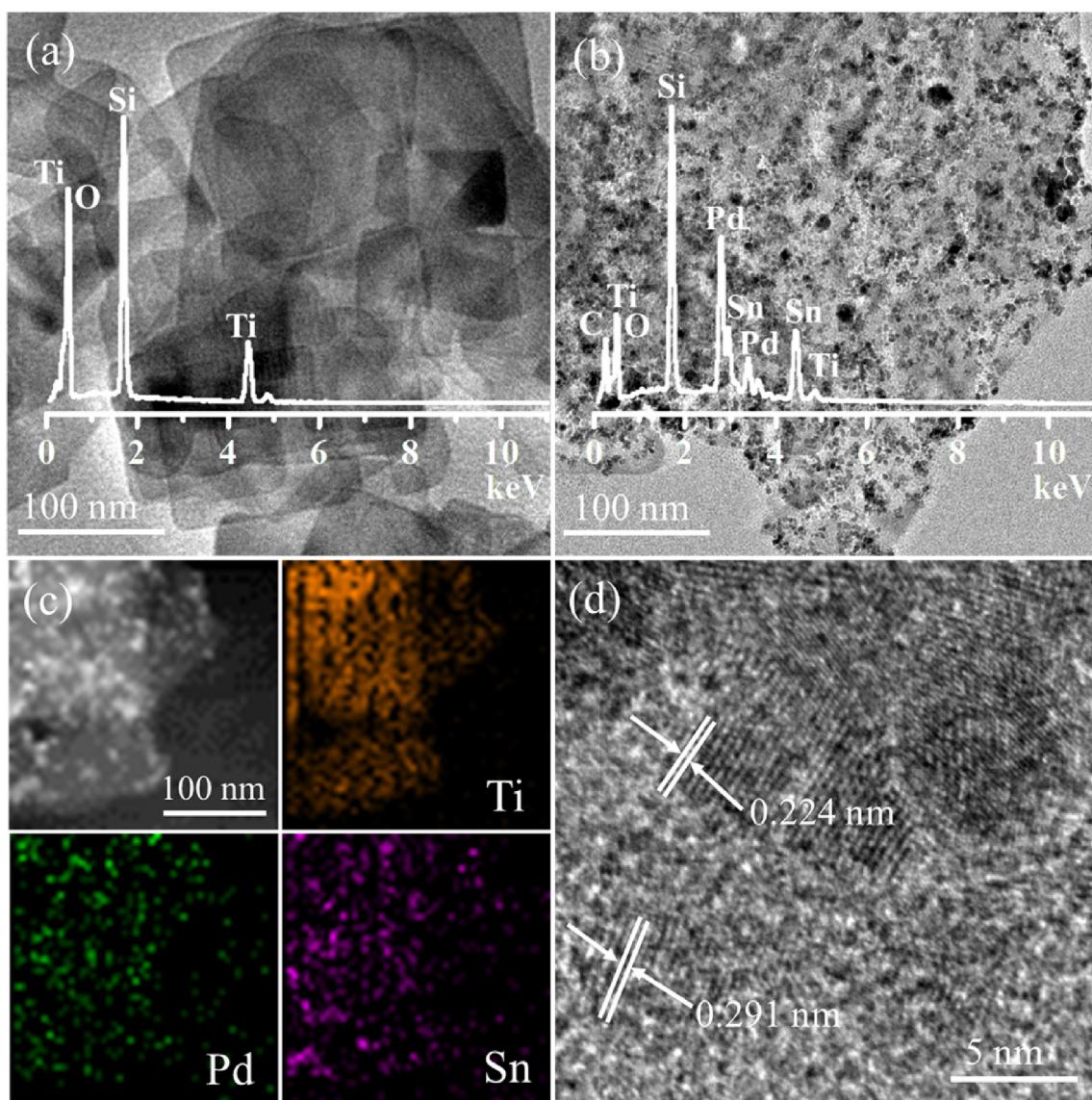


Fig. 2. TEM and EDX images of TiO₂ NSs (a), Pd–Sn/TiO₂ NSs (b), HAADF-STEM and EDX mapping images of Pd–Sn/TiO₂ NSs (c) and HRTEM images of Pd–Sn/TiO₂ NSs (Pd: Sn = 1 : 0.6) (d) with interplanar lattice fringe spacing.

[51,52].

3.2. XRD and XPS characterizations of catalysts

X-ray diffraction (XRD) pattern of the TiO_2 NSs (Fig. 3a) indicated the synthesized samples are crystallized and in a pure anatase phase. And a novel 2-dimension structure TiO_2 NSs can expose more active sites and have higher resistance CO poisoning ability [53,54]. Meanwhile, the XRD patterns of the prepared Pd–Sn/ TiO_2 NSs catalysts with different Pd/Sn atomic ratios and controlled samples. Among them, the $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs can be observed that all samples are fcc structure, the 2θ values of which are 40.1° , 46.6° , 68.1° , 82.1° and 86.6° , corresponding Pd crystal planes (JCPDS “card no.” 46–1043) [55]. Compared with the standard diffraction peaks, the binary of $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs shows slightly negative displacement, which indicates that Pd lattice is modified by adding Sn. And the (331) and (220) crystal planes of Pd were observed to become inconspicuous and almost disappear, which can be assigned to the insertion of Sn with the larger atomic radius into the Pd lattice. The lattice expansion indicates that there was the partial alloy forming between Pd and Sn. With the increase of Sn concentration in the catalysts, the decline of the lattice parameter reveals alloy formation between Pd and Sn owing to the partial substitution of Pd by Sn [56,57]. Meanwhile, the lattice parameters of Pd in the Pd–Sn/ TiO_2 NSs increased so that the diffraction peak had a negative deviation [58–61]. By comparing the XRD spectra of Pd/ TiO_2 NSs, Pd–Sn and Pd/C (JM), a slight decline of the lattice parameter of Pd can also be found, indicating there is partial alloy between Pd and Sn. However, there are no distinct diffraction peaks in regard to Sn or SnO_x appear in the XRD pattern, implying that the Sn exists in amorphous state. The peaks of the prepared Pd–Sn/ TiO_2 NSs did not shift significantly, which is consistent with the results in the literature [3,12], indicating that Pd

and Sn were jointly reduced and the partial alloy was formed in this experiment. Moreover, The metal interaction between Pd and Sn allows ordering effect to resist leaching of specific elements from the system and ensure the uniformity of active sites on the catalyst so that the catalyst have excellent stability [29,36]. At the same time, the crystallinity of the sample decreases because of the loading of Pd, which may reduce the catalytic activity and stability of $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs. By quantitative phase analysis, the suitable fitting atomic ratio of Pd/Sn is about 1.67%.

The surface components and valence states of the prepared Pd–Sn/ TiO_2 NSs were explored by XPS. The XPS wide scan spectra confirmed Pd (3d) and Sn (3d) along with SiO_2 , O (1s) and C (1s) (Fig. 3b). Only Pd (3d) and Sn (3d) were presented to emphasize and explain the surface chemistry.

Fig. 3c shows the regional states of the horizontal range of Pd 3d and Sn 3d of the prepared Pd–Sn/ TiO_2 NSs catalyst. The bond energies corresponding to the metal state of Pd in the Pd 3d_{5/2} orbital and Pd 3d_{3/2} orbital are 334.9 eV and 340.2 eV respectively. And the bond energies corresponding to the oxidation state of Pd are 335.6 eV and 340.9 eV, indicating that Pd elements mainly exist in the metal state in the prepared compounds. According to the integral area of the two valence states of Pd, the composition ratio of metallic Pd/oxidative Pd is about 1.5:1. Compared with pure Pd, the 3d peak of Pd has a positive shift (0.7 V) in $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs, in line with the charge transfer between Pd and Sn in the catalyst [16].

Fig. 3d shows that the two peaks at 486.7 eV and 495.2 eV correspond to Sn 3d_{5/2} and Sn 3d_{3/2} of the oxidation state, respectively. The two peaks at 485.8 eV and 494.3 eV correspond to the Sn 3d_{5/2} and Sn 3d_{3/2} metal orbitals, respectively. Hence, most of the Sn on the surface of $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs nanocomposite has been oxidized due to the oxophilic metal nature of the Sn atoms [33]. It is obvious that Sn element mainly exists on the surface of $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs in the form of oxygen-containing species where

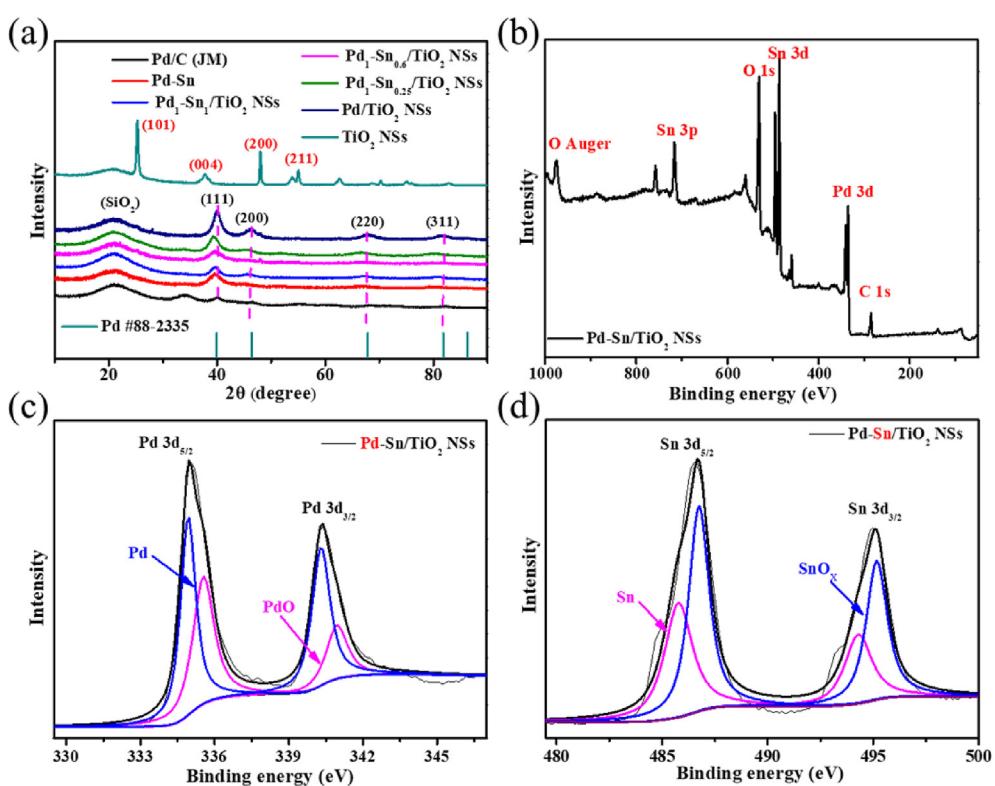


Fig. 3. (a) XRD patterns of $\text{Pd}_1\text{Sn}_x/\text{TiO}_2$ NSs and control samples, (b) Pd–Sn/ TiO_2 NSs, (c) Pd 3d and (d) Sn 3d XPS spectra of the Pd–Sn/ TiO_2 NSs nanocomposites.

Sn plays an important role in the oxidation of CO ads to CO_2 and acetaldehyde to acetic acid [2,13]. Therefore, the charge transfer interaction between Pd and Sn significantly changes the electronic state of the Pd atom, which may enhance the electrocatalytic activity and stability.

3.3. Electrochemical characterization

Fig. 4a shows the typical CVs of $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs (with different atomic ratios) and Pd/C (JM, wt%_{Pd} = 50%) which were obtained between -0.8 and 0.6 V. The activation peak of water on Pd surface occurred at the -0.5 V, and in this way the oxygen species were produced [16]. For $\text{Pd}_1\text{-Sn}_{0.25}/\text{TiO}_2$ NSs, $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs, $\text{Pd}_1\text{-Sn}_1/\text{TiO}_2$ NSs and Pd/C catalysts, the activation peaks of water

appeared at -0.3, -0.37, -0.23 and -0.33 V, respectively. The potential has an obvious peak value between -0.6 ~ -0.2 V, which is caused by the reduction of PdO to Pd [38,42]. Furthermore, results show that all peak values of $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs were more negative than that of Pd/C (JM), which is mainly put down to the fact that the activation process to generate OH^- oxidation adsorption CO requires a high potential on Pd. Moreover, the potential of $\text{Pd-Sn}/\text{TiO}_2$ NSs slightly ascent to positive than that of Pd/TiO_2 NSs, Pd-Sn and Pd-Sn/C catalysts (**Fig. S4a**) which is put down to charge transfer for the synergistic effect between Sn and TiO_2 NSs. Compared with Pd-Sn and Pd-Sn/C , the PdO reduction potential of Pd/TiO_2 NSs is lower. This phenomenon indicates that TiO_2 NSs bring about more significant improvement on the catalytic performance in contrast with oxophilic Sn.

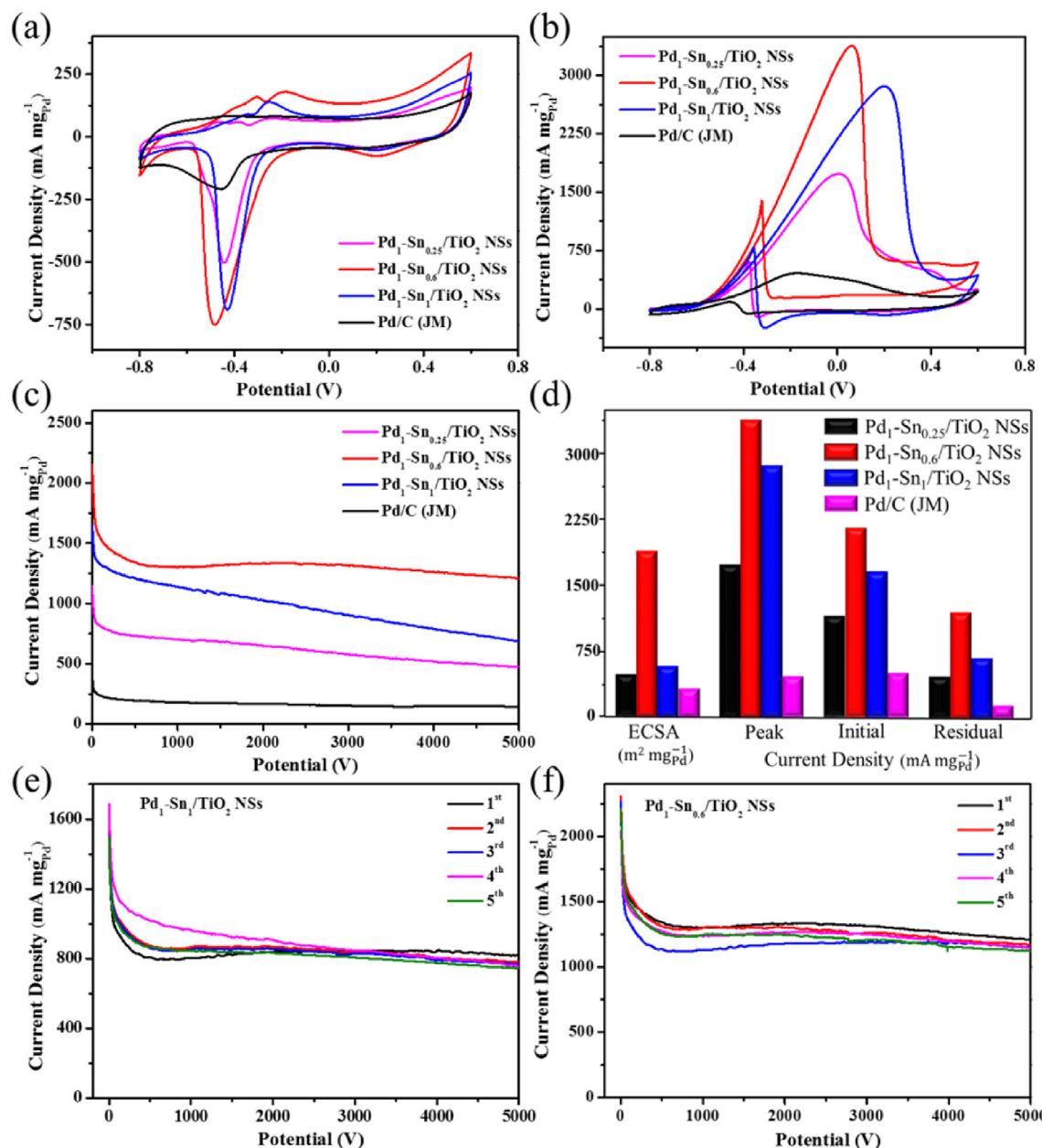
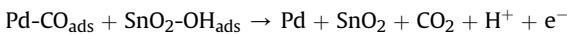
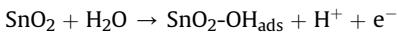
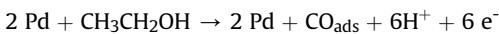


Fig. 4. CV of $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs and Pd/C (JM) measured in 1 M NaOH (a) and 1 M NaOH + 1 M $\text{C}_2\text{H}_5\text{OH}$ (b) at a scan rate of 50 mV s⁻¹. (c) CA of $\text{Pd}_1\text{-Sn}_x/\text{TiO}_2$ NSs and Pd/C (JM) measured in 1 M NaOH + 1 M $\text{C}_2\text{H}_5\text{OH}$ at -0.2 V vs. Ag/AgCl. (d) The detailed data of ECSA, Peak Current Density, Initial, and Residual Current Density after 5000 s test for $\text{Pd}_1\text{-Sn}_{0.25}/\text{TiO}_2$ NSs, $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs, $\text{Pd}_1\text{-Sn}_1/\text{TiO}_2$ NSs and Pd/C (JM). (e) $\text{Pd}_1\text{-Sn}_1/\text{TiO}_2$ NSs and (f) $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs catalysts obtained in 1 M NaOH + 1 M $\text{C}_2\text{H}_5\text{OH}$ at -0.2 V vs. Ag/AgCl.

To verify that the amendment of Pd–Sn on TiO₂ NSs provided more active sites for EOR, the electrochemical active surface area (ECSA) of Pd was calculated from the reduction peak region of PdO [62]. The ECSA values of Pd₁–Sn_{0.25}/TiO₂ NSs, Pd₁–Sn_{0.6}/TiO₂ NSs, Pd₁–Sn₁/TiO₂ NSs and Pd/C (JM) catalysts are 478.6, 1887.2, 578.75 and 327.12 mA mg_{Pd}⁻¹, respectively. The results are as the following sequence: Pd₁–Sn_{0.6}/TiO₂ NSs > Pd₁–Sn₁/TiO₂ NSs > Pd₁–Sn_{0.25}/TiO₂ NSs > Pd/C (JM). The ESCA values indicate that the Pd/Sn loading ratio has a certain influence on the electrocatalytic performance. The ECSA of Pd₁–Sn_{0.6}/TiO₂ NSs is much larger than Pd/TiO₂ NSs, Pd–Sn and Pd–Sn/C, clearly confirming the strong interaction of Pd–Sn nanoparticles and TiO₂ NSs. Adding Sn can make CO oxidize to CO₂ in Pd–Sn/TiO₂ NSs which has high CO anti-poisoning in the kinetic process of EOR. Besides, a suitable proportion between Pd and Sn in the catalysts is also important. Combining elemental mapping and ECSA analysis, the Sn NPs have been uniformly distributed around Pd, which is formed for the bi-functional effect between Pd and Sn [16,46,63,64]. Sn reduces the oxidation potential of the provided OH_{ads} group to remove the CO_{ads} in the adsorption state by the following pathway [11,33,65]:



Thus, the electronic effect of Pd and Sn could enhance the catalytic activity of Pd–Sn/TiO₂ NSs catalysts.

Fig. 4b exhibits CV curves of the Pd₁–Sn_x/TiO₂ NSs and Pd/C (JM) tested in an N₂-saturated 1.0 M NaOH + 1.0 M C₂H₅OH solution. Two typical characteristic peaks can be seen from the CV curves. A significant peak is observed in -0.2–0.4 V, and another peak is observed in -0.1–0.2 V, showing the oxidation capacity of ethanol

to acetate. The electrochemical activity of the Pd₁–Sn_x/TiO₂ NSs is higher than that of commercial Pd/C (JM). Notably, the peak current density of Pd₁–Sn_{0.6}/TiO₂ NSs, Pd₁–Sn₁/TiO₂ NSs and Pd₁–Sn_{0.25}/TiO₂ NSs are approximately 3381, 2862, 1735 mA mg_{Pd}⁻¹, respectively, which are 7.3, 6.2 and 3.8 times than that of Pd/C (JM) (458 mA mg_{Pd}⁻¹). In addition, the Pd₁–Sn_{0.6}/TiO₂ NSs is much higher than that of Pd/TiO₂ NSs (483 mA mg_{Pd}⁻¹), Pd–Sn (446.5 mA mg_{Pd}⁻¹) and Pd₁–Sn_{0.6}/C (331.8 mA mg_{Pd}⁻¹) (Fig. S4b), implying that the existence of Sn and TiO₂ NSs could boost the catalytic activity toward EOR. Actually, the TiO₂ NSs can provide enough specific surface area and activity sites so that Pd–Sn nanoparticles can be uniformly anchored on 2D-nanostructured TiO₂ NSs. Furthermore, the onset potential is similar to that of CO oxidation, demonstrating that the second peak is due to the oxidative desorption of the unoxidized intermediate products [66–68]. The catalytic activity of Pd₁–Sn_{0.6}/TiO₂ NSs was evaluated by the CV test (Figs. S2a–b). The current density of Pd₁–Sn_{0.6}/TiO₂ NSs increased gradually during the initial few cycles of scanning due to the fresh catalyst possesses abundant active sites for EOR. After 40 cycles of scanning, the current density still showed up trend, indicating the catalytic activity and durable stability was enhanced.

The stability test of Pd₁–Sn_x/TiO₂ NSs and Pd/C (JM) is performed by chronoamperometry (CA). The initial current density (Fig. 4c) of the prepared Pd–Sn/TiO₂ NSs catalyst was much higher than that of Pd/C (JM), because Pd–Sn/TiO₂ NSs expose plentiful active sites in the initial stage. Moreover, the activity of the prepared Pd–Sn/TiO₂ NSs catalyst still kept at a high level after the 5000 s I-t test. In 0–40 s, the abundant exposed active sites resulted in a high initial current density. In 40–500 s, the rapid descent of the current density is ascribed to an increasing ratio of CO_{ads} and oxygen donating species in the few seconds [3,58].

Among them, the Sn on the prepared Pd₁–Sn_{0.6}/TiO₂ NSs catalyst can enhance the anti-poisoning ability to the intermediate medium such as CO due to the electronic effect, thus promoting the

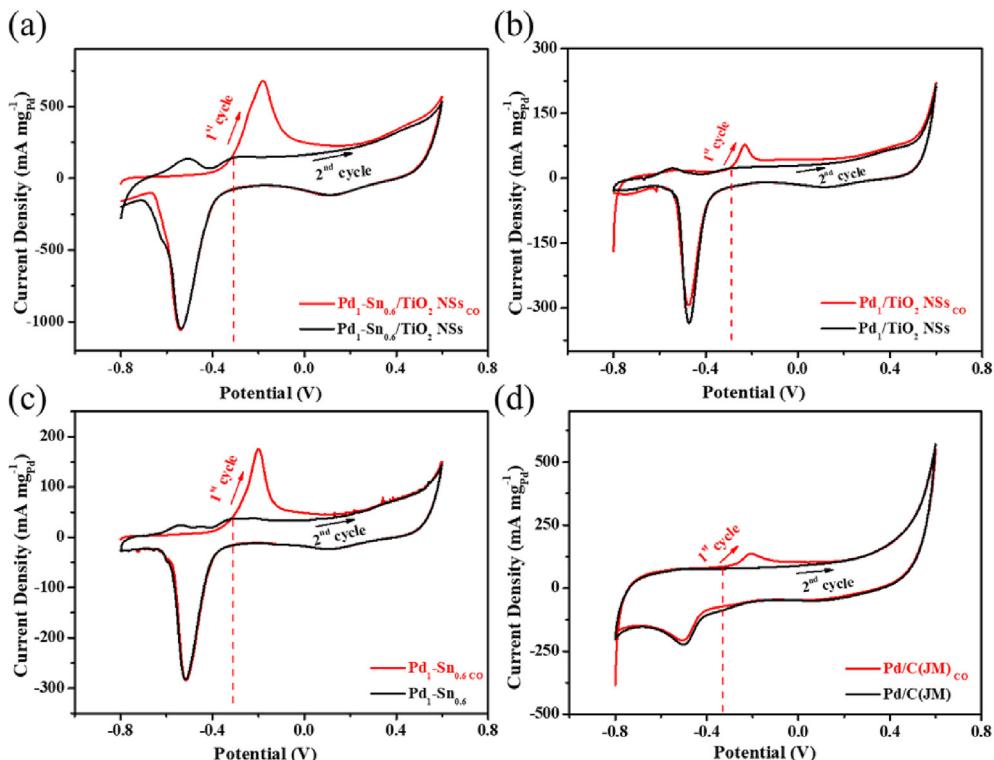


Fig. 5. CO stripping curves of Pd₁–Sn_{0.6}/TiO₂ NSs catalysts (a), Pd/TiO₂ NSs (b), Pd–Sn (c) and Pd/C (d) in 1 M NaOH.

kinetics of ethanol oxidation [12,53]. Meanwhile, Fig. 4d shows the residual current density of $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs, $\text{Pd}_1\text{-Sn}_1/\text{TiO}_2$ NSs and $\text{Pd}_1\text{-Sn}_{0.25}/\text{TiO}_2$ NSs are 1207, 685 and 472 $\text{mA mg}_{\text{Pd}}^{-1}$, which are 8.5, 4.8 and 3.3 times than that of Pd/C (JM) (142 $\text{mA mg}_{\text{Pd}}^{-1}$), respectively. After the 5000 s durability test, the partially deactivated catalysts, such as $\text{Pd}_1\text{-Sn}_1/\text{TiO}_2$ NSs (Fig. 4e) and $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs (Fig. 4f) could be easily reactivated with several CV cycles in 1.0 M NaOH. It is found that the current density can still be maintained at a high level. Due to the sample in the alkaline solution eliminates the carbonaceous species absorbed on Pd surface, the active sites can be re-exposed and the aggregation of NPs and the dissolution of Pd in the NaOH solution. The performance of $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs decay only 20% after 300 consecutive sweeps of CVs (Fig. S3) although the catalyst have been kept in the air for 7 months. It proves in further that the $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs have the good long-term cycle stabilities of catalysts.

In addition, it can be seen clearly in (Figs. S4c–d) that the residual current of $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs is much greater than that of Pd-Sn , Pd/C (JM) and Pd-Sn/C . The reaction activity of the catalyst can be adjusted by changing the preparation conditions such as the metal loading and the carrier. It is clear that the crystal lattice surface (001) of TiO_2 NSs affects the catalyst performance from the analysis above. And the interface effect is formed on the crystal lattice surface (001), which greatly improves the stability and activity of the catalyst [8,69].

During process of ethanol electrooxidation on the surface of the catalyst, the CO_{ads} affects the mass activity and long-term stability of the catalyst. To further explore the anti-poisoning ability of catalyst, CO stripping voltammograms of $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs catalysts are plotted in Fig. 5a. Evidently, the CO oxidation peaks of the $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs at about -0.32 V to -0.15 V during the first CV scan cycle can be attributed to the adsorbed CO (CO_{ads}) on catalyst [58,70]. Subsequently, the second CVs go with by the vanishing of CO oxidation peaks due to the removal of adsorbed CO (CO_{ads}). The anti-poisoning ability of CO can be seen from the peak sharpness and the area of the oxidation peak of CO [3]. So it is not hard to find in Fig. 5a–d that $\text{Pd}_1\text{-Sn}_{0.6}/\text{TiO}_2$ NSs > Pd/TiO_2 NSs > Pd-Sn > Pd/C (JM). Moreover, Pd/TiO_2 NSs (Fig. 5b) and Pd-Sn (Fig. 5c) were compared with Pd/C (JM) (Fig. 5d) in the CO stripping voltammetry indicating the harder exclusion of CO_{ads} on Pd/TiO_2 NSs and Pd-Sn . This could be concluded that the combination of Pd and Sn can decrease the initial potential of the catalyst reaction and the oxidation of adsorbed CO. These results indicated that the addition of Sn may alleviate the CO poisoning of Pd-based electrocatalysts. At the same time, the TiO_2 NSs catalyst carrier has a great promoting effect on the anti-CO poisoning ability. The main function of the carrier is to provide enough active sites, so that Pd and Sn can play an important catalytic role in DEFC.

4. Conclusions

In summary, Pd-Sn/TiO_2 NSs catalyst with high activity for EOR was successfully synthesized by chemical reduction method. Pd-Sn/TiO_2 NSs nano-catalyst has good activity and durability, mainly because of the electronic effect between Sn and Pd and the fact that TiO_2 NSs (001) surface provides enough active sites for the metals to be loaded on uniformly. Meanwhile, the current density of the catalytic oxidation activity of Pd-Sn/TiO_2 NSs was 7.2 times than that of Pd/C (JM), and the residual current density (1207 $\text{mA mg}_{\text{Pd}}^{-1}$) was 8.5 times higher than that of Pd/C (JM) (142 $\text{mA mg}_{\text{Pd}}^{-1}$) after the 5000 s I-t test. At the same time, the prepared catalyst showed excellent CO anti-poisoning ability towards EOR. All the results show that Pd-Sn/TiO_2 NSs is a promising electrocatalyst with superior performance for DEFCs.

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Appendix A. Supplementary data

Supplementary data to this article can be found online at <https://doi.org/10.1016/j.electacta.2019.134588>.

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